

PECFIVED

ະລິສ 200

January 18, 2000

149462.A1.RP

ZUUU

GRANTS MANAGEMENT

CH2M HILL

1620 W. Fountainhead Parkway

Suite 550

Tempe, AZ

85282-1843

P.O. Box 28440

Tempe, AZ

85285-8440

Tel 602.966.8188

Fax 602.966.9450

Proud Sponsor of

National Engineers Week 2000

Mr. Robert Jurenka, P.E.
Grants and Cooperative Agreements Officer's Technical Representative
Stop D-8230
Bureau of Reclamation
Denver Federal Center
Building 67 at 7th Street
Denver, CO 80225

Dear Bob: ...

Subject: Transmittal of Final Technical Report

On behalf of the City of McAllen, Texas and in accordance with the Cooperative Agreement No. 98FC810073 entitled "Demonstation Testing of ZenoGem and Reverse Osmosis for Indirect Potable Water Reuse – City of McAllen, Texas", please find enclosed five (5) bound copies of the Final Technical Report, one unbound copy, and an electronic copy on compact disk in Word 97 format.

Sincerely,

CH2M HILL

Principal Investigator

Enclosures:

Final Technical Report (5 bound copies; 1 unbound copy)

Compact Disk

Cc:

Bart Hines/City of McAllen

Frank Oudkirk/EPRI Bud Clark/C&SWS Bill Hoffman/TWDB

Doreen Benson/ZENON Environmental Systems

Mike Anglea/CH2M HILL/SAN Angie Fernandez/CH2M HILL/PHX Glen Daigger/CH2M HILL/DEN



RECEIVED

MAR 0 3 2000

TWDB R&PF GFANTS MANAGEMENT CH2M HILL

1620 W. Fountainhead Parkway

Suite 550

Tempe, AZ

85282-1843

P.O. Box 28440

Tempe, AZ

85285-8440

Tel 480.966.8188

Fax 480.966.9450

Proud Sponsor of

National Engineers Week 2000

February 29, 2000

149462.A1.RP

Mr. Robert Jurenka, P.E.
Grants and Cooperative Agreements Officer's Technical Representative
Stop D-8230
Bureau of Reclamation
Denver Federal Center
Building 67 at 7th Street
Denver, CO 80225

Dear Bob:

Subject:

Transmittal of Final Technical Report Addendum

Cooperative Agreement No. 98FC810073

On behalf of the City of McAllen, please find enclosed an addendum to the Desalination Research and Development Program Report No. 51, Final Technical Report for *Demonstration Testing of ZenoGem and Reverse Osmosis for Indirect Potable Reuse-City of McAllen, Texas.* Copies of all draft and final report comments are included in this addendum. All comments were either previously incorporated into the final report as appropriate or are enclosed for incorporation. Please replace Page 4-5, Section 6, and Appendix I in each copy of report previously furnished.

Sincerely,

CH2M HILL

Jim Lozier, P.E.

Principal Investigator

Enclosures:

Addendum

OF REPORT	OF THIS PAGE I IT	UP ABSIRAGI TIT		tπ
17. SECURITY CLASSIFICATION	18. SECURITY CLASSIFICATION	19. SECURITY CLASSIFICATION OF ABSTRACT		28. LIMITATION OF ARSTRACT
membrane technology; indirect		,		16. PRICE COBE
14. SUBJECT TERMS wastewater reclamation; McAlle	en. Texas: ZenoGem: ZeeWeed	reverse osmosis: microfiltra	tion:	15, NUMBER OF PAGES
Available from the National Ter 5285 Port Royal Road, Springfi This study involved demonstrat to reclaim the City of McAllen' demonstration testing objective drinking water regulations, (2) of to control of membrane fouling processed by composite RO me MBR/RO system. The results swhile meeting the City's current filtrate that meets all drinking water tends of the control of the city's current filtrate that meets all drinking water tends.	chnical Information Service, Opeld, Virginia 22161 ion-scale testing of an integrated smunicipal wastewater to a quastic include: (1) demonstration that demonstrate reliable operation of through automatic cleaning, (3) mbranes with minimal fouling, a howed that (1) the ZenoGem protowastewater effluent discharge in the service of the	I membrane bioreactor (MBI lity suitable for use as a new at RO product water meets al f the MBR on screened, degr demonstrate the MBR filtrat and (4) develop estimates of ocess is capable of producing requirements, and (2) the RO	R)/reverse drinking v I federal p ritted sewa te (RO fee capital and g a filtrate	water supply. The rimary and State secondary age, particularly with respect dwater) can be efficiently disperating costs for a suitable for RO treatment capable of producing a anings.
11. SUPPLEMENTARY NOTES				
P.O. Box 25007 Denver, Colorado 80225-0007				
Bureau of Reclamation Denver Federal Center			AGENCY REP	ORT NUMBER
9. SPONSORING/MONITORING AGENCY NAM	E(S) AND ADDRESS(ES)		10. SPONSOI	RIME/MONITORING
CH2M HILL 1620 W. Fountainhead Parkway Tempe, Arizona 85282-1843	, Suite 550			tion Research and ment Program Report No. 51
7. PERFORMING ORGANIZATION NAME(S) AN	# WBOUF32(F2)			INE SEGANIZATION
Jim C. Lozier and Angela M. Fe	······································			
Demonstration Testing of Zeno of McAllen, Texas 8. AUTHOR(S)	Gem and Reverse Osmosis for I	ndirect Potable Reuse, City		,
4. TITLE AND SUBTITLE			5. FUNDING	HUMBERS
1. AGENCY USE ONLY (Loave Blank)	January 2000	3. REPORT TYPE AND DATES Final	COVERED	
Public reporting burden for this collection of in maintaining the data needed, and completing ar suggestions for reducing this burden to Washing and to the Office of Management and Budget.	formation is estimated to average 1 hour per re dd reviewing the collection of information. Send fron Headquarters Services. Directorate for Info aperwork Reduction Report (0704-0188), Wasi	comments regarding this burden estimate or mation Operations and Reports, 1215 Je nington DC 20503.	nstructions, sea or any other asp offerson Davis H	arching existing data sources, gathering and ect of this collection of information, including
REPORT DOCUMENTATION	N PAGE			orm Approved MB No. 0704-0188

NSN 7546-81-280-5500

Standard Form 298 (Rev. 2-88)

Prescribed by ARSI Std. 239-18 298-102 Mr. Robert Jurenka, P.E. Page 2 February 29, 2000

Cc: Bart Hines/City of McAllen

Frank Oudkirk/EPRI Bud Clark/C&SWS John Sutton/TWDB

Doreen Benson/ZENON Environmental Systems

Mike Anglea/CH2M HILL/SAN
Angie Fernandez/CH2M HILL/PHX
Glen Daigger/CH2M HILL/DEN
Brock McEwen/CH2M HILL/DEN
Paul Mueller/CH2M HILL/CVO
Bob Bergman/CH2M HILL/GNV
George Crawford/CH2M HILL/TOR

Fair Miller/CH2M HILL/PHX

DEMONSTATION TESTING OF ZENOGEM AND REVERSE OSMOSIS FOR INDIRECT POTABLE REUSE

FINAL TECHNICAL REPORT

City of McAllen, TX

by

James C. Lozier, P.E. and Angela M. Fernandez, E.I.T CH2M HILL

Cooperative Assistance Agreement No. 98-FC-81-0073

Desalination Research and Development Program Report No. 51

January 2000

U.S. DEPARTMENT OF THE INTERIOR
Bureau of Reclamation
Technical Service Center
Water Treatment Engineering and Research Group

Mission Statements

U.S. Department of the Interior

The mission of the Department of the Interior is to protect and provide access to our Nation's natural and cultural heritage and honor out trust responsibilities to tribes.

Bureau of Reclamation

The mission of the Bureau of Reclamation is to manage, develop, and protect water and related resources in an environmentally and economically sound manner in the interest of the American public.

Federal Disclaimer

The information contained in this report regarding commercial products of firms may not be used for advertising or promotional purposes and is not to be construed as an endorsement of any product or firm by the Bureau of Reclamation.

The information contained in this report was developed for the Bureau of Reclamation: no warranty as to the accuracy, usefulness, or completeness is expressed or implied.

Researcher Acknowledgments

The authors would like to thank the Bureau of Reclamation (Bob Jurenka, Michelle Chapman-Wilbert, and Kim Linton), Texas Water Development Board (Bill Hoffman), Electric Power Research Institute (Frank Oudkirk), and Central and Southwest Energy Services (Bud Clark and Lance Orner) for sponsoring this research.

The authors would also like to thank the City of McAllen, Texas, specifically: Bart Hines, Public Utility Manager, and his Board for their financial and management support; Joe Ibarra, Rey Palomo, Henry Perez and Javier Hinojosa and others at the South WWTP for their assistance in construction, operation, and maintenance of the demonstration plant facilities; and Rosie Villarreal, Ramon Trevino, David Garcia, Juan Morales and their respective staff for sample analysis.

Researcher Disclaimer

The information contained in this report regarding the performance of tested commercial products and the conclusions and recommendations drawn regarding such performance are based on testing conducted on wastewater sources from the City of McAllen, Texas, and are not to be considered an indication of the performance of such products on other water sources either at McAllen, Texas, or at other locations.

Bureau Point of Contact

The Bureau of Reclamation's Water Reuse Task Manager for this work is Robert Jurenka. He can be reached in Denver at (303) 445-2254.

Contents

Sect	ion		Page
1	Intro	oduction and Background	1-1
	1.1	Indirect Potable Reuse—Definition and History	
	1.2	The Need for Indirect Potable Reuse for the City of McAllen	
	1.3	Water Quality Considerations and Proposed Treatment Strategy	
	1.4	Membrane Technologies in Indirect Potable Reuse	
	1.5	Conclusions	
		1.5.1 ZenoGem System	
		1.5.2 RO System	
	1.6	Recommendations for Further Research	
		1.6.1 Membrane Bioreactors	1-9
		1.6.2 Reverse Osmosis	
2	Test	ing Objectives	2-1
3	Dem	onstration Plant Facilities	
	3.1	Raw Water Supply, Abstraction, Pumping, and Screening	3-1
	3.2	ZenoGem Treatment System	
		3.2.1 Methods to Control ZeeWeed Membrane Fouling	3-3
		3.2.2 Permeate Storage, Disinfection, and Pumping	3-4
		3.2.3 ZenoGem Operation	3-4
	3.3	RO Treatment System	3-5
		3.3.1 RO Feedwater Characterization	3-6
		3.3.2 RO Feedwater Pretreatment to Control Membrane Fouling	3-7
	3.4	Criteria for Treatment System Operation	
4	Test	ing Approach	
	4.1	ZenoGem Treatment System Tasks	
	4.2	RO Treatment System Tasks	
	4.3	Additional Testing Activities	
		4.3.1 RO Feedwater Characterization	4-3
		4.3.2 IPR Characterization	4-3
		4.3.3 RO Concentrate and WWTP Effluent Characterization	4-4
		4.3.4 RO Integrity Testing	4-4
	4.4	Treatment System Monitoring	4 - 5
		4.4.1 Operator Training	
		4.4.2 Sampling and Analysis	4-5
	4.5	Data Evaluation	4-8
		4.5.1 Filtrate Flow and Membrane Flux	
		4.5.2 Transmembrane Pressure and Permeability	4-9
		4.5.3 Turbidity and SDI	

	ion	Page
5	Demonstration Testing Results	5-1
	5.1 Operations	5-1
	5.1.1 Startup Activities	5-3
	5.1.2 Operating Stages	
	5.2 ZenoGem Testing Results	
	5.2.1 ZenoGem Operating Conditions	
	5.2.2 ZeeWeed Membrane Performance	
	5.2.3 ZenoGem Biological Treatment Performance	
	5.2.4 ZenoGem Water Quality Impacts	
	5.3 RO Testing Results	
	5.3.1 RO Feedwater Quality	
	5.3.2 RO Operating Conditions/Membrane Performance	
	5.3.3 RO Water Quality Impacts	
	5.4 Impacts of IPR on Waste Discharges	
	5.5 Comparing Reclaimed and Existing Raw Water Quality	
6	Cost Estimates Using ZenoGem, ZeeWeed, and RO Facilities	6-1
	6.1 Cost Assumptions	6-3
	6.2 Cost Estimates	6-3
7	References	7-1
TABI	LES	_
TAB]		
3.1	Results of RO Feedwater Characterization	3-6
3.1 3.2	Results of RO Feedwater Characterization Operating Criteria for the ZenoGem System	3-6 3-8
3.1 3.2 3.3	Results of RO Feedwater Characterization Operating Criteria for the ZenoGem System Biological Treatment Performance Criteria for the ZenoGem System	3-6 3-8 m3-9
3.1 3.2 3.3 3.4	Results of RO Feedwater Characterization Operating Criteria for the ZenoGem System Biological Treatment Performance Criteria for the ZenoGem System	3-6 3-8 m3-9 3-9
3.1 3.2 3.3 3.4	Results of RO Feedwater Characterization	3-6 3-8 m3-9 3-9 e ZenoGem
3.1 3.2 3.3 3.4 4.1	Results of RO Feedwater Characterization	3-63-8 m3-9 e ZenoGem
3.1 3.2 3.3 3.4 4.1	Results of RO Feedwater Characterization	3-63-8 m3-9 e ZenoGem4-6
3.1 3.2 3.3 3.4 4.1 4.2 5.1	Results of RO Feedwater Characterization	3-63-8 m3-9 e ZenoGem4-64-8
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5 5.6	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5 5.6	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5 5.6 5.7 5.8 5.9	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5 5.6	Results of RO Feedwater Characterization	
3.1 3.2 3.3 3.4 4.1 4.2 5.1 5.2 5.3 5.4 5.5 5.6 5.7 5.8 5.9	Results of RO Feedwater Characterization	

TABLES CONT.

5.13 5.14	Average Membrane Performance Parameters for the RO System	5-41 5-47
5.15	Comparative Loading of Critical Contaminants to Arroyo Colorado/ Laguna Madre	
5.16	Results of ZenoGem and RO Permeate Sampling for IPR Characterization	5-51 5-54
6.1	Order of Magnitude Cost Estimate for The ZenoGem and RO Alternative	6-4
6.2	Order of Magnitude Cost Estimate for the ZeeWeed and RO Alternative	6-4 6-6
6.3	Design Criteria Assumptions for the ZenoGem, ZeeWeed and RO Systems	
EXHI	BITS	
5.1	ZenoGem Operating Stages	5-4
5.2	RO Operating Stages	5-6
5.3	Wastewater Discharge Characterization	
FIGU	RES	
3.1	Demonstration Plant Feedwater Abstraction Point from WWTP No. 2	3-1
3.2	ZenoGem Treatment System Process Flow Diagram	3-2
3.3	RO Treatment System Process Flow Diagram	
6.1	Existing WWTP Schematic	
6.2	ZenoGem Membrane Bioreactor and RO Facilities	
6.3	Conventional WWTP with ZeeWeed and RO Facilities	6-2
ZenoC	Gem System	
5.1	Permeate Flowrate and Membrane Flux vs. Run Time	5-13
5.2	Transmembrane Pressure and Permeate Flowrate vs. Run Time	
5.3	Normalized Membrane Permeability and Transmembrane Pressure vs.	
	Run Time	5-14
5.4	Hydraulic Residence Time vs. Run Time	
5.5	Solids Retention Time vs. Run Time	
5.6	Mixed Liquor Suspended Solids vs. Run Time	5-19
5. <i>7</i>	Mixed Liquor Volatile Suspended Solids vs. Run Time	
5.8	Dissolved Oxygen vs. Run Time	
5.9	Oxygen Uptake Rate vs. Run Time	
5.10	Total Suspended Solids vs. Run Time	
5.11	5-Day Carbonaceous Biochemical Oxygen Demand vs. Run Time	
5.12	Chemical Oxygen Demand vs. Run Time	
5.13	Permeate Turbidity vs. Run Time	
5.14	Permeate Total and Fecal Coliforms vs. Run Time	
5.15	Ammonia Nitrogen vs. Run Time	
5.16	Percent Ammonia Nitrogen Removal vs. Run Time	
5.17	Nitrite/Nitrate Nitrogen vs. Run Time	
5.18	Total Nitrogen vs. Run Time	
5.19	Percent Total Nitrogen Removal vs. Run Time	

FIGURES CONT.

5.20 5.21 5.22 5.23	Percer Total I	nity vs. Run Time
RO Sy	stem	
5.24		lity vs. Run Time5-38
5.25		ensity Index vs. Run Time5-38
5.26		Pressure vs. Run Time5-40
5.27		rane Flux vs. Run Time5-42
5.28	Norma	alized Product Flow and Salt Passage vs. Run Time5-42
5.29	Pressu	re Drop vs. Run Time5-44
5.30	Stage :	1 Pressure Drop Coefficient vs. Run Time5-44
5.31	Total I	Dissolved Solids vs. Run Time5-49
5.32	Total (Organic Carbon vs. Run Time5-49
APPE	NDICE	s
Appen	dix A	Photographs of Demonstration Plant Facilities and Associated Equipment
Appen		RO Projections
Appen		ZenoGem and RO Operating and Water Quality Data
Appen		Laboratory Reports
Appen		RO Spent Cleaning Solution Analysis
Appen		ZenoGem Permeate Ion Analysis
Appen		RO Element Autopsy
Appen		ZENON Budget Proposals
Appen		ZenoGem and ZeeWeed Cost Comparison
Appen	idix J	RO Integrity Testing

Acronyms and Abbreviations

ACOE Army Corps of Engineers

ALK alkalinity

ASL Applied Sciences Laboratory bio-P biological phosphorus

BOD biochemical oxygen demand BOR Bureau of Reclamation

C celsius

CBOD₅ carbonaceous biochemical oxygen demand

cfm cubic feet per minute
CFU colony forming units

CIP clean in place

COD chemical oxygen demand CST capillary suction time

CSWS Central and Southwest Services

DO dissolved oxygen

DSVI diluted sludge volume index
EPA Environmental Protection Agency
EPRI Electric Power Research Institute

ft² square feet g/L grams per liter

GAC granular activated carbon gfd gallons per square foot per day

gpd gallons per day gpm gallons per minute HAA haloacetic acid

HPC heterotrophic plate count
HRT hyraulic residence time
I&C instrumentation and controls

in Hg inches of mercury
IPR indirect potable reuse
KLT King Lee Technologies
MBR membrane bioreactor

MCL maximum contaminant level
MF microfiltration

mg/L milligrams per liter
mgd million gallons per day

mL milliliters
ML million liters

MLSS mixed liquor suspended solids

MLVSS mixed liquor volatile suspended solids

mm millimeter N nitrogen

NH₃-N ammonia nitrogen

NPF normalized product flow
NTU nephelometric turbidity unit
O&M operations and maintenance

OUR oxygen uptake rate

P phosphorus

pCi/L picoCuries per liter
PDC pressure drop coefficient
PLC programmable logic controller

ppm parts per million

psi pounds per square inch

psig pounds per square inch gauge

RO reverse osmosis

scfm standard cubic feet per minute

SDI silt density index

SDS screened degritted sewage SDWA Safe Drinking Water Act

SI solubility index
SRT solids retention time
TDS total dissolved solids
THM trihalomethane

TKN total Kjeldahl nitrogen transmembrane pressure

TN total nitrogen

TNRCC Texas Natural Resources Conservation Committee

TOC total organic carbon
TP total phosphorus
TSS total suspended solids

TWDB Texas Water Development Board

UF ultrafiltration

UOSA Upper Occoquan Sewage Authority

UV ultraviolet

μg/L micrograms per liter

μm microns

μS/cm microSiemens per centimeter
WWTP wastewater treatment plant

Introduction and Background

This report documents wastewater reclamation demonstration testing performed at the McAllen, Texas, wastewater treatment plant (WWTP) No. 2. The study was conducted under Task D: Water Recycling and Reuse of the U.S. Bureau of Reclamation's (BOR) Desalination Research and Development Program. The Program sponsors this research in an effort to lower the cost of treatment technologies. Testing was conducted from February 1999 to October 1999.

The results of previous pilot testing conducted for the City of McAllen (*Water Treatment Technology Program Report No. 26*) concluded that treating the City's wastewater with a membrane bioreactor (MBR) system (ZenoGem) followed by reverse osmosis (RO) and final disinfection (chlorination or ultraviolet [UV] light) may provide for a simpler, potentially less costly, treatment process for the reclamation of a portion of the City's wastewater to supplement current water supplies obtained from the Rio Grande River. The reclaimed water produced by the MBR/RO/disinfection process would in most respects contain significantly lower concentrations of most substances currently regulated under the Safe Drinking Water Act (SDWA), and as such, could improve the inorganic quality of the Rio Grande River water. However, unlike microfiltration (MF), which has been used extensively for RO pretreatment of secondary effluent, no testing has been reported on the use of the ZenoGem process to convert wastewater directly to RO feedwater for the purpose of producing a high quality effluent suitable for indirect potable reuse.

The purpose of this study was threefold: 1) to demonstrate the long-term operability and reliability of the ZenoGem system, 2) demonstrate the feasibility of RO treatment of ZenoGem permeate for the production of reclaimed water, and 3) determine if the MBR/RO process has operational, cost, and water quality benefits compared to the conventional WWTP/MF/RO in the context of indirect potable reuse (IPR).

This section addresses the following information:

- Defines indirect potable reuse.
- Explains the City of McAllen's motivations for considering implementation of indirect potable reuse to help solve their water supply problems.
- Describes the regulatory issues associated with implementation, and explains the reasons membrane processes, in particular MF/ultrafiltration (UF) and RO, are integral to its implementation.
- Presents conclusions and recommendations from this study.

1.1 Indirect Potable Reuse—Definition and History

Indirect potable reuse is the recovery of water from wastewater for the purposeful reintroduction into either a surface water or groundwater body that ultimately serves as a drinking water supply. Unplanned IPR has been occurring since humans first began disposing of wastewater into watersheds that are hydrologically connected to raw water supplies. Planned IPR began in the U.S. in the 1960s. A summary of some of the major milestones in the development of potable reuse as a viable component of a water resource management plan is presented below.

The Whittier Narrows Groundwater Replenishment Project, California. In 1962, the County Sanitation Districts of Los Angeles began spreading disinfected secondary effluent from a 10-million-gallon-per-day (mgd) (37.9 million liters [ML]/day) water reclamation plant to an underground potable water supply. The reclaimed water accounts for an annual average of 16 percent of the total inflow to the groundwater basin. The local population is estimated to be exposed to from 0 to 23 percent reclaimed water. An independent scientific advisory panel to the State of California conducted an extensive review of the project data and concluded that the Whittier Narrows Groundwater Replenishment Project was as safe as commonly used surface water supplies.

Orange County, California, Water District. Since 1976, the Orange County, California, Water District's Water Factory 21 has been reclaiming unchlorinated secondary effluent to drinking water quality and recharging it into a heavily used groundwater source to prevent salt water intrusion. The water recovery treatment facility is a 15-mgd (56.8 ML/day) facility that includes lime clarification, air stripping, recarbonation, filtration, carbon adsorption, slip-stream RO, and disinfection. It is estimated that less than 5 percent of the domestic water supply is comprised of the recovered water. The Orange County Water District has not identified any significant risk to users of the groundwater from the indirect potable reuse practice.

Upper Occoquan Sewage Authority Water Reclamation Plant, Virginia. In 1978, the 15-mgd Upper Occoquan Sewage Authority (UOSA) Water Reclamation Plant in northern Virginia began reclaiming wastewater for subsequent discharge to the Occoquan Reservoir. This reservoir is a critical source of drinking water for approximately 1 million people. The reclaimed water has accounted for as much as 90 percent of the flow into the reservoir. Treatment includes primary treatment, secondary treatment, biological nitrification, lime clarification and recarbonation, filtration, activated carbon adsorption, and disinfection. The plant has been expanded to 26 mgd (98.4 ML/day) and will be further expanded to 54 mgd (204 ML/day) by the year 2000. No negative health effects have been attributed to the plant or effluent discharges.

Potomac Estuary Experimental Water Treatment Plant, Washington, D.C. From 1981 to 1983, the 1-mgd (3.8 ML/day) Potomac Estuary Experimental Water Treatment Plant was operated with an influent blend of Potomac Estuary water and nitrified secondary effluent. The blend was designed to simulate influent water quality expected during drought conditions when up to 50 percent of the estuary flow may comprise treated wastewater. Treatment included aeration, coagulation, clarification, pre-disinfection, filtration, carbon adsorption, and post-disinfection. An independent panel reviewed the extensive testing performed by the U.S. Army Corps of Engineers (ACOE) and concluded that the advanced treatment could recover water from a highly contaminated source similar in quality to three major water supplies for the Washington, D.C., metropolitan area.

San Diego Total Resource Recovery Project, California. In 1983, a 1-mgd potable water recovery demonstration facility was commissioned as part of a total resource recovery

program established in San Diego, California. The purpose of the treatment system was to reclaim raw water from raw wastewater. The system included primary treatment, a water hyacinth aquaculture system, coagulation, clarification, filtration, UV disinfection, RO, aeration, carbon adsorption, and disinfection. An extensive chronic toxicity risk analysis showed that the risk associated with use of the recovered water as a raw water supply was less than or equal to the use of the existing raw water entering the City's Miramar Water Treatment Plant. The City is now planning to reclaim up to 20 mgd (75.7 ML/day) of secondary effluent for augmentation of their 90,000 acrefoot San Vicente Reservoir for eventual distribution to water customers.

El Paso, Texas, Fred Hervey Water Reclamation Plant. The 10-mgd (37.9 ML/day) Fred Hervey Water Reclamation Plant began operation in El Paso, Texas, in 1985. The recovered water is recharged to the Hueco Bolson drinking water aquifer where, over a 2-year period, the water travels to one of El Paso's potable water wellfields to become part of the potable water supply. The treatment system includes primary treatment, activated sludge/powdered activated carbon treatment, lime treatment, recarbonation, filtration, ozonation, and granular activated carbon (GAC) adsorption. Although no negative health effects have been correlated with the reuse practice, an increase in the total dissolved solids (TDS) content of the aquifer has occurred because the increased pumping has lowered the aquifer level to the higher salinity water source. Slip-stream demineralization will be included in future plant expansions to address the TDS issue.

Tampa Water Resource Recovery Project, Florida. The City of Tampa's Water Resource Recovery Pilot Plant began operation in 1986 with the purpose of evaluating the feasibility of reclaiming denitrified secondary effluent to a quality suitable for blending with existing surface water and groundwater sources for indirect potable reuse. Several treatments were evaluated, and one was selected for health effects testing. This treatment system consisted of aeration, high pH lime clarification, recarbonation, filtration, GAC adsorption, and ozonation. The results of the health effects testing coupled with the microbiological and chemical analyses performed during the evaluation indicated that the quality of the reuse water was equivalent to or exceeded the quality of the local raw water supply. The City of Tampa intends to develop a 20- to 50-mgd (189 ML/day) water resource recovery plant in the near future.

West Basin Water Recycling Program, California. From 1990 through 1995, the West Basin Municipal Water District conceived, designed, constructed, and began operation of the West Basin Water Recycling Program. This program includes reclaiming 5 mgd (18.9 ML/day) (expandable to 20 mgd, or 75.7 ML/day) of secondary effluent from the City of Los Angeles' Hyperion Treatment Plant for injection into the West Coast Basin Barrier Project. The West Coast Basin Barrier Project has historically received an average of 20 mgd of potable water for injection into the coastal reaches of local South Bay aquifers for mitigation of saltwater intrusion. Substituting reclaimed water for the potable water provides substantially greater water use efficiency in the area. Reclamation treatment includes predecarbonation, lime clarification, recarbonation, filtration, RO, postdecarbonation, and final disinfection. Based on hydrogeologic investigation and modeling of the West Coast Basin, it is anticipated that the reclaimed water will improve groundwater quality along the Barrier because of the high quality of the reclaimed water relative to the imported water and the native groundwater.

Reedy Creek Improvement District, Advanced Water Reclamation Program, Florida. In 1992, the Reedy Creek Improvement District began a pilot program to reduce phosphorus (P) and nitrogen (N) in the effluent from their WWTP to very low levels. Although the goal of treatment was not IPR, this was the first project to evaluate the feasibility of using MF and UF as a replacement to lime clarification, recarbonation, and gravity filtration for RO pretreatment. This approach was shown to be so effective that MF and UF have displaced lime treatment as the preferred means of RO pretreatment on subsequent IPR projects.

City of Scottsdale, Arizona, Water Campus Project. In 1994, the City of Scottsdale began pilot testing MF and RO for the purpose of reclaiming wastewater for groundwater recharge. The testing program, which has culminated in a 6.8-mgd (25.7 ML/day) IPR project currently under construction at the City's Water Campus site, represents the first planned IPR project in Arizona. During periods when demand for non-potable reclaimed water is low, product water from the MF/RO system will be blended with filtered surface water and injected into a potable aquifer using dry wells. The 6.8-mgd facility represents the first phase of a multi-year project designed to have an ultimate capacity of 25 mgd (94.6 ML/day).

City of San Diego, California, Water Repurification Project. As an outgrowth of their Total Resource Recovery Project, the City of San Diego began the Repurification Project to reclaim up to 20 mgd of wastewater for indirect potable use. The program is currently evaluating the feasibility of using the following advanced water treatment processes to re-purify tertiary effluent from the City's new North City Water Reclamation Plant to a quality suitable for direct discharge to the San Vicente Reservoir, one of the City's main raw water reservoirs: MF/UF, RO, ion exchange, and ozonation. The project represents the first surface supply augmentation IPR project in California and must satisfy stringent California Department of Health Services requirements regarding virus removal and real-time monitoring of individual processes for pathogen removal. If successful, the project will result in the construction of the largest IPR plant in the U.S.

1.2 The Need for Indirect Potable Reuse for the City of McAllen

The City of McAllen, Texas, is located in the Lower Rio Grande Valley near the United States-Mexico border, approximately 40 miles upstream from the mouth of the Rio Grande River. The City presently derives its water supply from water rights in the Rio Grande River that it shares with multiple parties, including other cities, water supply corporations, irrigation districts, and Mexico. The Lower Rio Grande Valley is a growing area with an existing water shortage problem. The Texas Water Development Board (TWDB) reports that all surface water resources in the area are 100 percent appropriated. Additionally, this semi-arid area often experiences drought conditions. Projected growth in population and water use indicates that the demand for potable water will exceed the City's authorized water rights by the year 2003. Consequently, alternative water supply strategies are necessary to ensure a safe, reliable source of potable water.

The two most feasible alternative sources are groundwater and re-purified wastewater. Many of the groundwater supplies in the Lower Rio Grande Valley have an elevated

dissolved solids concentration and require demineralization by RO or electrodialysis to make them suitable for potable use. Consequently, wastewater reclamation is considered by the City to be a desirable means of augmenting its water supply.

1.3 Water Quality Considerations and Proposed Treatment Strategy

In general, reclaimed water should be treated to a level where its quality exceeds that of the historical water supply. In Texas, public heath issues related to the use of reclaimed water fall under the purview of the Texas Natural Resources Conservation Commission (TNRCC). The preliminary requirements of the TNRCC with respect to IPR for the City are: 1) reclaimed water must be of equal or better quality than that of the City's current water supply, and 2) RO must be used to treat all of the reclaimed water prior to its reuse. Based on these requirements and in view of the City's desire to reduce the dissolved solids of its finished water to improve consumer acceptability, the following IPR treatment sequence was proposed for the City in 1997 and subsequently demonstrated via testing conducted in that year and reported in *Water Treatment Technology Program Report No.* 26:

- · Primary and secondary treatment
- Chlorine disinfection
- MF/UF
- RO
- UV disinfection

This sequence not only satisfies the TNRCC's preliminary requirements, it also provides multiple treatment barriers to the passage of microbial, inorganic, and organic contaminants in the wastewater. The concept of "multiple barriers" has been adopted by the water supply industry to achieve the appropriate level of safety and reliability by providing redundant treatment steps for the removal of wastewater contaminants, primarily pathogens.

1.4 Membrane Technologies in Indirect Potable Reuse

A primary focus of one task of BOR's Desalination Research and Development Program is research on membrane processes for wastewater reclamation. In this context, three membrane processes (MF, UF, and RO) represent key treatment processes in the proposed treatment sequence for IPR at McAllen. RO has been applied for wastewater reclamation for more than two decades and is considered a proven treatment process. RO serves as the "workhorse" for the IPR process because it is efficient in removing nearly all contaminants of public health concern. Cost-effective RO operation on municipal wastewater requires a high degree of preliminary treatment to control membrane fouling. Such treatment is provided through the use of MF/UF to polish secondary effluent.

During the last 5 years, MF has been shown at demonstration- and full-scale to be a reliable process in the context of IPR. Production MF facilities are currently in operation in California and Arizona with additional facilities planned for Pennsylvania, Virginia,

and Georgia. UF technologies have also been demonstrated for the same purpose; however, to date none have been implemented full-scale. All of the MF/UF products at these sites have employed pressure modules.

During the 1997 pilot study at McAllen, pressurized MF was demonstrated for the treatment of effluent from the City's south WWTP using Memcor MF technology. At that time, a novel, immersed MF product (ZeeWeed) was tested and found to provide performance competitive with or somewhat superior to the pressurized MF approach. In addition, ZeeWeed was also evaluated in the context of a membrane bioreactor process (ZenoGem) and found to be feasible for direct treatment of the City's screened, degritted wastewater. Preliminary results indicated that the ZenoGem filtrate was of equivalent quality to both Memcor and ZeeWeed filtrate with respect to general water quality (TDS, total organic carbon [TOC], coliforms, and turbidity) but had significantly higher RO feedwater colloidal fouling potential (as measured by silt density index [SDI]). Longer term testing of ZenoGem coupled with a follow-on RO system was recommended at that time and is the subject of this research.

1.5 Conclusions

Conclusions drawn from the results of this study are presented below.

1.5.1 ZenoGem System

- The ZenoGem membrane bioreactor process successfully treated screened, degritted sewage (SDS) to a quality suitable for RO processing.
- The ZenoGem process produced a permeate (see Tables 5.8 through 5.10) that exceeded the City's effluent discharge requirements for carbonaceous biochemical oxygen demand (CBOD₅<10 milligrams per liter [mg/L]), total suspended solids (TSS <15 mg/L)), and ammonia nitrogen (NH₃-N <3 mg/L). This result was attained at all mixed liquor suspended solids (MLSS) concentrations and with both membrane types.</p>
- The ZeeWeed OKC MF (0.4-micrometer [μm] pore size) membrane exhibited higher sustained permeability than OCP UF (0.035-μm pore size) membrane at high MLSS levels (13 grams per liter [g/L]).
- Permeability of the MF membrane was sensitive to MLSS level. Permeability was stable at 10 g/L but declined at 13 g/L because of increased membrane fouling not adequately controlled by frequent permeate backpulsing or maintenance cleans.
- At an MLSS concentration of 13 g/L, simultaneous nitrification/denitrification and biological phosphorus (bio-P) removal occurred most likely because of the inability to completely transfer oxygen from the bulk liquid to the interior of the bioflocs at the hydraulic residence time (HRT) selected for this study (5.7 hours). The oxygen transfer limitations inhibited complete nitrification but promoted nitrogen removal.

- At an MLSS concentration of 10 g/L, the rate of oxygen transfer was sufficient to maintain complete nitrification and suppress denitrification and bio-P uptake.
- Flow peaking tests (i.e., permeate flowrate increased for a specific duration of time) were conducted over a 24-hour period to simulate the types of peak loading conditions that typically occur in a conventional WWTP. However, peaking significantly increased the rate of permeability decline and accelerated the fouling rate (fouling not reversed by backpulsing or maintenance cleans as defined in Section 3.2.1). As a result, normal diurnal variations in wastewater flow, in which peak hourly flows can equal 300 percent of average daily flow, must be dampened through flow equalization so that the ZenoGem process can operate at more or less a constant hydraulic loading (flux) rate.
- Intermittent aeration (i.e., air cycled at 15 minutes on/15 minutes off) to the aeration tank (at 6 g/L MLSS concentration) produced the greatest degree of total nitrogen removal (optimum simultaneous nitrification and denitrification).
- With respect to RO feedwater quality, ZenoGem permeate quality consistently exceeded goals for turbidity and SDI, and generally exceeded goals for bacterial concentrations.
- Per Table 5.16, compared to the City's existing raw water source, the ZenoGem permeate was of lesser quality with respect to TOC and many inorganic contaminants while the RO permeate was of better quality in nearly all respects.
- Coliform removal by the both membranes was less than 100 percent. MF membrane
 permeate contained significantly greater coliform concentrations at 13 g/L MLSS
 concentration than the UF membrane. Furthermore, coliform removal appeared to be
 a function of MLSS loading for the MF membrane. However, the RO system
 consistently removed any remaining coliform regardless of the MF or UF
 pretreatment.
- Cycled aeration to the membrane tank appeared to significantly increase the rate of membrane fouling (permeability decline) compared with continuous aeration.
 However, it is difficult to draw firm conclusions regarding aeration given the brief operating time with cycled aeration and its use in combination with other operating modifications (flow peaking, cycled aeration to the aeration tank).
- Footprint for ZenoGem facilities represents about 32 percent of the total area required for a conventional activated sludge plant providing comparable biological treatment and flow equalization.

1.5.2 RO System

- Membrane fouling by particulates and soluble organics in the screened, degritted wastewater was well controlled by the ZenoGem process as illustrated by stable first stage flux and salt rejection. Continuous disinfection, in the predominant form of monochloramine, with a low concentration of combined chlorine (approximately 1 mg/L) was effective in preventing biological fouling of the RO membranes as measured by stability of first stage feed/concentrate differential pressure (see Tables 5.12 through 5.14).
- Elevated concentrations of calcium and phosphate in the City's wastewater (and ZenoGem permeate) most likely caused precipitation of the calcium phosphate salt, hydroxyapatite, in the RO system second stage at feedwater pH levels designed to control calcium carbonate scaling. This precipitation caused rapid increases in RO feed pressures, rapid declines in normalized product flow, and marked increases in salt passage. The precipitate was readily dissolved using citric acid cleaning, and performance declines were consistently reversed by such cleanings. Further acidification of the RO feedwater to pH 5.0 (concentrate pH to 5.6) prevented such precipitation except at design (80 percent) recovery. A better control method may be to precipitate the majority of the soluble phosphorus in the wastewater during MBR treatment using a ferric or aluminum coagulant.
- RO permeate at design (80 percent) recovery was very high quality: TDS <75 mg/L, TOC <0.5 mg/L, and turbidity <0.1 nephelometric turbidity units (NTU). Levels of these and other contaminants monitored for in the RO permeate were significantly less than the maximum concentrations permitted under federal drinking water regulations or indirect potable reuse guidelines established in certain states (e.g., California and Virginia). The exception being coliforms, which were consistently detected at low levels. From this standpoint, the RO permeate is of satisfactory quality for IPR use subject to additional disinfection (chlorination or UV). TNRCC has not established guidelines or regulations for IPR use at McAllen, however, their preliminary position is that RO treatment would be required. On the other hand, TNRCC may consider establishing quality requirements for IPR that use the quality of the existing raw water supply as the benchmark for treatment. In this case, it may be possible that an acceptable quality of reclaimed water can be produced through a blend or ZenoGem and RO permeate with post-disinfection.

1.6 Recommendations for Further Research

The following recommendations are provided with respect to further research involving MBRs and RO in the context of indirect potable reuse.

1.6.1 Membrane Bioreactors

1.6.1.1 MLSS Levels and Membrane Flux

This research illustrated that membrane fouling and permeability is sensitive to MLSS level. Further research is needed to define the optimum combination of these two parameters (MLSS level/membrane flux) as they contribute to both capital and operating cost. Increased MLSS levels permit higher solids retention times (SRTs), reducing sludge yield, however their use may result in higher capital costs and operating costs associated with additional membrane area (reduced flux).

1.6.1.2 Cycled Aeration to Promote Nitrification/Denitrification

Optimize conditions of cycled aeration for the purpose of promoting simultaneous nitrification/denitrification. Testing in this study was conducted at only one on/off cycle (15 minutes on, 15 minutes off) to the aeration tank. No water quality parameters were measured at other cycles to determine if control at other cycles may be more efficient at achieving improved or complete nitrogen removal. Control methods need to be developed in conjunction with such testing.

1.6.1.3 Cycled Aeration to Reduce Membrane Air Scour Requirements

Aeration for control of membrane fouling represents a significant operating (power) cost. Cycling of air to the coarse bubble aerator integral to the membrane module (membrane tank) represents one way to reduce operating cost; however, aeration reductions must not come at the detriment of membrane permeability. Testing is needed to determine optimum airflow rates and cycle times to achieve the optimum balance of these two needs.

1.6.1.4 Alternative MBR Designs

This research tested one MBR product, Zenon Environmental System's ZenoGem using a MF membrane module. Other MBR products are available and have been installed for municipal wastewater reclamation both in Europe and Japan. Testing of these products is needed to assess their performance relative to ZenoGem and to determine if such products represent competitive technologies for application in the U.S. IPR and wastewater treatment market.

The BOR is currently funding research by Montgomery Watson and the City of San Diego to compare the performance of ZenoGem and Mitsubishi systems. Also, the ZenoGem UF system should be retested at 10 g/L and 6 g/L for comparison to the MF system at these concentrations.

1.6.2 Reverse Osmosis

1.6.2.1 Scale Control

For wastewaters containing elevated concentrations of calcium and phosphate, additional research is needed to determine the most cost-effective and operationally reliable means to control calcium phosphate scaling. Acidification has the advantages of low cost and typically being required for calcium carbonate scale control; however, its use to reduce pH to levels considered effective in this study (see Section 5.0) resulted in an aggressive RO permeate that was supersaturated with carbon dioxide (most likely requiring stripping). Ferric or aluminum coagulant addition to the MBR (or conventional plant) will reduce phosphorus levels in both the RO feedwater and concentrate. However, the doses required in the City's case (approximately 50 mg/L ferric chloride and 91 mg/L alum) produce additional solids in the MBR, potentially increasing membrane fouling and requiring acid maintenance cleans and reducing SRT for a given operating MLSS level.

1.6.2.2 Membrane Flux

RO testing in this study was performed at relatively low flux (10 to 11 gallons per square foot per day [gfd]). Given the low turbidity and SDI of the ZenoGem permeate, higher flux operation (reduced membrane capital cost) may be feasible if scale control can be resolved as discussed herein.

Testing Objectives

The research to be conducted under this program has the following objectives:

- 1. Demonstrate feasibility and benefits of the ZenoGem process:
 - Produce a high quality RO feedwater (i.e., turbidity <0.2 NTU, SDI <3, heterotrophic plate count [HPC] <500 colony forming units [CFU]/milliliter [mL]).
 - Meet the City's effluent discharge permit requirements (i.e., TSS <15 mg/L, CBOD₅ <10 mg/L, NH₃-N <3 mg/L).
 - Operate reliably (i.e., sustained production).
- 2. Demonstrate successful RO treatment on ZenoGem permeate:
 - Reliable operation with minimal fouling and effective membrane cleanings.
 - Meet all drinking water/reuse standards.
- 3. Define design and operation and maintenance (O&M) requirements to develop full-scale ZenoGem and RO plant design criteria.
- 4. Develop cost estimates for current and proposed IPR advanced treatment processes for the City of McAllen.
- 5. Characterize ZenoGem and RO permeates relative to the City's existing raw water supply (i.e., Rio Grande River) based on:
 - Regulated drinking water contaminants.
 - State of Texas secondary drinking water requirement of TDS for 1,000 mg/L.
- 6. Determine impacts of IPR on waste discharges to the City's current discharge location (i.e., Arroyo Colorado/Laguna Madre).

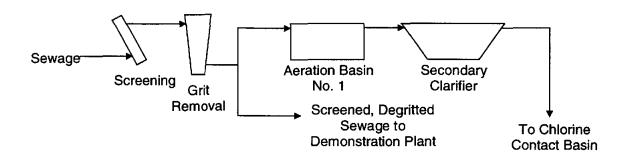
Demonstration Plant Facilities

The demonstration plant facilities consisted of ZenoGem (MBR) and RO treatment systems. The plant also contained ancillary equipment, including a raw water supply pump, chemical feed systems, transfer pump, and associated piping, valves, and fittings for delivery of raw water (i.e., ZenoGem feed), transfer of processed water (i.e., ZenoGem permeate/RO feed), and disposal of discharge flowstreams (i.e., ZenoGem sludge, RO concentrate, and RO permeate) and membrane cleaning solutions to the WWTP. A description of the other components of the demonstration plant facilities is presented in the following sections.

3.1 Raw Water Supply, Abstraction, Pumping, and Screening

The raw water source (feedwater) to the demonstration plant was SDS from the City's South WWTP No. 2. SDS was abstracted from the influent splitter box (located upstream of Aeration Basin No. 1) and transferred to the ZenoGem system via a submersible pump located in the splitter box. The abstraction point relative to the WWTP processes is shown in Figure 3.1.

FIGURE 3.1
Demonstration Plant Feedwater Abstraction Point from WWTP No. 2

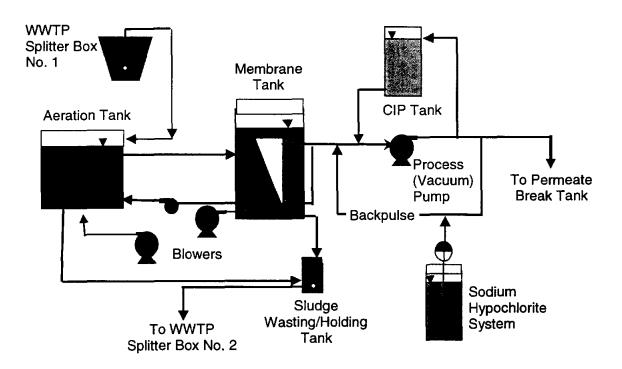


Raw water to the ZenoGem system was screened using a basket strainer and a 3-millimeter (mm) screen. Screening was necessary to prevent clogging of the inlet distributors of the membrane modules.

3.2 ZenoGem Treatment System

The ZenoGem treatment system is comprised of the following components: ZeeWeed Model MSTD ZW-4 unit, a 3,000-gallon aeration tank, auxiliary aeration blower, solids recirculation pump, and sludge wasting system (submersible pump located in aeration tank and 200-gallon calibrated sludge wasting/holding tank). The ZeeWeed unit consists of the following: 185-gallon tank containing the membrane module (membrane tank); one ZW-500 module containing 500 square feet (ft²) of hollow-fiber MF membrane with a nominal pore size of 0.4 microns (OKC membrane); permeate pump; membrane aeration blower; and backpulse/clean-in-place (CIP) tank. The ZeeWeed ZW-500 membrane module consists of loose fibers connected to a manifold rack system at either end, with the rack/fiber assembly suspended in the membrane tank and submerged in the mixed liquor. Treatment occurs when a vacuum of 1.5 to 9.0 pounds per square inch gage (psig) is applied to the filtrate side of the fibers using the process (vacuum) pump. The vacuum causes the water in the mixed liquor to flow from the feed side to filtrate side of the membrane in a direct filtration mode under a positive transmembrane pressure. A process flow diagram for the ZenoGem treatment system is shown in Figure 3.2. Photographs of the ZenoGem system are presented in Appendix A.

FIGURE 3.2
ZenoGem Treatment System Process Flow Diagram



¹During the commissioning stage of the testing (Stage A), a 0.035-micron UF (OCP) membrane module was installed in the membrane tank. This module was replaced with the 0.4-micron MF (OKC) membrane module to increase flow and reduce fouling.

During ZenoGem operation, biodegradable matter in the sewage (biochemical oxygen demand [BOD] and ammonia) is oxidized by the biomass maintained at high mixed liquor concentrations in the membrane and aeration tanks with air input to these tanks using coarse and fine bubble diffusers, respectively. MLSS levels and SRTs are maintained in the tanks through the frequency and volume of sludge wasted to a calibrated sludge wasting/holding tank. Waste sludge is returned to Splitter Box No. 2 using a submersible pump. The desired HRT is maintained by controlling the rate of permeate flow. Consistency of MLSS concentrations between membrane and aeration tanks is maintained by recirculating MLSS between the tanks using a submersible grinder pump located in the aeration tank.

3.2.1 Methods to Control ZeeWeed Membrane Fouling

Control of solids buildup on the outside surface of the membrane fibers and related increases in permeate side vacuum are achieved in three ways. First, a blower is used to provide continuous air input (in the form of coarse bubbles) at 25 to 30 standard cubic feet per minute (scfm) into the bottom of the membrane tank directly below the membrane fibers. The air bubbles flow upward between the vertically oriented fibers, causing the fibers to agitate against one another. This results in mechanical cleaning through air scour.

Secondly, filtration is interrupted every 10 minutes and the membrane fibers are backpulsed repeatedly for 15 seconds with permeate from the backpulse/CIP tank. The system remains on-line during backpulsing and is in a backpulse mode for a total of 36 minutes per day. Typically, a low concentration of chlorine (<5 parts per million [ppm]) is maintained in the backflush water to inactivate and remove microbes (primarily bacteria) that colonize the outer membrane surface. Hydraulic cleaning via backflushing is accomplished using discharge head from the process pump, and backwash water is retained in the membrane tank.

Thirdly, three times per week, a 100-ppm sodium hypochlorite solution is added to the backpulse/CIP tank, and the membrane module is backpulsed repeatedly for 45 minutes in a procedure called a "maintenance clean." After the 45-minute in situ cleaning, the system is flushed with permeate for 15 minutes. An additional permeate flush to drain is performed for 10 to 15 minutes to purge the system of free chlorine once permeation (i.e., vacuum applied to filtrate side of membrane module) is re-initiated. The total system downtime during a maintenance clean is about 75 minutes.

The combination of air scour, backpulsing, and maintenance cleaning may not be completely effective in controlling membrane fouling, and with time, the pressure differential across the membrane (transmembrane pressure [TMP]) may increase to a maximum of value approximately 17 inches of mercury. When this condition occurs, which is anticipated to be (>3 months) infrequently at full-scale application, the membrane module is chemically cleaned with a 1,500 to 2,000-ppm sodium hypochlorite solution in a procedure called a "recovery clean." Recovery cleaning requires in situ full tank soaking and clean water flux testing. The chemical cleaning dissolves and removes the refractory solids, and reduces TMP to "clean membrane" initial levels (i.e., levels at startup prior to any evidence of fouling).

3.2.2 Permeate Storage, Disinfection, and Pumping

The ZenoGem permeate flows from the ZeeWeed unit to a permeate break tank that serves to balance the intermittent flow of ZenoGem permeate (resulting from backpulsing and maintenance cleans) with the continuous feed flow requirement of the RO system. After the break tank and prior to entering the RO treatment system, the permeate is dosed with combined chlorine (in the predominant form of monochloramine) using a solution tank and metering pump. Combined chlorine is batched using sodium hypochlorite and aqueous ammonia. The dosage is based on maintaining at least 1 to 2 mg/L of total chlorine residual and zero free chlorine residual. The thin film composite RO membrane material is intolerant to free chlorine, and any exposure will reduce the membrane life. Combined chlorine serves to prevent the low levels of bacteria that can be present in the ZenoGem permeate (primarily through contamination) from growing in the RO feed piping and on the membrane elements (biofouling). The addition of combined chlorine is not intended to serve as disinfection to eliminate pathogens. The "disinfected" ZenoGem permeate is pumped from the break tank to the RO system using a transfer pump. Excess ZenoGem permeate overflows the break tank through drain piping.

3.2.3 ZenoGem Operation

The ZenoGem system is designed to operate at a constant flux with the TMP varying over time to maintain the design flux. The rate of filtrate discharge to the break tank is controlled to achieve the desired HRT in the membrane tank (bioreactor). Proper HRT control is required to achieve the desired degree of CBOD $_5$ and ammonia removal by the biomass maintained in the bioreactor. Solids buildup in the bioreactor is controlled through daily manual wasting to achieve the desired SRT (concentration of MLSS) in the bioreactor. Unlike a conventional WWTP that operates at MLSS levels of 2,000 to 3,000 mg/L, the ZenoGem process is designed to operate at MLSS levels of 10,000 to 15,000 mg/L. This allows for a higher organic loading of wastewater in the ZenoGem treatment system.

Three modes of operation were employed during the study:

- Normal Flow: Permeate flowrate maintained at 6.5 gallons per minute (gpm).
- Peak Flow: Permeate flowrate increased to 9.5 gpm for 6 hours over a 24-hour period.
- Cycled Aeration: Air cycled to membrane tank at 10 seconds on/10 seconds off with or without air cycled to aeration tank at 15 minutes on/15 minutes off.

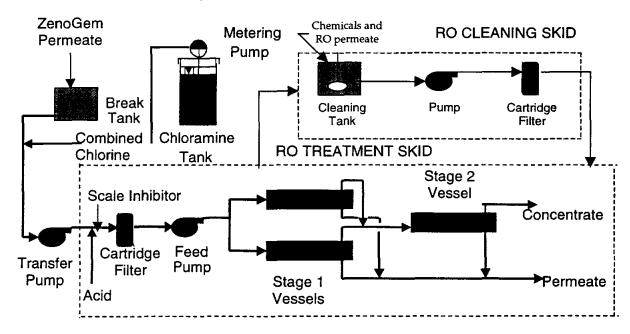
As detailed in Table 5.1, these operating modes are presented as specific operating events during ZenoGem operation.

3.3 RO Treatment System

The RO treatment system is comprised of the following components: a treatment skid and a cleaning skid. The treatment and cleaning skids are provided courtesy of the Bureau of Reclamation's Water Treatment Engineering and Research Group.

The RO treatment skid consists of the following equipment: chemical feed systems for the addition of acid and scale inhibitor, 5 micron cartridge filter, feed (high pressure) pump, two-stage pressure vessel array, programmable logic controller (PLC) and associated instruments and controls, piping, gauges, and valves. The cartridge filter serves as backup in the event of MF pretreatment failure. The RO elements, model LFC1-2540, are manufactured by Hydranautics and contain low fouling composite polyamide membranes. Stage 1 contains four pressure vessels each containing three 2.5-inch-diameter by 40-inch-long spiral wound elements in a "2:2" configuration. Stage 2 contains two pressure vessels of identical design plumbed in a "1:1" configuration. The two-stage array permits operation up to 80 percent recovery and simulates design of a full-scale RO plant using a "2:1" array with six-element vessels. A process flow diagram for the RO treatment skid and associated pretreatment equipment is shown in Figure 3.3. Photographs of the RO treatment system are presented in Appendix A.

FIGURE 3.3
RO Treatment System Process Flow Diagram



3.3.1 RO Feedwater Characterization

Three separate samples of unchlorinated secondary effluent (from the City's WWTP) were collected prior to the start of testing to estimate the inorganic quality of the RO feedwater. (The inorganic quality of the WWTP effluent was considered to be a good simulation of that produced by the ZenoGem system given that both were designed to operate on the same feedwater and provided the same degree of biological treatment and nitrification.) The results are shown in Table 3.1.

TABLE 3.1
Results of RO Feedwater Characterization

Parameter	Units	12/14/98	12/16/98	12/18/98	Average
Alkalinity	mg/L as CaCO₃	153	161	164	159
Bicarbonate	mg/L	187	196	200	194
Chloride	mg/L	388	359	378	375
Reactive Silica	mg/L	13.90	14.70	14.60	14.40
Sulfate	mg/L	327	305	332	321
Anion Sum	mg/L	1,069	1,036	1,089	1,064
Barium	µg/L	78.30	77.60	87.80	81.23
Calcium	µg/L	112,000	127,000	103,000	114,000
Magnesium	μg/L	29,100	29,700	26,800	28,533
otassium	μg/L	17,100	18,900	19,400	18,467
Sodium	μg/L	236,000	271,000	233,000	246,667
Strontium	μg/L	1,260	1,310	1,380	1,317
Cation Sum	μg/L	395,538	447,988	383,668	409,065
TDS (Sum of lons)	mg/L	1,465	1,484	1,473	1,473

The mean values were then used with two software programs, King Lee Technologies (KLT) WaterWizard and Hydranautics' RODesign, to develop feedwater chemical conditioning requirements and establish product water recovery of the RO system based on the presence and concentration of sparingly soluble salts. The program outputs, shown in Appendix B, indicated the following design condition:

- RO feedwater acidification to pH 6.8 (with sulfuric acid)
- RO feedwater dosing with scale inhibitor at 2 ppm (KLT PreTreat 0100)
- Product water recovery of 80 percent based on 53 times saturation of barium sulfate in the RO concentrate

This condition served as the basis for target operating criteria for the RO system.

3.3.2 RO Feedwater Pretreatment to Control Membrane Fouling

During extended operation, RO membrane elements are subject to fouling caused by both suspended and dissolved matter. Suspended matter includes organic and inorganic colloids and microorganisms. Sparingly soluble salts, such as carbonates, sulfates, and silica, can precipitate from solution because they are concentrated by the RO process. Suspended particles accumulate on the membrane surface causing biofouling and colloidal fouling, and can block feed channels thereby increasing the pressure drop across the system. These phenomenon reduce water permeability through the RO membranes causing flux decline and increased salt passage. The nature and rapidity of fouling depends on the condition of the feedwater. Fouling is progressive, and, if not controlled early, can impair the RO system performance in a relatively short time. For these reasons, fouling must be controlled.

Particulate fouling was addressed through the use of the ZeeWeed MF membrane. Scaling was controlled using acidification and scale inhibitor addition. Chloramines were batched and dosed into the RO feedwater to prevent biological growth (biofouling) on the membranes as discussed in Section 3.2.

The RO feedwater from the transfer pump enters the treatment skid where it is dosed with a scale inhibitor and sulfuric acid prior to entering the cartridge filter. The addition of scale inhibitor prohibits the precipitation of sulfate and carbonate scalants (specifically calcium carbonate and barium sulfate). KLT PreTreat 0100 was used for mineral precipitate control. Acidification further reduces the potential for calcium and carbonate to precipitate from solution. Sulfuric acid was used for feedwater pH control.

Chemically conditioned with King Lee PreTreat 0100 scale inhibitor and sulfuric acid, the filtered water is pumped to the RO vessels at a pressure needed to produce the design permeate flow. Target feedwater recovery is attained by adjustment of the concentrate flow control valve. The system operates in a constant permeate flow/constant recovery mode with feed pressure increasing to compensate for decreases in water mass transfer rate.

The combination of filtration, chloramination, scale inhibition, and acidification may not be completely effective in controlling membrane fouling, and with time, the pressure drop across the stages may increase with simultaneous decreases in permeate flowrate and feedwater recovery. Recirculating a citric acid solution (low pH cleaning) or an alkaline solution (high pH cleaning) containing a mixture of surfactant, detergent, and chelating agent from the cleaning skid through the RO vessels serves to chemically clean the RO system when fouling is apparent. Recirculation is coupled with soak periods to remove the membrane foulants and restore lost performance.

Cleaning was performed five times on the system throughout the study. Low pH cleanings using citric acid and sodium hydroxide (for pH adjustment) were performed to remove inorganic fouling, such as calcium precipitates (e.g., calcium carbonates and phosphates) and hydroxide precipitates (e.g., metal oxides such as ferric hydroxide). High pH cleanings using a caustic solution and sulfuric acid (for pH adjustment) were performed to remove calcium sulfates and organics.

3.4 Criteria for Treatment System Operation

Tables 3.2 and 3.3 present criteria that were established for operation and biological performance, respectively, of the ZenoGem system. Table 3.4 presents the initial operating criteria for the RO system based on RO feedwater analyses and projection results. These criteria reflect the individual manufacturer's experience with the systems. Some of the criteria were modified during the study to improve operability (i.e., reduce potential for membrane fouling) and biological treatment stability and performance. Detailed descriptions of the operating stages for each treatment system are presented in Section 5.1.

TABLE 3.2
Operating Criteria for the ZenoGem System

Parameter	Units	Target
Aeration Tank Air	scfm	45
Backpulse Duration	sec	15
Backpulse Frequency	min	10
Biomass Recirculation Rate	gpm	36
Flux	gfd	18.7/27.3ª
Membrane Tank Air	scfm	25/30 ^b
Permeability	gfd/psi	5°
Permeate Flowrate before Backpulse	gpm	6.5/9.5°
TMP	psi	2.5 - 8.5
Vacuum before Backpulse	in Hg	5.1 - 17.3

^aTarget value during flow peaking.

^bApplied rate increased to 30 scfm during intermittent aeration.

^cExpected value based on control variables.

TABLE 3.3Biological Treatment Performance Criteria for the ZenoGem System

		Target				
Parameter	Units	Stage A	Stage B	Stage C	Stage D	
DO	mg/L	> 1.5	> 1.5	> 1.5	> 1.5	
OUR	mg O₂/L-min	1.0 - 1.5	1.0 - 1.5	1.0 - 1.5	1.0 - 1.5	
MLSS	mg/L	13,000	13,000	10,000	6,000	
Sludge Wasted Daily	gals	90ª	90 ^a	110 ^a	150ª	
HRT	hrs	6.2	6.2	6.2	6.2	
SRT	days	25ª	25ª	20ª	15 ^a	

^aExpected value based on control variables.

TABLE 3.4Operating Criteria for the RO System

		Target				
Parameter	Units	Stage A	Stage B	Stage C	Stage D	
Acidified Feedwater pH		6.8	6.8	6.8	5.6ª	
Feedwater Flowrate	gpm	5	5	3	3 - 5	
Feedwater Recovery	%	80	80	50	50 - 80	
Permeate Flowrate	gpm	4	4	1.5	1.5 - 4.0	
Scale Inhibitor Dose	ppm	2	2	2	2	

^aSet target to concentrate pH during this stage (feedwater pH = 5.0).

Testing Approach

The demonstration testing program was divided into two phases:

- Phase I: Operation of ZenoGem treatment system for 1 month to establish stable biological treatment performance and permeate water quality.
- Phase II: Operation of ZenoGem and RO treatment systems for 5 months to demonstrate project goals and objectives.

The demonstration plant operated 24 hours per day, 7 days per week except for chemical cleanings or planned and unplanned maintenance. Equipment was supervised on an 8-hour per day, 5-day per week basis and as required on weekends to ensure proper operation and data collection. Operating data were recorded at the beginning and end of the each shift. Water quality samples were collected at the beginning of the shift. The results of Phase I and Phase II testing are discussed in Section 5.0.

4.1 ZenoGem Treatment System Tasks

The ZenoGem treatment system tasks under Phases I and II were to:

- 1. Operate ZenoGem system to produce a permeate whose quality complies with the City's discharge permit (TSS <15 mg/L; BOD <10 mg/L; NH₄-N <3 mg/L).
- 2. Characterize ZenoGem permeate relative to goals for RO feedwater quality, defined as follows:

Turbidity: < 0.2 NTU

• SDI: <3

Fecal coliforms: <1 CFU/100 milliliters (mL)

- 3. Characterize ZenoGem permeate relative to IPR water quality requirements and for development of RO feedwater design composition.
- 4. Measure O&M requirements for ZenoGem system (plant efficiency factor, labor hours required, energy consumption, and chemical and other consumable consumption); demonstrate reliable, long-term performance of the ZenoGem process; and develop criteria for design of full-scale ZenoGem system.
- 5. Develop information necessary for design of a full-scale ZenoGem plant. Design criteria to be developed as part of this task include the following:
 - HRT (at average and peak loading)
 - SRT
 - Aeration requirements, separately for maintenance of membrane flux (air scour) and for carbonaceous and nitrogenous removal

- Membrane flux rate
- Duration of operation between chemical cleanings
- Frequency and duration of backpulse
- Backpulse volume
- Chemical type and concentration (if any) needed in backpulse water
- Chemical cleaning regime, including chemical type(s) and concentration(s) and contact time to ensure maintenance of membrane
- Sludge production rate and characteristics to define and assess proper sludge handling, drying, and disposal
- 6. Evaluate the effect of flow peak testing (hydraulic peaking) on the ZenoGem process. The approach is to initially operate the ZenoGem process at a target SRT of 25 days and a HRT of approximately 6 hours to establish baseline performance. After a predetermined period of operation, the HRT will be decreased to about 4 hours. Following this change, system operation (membrane performance) will be monitored at the new HRT by tracking changes in TMP and permeability.
- 7. Evaluate the effect of intermittent aeration on operational (blower) costs and the ability to concurrently nitrify and denitrify in the ZenoGem process. This task includes cycled aeration to the membrane tank and aeration tank to determine the impacts on operational (blower) costs and biological nitrogen removal, respectively.

4.2 RO Treatment System Tasks

The RO treatment system tasks under Phases II were to:

- 1. Characterize RO permeate quality relative to IPR quality requirements.
- 2. Monitor RO system operating performance as measured by the following:
 - Feed and permeate conductivity
 - Feedwater recovery
 - Feed pressure
- Assess changes in RO membrane performance caused by fouling of RO membrane and elements and by chemical oxidation of RO membrane surface by monitoring the following parameters:
 - Normalized permeate flow
 - Normalized conductivity passage
 - Normalized vessel differential pressure
- 4. Perform chemical cleanings as required when normalized performance parameters change by a pre-determined amount. Assess the efficiency of one or more chemical cleaning formulations/regimes to restore RO performance losses.

- 5. Confirm RO membrane manufacturer's projections of attainable feedwater recovery and document RO feedwater chemical conditioning requirements to control mineral precipitation.
- 6. Confirm effectiveness of RO feedwater chloramination as a means to control biological fouling of RO membranes.
- 7. Develop information necessary for design of a full-scale RO plant. Design criteria to be developed as part of this task include the following:
 - Feedwater chemical conditioning
 - Feedwater biological monitoring requirements
 - Feedwater disinfection (chloramination)
 - Feedwater pressure
 - Membrane flux
 - Feedwater recovery
 - Membrane composition
 - Cleaning frequency and regime
 - Post-disinfection requirements

4.3 Additional Testing Activities

Prior to and during the operation of the demonstration plant, several additional activities were required and performed, including RO feedwater characterization, IPR characterization of the ZenoGem permeate and RO permeate, RO concentrate/WWTP effluent characterization, and RO integrity testing. These activities are described below.

4.3.1 RO Feedwater Characterization

Prior to testing, three sets of samples of unchlorinated secondary effluent from the South WWTP were collected to characterize the inorganic quality of the feedwater to the RO system. These analyses were required to estimate RO system operating conditions with respect to acid and scale inhibitor dosage and feedwater recovery. The samples were collected on December 14, 16, and 18, 1998, by the plant operating staff and analyzed by the CH2M HILL's Applied Sciences Laboratory (ASL). Results of these analyses were presented and discussed in Section 3.0.

4.3.2 IPR Characterization

The overall goal of IPR is to produce reclaimed water of suitable quality for supplementing McAllen's current raw water supply. Thus, it was desirable to characterize the quality of the raw water supply as part of this study to compare it with quality of reclaimed water produced by MF treatment (ZenoGem permeate) and by RO treatment (RO permeate).

Raw water characterization of McAllen's current raw water supply was conducted during the previous pilot testing. With respect to the demonstration plant, samples of ZenoGem permeate and RO permeate were collected on August 18 and September 14, 1999, respectively, by the plant operating staff and analyzed by ASL. Results of these analyses are presented and discussed in Section 5.0.

4.3.3 RO Concentrate and WWTP Effluent Characterization

RO will produce a waste stream (concentrate) containing elevated levels of most constituents present in the ZenoGem permeate, most notably TDS, TOC, and nutrients. Based on an assumed rejection of 90 percent for these constituents by RO and a feedwater recovery of 80 percent, the concentrate will contain TDS, TOC, and nutrients at four to five times their concentration in the ZenoGem permeate. It is anticipated that the RO concentrate will be disposed of by blending it with that portion of the South WWTP secondary effluent that is not reclaimed for IPR. This secondary effluent discharge point, the Arroyo Colorado, which flows into the Laguna Madre, a marine lagoon. Low freshwater inflows and variable salinity characterize the Arroyo Colorado-Laguna Madre system, which has TDS ranging from 3,000 to 10,000 mg/L. It is anticipated that TDS levels of the concentrate/effluent blend (which will be between 1,200 and 7,500 mg/L) will not adversely impact the ecology of the Arroyo Colorado-Laguna Madre system; however, there is concern that elevated nutrient concentrations in the blend could promote eutrophication and could adversely affect marine ecology.

Samples of WWTP effluent and RO concentrate were collected on August 18 and September 14, 1999, by the plant operating staff and analyzed by ASL and the South WWTP laboratory. The concentrations of the following constituents were measured to: 1) determine the suitability of discharge of the WWTP effluent/RO concentrate blend, and 2) develop requirements for treatment of the RO concentrate to ameliorate any constraints on discharge that are identified:

- TDS (gravimetric)
- TOC
- pH
- Total phosphorus
- Total Kjeldahl nitrogen (TKN)
- Nitrite/nitrate nitrogen

Results of these analyses are presented and discussed in Section 5.0.

4.3.4 RO Integrity Testing

The BOR performed an evaluation of RO element integrity test methods. This evaluation was outside of the scope of CH2M HILL's activities under their agreement with the City; however, activities conducted as part of the BOR's evaluation were closely coordinated with those conducted under this study and were, in large part, conducted by the City's operations staff. Furthermore, the results of the integrity method evaluation should provide useful information for future implementation of indirect potable reuse at McAllen and other locations where RO is used. Development of a field-applied integrity test method for RO elements will provide greater assurance that RO treatment is providing contaminant removal to the degree necessary to protect public health in this reuse context. Results of these analyses are presented in Appendix J.

4.4 Treatment System Monitoring

During the demonstration testing, various performance parameters were monitored to evaluate operation of the treatment systems and the quality of the water fed to and produced by the systems. The parameters that were monitored are presented in the following sections.

4.4.1 Operator Training

The City provided two dedicated operators to supervise, operate, and maintain the demonstration plant during the course of the study. The operators were responsible for, but not limited to, equipment maintenance and operation, including manually recording operational data, saving RO system PLC data, batching chemicals, adjusting chemical addition rates, performing chemical cleanings, collecting routine water quality samples, and recording all demonstration plant activities.

Operating parameters for the systems were monitored daily to evaluate treatment: system performance. ZenoGem system operating data were collected from equipment instruments and recorded manually on operations log sheets at least twice daily. RO system operating data were collected by two methods: 1) electronically via a PLC for a specified interval and duration (typically every hour over a 12-hour period), and 2) manually at the end of each operating shift from equipment instruments and panel readouts and recorded on operations log sheets. Method 1 was used for primary data collection; method 2 served as a backup source in the event of difficulties with PLC data downloading. Logbooks for each system were maintained to record all O&M events that occurred during the testing period including, but not limited to, date and time of chemical cleanings; type and amount of chemicals used during cleaning, cleaning temperature, and pH; downtimes; alarms or failures; and changes in any operating conditions.

The operating criteria (targets) were presented in Section 3.0. The actual average operating conditions, along with targets, are presented and discussed in Section 5.0.

4.4.2 Sampling and Analysis

The operators collected water quality samples from each treatment system on a routine basis. The South WWTP laboratory was responsible for performing selected physical/chemical and biological analyses. The WWTP laboratory was also responsible for collecting samples for TOC, chemical oxygen demand (COD), TKN, nitrite/nitrate nitrogen, and total phosphorous, and shipment of these samples to ASL for analyses. The central water laboratory, located at McAllen's Water Treatment Plant No. 1, was responsible for performing microbiological analyses.

Sampling activities commenced on February 8, 1999, for the ZenoGem system and on April 16, 1999, for the RO system. At these times, the operators began routine recording of system operating data and collection of water quality samples for each system. In addition, the water and wastewater treatment plants and ASL began routine sampling analyses. The biological treatment and water quality parameters, sampling location and frequency, and responsible analytical party for each treatment system are presented in Tables 4.1 and 4.2.

SECTION 4. TESTING APPROACH

TABLE 4.1
Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System

		Location and Frequency					
Parameter	ZenoGem Feed	Membrane Tank	Aeration Tank	ZenoGem Permeate	Aeration Tank Waste Sludge	Sample Day(s)	Responsible Party
Physical/Chemical							
pH	2/W	2/W	2/W	2/W	NONE	M & W	WWTP
Temperature*	1/D	1/D	1/D	1/D	NONE	M - F	OPERATOR
Conductivity	1/D	NONE	NONE	1/D	NONE	M-F	WWTP
Turbidity	NONE	NONE	NONE	1/D	NONE	M - F	WWTP
COD _p	2/M	NONE	NONE	2/M	1W	М	CH2M
Total Chlorine	NONE	NONE	NONE	1/D	NONE	M-F	WWTP
Free Chlorine	NONE	NONE	NONE	1/D	NONE	M-F	WWTP
ALK	1 <i>N</i> V	NONE	NONE	1/W	NONE	М	WTP
Biological							
DO ⁴	1/D	1/D	1/D	NONE	NONE	M - F	OPERATOR
OUR	NONE	2/W	2/W	NONE	NONE	M & W	WWTP
MLSSb	NONE	3/W	3/W	NONE	3/W	M,W,F	WWTP
MLVSSb	NONE	3/W	3/W	NONE	1/W	M or M,W,F	WWTP
DSVI	NONE	3/W	NONE	NONE	NONE	M,W,F	WWTP
CBOD ₅ ^b	3/W	3/W	3/W	3/W	NONE	M,W,F	WWTP
TSS ^b	3/W	NONE	NONE	3/W	NONE	M,W,F	WWTP

SECTION 4. TESTING APPROACH

TABLE 4.1 Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System

	Location and Frequency						
Parameter	ZenoGem Feed	Membrane Tank	Aeration Tank	ZenoGem Permeate	Aeration Tank Waste Sludge	Sample Day(s)	Responsible Party
NH ₃ -N ^b	3/W	NONE	NONE	3/W	NONE	M,W,F	WWTP
TKN⁵	1/W	NONE	NONE	1/W	1/W	М	CH2M
NO ₂ /NO ₃ -N ^b	1/W	NONE	NONE	1/W	NONE	М	CH2M
T Phosphorus	1/W	NONE	NONE	1/W	1 <i>W</i>	М	CH2M
Microbial							
Total Coliform	2/W	NONE	NONE	2/W	NONE	M&W	WTP
Fecal Coliform	2/W	NONE	NONE	2/W	NONE	M & W	WTP
HPC	NONE	NONE	NONE	2/W	NONE	M&W	WTP

^aThese samples are to be taken at the same time. ^bOperator to analyze at sample location.

^{1/}D=once per day

^{1/}W=once per week

^{2/}W=twice per week

^{3/}W=three times per week

^{2/}M=2 times per month

ALK=alkalinity

CH2M HILL=CH2M HILL's Applied Sciences Laboratory (ASL)

DO=dissolved oxygen
DSVI=diluted sludge volume index
MLVSS=mixed liquor volatile suspended solids
OUR=oxygen uptake rate

WTP=McAllen's Central Water Treatment Plant Laboratory
WWTP=McAllen's South Wastewater Treatment Plant Laboratory

TABLE 4.2
Water Quality Sampling Schedule for the RO System

	Lo	cation and Freque			
Parameter	RO Feed	RO Permeate	RO Concentrate	Sample Day(s)	Responsible Party
Physical/Chemical					
рН	1/W	1/W	1/W	М	WWTP
Conductivity	1/W	1/W	1/W	М	WWTP
Turbidity	1/D	1/D	1/D	M - F	WWTP
SDI ^a	1/D	1/D	NONE	M - F	OPERATOR
TOC ^b	1/D	1/D	NONE	M-F	OPERATOR
тос	2/M	2/M	NONE	M	CH2M
Total Chlorine	1/D	1/D	NONE	M - F	WWTP
Free Chlorine	1/D	1/D	NONE	M - F	WWTP
TDS	1/W	1/ W	1/W	М	WWTP
Microbial					
Total Coliform	NONE	2/W	NONE	M & W	WTP
Fecal Coliform	NONE	2/W	NONE	M & W	WTP
HPC	2/W	2/W	NONE	M & W	WTP

^aOperator to analyze at sample location using auto analyzer.

CH2M=CH2M HILL's Applied Sciences Laboratory (ASL)

WWTP=McAllen's South Wastewater Treatment Plant Laboratory

WTP=McAllen's Central Water Treatment Plant Laboratory

4.5 Data Evaluation

Several of the operating parameters and water quality parameters presented previously were compiled, reduced, and analyzed to evaluate operational, biological, and membrane performance of the treatment systems. Evaluating the flux, TMP, and permeability characterized ZenoGem membrane performance. The primary water quality parameters used to evaluate the effectiveness of the ZenoGem treatment process in producing a high quality RO feedwater were turbidity and SDI. Evaluating the feedwater recovery, normalized product flow (NPF), and the pressure drop across the vessels characterized RO membrane performance.

^bOperator to analyze at sample location using monitor.

^{1/}D=once per day

^{1/}W=once per week

^{2/}W=twice per week

^{2/}M=twice per month

4.5.1 Filtrate Flow and Membrane Flux

Membrane flux is directly proportional to the permeate (filtrate) flow rate as shown in the following equation:

```
Flux [gfd] = Permeate Flow rate[gpm] x 1440 / Membrane Area [ft<sup>2</sup>]

where [gfd] = gallons per day per ft<sup>2</sup>
```

As the filtrate flow rate increases, the membrane flux increases proportionately.

4.5.2 Transmembrane Pressure and Permeability

TMP represents the resistance to flow of water of 1) the membrane, and 2) the materials in the feedwater (foulants) that accumulate at the membrane surface or within the membrane pores. TMP at the start of testing (with a clean membrane) represents only the resistance of the membrane. As foulants accumulate and cannot be effectively removed by backwashing/backpulsing with disinfectant, TMP increases because of the resistance of flow exerted by the foulants. Thus, the rate at which TMP increases is directly proportional to the rate of membrane fouling.

Membrane permeability is inversely proportional to the TMP as shown in the following equation:

```
Permeability [gfd/psi] = Flux [gfd]*1.024^{(25-T)}/TMP [pounds per square inch (psi)] where T = feedwater\ temperature, ^{\circ}C
```

Permeability is a direct measure of the water flow through the membrane fiber and any foulants that have accumulated on the surface or within the membrane pores. The permeability equation includes a temperature correction factor to remove or "normalize for" the effects of changing temperature on membrane permeability. Increases in temperature increase water flow through the membrane because of decreasing viscosity. This effect must be removed to accurately assess changes in permeability with run time.

4.5.3 Turbidity and SDI

Traditionally, the RO membrane manufacturers have established the following as criteria for efficient RO operation:

Turbidity: \leq 0.2 NTU

 $SDI: \leq 3$ (based on 15-min test interval)

SECTION 5

Demonstration Testing Results

This section presents the results of demonstration plant testing. All data collected during the study are presented in Appendix C as follows:

Operating data for ZenoGem System	Table C-1
Water quality data for ZenoGem System	Table C-2
Operating data for RO System	Table C-3
Water quality data for RO System	Table C-4

Results for water quality parameters routinely analyzed by the McAllen water and wastewater laboratories were communicated to CH2M HILL by facsimile on daily or weekly sampling logs. These data, along with CH2M HILL laboratory data, were tabulated and incorporated into Tables C-1 through C-4 in Appendix C.

5.1 Operations

A summary of ZenoGem and RO system operating stages and events is presented in Tables 5.1 and 5.2. Additional details regarding the specific operating stages are discussed below.

TABLE 5.1
Operating Stages and Events for the ZenoGem System

Stage	Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
A		2/6/99	0.00		Start of Testing (MLSS concentration at 13 g/L and OCP Membrane)
В		3/20/99	677.58		OKC Membrane
	1	3/31/99 - 4/1/99	915.58 - 941.00	25.42	Peak Flow Testing (9.5 gpm for 6 hrs over 24-hour period)
С		5/6/99	1783.00		Decrease MLSS Concentration to 10 g/L
	2	6/1/99	2406.08	2.42	Bubble Point Test
	3	8/12/99 - 8/13/99	4129.58 - 4158.33	28.75	Peak Flow Testing (9.5 gpm for 6 hrs over 24-hour period)
	4	8/16/99 - 8/20/99	4225.08 - 4326.25	101.17	Peak Flow Testing (9.5 gpm for 6 hrs over 24-hour period)

TABLE 5.1 CONT.Operating Stages and Events for the ZenoGem System

Stage	Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
	5	8/30/99 - 9/1/99	4561.08	51.50	Recovery (Full Tank) Clean
	6	9/14/99 - 9/16/99	4875.91	50.25	Raise Membranes
	7	9/17/99 - 9/27/99	4894.16 - 5136.25	242.09	Cycled Aeration to the Membrane Tank (10 sec on/off)
	8	9/27/99 - 9/29/99	5136.25 - 5186.91	50.66	Peak Flow Testing without Cycled Aeration
D		10/4/99	5303.41		Decrease MLSS Concentration to 6 g/L
	9	10/7/99 - 10/8/99	5328.75 - 5352.50	23.75	Cycled Aeration to the Membrane Tank (10 sec on/off)
	10	10/8/99 - 10/13/99	5352.50 - 5476.00	123.50	Peak Flow Testing with Cycled Aeration to Membrane Tank
	11	10/14/99 - 10/19/99	5476.00 - 5615.66	139.66	Normal Flow with Cycled Aeration to Membrane Tank
	12	10/19/99 - 11/2/99	5615.66 - 5948.25	332.59	Normal Flow with Cycled Aeration to Both Tanks (Aeration Tank at 15 min on/off)
	13	11/2/99	5948.25		End of Testing

TABLE 5.2Operating Stages and Events for the RO System

Stage	Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
A		4/21/99	0.00		Startup
В		5/19/99	0.00		Start of Testing (Target Feed pH = 6.8)
	1	5/24/99 - 5/25/99	114.89 - 147.69	9 32.80 1st Cleaning (Citric Acid:Stage and 2)	
	2	5/30/99	256.41		Decrease Recovery to 50%
	3	6/1/99 - 6/2/99	305.9 - 328.42	22.52	2nd Cleaning (Citric Acid:Stages 1 and 2)
	4	6/8/99 - 6/10/99	475.88 - 526.38	50.50	3rd Cleaning (Citric Acid:Stages 1 and 2 followed by Caustic:Stage 1)
С		6/11/99	544.50		Decrease Recovery to 50% (Stage 2 Removed from Service)
D		7/7/99	1176.51		Stage 2 Returned to Service (50% Recovery)

TABLE 5.2 CONT.

Operating Stages and Events for the RO System

Stage	Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
	5	7/8/99	1196.78		Increase Recovery to 60%; Decrease Feed pH to 6.5
	6	7/9/99	1208.73		Increase Recovery to 70%; Decrease Feed pH to 6.0
	7	7/22/99	1532.92		Set Target pH to Concentrate pH = 5.6 (Feedwater pH = 5.0)
	8	7/24/99 - 7/27/99	1578.67 - 1650.27	71.60	4th Cleaning (Citric Acid:Stages 1 and 2)
	9	8/10/99	1985.17		Increase Recovery to 75%
	10	8/30/99 - 9/1/99	2464.77- 2519.55	54.78	Unit Down due to ZenoGem System Recovery (Full Tank) Clean
	11	9/2/99 - 9/8/99	2543.79 - 2687.50	143.71	5th Cleaning (Citric Acid:Stages 1 and 2); Acid Pump Failure
	12	9/14/99 - 9/16/99	2830.65 - 2880.25	49.60	Unit Down due to Raising ZenoGem System Membranes
	13	9/23/99	3041.97		Increase Recovery to 80%
	14	10/4/99 - 10/6/99	3308.51 - 3359.81	51.30	Unit Down due to Decreasing ZenoGem System MLSS
	15	10/8/99	3399.11		End of Routine Testing
	16	10/21/99	3715.41		End of Special Testing

5.1.1 Startup Activities

ZenoGem Equipment Commissioning. ZENON field service technicians arrived at the plant site on January 11, 1999, and performed commissioning of the ZenoGem system through February 6, 1999. ZenoGem system commissioning included equipment installation; membrane bubble point and clean water flux testing; introduction and concentration of mixed liquor in the bioreactor tank; and operation on SDS to establish steady-state biological treatment (carbonaceous and nitrogenous oxidation) and membrane treatment. Operational activities included establishing target MLSS concentrations in both the membrane (process) and aeration tanks; air flow rates and dissolved oxygen (DO) levels in both tanks; solids recirculation rate between tanks; and membrane permeate flow (flux) rate. The ZenoGem system achieved steady-state operation on March 22, 1999.

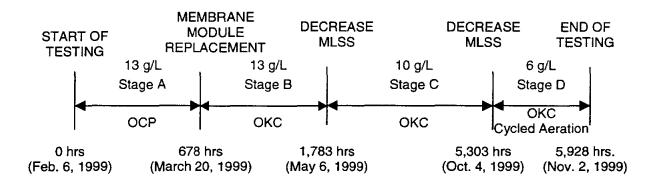
RO Equipment Commissioning. BOR project managers performed commissioning of the RO system during two site visits on February 2 through February 12, 1999, and on March 15 through March 19, 1999. During the first visit, RO system commissioning included installation of plumbing and electrical connections; delivery and storage of chemicals; modifications to the computer recording system; PLC programming; and installation of temporary membranes. During the second visit, additional RO system commissioning

included instrument calibration; SDI auto analyzer installation; system cleaning and disinfection; installation of permanent membranes and integrity tests. At that time, the RO system was scheduled for startup on March 22, 1999, coincident with steady-state operation of ZenoGem system. However, due to ZenoGem system special testing, replacement of defective chloramine metering pump parts, difficulties in attaining stable and effective chloramine stock solutions and residuals, combined with minor RO equipment problems, RO system start of testing was delayed until April 21, 1999.

5.1.2 Operating Stages

ZenoGem System. The ZenoGem operating period has been divided into four separate operating stages as shown in Exhibit 5.1. The ZenoGem operating stages were as follows:

EXHIBIT 5.1 ZenoGem Operating Stages



Stage A represents the start of testing using the OCP UF membrane and a target MLSS concentration of 13 g/L. During this stage, the aeration and membrane tanks were seeded with activated sludge from the WWTP and MLSS levels increased step-wise to the target level. The system accumulated 321 operating hours out of a possible 678 available hours, for an online factor of 0.47 (47 percent). This online factor includes two separate periods when the system was offline due to failure and subsequent replacement of the recirculation pump impeller, feedwater inlet level sensor replacement, and membrane module replacement.

The originally supplied membrane module, which used the OCP membrane, has recently been classified by ZENON as their drinking water membrane and is marketed primarily as an UF membrane for the treatment of natural raw water supplies to produce potable water. This membrane, which has a nominal pore size of 0.035 microns, has been found to have flux limitations when operated on high MLSS wastewaters and consequently is being phased out by ZENON in favor of the OKC MF membrane for wastewater treatment. The OKC membrane is more porous, with a nominal pore size of 0.4 microns. Initial in-house testing by ZENON showed the OKC membrane to operate at higher permeability and to benefit from a lower rate of fouling on wastewater, particularly when operating at peak loading conditions. Consequently, it was decided jointly by ZENON and CH2M HILL that the OKC membrane would be better suited for the

McAllen IPR application. After the OCP module was replaced with a new OKC module, the permeate flow rate was slowly increased to the target 6.5 gpm.

Stage B represents the period of operation using the OKC module and a target MLSS concentration of 13 g/L. During this stage, the system accumulated 1,077 operating hours out of a possible 1,105 available hours, for an online factor of 0.97 (97 percent). This online factor includes a short period of time when the system was offline due to replacement of a valve in the aeration tank. A single-day peak flow test was conducted during the latter part of this stage.

Stage C represents the period of operation at a target MLSS concentration of 10 g/L. During this stage, the system accumulated 3,416 operating hours out of a possible 3,520 available hours, for an online factor of 0.97 (97 percent). This online factor includes three separate periods when the system was offline due to bubble point testing, clean water flux testing/full tank soaking, and to raise the module height (in the membrane tank). During this stage, peak flow testing continued and cycled aeration (to the membrane tank only) was initiated.

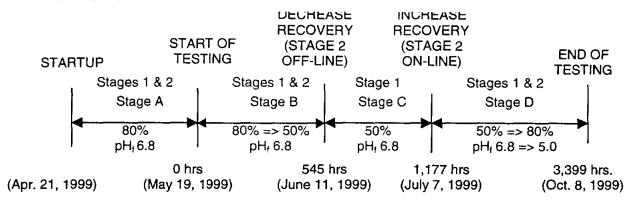
The target MLSS concentration was decreased from an initial target of 13 g/L to 10 g/L after 1,783 total available hours of operation following detailed discussions with ZENON technical personnel. Based on ZENON experience, lowering the MLSS concentration to 10 g/L provides for improved operability (lower membrane fouling) and more stable biological treatment. As discussed later in this section, MLSS reduction also improved oxygen transfer from the bulk fluid to the biomass, thereby improving nitrification efficiency and decreasing the degree of denitrification. Consequently, it was decided jointly by ZENON and CH2M HILL that the decrease in MLSS concentration would be preferred for the McAllen indirect potable reuse application.

Stage D represents the period of operation at a target MLSS concentration of 6 g/L. During this stage, the system accumulated 596 operating hours out of a possible 645 available hours, for an online factor of 0.92 (92 percent). This online factor includes a short period of time when the system was offline to decrease the MLSS concentration (i.e., wasting half the aeration tank volume) and subsequent aeration-only operation to reestablish proper biomass condition. Peak flow testing continued and cyclic aeration to the membrane and aeration tanks was also initiated during this stage.

The MLSS concentration was decreased from 10 g/L to 6 g/L after 5,303 total available hours of operation following detailed discussions with ZENON technical personnel. ZENON indicated that maintenance of stable membrane permeability during flow peaking would most likely depend on sludge filterability characteristics as indicated by the sludge capillary suction time (CST). Sludges with high CSTs are viscous and difficult to filter. The sludge generated in the ZenoGem process had a high CST (exceeding 100 seconds). ZENON indicated that for such sludge, reducing the MLSS concentration reduces the resistance to filtration and would maximize permeability during flow peak peaking. Consequently, it was decided jointly by ZENON and CH2M HILL to perform peak flow tests at a lower MLSS concentration in order to demonstrate maximum performance.

RO System. The RO operating period has been divided into four separate operating stages, as shown in Exhibit 5.2. Since the hour meter on the system was not functional, the online factor for each stage of operation was approximated by system downtimes recorded by the operators. The first two RO operating stages were as follows:

EXHIBIT 5.2 RO Operating Stages



Stage A represents the period of operation from startup to the actual start of steady state testing (commissioning phase). During this stage, the system was off line approximately 70 percent of the time due to numerous downtimes associated with PLC reprogramming and tuning to optimize control of feedwater flow and pH; failure and subsequent replacement of the scale inhibitor feed pump; de-commissioning of automatic sampling valves; and troubleshooting acid feed pump loss of prime. Data collected during this phase was considered representative of continued startup activities and system troubleshooting. By May 19, the system was successfully online, and the actual start of steady state testing was achieved.

Stage B represents the period of operation at a target recovery of 80 percent. During this 545-hour stage, the system was off line approximately 19 percent of the time due to three RO membrane cleanings and maintaining target pH.

RO Feedwater Pretreatment to Control Membrane Fouling. RO membrane elements are subject to fouling during extended operation caused by both suspended and sparingly soluble salts. Suspended matter includes organic and inorganic colloids and microorganisms. Sparingly soluble salts, such as carbonates, sulfates, and silica, can precipitate from solution as the RO process concentrates them. Suspended particles accumulate on the membrane surface causing biofouling and colloidal fouling, and they can block feed channels thereby increasing the pressure drop across the system. These phenomenon reduce water permeability through the RO membranes causing flux decline and increased salt passage. The nature and rapidity of fouling depends on the condition of the feedwater. Fouling is progressive, and, if not controlled early, can impair the RO system performance in a relatively short time. For these reasons, fouling must be controlled.

Particulate fouling is addressed through the use of the ZeeWeed MF membrane. Chloramines were batched and dosed into the RO feedwater at a target dose of 1 to 2 mg/L to prevent biological growth (biofouling) of the RO elements. As described in an

earlier section, mineral precipitation is controlled through a combination of acidification and scale inhibitor addition. The last two RO operating stages are described below.

Stage C represents the period of operation at a target recovery of 50 percent (operating first stage vessels only) to demonstrate that performance losses observed in Stage B resulted from mineral precipitation (as opposed to particulate or colloidal fouling). During this 632-hour stage, the system was online 100 percent of the time.

Stage D represents the period of operation at recovery of 50 to 80 percent (operating first and second stage vessels) and acidification of the concentrate stream to a reduced feedwater pH of 5.0 (concentrate target pH of 5.6) to control calcium phosphate and calcium carbonate precipitation. During this 2,222-hour stage, the system was off line approximately 10 percent of the time due to two RO membrane cleanings. It excludes three downtimes associated with ZenoGem full tank soaking, raising module height, and decreasing the MLSS concentration.

5.2 ZenoGem Testing Results

5.2.1 ZenoGem Operating Conditions

Table 5.3 presents the target and average operating conditions for the ZenoGem system during Stage A operation. The system operated at a target MLSS concentration of 13 g/L using the OCP UF membrane. After 678 hours of startup activities, the membrane was replaced with the OKC MF membrane.

TABLE 5.3Stage A Average Operating Conditions for the ZenoGem System

Parameter	Target*	Normal Flow
Aeration Tank Air (scfm)	> 45	48
Backpulse Duration (sec)	15	15
Backpulse Frequency (min)	10	10
Biomass Recirculation Rate (gpm)	> 36	26.2
Flux (gfd)	18.7	17.3
Membrane Tank Air (scfm)	25	25
Normalized Permeability (gfd/psi)	5	20.8
Permeate Flowrate before Backpulse (gpm)	6.5	6.0
Permeate Flowrate after Backpulse (gpm)		6.0
Temperature (degrees C)		26.2
TMP (psi)	2.5 - 8.5	1.34
Vacuum before Backpulse (in Hg)	5.1 - 17.3	2.73
Vacuum after Backpulse (in Hg)		2.57

^aWhere target left blank, no target was established.

^bValues calculated when permeate flowrate reached 6 gpm.

Table 5.4 presents the target and average operating conditions for the ZenoGem system during Stage B operation. The system continued to operate at a target MLSS concentration of 13 g/L during this stage. After 916 hours of operation (Event 1), the permeate flowrate was increased for 25 hours to determine the short-term impact of higher membrane loading on permeability and TMP.

TABLE 5.4Stage B Average Operating Conditions for the ZenoGem System

Parameter	Target ^a	Normal Flow	Peak Flow (Event 1)
Aeration Tank Air (scfm)	> 45	43	42
Backpulse Duration (sec)	15	15	15
Backpulse Frequency (min)	10	10	10
Biomass Recirculation Rate (gpm)	> 36	38.3	39.5
Flux (gfd)	18.7/27.3 ^b	18.5	27.3
Membrane Tank Air (scfm)	25	25	25
Normalized Permeability (gfd/psi)	5	17.82	13.19
Permeate Flowrate before Backpulse (gpm)	6.5/9.5 ^b	6.40	9.50
Permeate Flowrate after Backpulse (gpm)		6.40	9.50
Temperature (degrees C)		28	25.8
TMP (psi)	2.5 - 8.5	1.2	2.1
Vacuum before Backpulse (in Hg)	5.1 - 17.3	2.66	4.17
Vacuum after Backpulse (in Hg)		2.59	4.12

^aWhere target left blank, no target was established.

Table 5.5 presents the target and average operating conditions for the ZenoGem system during Stage C operation. At the beginning of this stage (after 1,783 hours of operation), the MLSS concentration was decreased to 10 g/L. From 4,130 to 4,158 hours (Event 3) and from 4,225 and 4,326 hours (Event 4) of operation, the permeate flow rate was increased by 46 percent (6.5 to 9.5 gpm) for a period of 6 hours (flow peaking) over a 24-hour period to simulate the types of hydraulic peak loading that typically occur in a conventional WWTP. This was done to determine if the MBR system could be operational in the same manner or if additional means would be required to ensure slower changes in loading to the system. After 4,876 hours of operation, the membrane module height was raised (Event 6) to minimize sludge accumulation on the module aerators during non-aeration periods. From 4,894 to 5,136 hours (Event 7) of operation, air was cycled to the membrane tank at an applied rate of 30 scfm for 10 seconds on and 10 seconds off to evaluate the effect of intermittent aeration on operations and membrane performance. From 5,136 to 5,187 hours (Event 8) of operation, flux peaking was conducted without intermittent aeration to the membrane tank.

^bTarget value during flow peaking.

TABLE 5.5Stage C Average Operating Conditions for the ZenoGem System

				Normal Flow with Cycled Aeration to Membrane Tank
		Normal	Peak Flow	Only
Parameter	Target ^a	Flow	(Events 3,4,8)	(Event 7)
Aeration Tank Air (scfm)	> 45	59	61	63
Backpulse Duration (sec)	15	15	15	15
Backpulse Frequency (min)	10	10	10	10
Biomass Recirculation Rate (gpm)	> 36	48.2	47.5	44.6
Flux (gfd)	18.7/27.3 ^b	18.7	26.6	18.7
Membrane Tank Air (scfm)	25/30°	25	25	31
Normalized Permeability (gfd/psi)	5	6.61	3.05	8.67
Permeate Flowrate before Backpulse (gpm)	6.5/9.5 ^b	6.50	9.20	6.50
Permeate Flowrate after Backpulse (gpm)		6.70	11.10	7.10
Temperature (degrees C)		31.2	31.9	30.3
TMP (psi)	2.5 - 8.5	2.8	7.5	2.4
Vacuum before Backpulse (in Hg)	5.1 - 17.3	5.70	15.30	4.90
Vacuum after Backpulse (in Hg)		5.10	15.90	4.10

^aWhere target left blank, no target was established.

Per discussions with ZENON, cycled aeration operation to the membrane tank was planned at 10 seconds on and 10 seconds off. However, a cycle time of 15 seconds on and 15 seconds off was implemented at the site due to communication and programming error between ZENON and the demonstration plant operators. ZENON Corporate Technology tested a number of different air cycle times at other pilot locations and concluded that 10 seconds off is the maximum allowable period before a decline in permeability is observed. Longer air OFF periods allow the mixed liquor solids to accumulate in the fiber bundle and are not subsequently removed by the air pulse during the ON cycle. Thus, the error in cycle time implemented is significant enough to cause the permeability decline observed during cycled aeration events as discussed in Section 5.2.2.

Target value during flow peaking.

^cApplied rate increased to 30 cubic feet per minute (cfm) during intermittent aeration.

Table 5.6 presents the target and average operating conditions for the ZenoGem system during Stage D operation. At the beginning of this stage (after 5,303 hours of operation), the MLSS concentration was decreased to 6 g/L. From 5,329 to 5,353 hours (Event 9) of operation, air was again cycled to the membrane tank. From 5,353 to 5,476 hours (Event 10) of operation, flux peaking was conducted; however this time with intermittent aeration to the membrane tank. From 5,476 to 5,616 hours (Event 11) of operation, the flowrate was reduced to normal conditions and air continued to cycle to the membrane tank. From 5,616 hours to the end of testing (Event 12), air was cycled to the aeration tank at an applied rate of 45 scfm for 15 minutes on and 15 minutes off to evaluate the effect of intermittent aeration on biological treatment performance (i.e., to concurrently nitrify and denitrify).

TABLE 5.6
Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGem System

		Normal	Normal Flow with Cycled Aeration to Membrane Tank Only	Peak Flow with Cycled Aeration to Membrane Tank Only	Normal Flow with Cycled Aeration to Membrane Tank Only	Normal Flow with Cycled Aeration to Membrane and Aeration Tanks
Parameter	Target ^a	Flow	(Event 9)	(Event 10)	(Event 11)	(Event 12)
Aeration Tank Air (scfm)	> 45	65	66	64	66	65
Backpulse Duration (sec)	15	15	15	15	15	15
Backpulse Frequency (min)	10	10	10	10	10	10
Biomass Recirculation Rate (gpm)	> 36	47.3	48.0	47.0	46.2	43.1
Flux (gfd)	18.7/27.3 ^b	18.7	18.7	27.3	18.7	18.7
Membrane Tank Air (scfm)	25/30°	25	32	32	32	32
Normalized Permeability (gfd/psi)	5	7.27	7.52	3.25	3.86	3.42
Permeate Flowrate before Backpulse (gpm)	6.5/9.5 ^b	6.50	6.50	9.5	6.50	6.50
Permeate Flowrate after Backpulse (gpm)		6.90	6.70	11.50	6.90	6.90
Temperature (degrees C)		30.3	30.0	31.6	29.0	26.4
TMP (psi)	2.5 - 8.5	2.39	2.2	7.37	4.5	5.7
Vacuum before Backpulse (in Hg)	5.1 - 17.3	4.90	4.50	15.0	9.10	11.50
Vacuum after Backpulse (in Hg)		4.30	4.60	16.30	8.20	10.50

^aWhere target left blank, no target was established.

^bTarget value during flow peaking.

^cApplied rate increased to 30 cfm during intermittent aeration.

5.2.2 ZeeWeed Membrane Performance

Permeate Flow and Membrane Flux. Figure 5.1 illustrates changes in ZenoGem permeate flow and flux as a function of operating time. During Stage A (prior to membrane replacement), flow and flux were increased in step-wise increments to "condition" the membrane fibers to the mixed liquor. This was done to prevent the fibers from becoming fouled. Permeate flow was held constant during Stages B through D except for five events:

- Event 1: Flow increased for 25 hours to determine the short-term impact of higher membrane loading on permeability and TMP; and
- Events 3, 4, 8 and 10: Flow increased by 46 percent (6.5 to 9.5 gpm) for a period of 6 hours (flow peaking) over a 24-hour period to simulate WWTP peak hydraulic loading.

The increases caused a corresponding increase in TMP and decrease in permeability; however both changes were reversed once the flow was decreased to the target level. Thus, the temporary flux increase caused only reversible membrane fouling and flow peaking for short (one-day) periods of time can occur in response to actual WWTP loading without causing a permanent increase in fouling.

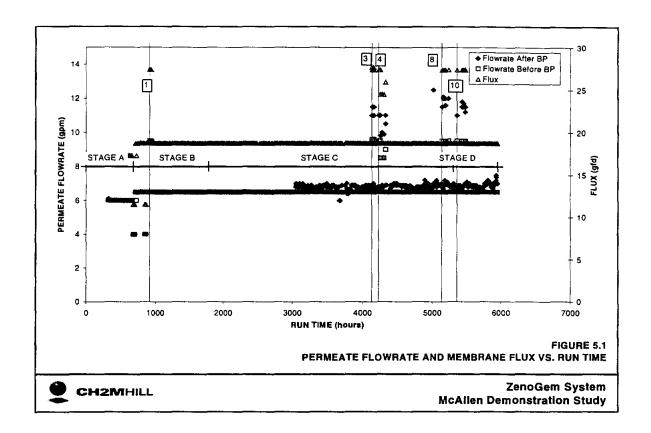
Transmembrane Pressure. Figure 5.2 illustrates changes in ZenoGem TMP as a function of operating time (permeate flow is also shown for reference).

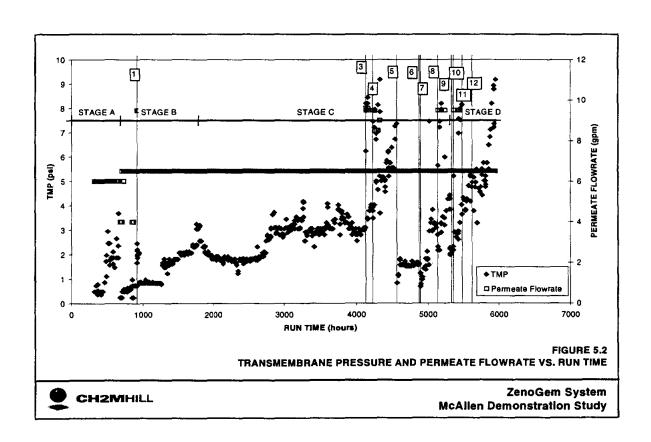
Stage A. TMP increased gradually as permeate flow was increased to the target value. The sharp decline in TMP that occurred at 653 hours was caused by continuous aeration of the module during the 12-day period when the ZenoGem system was offline due to recirculation pump failure and replacement. Continuous aeration in the absence of permeation was very effective in reducing membrane fouling.

Stage B. During the latter part of Stage B, TMP steadily increased even when permeate flowrate (and membrane flux) were held constant. This increase in TMP clearly indicates that membrane fouling was occurring at the higher MLSS concentration. The short-term flow peaking during Stage B (Event 1) caused a temporary increase in TMP that was reversed once flux was reduced.

Stage C. During operation at intermediate (10 g/L) MLSS concentration, TMP first decreased and then increased very gradually over a 1,000-hour period, indicating: 1) a very low rate of fouling, and 2) maintenance cleans were more effective in controlling fouling at the lower MLSS concentration. The step increase in TMP at ~2,700 hours was caused by a temporary loss of air scour in the membrane tank. Flow peaking during Stage C (Events 3 and 4) resulted in a more rapid rate of TMP increase, demonstrating that flow peaking of the membrane on a daily basis over an extended operating period caused a significant increase in fouling rate at the lower MLSS concentration. TMP increased to the maximum value (8 psi) which required a recovery (full tank) clean (Event 5) to reduce TMP to clean membrane levels (0.8 psi). At the end of Stage C, TMP rapidly increased when air was cycled to the membrane tank (Event 7) and again during flow peaking without cycled aeration (Event 8).

Stage D. During this stage, the impact of both flow peaking and cycled (intermittent) aeration was evaluated at low (6 g/L) MLSS concentration. The data in Figure 5.2 shows TMP increases were rapid when flow peaking and cycled aeration was practiced, consistent with flow peaking effect observed in Stage C. The impact of cycled aeration alone (no flow peaking) is more difficult to ascertain. TMP rise rate following Event 11 and the first part of Event 12 was low, but increased rapidly near the end of testing. The latter effect may be the result of operation at high TMP levels (significant fouling present) rather than from intermittent aeration. Future testing using intermittent aeration should be conducted with a clean membrane to more clearly determine its impact on membrane fouling. It should be noted that during flow peaking events, the vacuum after backpulsing was slightly higher than before backpulsing. This indicates that backpulsing had little effect in reducing the TMP (or increasing permeability) during flow peaking. During normal flow operation, post-backpulse TMP was always less than pre-backpulse values.



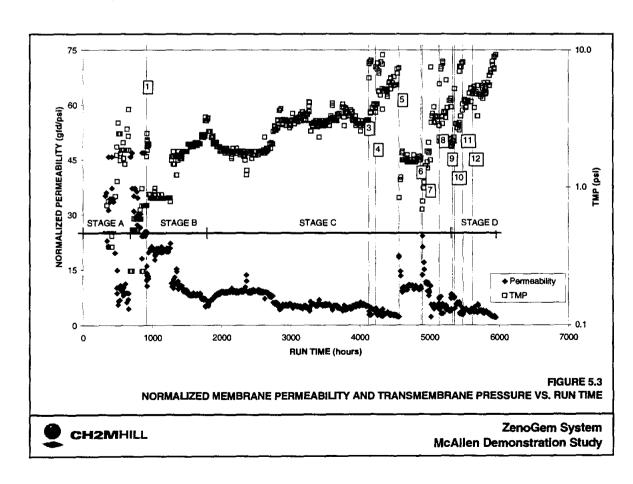


Permeability.

Stages A – C. Figure 5.3 illustrates changes in ZenoGem permeability as a function of operating time (TMP is also shown for reference). During Stage B, permeability (normalized to 20°C) steadily decreased as TMP increased, indicating membrane fouling at the higher MLSS concentration of 13 g/L. In contrast, at the lower MLSS concentration in Stage C, permeability increased and remained relatively constant as TMP very gradually increased. However during the flow peaking test periods (Events 3, 4 and 8), permeability sharply decreased as TMP increased. This showed that the MBR system must be provided with a means of ensuring slow changes in peak loading. The peak loading cannot be raised as quickly over a 24-hour period as in a conventional WWTP. These results also confirm that ZenoGem operation at 10 g/L MLSS concentration and constant flux provides for very stable system operation.

Following raising of the membrane module and subsequent aeration of the membrane tank without operation of the permeate pump (no permeation), permeability decreased (Event 7). Subsequent operation with cycled aeration to the membrane tank produced a rapid and significant decrease in permeability.

Stage D. Operation under conditions of cycled aeration and/or flow peaking generally caused more rapid declines in permeability than operation at normal (steady) flow and continuous aeration, consistent with results under similar conditions during Stage C. This performance indicates that cycled aeration is less effective than continuous aeration in controlling foulant accumulation.



5.2.3 ZenoGem Biological Treatment Performance

Table 5.7 presents the average conditions within the ZenoGem bioreactor (volume weighted composite of the aeration and membrane tanks) during each stage of operation.

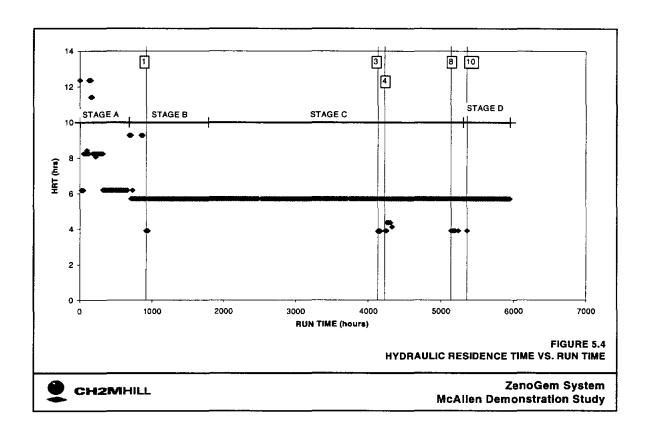
TABLE 5.7 Results of Biological Treatment Performance Analyses for the ZenoGem System

Parameter	Target ^a	Stage A	Stage B	Stage C	Stage D
DO (mg/L)	> 1.5	2.78	1.53	2.00	3.19
OUR (mg O₂/L-min)	1.0 - 1.5			0.87	1.34
MLSS (mg/L)	13,000 (Stage A & B) 10,000 (Stage C) 6,000 (Stage D)	11,454	14,070	10,634	6,661
MLVSS (mg/L)		8,339	10,243	7,655	4,873
Sludge Wasted Daily (gals)	90 (Stage A & B) 110 (Stage C) 150 (Stage D)	96	131	114	182
Sludge Yield		1.27	1.50	1.14	2.03
HRT (hrs)	5.7/3.9 ^b	6.2	5.8/3.9 ^b	5.7/4.0 ^b	5.7/3.9 ^b
System SRT (days)	25 (Stage A & B) ^c 20 (Stage C) ^c 15 (Stage D) ^c	21.29	16.79	19.25	14.04

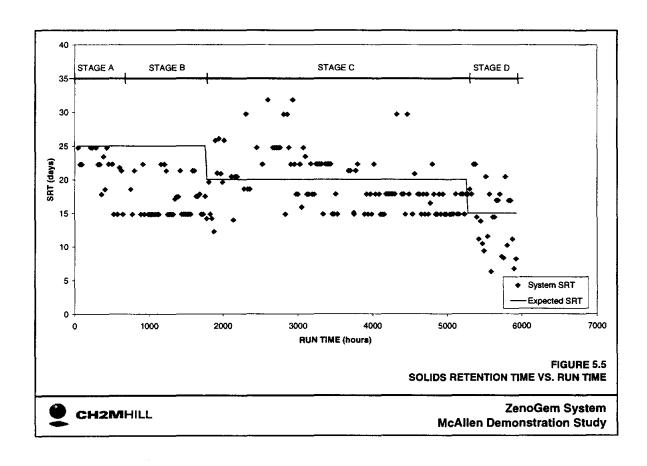
^aWhere target left blank, no target was established. ^bValue during flow peaking.

^cExpected value based on control variables.

Hydraulic Residence Time. Figure 5.4 presents the HRT for the ZenoGem bioreactor. The average HRT for Stage A was slightly higher than the target range due to the step-wise increase in permeate flow to the target value of 6.5 gpm. HRT was held constant and near the target range during subsequent stages, except during flow peaking (Events 1, 3, 4, 8 and 10) when the HRT dropped by 32 percent (from 5.7 hrs at 6.5 gpm down to 3.9 hours at 9.5 gpm). A 6.5-hour HRT was selected to ensure sufficient retention time to achieve complete nitrification based on prior testing at McAllen and other locations. This compares with a HRT of 30 hours for the McAllen WWTP (3 to 4 g/L MLSS) and reflects the greater biochemical oxidation efficiency at the higher MLSS levels.



Solids Retention Time. Figure 5.5 presents the SRT for the ZenoGem bioreactor. The average SRTs were near expected values during each stage, except for Stage B. A higher SRT would be expected for Stage B (versus Stage C) given that the MLSS concentration in the bioreactor was higher and loadings were similar. A lower SRT during Stage B resulted from excess sludge wasting (average 150 gpd compared to the target 110 gpd) in an effort to maintain the target MLSS concentration of 13 g/L. The ZenoGem process has the capability to be operated at a longer SRT (15 to 25 days) than the McAllen WWTP (15 days) because it is not limited by sludge settleability that limits the maximum MLSS concentration that can be accumulated in the system when using clarifiers rather than membranes for biomass retention.

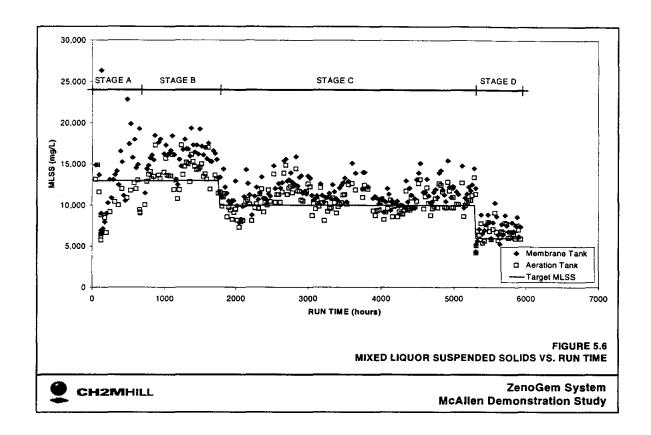


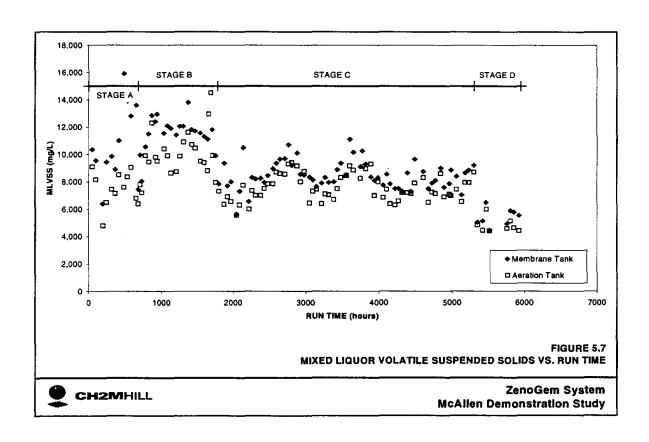
Mixed Liquor Suspended and Volatile Suspended Solids. The McAllen WWTP and the ZenoGem system both use the suspended growth process (activated sludge) to achieve biological treatment. Removal of carbonaceous organic matter in a suspended growth process is directly dependent on the concentration of biomass present in the mixed liquor (activated sludge). Biomass levels can be roughly estimated by measuring the concentration of either the MLVSS or MLSS in the treatment reactor. The latter is more practical for maintaining proper bacterial levels because it is an easier and more rapid method. MLVSS is a more accurate measure of bacterial content because it excludes some of the inert fraction of the suspended solids, however it requires an additional drying and weighing step, which adds time and effort.

MLSS and MLVSS levels measured in the ZenoGem membrane (bioreactor) and aeration tanks are shown in Figures 5.6 and 5.7. The concentration of both parameters should be the same in both tanks under ideal conditions (infinite sludge recirculation rate and exact sludge wasting rates). The average MLSS concentrations in the tanks were at or near target values during each stage. Lower MLSS concentrations in Stage A are representative of startup operations (seeding and MLSS concentration increase to steady-state conditions). Higher than planned MLSS concentrations in Stage B resulted in greater sludge wasting volumes and higher sludge yields. The most common range of MLVSS values for conventional air activated sludge systems is 2,000 to 2,500 mg/L (WEF, 1991). Although air based conventional systems can operate at somewhat higher MLVSS level (up to 3,000 mg/L in practice), sludge settleability decreases as MLSS levels decrease. Settleability is not an issue for the ZenoGem process because separation is not dependent on gravity settling but rather on membrane filtration. However, sludge dewatering characteristics are important as they directly impact observed membrane permeability.

The significance of the greater MLVSS levels is that the ability to remove CBOD $_5$ is directly proportional to bacterial density in the activated sludge tank (or bioreactor). By maintaining higher MLVSS concentrations, the ZenoGem process can attain comparable reduction in CBOD $_5$ at a much lower hydraulic retention time. This is clearly illustrated in Table 5.7, where the average HRT for ZenoGem is about 6 hours versus 30 hours for the WWTP. In fact, as discussed in the following section, CBOD $_5$ removal efficiency was slightly better for the ZenoGem system. In other words, the same, or even greater, degree of treatment can be accomplished in roughly one-fifth of the time or volume used by the extended aeration process used at McAllen. Assuming similar depths for an aeration basin and ZenoGem bioreactor, the tankage area of the ZenoGem process would require only 20 percent of the land area required for the extended aeration basins. It should be noted, however, that it is possible that acceptable treatment could have been achieved in the full-scale McAllen WWTP if another activated sludge process was used.

The average ratio of MLVSS to MLSS for the ZenoGem process was 0.73. This is at the lower end of the typical range (0.7 to 0.9) and reflects the absence of a primary sedimentation step ahead of the ZenoGem process to settle and reduce inerts.



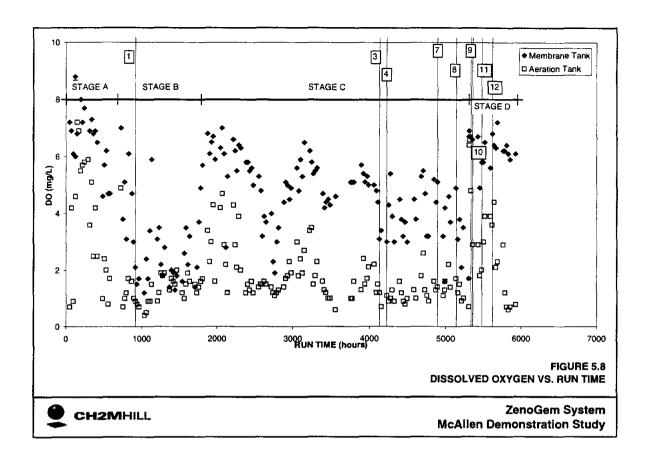


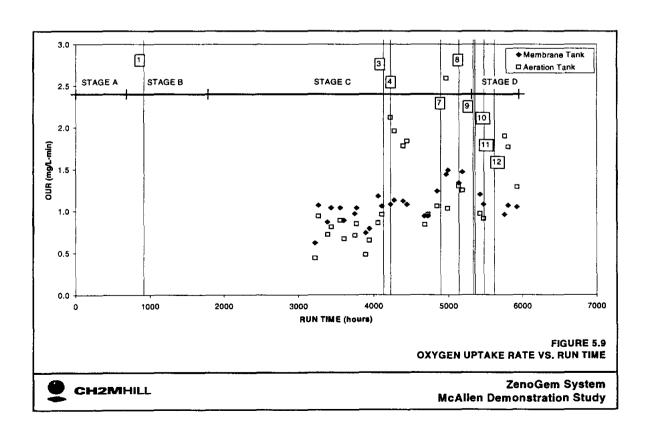
Dissolved Oxygen. Proper DO levels must be maintained in the activated sludge process to enable efficient degradation of both carbonaceous organic matter and organic nitrogen. Generally, DO levels in the activated sludge process should be maintained around 2.0 mg/L or greater to ensure that sufficient oxygen is present to achieve effective BOD₅ removal and nitrification (WEF, 1990). Lower levels will impede nitrification. DO levels of 1.5 mg/L or greater were targeted for the ZenoGem system.

DO levels in the membrane and aeration tanks are presented in Figure 5.8. DO levels were considerably higher than planned during Stage A as the air flowrate was optimized. Lower DO levels in the aeration tank than the membrane tank (38 to 58 percent lower throughout the study) resulted from inadequate air supply. Low DO levels in both tanks during Stage B resulted from high oxygen demand due to high BOD and TSS loading in the feedwater and to the higher MLSS concentration. Periodic increases in the ammonia content of the feedwater resulted in low DO levels during the other stages due to the increased oxygen demand required for nitrification.

Oxygen Uptake Rate. OURs in the membrane and aeration tanks are presented in Figure 5.9. OUR values were less than target from startup to the middle of Stage C due to error in the analytical method used. Samples were held for several hours prior to analysis (rather than being performed immediately), thereby decreasing oxygen uptake potential. After 3,216 hours of operation, OUR analysis was performed correctly and OUR values increased significantly.

Sludge Yield. Sludge yield coefficient, *Y*, is a measure of the amount of biological solids produced by a wastewater treatment process relative to the amount of organic matter removed. Ideally, the sludge yield should be as low as possible to minimize the need to dispose of sludge. For the extended aeration process used at the WWTP, *Y* is typically low because the microorganisms in the activated sludge operate in the endogenous phase based on the long mean SRT for this type of system (15 days). *Y* values for the ZenoGem system should be somewhat lower than the WWTP because the ZenoGem system operated at slightly higher SRTs; however this was not the case. The average sludge yield for the ZenoGem process ranged from 1.14 to 2.03 grams of sludge produced per gram of CBOD₅ removed. Based on the data available from the McAllen WWTP control logs, sludge yield for the McAllen WWTP was 0.73.





5.2.4 ZenoGem Water Quality Impacts

Several water quality parameters were measured to monitor the effectiveness of ZenoGem biological treatment and membrane filtration in improving wastewater quality. Table 5.8 presents the results of water quality analyses of the ZenoGem feed (SDS) and permeate during Stages A and B. The system operated at constant flow/flux during both stages, except for a brief 25-hour flow peaking period at the end of Stage B.

TABLE 5.8

Results of Stages A and B Water Quality Analyses for the ZenoGem System

					Sta	ge B		
Parameter		Stage A		Norm	al Flow	Peak Flow (Event 1)		
Physical/Chemical	Permeate Target ^a	Feed	Permeate	Feed	Permeate	Feed	Permeate	
рН		7.23	7.33	7.22	7.59	7.12	7.58	
Temperature (degrees C)		25.6	26.3	27.1	28.2	26.0	26.5	
Turbidity (NTU)	< 0.2		0.17		0.24		0.34	
Conductivity (µS/cm)		1,986	1,714	2,138	1,716	1,975	1,765	
COD (mg/L)		300	5.0	620	15.0			
CaH (mg/L as CaCO ₃)					331		360	
ALK		391	154	422	203		230	
Biological								
CBOD₅ (mg/L)	< 2	228	1.77	230	0.85	276	1.98	
TSS (mg/L)	< 1	238	0.30	183	0.27	152	0.40	
T-Phosphorus (mg/L as P)		20.65	0.96	14.00	0.18			
NH ₃ -N (mg/L as N)	< 0.5	26.93	0.16	25.36	5.68	26.50	6.58	
TKN (mg/L as N)		111	3.31	75	9.73			
NO ₂ /NO ₃ -N (mg/L as N)		0.03	19	0.17	5.83			
Total Nitrogen (mg/L as N)		111	22	75	16			
Microbial								
Total Coliforms (CFU/100mL)	< 2.2		3.0		109.4		84.0	
Fecal Coliforms (CFU/100 mL)	0		4.5		41.9		175.0	
HPC (CFU/mL)	< 500		1,619		3,276			

^aWhere target left blank, no target was established. μS/cm=microSiemens per centimeter.

Table 5.9 presents the results of water quality analyses of the ZenoGem feed and permeate during Stage C. The system operated at constant flow/flux during this stage, except during three flow peaking events and a 242-hour period when air was cycled to the membrane tank.

TABLE 5.9Results of Stage C Water Quality Analyses for the ZenoGem System

				Pea	k Flow	Normal Flow with Cycled Aeration to Membrane Tank Only	
Parameter		Normal Flow		(Even	ts 3,4,8)	(Event 7)	
Physical/Chemical	Permeate Target ^a	Feed	Permeate	Feed	Permeate	Feed	Permeate
pH		7.16	7.42	7.20	7.37	7.20	7.35
Temperature (degrees C)		29.6	30.8	30.6	31.5	28.7	29.9
Turbidity (NTU)	< 0.2		0.15		0.10		0.15
Conductivity (µS/cm)		1,904	1,612	1,669	1,469	1,958	1,678
COD (mg/L)		383.3	15.6	380	13.0		
CaH (mg/L as CaCO ₃)			345		312		322
ALK		352	128	336	158	334	176
Biological				_			
CBOD₅ (mg/L)	< 2	164	0.57	161	0.08	156	0.54
TSS (mg/L)	< 1	130	0.28	122	0.20	107	0.24
T-Phosphorus (mg/L as P)		9.55	3.34	5.23	3.15		1.97
NH ₃ -N (mg/L as N)	< 0.5	23.17	0.56	23.16	0.24	23.18	0.91
TKN (mg/L as N)		47	2.94	37	2.20	38	8.50
NO ₂ /NO ₃ -N (mg/L as N)		0.38	15.47	0.03	6.51	0.04	1.46
Total Nitrogen (mg/L as N)		47	18	37	9	38	10
Microbial							
Total Coliforms (CFU/100mL)	< 2.2		15.1		17.3		82.2
Fecal Coliforms (CFU/100 mL)	0		8.9		8.8		26.1
HPC (CFU/mL)	< 500		1,383		2,891		3,237

^aWhere target left blank, no target was established.

Table 5.10 presents the results of water quality analyses of the ZenoGem feed and permeate during Stage D. The system operated in an alternative operating mode with a reduced MLSS concentration (6 g/L) and peak flow and/or cycled aeration to one or both tanks.

TABLE 5.10Results of Stage D (Alternative Operating Mode) Water Quality Analyses for the ZenoGem System

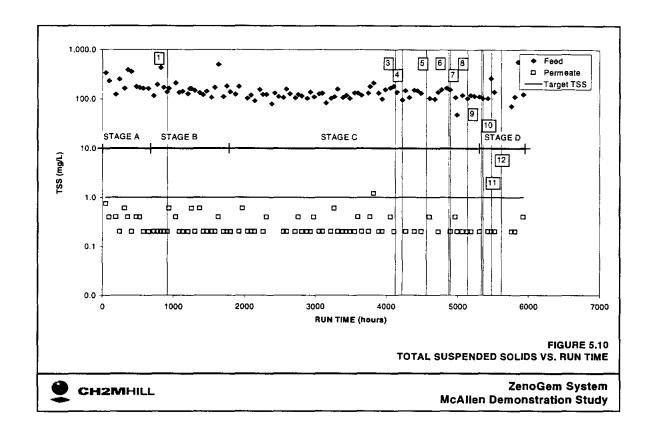
		Normal Flow with Cycled Aeration to Membrane Tank		Peak Flow with Cycled Aeration to Membrane Tank Only		Normal Flow with Cycled Aeration to Membrane Tank Only		Normal Flow with Cycled Aeration to Membrane and Aeration Tanks	
Parameter		(E	vent 9)	(Event 10)		(Event 11)		(Ev	ent 12)
Physical/Chemical	Permeate Target ^a	Feed	Permeate	Feed	Permeate	Feed	Permeate	Feed	Permeate
pН				7.06	7.13	-		7.13	7.33
Temperature (degrees C)		29.3	29.8	29.4	30.3	29.1	31.0	28.1	26.6
Turbidity (NTU)	< 0.2		0.12		0.10		0.13		0.14
Conductivity (µS/cm)		1,796	1,533	1,695	1,487	1,595	1,448	1,575	1,338
COD (mg/L)				448	15.0			292	14.0
CaH (mg/L as CaCO ₃)					280		300		316
ALK				360	110	320	124	380	180
Biological									
CBOD ₅ (mg/L)	< 2	146	0.03	157	0.15	154	0.17	154	0.37
TSS (mg/L)	< 1	104		184	0.20	140	0.20	220	0.27
T-Phosphorus (mg/L as P)		6.07	3.19	5.45	1.44	3.87	2.73	4.94	1.44
NH ₃ -N (mg/L as N)	< 0.5	21.30	0.05	24.85	0.15	17.20	0.14	24.28	0.31
TKN (mg/L as N)		42	2.0	43	2.0	39	2.0	47	2.85
NO ₂ /NO ₃ -N (mg/L as N)		0.01	18.30	0.02	13.5	0.01	20.10	0.01	3.96
Total Nitrogen (mg/L as N)		42	20	43	16	39	22	47	7
Microbial									
Total Coliforms (CFU/100mL)	< 2.2				8.5		9.0		6.4
Fecal Coliforms (CFU/100 mL)	0				2.0				
HPC (CFU/mL)	< 500				2,102		1,600		2,458

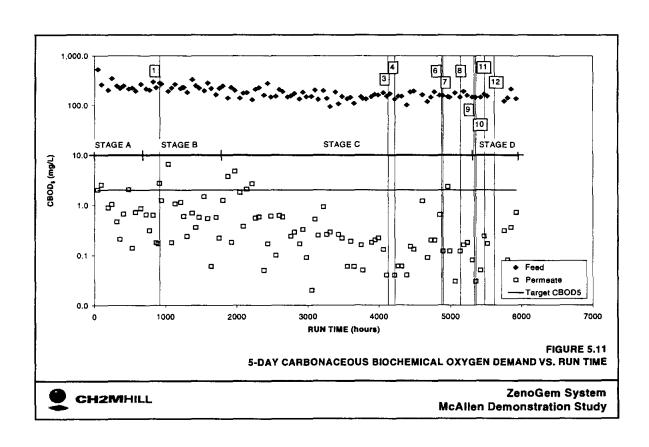
^aWhere target left blank, no target was established.

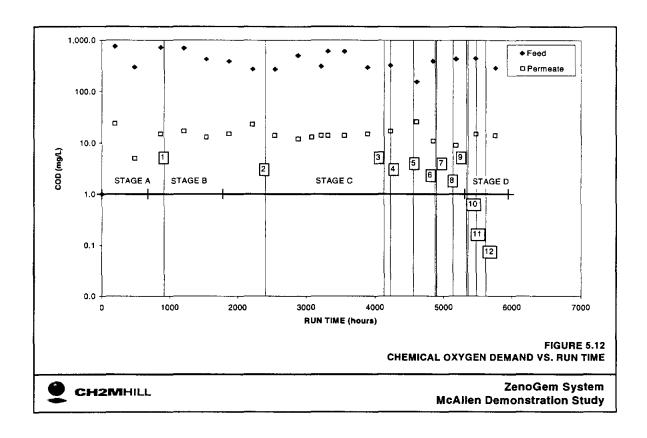
Particle Removal. The ZenoGem system achieved greater than 99 percent removal of TSS and CBOD during all stages of operation and was effective in reducing TSS and CBOD₅ in the wastewater to below target levels as shown in Figures 5.10 and 5.11. TSS measurement is not sufficiently sensitive to detect potential differences in TSS removal as a function of MLSS concentration. Figure 5.12 illustrates that COD was consistently reduced to less than 20 mg/L in the ZenoGem permeate. COD removal efficiency was not impacted by MLSS concentration.

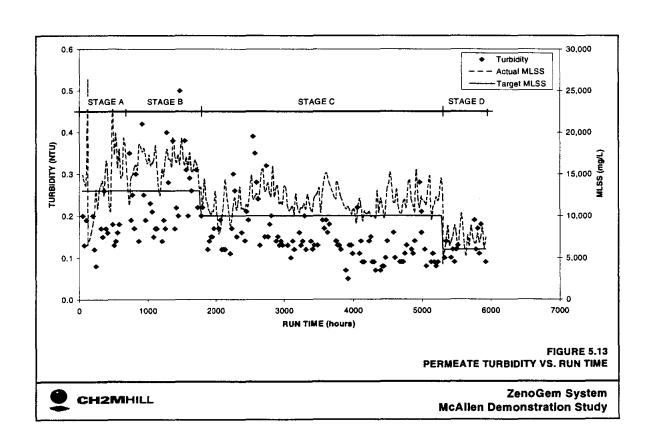
As shown in Figure 5.13 and Table 5.8, the average permeate turbidity was slightly higher in Stage B as compared to Stage A and to the target level of 0.2 NTU established for feedwater to the downstream RO system. This suggests greater particle passage through the OKC MF versus the OCP UF membrane at the higher MLSS concentration. Permeate turbidities were higher during Stage B than Stage C (see Table 5.9), suggesting that particle passage through the OKC membrane is greater at high solids loading (high MLSS concentration).

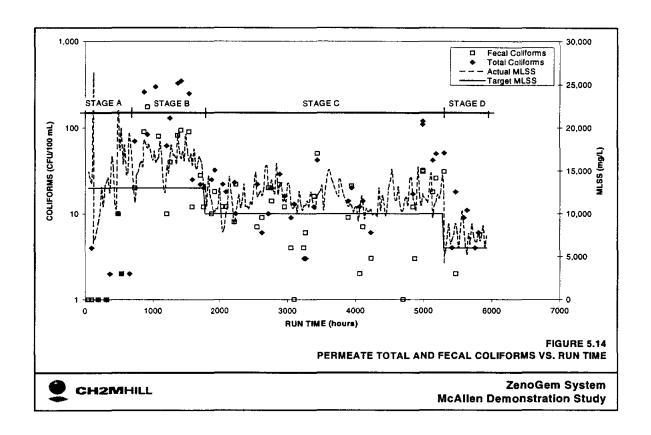
Microbial Removal. Trends observed for turbidity removal were also seen with microbial removal. As shown in Figure 5.14, the average total and fecal coliform levels were higher in Stage B as compared to Stage A. This suggests greater bacteria passage through the MF versus the UF membrane at equal MLSS loadings. The increase coliform levels observed in Stage B compared to Stage C suggest bacteria passage through the MF membrane is a function of MLSS concentration. The high HPC levels may reflect bacterial regrowth in the ZenoGem permeate piping in the absence of a continuous disinfectant. In general, total and fecal coliform levels exceeded the informally adopted goal of State of California "Title 22" regulations pertaining to unrestricted access (2.2 CFU/100 mL for total coliforms and 0 CFU/100 mL, respectively).











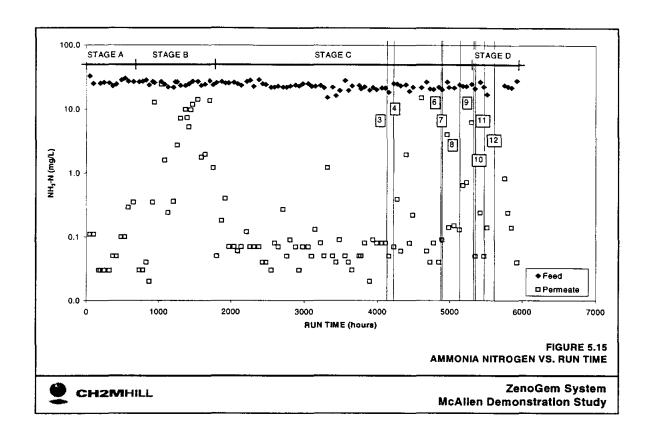
Nutrient Removal.

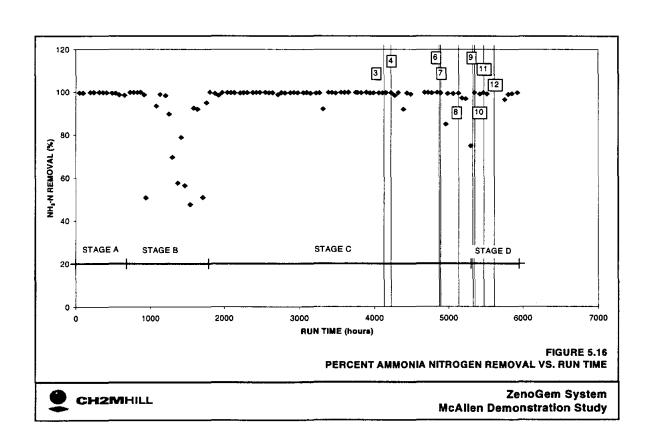
Nitrogen Transformation. At the long SRTs used in this study and the high wastewater temperatures, the activated sludge portion of the ZenoGem process should be able to achieve complete nitrification, i.e., the conversion of ammonia-nitrogen to nitrate-nitrogen. A potential constraint is the ability to supply sufficient oxygen to the process, given the relatively short HRT and the high volumetric organic loading rate. Assuming sufficient DO levels and a well mixed biomass, denitrification should be minimized. These were the expectations at the start of the study.

Ammonia Removal. Ammonia nitrogen feed and permeate levels and percent removal by ZenoGem as a function of operating time are shown in Figures 5.15 and 5.16. Feed levels were relatively constant, ranging from 15 to 30 mg/L. Permeate concentrations were less than the target of 0.5 mg/L at normal flow conditions, except during Stage B. Removals were essentially complete during all stages, except Stage B. Reduced removals (partial/incomplete nitrification) during Stage B most likely reflect impaired efficiency of oxygen transfer to the nitrifiers within the dense flocs present at the higher MLSS concentration (~13 g/L) and high wastewater temperatures. Although dissolved oxygen levels in the bulk liquid were within acceptable range to achieve nitrification (under conventional wastewater MLSS levels), transfer of this oxygen from bulk liquid to bacteria contained within the flocs was not sufficient to achieve complete nitrification at the provided HRT. The reduced nitrification efficiency at higher MLSS levels suggests that MBR operation at such levels may be constrained by oxygen transfer efficiency unless such a constraint can be overcome by increase air input or better gas-to-liquid transfer efficiency than attained in this study.

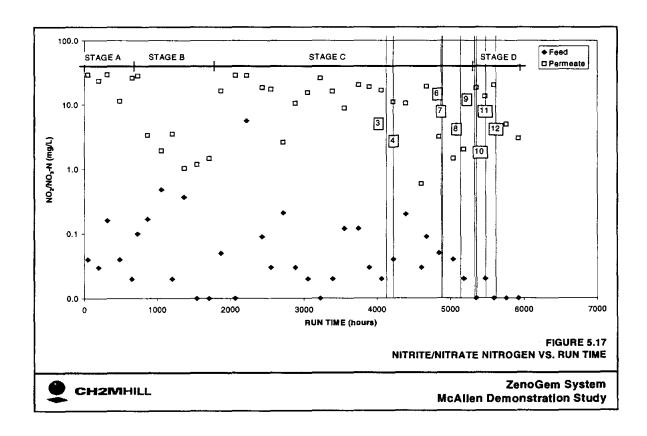
When comparing normal flow versus flow peaking in Stages B and C, nitrification (ammonia removal) was incomplete during peaking due to the decrease in HRT from 5.7 hrs to 3.9 hrs. Cycled aeration to the membrane tank had no real effect on nitrification efficiency in Stage C. Ammonia removal was reduced from 98 to 97 percent only. This result is not surprising as most of the oxygen for biological oxidation is provided in the aeration tank. During Stage D, flow peaking with cycled aeration to both tanks during showed no significant decrease in nitrification when compared to normal flow and full aeration operation.

During all stages, the rate of nitrification was calculated at $0.48 \text{ mg/L NH}_3\text{-N}$ per mg/L MLVSS per day regardless of MLSS concentration or permeate flowrate. However, during cycled aeration to both tanks in Stage D, the nitrification rate increased to $0.72 \text{ mg/L NH}_3\text{-N}$ per mg/L MLVSS per day.





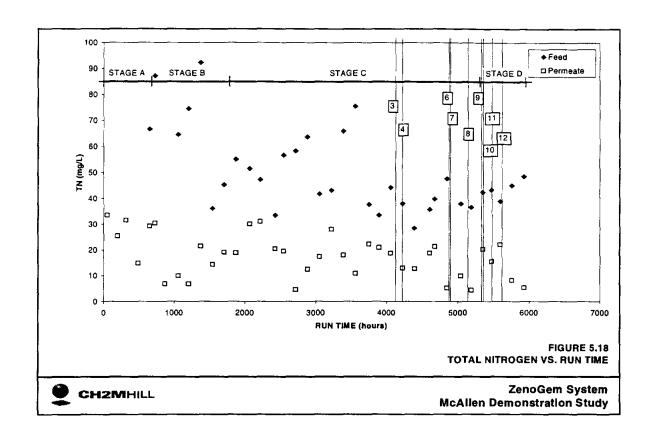
Nitrite/Nitrate Removal. Feed and permeate nitrite/nitrate nitrogen levels for the ZenoGem system as a function of operating time is shown in Figure 5.17. Feed levels were < 0.4 mg/L in all cases, as anticipated. Permeate levels ranged from 15 to 19 mg/L in Stages A and C. During Stage B and the end of Stage D, permeate levels were significantly less. Permeate levels are a function of the amount of ammonia and organic nitrogen converted to nitrite/nitrate (nitrification) and the extent to which this "converted" nitrogen is reduced to nitrogen gas by denitrifiers. In an aerated system, denitrification (nitrite/nitrate conversion to nitrogen gas) is not anticipated as the bacteria responsible for this reduction operate under anoxic conditions. During Stages A and C, denitrification was minimal yielding higher permeate nitrite/nitrate levels. However during Stage B and the end of Stage D, a significant fraction of the nitrite/nitrate generated from nitrification was converted to nitrogen gas, resulting in a condition of "simultaneous nitrification/denitrification" thus yielding lower permeate nitrite/nitrate levels. This result is consistent with the hypothesis offered under the Ammonia Removal discussion where reduced oxygen transfer creates micro anoxic zones within the mixed liquor, providing conditions conducive to the growth of denitrifiers. At the end of Stage D, conditions to produce this effect were put into place through cycled aeration in both treatment tanks. Such conditions were very effective for achieving a high level of both nitrification and denitrification, as illustrated by the data in Table 5.10 (Event 12) where permeate ammonia and nitrite/nitrate nitrogen concentrations were 0.31 and 3.96 mg/L, respectively.

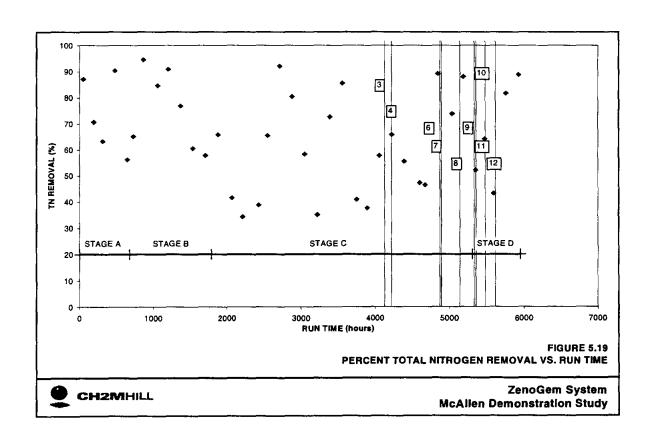


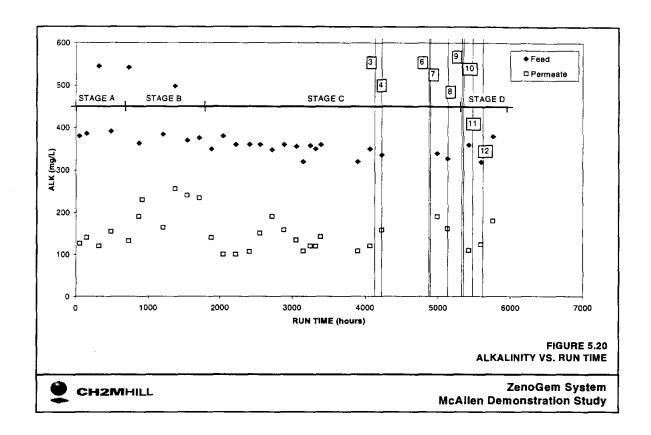
Total Nitrogen Removal. Feed and permeate total nitrogen (TN) levels and percent removal by the ZenoGem system as a function of operating time are shown in Figures 5.18 and 5.19. Feed TN levels were exceptionally high during Stages A and B, decreasing to the 38 to 47 mg/L range during the remainder of testing. As shown in Tables 5.8 through 5.10, highest permeate TN levels were observed at normal flow rates and at low to medium MLSS levels. Cycled aeration to the membrane tank had only minor impact on TN levels. TN removal was higher in Stage B as compared to Stage C due to nearly complete denitrification, in spite of the fact that partial nitrification (higher permeate ammonia and lower permeate nitrite/nitrate levels) was observed. TN removal decreased as a result of complete nitrification (lower permeate ammonia and higher permeate nitrite/nitrate levels) and reduced denitrification when the MLSS concentration was decreased in Stage C. The greatest degree of TN removal was observed at the end of Stage D (Event 12) during cycled aeration to both tanks. As previously discussed, such aeration is effective at maximizing simultaneous nitrification/denitrification. With a 15-minute on/off aeration cycle, the ZenoGem system was capable of reducing TN levels to 7 mg/L.

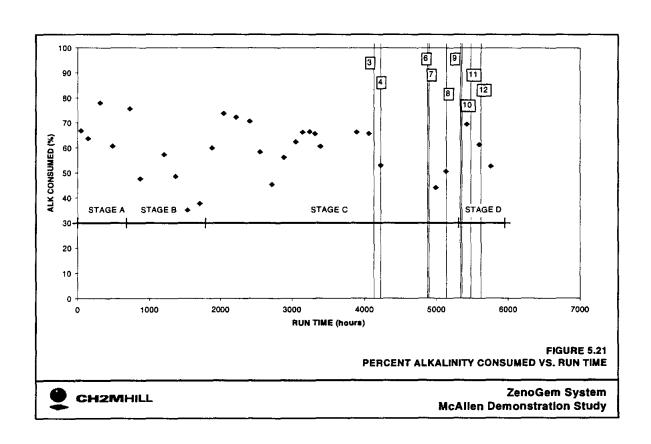
Alkalinity Consumption. During nitrification, alkalinity is consumed. During denitrification alkalinity is created. Assessing alkalinity reductions during the various stages of operation provides a means of "proofing" observed ammonia removals as well as providing a semi-quantitative measure of biological oxidation of non-ammonia organic nitrogen compounds. . Theoretically, 7.1 parts of alkalinity are consumed for each part of ammonia oxidized. As shown in Figure 5.20 during Stage B, alkalinity levels were reduced from an average of 422 mg/L as CaCO₃ in the feed to 203 mg/L as CaCO₃ in the permeate, yielding an alkalinity consumption of 219 mg/L as CaCO₃. In Stage C, levels were reduced from an average of 352 mg/L as CaCO₃ in the feed to 128 mg/L as CaCO₃ in the permeate, yielding an alkalinity consumption of 224 mg/L as CaCO₃.Based on an average ammonia nitrogen removal of 20 mg/L in Stage B and 23 mg/L in Stage C, 142 mg/L and 163 mg/L of alkalinity (as CaCO₃) should have been consumed in Stages B and C, respectively. The additional alkalinity consumption (77 mg/L as CaCO₃ in Stage B and 61 mg/L in Stage C) would have resulted from the biological oxidation of (non-ammonia) nitrogen compounds present in the wastewater. Ammonia nitrogen accounted for only 34 percent of the 75 mg/L of organic nitrogen (TKN) in Stage B and only 49 percent of the 47 mg/L of TKN in Stage C. These levels of TKN are unusually high for a domestic wastewater and indicate that nitrogen-rich discharges are present in the McAllen wastewater.

From previous discussions, nitrification was reduced and denitrification was significant during Stage B. Alkalinity changes between ZenoGem feed and permeate should reflect these differences; alkalinity removals during Stage B should be less than during Stage C as less alkalinity is consumed (from nitrification) and more is created (from denitrification). As shown in Figure 5.21, average alkalinity removal was 50 percent for Stage B and 64 percent for Stage C. Another way of comparing alkalinity consumption and nitrogen transformation is to correlate alkalinity consumption with total nitrogen removal. Lesser alkalinity consumption should occur with greater nitrogen removal as the ratio of nitrogen transformed from nitrate to nitrogen gas increases relative to the amount of organic nitrogen oxidized to nitrite/nitrate. Total nitrogen removal was 76 percent for Stage B and 58 percent for Stage C.

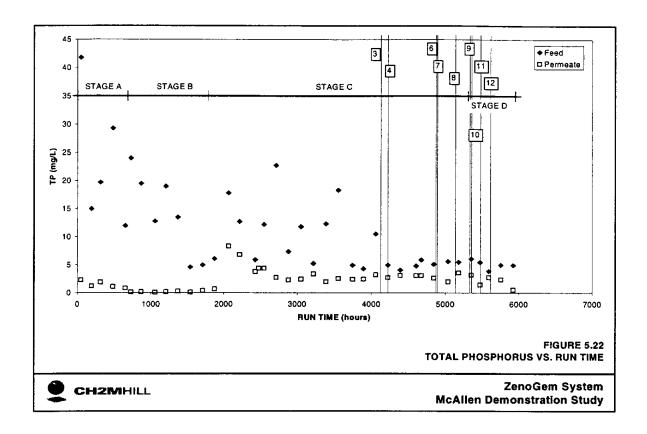


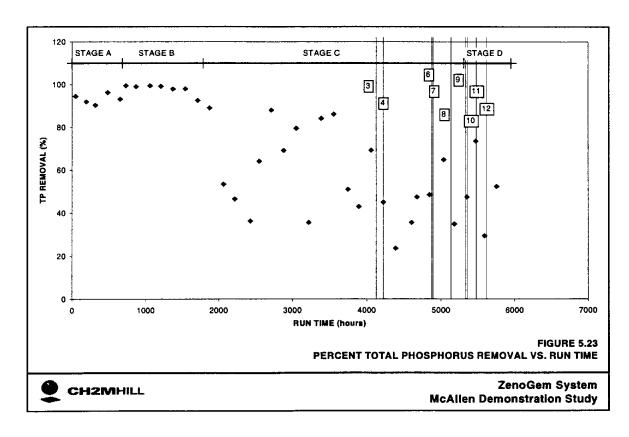






Phosphorus Reduction. Feed and permeate total phosphorus (TP) levels and percent removal by the ZenoGem system as a function of operating time are shown in Figures 5.22 and 5.23. Phosphorus reduction by the ZenoGem process was significantly greater in Stage B than in Stage C at 98 percent and 58 percent, respectively. At the higher MLSS concentration, oxygen transfer to certain zones of the aeration tank was most likely poor, resulting in anaerobic conditions within segments of the biomass producing favorable conditions for biological phosphorus uptake. When the MLSS level was reduced at the beginning of Stage C, these anaerobic zones were eliminated (or greatly reduced) and the phosphorus bound in these organisms was subsequently released, causing phosphorus removal to temporarily increase as shown in Figure 5.23. During the latter part of Stage C, the phosphorus levels in the permeate were in the 2 to 5 mg/L range, which is typical for the conventional wastewater treatment process using secondary treatment and nitrification. Phosphorus removal variability in Figure 5.23 reflects variability in the measured phosphorus levels in the ZenoGem feedwater. Also during Stage C, the phosphorus reduction decreased from 58 percent at normal flow/flux to 40 percent during flow peaking due to the decrease in HRT (insufficient time for phosphorus removal).





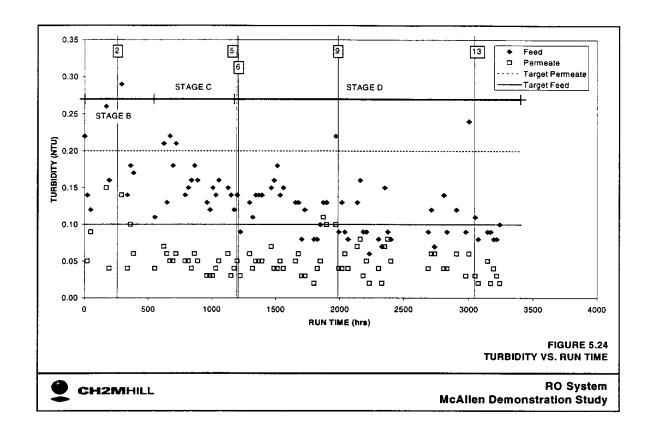
5.3 RO Testing Results

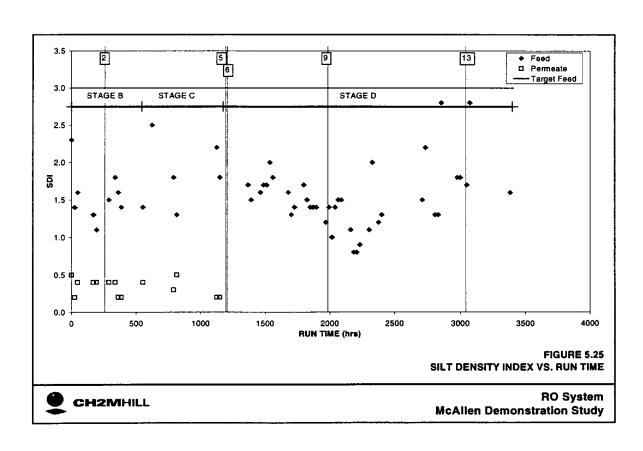
5.3.1 RO Feedwater Quality

Particulate Fouling Potential. Table 5.11 presents the average values for the RO feedwater quality parameters that reflect particulate and colloidal fouling potential (turbidity, SDI and heterotrophic bacteria). For all stages of testing, turbidity and SDI values were less than corresponding target levels, reflecting the low particle water produced by the ZeeWeed membrane. (Turbidity and SDI targets are those established by the spiral wound RO industry based on minimizing RO element fouling and cleaning. With a few exceptions, RO feedwater turbidity averaged less than the 0.2 NTU target (Figure 5.24). As shown in Figure 5.25, the ZenoGem system consistently produced a permeate with a SDI less than the target value of 3. The target of 500 CFU/mL for HPCs is an informal goal that is related to the acceptable level of HPCs in drinking water. There is not established correlation between HPC level in RO feedwater and degree of biological fouling, however, the greater the level the greater the potential to establish biofilms. Actual propensity to form biofilms depends on a number of interrelated factors, including organism type, level of nutrients, water chemistry, membrane material and flow hydraulics through the element. HPC levels were consistently above the target, however, as discussed in a later section of the report, there was no evidence of biological fouling. Taken together, the data in Table 5.11 indicate that the permeate from the ZenoGem permeate should cause little if any particulate fouling of downstream RO membranes.

TABLE 5.11
Average RO Feedwater Quality Parameters

Parameter	Target	Stage B	Stage C	Stage D
Turbidity (NTU)	< 0.2	0.18	0.16	0.11
SDI	< 3	1.46	1.83	1.53
HPC (CFU/mL)	< 500	3,274	865	1,444





Mineral Precipitation Potential. Section 3 discussed the need for chemical conditioning of the RO feedwater to prevent the precipitation of calcium carbonate and barium sulfate, based on their levels in the WWTP secondary effluent and the degree to which their coions would be concentrated during RO treatment at target recovery. The mineral saturation calculations provided in the RODesign program (and also by the scale inhibitor suppliers contacted at the beginning of the project) estimate percent saturation for only the following sparingly soluble salts: calcium carbonate, calcium fluoride, barium sulfate, calcium sulfate, strontium sulfate and silica. Consequently, other sparingly soluble salts present in the effluent, including calcium phosphate salts, were not identified as being supersaturated as a result of RO treatment of the ZenoGem permeate. As discussed in Section 5.3.2 of this report, precipitation of calcium phosphate salts occurred during testing and required additional feedwater acidification to control. Analysis of spent cleaning solutions and materials removed from the membrane surface from element autopsies, showed that calcium carbonate and barium sulfate scaling was effectively controlled and that calcium phosphate was the major mineral precipitate.

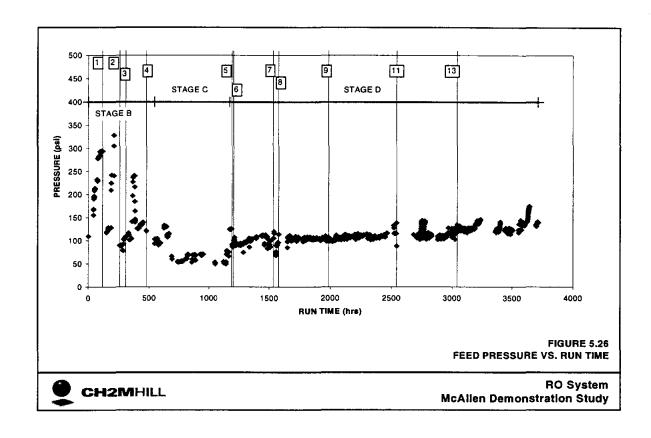
5.3.2 RO Operating Conditions/Membrane Performance

Operating Conditions. Table 5.12 presents the average RO system operating conditions for the following parameters: (recovery, flux, flow, pressure, and conductivity). With the exception of periods during Stage B, the RO system operated at or near target flowrates. Average feed pressure and permeate conductivity was significantly greater during Stage B operation at high recovery because of the increase resistance to flow caused by scaling in the second stage elements during this period. Feed pressure variations as a function of operating time is shown in Figure 5.26. This plot clearly illustrates the high feed pressure periods associated with scaling of the second stage membrane elements during Stage B. These effects were reversed by citric acid cleanings (Events 1, 3 and 4).

TABLE 5.12
Average Operating Conditions for the RO System

		Target	Actual	-		Flow (gpm)			Pressure (pai)			Conductivity (µS/cm)			
Stage	Operation	Recovery (%)	Recovery (%)	Flux gfd	Feed	Conc	Permeate	Feed	Interstage	Conc	Feed	Interstage	Conc	Permeate	
В	182	80	70.4	10.37	3.98	0.94	2.85	231	220	213	1,608	4,408	3,729	182	
Bª	182	50	59.0	10.63	5.04	2.29	2.92	132	111	91	1,701	3,544	4,024	150	
С	1	50	47.9	9.83	4.11	2.31	2.01	80	NA	65	1,636	3,167	3,330	71	
D	1&2	50	48.9	7.71	5.45	2.67	2.95	125	100	63	1,798	2,958	3,520	104	
D	1&2	62	63.8	10.03	4.33	2.76	1.45	90	76	63	1,814	3,510	5,017	148	
D	1&2	70	68.1	10.50	4.24	2.89	1.41	101	86	74	1,741	3,408	4,998	118	
D	1&2	74	72.6	10.62	4.02	2.92	1.12	110	97	87	1,549	3,187	4,970	95	
D	1&2	80	79.3	11.89	4.12	3.27	0.86	128	115	107	1,731	3,841	7,210	105	

^{*}Target feedwater recovery decreased from 80 to 50 percent after 256 hours of operation (Event 2). NA≖Not Applicable



Performance Parameters. Table 5.13 presents RO system target and average actual membrane performance parameters (NPF, salt passage and salt rejection) as a function of operating time. Figure 5.27 illustrates changes in flux as a function of operating time. Membrane flux varied considerably during Stage B, decreasing in proportion to the decline in system productivity. Although testing called for operation at constant flux, the rapid and severe increases in feed pressure make it difficult for the plant operators to provide such control. The step decrease in flux during Stage C was intentional and reflects an attempt to reduce RO fouling potential. Flux was steady during Stage D as mineral precipitation and feed pressure was more effectively controlled.

TABLE 5.13

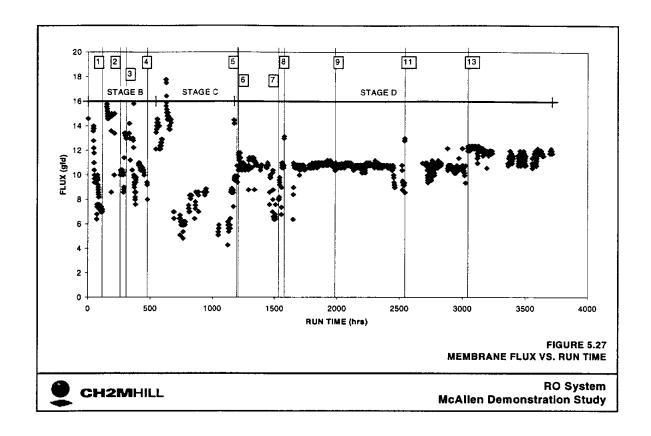
Average Membrane Performance Parameters for the RO System

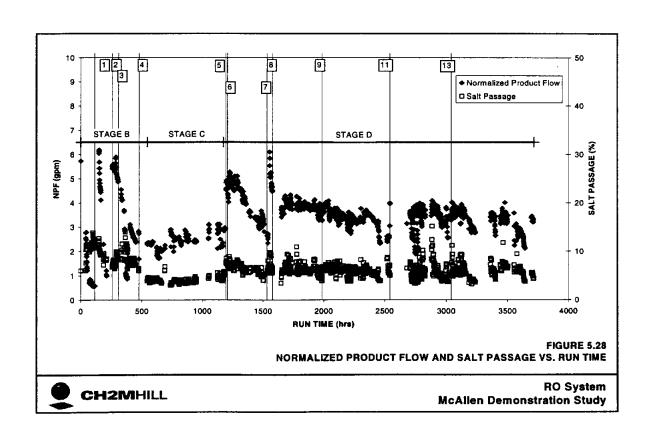
Stage	Stages in Operation	Target Recovery (%)	Normalized Product Flow (gpm)	Salt Rejection (%)	Salt Passage (%)
В	1&2	80	1.88	89.26	10.74
B^a	1&2	50	3.47	91.65	8.30
С	1	50	2.38	95.90	4.10
D	1&2	50	2.92	94.57	5.43
D	1&2	62	4.71	92.27	7.73
D	1&2	70	4.02	93.63	6.37
D	1&2	74	3.36	94.18	5.82
D	1&2	80	3.39	94.24	5.76

^aTarget feedwater recovery decreased from 80 to 50 percent after 256 hours of operation (Event 2).

Similarly, NPF showed severe and rapid declines during Stage B. As shown in Figure 5.28, these declines were readily reversible by citric acid cleanings, however operation at high recovery and feed pH (6.8) was not sustainable on a long-term basis. At lower recovery (Stage C), NPF was quite stable confirming that performance declines were recovery and scaling related. With return to two-stage operation and recovery of 70-75 percent (Stage D), NPF again declined but a lesser rate, reflecting the partial effectiveness of reduced pH (6.0-6.5) operation. However, stable performance could not be achieved until feedwater pH was reduced to 5.0, corresponding to a concentrate pH of 5.6. As recovery was further increased to 80, inability to effectively control concentrate pH at 5.6 again resulted in rapid NPF decline.

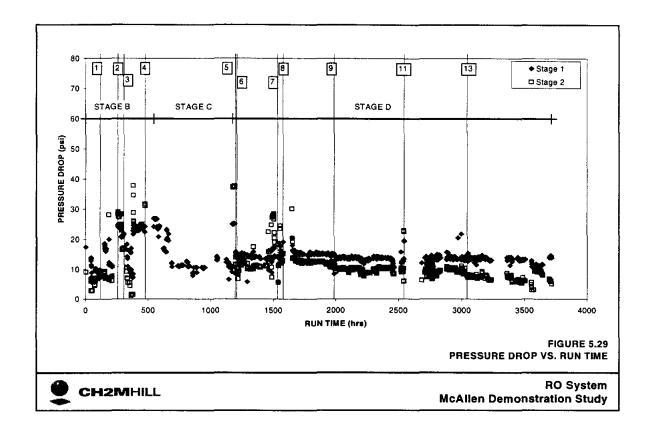
Normalized salt passage was less impacted by scaling than NPF, with the exception of Stage B operation when scaling was worst (Figure 5.28). Normalized salt passage was comparable at the very beginning of Stage B (6 percent at 4 hours) and at the end of routine testing (5 percent at 3,400 hours). This indicates no loss in salt rejecting capability by the RO membranes over the course of this testing despite repeated membrane scaling and citric acid cleaning.

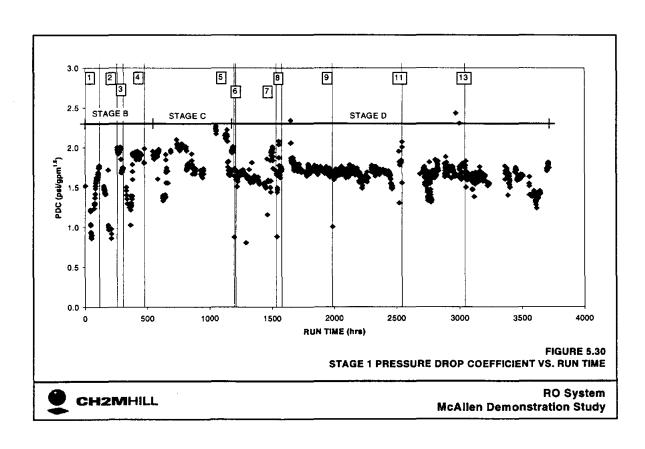




Figures 5.29 and 5.30 present vessel differential pressure (pressure drop) for each RO system stage during the testing as well as pressure drop coefficient for Stage 1 only as a function of operating time. In RO systems operating on MF-treated wastewater effluent or MBR permeate, pressure drop is monitored primarily to indicate the occurrence biological fouling, which causes a characteristic rise in Stage 1 pressure drop. Pressure drop reflects the resistance of water flow through the RO element feed spacer. As material accumulates within the spacer or on the membrane surface, pressure drop increases. Pressure drop coefficient accounts for changes in flow through the pressure and allows for a better comparison of systems operating at different recoveries. In general, the data in the figures indicate the absence of biological fouling. Stage 1 PDC was relatively unchanged, except during the beginning of Stage B. During the period considered most representative of a properly operated RO system (Stage D, 1,500 to 3,000 hours), both pressure drop and PDC were extremely stable. The very gradual decline in pressure drop during Stage C was associated with the decrease in recovery (lower feedwater flow through the feed channels).

¹Pressure drop coefficient (PDC) is defined as follows: PDC = pressure drop /(feed flowrate)^{1,5}





Calcium Phosphate Scaling and Its Impacts on RO System Feed Pressure and Productivity. During Stage B, NPF declined rapidly (see Figure 5.28). Cleanings with citric acid were effective in restoring performance losses (Event 1) but with subsequent operation, NPF again rapidly declined. At this time, mineral precipitation was considered the likely cause for loss of RO performance. Biofouling was unlikely based on stable pressure drop readings. A second citric acid cleaning was then conducted (Event 2) and a portion of the second stage spent cleaning solution was analyzed to better determine the nature of the mineral precipitant. Calcium, aluminum and phosphorus were present in elevated concentrations relative to the other metals. Calcium and aluminum phosphate salts were considered the primary scaling concern, as calcium carbonate precipitation was controlled by feedwater acidification. Appendix E presents results of the cleaning solution analysis.

To determine the exact type of scale, the ZenoGem permeate, which becomes RO feedwater after chloramination, was analyzed twice a week during the period June 9 through June 23, 1999 for ions that can form precipitable salts, including phosphorus and sulfate, and metals, including barium, aluminum, and iron. (Calcium hardness, alkalinity and phosphorus levels in the ZenoGem permeate were routinely analyzed as part of ZenoGem peformance monitoring protocol.) The analysis showed less than detectable levels of the oxidizable metals aluminum and iron (<0.1 mg/L). Barium and sulfate were present at concentrations less than their solubility (as barium sulfate salt) for operation at 80 recovery (0.06 mg/L and 226 mg/L, respectively). Phosphorus levels were significant relative to natural water supplies (14 mg/L). Given the high concentration of calcium hardness in the wastewater (356 mg/L), calcium phosphate scaling was indirectly suspected. Appendix F presents results of ZenoGem permeate ion analyses.

To further confirm that scaling and not fouling caused performance losses, the second stage was removed from service after 546 hours of operation and the first stage was operated at 50 percent recovery (Stage C). At the lower percent recovery and operating only the first stage vessels, the feed pressure and NPF decreased and remained relatively low and constant during Stage C. Performance stabilized at the lower recovery confirming that performance declines were a result of ion concentration and mineral precipitation. Calcium phosphate scaling is not commonly encountered in municipal RO operations because phosphate levels in most natural raw water supplies are not elevated. Furthermore, based on discussions between CH2M HILL and several scale inhibitor manufacturers (i.e., FMC, KLT, Permacare), calcium phosphate precipitation is not effectively prevented by commercially available RO scale inhibitors. Consequently, three scaling mitigation methods were considered to control the precipitation tendency in lieu of a specific inhibitor:

1. Decrease RO feedwater pH. The calcium phosphate solubility index² was used to calculate the pH of the RO concentrate at which calcium phosphate concentration in the RO concentrate would be less than solubility (SI = pH-pH_c, where SI is <0). By trial and error iteration, the resulting pH was used to calculate corresponding feed

The calcium phosphate solubility index (SI) is defined as follows: $SI = pH - pH_c$, where $pH_c = 11.755 - (log calcium ions + log of phosphate ions = 2*log temperature)/0.65 (Green and Holmes, 1947).$

pH using Hydranautics RODesign and the design conditions discussed in Section 3.3.1. Although this approach would require significant acid dose (~100 mg/L), it has the added benefit of increasing the solubility of both aluminum phosphate and calcium carbonate. This approach was considered the easiest to implement for this study.

- 2. Chemically precipitate excess phosphorus from the screened, degritted wastewater during ZenoGem treatment. Addition of an aluminum or iron salt to the wastewater would produce highly insoluble aluminum or ferric phosphates easily filterable by the ZeeWeed MF membrane. It was calculated that a dose of 45 mg/L of ferric chloride would be required to reduce the phosphate concentration in the ZenoGem permeate to 0.5 mg/L. a level that would reduce the calcium phosphate solubility index to < 0 at 80 percent recovery. This level of coagulant addition would generate more sludge, increase MLSS concentrations, require a reduction in SRT to maintain the 10 g/L target MLSS concentration and potentially increase the fouling rate of the ZeeWeed membrane.
- 3. Biologically remove phosphorus by creating an anaerobic zone in the membrane bioreactor. This was done in an uncontrolled manner during ZenoGem Stage B operation but would require extensive testing to develop the necessary operating strategy relative to oxygen input. Such testing was beyond the scope of this project.

The second stage was returned to service after 1,177 hours of operation (Stage D) and the system continued to operate at 50 percent recovery. After 1,533 hours of operation and step-wise increase in recovery to 70 percent, a target pH of 5.6 was established for the RO concentrate (corresponding to feed pH of 5.0) to maintain calcium phosphate solubility (Scaling Mitigation Method 1). However, difficulties with both the acid feed pump and PLC pH control loop caused difficulty in consistently maintaining the pH during the remainder of testing. After 1,579 hours of operation, the fourth acid cleaning was performed. Feed pressure and NPF was reduced by the cleaning and remained relatively constant until feedwater was increased to 75 percent after 1,985 hours of operation. Thereafter, feed pressure increased and NPF decreased until another cleaning was performed at 2,544 hours of operation to restore performance. Increasing the recovery to 80 percent after 3,042 hours of operation resulted in a rapid increase in feed pressure and decrease in NPF. These results indicate that the decrease in RO feedwater pH effectively stabilized system performance and reduced fouling potential when operating at a feedwater recovery up to 70 percent. Stable system performance could not be maintained at the higher recoveries (75 to 80 percent), even with the decrease in RO feedwater pH.

Autopsy of the trailing element(s) from Stage 2 confirmed calcium phosphate as the primary precipitate (see Appendix G).

5.3.3 RO Water Quality Impacts

Control of Major Contaminant Categories. Table 5.14 presents the results of water quality analyses of the RO system feed, permeate, and concentrate during each stage of operation. These data are presented to illustrate the ability of RO treatment to reduce the concentration of particulate, microbial, inorganic and organic contaminants in the ZenoGem permeate (i.e., wastewater effluent). Per the objectives of the study, the following surrogate parameters were monitored through the study to demonstrate such removal capability: turbidity (representing particles), coliforms and HPCs (representing pathogenic bacteria), conductivity and TDS (representing inorganic) and TOC (representing organic).

TABLE 5.14
Average Water Quality Results for the RO System

Parameter			Stage B			Stage C			Stage D	
Physical/Chemical	Permeate Target	Feed	Permeate	Conc	Feed	Permeate	Conc	Feed	Permeate	Conc
pH		7.13	6.00	7.32	7.30	6.07	7.44	6.22	5.66	6.06
Conductivity (uS/cm)		1,651	86	3,420	1,560	63	3,718	1,668	110	5,367
Turbidity (NTU)	< 0.1	0.18	80.0	0.54	0.16	0.05	0.32	0.11	0.05	0.36
SDI		1.46	0.33		1.83	0.32		1.53		1.57
TOC (mg/L)	< 1	6.18	< 0.5		6.77	< 0.5		6.62	< 0.5	
TDS (mg/L)	< 500	999	51	2,341	943	44	1,702	899	73	3,503
Microbial										
Total Coliform (CFU/100 mL)		2.0	7.0		5.7	2.9		6.0	1.0	
Fecal Coliform (CFU/100 mL)	0				2.0	2.0		3.0	2.0	
HPC (CFU/mL)		3,274	110		865	65		1,444	276	

^aWhere target left blank, no target was established.

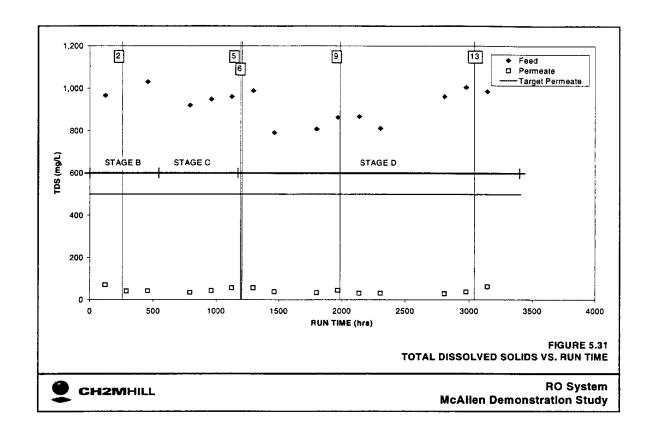
Particulate. As described in earlier in this section, turbidity levels in the RO feedwater were well controlled by ZeeWeed membrane (average of 0.15 NTU). Consequently, only minor improvements in turbidity were possible by the RO system. RO permeate turbidity was consistently measured at to 0.05 NTU. This compares with the target level of 0.1 NTU and the current Environmental Protection Agency (EPA) regulatory level of 0.3 NTU for conventional water treatment plants (95 percent of readings).

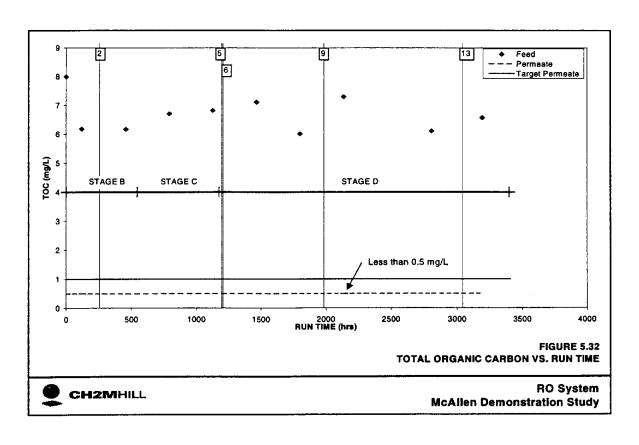
Microbial. The target level of coliforms was established at 0 CFU/mL. Coliforms were routinely measured in the RO permeate, typically at levels of 2 CFU/mL based on similar levels in the feed. This is surprising given the presence of a low level of monochloramines in the RO feed and permeate. HPCs were reduced by more than an order of magnitude by RO treatment, with permeate levels less than the drinking water trigger level of 500 CFU/100mL.

Inorganic. At the target 80 percent recovery (beginning of Stage B and end of Stage D), RO treatment produced an effluent (permeate) having an average TDS of 66 mg/L (in the absence of mineral scaling effects), significantly below both federal and State of Texas secondary drinking water standard for TDS (500 and 1,000 mg/L, respectively). The average RO permeate TDS compares very favorably with the 700 to 800 mg/L TDS level that is typical for the City's existing raw water supply (Lozier, 1998). As shown in Figure 5.31, permeate TDS was consistently < 75 mg/L (greater than 92 percent removal) throughout the study, despite periods of severe membrane scaling.

Organic. As shown in Figure 5.32, TOC levels in the RO permeate grab samples were consistently less than detectable (0.5 mg/L) based on a feedwater TOC range of 6 to 8 mg/L. This represents greater than 92 to 94 percent TOC removals. By comparison, TOC levels in the City's existing raw water supply average 3.8 mg/L (Lozier, 1998) and the California Dept. of Health Services TOC limit for direct injection of reclaimed water is 1 mg/L.

In association with RO membrane integrity studies conducted by the BOR and coincident with these research, permeate TOC levels were measured on-line using two low detection limit (20 ppb) analyzers provided by Sievers and Anatel on a short-term trial basis. Other sites using the Sievers instrument have shown RO systems treating microfiltered secondary effluent contain less than 100 µg/L TOC.





5.4 Impacts of IPR on Waste Discharges

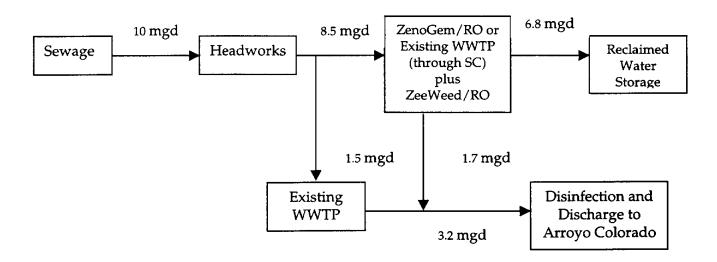
One of the objectives of this testing was to characterize the quality of the ZenoGem permeate and RO concentrate for water quality parameters important to the ecosystems of the Arroyo Colorado and Laguna Madre. The former is a non-perennial waterway to which the City currently discharges the effluent from the South WWTP. Flows into the Arroyo Colorado eventually empty into the Laguna Madre, an estuary that is connected to the Gulf of Mexico. Currently, the City's discharge is regulated with respect to three parameters: CBOD₅, TSS, and ammonia nitrogen. The limits for discharge are as follows:

CBOD₅: 10 mg/L
 TSS: 15 mg/L
 NH₃-N: 3 mg/L

As part of a reuse feasibility study previously conducted for the City, TNRCC expressed concern regarding the presence and concentration of nutrient and TDS in the waste stream(s) from a future IPR treatment system, as it would pertain to discharges to these water bodies. The IPR treatment system evaluated in this research would generate one waste stream, the RO concentrate. Sludge from the ZenoGem system would be dewatered and dried using existing WWTP facilities. For the purpose of this evaluation, it is assumed that 8.5 mgd of wastewater from the WWTP would be diverted to ZenoGem/RO treatment system or, alternatively, 8.5 mgd of WWTP effluent (from the secondary clarifiers) would be diverted for ZeeWeed/RO treatment system. With either alternative, 1.5 mgd (average flow) of undiverted secondary effluent would be disinfected and discharged to the Arroyo Colorado as is currently done. As shown in Exhibit 5.3, these assumed treatment scenarios would result in the following discharges:

- 1.5 mgd of effluent from the South WWTP
- 1.7 mgd of RO concentrate (20% of 8.5 mgd RO feedwater flow)

EXHIBIT 5.3Wastewater Discharge Characterization



In both alternatives, the 8.5 mgd of secondary effluent would be processed by RO to produce 6.8 mgd of final efffluent and 1.7 mgd of RO concentrate (waste). This waste concentrate would then be blended with the remaining 1.5 mgd of WWTP effluent (flow which bypasses IPR treatment), disinfected, and discharged to the current location. As shown in Table 5.15, concentrations of TDS, nutrients and TOC were then calculated for the 47:53 blend of WWTP effluent/RO concentrate using the data collected in Appendix D.

TABLE 5.15
Comparative Loading of Critical Contaminants to Arroyo Colorado/Laguna Madre

	(A)	(B)		
Parameter	RO Concentrate (mg/L) ^a	WWTP Effluent (mg/L) ^a	Composite Stream (Blend) Loading (Ibs/day) ^b	Existing WWTP Effluent Discharge Loading (lbs/day) ^c
NO ₂ /NO ₃ -N	29.9	3.45	467	288
T-Phosphorus	10.20	2.38	174	199
TKN	3.16	2	70	167
TDS	3,780	930	65,227	77,562
тос	28.15	7.25	490	605

^aBased on average results of two sampling events.

Calculated as: 8.34*10*B where 10=existing average WWTP effluent flow (mgd).

The comparison shows that for each parameter, the concentration is much higher in the RO concentrate than the WWTP effluent. This reflects the concentration of each parameter by RO treatment and in the case of nitrate, a higher level in the ZenoGem permeate than the WWTP effluent. In some cases, agencies regulate contaminant discharges based on mass loading (pounds of contaminant per day) rather than concentration. Table 5.15 also shows the predicted mass loading for the RO concentrate/WWTP effluent composite stream (blend) verses the current WWTP effluent discharge. In contrast to the concentration comparison, mass loadings for the blend are higher only for nitrate. Consequently, it would be in the City's best interest to work toward establishing mass loading-based discharge regulations versus the current concentration-based regulations if they wish to discharge RO concentrate to the Arroyo Colorado/Laguna Madre ecosystem. If successful, the City could incorporate biological denitrification into the design of the ZenoGem system to control nitrate loadings at the current levels.

^bCalculated as: 8.34*(1.7*A + 1.5*B) where 1.7=RO concentrate flow (mgd) and 1.5=WWTP effluent flow (mgd).

5.5 Comparing Reclaimed and Existing Raw Water Quality

No federal regulations exist regarding the quality requirements for reclaimed water to be used in the context of indirect potable reuse. Currently, such requirements are established on a state-by-state basis. To date, the City has had preliminary meetings with TNRCC regarding such requirements. However TNRCC has not yet proposed regulations for McAllen, but have only referenced potential treatment techniques (e.g., treat all the reclaimed water with RO). To provide a basis for development of IPR regulations for this project, all primary and secondary contaminants currently regulated under the SDWA were analyzed in both the ZenoGem and RO permeates. Results of these analyses are presented in Appendix D. The results were then compared with data from similar characterization of the City's existing raw water supply (Rio Grande River) as sampled in 1997 during the Wastewater Reclamation Pilot Study, City of McAllen, Texas (1998).

Comparing the quality of the ZenoGem permeate to the City's existing raw water supply and to federal and state drinking water regulations as shown in Table 5.16, the following conclusions are drawn:

- The ZenoGem permeate contains greater levels (i.e., lower quality) of most inorganic contaminants than the City's raw water supply. The degradation reflects: 1) the inability of the City's water treatment plant and the ZenoGem process to remove such compounds, and 2) increases in these contaminants from the domestic water use/wastewater generation process. Consequently, the ZenoGem permeate, on at least one sampling event, exceeded the maximum contaminant level (MCLs) for chloride, color (APHA) apparent, and TDS.
- The ZenoGem permeate contains lower concentrations of certain metals (i.e., iron, manganese, aluminum, barium, and strontium) than the City's raw water supply and the MCLs as a result of their removal by oxidation or precipitation in both the WWTP and the ZenoGem processes.
- The concentration of dissolved organic matter (as measured by TOC) is significantly greater in the ZenoGem permeate than the City's raw water supply. Although there is not a current MCL for TOC, the greater the TOC level, the greater the potential for formation of trihalomethanes (THMs) and haloacetic acids (HAAs). These chlorinated byproducts have been shown to be carcinogenic and are regulated at very low levels (μg/L levels). This greater potential is illustrated by the significantly higher levels of HAAs in the ZenoGem permeate relative to the raw water supply. Further, the chronic health risks associated with identified organic compounds in wastewater are not well understood. For this reason, respected authorities in the field of IPR recommend that TOC levels be reduced. In the State of California, a TOC guideline of 1 mg/L has been established for reclaimed water used for surface water supplementation IPR projects.

Particle levels in the ZenoGem permeate are significantly lower than the City's raw
water supply based on turbidity measurements. This reflects the very small pore
size of the MF and UF membranes used with ZenoGem, which serves as a effective
barrier to the passage of most particles.

Comparing the quality of the RO permeate to the City's existing raw water supply and to federal and state drinking water regulations as shown in Table 5.16, the following conclusions are drawn:

- The RO permeate meets all established drinking water regulations as well as the TOC guideline of 1 mg/L.
- To produce reclaimed water meeting state and federal drinking water regulations and the State of California TOC guideline, both ZenoGem and RO treatment of the City's wastewater is required. Assuming an RO permeate TOC of 0.5 mg/L, greater than 90 percent of the wastewater would require RO treatment. If the TOC guideline were not considered, RO treatment would still be required, however, the percent of treatment would be reduced depending on the controlling contaminant (e.g., HAAs, nitrate or TDS). Assuming nitrate would be more cost effectively removed through biological denitrification, approximately 80 percent of the wastewater would require RO treatment to control HAA formation.
- Beyond simply meeting the drinking water regulations, experts involved in setting
 IPR policy strongly recommend the concept of multiple treatment barriers to ensure
 that the proposed treatment scheme adequately protect public health, particularly
 with respect to acute health risk from microbes. In this regard, the combination of
 ZenoGem and RO treatment provides two robust barriers to the passage of viral,
 bacterial and protozoan pathogens as opposed to relying on only a single barrier (i.e.,
 ZenoGem only). An additional barrier or chlorine/UV disinfection may also be
 desirable while only marginally increasing costs.
- If TNRCC were to approach IPR guidelines for this project from the viewpoint that the reclaimed water must equal or exceed the quality of the existing raw water supply, a lower percentage of the ZenoGem permeate would require RO treatment. Based on the data shown in Table 5.16, it is estimated that about 50 percent of the wastewater would require RO treatment to have a reclaimed water match the TOC concentration of the raw water.

TABLE 5.16Results of ZenoGem and RO Permeate Sampling for IPR Characterization

	Primary	Existing F	Raw Water	Zeno	Gem		
	MCL	Sup	plya	Perm		RO Pei	meate
Parameter		3/11/97	6/2/97	8/17/99	9/14/99	8/17/99	9/14/99
General Chemistry							
Alkalinity (mg/L as CaCO ₃)		130	106	121	153	14	16
Bromide (mg/L)		0.100	0.54	0.132	0.32	0.02 ^b	0.02 ^b
Chloride (mg/L)	250	155	207	160	281	9.73	15.20
Color Apparent	15	17	10	22	17	5 ^b	5 ^b
Fluoride (mg/L)		0.59	0.99	1.07	1.14	0.32	0.45
NH ₃ -N (mg/L as N)					0.1 ^b		0.1 ^b
NO ₂ -N (mg/L as N)				9.55	7.90	1.11	1.08
TKN (mg/L as N)				2 ^b	2 ^b	2 ^b	2 ^b
Reactive Silica (mg/L)		6.0	13.5	15.1	16.1	0.65	0.90
Sulfate (mg/L)	250	247	262	150	247	4	5.31
TDS (mg/L)	500 - 1,000	720	772	774	1,950	33	72
TOC (mg/L)	19	3.70	3.90	7.48	5.90	0.63	0.52
T-Phos (mg/L)		0.05	0.05 ^b	2.48	2.89	0.10	0.1 ^b
UV-254 (cm ⁻¹)		0.112	0.092	0.129	0.126		
Metals							
Aluminum (mg/L)	0.05 - 0.2	1.22	0.248	0.111	1 ^b	0.046 ^b	0.1 ^b
Arsenic (mg/L)				0.004*	0.01 ^b	0.004 ^b	0.01 ^b
Barium (mg/L)		0.127	0.124	0.056	0.062	0.0008 ^b	0.025*
Cadmium (mg/L)				.003	0.005 ^b	0.0004 ^b	0.005 ^b
Calcium (mg/L)		77	77.7	72.1	86.9	0.714	833
Chromium (mg/L)				0.007 ^b	0.010 ^b	0.008 ^b	0.01 ^b
Iron (mg/L)	0.3°	0.77	0.171	0.032	0.1 ^b	0.01	0.1
Lead (mg/L)				0.028	0.003 ^b	0.002 ^b	0.003 ^b
Magnesium (mg/L)		22.1	27.9	20.4	25.6	0.197	0.5 ^b
Manganese (mg/L)	0.05°	0.025	0.018	0.015	0.017	0.001 ^b	0.01 ^b
Mercury (mg/L)				0.0003 ^b	0.0003 ^b	0.0003 b	0.0003
Potassium (mg/L)		9	9.58	17.8	29.9	1.36	2*
Selenium (mg/L)				0.007 ^b	0.007 ^b	0.007	0.007 ^b
Silver (mg/L)				0.008 ^b	0.010 ^b	0.008 ^b	0.01 ^b
Sodium (mg/L)		102	140	157	253	13	16.2
Strontium (mg/L)		2.05	2.40	1.87	2	0.029 ^b	0.1 ^b
Zinc (mg/L)				0.463	0.054	0.007	0.02 ^b
Purgeable Volatiles							
Vinyl Chloride				1 ^b	1 ^b	1 ^b	16
tran-1,2-Dichloroethene				1 ^b	1 ^b	1 ^b	1 ^b
cis-1,2-Dichloroethene				1 ^b	1 ^b	1 ^b	1 ^b
1,1,1-Trichloroethane				1 ^b	1 ^b	1 ^b	1 ^b
Carbon Tetrachloride				1 ^b	1 ^b	1 ^b	1 ^b
Trichloroethene				1 ^b	1 ^b	1 ^b	1 ^b

TABLE 5.16 Results of ZenoGem and RO Permeate Sampling for IPR Characterization

	Primary	Existing I	Raw Water	Zeno	Gem		
	MCL	Sup	plya		eate	RO Per	rmeate
Parameter		3/11/97	6/2/97	8/17/99	9/14/99	8/17/99	9/14/99
1,4-Dichlorobenzene				1 ^b	1 ^b	1 ^b	0.60
Disinfection Byproducts							
Trihalomethanes (SDS THMs) ^c (µg/L)	80	236.00	215.00	198.00	244.00	5.40	8.30
Haloacetic Acids (SDS HAA5) ^d (µg/L)	60	58.00	72.00	119.00	90.60	1.10	1.10
Semi-volatile Organics							
Lindane (µg/L)				0.024	0.011	0.02 ^b	0.02 ^b
Endrin (µg/L)				0.02 ^b	0.01	0.02 ^b	0.02 ^b
Methoxychlor (µg/L)				0.04 ^b	0.04 ^b	0.04 ^b	0.04 ^b
Toxaphene (µg/L)				0.5 ^b	0.5 ^b	0.5 ^b	0.5 ^b
Radiochemicals				·			•
Radium-226 (pCi/L)				0.2 ^b	0.2 ^b	0.2 ^b	0.2 ^b
Radium-228 (pCi/L)				1 ^b	1 ^b	1 ^b	1 ^b
Gross Alpha (pCi/L)				1 ^b	1 ^b	1 ^b	1 ^b
Chlorinated Herbicides							
2,4-D (µg/L)				ND	ND	ND	ND
Silvex (2,4,5-TP) (µg/L)			_	ND	ND	ND	ND

^aSource: Table 5.2 of Water Treatment Technology Program Report No. 26

ND =No Detection

pCi/L=picoCuries per liter

bNot Detected at specified reporting limits.

SDS THM - Simulated Distribution System Trihalomethanes (4 species)

SDS HAA5 - Simulated Distribution System Haloacetic Acids (5 species)

^{*}Secondary MCL
*Secondary MCL: Federal = 500 mg/L; State = 1,000 mg/L

⁹Guildeline set by the State of California

SECTION 6

Cost Estimates Using ZenoGem, ZeeWeed, and RO Facilities

This section presents the cost estimates for two advanced treatment systems to produce 6.8 mgd of reclaimed water that would supplement the City of McAllen's drinking water supply by providing a new source of raw water to the City's water treatment plant. The advanced treatment system would be located at the site of the City's south WWTP. The effluent from the advanced treatment system would be of a quality suitable for discharge to a new reclaimed water storage reservoir to be located in the vicinity of the City's existing water treatment plant. It is anticipated that the effluent from the advanced treatment system would receive additional disinfection depending on TNRCC requirements.

UV light disinfection or chlorination are two candidate disinfection methods. The most appropriate may depend on whether the effluent consists of 100 percent RO permeate or a blend of RO permeate and ZenoGem/ZeeWeed permeate¹. In the latter case, UV disinfection may be required because of the increased chlorine disinfection byproduct formation potential of the UF permeate. For the purposes of this exercise, costs for final disinfection have not been included because the method of disinfection has yet to be determined. Costs for disinfection of the UF permeate with chloramines (prior to RO treatment) have been included.

Estimates were developed for two alternatives:

- Treatment Alternative 1: ZenoGem MBR, UF permeate storage/disinfection and RO facilities treating screened, de-gritted wastewater
- Treatment Alternative 2: Extended aeration and clarification (existing), ZeeWeed system, UF permeate storage/disinfection and RO facilities treating secondary effluent from the existing south WWTP

For Alternative 1, a new ZenoGem MBR system would be installed to treat the screened, de-gritted wastewater and produce 8.5 mgd of reclaimed effluent. The UF permeate would be disinfected with monochloramines, stored, and then treated by the RO system (which includes acidification and antiscalant addition to the RO feedwater) to produce 6.8 mgd of RO permeate.

For Alternative 2, 9.4 mgd of effluent from the existing secondary clarifiers would be treated by the ZeeWeed UF system to produce 8.5 mgd of permeate. The UF permeate would then be disinfected, stored, and treated by RO as described for Alternative 1. For either alternative, wastewater flows in excess of those necessary to produce 6.8 mgd of RO permeate and would be processed by the existing WWTP facilities. Concentrate from the ZeeWeed UF system would be recycled back to the aeration basins, while sludge

¹ For purposes of the estimates, the ZenoGem/ZeeWeed permeate is referred to as UF permeate, as both processes use the same UF membranes.

from the ZenoGem system would be digested and dried using existing facilities at the WWTP. Both alternatives use existing headworks facilities for wastewater screening and de-gritting.

Figure 6.1 displays a schematic of the existing WWTP. Figures 6.2 and 6.3 are schematics of the two alternatives including existing facilities.

FIGURE 6.1 Existing WWTP Schematic

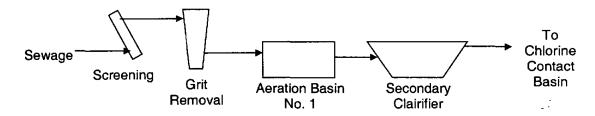


FIGURE 6.2
ZenoGem MBR and RO Facilities

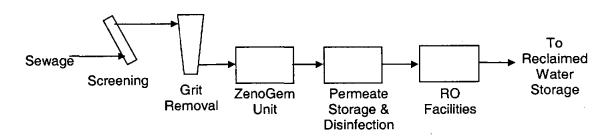
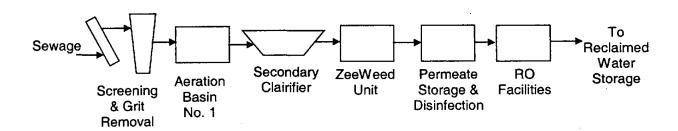


FIGURE 6.3
Conventional WWTP with ZeeWeed and RO Facilities



6.1 Cost Assumptions

The estimates were prepared at an order-of-magnitude level to provide a relative and preliminary cost comparison between the two treatment alternatives and are based on information presently available. Order-of-magnitude cost estimates are defined by the American Association of Cost Engineers as an approximate estimate made without detailed engineering data. Final costs for each alternative will depend on such variables as actual labor and material costs, market conditions, project scope, implementation schedule, and will differ from the estimates presented. The costs are in present day dollars, and annual unit costs are based on ZenoGem/ZeeWeed permeate capacity of 8.5 mgd and RO permeate capacity of 6.8 mgd. The plant availability factor assumed for calculation of unit treatment costs (in \$/1000 gallons) is 95%. A higher availability factor is not required as the plant is intended to operate as a seasonally-average reuse production plant. ZENON budget proposals used in estimating ZenoGem/ZeeWeed and RO equipment costs are presented in Appendix H.

The estimates do not include costs for sewage screening and de-gritting (these facilities are currently being upgraded at the south WWTP) for either alternative. Alternative 2 does not include capital costs for extended aeration or secondary clarification, as these are existing. The costs related to ZenoGem, ZeeWeed, and RO equipment and required ancillaries are included. The ZenoGem system is sized to account for downtime associated with backpulsing and maintenance cleanings while the ZeeWeed system is sized to account for downtimes associated with backpulsing only. At the assumed RO feedwater recovery of 80 percent, 20 percent of the RO feedwater flow (1.7 mgd) becomes waste concentrate requiring appropriate disposal. For purposes of this estimate, RO concentrate is assumed to be discharged without further treatment to the Arroyo Colorado using the City's existing outfall. Consequently, costs are not included for concentrate disposal.

6.2 Cost Estimates

Estimates were prepared for the following cost categories:

- Installed equipment, total construction, total capital, total unit capital, and amortized capital
- Total O&M and total unit O&M
- Total annual and total unit annual

Tables 6.1 and 6.2 present the estimates for the Alternatives 1 and 2, respectively. The tables include the assumptions and references used in developing component capital costs and operating and maintenance costs. Table 6.3 presents design criteria assumptions used in developing the cost estimates for each major process. In addition, a line-item comparison of capital and O&M costs for the ZenoGem and ZeeWeed technologies is presented in Appendix I.

TABLE 6.1Order of Magnitude Cost Estimate for ZenoGem® and RO Alternative Capital and O&M Cost Opinion

Capital and O&M Cost Opinion	 		
Item	Cost	Assumption	Cost Reference
Fine Screening	\$ 20,000	3-mm screen	CH2M HILL estimator b
ZenoGem® System®	\$ 8,620,000		Zenon Budget Proposal
Bioreactor/Equalization Tanks	\$ 1,307,808	6 tanks @ 170 ft x 21 ft x 23 ft (1.29 MG for equalization)	CH2M HILL estimator ^b
Permeate Storage	\$ 70,000	180,000 gallons	CH2M HILL estimator b
Transfer Pump to RO System	\$ 52,500	(2) 2,950 gpm @ 70 ft TDH pumps plus one stand-by	CH2M HILL estimator ^b
Chloramine Feed System			
Chlorinator	\$ 30,000	50 lb/day duplex system	CH2M HILL estimator b
Ammoniator	\$ 30,000	100 gal/day duplex system	CH2M HILL estimator b
RO System*	\$ 2,300,000		Zenon Budget Proposal
Installation	\$ 2,730,000	25% of installed equipment costs	
installed Costs Subtotal	\$ 15,160,308	}	
ZenoGem Equipment Building	\$ 288,000	4,800 SF	CH2M HILL estimator ^b
RO Building	\$ 390,000	6,500 SF	CH2M HILL estimator ^b
Installed Costs and Building Cost Subtotal	\$ 15,838,308		
Unit Process Noncomponent Costs			
Yard Piping Allowance (10%)	\$ 1,583,831		
Site Electrical Allowance (8%)	\$ 1,267,065	•	
Site I&C Allowance (5%)	\$ 791,915	i e	
Site Civil Allowance (5%)	\$ 791,915	•	
Unit Process Subtotal	\$ 20,273,034		
Contingency (10%)	\$ 2,027,303	•	
Contractor Overhead & Mark-up (10%)	\$ 2,027,303		
Total Construction Cost	\$ 24,327,641		
Engineering & Administration (15%)	\$ 3,649,146	i	
Total Capital Cost	\$ 27,976,787	•	•
Total Capital Unit Cost (\$/1,000 gallon)	\$		
Amortized Capital Cost (20yr @ 6.5%)	 2,539,072		
Operation & Maintenance Costs			
Major Chemical Costs			
Disinfection: Chlorine	\$ 21,350	\$610/ton	Hill Brothers Chemical Co.
Disinfection: Ammonia		\$370/ton	Hill Brothers Chemical Co.
Backpulse Chemicals: Sodium Hypochlorite	\$ 8,232	! \$0.31/Liter	Zenon Budget Proposal
CIP Chemical #1: MC-1	\$ 220	\$1.67/Liter	Zenon Budget Proposal
CIP Chemical #2: Sodium Hypochlorite (250 mg/L)	•	\$0.31/Liter	Zenon Budget Proposal
RO - Sulfuric Acid	\$ 5,745	\$ \$0.04/lb	Zenon Budget Proposal
RO - Sodium Bisulfite	\$ 2,594	\$ \$0.25/lb	Zenon Budget Proposal
RO - Antiscalant	\$ 122,359	9 \$3.27/Liter	Zenon Budget Proposal

TABLE 6.1Order of Magnitude Cost Estimate for ZenoGem® and RO Alternative Capital and O&M Cost Opinion

Item	C	ost	Assumption	Cost Reference
RO - Organic Acid: MC-1		\$ 8,658	\$2.29/kg	Zenon Budget Proposal
RO - Alkali Surfactant: MC-4		\$ 1,738	\$3.06/kg	Zenon Budget Proposal
RO - Sanitizer: MP-1		\$ 4,748	\$5.01/Liter	Zenon Budget Proposal
Major Power Costs			\$0.075/kW-hr	
Screening	\$	-	Existing	
Permeate Pumps	\$	37,392		Zenon Budget Proposal
Recirculation Pumps	\$	59,068		Zenon Budget Proposal
Sludge Wasting Pumps		\$ 890		Zenon Budget Proposal
Membrane Air Scour Blowers	\$	237,213		Zenon Budget Proposal
Process Air Blowers	\$	119,501		Zenon Budget Proposal
Anoxic Zone Mixers		\$ -		Zenon Budget Proposal
Air Separation System Vacuum Pumps		\$ 2,520		Zenon Budget Proposal
Backpulse Sodium Hypochlorite - Metering		\$ 3		Zenon Budget Proposal
Chemical Feed #1 - Metering		\$ 245		Zenon Budget Proposal
Air Compressors		\$ 2,515		Zenon Budget Proposal
Air Driers		\$ -		Zenon Budget Proposal
Controls & Instrumentation		\$ 657		Zenon Budget Proposal
Miscellaneous		\$ 657		Zenon Budget Proposal
RO - Pretreatment Chemical Mixers, Process Pump, CIP Pump	\$	501,591		Zenon Budget Proposal
Membrane/Cartridge Filter Replacement Costs				
ZenoGem	\$	329,311	1-yr warranty; 8-yr replacement frequency	Zenon Budget Proposal
RO	\$	226,286	5-yr replacement frequency	Zenon Budget Proposal
Cartridge Filter	\$	24,637	Annual replacement	Zenon Budget Proposal
Other Costs				
Maintenance	\$	63,750		Prorated South WWTP Costs
Permit Fees	\$	39,100		Prorated South WWTP Costs
Land Maintenance	\$	12,750	Replacement of sand in drying beds	Prorated South WWTP Costs
Supplies	\$	61,200	Includes land application of sludge (\$31.50/dry ton)	Prorated South WWTP Costs
Labor	\$	436,800	14 O&M personnel @ \$15.00/hr (9 ZenoGem; 5 for RO)	CH2M HILL estimate
Laboratory	\$	141,100	Includes 4 lab techs, analysis, O&M, etc.	Prorated South WWTP Costs
Total Annual Operation & Maintenance Cost	\$ 2	2,482,754		
Total Annual O&M Unit Cost (\$/1,000 gallon)	\$	1.05		

TABLE 6.1Order of Magnitude Cost Estimate for ZenoGem® and RO Alternative Capital and O&M Cost Opinion

Item	Cost As	sumption	Cost Reference
Total Annual Cost	\$ 5,021,826		
Total Unit Cost (\$/1,000 gallon)	\$	MGD product water allability factor = 95%	

^a Detailed listing of components comprising ZenoGem and RO systems are presented in Appendix H.

TABLE 6.2Order of Magnitude Cost Estimate for ZeeWeed® and RO Alternative Capital and O&M Cost Opinion

item	Cost	Assumption	Cost Reference
Fine Screening	\$ 20,000	3-mm screen	CH2M HILL estimator b
ZeeWeed® Tertiary Treatment System®	\$ 5,075,000		Zenon Budget Proposal
ZeeWeed Tanks	\$ 162,468	4 tanks @ 70 ft x 10 ft x 10 ft	CH2M HILL estimator b
Permeate Storage	\$ 70,000	180,000 gallons	CH2M HILL estimator b
Transfer Pump to RO System	\$ 52,500	(2) 2950 gpm @ 70 ft TDH pumps plus one stand-by	CH2M HILL estimator ^b
Chloramine Feed System			
Chlorinator	\$ 30,000	50 lb/day duplex system	CH2M HILL estimator b
Ammoniator	\$ 30,000	100 gal/day duplex system	CH2M HILL estimator b
RO System*	\$ 2,300,000		Zenon Budget Proposa
Installation	\$ 1,843,750	25% of installed equipment costs	
Installed Costs Subtotal	\$ 9,583,718		
ZeeWeed Equipment Building	\$ 84,000	1,400 SF	CH2M HILL estimator b
RO Building	\$ 390,000	6,500 SF	CH2M HILL estimator b
Installed Costs and Building Cost Subtotal	\$ 10,057,718		
Unit Process Noncomponent Costs			
Yard Piping Allowance (10%)	\$ 1,005,772		
Site Electrical Allowance (8%)	\$ 804,617		
Site 1&C Allowance (5%)	\$ 502,886		
Site Civil Allowance (5%)	\$ 502,886		
Unit Process Subtotal	\$ 12,873,879		
Contingency (10%)	\$ 1,287,388		•
Contractor Overhead & Mark-up (10%)	\$ 1,287,388		
Total Construction Cost	\$ 15,448,655		
Engineering & Administration (15%)	\$ 2,317,298		
Total Capital Cost	\$ 17,765,953		
Total Capital Unit Cost (\$/1,000 gallon)	\$ 7.53		
Amortized Capital Cost (20yr @	\$ 1,612,374		

^b ENR CCI reference number 6126.79

TABLE 6.2

Order of Magnitude Cost Estimate for ZeeWeed® and RO Alternative Capital and O&M Cost Opinion

item		Cost	Assumption	Cost Reference
5.5%)				
Operation & Maintenance Costs				
Major Chemical Costs				
Disinfection: Chlorine	\$	21,350	\$610/ton	Hill Brothers Chemical Co.
Disinfection: Ammonia	\$	9,620	\$370/ton	Hill Brothers Chemical Co.
Backpulse Chemicals: Sodium Hypochiorite	\$	8,232	\$0.31/Liter	Zenon Budget Proposal
CIP Chemical #1: MC-1	\$	3,211	\$1.67/Liter	Zenon Budget Proposal
CIP Chemical #2: Sodium Hypochlorite (250 mg/L)	\$	4,435	\$0.31/Liter	Zenon Budget Proposal
CIP Neutralization Chemical #1: Sodium Hydroxide	\$	175	\$0.36/Liter	Zenon Budget Proposal
CIP Neutralization Chemical #2: Sodium Bisulfite	\$	117	\$0.06/Liter	Zenon Budget Proposal
RO - Sulfuric Acid	\$	5,745	\$0.04/lb	Zenon Budget Proposal
RO - Sodium Bisulfite	\$	2,594	\$0.25/lb	Zenon Budget Proposal
RO - Antiscalant	\$	122,359	\$3.27/Liter	Zenon Budget Proposal
RO - Organic Acid: MC-1	\$	8,658	\$2.29/kg	Zenon Budget Proposal
RO - Alkali Surfactant: MC-4	\$	1,738	\$3.06/kg	Zenon Budget Proposal
RO - Sanitizer: MP-1	\$	4,748	\$5.01/Liter	Zenon Budget Proposal
Major Power Costs			\$0.075/kW-hr	
Screening	\$	-	Existing	
Aeration Basins	\$	419,000	18 motors @ 50 HP; 24 hrs/day	South WWTP info
Recirculation Pumps	\$	74,500	4 pumps @ 40 HP; 24 hrs/day	South WWTP info
Permeate Pumps	\$	36,901		Zenon Budget Proposal
Membrane Air Scour Blowers	\$	114,440		Zenon Budget Proposal
Air Separation System Vacuum Pumps	\$	2,520		Zenon Budget Proposal
Backpulse Sodium Hypochlorite – Metering	\$	7		Zenon Budget Proposal
Air Compressors	\$	2,515		Zenon Budget Proposal
Air Driers	\$	-		Zenon Budget Proposal
I&C	\$	657		Zenon Budget Proposal
Miscellaneous	\$	657		Zenon Budget Proposal
RO - Pretreatment Chemical Mixers, Process Pump, CIP Pump	\$	501,591		Zenon Budget Proposal
Membrane/Cartridge Filter Replacement Costs				
ZeeWeed	\$	190,905	1-yr warranty; 8-yr replacement frequency	Zenon Budget Proposal
RO	\$	226,286	5-yr replacement frequency	Zenon Budget Proposal
Cartridge Filter	\$	24,637	annual replacement	Zenon Budget Proposal
Other Costs				
Maintenance	\$	63,750		Prorated South WWTP Co
Permit Fees	\$	39,100		Prorated South WWTP Co
Land Maintenance	\$	12,750	replacement of sand in drying beds	Prorated South WWTP Co

TABLE 6.2Order of Magnitude Cost Estimate for ZeeWeed® and RO Alternative Capital and O&M Cost Opinion

Item	Cost	Assumption	Cost Reference
Supplies	\$ 61,200	includes land application of sludge (\$31.50/dry ton)	Prorated South WWTP Costs
Labor	\$ 655,200	21 O&M personnel @ \$15.00/hr (16 exst. plant w/Zeeweed; 5 for RO)	CH2M HILL estimate
Laboratory	\$ 141,100	includes 4 lab techs, analysis, O&M, etc.	Prorated South WWTP Costs
Total Annual Operation & Maintenance Cost	\$ 2,760,698		
Total Annual O&M Unit Cost (\$/1,000 gallon)	\$ 1.17		٠
Total Annual Cost	\$ 4,373,072		
Total Unit Cost (\$/1,000 gallon)	\$ 1.85	Based on 6.8 MGD product water flow; plant availability factor = 95%	

^a Detailed listing of components comprising ZeeWeed and RO systems are presented in Appendix H.

TABLE 6.3Design Criteria Assumptions for ZenoGem, ZeeWeed, and RO Systems

Criterion	Value
ZenoGem System	
Design Permeate Flow, mgd	8.5
Hydraulic Residence Time, hours	6
Solids Retention Time, days	17
Mixed Liquor Suspended Solids Level, g/L	10
Aeration Rate, fine bubble, scfm/mgd	647
Aeration Rate, membrane air scour, scfm/mgd	2,586
Aeration mode (both systems)	Cyclic
Membrane flux, gfd	15.4
No. of membrane trains	6
No. of reactor tanks	6
Backpulse interval, minutes	15
Backpulse duration, seconds	30
Backpulse pressure, psi	8
Maintenance clean interval, hours	168
Maintenance clean duration, minutes	60
ZeeWeed System	
Design Permeate Flow, mgd	8.5
Hydraulic Residence Time, hours	0.56
Feedwater Recovery, percent	95
Aeration Rate, membrane air scour, scfm/mgd	1,207
Aeration Mode	Continuous
Membrane flux, gfd	20.4
Backpulse interval, minutes	15
Backpulse duration, seconds	30

^b ENR CCI reference number 6126.79

TABLE 6.3

Design Criteria Assumptions for ZenoGem, ZeeWeed, and RO Systems

Criterion	Value	
Backpulse pressure, psi	8	
RO System		
Design Permeate Flow, mgd	6.8	
Feedwater pH, units	5	
Antiscalant dose, mg/L	Manufacturer dependent; 3 max	
Feedwater recovery, percent	80	
Membrane flux, gfd	12	
Membrane type	low fouling, aromatic composite	
Vessel array	three stage, concentrate taper	

Estimated total capital cost for the ZenoGem/RO approach (Alternative 1) is significantly higher than for the ZeeWeed/RO approach (Alternative 2), \$28.0MM versus \$17.8MM, a difference of nearly \$10MM. The difference reflects the higher cost of treatment for ZenoGem relative to ZeeWeed. Compared to the requirements for ZeeWeed, ZenoGem requires more membrane modules because a lower flux rate must be used to treat the significantly higher solids concentration of the mixed liquor (relative to the secondary effluent from the existing WWTP); larger tankage to provide wastewater flow equalization and the necessary hydraulic retention time to complete nitrification; and increased blower capacity to achieve carbonaceous and nitrogenous oxidation of the wastewater.

Estimated annual operating and maintenance costs for the ZenoGem-based alternative were slightly lower than for the ZeeWeed alternative (\$2.48MM/year versus \$2.76MM/year). This reflects lower energy and labor costs associated with operating the ZenoGem system versus those for operating costs for the extended aeration basins, secondary clarifiers and ZeeWeed system.

The significantly higher capital cost for Alternative 1 outweighs the slightly lower O&M costs. Consequently, total unit cost for Alternative 1 is higher (\$2.13/1000 gals versus \$1.85/1000 gals). Based on these estimates, it would be more cost-effective for McAllen to implement Alternative 2 (using ZeeWeed and RO to treat existing plant secondary effluent) to achieve their indirect potable reuse treatment goals. This reflects the cost savings of associated with the use of their existing flow equalization and secondary treatment facilities that are a sunk cost.

The disparity in capital cost between the ZenoGem and ZeeWeed alternatives could be reduced somewhat in the instance where a municipality's existing WWTP utilized concrete basins for aeration, rather than the earthen basins used at McAllen. Cost savings in this instance would result from avoiding the costs associated with constructing new concrete basins and instead retrofitting the membrane modules into the existing tankage. For the flow rate assumed in this cost comparison (8.5-mgd), the avoided cost would be \$1.3MM or 5.5% of the total capital cost for the ZenoGem alternative. Actual savings would be somewhat less due to the costs associated with basin retrofit. The \$1.3MM savings would reduce the difference in capital costs between the two alternatives, however, the ZeeWeed alternative would still be significantly less

expensive (by \$8.9MM). Additional capital cost savings could be realized if the blowers used for aeration in the conventional, concrete basin plant could be adapted and used where membrane modules are retrofitted into existing basins.

It was beyond the scope of this study to perform an order-of-magnitude level cost estimate for conventional treatment facilities (primary clarification, secondary [activated sludge] treatment and secondary clarification) followed by ZeeWeed in the case where no conventional wastewater treatment existed. However, based on design and costing of conventional treatment facilities that CH2M HILL has performed over the past 20 years, rule-of-thumb costs for 8.5-mgd of conventional treatment would be in the \$16MM -\$20MM range. Adding ZeeWeed costs of \$12MM results in a cost estimate of \$28-32MM. This compares with ZenoGem cost of \$22MM as estimated in this report. Based on these estimates, constructing a 8.5-mgd ZenoGem treatment plant to treat screened, de-gritted sewage would save \$6-10MM compared with the conventional treatment/ZeeWeed approach using the combination of rule-of-thumb and order-ofmagnitude cost estimates. This represents a significant savings potential and indicates that for municipalities considering indirect potable reuse and who would be starting with raw sewage, it should be considerably less expensive to construct a treatment facility using ZenoGem/RO versus conventional wastewater plant (through secondary treatment)/ZeeWeed/RO.

SECTION 7

References

- Green, J and J. Holmes. 1947. Journal American Water Works Association. Volume 39. p. 1090.
- Lozier, Jim. 1998. Water Treatment Technology Program Report No. 26. Wastewater Reclamation Pilot Study, City of McAllen, Texas.
- Water Environment Federation. 1990. Operation of Municipal Wastewater Treatment Plants.

 Manual of Practice 11, Volume II.
- Water Environment Federation and American Society of Civil Engineers. 1991. Design of Municipal Wastewater Treatment Plants, Volume I. WEF Manual of Practice No. 8. ASCE Manual and Report on Engineering Practice No. 76.

SI Metric Conversions

English Unit	Multiply By	SI Metric Unit
ft²	0.0929	m²
gal	3.785	L
gal	0.003785	m³
gpm	0.06309	L/s
gpd/ft²	1.698	L/m²/hour
in	2.54	cm
lb	454	g
psi	psi 0.0703	

Appendix A. Photographs of Demonstration Plant Facilities and Associated Equipment

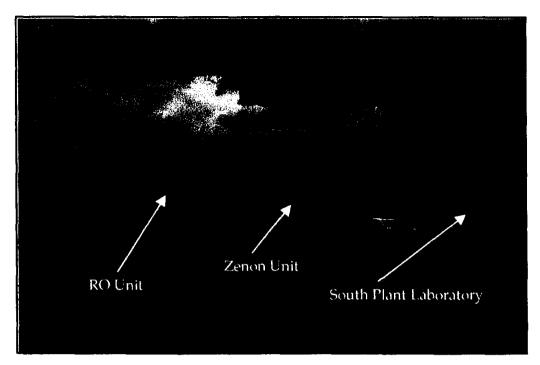


Exhibit A-1. Demonstration plant location (located to the west of the South WWTP laboratory).



Exhibit A-2. ZenoGem® and RO treatment systems (looking west).

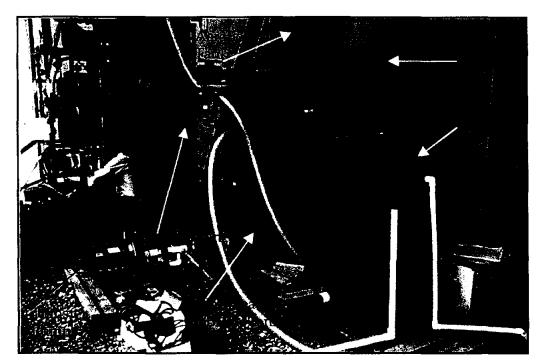
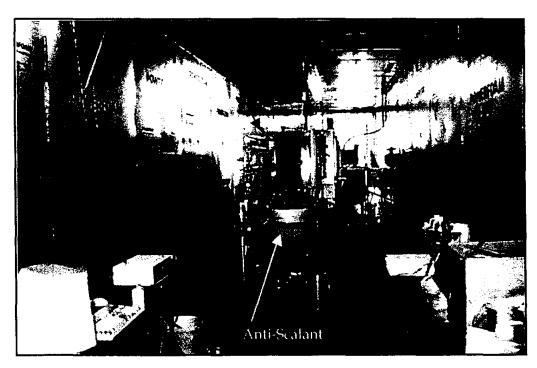


Exhibit A-3. Process tanks for ZenoGem system (operator Henry Perez in background).



 $Exhibit \ A-4. \ \ RO \ system \ equipment \ (looking \ east \ inside \ trailer).$



Exhibit A-5. RO data acquisition equipment (looking west inside trailer).



HYDRANAUTICS RO SYSTEM DESIGN SOFTWARE, VERSION 6.4 (c) 1998 12/12/1999 BASIC DESIGN RO program licensed to: Calculation created by: J. Lozier (CH2M HILL) Project name: McAllen Phase II Permeate flow: 12.7 gpm 15.9 gpm HP Pump flow: Raw water flow: 15.9 gpm Recommended pump press.: 132.2 psi 80.0 8 (Stages 1 \$ Feed pressure: 121.4 psi Permeate recovery ratio: 31.0 C(88F) Feedwater Temperature: Raw water pH: 7.80 Element age: 0.0 years 56.9 H2SO4 Acid dosage, ppm (100%): Flux decline % per year: 7.0 Acidified feed CO2: 57.9 Salt passage increase, %/yr: 10.0 12.0 gfd Feed type: Average flux rate: Wastewater

Stage	Perm. Flow	Flow per Feed	C Vessel Conc	Flux	Beta	Conc. Press.	Element Type	Elem. No.	Array
	gpm	gpm	gpm	gfd		psi			
1-1	5.7	7.9	5.1	16.2	1.16	111.5	LFC1-4040	6	2x3
1-2	4.5	5.1	2.8	12.7	1.21	103.6	LFC1-4040	6	2 x 3
1-3	1.6	5.7	4.1	8.8	1.10	94.1	LFC1-4040	3	1x3
1-4	0.9	4.1	3.2	5.3	1.07	86.7	LFC1-4040	3	1x3
++	Rav	v water	+Feed	water-	+	Permea	te	ncentra	te+
I Ton	mcr / 1	CaCO3				mcr/l			acos I

+	+Raw	water	+Feed	water	+Perme	ate	+Conce:	ntrate+
Ion	mg/l	CaCO3	mg/l	CaCO3	mg/l	CaCO3	mg/l	CaCO3
Ca	140.0	349.1	140.0	349.1	2.3	5.7	690.9	1723.0
Mg	29.1	119.8	29.1	119.8	0.5	1.9	143.6	591.0
Na	332.0	721.7	332.0	721.7	25.2	54.8	1559.2	3389.5
K	17.1	21.9	17.1	21.9	1.6	2.1	79.1	101.4
NH4	1.0	2.8	1.0	2.8	0.1	0.3	4.6	12.8
Ba	0.1	0.1	0.1	0.1	0.0	0.0	0.4	0.3
Sr	1.3	1.4	1.3	1.4	0.0	0.0	6.2	7.1
CO3	0.3	0.5	0.1	0.1	0.0	0.0	0.3	0.6
HCO3	293.0	240.2	224.0	183.6	25.5	20.9	1017.8	834.3
S04	327.0	340.6	382.8	398.7	6.3	6.6	1888.6	1967.3
Cl	388.0	547.2	388.0	547.2	25.0	35.3	1839.8	2594.9
F	1.0	2.6	1.0	2.6	0.1	0.3	4.5	11.8
NO3	1.5	1.2	1.5	1.2	0.5	0.4	5.7	4.6
SiO2	13.9		13.9		0.5		67.7	Ì
TDS	1545.2	+	1531.8		87.6		7308.5	
Hq	7.8		6.8		5.9		7.4	
- -					·		. – – – – – – –	

	Raw water	Feed water	Concentrate
CaSO4 / Ksp * 100:	88	10%	73 ቴ
SrS04 / Ksp * 100:	5%	6%	42%
BaSO4 / Ksp * 100:	371%	428%	2994%
SiO2 saturation:	9%	9%	45%
Langelier Saturation Index	0.92	-0.19	1.73
Stiff & Davis Saturation Index	0.95	-0.17	1.35
Ionic strength	0.03	0.03	0.16
Osmotic pressure	13.3 psi	13.1 psi	62.8 psi

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYD	RANAUT	ICS RO	SYSTE	M DES	IGN SO	FTWARE	DEST	######################################					
		m licen on crea			Lozie								
Pro	iect n	ame: Mc	Allen	phase	TT	_ (C112			TaT •		1	27 ~	~~
	Pump f			1	15 9 a	r)m	Raw w	ater fl	w.				
		led pump	pres				1.011	~cc1 11	Cw.		_	J. J 9	ρm
	d pres dwater	sure: Temper	ature		21.4 p 31.0 C		Perme	ate rec	overy	ratio:	8	0.0 %	
	water				7.80							0.0 y	ears
Aci	d dosa	ge, ppm	(100	કે): 5	66.9 H	2SO4		decline	% per	year:		7.0	
Aci	dified	feed C	02:		57.9		Salt	passage	incre	ase, %	/yr: 1	0.0	
Ave	rage f	lux rat	e:	1	.2.0 g	fd	Feed	type:	-	W	astewa	ter	
Sta			low po Feed	er Ves Co	sel	Flux	Beta	Press.			_		rray
			gpm	gr		gfd							
1-1			7.9	5.		16.2				–			
1-3			5.1	2.		12.7							
1-1			5.7	4.		8.8							
1-4	4 0	.9	4.1	3.	2	5.3	1.07	86.7	LFC:	L-4040	;	3 :	Lx3
Sta	Elem	Feed	Pres	Perm	Perm	Beta	Peri	n Conc	Concer	ntrate	satura	ation	level
9	no.				Flux								
				gpm	gfd		TDS						-
1-1	1	121.4	4.0	1.0	17.0	1.13	20 /	1 15 (12	7	E04	1.0	0 0
1-1	1 2	117.4		0.9	16.1			_					
1-1	3	114.2	2.6	0.9	15.2	1.14							
1-1	3	114.2	2.0	0.5	13.2	1.10	34.	20.5	, 1,	Τ0	733	7.4	0.4
1-2	1	108.5	2.1	0.8	13.7					_			
1-2	2	106.4	1.6	0.7	12.7	1.19							
1-2	3	104.8	1.2	0.7	11.5	1.21	51.5	36.2	35	20	1476	25	1.1
1-3	1	100.6	2.6	0.6	9.8	1.10	55.9	40.7	40	23	1679	28	1.2
1-3	2	98.1	2.2	0.5	8.6								
1-3	3	95.9	1.9	0.5	7.8							_	
	_												
1-4	1	91.0	1.7	0.4	6.1							-	
1-4	2	89.3	1.5	0.3	5.0					_			
1-4	3	87.8	1.3	0.3	4.5	1.07	88.6	63.9	71	41	2925	44	1.8

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics.

Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578

Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYDRANAUTICS RO SYSTEM DESIGN SOFTWARE, VERSION 6.4 (c) 1998 12/12/1999 BASIC DESIGN

RO program licensed to:

Stage Perm.

Flow

gpm

7.8

Calculation created by: J. Lozier (CH2M HILL)

Project name: McAllen Phase II Permeate flow: 7.2 gpm 14.4 gpm HP Pump flow: Raw water flow: 14.4 gpm

Recommended pump press.: 100.5 psi

Feed pressure: 91.1 psi Permeate recovery ratio: 50.0 %

Conc.

Press.

psi

62.4

5.7

Element

Type

3001.1

7.1

Elem. Array

No.

31.0 C(88F) Feedwater Temperature: 7.80

Feed

gpm

TDS | 1545.2 1531.8

Raw water pH: Element age: 0.0 years Acid dosage, ppm (100%): 56.9 H2SO4 Flux decline % per year:

Acidified feed CO2: 57.9 Salt passage increase, %/yr: 10.0 10.2 gfd Wastewater Average flux rate: Feed type:

gfđ

Flow per Vessel Flux Beta

Conc

gpm

6.8

1-1 1-2	4.1	7.2 5.2	5.2 3.6		.11 81.9 .12 73.2				x3 x3
Ion	+Raw mg/l	water	+Feed mg/l	water CaCO3	-+Perm mg/1	eate CaCO3	+Conce mg/l	ntrate- CaCO	
 Ca	140.0	349.1	140.0	349.1	1.6	4.0	278.4	694.	÷
Mg Na	29.1 332.0	119.8 721.7	29.1 332.0	119.8 721.7	0.3	1.4 39.1	57.9 646.0	238.1 1404.4	4
K NH4	17.1	21.9	17.1	21.9	1.2	1.5	33.0	42.4 5.4	4
Ba Sr CO3	0.1 1.3 0.3	0.1 1.4 0.5	0.1 1.3 0.1	$0.1 \\ 1.4 \\ 0.1$	0.0	0.0 0.0 0.0	0.2 2.5 0.1	0.1 2.9 0.2	9
HCO3	293.0 327.0	240.2 340.6	224.0 382.8	183.6 398.7	18.3	15.0 4.6	429.6 761.1	352.2 792.8	2
C1 F	388.0 1.0	547.2	388.0 1.0	547.2 2.6	17.8	25.1 0.2	758.2 1.9	1069.4	1
NO3 SiO2	1.5 13.9	1.2	1.5 13.9	1.2	0.3	0.3	2.7 27.5	2.1	L

	Raw water	Feed water	Concentrate
CaSO4 / Ksp * 100:	8%	10%	23%
SrSO4 / Ksp * 100:	5%	6%	13%
BaSO4 / Ksp * 100:	371%	428%	990%
SiO2 saturation:	9%	9%	18%
Langelier Saturation Index	0.92	-0.19	0.65
Stiff & Davis Saturation Index	0.95	-0.17	0.56
Ionic strength	0.03	0.03	0.06
Osmotic pressure	13.3 psi	13.1 psi	25.7 psi

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics.
Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYDRANAUTI	CS RO SYST	EM DESIGN S		. VERSI		(c) 1	998	1	2/12/	1999
Calculation Project na	me: McAller	to: by: J. Lozi n Phase II 14.4 (Permea	te flow	7: W:		1	7.2 g 4.4 g	iom Tom
Recommende Feed press Feedwater	d pump pres ure: Temperature	ss.: 100.5 p 91.1 p e: 31.0 c	psi psi C(88F)	Permea	ite reco	very :	ratio:	5	0.0 %	•
Acidified	feed CO2:	7.80 0%): 56.9 1 57.9 10.2 g		Salt p	t age: lecline assage ype:	<pre>% per increa</pre>	year: ase, %	/yr: 1	7.0 0.0	ears
		er Vessel Conc gpm			Conc. Press. psi		ement Type		m. A	rray
1-1 4.	1 7.2	5.2 3.6	11.5	1.11	81.9	LFC1 LFC1	L-4040 L-4040	(6 5	2x3 2x3
Stg Elem no.	pres drop	Perm Perm flow Flux gpm gfd	3	sal						level Lang.
1-1 1 1-1 2 1-1 3	91.1 3.5 87.5 3.0 84.5 2.6		1.10	42.4	14.6 16.2 18.1	13		486 555 638		
1-2 1 1-2 2 1-2 3	78.9 2.2 76.7 1.9 74.8 1.6	0.5 8.8			20.5 22.7 25.9		10 11 13	733 848 985	14 16 18	

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYDRANAUTICS RO SYSTEM DESIGN SOFTWARE, VERSION 6.4 (c) 1998 12/12/1999 BASIC DESIGN

RO program licensed to:

Calculation created by: J. Lozier (CH2M HILL)

Project name: McAllen Phase II Permeate flow: 12.7 gpm 25.4 grpm HP Pump flow: Raw water flow: 25.4 gpm

Permeate recovery ratio:

50.0 8 (Stages

0.0 years (\$ 2)

Recommended pump press.: 140.9 psi

131.5 psi Feed pressure:

31.0 C(88F) Feedwater Temperature:

Raw water pH: 7.80

Element age: Acid dosage, ppm (100%): 56.9 H2SO4 Flux decline % per year: Acidified feed CO2: 57.9 Salt passage increase, %/yr: 10.0

the street of the state of the

Average flux rate: 12.0 gfd Feed type: Wastewater

Perm. Flow	Feed	Conc		Beta	Conc. Press.	Element Type	Elem. No.	Array
gpm	gpm	gpm	gra		psı			
6.0	12.7	9.7	17.0	1.09	110.5	LFC1-4040	6	2x3
4.6	9.7	7.4	13.0	1.09	93.2	LFC1-4040	6	2x3
1.5	14.8	13.3	8.4	1.03	61.3	LFC1-4040	3	1x3
0.6	13.3	12.7	3.3	1.01	32.4	LFC1-4040	3	1x3
	Flow gpm 6.0 4.6 1.5	Flow Feed gpm gpm 6.0 12.7 4.6 9.7 1.5 14.8	Flow Feed Conc gpm gpm gpm 6.0 12.7 9.7 4.6 9.7 7.4 1.5 14.8 13.3	Flow Feed Conc gpm gpm gpm gfd 6.0 12.7 9.7 17.0 4.6 9.7 7.4 13.0 1.5 14.8 13.3 8.4	Flow Feed Conc gpm gpm gfd 6.0 12.7 9.7 17.0 1.09 4.6 9.7 7.4 13.0 1.09 1.5 14.8 13.3 8.4 1.03	Flow Feed Conc Press. gpm gpm gfd psi 6.0 12.7 9.7 17.0 1.09 110.5 4.6 9.7 7.4 13.0 1.09 93.2 1.5 14.8 13.3 8.4 1.03 61.3	Flow Feed Conc Press. Type gpm gpm gfd psi 6.0 12.7 9.7 17.0 1.09 110.5 LFC1-4040 4.6 9.7 7.4 13.0 1.09 93.2 LFC1-4040 1.5 14.8 13.3 8.4 1.03 61.3 LFC1-4040	Flow Feed Conc Press. Type No. gpm gpm gfd psi 6.0 12.7 9.7 17.0 1.09 110.5 LFC1-4040 6 4.6 9.7 7.4 13.0 1.09 93.2 LFC1-4040 6 1.5 14.8 13.3 8.4 1.03 61.3 LFC1-4040 3

				water				
Ion	mg/l	CaCO3	mg/l	CaCO3	mg/l	CaC03	mg/l	CaCO3
Ca	140.0	349.1	140.0	349.1	1.4	3.6	278.6	694.7
Mg	29.1	119.8	29.1	119.8	0.3	1.2	57.9	238.3
Na	332.0	721.7	332.0	721.7	16.2	35.1	647.8	1408.4
K	17.1	21.9	17.1	21.9	1.0	1.3	33.2	42.5
NH4	1.0	2.8	1.0	2.8	0.1	0.2	1.9	5.4
Ba	0.1	0.1	0.1	0.1	0.0	0.0	0.2	0.1
Sr	1.3	1.4	1.3	1.4	0.0	0.0	2.5	2.9
CO3	0.3	0.5	0.1	0.1	0.0	0.0	0.1	0.2
нсоз	293.0	240.2	224.0	183.6	16.7	13.7	431.3	353.5
SO4	327.0	340.6	382.8	398.7	4.0	4.2	761.5	793.2
Cl	388.0	547.2	388.0	547.2	16.2	22.8	759.8	1071.7
F	1.0	2.6	1.0	2.6	0.1	0.2	1.9	5.0
NO3	1.5	1.2	1.5	1.2	0.3	0.3	2.7	2.2
SiO2	13.9		13.9		0.3		27.5	
TDS	1545.2	+	1531.8	+	56.5	+	3007.0	
pН	7.8		6.8		5.7		7.1	

	Raw water	Feed water	Concentrate
CaSO4 / Ksp * 100:	8%	10%	23%
SrSO4 / Ksp * 100:	5%	6%	13%
BaSO4 / Ksp * 100:	371%	428%	990%
SiO2 saturation:	9%	9%	18%
Langelier Saturation Index	0.92	-0.19	0.65
Stiff & Davis Saturation Index	0.95	-0.17	0.56
Ionic strength	0.03	0.03	0.06
Osmotic pressure	13.3 psi	13.1 psi	25.8 psi

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics.

Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578

Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYDRANAUTICS R	RO SYSTEM DESIGN SO		. VERSION	ON 6.4 (d	2) 1998	12/1	2/1999
RO program lic Calculation cr	ensed to: eated by: J. Lozie						
HP Pump flow:	McAllen Phase II 25.4 cmp press.: 140.9 p	mqg		e flow: er flow:			gpm gpm
Feed pressure:	131.5 perature: 31.0 (osi	Permeat	e recove	ery ratio:	50.0	8
Raw water pH: Acid dosage, p	7.80 pm (100%): 56.9 F	H2SO4		cline %	per year:	7.0	years
Acidified feed Average flux r	CO2: 57.9 ate: 12.0 g	gfd			crease, % W	/yr: 10.0 astewater	
Stage Perm. Flow	Flow per Vessel Feed Conc	Flux		Conc.	Element Type	Elem. No.	Array
gpm 1-1 6.0	gpm gpm 12.7 9.7	gfd 17.0	_	psi	LFC1-4040		2 x 3
1-3 1.5	9.7 7.4 14.8 13.3	13.0 8.4	1.03	61.3	LFC1-4040 LFC1-4040	_	2x3 1x3
1-4 0.6	13.3 12.7	3.3	1.01	32.4	LFC1-4040	3	1x3
no. pre	ed Pres Perm Perm es drop flow Flux i psi gpm gfd	:	Perm sal TDS		ncentrate SO4 SrSO4		
1-1 1 131 1-1 2 123			25.6 27.9	14.3 15.7	11 6 12 7		LO -0.1 L1 0.0
1-1 3 116			30.3	17.1	14 8		0.1
1-2 1 107 1-2 2 102	.1 4.8 0.8 12.9	1.08	33.3 36.4	18.8 20.4	15 9 17 10	738 1	0.3
1-2 3 97.		-	3,9.7	22.4	19 11		L6 0.5
1-3 1 90. 1-3 2 80. 1-3 3 70.		1.03	41.8 44.2 46.8	23.5 24.0 25.0	20 12 21 12 22 13	903 1	.6 0.5 .7 0.6 .7 0.6
1-4 1 58. 1-4 2 49. 1-4 3 40.	4 8.6 0.2 3.2	1.01	49.9 53.3 56.9	25.6 25.6 26.2	23 13 23 13 23 13	977 1	.8 0.7 .8 0.6 .8 0.7

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

				_			_		_		_	_	_				_	_		_		—			_		_					—	_				_				_				_			_		
(40 mey) (44) 114,5	:	• -	£ £	173	2 :	2	. 6	130	132	ŝ	ê :	: :	:	:	::	::	13.0	130	į	e i	200	130	e -	ŝ :		2	ç	13.0	ē.	š :	. 624	6.7.	•	: :		173	17.3	173		17.3		173	: :		5,4	17.3	2		173	
(em) Tite	75.27	12 37	5	:	2 :		**	*	154	:	2 2	12 37	1237	12.37	12.37	7 2	8 24		824	1 5		6	:	2	ž 2	- 2	171	124	171	2 5	:		:		:	:	:	= :	: :	61.0	:	: :	: :	:	:	:	:	::	3	
Permentally Common but Temperature Ellevin (glelpal)				1	8 9	2 5	27 22	72.75	8	40 12	7.74	3	8	8	1	9	25.35	10801	65 93	65.83	8 3	0	10 80	1000	101.01	8 8	270 04		3	8 E	35 16	35 ce	38 1	5 20	3.4	23.48	45.78	2 2	; 2 ; 3	ž	Ä	Ę.	# 3 2	1 2		ë	9	2 6	3	
jedgyl) (lyppeni				#	22	2 2	, N	8	7, 25	22.74	E 8	*	9.00	8 78		3	75.35	8	88	\$ 2	8 5	A 15	44 90	108.48	7 5	2 20	263.7		22 25	8 2	8 8	38.16	91 SC	2 2	2.2	21.98	\$	8 : F :		38.18	35 76	=	io :	2 12		8 92	8	5 5		
(hel) Will				150	0.25	9 29	637	0 37	0.25	0.25	\$ 5	;	010	010	;	ŝ	710	0.12	0.20	0.20	2 5	200	21.0	21.0	0.25		900		978	£ 8	3 3	0.49	840		2.0	97.0	20	, t	•	870	9.40	160	Į ;			1	ŗ.	ž :		
Approximates	START OF TESTING	3 44 5			married charming	Guandaren sena	·	Constitution of the Consti			und down due la recreatifich purry impelier		•	Drawing Chairman			Proceed flow rate to 4.5			mart claining			granul charms		Granably streets	_			-		S region of the Residence	marr clearing				meet cleaning					mant cleaning							Disputation Franch	Company of the same and the company of the company	
Physical (min)	ā	2 5	· •	5	9	5	2 5	2	ě	<u> </u>	\$	2 2	•	٤	9	9 9	5 5		2	•	۶ :	2 5	2	2	2 :	2 9	2 5	2 2	2	2	2 5	· •	2	2 1	2 2	5	2	9	<u> </u>	. 5	•	5	<u> </u>	2 9	. 5	•	2	9 9		
(see) Pedianud W	8	8 8	. ž	8	15 10	8 :	8 8	8 8	15.00	8 2	8 :	8 8	5 20	8	š	8 8	8 8	8	8 5	01.81	0 5	5 5	\$	8	£ 4	8 8	3 8	8 2	9 5	8 :		8	15.00	8 5	8 8	8 5	5 80	ž 8	8 8	8	8	8	8 :	8 8	15.00	8 5	8	8 :		
n) the cale of the last			5 6	8	60	8	8 8		6	60	:	6 6	:	10	10		5	:	70	•	8	6 3	: 5	5	9.5	: :	5		9	60			9.0	• :	2 5	5.	:	8.0	: :		=	:	:	5 5	:	•	3.0	a	2 %	
48 wife staff inemity? (mqg)	ŝ	: :		:	ş	÷ :		; ;	;	¥	;	2 2	9	30	33	ê :	5 5	*	ş	ş	; ;	: :	: :	:	÷ :	;;	•	: :	ş	\$	ş ;	: :	:	: :		•	:	9	2 :	2	*	:	•	::	::	•	:	:	2 2	
Marie (SP) riamit (smell.)	ş	ο :	130	:	?	•	2 :	2 5	13.0	130	8	6.5	9 6	96	130	ē i	2 5	130	130	130	ŝ.	9 5	5 6	ŝ	130	200	ē:	.30	0 64	96	95	130	130	130	5 5	130	ē	130	0 0	9 6	130	130	ě	2 5	5 65	9.5	95	ŝ	2 6	
(lod) stressed di	3.0	30		ŝ	30	30	9:	; ;	: 2	30	2	8 8	3 6	30	33	35		35		90	6	÷ :	2	30	30	£ :	;	32	33	12	7 7	3 2	32	32	2 2	33	33	93	2 :	7 6	- 6	318	3.5	7 ;	32	32	33	33	33	
nd of control matrices.			9 9	57.0	850	2	9 5		950	20	326	023	070	020		0 10	3,0	0.25	040	0.40	0.25	9 9	52	0.25	9.50	0.25	979	9	0.50	97	970	8 8	8	8	3 3	. 2	0.75	110	8 3	8 8	8	87.0	9	8 8	3 3	5	350	8	2 g	
encied chiff chemics (mag) %	e.	30	9 9	:	4.5	4.5	¥ ;	: :	: \$	\$	=	8 5	30	30	ê	E :	6 *	: 4	ş	*	\$	\$;	; ;	\$	\$	÷	Ş ;	÷ ÷	\$	ş	:	2 0		:	ş ç		9	ç	•	0 0	•	:	6.0	:	2 9	0	9	Q.	: :	
notestavinos control (mpg) terri	ŝ	ä	ğ	8	٠ 1	ê	92	5 5	3 5	å		ů ;	ž	ŝ	8	ŝ	8 8	1	ě	ů	310	ř	3 2	Ř	Ř	ŝ	Š.	, i	ĝ	8	ŝ	3 3	ŝ	2	2 2	27.0	280	27.0	96	5 5	280	ž	ŝ	ř :	8	Š	ĝ	ž	, p	
(refr) AA bekeeringeri	=	35	; ;	3 50	9	3.6	98	£ :	: ::	==	<u> </u>	: :	; ;	35	38	*	ş ;	, ,	£	£	\$: :	= =	2	36	- F	35	- S	; ş	3.5	<u> </u>	35	#	30	7 7	; ;	30	35	£ :	2 :	:	*	9	7		#	7	2	35	
(man) W.Z. et	2	35	25.0	ž	25 0	28.0	ŝ	23.0	ž	3 2	380	82	Š	ŝ	26.0	25.0	2 5	2 2	*	280	82	380	s 8	28.0	0 52	ř	ž	£ £	9	82	380	2 22	ž	250	22 22	ŝ	280	250	22.0	220	320	250	28.0	S	8 8	28.0	\$2	28.0	28 28 28 28	
(O correct) Wil spice	- ₹	3gr	2 2	27.0	27.0	280	27.0	2 20	27.0	: :	27.0	= ;	2	ž	23.0	20	2 1	2 5	2 92	28.0	82	ž	2 2	8	340	\$ 2	27.0	2 2	2	2.0	22.0	32 %	. %	2	2 2	* *	38	280	ž	220		Ř	27.0	Š	2 2	ž	250	ŝ	27.0	
(md8) aprendy pro	1		_																					_		_					_					_										_	_			
Telegopa general	a iğ	4.251	4287013	436718.9	4373334	4375380	4412984	443078	1000	448200	467864 7	456015-0	1 2 2	4881450	458208	4684400	4423275		200	1100	11/2	* SOZ	474404.0	479780.0	\$ 179E/1	4797211	4,000,7	199997	******	401046 4	400001 S	11.11.1	7	\$431.72	504924 0	10103	508155	5100714	\$156201	5160340	2	5214884	0 089 25	\$27005	52000 1	536146.7	1717	14G777 2		
	- Z	2	5662	100	7 01 95	21.7	757	ğ		2 9995	2	E		5700.2	9 504.6	5708.2			57474	5748 B	6750	57542	2 2	,	274.7	5787.5	27.00	1		i	9		20,5	5000 2	į	9 9 9 9	ž	\$617.2	8 9035	100		•	•	Š	3	8	\$ 1,20	7000	8 6	
Brettersey's destinations (even) and	900	95 E	2 80	2 2	8	2	8	8	¥ 5	8	127 68	22.	3 2	-	8	18.081	8	8 1	2	2	£.3	200 SE	27.2	8	245 08	244 55	247 08	346.00		283.08	313 68	319.08	8	337.08	8 :	8 5	71 18	3	386.28	20.00		41217	#15 OB	£ 13	8		2	8 74	1 2	
(minute) and	4 8	17:30 AM	30.44		100	2-46 PM	730 AM	8	715 AM	1 8	10 M AM	# 00 *	8 8	W 80	3 3	ž.	7 30 AM	200 PM		10.00	4 to 10	1007	730 44	3	***	11.00 AM	130 PM	30.44	1000	11 30 AM	730.484	200	130 %	7.30 AE	30 Pt	8 8	MV 97 01	18 PE	700	36 PE	# 3 R 2	7 7 7	5	*10.4	11.2	1000	730 /4	1 8	2 40 PM	
-	+	02,11 8881-800		_	_	_			_	201010101010101010101010101010101010101	_		_			_	-	_	STATE OF THE PARTY		6217/1988 11:16	_	Mariante 7.30	_	02/14/1888 P.38		_		_	02:11 0001/12/20		_	_	OF 1.30		02 1 00 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	_	44214441444	CD/25/1988 8:50	4472671980 13:30		M. 01 MALES	BE-ST- GRETTER	34 T771000 0E.10	6007771500 (1:16		WASTATION TO BE	G201/1980 13:30	CONTRACTOR TO SE	
•		1	Sam bridge	Des. 1/7/20		-	Tun 2/8/48	T. 2008	and an and		301.00	Ban 271 048	800 PJ 400		5	***********	Tue Brieff	The bridge	Tan Milana	- Table 1	B111.00 Pmg	Wed 2/17/80	-		BARRAT VA	-	FA 27878	173677	2000		Man 1/23/80	Man 2/23/46	- NO.	Two Prints	Two Miles	2000			7 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	The Militar			To breeze	-				2014	4 m	
possgriffi		•																																																

Page 1 of 13

		_				_	_			_			_			_			_			_						_	_	_	_		_		_			_	_			_			_	_	_	_	_			_	_
(see may) (see)	. .	E.7.1	: :		17.3	17.3	17.3	173	173	<u>.</u>	<u>.</u>	: :	: :	173	17.3			_				_	_			ş =	:	: :	<u>:</u> :	<u>:</u>	•	•	<u>•</u>		<u>.</u>	•	<u>:</u> :	· •	·#1	è	-	•	•	• •	<u> </u>	: :	=	•	11.7	ì	<u>.</u>	•	<u>}</u>
(cont) Title	: :	=	= :	:			-	-		:	: :	: :	: :	:												424	1.28	4 24					\$ 7.5	5.71	5.2	5.71	2 2	: 5	5 73	5.71	\$ 7.	5.75	£ ;	5 :			2	2	6.73	571	5		
Permentality Correctors for Temperature Effects (probps)	2 2	689	, i		ş	\$	š	10 18 B1 01	26.	=	= 1	2 :		•	8 62											£	£ 23	2	2 :	9 8	8 8	R (6	37.20	29 62	R	27.28	SF 2	, ,	28.87	26 57	20 22	30.27	20.57	7	•	2 1		24 80	8	2	E 22	2	R S
(Indicate) (Silderented	8 E	8	8 :	* 6	52	:	\$28	50 01	\$28	2	2 :	9 :			\$25		_						_			2	1	:	8	2 2	* *	8	8	27.16	8	8	2 1	3 2	7.	27.21	31.74	2.6	2	8 :	8 :	8 1		8,52	R	8 82	R K	*	F 22
(bed) Will	* *	2.	6	-		:-	4	ŝ	•	÷	ē		9	3 2		_	_		_							0.75	520	0.25	•					0.50	•	Ş	2		850	880	3.0	950	8 5	0 74	2		5 5	9.7.0	27.0	77.0	0 74	974	7.0
.,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		Durant chanters					Charles Charleton			_					and the to secretarion parts blice														mantheus chargeod		mart dearing					make distant	alter classimity				Preside Comments	after cleaning			Designa masters flustri	Mary many float	,		Sales man charles				
ps, Landrouck (upu)	9 9	•	2	2 :	2 9	2	2	9	0	2	9	2	9	2 2	2 5											2	•	2	•	2	2 :	2 9		٥	•	2	2	2 .	: 2	•	٥	0	9	•	2	2	2 :	2 2	2	2	2	ē	5
Dif Duration (sec)	8 8	15.00	8	8 5	3 8	15.00	8	8	15.00	8	8	÷ 8	8	8 8	3 8	!										15.00	B	15.00	8	8	8 5	8 8	3 8	8	15.00	8 2	8	8	8 8	8 5	8	15.00	5.8	15 10	5 5	1. 0	8 5	8 8	8	8.5	8	8	8
nt) will solve gardy.	3 \$	20	8		: :	:	÷	38	1	2		:		; ;	::	;			_						_	\$0	*	50	-	ē	7 :	~ :	::	: :	-	1.2	~	~ :	: :	:	:	3	:	į	ş.	7	5 .	:	: :	=	ē	-	•
To refer that the office of the control of the cont	::	:	:	9 :	2 9	: :	9	•	9	:	•	•	:	::	:	}	_									÷	÷	•	:	:	S :		: :	; .	4	5	ş	2	* *	•	Ş	ş	50	:	*	2	4	: :	: :	: 5	3	•	\$
Series in the year Tare (credit)	13.0	ŝ	13.0	5	2 5	95	130	130	061	6	130	<u>6</u>	2	£ :	2 :	•			_	_			_			96-	9	9.		9	9	•			65)	130	65	ê	9 65	130	130	130	130	85	ē.	13.0	65		9 6	÷	140	•	13.0
(log) ericocerd #6	2 2	35	98	?	7 :	: :	: :	*	35	:	7.	77	32	2 5	? ;	;			_			_				*	2.8	5.4	2.2	7	# 2 2	8 :		2 2		*	\$ 2	3.6	* *	*	92	B 2	*	\$	52	3.6		: :	: :	: 2	2.7	**	.
nt) 45 probed passery (pr)	8 8	8	320	ş	8 8	:	3 8	336	8	8	8	8	9.50	3 5	8 8	§ 	_	_								ş	0.50	8	8	\$	62	2	8 5	3 8	8	8	8	ŝ	R E	\$	8	8	ž.	5.	8	8 7	8	3 5	3 5	3	8	8	š
enthal state designed (magg) the	::	•	:	.	::	: :	: :	9	:	9.0	:	•	9	9 :	2 ;				_	_		_				ş	•	÷	59	:	:	5	:	9 :	: :	:	:	:	5 :	: :		•	:	:	-	:	3	: :	::	: 2	:	45	3
	2 2	24.0	27.0	Ř	2 :	:	: :	•	z	210	170	3	280	_									_			2.2	Ř	, ř	ŝ	37.0	37.0	37.0	*	•	3.6	8	*	9,6	ž (· 8	37.0	37.0	ä	*	Ř	ž	Ř	ž :	ğ ;	ì	Ř	98	i
(print) the intermediated	3 2	=	:	38	£ :	: :	: :		35	35	36	*	:	£ :	£ :	=	_				_	_				37.0	350	*	ê	Ř	ŝ	38.0	¥	8 8	Š	8	98	ĝ	2 2	*	×	98	98	Ř	å	3	ž	× :	3	3 8	ŝ	÷	•
(man) WS and	S 82	ĸ	28.0	28.0	8	è i	9 5		25.0	280	38	220	220	23	2	ŝ			_	,		_	_		_	ŝ	ŝ	220	280	\$2	280	22	\$2	ž ž		82	250	28.0	2 2	25.0	8	\$2	25.0	280	220	92	8	8	8	Ĉ K	8	ģ	280
() stergeb) WS que?	£ \$	ž	28.0	9. %	ž,	R :			22.0	27.0	27.0	27.0	27.0	22	230	•			_			_		_	_	ŝ	ž	*	ž	ŝ	8	\$ 8 0	è E	2	2	280	280	280	2 2		57.0	270	27.0	27.0	27.0	27.0	\$	8	2	R %	Ř	27.0	28.4
(met) annual pro-					_	_					_		_	_			_					_	_			_			_	_	_		_	_					ř i		ĝ	_	_		20	_				2 2			
(ex)				_	_	_	_	_	_	2772	573001	546120	507408	CHARGE	561 108	20.5	_					_			_	568140	See CO.	900456	804443	61128	61218	91249	613120			620730	629162	81009	436		90579	15.534	646227.2	19/238	66,3689	840775	96038	#12#2 7	Ī			671511.4	677430
gretnerelt senset transf	60487	0.00	8	8072.8	809	_				6130	41412	6.29.9	-	£	6178	- - - -				_	_					62129	62150	903	623		428	ē				6307.0	6308.2	6312.2	2	9 8	ì	6.000	963	5	63778	1878	900	•	2198	1	3	ş	1
grammer articles and the first out of th	811.08	2	502.58	8	563 G	8 9	2,		5	1	80 408	80.909	E 629	3	B6 2 08	2			80 634	8	80.03	8 3	80.08	863.08	20	2 2	5	5	708.00	¥.	728.17	5. B.	ž.	37 (# #		788	78.00	197	i	2 5	2	127 58	3	3	3	2	8	867.36	1	1		913
(represent) energy	130 PM	M 400 01	11-00-44	130 PM	7:30 444	8	1807	8			10.30 AM	7.30 AM	11:30 AM	7:30 AM	10.30 AM	3	8	8 8	700	8 21	12 CO AM	12 00 AM	12 00 AM	12 00 AM	¥ 82	100		200	8 2	7.30 AM	10-08 AM	11:40 AM	30.00	130 4	8	W # 01	1000	300 PM	130 AM	8 2		1 20	30 94	7.30 AM	10:00 AM	10 16 AM	200 PE	7:50 AM	10-00 444	# R	7.00		7.30 AE
	eposition 1979		######################################	86.01.986.13.38	900-01100 T.30	10 to	654 Table 7:30				02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02-01-02	#:: 49017779GS	44/7/1989 11:39	62/GB/1000 7:30	61-04-10-10-10-10-10-10-10-10-10-10-10-10-10-	42-51 0001789405				CONTACTOR CON	*****************************	03/16/1888 6-68	CHITCHES OF SO	83/17/1688 6-86	Serialism area	ar all all all a		00001/1880 7:30	04/21/1908 12:48	425 MINISTER TORS	Destantes 10:46	BK11 6881/27/20	8775/1888 13:38	4477 WELLER 7:30	COLUMN IS IN	-	92247888 12:48	CONTACTOR 16:00	BEST 888 T-242	0.71 mai/22/40	117	100	C.21.001.700	642771988 7.30	08-27/THEN 10-00	BE-94 40-1/2000	SECTION 12:00	Mary and Parket	42 Taring 18:40	E-11 0001/05/02			66.7 SMINITED
	1 m		200	***	The State	The Bear	frd artifes	Fit Mells			4	See. 37789	East 27.00	1	Mar. 1884	Man 3880	T. Mar.	-			200	- N. C.	Tue bridge	West any Tree	The STREET	PA STATE			1	-	Men ydzyse	Men 34234	Man 972348	Tue 2/23/10	A STORE		Wast Miles	West 3/34/80	The articles	1 × × × ×				Bet 25778	Par 207778	Sec harries	1	20 Marie	1				agracia page
																											•																										

Page 2 of 13

	_						_		_			_						_	_				_	_						_	_	_		_	_	_		_	-	_		_	_		_	_	_	_	_	_	_	-		_	
(48 10(1) (148) 20(4	•	22		27.3	27.3	27.3	27.3	873	2.2	2	:	2 2	1 2	•	-	-	ţ	-	ž	•	, F	•	•	•	•	**	•	<u>*</u>	-	•	<u>.</u>	<u>.</u>	•	•	:	187	•	•	è	-	<u> </u>	•	•		18.7			18.7	•	-	•	•			-
(end) Trib)	£	<u>.</u>			ē	â	18 5	5	18.0		ā ;							5 71	571	5.71	5.71				\$ 7.	5.73	\$71	17.5	573	\$ 7.1	571	571				571	571	125	5.71	5.2	E .			573	5.71	571	17.5		7.		2.5	2.7	5.71	5.73	7.
Sacrista (gridina)	28 72	8 5	1 2	96	12 08	10 62	1327	1387	245	3	£ ;			-	20.02	20 67	20.38	21.33	20 02	20 12	20 87	19 12		2 9	78.02	20.38	20 87	16.71	8	8		8	21.37			20 67	8	20 M	20.38	20 67	20 M	# 8 R 5		96	20.87		20 87	71.22	¥ =	200	8	8001	12.40	į	861
مستجهون (فیجیده)	8 8	6 1	2 1	12.37	12 37	- 61:	23.62	8 7	24 0	3	2 1	R 8		-			24	324	24	241	1341	8 :	9 :		-	., 22	1.52	21 16	72	1,22	22 41	- 224	3 3	= :			24	23.61	17 42		÷ 2	-		24	3	24	5		8	R	8	200	2	8	2 70
(red) 481		2					_	_	_		_		8 1		-						<u>. </u>					-	_	_	-	-					_	_		-				_	_	_	_		_	_	Ŀ		•	2	•	6	-
	_	_	_	_	_	_	_	_		_	_					_	_	_	_	_	_	_		_	_	_	_	-	_		_	_		_			_	_		_	_	_	_	_	_	_	_	_	_	-	-	_	_	_	_
sperios y			And best for leasing a 9 5 graph and hand			grades choring	after marri channers				_		grant and send bree		and character	-				Distance mental channels			mand cleaning	_		_		mant chancing													mark cleaning					mary deserve				_					
PP Frequency (min.)	10	9	₽:	2 2	2	2	9	٥	2	ē	9	2 :	9 9	2 !	2 9	2 9	2 9	2	2	2	ē	2	٠ :	g :	2 5	2	9	2	2	9	2	2	2	6	2 5	2 5	. 5	٥	5	٥	2	9	2 :		? 5	. 9	. 9	· •		•	2	5	2	•	•
(see) notice (sec)	15.00	60 51	8 :	3 8	8 5	85	98	5 00	ts 00	8	8	8	8 5	9 1	8 5	8 8	3 8	8 8	8	ž 8	5 00	15 00	8	8 8	3 8	8	15 00	8	8	ĕ	8	5 8	5 8	\$ 8	8 8	8 8	8 8	8	\$ 00	58	5 8	8	8	3 8	3 8	3 8	8 5	8	15.00	15.00	8.5	15.00	5	15 00	15.00
ni) 98 volta amenty 1971	2	1	•	: :	: :	:	3	:	:	÷	;	42	?	•	: :	= :	: :	: :		:	-	:	20	•	- :	: :	-11	:		1.1	11		-	:	• :	: :	: :	: :	:	-	11	-	-	-:	: :	: :		:	32	32	3.5	37	2	2.3	2.
استعدد العلم عالم: 15 (جوس)	::	5.6		2 2	: :		\$ 8	9.8	5	\$	5	S.	•	S :	•	::	: :			5	Š	:	S.		::	: :		6.5	5.0	÷	5	2	5	ş	ş.	: :		: :	5	•	\$	59		: :	: :	1 :	: :		9	2	:	2	Ş	:	\$
life been in Cife Territ. (Linear)	13.0	12.0	12.0	2 :	2 2	967	130	130	130	130	0.0	130	13.0	92	0 0	98 9	2 5	2 5	9 6 5	130	13.0	001	13.0	50	2	2 5	130	130	13.0	130	9	13.0	130	0.0	130	9 9		130	0 7	30	96	130	Š.	9 9		2 5	2 5	9	9.5	0.61	130	13.0	130	13.0	13.0
(log) enterery 94	2.8	2.8	2.8	2 :	::			*	32	33	33	32	35	35	33	? :	£ ;	. :	; ;			?;	Ę	2	35		33	7	33	30	3.2	32	32	32	£ ;	2 :		3 2	32	32	7	77	2	7	7 :	; ;	; ;	2	33	2	3.5	3.5	37	38	35
A) 48 mated moresty (git)	3	340	8	9 5	3 5	8 8	8	9	8	9.	5	50	8	2	2	8 1	2 5	2 :	2 2	2	5	8	8	8	2 5	2 2	2	8	8	0,1	67.	2	e	8	0, 1	P 1	2 5	2 2	5.	0,1	1.70	0,7	5	2	R :	2 :			2,5	9	3.40	£	8	3.6	3.00
erated while absorbed (magg) Th	:	:	2	5	: :		\$	*	5	5	ş	r	:	:	:	*	·	: :			50	:	5	2	: :	:	: :	9.0	2	48	2	9	\$	\$.	9	3 :	: :		\$	5	\$	\$	9 :		2	:	: :	: :	2	9	: :	4.5	:	:	6.5
App. (80-44)	ŝ	9	Ř	8 1	Ř		360	9	37.0	410	37.0	š	320	Š	9	ž	Ř	R S	2 5	â	3.0	ŝ	ş	Š	ě :	•	. 6	31.0	Ř	ê	42.0	37.0	9	8	2	8			37.0	Ř	ŝ	9	ŝ	370	è	3 1	Ř į			2	0.5	•		Ř	Ř
ofts) at here of the (other	۽	0;	0.1 4	0	•	2 02	9	0	01	47.0	45.0	430	ŝ	:	0.7	0,7	9	\$:	1 5	2	43.6	9	ş	0	9	ŝ	3	9	9	9	007	0;	42.0	ţ	5.0	3	5 5	2 5	20	42.0	45.0	ŝ	ŝ	\$	\$	9			1	•	ŝ	9	0	919	65.0
(mile) WZ M	0.52	25.0	25.0	280	Ĉ.	C K	250	£	250	230	25.0	220	28.0	220	25.0	986	250	ê i	Ĉ ;	220	0 52	250	25.0	22	230	230	24.0	ž	25.0	220	280	\$2	25.0	28.0	052	220	2	£ \$	28.0	25.0	250	25.0	250	ž	220	22	8 3	2 5	ž	2	2	280	ŝ	ž	22.0
(5 seergeb) WS gras.	ı	Ê	3 8 .0	30	5 5	£ :	200	27.0	22	25.0	28.0	27.0	27.0	200	27.0	270	2	ž :	0 2	2 %	0 82	27.0	28.0	õ	ĝ				2	90	26.0	900	27.0	ę.	380	ŝ	2 2	9 8	ž	280	280	982	30.0	0 R	96	Ř	2	R S				20	ž	*	2
(mag) aterprefit bee	22	ន	22	2.0	510	2		57.0	92	92	280	82	9 12	240	210					_							_		_														_		_	_	_	_	_		_		į		Ř
resident america (reg.) prainced	671916.5	67EG4217	5.0796.0	678727.5	878811 S	6780810	CONTRACT OF	8807821	984380	0.904460	1.009689	6010672	9 279186	0 827289	0000740	700018 4	70011014	7000782		716407	714666.5	773848.2	724634 0	7240514	725301 2	A THE	TATOOR A	1	741217 5	7 17 2027	7488S7 8	7508151	750001 8	757577	754047.5	758039 6	4		77877	782388 1	7834720	783867.8	784229 P	7906142	782718 5	2000	78615	2000			9	2.00		1	7447
town Notes Personal year	į	7 99	185	9	3		į	1	5	£7.	£19.	12	•	i	- 1099		1,000	6908	2		1.099	£7.5	45754	1.00	6678.2	•			Ì		1	80	į	į	01/10	5 EZ 5 S			2110	Ę	6741.7	8742.5	6744.1	-	Ē	Ē	5					i		Ì	7 55
(LAS) cop Supporto entreprinto	3 2	62,619	915.68	915.60	8	8 1		20128	B2138	75.126	35 85	2	8	3	8	35 52	8	3	3 :		3	. CSO	1036 54	1007.00	1027 08	£ 787				200	108.33	112.0	8	131 04	133.33	138.08	3	157.08		80.00	201.00	1206 50	207 08	1225 00	27.08	1248 08	35	25		2					1 000
(referency) even		7.0 AL	9:00 Met	MA 40.0	0.25 AM	D-65-744	8 3		2	- No Par	MV 90 /	₩ 000	7	M- 90 2	30 AM	# 80	130 Att	8	8	8	MV 00-01	1	94 OO-O	126 AM	MA 0C 1	30 AM	8		1		3	74	7.30 All	20 AL	11.46 AM	20 00	8	2		100.7	MV 00.0.	11:56 Ale	- S	7.80 All	30 Pa	7 30 AL	¥ 95	\$ \$		8 1	2				
 	+-	_				_	_		_							_	_	_	_				_	_	_	_	_	_					_	_	_	_		_		_				-		-	_	_	-	_	_	_		_	_
-		SATATION 7:48	82717888	03/31/1888	ON THE	9861/15/0	Control Man		A. 41 COLOR	03/31/18	9-4-01/1988 7:08	04/81/1989 10:SE	0401/1000		04/EF/1988 7:38	BANKSTING 10-40	04-11-888 11-30	# E1 ##CENTERS	PACE PACE	04-10-10-10-10-10-10-10-10-10-10-10-10-10-	-		GARDETTERS 19:40	82-11- 588 71 584 48	AC: 0001/2040	04:17 0001120Teq	441 888 7884	THE REAL PROPERTY.					at / marriage	04/DB/1988 9:30	84.11.4881TEMAG	04/08/1988 14:39	B018 6841461490	SCHOOL STORY	Section of the sectio		M. 91 #8874700	85:11 886 TETANO	04/13/1444 13:30	04/3/1998 7:30	D41 31989 13:38	041419987:38	BAY14/1988 9: 20	86:11 (86)	84.47.900 14:30						ACC 77000 7:15
	<u> </u>		1	97178	100							8			į	•	į	į	•	*			ş	į	į	1	ļ					_		į	FH 47878	Į			5			*	845		*		•	200	•	•	8		1	•	
			ì	į	ì	į	•		1	j	į	Ž	2	į	ž	•	į	į	i	i	i i	i i	Ì	Ì	ì	<u>i</u>	į		-			! <u>}</u>		į	į	Ĭ	i	<u>;</u>	j	i i	i	i	į	į	1	Ì	Ì	ì	Ì	į	į	Ē	E		<u>.</u>
, magazin		-			-	-	-	_				. .																																											
	ļ																																																						

Page 3 of 13

				_	_		_	-	_		_	-	_	_			_			_	_	_			_		_	_		-		_	_		_	_	_						_		_	_	_				7	$\overline{}$		_			_	
Land (yeger, gap.) Land	•	•	2	•		•	-	•	-		•	•	1		•	-	18.7	•		È	•	•	69		•	-	-	•	, 1	•	•	ê :	•		•		•	•	14.7	•	1 1	=	•		•	•	-	-	-	=	10,1	183	ē.	•	-	117	=	
(end) Title	5.71	5.7					: :		; ;		2.2						2.5	571	5.73	57.	571	5.71	571	5.71	571	5.73	5.7	571	5.7	2		2.5	2		2.	5 5		57.	5.73	5.71	5.72				; ;		; ;		2.5		5.71	17.8	2,5	57	577		571	
Personal Statement of the Temperature The Spirited (spirited)	2	15 24	2 :			8 8	2 3	2 9	3 1	2 8	10.00	5, 0,	9 3	2 2			*	2	95.0		\$	8.25	8 45	155	8	:	\$	2	3	. 25	8	5 .	52		928	8 8	5 5	8	22	\$	\$	101	7.53	16.	R :	; ;	2	8			95.5	8.5	ž	2,5	150	iş.	=	
(adjust) Assessed	2.5	15.24	25		2 :	: :	B 2			8 3	5	X .	2	2 5		2 2	20.02	20.02	200	62.01	60	40.6	000	206	0 03	25.		208	3	6	404	9.20	60		408	6 5	200		6 07	404	404	7.7	ž	9	2 :		2 3			: :	ĭ	:	ž	3	2	Ŗ	28	
(loop) *Mil T	1.67	1.23	ā i	2	2 :	i F	2 1		2 !	2 1	-1	ě	-	2 5	1	2 2	2	2	2	2	80	8.7	2.00	2 08	8	8	201	8	ž	28	8	201	8	:	2 08	8 1	5 6	: :	8	80 2	8	7.	ž	531		5 :	:	:	75.		80.	8	7		3	2	28	
******* *****************************					Contract Contract						mant clatering											_		mays chang		-	_			ment clearing		_				Depart seem	_						ment clatering									Apr. (and 14 AS to 10 000 mg/.						
(rein) described (12	2	2	2	2	2 :	•	<u> </u>	2 :	•	<u>-</u>	2	9	2	•	9 !	٠ :	2 9	-	2 5	? 9	2 2		. 0	2	•	9	ō	9	ç	•	2	<u>.</u>	2	9	5	•	2 5	2 9	2	•	9	ō	6	 5	٥	<u>.</u>	2 9	2 1	2 5	2 9	2 2	٩		. 9	: :	2 9		
(see) nedamic we	15.00	8.5	8 2	<u>.</u>	8	8	<u>8</u>	8 .	8	8	8	8	8	8	8 :	8 :	3 8	3 8	3 8	1 8	3 8	8	8	8	8	\$	35	8	1800	8 8	8	\$	ě	88	90 \$1	5 00	ž ;	8 8	8 8	5 8	8 5	15.00	58	š.	8	ž :	8 9	B 8	8 8	3 8	8 8	٤	3 5	3 5	3 8	3 8	8.0	
A) 98	2	52	5.5	35	.	6	<u>.</u>	66	2	SE	37	c	35	·	ě	32	; ;	; ;	; ;	; ;	; ;	; ;	; ;	-	÷	•	; 	7	38	:	Ş	ŧ	¥	:	42	4 5	: :	; ;	: :	7	7	;	;	;	Ş	\$	•	•	9 :		3 3		3	: ;	: :		: 3	
**	:	979	5	\$	er .	•	•	9	<u>.</u>	49	*	5 9	:	\$:	S	: :	::	: :	: :	: :	: ;	: :		*	:	:	43	6.5	\$	5	:	2	5 P	2	ş	; ;	: :	: :		ş	65	5	45	ş	\$:		n :	9 ;	4 5	:	::	: :	: :	3 5	: \$	
200 to 600 Tours (mail:	130	130	13.0	9	6	130	130	130	96	50	961	6	000	Ē	9	9 1	0 9	0 5	2 :	2 5	9 5	:	2 5	2 2	130	130	130	30	130	130	9	13.0	130	5	13.0	ê	ŝ :	9		2	130	130	ů.	6	13.0	130	0	200		200	2 5		9.51	? :	-		: :	
(log) primering qu	:	3.	7	98	35	36	3.5	ŞE	38	32	3.5	3.6	•	3.5	3. 5.	36	9 9	•	: :	; ;	. :	; ;		; ;	- `	37	36	3.6	36	3.6	37	37	3.7	36	32	37	: :	6	÷ -		3.7	96	38		38		8	3.5	£ :	36	; ;	:	; ;	;	:	: :	: :	
ni) 'till croked antuce's	S.	5.50	250	320	2	9	8	9	98	55	96	900	9	1. E	6 6	3.70	P 1	2 5	2 2	2 5	2 5	; ;	3 5		62	8	9	4 20	8	4.20	4.20	2	ş	8	4.20	Ŗ	9	= !	8 8	8	8	8	8	4.70	2,7	5.	Ŗ	3	2	8	2 2		3		2	Ŗ :	1 5	
mated shall almano? (mag) '98	:	\$	÷	5	5.5	s.	\$	53	9	5	8.8	÷	2	\$ \$	ş.	ş	:		÷ ;	:	: :	: :		3 5	5		:	ş	8.5	59	65	5	\$	99	S.	Ş	\$	÷ :			ş	9	\$\$	5 9	5	\$	•	5	•	•	: :	:	::	2 :	2	2 :	; ;	
(-44)	ŝ	ş	37.0	•	ĝ	37.0	*	÷	9	9	ě	38.0	970	420	ŝ	÷	37.0	37.0	9 !		3	, ;	4 8	2 6	2	ş	42.0	ĝ	38.0	å	ĝ	340	2	R	2	ş	8	\$;	÷ \$; ×	8	\$	8	8	\$	3	*	3	R	÷	9 :	•	3 :		*	9 :	1 8	
(mfa) AA latnomelaguel	957	420	ŝ	0.0	0	60.0	98.0	ŝ	Š	ŝ	9	ŝ	ŝ	8	9	100	į	9	9	9	9 :	9			9			45 0	0	90	•	0.64	0.67	45.0	•	\$	9	2.0		2 9	0	0 87	0.89	0#	95	9	450	š	•	\$	\$:		0 0	ŝ	ş	ŝ	Š	
(mp) MZ 4%	25.0	25.0	052	25.0	25.0	250	250	25.0	0 52	250	25.0	280	28.0	25.0	25.0	22.0	280	380	250	2	ŝ	8	22	23.	, ,		250	0 \$2	25.0	24.0	25.0	25.0	ĸ	\$2	10	ĸ	22	ю :	: 3	s x	28	52	22	ĸ	22	\$2	ĸ	ĸ	20	ĸ	× ;		2 3	K :	ĸ	ĸ:	8 12	
(3 Tending) M.Z daw.	28.0	22	27.0	10	27.0	27.0	280	240	280	260	27.0	280	30	27.0	30.0	280	28	200	9 .	280	900	2	2	28.0		2		30.5	ž	20	300	R	2	20.5	8	2	8	28.5	2 1			2	2	52	8	8	a	2	8	5	R 1		2 :	:	R	R :	RR	
(vedd) republically from	2 2	28.0	340	58.0	280	240	240	280	27.0	22.0	10.0	28.0	280	280	27.0	280	•	280	24.0	200	Ê	2	ž :				i	200	27.0	240	280				210		012	280	8		210	280	28.0	ę	8	280	200	ê	270	27.0	ž i	Ί.			•		ę ę	
vetilato) Totalizare (ing.) gelland	0.0000	832190 \$	SECTION S	\$40240.4	841078 0	BM123m 0	M2082 4	84418	850815.4	857057 6	1 200728	10000	0 881 990	\$ 1100300	847248	873852 0	174407	174841.5	878139	1962	E #50000	0 246	20.00				9078104	800873.5	916233.4	916847 S	917156.4	B18137.0	2 14772	0 979924	WOODER D	823628	12/2008	934460	010010	0.025240	9513479	0.66617.0	0.015054	9506100	0.512000	6 Zegges	900007.2	\$75451 B	1782412	978408 0	0.01110	98	O WEST	7.071.280	7	100	5 790000)	
Desirate Asset No.	۽ ڇ	7.0000	5 0385	8 53 8	60082	8008	2 6069	0.627.0	6 6269	21909	6063.5	3	, com	8874.6		5	2000	2001.3	7004 8	7022 3	200		2	Ě				7000	1117	71181	71199	7122.7	7140.4	7148.4	7164.0	718.	71672	7.82	718.7		7215.6	7887	7280	2 8222	7260 6	7258	2880	7.7	1	7	4.00	200	7312.0	į	1	Ĩ	7 26.27	
Bolterogic articularies (evil) and	3 2	1346.58	1348.58	80 880	iği i	37.60	1375 00	1383 00	28 GB	1417.04	1419.33	62139	1423 11	<u>8</u>	£7.0	1465 08	3	145 24	1472 08	3	1643 08	1513 04	1817	1537.33		8 5	8	5	8 28	80 786	1544 58	8	1609 08	1815 08	1634 OB	1635 08	28.00	25 BC3	1868 08	2 2		208.08	1707 58	1709 08	1711 06	1728 08	1735.23	173.3 08	1755.20	37.33	20 00 1	3	1783 06	8	\$ B8	1808.08	3 2	;
(mineral) and	4 2	100	11:00 AM	7 30 AM	NA 02	11.15 AM	30.5	7 30 AM	N 00	130.44	9.45.AW	11 46 AM	28.2	3	2	38.4	10 00 th	N 00	2 2	. NO 944	38.48	3 8	11.30 M	3	8 1				38.4	W 00.0	***	£ 3	30 AM	30 96	MY 00:8	9 30 AM	8 :	8	70.	1045 41	1 2	7 30 AM	MV 00 01	11 30 AM	30 74	7 30 AM	2 2	7 30 AM	1 5 4		2 2	7,00	ž g	38.48	7 000	130 44	8 8	
<u> </u>	┿	_	—-				_		_	_	_	_	_	_	_			_		_	_		_		-	_				-	_					_	_	_		_	-	_			_		_			-	_	+	_	_	_	_	_	-
-	╅	Deviation for					_	04/30/1968 7:38	_		_	_	_	_	64/25/1969 13:38	84.7 MHT-01.38	84727188 19-89	BE-11 686179590	OF PT BEALTHON	0474/1989 8:00	DE:11 8881/9/2/90	D4/28/1998 7:36	04/26/1980	PACTAL DE	OCACION IN	OK I I WANTED	A 10.00		27 SECTION 1.28	85-38-1-88 0-38	04/78/1988 11:00	04/28/1888	04/20/1998 7:30	04/28/1998 13:38	40.3 MB1000	04/38/1988 P.30	04/30/1988 11:40	D478/1988 13:50	BE:0 0001/1000	04/01/1968 10:48	of the second second	at 2 age 1 a	00/01/1989 10:00	M:11 8847-8850	05:30 eect/200e	04/04/19EE 7:30	D-00-0-12:41	06/06/1966 7:30	04/14/1646 T-46	04/04/1000 11:46	12.1 4 4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	06/Ne/1688 7:38	BE:E1 888 13:30	Marthem 7:30	04/87/1980 19:00	C6/67/1908 11:3	04/07/17/04/04 12:40	-
•			1	Man 41 mm	Man 4100	-	Bee 41070	Twe 4/20/88	1 00 47078	Wed 4/21/80	- C	#15 45 VA	200	Thu 472/80	Thu 472.46	Fr 47256	F-1-47200	Fet 4/23/88	fel ATTARA	5	Sec 47478	Per 4254	Bun 475/88	***************************************						W. 472			Thu 4/20/20	100	F-1-4780W	F. A. A. Shares	******	Fri 47078				9	S			7.0	70. 25.	ST	-	#25 PM	1	The Mans	į	F# 4770	44 E//18	Fre error	E	
پيندو ميندو د ميندو ميندو د ميندو																																																					J					

Page 4 of 13

	_		-	_	_	_				-			_		_				_							_					-			-		_					-	_					_					_	-		_	_		_	_	_					
End's (*M value) (***)	•	<u>:</u> :	:	=	=	•	•	£	£	-	•		187	•	:	•	È	•	•	-	•	, Đ	187	<u>:</u>	-	1.	1	•	•	•	•	•	•	18.7	1	ě	787		•	•	:	:	: :	•	•	-	<u>:</u> :	È	•	-	È.	<u>.</u>	187	1.	-	•	•	1	•		<u> </u>	•	÷	-	
(end) TRM	128	; ;			; ;				17.5	5.71	571	17.5		5	: :		5.11	5.7	\$71	\$ 71	5 7.1	5.71	17.5	12.4	5.7.6	521	\$ 7.1	5	; ;	; ;	371	5.	5.73	5.73	5.71	5.71	5			; ;	; ;	5			2.	2.5	2.5		573	5 71	571	5.73	171	5.73	17.5	2.5	\$ 7.	17.4			Ę	5.71	571	5.73	
Personality Correspond to Temperature Filmets (philysis	15.9	7.20	3 ;		:		9	8	7 B 7	8	8	3 46		:	8	8 Z 8	9 49	# Y	2	8 72	:	2			8			3		2 1	4	-	7	20.0	20.0	×.	:	: :		9 8	9	6 1		3	2	š	\$3	467	2	404	-	\$ 72	9.25	7	:	224	ŝ		: :		2	2	9		
(estippi) (improve)	133	2		2 2			6	206	20 6	3	2	9			8	3	25	22	10.29	20.03	10 28	80	60.0		8 9		. 9		<u> </u>			2	£	10.29	5 01	6.01			2	2 :	2 :	X :		r.	£ Ç	£ 0	 2	-	2	3,	20	5,01	EZ 01	10.29	2		55 92				10.28	10	8,	8	
ford) Will	# #	53	ř :		, ;		8	8	5 06	11.2	2.11	3	: :		8 1	2	3	<u>.</u>	2	281	2	2	2	! !			-		- 1	¥ !	2	2	5	1 112	1.7	182		2 1	2 1	2 :	è :	2	2 :	2	<u>.</u>	ā	ŝ	2	28		<u></u>	ŝ	79.	2	111	1.72	111			<u> </u>	ā	22		1 87	
	T				_						_	•							_					_					_							_					_	_				_						_													
Olympianac					Distriction Company						Date of the Control							Burnest Justin								1000							Granded Street			_				Duning Charles		_	ar flow mater broken					Cupulatio Seam						Dunied Resu	•						mant charact				
(upu) Asusabauj 🚜	2	9	2	<u> </u>		2	2	2	9	₽	5	2 :	2 :	2	9	2	2	5	ē	:		? ;	2 9	2 ;	2 9	2 5	2 :	2 :	2	2	9	ç	9	5	2	9	2	2	ē	9	2	9	2	ē	õ	2	9	5	0	5	5	2	9	9	9	! :	: :	2 ;	2	2	2	9	9	: 5	
(see) waterned **	8 5	8	8	5.00	8	8	8	5.00	15.00	15.00	8	3 1	3	8	- 8	8	8 8	90 51	8 51		3 8	3 1	8 8	8 :	8 8	8 5	8 :	8 1	8	8	8	\$ 8	8	8	8		3	8	5.00	8	ž. 8	8 8	8	8	88	8	88	8	15.00	8	8	8	8	8	5		1 5	8 :	8	8	5 98	8	8		
A) 45 wite muses (2)	=	;	-	Ş	•	7	÷	7,	77	7	;	: :	=	÷	•	:	ç	3	3.7	; ;		; ;	; ;		3 ;				:	5	•	3.7	37			; ;	'n	3.7	3.7	26	<u>.</u>	2	3.0	37	46	3,	37	3.7	3.6	32	3.7	37	3.7	;	; ;	; ;	; ;	=	2	37	3.7	33	: :	; ;	!
44 with staff feeting	2	ur T	S.	بر 10	Š	5		8.5	5	4.5	÷	: :	9	.n	ş	45	5	5	5	;	: :	: :	::	ç	n :	•	•	s :	v:		*		80	40		: :	3	9	£.	٠ د	ep vs	·	4	5	5	٠ ٩	5	•	5	9.2	5	*	4	3	:	: :	; ;	9	·	ş	5	10	: :	1 :	
dress for Cife Teach (exact.)	1 2	130	ŝ	13.0	130	130	ē	669	130	9 5 1	:		e e	ŝ	30	984	0	130	95	3		2		-	ê	30	0.00	5	5	ě	130	130	130	13.0	; ;	3	000	13.0	30	13.0	130	130	ŝ	ê	000	ē	130	130	13.0	130	130	091	011	:		3	2	30	6.5	ŝ	ê	13.0	:	1	•
(log) musserid 4	ş	7	37	9.6	=	:	37	37	37	1,	;	-		ĥ	36	9,	37	76	3.7	; ;	: :	2	9 :	96		÷	9.	À	9	33	3,	36	36	96		; ;	:	38	3.7	3.6	80		ě.	*	3.6	36	36	3.6	3,1	9.	3.8	•	•	; ;	; ;	; ;		ş		*	ţ	95	; ;	,	,
A) 18 motor manus (p	2.53	P. 4	2	2	2	8	2	22	4 20		! !	2	8	8	8	8	8	8	5	2 :	0, 1	2	9.19	2	8	9	8	2	8	8	8	370	3.70	170	2 6	3 :	9,20	5 6	0.0	3.70	9,50	š	ě	3.70	3.76	3.70	3,0	8	370	360	3.70	3.70		: :	: :		3	8	9	9,76	3.70	5	3 3	3	}
	2	2	 •	7	· ·	5	5	5	4	: :	; ;	Š	5	5	5	:	5	9	: ;		•		S .	٠. •	ş	5	ç	÷	5	9	5	6.5	9	:	9 ;	:	5	5	S,	5	92	\$ \$	ş	Ş	š	\$:	9	65	\$ 8	5 9	2	:	: ;	: :	:	3	5	5	9 2	68		: :	•	}
collectored seemed (mag) ele		ħ	4	2	8	27	×	2	3		; ;	5	5	8	2	8	ş	5		, i		э	ŝ	2	5	8	9	ā	2	Ŧ	;	*	\$	•	; ;		3		1	;	7	;	•	5	4	\$	3	:	=	4	;	\$	•	, ,	: :			3	1		7	=	: :	•	ı
(mts) st. intermedica.		9.0	40	0.64	2	ě	9	480	4.6	; ;		0.5	ŝ	920	989	510	25.0	90		210	Š	0.5	ŝ	220	Š	919	ş	ŝ	9	ŝ	25.0	920	250	i	2 5	2	ŝ	ŝ	93	8	ŝ	ŝ																		ŝ	ŝ	3	ì	S S	
E KAN (coper)	~ ~	72	52	ĸ	ĸ	æ	ĸ	25	,	: :	Ç	8	23	52	22	×	52	. *	: :	£	ĸ	ĸ	ĸ	E	æ	\$2	23	ĸ	23	22	×	25	K	: :	e :	5	52	\$2	22	22	53	23	22	\$2	£	\$2	22	22	22	22	×	*	: :	9 :	ς :	×	2	*	2	ĸ	×	: :	g :	ĸ,	Ç
(3 southerp) MZ desir	, s	8	5	R	R	5	32	96		; ;		29.5	8	8	*	F	8	ş	;	F.	ž	2	31.5	8	8	8	R	16	31.5	38	8	R	8	3 7	ī, ;	ž.	2	£	2	28 8	æ	5	2	80	z	308	28.5	8	=	31.6	ş	; ;	; ;	•	R	Ä	¥	ž	pj	R	Ę	;	÷ :	Ħ	*
(mqg) etamol4 per	9	22.0	÷	21.0	170	280	240	280		3	917	280	9,2	2	900	980	210	,		27.0	2	27.0	280	ŝ	27.0	982	ŝ	200	2	ê	130	97.0				ž	ž	30	90	ě	27.0	8	92	2	28.0	260	280	200	9	380	,	;		2	ŝ	ž	2	280	ŝ	012	940	}	Ř:	380	0/2
Sept British	181	+008785.4	10105561	10178440	101 848 8	1018858 8	8 6354101	1 CONTRACT S				10363200	0 1855811 0	10384560	10428100	10449660	10516464	000000		1062503	1063304 4	1069804 6	10612621	CHESTON O	5 25/100	1077017	1077644 2	10781116	1078636	1085424	1087512.6	1 CHESTAGE 2	A CHICAGO		00000	108500.5	1102085.3	(104291.3	1110626.8	1111560.0	11117810	11123300	1118808.0	1120108 5	11277540	1120005	11396216	11363712	0.0000001	11374072	250			112207	-	153813	154670	1161080 6	11632230	11007419	*******		1170000	-	11/10/20
Suprey Anny an	787.2	7,8727	73817	24012	7400.4	7404.2	7408 8	7.694.8				74500	74509	74834	7471.3	7477 3	7405.8			7	3,00	3 11 5	7.52	7542	7548.1	75688	2	7	7571 9	7560 1	7596 8	7813.8			78172	78182	7657.2	7843.2	76812	70007	7864.5	7886.1	7887	7,687	77083	77123	5257	5 MC//		****					Ē	, 100 100	Į.	7802	7808 0	788		,		22	1
Buggarado sugarpas	2 8	1948 58	98.C381	10.573.00	E 51	C3 8/8:	22.62.51			8	80128	1823 08	1924 84	1927.08	80 594	8	1	1	8	2	1078.00	800	1 mar 7 con	2016 58	2020 58	201.00	2002	2045.08	2047.08	2085.33	2071.04			ž	2083.08	2082 08	211308	2119.08	2137 04	2130 50	2141 08	2142 58	216108	3.5	2186.08	2169 00	2213 08	2211.08	****	40.00		25.00	22.0	8	2258 04	236.00	220 68	85 (BZZ	2287 08	2308.08		100	200	2311 08	2326.25
(max.el) as	- N	₩ 8	2:00 PM	MA 00.	# S	1.15 AM	2			8	3	30.	11 05 /44	M oc i	M 00	2	1		1	78	8	MA. 05.	1 R	# 8 #	# 8 ·	7 X M	* 8	- 30 AM	28.2	3	2			800	30 AM	2	30.48	2 8	7.30 AM	*** an a	7	8	30 44	8	7	1 10 AM	MA 05.		1	100		ł i	e e	3	3 8	1 8 Ai	2-00 PM	38	100	W 95.		2	18 AL	28	- M
	-+~	_			_			_				_			_		_					_	_	_					_	_		-		_		_	—		_			_		_	_	_	_				_	_				_			_				_	_	_
-		06.7 600119.000	CASSET SEE	OK:/ BRETSTA	84.10/1980 S.48	Section 18	ALTONOMIST 17-44		DE LA COLLEGE	OE/1/1/200 12:30	BET ST PER	DE-S MINISTER 9-30	66/13/1888 11:08	OE:81 996 NE 18:30	06/13/1988 7:30	-			20 - CONTACTOR	00:11 000 IV-00	DENAMED		04:11 00FT-24:00	967/9/36	DECEMBER 13:40	#41771988 7.30	06/17/1990 D:50	96177190	06/17/1980 12:30	35.7 660 rainage	ACT 19.20				05:11 686 1/81/80		B6/28/1989 7:30	DE:21 989 13:30	96/21/11/950 7:30	09-01 (BM) 12-00	OC:11 0001/12/00	09-E1 000 13-00	06/22/1999 7:39	D-11 988 11-55		00-11 manual 11-30	00:11					N::/ 0441/32/00	00:21	OK:/ 888/JPM/80	M. 4 888 1/82/84	81:11 G981/85/89	DE/MET 998 14:40	ME:T 000 T.S.	CAL CALLETTE 13:30	- CHICARO			06/74/14/14/00 11:40	OE/20/1000 13:30	
•		\$	-	Men 6/10/8	Man Scione	- From			5	15.5	West Int Driet	West Syl 2/88	West 5/12/86	Wed 6/12/88	#X54				8551	ra in 678	#4 £3 £4	5	5 3	87154 ung	# 5 CM	\$84.2 Life washing	Man British	Man 647786	Man Avi 7/44	The System						West Scribble	The S/2000	The Contra	Fri 6/21/78	Fri farms	£4 6/21/20	Frt 6/21/80	2	1								14- 6/20/8		West States	West 678078	Wall States		The Sept And	The BITTH	Tot some		F-1 5-2	Fri G78/80	Pri cyange	Sher Scribbins
passagene																																																																	

Page 5 of 13

	_			_		_			_							_		_	_		_	_	_	_		_	_	_		_				_		_		_	_		_		_		_		-	_			_		_	_	
																																																							ngarli sursi
Man 421/19						F1 2712	r see	Fields	Thu de 200	7 277								Mon 6/14/M	Hon 674/80	# 14 T	Sun 6/12/00	San 6730	36.012.00	Feldriche	Fi MINING	F# 4/11/00	Thu eriotes	17W 6-10-96	1		W-10-10-10-10-10-10-10-10-10-10-10-10-10-	114 4478	Tue degree	Man arrive	Man 6/7/704		Sum 64-96	Sup adjust	Fri BUATE	F-1 04-70	Fri second		Water Profes	Wed 9/2/70	Wed 672	W-4 0/2/90		Total Bridge	Most 62 1/10	Men 621/80	Hon 6/21/90	Sun 67098	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		•
96/21/1986 7:16	04/36/1 mm 11:04			-	08/18/1940 12:46	0478788 11:45	OE 10 000 LAUNO	08/10/1000 7:30	1,16	04/1771mm 7:15	10.10	06/16/16/06/16/06	04.4 046.40.40	7.30	OC.C. 8861/51/80	OB/15/1999 7:15	04/14/1B00 1:15	06/14/1988 11:00	06/14/1908 0-30	06/14/1999 7:30	00/11/00011/00	06:9 4881/6:100		ON 1/1999 12:36	05/11/1000 0.45	08/11/1988 7:30	06/10/1980 12:15	06/10/1999 7:30	OR.C. 0461-40780		0505/1998/1000	08/08/1998 13:00	04/04/1990 7:30	04/07/1988 13:38	04/07/1898 11:30	000771900 t. 30	CHARGE 11:30	06.7 B66.270070	06/04/1988 13:08	05/04/1000 5:45	06:7 888174980	OC. 1 MARIA (1900)	04.02/1990 13:30	08/02/1898 11:20	06/02/1998 8:30	06/02/1986 7:30	06/01/1900 12:30	GEOTIFICA 7 30	\$1:11 8661/15/90	06/21/1840 9:30	06/31/1968 7:30	06/30/1898 11:90	06/20/1998 7:00	De la	44
7.30 AM	8			i	1245 PM	1 6 A	- A	730 A	Ē	715 &	2	8	20 6	730.4	150 PM	7:5 🕊	115 1	11 00 44	8	7 30 44	8	20.4	10 10 14	12 36 PM	8 45 AM	7 30 4	1 15 00	7 30 4	1 30 PM		730.44	8	730.4	1 30 7	11 30 Æ	e de la	31,7	730 4	1 00 PM	8 45 AE	7 % E	3 2	3 2 2	11 20 AM	8 30 A	7 30 👫	12 30 00	7 20 2	11.5 A	3 30 AM	7 30 A	: 8 A	788	,	ne (hrmin)
2000				_	20.03	_	2011.00			_	278					_				_	_	_			Ž		_	2817 08	_	_	2500025	_	2589 08		2549.08			2521 08		_	2473 08				_	_		_	2300 83	_			236258	†	me (hre)
574		_		-	3			_	<u>.</u>		-			_		_	_			_			81807			_		81311		-			8084.	_		_		_			—	78.7	_	7944.0	_			78215	_		_	_	78740	+	our Make Reading
1 3866	0 135882	_			_	_	7 1346114	-			_			0 1329341 0			_			_				12		_		_		_	4 1277151	_	_				12530	_		_		122143		_	_			5 1203879					0 1179017 5		prysode Tatelizer ending (yel)
270	\$.1 28.0	70.0	17	_	250	27.0	78.0	-	250	۵.	2	0	270	280	78.0	•	÷	20 280	240		160	230	_	27 270	_	280	270	-	280	240		240	280	•	-		270	78 280	<u> </u>	13 27.0	-	• •	270		-	-	•	280	280				210	7	ned Florrate (gpm)
*	ĸ	8 :	E :		3.55	ĸ	315	2	ĸ			_		8	×	_			315	_	_	K :	_			-	#	_		-	_			_	_			_		31		_	_		_				-				-	+	ang ZW (dagraas C
_		_			_		_		_	_			_			_			_				_	_			_		_			_	_				_	_					_					_		_	_		_	+	ir ZW (offer)
910	8	8	*	8	80	8	80	800	8	9.0	\$	ž.	8	80	S.	£	S	58 0	S	570	ž.	ž.	570	¥ ¥	: :	E	570	*	ķ	8	* 5	_	S	ž.	ř	\$60	S 5			\$7.0	57 0	ž į	2 8		*	£	ž	x	S 1	570	570	¥.	8 1	5	upplemental Air (ct
<u>.</u>	ĸ	5	-	r	5	*	×	ĸ			5	s	8	.	ĸ		±			•			£ :			£	•	•	±	•				•	•						*	8	. t	-		ŧ	4	± :				\$	ĸ:		teenan Recirculations (gpm)
9.5	5	<u>۔</u>	.	:	6.5	2	:	•	5	•	•	6	:		8.5	0.5		6.5		•	9		•		: :	6.5	8.5	:	5		\$ 1	: :	: :		6.	•			: :		3,	:	. :	: :	: 5	8 5	•	.	6 6					1	armesto Rata befor P (SPM)
•	*	ž	7	76	620	9,0	5	š	5	5.30	5	28	5 70	8	5.20	4.20	380	4 20	\$	*	120	4 20	2	2 3	3 3	3 90	3 80	4 70	ĕ	370		1 2	3 70	3 70	370	3.70	8		3 2	ž	370	35	5 5	3 70	3 70	3 70	3.70	Š	8 3	- 3 76	3 70	2 70	28	32 4	'astrum before RP (i
-	2	=	<u>.</u>	:	37	37	3	3	37	3 .	3.7	:	37	3.	3,7	37	3.7	-	3,7	3.	·		·	<u>.</u>			30	37	:	¥.	3 .		: :	36	37	37	9	: :		37	36	3	2 6	3 3		3	3 E	3.6			3	36		3.	IP Pressure (pal)
130	ē	20	13.0	ē	ũ	130	130	13.0	ē	130	130	130	130	130	130	130	130	130	130	130	110	130	130	12 12			130	130	130	130	ĵ.	: :		130	130	ű	130		130	130	130	ī 30	ř	130	1	130	130	130	13 6		130	130	13 0	120	IP fees in CIP Tank Litery)
:	:	:	:	:		:	:	:	:	:	:	•	6.5	65	- 65	65	:	:	:	;	•	:	:	: :	: :	: :	:	•		:	:	. :	: :	:		8.5	.	. :	: :	:		B 55	:			•	*	6.5			: :	6.5	:	:	Paryment Plate sitter II gpm)
	\$2	:	:	:	4.2	37	:	:	:	:	97	12		*2	::	11	::	¥	3	717	-	¥	2	<u>.</u>	۲:	: :	: :	•	5	:	2	= ;	32	3.2	3.	37	37	. :	2 2	32	ï	3.	32	2 5	: :	3.	3.7	37	¥ :	: :	: :	32	=	۲,	/assume after SP (in
5 8	<u>;</u>	š 8	15.88 15.88	 8	50	8	15.08	15 00	<u>.</u>	<u>.</u>	ž	15 00	8	15.00	58	- is 08	ĭ. 8	15 00	8	15.00	15.88	8	15 00	<u>.</u>	ŭ				3 8	Ē 8	58	ē :	3 8	8	58	15.08	<u>:</u> 8	F 8	 8 8	: 8	15 00	8	š 8	i		. i	15.00	š 8	š 8	5 8		58	3.8	15 00	ar Duration (sec)
ē	ő	ē	ő	 6	ā	á	- -	ã	ő	ō	ē	ŏ	<u>-</u>	5	5	ő	ã	ő	. 5	ĕ	ä	ō	ő	5	ō ;	5 a	. 6	- ē	ŏ	ŝ	ő		5 8		ő	õ	ő	- i	- 5 6	. 6	ā	õ	õ	5 ē	. ē		ŏ	ő	ŏ	- i	5 5	ã	5	ő	SP Frequency (min)
							Character Later			_			mani chareng		_	_			mart clearing			_				į					mane channing	_				mand channing					mand cleaning				and comment		buttom poeti raas				The Charles				Comments
		3	š	ž	: ;		: :		ŝ	ě	ě	*	2 85	275	255		í	3 8	 : =	-	ě	2 8	ê	į	í,				177	ě	1.87		ē i	É	Ē	É	13	Ē	7 7	1 2	í	172	172	ā	Ē.	ž	8	177	7.7	ř	ē	ž	ž	1 57	TOUP (p-all)
9	8	90	515	\$ 15	: :	: 6	2	: :	ş	ž	7:9	7 16	÷	8	ž		:			907	907	* 07	9.77	10 02	i 2	10.79			ě	2	10 PZ	5	70 29	5 5 8 2	0 2	10.29	10 52	10.28	ŏ 5			10 2	ě	Ē	6	5 5	10.20	ê	ĕ	52	628		15.24	: 8	Permentiny (glasp
3 3/	5 12	i	ż		;	: :	: 1		907		2	9	\$ 73		2	3	ř	: 1	ř	: 3	Ě	ě	6.27	8	2	Ē				9.77	i	:	. 72		. 72	2	8	:			: :	922	847	ż		2 2	8 72	8.46	8 75	. 73	72	2 5	13.53	ě	rarmanilly Corre for Femperature (Streets (glidjen)
-	: :	•			9	;	9 1			. 5		57	57				5 3	5	57 5	9 5				•	571	-			9 5	===	571	571	5				571	5 71	2	•	5 5	571	571	571	• • • • • • • • • • • • • • • • • • •	57 2	: ;	571	571	57:	577		571	5.71	PERT (Serv.)

Table C-1 ZeroGem Operating Data

						_								_						_														_												_						_			_			park vont
Man 7/	•				F # 77000	_	Z 2				7		****	W-ad 7/7/84	Wast 7	T to 7740	Tue Zieura			_		Sun Flore	Sun 714.	E-0 773/00	S-01771MB	Fei 27	Feiz	F-1 7/2/10	7hm 2/1/4	The 271/80	Wal short	March Inch	The same			***	-	f	Man 6/23/70	- F	Sum 0.027/80	\$4.4C9 PS		7107200	F-1 0/26-00	Fri e/25/70	7	7	Media Prin	Ward 6/23/9	WEL 9/23/1	Med 6/27/9	Tue 6/22/18	-	Eon e	Mar 4471/4	-	
Ĩ	Ī		•	•	i 	! _	ŧ	•	-		•	1	7	77	7.8	.	-			 -		§	ş	·	í	-	i	Ĭ	ì	} _	Ĭ		-			-	- C	SQL/M	2	7	27/1		-		•	1	ŧ	524	7	2				1	1	21.		
G771 BF8 7:30	97/1 V7888 11:80	6271 L/1000 K:30	67/ph/1000 10:46	#279#19## 4:16	80:E1 6801/86/20	07/Am/1988 9:16	47/86/1988 7:38	07/06/1000 15:00	17/80/1900 12:30	07/08/11 MB 11:00	97/04/1 990 7:30	07/07/1000 13:30	07/07/1988 11:00	97/97/1988 8:45	DE:2 0461/28/20	07/88/1980 00	00:1 000 100//0	0)70m (900 13.00	07-11-00 11-00 C	07/06/1998 1:00	0.2604/1848 7-64	07/04/1940 0:16	97/04/1988 1:38	97/03/1989 11:30	07/65/19 40 7:00	07/02/1998 13:00	07/00/1989 9:50	02/12 888 74D0	CD: E1 8881/19/10	07/01/1968 8:00	09/20/1000 12:00	00:11 MM1/00/30	04.707.80	06/20/1809 7.30		08:01 8661/85/80	06/28/1988 11:00	04/24/1999 1:30	OC:2 0061/82/80	98/27/1998 10:30	06/27/1980 8:00	OR-01 BBK1/3/5/90	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	04-01 041/45/NO	98/25/1989 R.36	06/26/1899 8:00	04/24/1808 11:00	08/24/1989 7.18	DP- E1 8881/CZ/30	04/23/1888 10:44	06/23/1998 B:30	06/23/1899 7:30	00:21 0001/25/00	DE-21/1808 13:16	08/21/1998 11:00	06/21/1900 0:30		•
7.30 AM	11.00 AL	30.4	10.45 AE	î È	ž	: E	730 AM	1982	ž	8	730,4	1308	11.00 4	9 45 AM	7 30 44	00		1 2	3 8	8	7 .		200	100	700 4	00 PM	\$ 50 A	7.30 44	100 PE		8	: 8	**	7 8 1		100 PM	184	8.30 AM	7.30 AM	10.30 4	8	1000			44 OC 6	8 00 AM	00 PM	7 15 Æ	00 PM	10.45	9 20 20	730	8 7	115 PM	11 00 A	3 30 AE	The	us (fur:anin)
3384 00			_		20.00		_			_		_	_		_	_				_	32 7 7 52		316	_			_		_	_		_		3087 08			_	3051 08		_			29862	_			2958 54	_	_		_				_	2883 08	+	mulative Operating
Ī	*	į	223		9602.2	9	1	1787	8781.5	_	271	17023	_	8757.2			-		17124	_	_			_	_		1637 7	_	0010.5	8813.5	_	_	8691 7				_	_	1542	1629	_	_	172	_			9 2394	-				_			_	8378 4	╁	ur Mehrer Plandling
1 1538534	1039432.7		_	_		_	-	_	_	_	_	1 1 1 1 1 1 1	3 1496312	_	_		-	_		_	_	_		_		_	_		_	5 14461712			_	_	1439725.2	_							2 14067224	_		_	_	1391140							130000		┿	mente Totaltzar ading (gal)
30			-			_	_		Ť	_	-	240	2.1 28.0	_	_			260			-		7		•			74 280	_		Ť	-	-	_	290	-		_	_~	•		<u> </u>	_	0 0	270	-	Ī	-				-				24.0	t	od Flourato (gpm)
8	z.	ĸ	=	8	3.5	8	8	ㅂ	t	315	4	32.5	31.5	•	5	5 8	<u> </u>	8	K	3.5	¥	= ;	<u> </u>	-	- t	5 5	_		_	_	22.5	z.	×	<u>.</u>	٠ .	: 5		: 13		 K	ĸ	ĸ	31	z ,	4 k	- 31.5	32.5	<u> </u>	k!	ĸ	<u>.</u>	30.5			_		+	mp ZW (dograss C)
7	2	¥	2	3	*	¥	2	2	28	2	23	3	э	2		* 1	· ·	25	3	25	_			-	_	_			_	2	25	Si.	2	25	2					-	3		24	3 S	× 1		*	25	-	_	_						╁	IW (sim)
	8	R	\$		• 10	Ŗ	8	80	8	•	20	80	80 0	610			8	200	610		•	6.0	2 :		R i	8 6	8		800	610	800	800	80	•	•		8 8			8 1.0	910	800	910	8	8 8			62 0	800	6 0 D	61.0	e e	800		8 8	•10		ppiornantal Air (cirr
•					8	8	*		g	Б	8		8	•		-	.	-	8	.	£	6	6 1	s :	8 8	s :	. 8	: 8	8	8	٤	8	8	÷	<u>.</u>					8	•	8	ĸ	K I	E 1	3 2	: 22	<u></u>	К	5	к	ĸ	 E	ıs :	r :	: 2		naptes Pastroutatio de (gpm)
:	:	• 5	8.5		:	•	£	:	:	:		4.5	8.5		: :	•	:	65	9.	•	;		:		: :	: :		: :		6.5	:	3	5	5	:			: :	, ph	8.5	85	\$	8.5	g.		: :		3		6.5	65	0.5	a.	a (. :		2	ryptata Piata before (gera)
4.20	9.20	ŝ	8	5.90		5 70	5.90	8	5.20	520	5.20	ŧ	720		: ;	7 8	8	8		6 20	700	8	8 20	8	720	3 3		:		ŝ	6	8.20		*	•	8 8	8 8			78	830	6.20	5 70	5	5 6		20	\$20	5 70	5 76	636	630	8	20	£ 8	ŝ	2.5	myum belore BP (in
7.3	:	72	72	7	7.2	73	23	Z	7.2	7.	2	7,	73	: 2	: :	73	7.3	73	7	-	:	72	72	7.2	70	7 :	: ;	: :	: :	77	70	71	õ	7.	;	7 7	7 :	: :	: :	\$:	:	:	:	70	7 4	70	2	3	2	:	30	3	3	= :	3	: •	Pressure (pol)
18.0	Ē	ě	180	100	20	:	:	i	18.0	•	ë	160		: :			.	•		18.0	5	í	100	•	:		; ;			÷	•	•	į	100						ě	14.0	100	ř	10	÷ ;		: 0	130	13.0	30	130	130	130	130	130	3 3	-	Inco in CSP Tank Bers)
:	:	:	:	:	:	•;	•;	:	:	:	=	8.7		: :		<u> </u>	6,7	6.7	•	:	:	:	:	•	:	•	: ;	3 ;	: :		:	70	:	:	:	•	•	7 8	: :			6.5	9.5		\$: :		8	5.5	8.5	85	3	65		: :		provident Plate after BF pm)
:	:	:	52	-	2	42	47	12	•2	4.2	42	50	:			:	52	5.2	:	\$	54	5	:	=	•			: :	5 ;	: :	:	ů	:	:	:	4.7	;	:	; ;	. 2	. 5	:	ŧ.	<u>:</u>	:	\$ 3	; ;	: \$:		:	;	•	•	12	: :		souven after BP (In B)
8	8	8	3.8	8	<u>.</u>	168	8	8	15 88	15 00	8	8		3 8	Š	5 8	15.8	15 00	ī. 80	8	16 8	5 98	8	8	ŝ	168	8	8	B I	8 8	8	15 00	8	<u>.</u>	500	8	8	8	8 8	8	8	8	<u>8</u>	15 08	<u>\$</u>	8	8 8	5 8	5 08	8	8	8	5 8	š 8	500	8 8		P Duration (eac)
3		ĕ	=	ő	5	6	5	5	ä	5	6			ā i	ő	ē	ō	ő	5	5	ē	ă	6	ة 	ē	6	• ·	6	i		5	ō	ē	ě	õ	õ	ő	ő i	ő ;	5 6	;	ĕ	ē	ĕ	ē	ē :	ē	5 6	6	5	ō	8	ā	ő	6	ē ē	•	P Frequency (min)
						700000								į	THAT CHANG					_	Water command	change OUR procedure (prest data received)							OWAL CHARGO				ment channed						mart caseren				-					70		mars diseasong						ļ	man design	o granda
			i			i		1		2.56			:	ř	1	2	338	ž	308	3 08	ž	1	306	326	ĭ	ž	9	32	ž	2		8		:	ï	8	ě	38	ě	ğ 1	ž 8	305	2 16	2 70	28	š	8	ž 8		2 80	8	8	305	ğ	8	3	30	110° (pol)
-			: 1	: :	: ;	; ;			ì	i	i i	i	ż	5 29	:	Ř	3.52	23.5	8	:	*	ī	:	552	5.28	529	:	577	ž	\$77		:		3	3 2 5	ř	:	:	8	: ;	ž 8	:	î	:		i	È	: :	: :		8	8	:	:	:	657	8 08	مر فای) رکشست
				: ;	î i	;		; ;				¥	8	ż	ž	4 23		*	512	527	î	4 72	5.27	4 2	į	4 70	:	î	3	:					5	2	5 6	4 20	5 12	ž	•		8	8	5 6	:	5 73	<u>.</u> :	ŝ	i	\$24	531	520	2	547	É	2	Permanistry Corrector for Temperature Essents (glidipel)
	<u>.</u>	9 9	9 :	5 5	5	;	5	5	;		•	5	5	571	571	571	571	37	57	571			5	571	•	571	571	=	\$ 71	5	57	: :	: :	: 3	571	571	\$ 71	57:	\$ 71	57	5 .	, ,		6.71	\$ 7	57	573	571		5 2	\$ 27	. 57	571	\$71	571	571	671	eri (m)
						 •	<u>.</u>	.				<u>.</u>	- :	•	:		-		-			_	•	•	i	i	•	8	:	•	<u>.</u>		8 9			=	=	3	Ī	•	ŧ.			ž	ž	- -	187	Ę					; ;	•	•	•	10,7	Fluis (grid) (Adear (GP)

	_		_		_	_	_		_	_				_		_						_		_	_			_	_			_	_	_	_	_	_		_			_	_				_			_	_	_		_	_	_	_	_	_	_	_	_		_	_					
																																																																			E ta	pa/Eva	e rt	
	7	-	-			- -	-	147.141		F# 7724				-	T-12.22	1017 Mail			_	_ *13	Wall 772	# 7/2			1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	T = 1/2	E 72	\$ 7a	3um 7/2					FA 721	Thu 702	72.72	# out 772	Wed 7/2	**** 772	***			7-70		Man 7/1	777	- II.	•	Sugar 7/1	E 70:	24 7/13	F# 7/14	F4 771		F# 774		-			W-277	West 7/1	1	1 27	88mn 7/1	Mon 7/1	Hon 7/1				
		1	1	ì	<u>:</u>	•	2	ì	•	*	3	1		! 	ŧ	į	1	i I	I :	!	•	•	1	i i	ì	i	ì	ŧ	Ī	ŧ	ì	i i	1	•	•	į	ş	*	ì	1	i i		ĺ	1	!	i	i	•	į	Ĩ	ż	ş		3	•	1	1	i	•	•	i	i	Ĭ	ž	ž	ŧ	L			
	0409/1999 13:09	00-07 800 70000	THE PERSON NAMED IN			08-11-08-11-08	60% Z 688 L/1948	87/31/1 988 10:30	82/21/1980 8-88	67/7m/1888 13:30	07/20/1300 11:00	SECTION NAMED IN		07/20/19 00 7:20	07/29/1000 14:00	07/20/1999 11:30	OC.2 000 (A22/70		05.7 988 LAGSE	07/26/1988 14:25	97/29/1998 11:30	07/24/1 686 1:30	ANC 1 444 1/873/10		97/27/1964 14:30	07/27/1998 4:00	07726/1988 7:30	OX:E1 886 19570	07/25/1980 7:30	07/26/1998 13:500			07/20/14:10	00:8 MBS1/52/20	07/22/1800 11:40	07/22/1980 4:15	07/21/1980 15:20	97/21/1909 11:30	07/21/1999 9:30	20.20			070071998 10-00	07/18/1996 14:00	97/18/1899 11:00	07/19/1990 B:30	07/19/1990 7:30	67/14/1980 10:30	07/18/1888 6:30	07/13/1900 0:30	07/17/1900 6:18	07/19/1986 13:00	07/18/1986 11:00	07/19/1998 8.30	07/10/10/07	DO: 1 040 USU10		7.5	07/16/1986 13:26	07/14/1990 7:30	07/14/1986 6:00	07/13/1999 13:09	07/13/1980 7:30	97/12/1998 13:00	97/12/1966 11:00	07/12/1888 9:30	-	•		
	715.4	10-45 /46	2		8	18 E	700	10:30 A	1.00 AM	1,30 PM	60.00			730	8	1304	2		7 30 4	2 20 PM	11304	9 30 AM			2 30 7	4004	7 30 AM	- 30 PM	7 30 44	9	1		200	B 00 A	11 40 AM	W 513	3 20 PM	13 30 AL	9 30 44			100	8	8	: 8 £	930	7 30 444	10 30 44	6 30 AM	9 30 4	6.15 AM	100 PM	8 4		20.00			3	125 PM	7364	8	00 PM	7 30 AM	1 00 PM	17 00 44	8 30 AM	-	m (By:	min)	
			_		_				_	_			_	_					_	_				_	_	_			_	_	-	_		_	_				_			_	_		_			_					_		_					_			_	_	_	_				
	9387		-	_	_	_		_	_	_	_			_	_		_		_	9251 1	_		_				_	_	_	_	_	_	_	_			_	_	_	_		_					_	_			_	_	_		_							_		-			,			ding
	177063				17170	170627	Ž	18008	18807	1			_	_	_	167944		1	14780	167194	187098	1876/1		_				194692	1		_	_	1002	142742	1000	161077	18133	181210						_		_				-	_				Ī		_				_		_	-	-	_			Totali	
	_				_	_				_			-	_					_					_					_	_	_		Ť	<u> </u>	-	Ť					_	_	-				-	_			_							_		_	=	-		_	_			ed Flor		 8P/R)
A PRIMARY OF THE PRIM				_	_		-			_	_			_	-				_				_	_		_		- +	_	_	_	_		_		_	_	_				_				_	_		_		_				_		_		_		-		_			_				
Approximate Angelon			, ,			_	_	_		_	_			_			_		_		_	_			~	2	_,			_			~		~	5	~	- 2	_	, ,						-								_			_		~			~			_		+			_
A D D D D D D D D D D D D D D D D D D D				-	- -	_	_	_	_	_	_	_	_	-		_	_		_	_	_			_	-				_		_	_	•	<u> </u>	-		•		_	_		_	<u>.</u>	_			_		-	•	_					-	•	۰ -		P:	<u>.</u>	*		_	_		ľ		 ,	
Transfer Service Company Compan		-	_	-	<u>-</u>	-	=	-	-	-	_	-	5	_					_			_		_		8		00	_	-	-	-	8	-		20	6			_		-	-	-			~		~	-	-		_	-	-		-	20	5	~ 	20	-	30	-				——		
## Company Matrix (Party Company Compa		-	_	-	-	_	*	-	-	_	_	-	-	_	*	8	-	e -	_ _	_	_	: 1		* -	N .	K		-	_	-	•	=	8	_	_	•,	-	-		_	* —	•	-	-	-	*			1	-		_		_			_	<u> </u>	-	-	-	*	-	-	-	*	[lo (gp	m)	
## Present (pri)	: :	-		-	5	=	5				-		5.	5	:			5	•	-5				: _	5	:	_	5			<u>,</u>		:	•	5	2.0			-	-	•	2			\$	•	-	5	-	65	- 5		: :	. :	-	-			5	6.5	5	6,0	*		- 5	5	5	(gpm))	
## Plants of CP Tank Plants of CP Tank	20	3 3	3	3	72	ž	76	70	- 70		-	16	8	710	200	è		70	š	576	. ē	<u> </u>	1	ž	20	8		8			Š.	20	820	20	20	36	ž	ž	: :	8	8	8	ð	570	5 70	5	8	820	8	620	8	2	* 6	70	8	20	ŝ	8	8	58	8	70	5 70	8	5	820	**	*	betors	BP (4
Lamber of the control	-	7	:	35	7	2	3	7.3	ì	: ;	3	:	-	7	71	-	:	õ	7 2	72	-	: :	3	72	72	7.2		73		,	3	3	2	ž	7.2	73	è	: à	; :	71	7	7	70	70	73	72	7.	73	73	72	73		7 .	3 7	: ;	2 :	73	73	7.2	72	7,3	72	7.3	73	- 2	73	-	Praes	нато (ре	e ()
Temporary (min) Tempor	5			=	:	1		1	į	: :	:	•	i	•	ě		•	5	ě	•	; ;	; ;	•	:	5	•		ě	:	•	•	•	•	•	ě	5	ě		; ;	:	5	•	•	ě		:	•	•	•	•		: :				ě	ē	•	:	•	180	•	•	•	ě	•	a c	loss (in CIP 1	Tank
## Frequency (min) **Prequency	:	:	:	=	:	:	:	:	: :	: :	:	5	Ş	:	:	: ;	,	:	:	:	: :		70	?	8.5	:		5	: :	•	:	:	=	:	•	0,	:	: :	: :	:	:	:	•	2	ŧ	•	:	2	•		:	: :		70	:	2	:	-	8	•	:	6.7	•	:				peri)	Plate of	A., I
## Frequency (min) **Prequency	5.7	=	=	5	:	57	:	: :	: :	: :	=	٤	=	7.2	:	: ;	70	2	:	•	: :	<u>:</u> :	•,	=	:	:			: :	5.7	5.7	70	57	s, _	57	۲		: :	: :	:	:	2	62	5.3	52	53	55	57		: :	: .	; ;	5 0	5 2	: -	5.5	5.5	53	52	:	5.2	51	:	*	: :	: :		p)	after B	MP (In
The state of the s	<u>.</u>	Ē	ž	5	15 08	58	58	8		3	Ē	8	15.00	3	600		ś	<u>15</u>	8	8	; ;	8	8	15 08	5 86	8		8	3	8	8	8	<u>15</u>	3 00	15 00	ě			8	8	38	8	15 00	15.00	15 00	15 00	8	1500	8	8	8	3 1	8	8	5 8	5 8	500	3 80	ī 5 08	8	15 00	15 00	8	8	ě	8	-	r Oure	ilon (or	ec)
Tum (pul) Tum (pul)	š	ā	ĕ	ō	ő	ä	ž			5	5	ĕ	ē	ē	ā		Б	ō	ő	ā	5 ;	ő	5	5	6	ă		ě	5	ō	ē	ő	ě	ă	6	ā	; ;	5 6	5	ē	ō	ä	6	ő	5	ě		5	ā	ē	- ;	5 ;	õ	á	ă	õ	ŏ	ã	ā	ă	ő	ő	á	ē		a	•	P Fraq	namency ((min)
######################################				mant deaming									ment cleaning						_			тъви севите																	_		mart cleaning					President and a									ment chapmeng						mant clearing								esta	
United States and the states of the states o	208	ĕ	324	ï	ř	ž	: ;	ž	ž	320	ï	ž	1	ě	: 5	ř	Ĕ	27	ĭ	;	š	324	37	ĕ	ê	=	:		ĭ	320	*	š	305	2		i :	8	<u>.</u>	<u>.</u>	3 83	è	329	31	2	,		 3 8	3 5	2		g.	2	8	28	ž	365	365	200	2 8 5	ž	298	2	į	:	375	8	Į,	- (-	a l)	_
	:	:	5.77	5	52	: :	:	*	*	•	Ē	2	1		ì	Ş	š			; ;	2	577	ż	î	8		-	•	i	š	8	:	:	:	: ;	:	8	ž	ž	4.78	ŝ	5 66	3		: 8	:					:	657	į	ŝ	•	:	:	6 35	457	ŝ	8		: 1	:	8	•			dellity (I	glery
	123	520	i	i	ŧ		2	Ė	È	Ė	:	÷		:		-	:	÷	÷	-	- *	417	è	•	ž	: ;	-		ŝ	ŧ	•	5	2	: :	: ;	5	<u>.</u>	÷	ì	ŧ	•	Ē	ş	ĭ	: ;	î :			£ :	5 97	5.27	-	ŝ	\$		î,	520	ŝ	2	8	8	: :	;	<u>.</u>	Ē		ž	orman as Toss	ndiny C specials (grid)s	
\$	_		_		_	_	_	_		-		_	_	_		_	_	_	_	_	_		_	_	_	_	_		-	•	_	_	_				<u> </u>	_		_		_							-		-	_	_		_			_	-		_						┪	_		
	* 7	5	3	5			9	=	-	9	:	5.71		:	:	-	3	574		7	2	=	5	3	: 3	: :	=		=	2	2	-	- 2	: :	2 :	2	2	3	3	3	2	2	2	: :	:	ŝ		7	7	7	3	=	\$ 71	7	7	7.	3	2	2	2				3	2	2	9 J	att ibr	10)	

Table C-1 ZenoGem Operating Data

(All talks) (All talks)	::		-		-	•	-			-	, ,	_	•			_		-			•	•	:	_						•	<u>-</u>		• •	. •	-			-	_	•	•				_	_	~	:			•	_
74	-		-	-	-	=	<u>.</u>	-	-		-	_	_	_	-	_		-		_	-	_			_		_		_			_	_	_					_	_		_			_				_	-	-	
(ant) Title		- 1	.7.8	\$.71	-5	5 71	5.7	-2	- 2			5.7	5.73	\$	5.7			. :	_		5.75	5.71	5.7	ž.	•			¥.	Ě	5.7	571	5 5	5 5	- 5	5.2	Ē		*		5.7	*	8 :		5 5		• 15	7 12	5.7		-		- 57
Portematility Corrected for Temperature Effects (glidtyes)	\$ 12		\$ 20	95 5	5.67	\$ 28	\$	Ä,	8 :	2 8	3	. 29	5 27	8	\$	ž	S 5	ž :	5 5	2 5	\$15	5 17	5 12	3 75	# :	2 78	: 3	283	2 88	4 29	4 10	= :	2 :	. 6	=	3 03	3 :	257	3.24	3.18	ğ	2	25.	25.	· 4	2 Z	233	3.24	567	8 8	ä	3 28
(mdpp) (Approximated	8	8 2	-	2	\$	97.9	-	\$		3 5	7 :	1	:	3	2	2	3	2	. :	8	ī	+2+	8	ş	1	R :	,	33,	324	4 95	4 95	22	\$;		Š	ž	4.65	200	373	377	ž	381	ō ;	8 2	. 8	97	2 12	E	9	9 5	, r	0,4
(ped)	8		908	98.7	2	2 80	8	8.	8	2 20	2 2	8 2	8	8	8	9 2	2.30	8	8 3	8 8		300	8	2	8	2		2	ž	3.78	3 73	3.83	8 :		7	7.47	8		\$ 61	8	5,	2	ò	: :	. 2	\$:	50	•	: :	: 5	8
Commence		Company Constitution							maeri clasimi						med charact									MAN OO B Grown & B OO AAA		educe bandpressure to 3 6 and 3.9	Company Company								ment cleaving	ercrease to 9 6 gpm at 10 AM		The same state of the same of		Constant Character	Marcales to A 5 gam at 6 PM			Accompted to 0.5 gram at 0.4M	Dayler Line	encreases to A 5 gom at 6 PM			-			maint channe
Et Frequency (min)	9	2 9	? =	5	5	2	0	ō	6	2	0	9 9	9	ç	9	9	ō	9	5	٠ :	2 5	2	9	ē	9	5	2 :	2 5	2 2	ō	ç	9	9	2 5	2 2	9	ō	2 5	5 5	5	9	ă	9	P :	2 9	2 9	2	9	?	2 :	2 9	2
Bl. Drubblos (sec)	8.21	8 8		8	80 51	8 5	8	8	8	8	8	8 8	8	8	8	8	5.00	8	8	8 5	8 8	8 8	8	8	8	8	8 1	8 8	8 8	8	8	90 \$1	8	8 8	8 8	65 20	8	8 8	8 8	15 00	8	8	9	8 1	8 5	8	8.5	8	15.00	8	8 8	8 8
of) the water grands by	3		: :	1 2	5.7	5.7	53	5.7	2.5	5.7	\$2			25	\$2	-	Ç	:	2.5	2,	. :	2,	\$8	12.2	6.6	:	: :	:	7.5	7	22	:	7.5	2 :	7 5	16.2	11	•		9.2	12.7	?	£ 4	1,1	:	18.7	17.7	46	:	2	2 :	::
Till safer flate after 85 (m46)	3	<u>.</u>	: :	=	4	29	6.7	:	:	:	è	: :				ç		8	•	: :		; ;	:	•		5:		2 ;	: :		:	÷	:	· ·	: ;	011	•	: :	: :		001	001	:	:	ş ;	:	505	:	9 8	ç,	ş ;	: 5
Annot 460 at seed 46 (credit)	9	2			•	9	0.	9	9	÷	9	0 0		•	0 11	0.	18.0	0	0	9	-		0	0	° E		130	120	9 00	130	130	13.0	110	30		9	30	30	0 0		130	30	130	130		0 0	130	0.61	951	13.0	0 0	
(led) grammer (led)	:	7.5		: :	:	1,	7.			:	7.	. :		7.3	7.3	-	7.3		7.3	73		: :					•		: ;	:	;	;	;	; ;		Ļ	•	Ļ:	-	: :	•	4.7	:	:	:	0, 1	:	:	;	:	•	 : :
(fig.	3	9		3 5	8	8	2 80	8	620	5 70	2.50	2.5		5.5	5 70	5.70	5.	•	2	2	e :	2 9	8	2 2	8 9	6 M	61.	8	2 2	7.70	5	2	\$20	6 :	8 =	85	g.	R	R R	01 01	5 6	2	3	8	8 :	R 8	2	10.20	8 9	05.01	8 1	 8 8
method sales between principal and principal	:	:	-	: :		- 50	• •	5	5		6.5	::		: :	5	- •	5	÷	·-	5 2	:			:		*	2	•	: :		5 9	5	\$ 0	\$. ·	\$	÷	50		: :	•		\$	- -	÷	v 5	: :	: :	·		¥.	
(mag) etc.	,	8				58	8		•	7	ţ.	5 !			3	;			7	3	7		-	2	•	•	7	7			*		•					*		; *				;	*	; ;		-	,		7	. ;
(clin) the infrarestration	ŝ	0.2		8 5		0 05	0.10	019	019	0 85	0.0	9		 8	0.00	ŝ	620	020	•	42.0	- 2		- 029	020			0 23	5	8 8	2 2	9		0.00	3	9 5	0 02	ş	62.0	8 :		8	- \$	0 29	200	÷	3 3	-	, S	629	0.29	0.19	
(mgo) MZ at	2 2	ĸ		 C :		: 2	15	×	52	52	- 52	23	s :	: 18	×	- 52	25	2	52	£	52	* *			52	×	25	z	* *	- ×	2 3	× ×	52	£	2 2	: x	*	28	x ;				*	2	23	* *		- x	- %	×	ĸ	e :
(5 annulling) <u>M2</u> days	1 22	500	- 5	P :	2 5		-	<u> </u>	g	=	я я	B.	Ř :		22	ន	a	=	a	Ę	\$ FE	7 7	- P	1 8	5.2	я я		3.5	32.4	 q		, k	5 22	311.5	- F	R	- 8		\$ 25	, £	32.5	B	- se	s a	- -	PF 1	- F	3 8	*	អ	Ŋ	8 8
(megg) mintwelf bee			-				0	- 05	•	-	001	D 22			ž	_ 	27.0			200	2	27.0		280				0.20				- 0	- 0.0	- 0.42	•	-	- 62	300				- 0.2	° R	27.0		° .				*	ê	
verliefe Tabority (leg) gelling	1								280	9 201.	2104	38204												7 1.7	0.001	8 290	1 (380)	0.00	100	C BOOK		2048	21815	1,50	2 9000		2 954	1238815.2	5		919	7 8620	2428	0000	-			\$ 700	198	2 1000		1882342 0
Scales and the	1	271	_						174	_		5 2340	_		95282	_		_	_			_			174	_		2.2				0 2996		_						0.770	_			_		_		3	_	_		2 2000
(toug) see	+	_		_	_		2000		—				_			_		_		410454	_		_	2 2 2 2	_	_		_	9 35.7	_	-	_		_		1 500	_	4249 58 8	_	22.5	_			-	_	_	-	200	_	_	-	80 S953
Superiod or superior	╀	_		_	_		_		_	_		_	_		_	_		_		_		_	_		_	_		_	_	_		_		_			_		_					_	_					_	_	
(mintrof) 4mm	<u>ة</u> ي	700 AM	4.30	11.15 AM	8	2 2	1 00	. 30 AM	11 00 43	1 00 1	7.30 AM	11-30 AM	78V	1		8	8	, is	2 20 7	7 00 AM	* 90	11 00 74	8	8 8	98 :	80	1.5 A	* 45 4	1.00	2	8	830 48	11 00 AM	38.	9 30 AM	200	8 7	# 00 W	8	100	200	100 t	7.15 AM	8	780	10 00 A	000	2		8		28.4
•	04/08/1999 12:30	64041988 7:00	00001300	######################################	0000/1888 13:88	00.7 8881/30780	Contract and T-to	M + 000	00-11-00-11-00	08-05-19-00	06/07/1989 7:30	04/07/1988 11:36	09/1869 7:00	04/04/1688 11:15		-		81-7 GBT-01-00	08-14-88E 14-80	DEPTATIONS 7:40	06/1 (11889 1:30	00/1/1999 11:00	48/11/16/40 13:50 13:50		# 11 00 LT 120	06/13/808 13:50	BIT SERVICES	DEVIZIONE BINE	00-11-00-11-00	08/13/1868 12-45	M: 0014/100	200	947 F/1988 11:40	DET STEET 7:30	6471-01-01-01-01-01-01-01-01-01-01-01-01-01	ORTHUR DESIGNATION	04177146 7 08	08-17/1000 0:50	00/17/1968 13:58	DETECTION 7:15		981818881300	21.7 441741740	09/16/1889 13/80	SELT BEST PACKED	B-01 0001-00-00	DECEMBER 19:30	A CAT BEST AND THE	2 1 2 1 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	##75 0001/4E48	# 11 CHILL. 11 CHILL	W.7. 000142740
•	20 S	Was alter	-	Mad Average	104 P#					1	Sec 67780	Bar 1779	20m 5A.ms	-				Tue eriore	Twe Bridge	Mark Bridge	Mare deline			8 2 2	1	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	-	Fri aviate	F4 513/8	Frankla	-			Mon Bridge	Men Ariente		Tue private	Tue Bri 7/88	Twe British				The Bridge	-	Fri BORNE	Fri arbains	Fi establish	a second			*****	Ban 672918
																								•		- 4	•		•	-						,	•	•	•			•	•	•			•	•				

Page 6 of 13

	_			_		_		_			_	_		_		_	_		_			_		_				_		_	_	_	_		_		_		_	_	_			_			_		_	_	_	_	_						_		_	
																																																														ngarE.veni
Two miles												24 512	Fri MTDVIII	Fri 97000	Fri artore	The 80 8					***	Tue 9/7/80	Tue 877/840	Mary Milder	******	Sicon Salara	April 1000						F4 536	Fr 173/10	F# 1734	F4 82388	Thu 8/2/88	Thu 8/2/98	Wad 0/1/20	#419 PM	West Private	Tue 9/31/98	More SCOOL	Hon score	3 m 4/2478	Sun 6/2 tribe	E-M 6/2/1/20		Fri 4/27/200	F1 877			Market Dear							Mary Day	,	26.0
08/14/1989 13:50	13:41 000179:40	11.00		7-16	-			7.00		04:30 mm (-20)	- T		00:1 0001/01/00	08/10/1988 0:35	08/10/1006 7:16	OB/08/1 800 12:48		200071800 7:16	ON/IN/1980 12:45	04:01:000 n:46	00/00/1808 7:16	QQ:E1 8481/7040	OMET/1888 7:48	08/08/1998 13:08	00:00 TO:00	0000110000	Carrel 1980		00-01		00:00 10:00	00:7 6641/pg/gp	08/02/1894 12:44	00:11 646 (429/80	06.4 8841/UMp0	00:0 0001/1000	03:07 1991 13:00	DB-00/1848 7:30	00:t1 0061/1000	06:11 0661/1980	00:11 6881/1940	06:7 8887(0)80	06:5 BHE F(60/40)	04/20/1488 7:00	OE:01 BEST /62/60	06:30 6000 142/40	08/26/1969 11:50	06:30	08/27/7988 13:00	DAC 277 BAR 0:44	20077717000	13:00	207207500 7:13	00/26/1000 13:00	A	DEC. 1000 1000		A		002271 000 17:500	•	ate
1502	12 & P			716	2		30.4					ž	:00 AE	835.4	7 15 AM	12 45 54		7 15 2	245	A	7 15 AM		7 40 1	1000	1000	8 30 30		Š		 8 F	10.00	78	263	11.00 4		8	8	7 30 AM	ě	1130 A	11:00 44	730.4	7.30 AM	700.44	1030 4	6 30 4	1,00		00 7		730.4	8 8	715	00			3 1	5 2	3 2		,	lano (hyriffilm)
_	47483	_				_	_				_	_	_	_				4740.33				-	_	_			_	_	4656.08	_	_	4629 08	_	_	4807 54	_	_		_	_		_		4560 58	_		_	_	1	_	_	_	1	_	_	_	_	_	_		+	unulative Operating
_	ã .	_	_	1000		-	_		_	_	_	_	102377	10000	10232				-		101852	101870		_	_		_		_	_	_	- 2000	_	10009 7	-	100673	-	10042	_	10022		-	_	_	_		_		9842.9	_	_	_	9 1		_	_		_	_	_	4	lour Motor Reading
_	2081318			_	30622775.5	_		_	_			_	2027888		20204150		-			2004749 8		_						_		_		1975351 4		_	_		_	_	ī	ž		_		1 1951462 4	_		_		P 1828342 4				_	_		1910:49				and the same	4	'ermanio Totalizar lending (pal)
_	200						_	_	_			_	-	٠	_	_	_										_	_	_	_	_	_		čn.	_	Ť				-				_							_		36 260			_		_			7	and Flowrate (Spri)
_	×		_		_	_		_	_		-	_				_				_	_	-	_			_	_		_	_								_						-	-								305				_				+	omp ZW (dograco C)
_	3	3	 34	× :	*		2	 %	3	2	×	25	25	.—. %	3		ž		- 25	28	25	25	2	. 6					8	2	23	25	3	25	25	25	25	25	35		25	_	_	3	~	25	25	25	2	25	23	 %	2	25	2	 25		25	~_ %	u	¥	hir ZW (clen)
-		•	<u>ه</u>	2	8	:	2	e e	S.	E 0	ŧ	E,	80	82.0		_	 Š	2	ę	80	ę	82 0	- 2				3	- 8	\$10	610	•	\$	e	\$	62 0		910	•	610	•:•	20		_	830	610	8	82 0	22	•	82 .0	ş	•	 &	8 2 0	 &		2	ŧ.	20	•		happersonial Air (cim
-	8	E	E	ŧ	*	•	•		*	.	•	•	=		•		.	<u>.</u>	•		2	*				: :	•	+	8	ŧ	*	*		*	•	*	•		•	*	±			47	•	±	±	٤.	4	•	4	<u>.</u>	.	•	•	*	•	<u> </u>	•	1	•	Nomes Resignistics Into (gpm)
-	:	£	5	- :	•	8		:	5	:	85	65	9	6.5	: :	-	-	0.5	•	2.5		;	: :	: :	: :	: :	•	.	:		5				8.5	0.5	6.5	9.	:	6.5	6			6.5	:	6.5	÷	6.5	5	6,5	6.5		<u>.</u>	2	05	8.5	e .	65	ŧ.	.	:	Permants Rate before MP (gpm)
-	3 90	330	Ř	38	320	3	3.60	320	ž	3	3.6	310	310	120		5	÷	3.10	310	310	3.20	9 10				3	38	3	330	3.20	320	320	320	3.20	3 70	3 80	240	2 20	1 76	1 70	1 70	_		15 00	13.70	ž	1 8	- -	5	17 28	2	=	1 7	: 8	ŝ	12 70	12 8	= 8	1170	9	87	Causum Botors BP (In
_	:	î.	:	12	÷.	į,	t	42	2	•	=	12	4.2	-	: :	:	=	:	=	12	=	:	; :	: :	;	4,	 :	ŝ	•	=	=	-	•	12	3	=	3	3	=	-				5-	50	51	:	:	:	5	:	;	:	:	5	50	•	:	:	•	•	BF Pressure (pul)
-	130	į,	100	136	ŭ	10	ä	13.0	ĩ	130	ō	130	- 140	: 5			ű	130	130	130	- 130				: :		130	:30	130	ī	130	120	ũ	ē	130	100		130	- 5	ű	130	_	_	190	130	130	٥٠	:30	130	130	13 0	130	130	10	130	130	10	:30	130	130	130	PF loca in CIP Tank (Litery)
-	:	:	:	•	:	•	:	\$:	4.7	:	:		: :	: :	•	•	• 7	•	• 7	6.7	: :	: :	: :	: :	:	:	:	:	:	:	:	:	:	:	6	•	:			: :			•	6		•	:	:	70	•	7.0	:	70	70	70	:	•	2	•	•	Perment Rate after SP (gpm)
-	3.6	35	<u>.</u>	2	32	3.3	:	:	33	:	31	32	32	: :	: :	32	32	12	=	- 1	32		: :	: :	3 1	32	ï	33	3.2	2	32	31	31	91	3.2	2.2	22	2 %		. 2				137	12.	14.2	107	10.7	107	122	127	107	8 RJ	9.7	=	127	107	•,	*	8.7	.,	Yeowan after BP (in Hg)
-	15.08	15.00	ē	š 8	15 00	58	15.00	15.00	<u>5</u> 8	<u>;</u>	15 98	5 8			Š	 8	ž.	15 00	3.0	- 5	8		8	B	i.	<u>=</u>	ī. 8	<u>1</u>	£ 08	ĩ. 8	3.08	8	8	. ş	8	8		; ;	9			:		58	15 08	ĩ. 8	ž 8	8	š 8	š 8	15 88	ŝ	ž	58	<u>15</u>	8	ĭ5 00	5 00	8	75 00	16 00	BP Duration (sec)
-	5	õ	ă	5	5	ō	ő	ā	5	ő	5	=	; a		8	ā	5	ō	ō	ĕ	iā	. ;	- E		5	ä	5	ő	ĕ	5	ő	ã	ē	- ē	ő	ő	: ē		i a	: 2	5 6	;	-	10	5	ŏ	ő	ő	ĕ	ő	ā	ě	ă	ő	ő	ŏ	ō	ő	ē	ő	5	BP Fraquency (min)
	reading between C S T 1444	reading between C S T test	reading before C S T 1set	-			react classing									granati channy					-						Guiners stress														_			put pror to ful Gen agen and ful				_	_	_	mages cleaning	_				mand classing						Comparativity
٠	ā	ē	Ē	1 57	157		1	ě	Ē	Ē	ž	; ;	Š	į.	157	177	ī.	ē	ě			=	ŕ	Ē	ž	157	72	ē	2	į	: ;	; ;	. ;	;		;	1	-	- -	-	8	 2		į	: :	727				\$	ů,	5 75	5.75	5 25	521	024	610	ř	5.75	457	.,	THE (pol)
•	2	- F	- -	- - 8	3	ā		ī	ž	ī	17.50		17 28	ž	: 8		12.29	2		3 :	3	 :	12 29	12.29	12.28	; 8	10	ž			. :	3 3		3 :				15 .		22.	22 4	22		-		, 24		į	337	3 6	203	324	3.2	3.37	359	8	302	320	326	ě	383	Permission Dy (plays
		:	10 01	10 44	_	-		100	ě	-			ě	ē	ő	967	8	10.4	_	ž :	67	10 87	10 74	10 00	ē	i 45	Ē	6				5 6		•			2	13 29	ř	ž	1	: 2		-	·	: 2		•		2 22	ř	274	ž	ž	2	8	2 65	271	ě	ž	ï	Personalisting Correct for Temperature Efficate (gridfont)
	-	: :		-			; ;	-	. 5	:	; ;	<u>.</u>	571	571	57	571	571		:	5	57	-	571	•	57	:			; ;	-	-	5	-	•	5 3	9	57	57	571	5 7	17.			_			-							- 5		571	5 7	• · ·	571			MECC (form)
	_		_			_					_			_		_	_		_			-	_		_		_	-		-	-						-	_		_	-	-					. :					. 8		. 3	20.1	. 20	=			:	:	Flux (gid) (After BP)
	_	_	_	_	_	_	_	_		_	_	_	_	_	_	_	_	_	_			_	_	_	_	_	_	_		_	_				_	_	_	_	_	_	_				_		_	_		_			_	_	_		_	_		_		L

		_		٦			_	_	_			_					_			•							_		_		_				_	_				_				_			_		_		Γ	
				ا -						-					-	•			-	-		-	7	•	, .				•	7	٠,	•		~	,	,		• •		7	•	7	7 .				7				-	per event
																																										_									L	
The 10/7/88			1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	10490 mail			340 10/3/80	Set 197/98	Sec. 10/2/8	Fr 181/80	64 ISTA	F-1 161700	The 873586	The 970/98	West Williams	# F F F F F F F F F F F F F F F F F F F			-	Ten 078478	Tue 9246	E- 82778	Ham 4/27/40	U- 17771	Man 9/27/20			10 m		Fr 8/24/98	-			BACZ-10 PP-M	WALES POR	M47A P*A	Wed will/10			Han \$2050	Mars 1/20/00	Burn 9/19/98	Sup 2124	-		24 27 7 M	Fri 8/17/90	F-1 917/80	Fri 9717/80	114 61878	-	
10-02/1000 10:00	10007100014401	100011001174	100071900 12:44	189471889 18:30	10017400171	10000110001110001	10010000	10/00/1980 10:28	10/02/1989 6:15	10-11-990 13-00	1001/1000 6:30	100377880 7:16	0870/1980 13-00	08/30/1989 7:30	0478/1980 14:0	DB/28/7899 13:40			00.00	09/28/1989 13:00	00/20/1000 7:30	12:44	DW17/1989 11:20	00/27/1000 10:46	08/27/1998 0:30	7.10	11.00	2 PER 10 PER	08/26/1988 6:90	09/24/1990 13:90	DE SE MESTAPAS	092419897-18	00725/1900 7:00	00-E1 0001/EE/00	98723/1989 11:10	04:73 BBB (VEZ-NO	00:1717900 0:00	12. description	-	08-1 6061/80/80	09/20/1009 7:18	09/18/1990 11:00	04:5 M81/4100	08/18/1990 10:45	0707070	771	00/17/1000 9:15	GB/17/1969 7:18	_	00710/1000 7:00	2	•
7 15 AM	20074	12.40 %		-		_	8.00.4	1025 4	9.5	ã	30.4	715.44	100 PM	7 30 44	_		6			8	_	_	11 20 AM	10.85	9:30 44	7 15 4	1			1-00 PM	130 AM	715.44	700,74	_	: 6	7 30 AL	8	12 65 72		1 50 AM	7 15 AM	18	7 30 £	ō.	8			7 15.	_	790 AL	╀	no (hi:min)
				_	_		_							_							_				_			_	_		_	_		_	£	_		_		_		_	£ -	Ē	_		_	È			十	madatha Counting
7 8	8		1	႕	5302 16	_	_	_	_	5220 81	_	_	5200 01 1	5204.41	_					_	_	5137 64 1	_	_			_	1	_			_	50.00 41			_		_	-	. 3	_	_		_	91491	1	_	- A	_	4075 91	F	ma (hre)
107746 22	_	_	20.00		_		_		_			_	108560 21	10863 5 21	08380 21			_	100.		_	10687 5 21	0500.0 21			_	-	0000			105188 21		0		_	10470# 21	_		O4470			10402 5 20		_		109745		. N	_	20	۲	ur Mater Presiding
2216304.0 2222081.5	22154004		271428 0 8 8 24 1 1 2	2213446.8	13713.0	T COURT	270421.5	219/0004	5188925.0	2100252.5	21871570	2100003.5	21803860	2176300 0	21719804	21714295	2170125	21700001		21623115	2158394 9	21575023	2151808.0	2151503.0	2161438 8	2150616.7	21430035	714383	713004.1	2129624 6	2120271 6	2127757 6	2121120	211224499	2711	2110008 4	21100000	21044701	200	201.7	2084820 1	2087250 7	2085955 1	2078370 1	2070050 4	20704201	0	086378.0	_	2082250	ř	rmente Tetaliner unding (gal)
280	78.0	_ :	270	2	200			270	240	0 18	280	270	280	260	270	27 0	20		1 2		27 0	240	270	27.0	2110	2	2	2 :		200	270	280	2 3	270	280	270	270	2	270	2 2	27 0	240	250	280	300	240				*	ļ.,	ed Flourido (gpm)
3 8	30.5	_	i ĝ	8	8	ž ,	3 2	3 8	- 2	8	3	28.5	20.5	28.5	28 5	28.5	8	8	ğ ;	3 5	8	315	ي	20.5	9 5	8	2	8 1	5 3	. H	8	ž	8 3	2 5	8	8	29 S	31.5	g 1	8 8	8	×	8	3	8	8 :	s 8	8		£	7.	ZW (dograce C)
26 25 	3		2 2	25	25	3 3	* 0	* 5	: 3	3	: 3	1 24	. 34	35	25	3	25	25	3 (* 5	75	25	25	32	ĸ	×	ಜ	E	ة <u>ا</u>	i ii	×	ಜ	* :	2 2	: 2	×	z	z	H :	4 ×	2	8	ĕ	8	32	K.	8 8	8		8	W	ir ZW (atm)
470	50		: :	2	ž :	5 !	2 2				2		67.0	50	20	ţ	\$	•	2 :	2 8	2	620	620	20	830	200	5	t :	2 1	20	200	0.10	200	2 5	3	2	2	98 0	.	2 2	50	610	2	630	2	62:0	2 2			8		upplementel Air (elle)
	1			\$	š		. 1	. :	: &			: 1		•	å	å	•	â	£ :	5 8	*		£	1	\$	×	£	*	. .		į	47	: :	: :	: 2	•	¥	å	4	= =			¥	3	ŧ		5 :	2 2	_	8	•	lanages Residential de (gyan)
. :	5		3 5	:	5		: :		: :	: 5	: :		:			3	± 55	3			: :	ī	5	:	:	\$:	:				• 5		a 5	: :	3	:		:	: :	: :	: :	ф U7		8.5	8	3 8	: :		£		remondo Rata boltary P (ggan)
2 5	5		8 8	7.80	8.70	8	70	* 70	1 3	1 2		ìà	7.20	720	18 70	16 20	58	8	8.70	3 3	8	- 5		470	5.70	5.70	8	8	6 70	5 5	8	78	8	. 70	3 8	320	430	370	38	2 E	370	290	2 80	220	8	ŝ	8 3	5 6		970	*	minum poloro BP (in Si
4 6	:		::	:	5	4,	.,	4 6	: :	: :	: :	; ;	: :		:	•	:	:	•		: :	:		ŝ	:	•	:	:	•	: :	:	47	:	: :		: :	ţ	:	:	: :	: :		12		*	4.2	•	: :	:	•	•	P Pressure (pel)
130	130	_	130	130	120		3 .	12 1				-	- 130	190	130	130	130	130	130	10 0		13.0	130	130	130	130	130	130	130	130	130	130	130		130	130	130	0 E1	130	2 2		- :	0.61	130	130	130	13	1 10	— !	5	-	P loos in CIP Tank Literaj
6.7	: :		70	- 3	- =	:	•	2 :		: 3	-	-	-		: :	120	:	70	72	72	; •	115	2	\$	70	70	•	•	•	70	- 2	•	7,	70	70 7		-	6.7	6.7	: :	: :	: :	70	7.0	2	70	•		 ;	:		wanted Rada after SP
. :	: :		::			•	-	7	7, :	; ;		. :			172	ă,	53			15.7		- 72	42	:	:	4.7	53	5 2	5.2			51	50	• •		_	37	32	30	2 .		-	2.3	23	23	17	20	20	 ;		-	Tempera salver BP (in
	150		5 8		╁	_	_		5 6		-	_				3.00		-	 8	_						- is			8		_	58				_					_	_		1500	1500	15 08	150	5 6		 5 8	١,	P Duration (sec)
		_	ō ;		 			_	_	-		_	_	_				_	_			_	-					_	-				_				-		-		_	-					-		_			IP Fraquency (min)
_					t				_		-	_			_			_	_			_	_			_					_		_			_		• • • • •	_			_			_				_		-	
	standard and at 12-40 PM			made from sensition tark MLSS to 6000 mg/L	main degray				-			rakding belove Peak Flow			and peak flow realing at 2 PM		start peak flow reeding at 10 45 AM	regard changing		and of peak flow leading at 2 PM			that page five at 95 gpm we members sention		Danes cases							Dayles came			- Control of the cont		ment cleaning					Change Change						start cycled air to membrane tank 10 aet ONVOFF			und off fire at 1 50 PM to name marriagness	
8	. S	!	7	3 5	427	à	427	4.27	3 78	378	2	:		č	i a	ž	2 10	324	320	747	7 25	. a		231	2 80	2.80	3	324	329	324	2 2	3	1	320	295	7 .	=	Ē	177	ž	ē i	ē :		ŝ	8	0.79	123	3 1	ě			TMP (p=q
807		:	128	:	K.	423	ž	ž	4	1 85	ŝ	ž	× :	5 2	ý 5	i	å	577	\$	ž	379	i	: ;	0	:	2	8	577	5 60	2 :		è	ž	ŝ	635	2 5	8	10.29	10.50	13 86	72 7	5 i	: :	1731	3	23.81	1524	15 24	2721			Permanelly (ghi/put)
		:	ž	, è	3 86	8	37,	ĕ	130	ŝ	ŝ	2	î ;	4 75	• •		3	513	3	3 10		ž		: 3		5	524	5 13	ŝ	5	. 1	30		ŝ	5 57	223	8	8 82	8	=	ē :		: 67	. 8	16.97	21 15	35	35	24 17			Permeability Corrected for Temperature Effects (gfd/pel)
571	5 . 5		571	5 5	571	\$ 71	571	571	571	5 7	3 .	571	\$ 71	5	5 2		571	571	571	3 9 1		· ·		; ;			\$ 7	571	5 7 1	\$71	5 2		571		5.71	571	5 7	5 7 1	571	\$ 71	5 1	5	3 5	573	. 57	5 71	5 7 1	57	• •	_	7	HITT (hes)
<u>.</u>	: ;		3			•	_ :	ž		:	y.	•	20 1	3	8 5	-	ž	70	20	¥	ŗ.	. !	-			20	-	•	-	20 5			20.	20.	20 1	*				•	ē :	- ·	ě			20.	- •	20 1			1	Fixa (grid) (After BP)
_	- '		_			_	_	_	_		~	_	_	_		_	_	_		_	-	_	- '	•	_	_	_	•	-	-		•	_	_		_ •	•			_	- '		_	_	_	_	_	•	_			

Page 11 of 13

	_						_		_			_			_	_		_	_	_	_		_			_	_	_			_		_					_		_	_	_	_		_		_					_	_		_	_	_	
	=	#	4	=	=	=	ű	=	=	z.	.	5	ı,	ā	ž	ú		: 2	1 5		3 4	÷ :	: :	:	: :	: 3	: =	: 3	: =	=	=	=	=	=	= :	= =	=	ē			ì	5 5		*	ī							=	•	•	-	•	- -	kangasté vorri
	Mark 19277.00	Wed 18277.00	West 10077.000	The Partners	Two 10/2L/80	10-107E/40	50m 1075599		Ban 10724-0	tun 1004/90	1074/201	Set 19/23/90	East 10/23/00	FH 10722/80	Fri 10/22/00	10000		THE LAND MALE		7 to 10/2 1/46	Wed 102040	96-02/01 peak	10000	The Street of th	The 10/1444	Tue 10188					# 10100#	14 107070	Fri 19715/80	Fri 18/16/80	Fri 1078.00	Thu 10/10/10	SECTION PM	Wast 10/13/80	Wed 10/13/80	MATURE PAR	##1012##	1 ma 10/12/ma	Tue 1012/00	Mon (0/11/98	Han 10/11/40	Man 1971/78	Hen 10/11/98	Men 10/11/16	2 m 10/10/10		24 (O 24)	Fri 10/8/80	Fri 104/98	Fri 104400	Fri 104490	Thu 19/7/01	Thu 10/7/80	u -
	10/27/1888 11:00	10/27/1988 0:48	10/27/1988 7:30	10/28/7 1888 12:45	10/26/1988 7:30	10/25/1980 13:00	1925/1868 11:40	1975/1989 8:46	10/26/1000 7:30	10747598 11:30	10/24/1989 6:38	10/23/1888 12/00	10/23/1988 7:00	10/22/1999 14:30	10/22/1898 10:40	000 mag //22ml		107111111111111111111111111111111111111	17.45	10/21/1800 7:15	10/20/1840 11:44	10/20/1986 0.30	10701	10/18/1986 13:00	10.00	10/18/1889 7:15			10/11/10 7.44	101//101	10/10/10/10	10/10/1998 6:15	10/15/1986 13:00	10/16/1898 0.20	107577888 4:45	10/14/1000 17:44	1072 1000 15:00	10/12/1898 12:46	19/13/1985 10:45	05-4 8081/11/01	10/13/1888 7:30	19/12/1000 14:00	10/12/1998 7:30	10/11/1988 15:00	10/11/1880 13:15	19/11/1988 10:45	10/11/1908 9:30	10/11/1000 7.30	10/10/1998 11:30	1000	10/09/1999 /:00	DC:E1 0001/80/01	1002/1986 11:30	10/05/1888 5:30	10/06/1998 6:46	10/07/1909 13:00	10/07/1986 11:46	
	11:00 AM	9 45 AE	7-30 AM	12.45 PM	7 30 Æ	100 PM	11:00 AM	\$ 45 AE	7 30 AM	11:30 AM	FF 00 9	12 00 PM	700 4	2 30 PM	10 40 44	8	3 3		1	715.4	i & E	¥ 00 ¥	Ě	8	8	715.4	15 15 15		ž į			6 15 AM	90 00	20 AM	* 45 E	12 45 674	300 PM	12 45 PM	10454	# 00.6	7 30 44	200 PM	136.00	300 PM	15.7	1045 AM	MY 00.6	730.44	1 3 E		8	30 PM	17.30	8 30 4	\$ 25 AE	9 PE	: * *	Ome (Ac;min)
	S809 00	5406 75	50 1000	5785 75	6730 50	5782.00	5780.00	\$758 75	\$754.50	5734 50	923150	5713.00	5708 00	5881 50	5487 66	90000		8		546025	5640 75	05 00.05	54.36 75	5618	56 5.	5412 25	5500 75	í í	\$ 10 m	** 0000		55.30 25	5522 00	\$\$17.33	5515 75	5407 75	5478.00	547375	971 75	80.00	05 BB#5	5451.00	¥ ¥	\$6.5	5428 25	5423.75	5422 S0	5420 50	S400 50	200	200	S# 50	\$352 50	53 BHC\$	5347 75	\$330.00	57, 850.3	Cumulative Operation Nave (New)
	11234.0	1,000	1,723.1	11215.3	112113	11182.8	11180.0	11190.4	1112	1100.4	1 59:1	11143	111397	111231	111193				1000	11092 5	110730	11071 6	1064	1061	_	i i	Ŕ		8	10040		108745	10967 3	10062 8	10861.7	10942 9	10021	100190	109170	10916.4	10914.5	10880	10005	10	10873.3	108723	10872 1	10870 2	10860.2			10804 2		10798 2	10798 1	10780 3	1	tour Motor Randing
	_	_	2782524				_	2378780.0				_	2369753.5	2363438 6	_		_	—		_			_	23291765	_	_		_		_			_	-				_	_			_		_	_	_											1	
			20.0	_			_					_						_				_	270	260		270	2	7,0	28.0	77.0	2 .			270	20							200	28 6				270	28.0	27.0			. 2	:			_	•	Food Flowrate (gym)
		28.5	25	275	255	2	27	*	Z6	27	24	27	×	2	· 2		۲.	25	27	t	25.5	25	ž	3		3	255	25.5	2	<u>.</u>	e :	2 8	31.5	×	8	31.5	8 8	315	36.5	18	295	21.	<u>.</u>	5 %	, ,,	ž	8	æ	¥	20.5	8 8	 5 5	 :	8	29.5	8		Tomp ZW (degrees (
	ĸ	ĸ	ĸ	×	ĸ	×	ĸ	K	ĸ	ĸ	×	×	×	8		3 .	k:	ដ	ĸ	ະ	×	ະ	32	23		×	z	æ	ä	x	.	4 5	ĸ	ĸ	ĸ	ĸ	E E	; %	z	æ	z	z	ki k	s k	i k	: 13	£	×	æ	ĸ	K .	3 16		к	×	z		Air ZW (cfm)
	630	8.0	:	8	80	ţ	850		0.60	8	0	80	2	8	8	\$	2	8	8	700	8	2	80	68.0			670	*	•	850	5	3 6	0	870	• • •	:	2 2		8	650	670	85.0				80	84.0	860	650	\$ 70	K 5		;	0.80	67.0	\$		Supplemental Air (c
	t	8	z	2	2		‡	å	47	47	*	*	=			•	.	*	*	<u>:</u>	*	•	•	:	_	£	•	•,	a	.	# :			:	•	.	t :	: :			•	•	2 1		: :	5			•	.	:		—	*	.			Stemane Restrouted Pute (gpm)
## Presented (gst)	8.5	;	\$.5		;	3.5	:	8.5	6.5		6.5	65	: :	: :	2	3	8.5	65	65	:	*	:	:		6.5	5	5		.	an i	65 0	: :	;		•	5 :	. :	6.5	6.5	5	•	10 (47 (: :		6.5	85	65	a S	: :	. 5	:	6.5	6.5	65		Permedia Raia befo BP (gpin)
## Comment (max) ## Comment (9 70	10 80	10,20	20	70	8	8	28	10 70	₽76	8	8	8	2	; à	670	6 70	ž	10 10 -	970	7 70	8	ë	010		• 70	8	10 70	66 66	8	ŝ	8 8	8	776	8	8	8		7 6	8	8 20	16.30	5 30	70 2		3 8	8	\$	8	8	8	ŝ g	ŝ	ŧ	4 70	à		
Company Comp	=	:	47	•	:	: :	:	:	:	•	:	•	•	: :	: :	-	:	:	:	:	50	:	:	:		÷	•	:	:	:	• 7	: :	; :	:	:	•	7	: :	: :	:	•	5	:	: :	: :	: :	\$	÷	•7	•	5	: :	:	:	:	•7		BP Pressure (psl)
## Character share the first control of the control	130	130	130	- 20	j	į į	3	13.0	130	5	130	130	: 5	; ;	5	5	130	30	130	130	130	130	130	130		120	130	50	30	100	5	3 6		0.0	13.0	:	30		1 12	30	9	10	13.0	130	100	3	130	50	30	130	00	2	110	130	0	í		BP less in CIP Tani (Litera)
### Characters March March	70	72	7.1	: 3	: :	: :	: :	76	:	:	•	.,	: :	: :	:	6.7	2	•,	2	• 7	•	:	•	2		:	:	:	:	:	:	: :	: :	: :		:	70	; ;	. 70	70	70	15	ξ:	•	= :	; ;	:	•	:	:	:	: :	<u> </u>	:	67	6.7		Parament Flata selor (gpm)
Transport Annual Street Colors (1974) 2 1 1 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2	: :	7	:	? ?		: :	ž	. į	•7	:	-	: :	: :	: ;	2	52	ő	92	•	72	9.7	•;	9.2	_	•	7.2	ē	162	1	:	: :	: : 	: :	2	:	:		: :	2	12	<u>.</u>	177	67		: :	: :	8.2	5.	57	=	: 3	10 7	Ġ	:	:		Vacative after EP (in
Exemple and the control of the Vision Add Comments of the Vision Add Commen	8	8	8				3 8	8	8	8	8	15 00		<u> </u>	8	8	8	8	8	500	<u>5</u>	8	8	8		8	15 00	5	š 8	8	8	8		8	8	8	8	8 8	8	8	500	15 00	<u>.</u>	8	8 8	8 8	8	8	8	5 00	5 8	8 8	ś	8	8	3 00		DP Duration (sec)
\$ Tief (per) ### ### ### ### ### ### ### ### ### #	-	5 6	5	· •	5 8	5 6		ā	. š	-	ő			5 i	ē .	ō	6	ĕ —	õ	ō	6	ő	ă 	6		ő	5	ē	ő	ő	ē	ă :	5 6	á	ē —	á	ē	5 6 9	5 6	. á	ě	ē	ā	6	5 i	ē		ō	ā	ő	ē	ā ;	š —		ā	ő		BF Fraquency (min
######################################						-						_					marii caaning	-			_	meral charact	_		*			present a brazery				_			man channy			g page flow lasting to MT commun entermedient are	Apriled Death State (Coll) is seen to 1 and	man man of					stanted peak flow from 6 AM to 2 PM		mart classing							stant make thus leading from 11 45 to 2 00 PM	ment clapsing		Š	- Comments
Transcription 1		2	9 9	6	9	575	ċ	ê i	£ :			: :	*	172	129	329	321	š	ż		378		*	î		4 74	4.7	2	521	•	:	127	=	ž :		2	*	•			83	01	751	22	ž	67	5 5		2 85	2 70	8	¥6	521	-	2 2	2 3		Time (pol)
\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$		ž		ä	ž	ž	Ė	2		į	1	; ;	387	¥	ĩ	*	5 60	•	777	1 5	3	ž		377		ž	•		ž	ž	ĕ	ê	:	i		á	ŧ	3	¥ .	: :		343	ž	\$	ž	25.	7 5		657	83	:	6 46	328	i	: :			Parmentally (give)
		375		÷ .	ž	122	ž	ĝ	£ 1		7		37	387	520	\$	5 60	5	3 80		:	ž	:	177	_	:	ŧ	3 63	361	337	346	ĕ	Ĭ				¥	?	2	Ė		ž	316	504	30	¥	2 1	: :	37	6.22	547	573	4 50		ě	, è		Der Temperature
**************************************	•	573	<u>.</u>	=	57	571	57	71	571			<u> </u>	5 71	571	571	571	5 ? :	571	571			: :		;	:				57	Ş	671	571	•	57	;	5 5	\$71	į	1	7				5.71		ij	571			571	571	571	ž		5 21			MIT (New)
		ŝ	8	3	š	:	š	:	3	•	<u> </u>		Ē	:	÷	:	:	: 5	: :		:	: :	: :	: :	:	i	:	:	:	Ē	:	:	8	:		. 3	8	Ę	£ 2	3	3 2	. 5	Ę	ž	4	į	:	: :	:	:	ĩ	ě	71.7		<u>.</u>			Flux gold (Alber BP)

Table C-1 ZenoGem Operating Data

	0	CROM	C(NONMAL)	200	The contract of	Percent.	MACON)	AIAT & GAME	T					_		_	_			_		-	_				_	_		_	_	_	_		_	_	
PRIAME WITH CYCLED AND TO MIT-EVENT 19 PRIAME WITH CYCLED AND TO MIT-EVENT 11) PROPRIAME AND CYCLED AND TO MIT-EVENT 11)	HOMEN	MITH CYCLED AM TO	HONNIAT)	EAR-EYENT 1)	CONTRACT INCOME.	CONTRACT BRANCO	COMMAN MENO	Š		0			n			-	į		ALAT & COM		ī	z.	ü	.	=	ā.	ū	=	=	12	ī	ı.	.	ı.	=	=	Bagarisvani
T AND AT-EVENT 121	1.000	α-€VENT 7	i					L																													
									MAX	1		I A	Ī	MEAN	MAX	•	MAZAN	MAX	į	MEAN	Tue 11/2/80	11/1/4	11/1/10	Mon 11/1/80	Mar. 1371/88	Bus 10/31/98	5471700 mas	Set 10/20/90	24 10/20/20	Fri 10/20/99	Fri 19/29/80	Fri 10/23/20	Fri 10/20/00	Thu 10/23/70	Thu 10/20/99	West 10/27/04	Date
			·																		17/02/1986 7:15	11/01/1988 13:50	11/01/1989 11:00	11/01/1998 6:45	11/01/1999 7:30	10/31/10/00 12:30	1031/1600 6:16	10/20/1000	10/20/1888 7:00	10/28/1988 13:SD	10/20/1969 17:00	10/23/1000 b.45	10/28/1808 7:30	10/28/1980 12:44	10/28/1898 7:30	10/27/1988 13:00	Date
									l												7 15 AM	100 PM	: 8 A	8 & &	7.30 &	12 30 PM	6.15 A	11 00 44	7 00 1	00 PM	1.88	6 A	7 30 444	2.45 PM	7:30 AM	7 00 PM	Time (N:min)
																					5944 25	5630 00	5028.00	5828 75	5924.50	5905.50	5800 25	5880 00	5876.00	5858 00	5856 00	5864 75	5852 50	\$633.75	5828.50	5810 00	Consultitive Operation Time (fire)
			İ																		11376 4	113572	13662	11364.7	113622	13224	11328	113079	11303.7	112857	112834	112005	112112	112025	112572	11238.7	Nove Motor Reading
	ĺ		ĺ														İ				24405822	2434441 9	2433905 0	2430669-0	2433077 4	2428487 8	24246720	24183123	24168559	2410666 6	24100000	2409862.0	2409099-4	2402608 5	2400763 5	23041PH 8	Personanto Tut <u>nitror</u> Penadireg (gal)
311	27.3	3	7 1	2	Ĕ	Ĕ	\$		=	ī	ž	29,0	z	25.5	8	٤	25.6				280	27 0	28.0	2 1 .0	200	28.0	240	15.0	25.0	*	28.0	200	26.0	28 0	270	2	Food Financia (gpm)
225		£	= =	26.1	21.0	#	26	E	22.0	Ē	r R	ž.	27.0	Ë	e a	77.0	27.8	28.0	76	¥.	25.5	2	27	¥	24.5	27	25	28	27	28.5	29.5	27	27	2	28.5	27.5	Tainp ZW (dagrees C
##	ě	31.4	2 2	25.0	ž	28.0	26	Ē	20	26.0	17	n,	ž	26	24.0	24.0	28.0	25.0	3	Ĕ	ಜ	ĸ	×	×	ĸ	ĸ	k	ĸ	ĸ	ĸ	Ħ	ਸ਼ 	ĸ	ĸ	ĸ	Ħ	Air ZW (clim)
EEE			- 1			B1.0	20,6	٤	700	\$3,0	Ē	20.0	ŧ	£	•	20	Ê	1.5	ï	5	0.20	8 2.0	.	ţ	8	•	:	820	\$	20	8	\$	850	2	8	8	Supplemental Air (cf
121								ŧ		37.0		1		- 1					Ē		×	\$	8	8	\$	=	ĸ	t	3	8	2	*	¥	5	.	<u>.</u>	Biompto Paniraviatio Cale (gen)
						:		:	l.	٤	:							l	2		┝		_		-	_			\$		25		65	_			Permatte Rate before BP (gpm)
	1	l			246	1		2	170	Ē	5	18.70			Ì					273	18 70		_	78	16.20	5 00	16 70	14 56	13 00 E	. 8	28	_	13 20	70	170		Vacuum bolors BP (t Hg)
::::					ĭ		E E	7.7	130		12.0				14.0		נו		12		13	130	: -	17 130	=		<u>-</u>	<u>-</u> ت	: 	- -	* -	• -	47		_		BP Processo (pol) BP loom to CIP Tank
::::							•		15			12.0	:			£		6.1		5	70	_	75	72	74	71 OE3	130 48	130 67	130	30 68	130	130	130 70		_	_	BP loos in CIP Tank (Liters) Permati Auto alter B
i i i								١	١				į				- 1	1			┝				_	_			_	_	·			_	_	_	(gen) Vanada alka BP (in
								1	1			1			Ì						H	_	_			_						_					
:::								1	Ì			1			ı			ŀ			H		_		_	_		_	_		_	_	_	_			
																					-		_		_	_			_						_	_	
																					ENO OF TESTING			many classing								Process same					Conjunta
		Ξ	ĕ	=	ij	324		١		ž	È	=	÷	ž	į	91.0	147	Ĕ	9.37	1,27	-	737	7 22	7.	î	77	₽ 20	712	ŧ	3.5	š	:	:	5 75	5.75	î	(140 (p=1)
:		=	12	2	Ē	ŧ	5	20.00	3.5	ě	12	it it	2	7.72	##	5.77	Ê		ŧ	70.00	202	ř	2 56	213	ě	?	2	263	274	3 6	34.0	2	ž	324	120	ž	
	3	5	ij	12.	77.00	ŧ	103	5	:	=	ŧ	11.17	Ë	į	3	6.9 1	17.44	4.7	ř.	10.07	201	237	247	7 8	2 12	ž	22	ž	2.0		3 Q £	775	2 75	8	=	ž	Permethility Correct for Temperature Effects (glidical)
995	99	2	i	Ē	Ē	Ē	5	=	.77	=	1	5	Ē	£	į	ž	6.57	-		-	1	571	•	6.73	571	571	571	571	571	5 71	571	57	571	6.71	 •	571	(MT (Mn))
	ĒĒ		ĭ	1	i	17.3	1	1	2	ī	21.6	1	17.2	ž	2	Ξ	Ē	1	2	22	-	2		8		2	ē			<u> </u>	=	_	3	8		3	Flux

•

Table C∗1 ZenoGem Operating Data

	(Julius) (SEVJA)	10,350.00	9,550.00					20 507 0	3	9.450.00		1	3	9 900 00		11,000 00			15 900 00		3,900 00		8					,					7,450.00	9.950.00		10,550,00	11,500.00		12 865.00		12.400.00	12.950 00	_		11,550 00		00.00	1,900.00		11,400,00	4	
¥ .	(Jen) SEAN	4,900.00	13,700 00	00.000.00	0.000.0	6,950.00	8 8 8	200000	10.250.00	13,100.00	10,875 00	3,100.00	8 97.7	12,500.00	16.550 00	15,250.00	11.175.00	10,550 00	22,850 00	17,450 00	19,900 00	15,800 00	8,900 00	14,550 00											14,450.00	14,850 00	16,190.00	15,500 00	0000		17.650 00	18.050.00	00 052 81	17,300.00	18,050.00	16,300 00	18,450.00	16,150.00	13,150.00	15,550.00	14,750 00	
ŀ	(nimi.Aso gm) Muo	3	8			_		:						9.4				_	89.0		89.0		_			_	_			_			T	-	B	60					800		_		_		8	_	_	\$20		
5-	(15 ⁴ m) 00		9		8		8		8 8	7 70			8 8			S						2	2					_						;	3 2	5.10	6 6 0 0					8	5.		8	8.	P 9	8			3	
	Temperature (degree	26.20	27.00	27.00				8 2	25.00	26.00			8 8	8	88	26.00			8	27.00	26.00	2	22.00											1	2 8	27.80	27.30		8	26 40	36.00	27 00	8		98 00	24.20	8 8	39.80		å	8 8	
-	H		7 07						2				8	27					8		9									_					•	8					7.38				7.47		į		_			
	Telef Phospherous (Ages)	41.80						_ ;	8				67.6						28.30							82								1	3				9	3						12.80			_		8	
-	آدفها الكادووم (سهال)							-	2				2						155 04				_			8									2				:							2				2	2	
	(Agm) HOIT							į	28				8 5.70		_			•	8				_		;	D/				_			T		2					3						2				;	<u></u>	
	(mg/high) H-EOHASON	å							8				81.0		_				8							8									0.0					-						ş				ş	8	
	MAS-14 (mg/L) (ASL Check)																																ĺ																			
•	(76m) H-8HH	33.00	25.30					_	72 4 0	26.20			8	4		88			28 60	•	97.00	_	27.20			8									96 90 96 90	27.20	28.60	3		3	27 90	26 00	_		27.00		24.50	22	<u> </u>	5	8 2 8	
9	(Agni) 881 beef	340.00	238.00						754.00	252.00			<u>3</u>	8		360.00			00.08		170.00		988			ž 8		_					Ī		8	8.8	8 62	3		3	90.00	8			212.00		98.00	8	1	5	180.00	
DED.	(vêw) squab (wêy)	530.00	8				_	_	8	8			246 00	8	3	248.00			216 00		224.00		8			8 8 8	-			_			T		215.00	8	8	8		8	262.00	270 00			80.26		8 %	96	200,000	,	28.00	
	(Agm) 00	QF O	3 2	Q	_			Q# (0	8 5	2 6		_	2	2 8	8	4		_	8.0		8	8	8				_			_					8 8	8	8 5	:		2 5		8,0	86	_	98	Ą	8.	2 5	}		6 5 5	
ľ	ALIK (INGAL)	380 00					396.00						545.00						39100																8					8											8 3	
	(7 ^{#w}) 000							_	8.8										300 00										_		_		T							8			_						_		00.00	
	Conductivity (usion)		800.00					_	00.06	1 740.00			00 080'1	00.02	8 02	8000			00 000	1.860 00	2.030 00	2,630 00	2,140.00							_					2,370.00	2,000.00	2.540.00	2007		2.080.00	1.860.00	2.000.00	1,920.00		1.980.00	1,880 00	2,040.00	2.300.00	2,140,00		2,150.00	
	seergeb) anulanegmal (2	28.00	8 8	28.40				24 50	8 8	2 8 8			25.00	22 00	8 8	3 8						8									_		1		28.00							26 00		_	27.00	36.±0	27.00	27 25	8		27.00	
		87	7.13						7. tō			-	Ē		P.				230		2,														10.7	727				Ľ,	7.12				127	!	7 12				7.18	
	EZYJH spiedz siny (Agm	-				-																																														
	SELM agout steat												_													_																	_									
	T agbult sime! (Jan							_							_																																		_			
	HMT agbuilt utset (Agm																																																			
	000 egitude electi (Ager	:						_							_																																					
	(arpab) TAS sastery	24.73	2 2			_				2, 2, 2	?	22	22 28	22.23	F :	2	2 2	5 5	22	20.00	1		3	21.77	21.30	ş						_			į	3 3	2 30				1 2	3	_	2	3 :	1	7	1	2 2		2 2	1
	bloff agout									E	X		80.0	_	8		g o		:	1	?		275			Ŗ										2					ta c	, E				<u> </u>	Ş		10.0		2	!
	DOS seeks into	2 2	:	:					Ξ	•	2		2		•		•		,	2	:	?	=			•				_					5.	*		æ		=	£	3 E			:	2	۵		Ę.		٠:	•
	becuber! seek late									a (2	9	Ξ	7.	ū	5	•		;	. :	2 :	; =		ĸ	R	۲,										. č	ñ				:	23		£	ឌរ	R R	2	ឆ	2 :	:	2 1	3
	med betself egbs (kgg) ihtel enmine									8	8	8	ŝ	ē	ß	£	£		1	3 8	3 9	8 %	9	ĸ	ŝ	ŝ										5 3	8				8 8	3 %	!	ž	8	8 9	ě	ä	ž 8	j	8	è
	most befastif egbu (b-gg) line? mellen		ŝ	<u>§</u>				_						8				8	8	8		ş	2 9	3 8	8					_			1				ŝ						_									8
İ	SET Innumer 97 W	8 8		8				_	25 00	-	8		00 021		88		9 5		:	8		-	8	3		8							1		8	95 00		212 00		240 00		8 8	! }			8	200.00		8		90 02	8 82
	WTP Influent CBGG	- 8.8 8.0		216.00				_	220.00		8		8		248 00		38.00			8		802	8 92	3		278.00				_	_		1		22.00	98		564.00		220.00	1	8 8	,			8	316.00		8		8	B 01.7
	N-DSI Inserted 47% (Ap	00 th	28.10				21.10	2 0					80.00	28.70		_				9	ă		_		_	8	8			_	5	2 2			8	ğ				8	D# 150		_			2 3	į				8	8
	atempt annual (m)	9	8	\$ 8	!		8 8	3 2	8	8	3	3 5	2	8	8	80	8	8	8	8	8	8 8	3 8	8	8	8		_	_	_				8 8	8	8 5	9	8	8 8	8	8	2 5	3	8	8	8 :	3	9	9	9	ş	<u> </u>
ł	(vi) emit a	- 5	8	22.55	8	8	8 3		2	217.08	8 2	8 1	313.00	30,708	8	20 000	8	E E	2	8	8	8 1 R 1	2 2	8 8	8 2	8	8	8	8 1	8 8	8 8	8	8 2	R 5	8	3 5	8	R	3 3	8	8	8 3	4 8 8 :		1013.58	100	8 8	1,000.70	20	9 5	208.08	10002
		THE NAME													West 2/2 aven 3	Thu 2/25/88	Fri 1/26/80	Set 2/7/AB	Sur 2/2 8/84	A STANK	1ue 3/2/90	Med 1/2/86				Bear State	Tue Manual	A 27098	The STIME			201778	Pri arienne	2	Man 3/22/8	Tue 3/23/86	The School	FM 3/26/88	A 327/8	and 3/20/00	Tue artistie							The Angle	5			- TAN
	BT AGENTENT							_									-			•••														•					•				-								-	-
		1																																										_					_	_		_

01.00

_						_	_	_	_			_		_			_	_	_		_			_	_		_		_			_		_									_		_			_	_	_	_	_		
																																	۰																					
Tweetend:			PH 6/1 VAR	l	A	744 645	S	١		Ц				Set 5729/98	1	Thu \$/27/80	Ł	1	_	_	_	100	Š	ŝ	Man 6/17/88		_			•	Ц	24 KA44	57		Š	Š	See 62/16	Fri 4000	_	_		Sun 475	_	Fri 4/23/98	_	_	L	Sun 4/11/00	_	5		-	Data	
2734.25	2713.00		2861.08	2017.00	2563.08	2500.00	2948.00	252	2473.08		200	23/7.08	2352 54	2728.58	2305.08	2281 08	257.08	2230	2100	2161.08	2137.08	2113.08	90 6805	2085.33	041.08	2018.54		945.08	100	80.78	1040.50	825 De	101 OS	1753.08	1729.08		881.08			_		1513.08	8 58	1465.00	2	417.08	9	1349.58	324 83	1300.83	1277.00	1253.08	Run Time (hr)	_
_	8	8	6	80	5	ŝ	_	8	8	6	_	8 8		50	8	8	_	_	8	8	š	8	6.50	_	_	8	\$ 8	8	_	_	8 8	8	ŝ	8 8	_		, S	8	8.80		_	8	250	ŝ	8	8 8	_		8	8	8	ŝ	Permante Flour (gpm)	***
28.50	22.50			_	_	8	24.0				8	8 8					_	26.20	-					27.80	8					28.00	37 38		_		30.70	8					27.50	ž Š			_	1	3 8	! 5				_	WWTP Influent [mg/L]	N#13-N
90.60	36.00	3 8	204.00	8	212.00	80.00	8	208.00	8	1	8 8	8 8	82.00	238.00	26.80	ž 8	208 00	8	1 8	8	92,00	218.00	230,06	212.00	8	236.00	3 20.00	218.08	251.00	8 8	225.08	8	236.00	230.00	285 85	8	8 8	80	240.00	67.08	300	\$ 22 B 8	260 00	20,00	28 88 88	386	2 20 10	3 8	}	264 00		278.00	WWTP Influent (mg/L)	CBO
8,00	12.00		8	200.00	14.08	8	ē,8	48.00	8	8	8 8	13 66	8	72 08	172.00	168.00	52.08	728 80	3 2	100	14.8	8	240.00	172.00	116,00	212.00	8 8	80.00	172.00	172.00	20.00	100.00	168.00	72.00	80.00	8.00	8 8	 	78.00	182.00	8 8	1 E	200.00	172.00	204.00	212.00	8 8	208.08	i	64.00			WWTP Influent (mg/L)	TES
												_							8	8	ŝ	ĕ				75		3	ë	35	3 2	ร์	ğ	Ē 5	ŝ	Ë	12 5	ž	8	ŝ	ŝ	ž ž	š	ŝ	š	ŝ :	ž 5	į					Bludge Wested Aerotion Tenk (from (ppd)
8	8	5 8	!		8			8		8			20	ä	3	ŝ			ŝ	8	ŝ	8				20 3	š	. ž	770	8	8 8	É	250	ž š	Ę	É	s e	ŝŝ	ź	ĕ	ŝ	ž ž	ž	ŝ	ĕ	É	Ē	ŝ 8	į	ž	É	8	Bhadge Wasted Membrana Tan	from
5	õ				7			12					ü	12	7	12			•	8	۵	27				23	# t	3 13	Ŋ	2	8 4	1 18	4	8 8	8 8	37	3 :	i K	1 88	ñ	8	4 8	ŧ	2	ŧ	ដ	¥ :	<u>.</u>	; 2	. 2	23	21	Total Mass Pro (Malday)	duce
	₹.	_	5		-		rž.		=	-	 Ri		 :		- -		- -			_			í		2			_	ā	_	=		-		 ;	<u>۔</u>	_	=======================================		22	_	<u>.</u>		17	_		_	 %		-			Total Mass BO Applied (M/Jey	
_	ê	_		_	0.65					_						_	_				3.04	_							ž	_	3 30		ī.	-		2.93		ē		 S	_	2 \$	_	223	_	1.70				- 1	_	1,1	Shudge Yield	
24.73	24.5	2 2	-	_	3180	_	_	22.26		24.73		_	- 60	9	29.64	18.55		_	_	20.42	8	20.42			_	25.80	1 6	20.07	20 8	25.88	- Z		ë	14.20	ī		17.81	17.48	21.30	21.0	ī	ī ;	Ē	- -	ī		—	17.49		ž		_	Dystem SAT (d	-
_	3140				2880	_	_	_		_		_				_		_				_		-		_	_		_	<u> </u>					_			_		_				_	_		_			_			Weste Studge (mg/L)	C00
_	130			_	150	 i	_			_	_	_		_		_	_	_	_	_	_	-			_		_	_		_			-	 			_										_		_			_	Waste Studge (regl.)	TKN
_	ž				ã	_			_					-	_	_				_	_	_		_	_	_	_		_		_	_	-	_			_	_			_					_	_		_			_	Waste Studge	TP.
_	12,300,00	_	_	_	17.70	_	_			_			10.75		12,000 00	_	_		_	_		_	_		_		_	12 950 00	10,150 00		11,400 00	_	11,000.00	-		16,900.00		(D) SMC-C)	 ;	15,800.00		19,150 80		16,500.00		17,700.00	_					_	(mg/L) Wasto Studge	MLS
_		_	_		8	<u>.</u>		_	_	_			8		- 8	_	_	_	_			_		_				8	- 8		8		8		3	8			<u>_</u> ,_	8		8		8	_	8	_				_	_	(mg/L) Wasta Bludes	
_	9,000,00	_	_	_	9,000,00	_			_	_			_	_				_	_		_	_												_		_		_	_		_		_		_		_	_			_		(mg/L)	
_	8	_			3		23	_	22	_	7 PK		<u>.</u>			- 2	6.83		731 2	_	_		36	_	710 25			-	8		8.97		2		3 ~	7.28			9 N	6.78		7.65			A)	7 18 2	_	8	_		~ ~	722	pit Temperature (-
	29.50	_		200			_	-		_	_	30 00		_	28.50		_		23 00		2	_		_	_	_		29 00		_	29 00 1.5		_	29.00		_			28.00	_	_	_			_	27.00 2.1	_		_	_		8		
70.00	1,980,00		2	3 8	8 8	3 8	2,110,00		20,00	8	80.00	00 529	8	_	8	0.00	8	8	_		2	8	00 8/28	00.00	8	_	_	8 8	8	846.00			8	940.00	8 8	8			864.00	8	70.00	_		8	200	2,150.00	80.00	8		90.00	8	2,080.00	Conductivity (u t /c
_		_		_		_	276.00		_		_						_		275 00				_								8			L								29.00	_			_		_		_	_		COD (mg/L)	
_	8			_			00.00		_	_	_	360.00			_	_			00 00		_	_	_	_	80			_		_	350 00			_		376.00				_	_	370.00		_		_		8		_	_		ALK (mg/L)	
2	8 2	_	_	180	3		18	_	146	8		8	161	_		3 5	_	8	8 E	_		_	200.0	_	870	_	_	_	0.70	8	<u>8</u>		24	0.70	20	0.70		_	0.70	8	_	<u>8</u>		222		090 248	_	330	_	e T	_	0.70	DO (mg/L) Feed CBOOM	
_	100	_	_	8	- 8	B	153.00	_	8	_	278.00 13		8	_	_ E	3	210.00 124		<u>š</u>	-	_!	3	8		8		_	20 20 20 20 20 20 20 20 20 20 20 20 20 2	-8		8		8	Ŀ	8	8			219 BB	8		8		8		8		š š		8	3	8		_
-	106.00	_	_	8	_	8 	22		200 24	_	200 25	_	80.D0 29	_		3	28	_	27		_	8 	8	_	8		_	22	8	_	124 00 27		8	╄~	Ē 8 2	12.00 27	_		\$60.00 	172 00 23		108 00 27	_	27	_	22.00 25	_	23	_	48,00	_	26	 	_
-	22.20	_		8	- 1	8	22,00	_	24.40	_	25.08		8	-	8	š 	8	-	ő			7	8	_	36.30	-	_	25 70	9	-	27 00		8	\vdash	8	- 8			¥ •	23.50 26.80		ô	_	27:30 27:60		25 00 11 30		\$			<u> </u>	6	1013-14 (mg/L)	_
-	0.21	_		_	_		6	_			0.00				_		_	_				_			_		_		_		0.05	-	_	\vdash		- 0.01				8		001		8	_	8	_	0.37		_			HOSMOS-N (
-	54.10	_	_	_	_		SE.70	_	_	_	20 40			_	_	_		_		_	_	_	_	91 90			_	-		_	5 55 00	_		+	_	- 45 36	_		_		_	36.10					_	91 90			_		TKN (mg/L)	_
-	g 3531		_				8		_	_	6 TI 49	_			_	_	_	_	0 4722			_	_		_		_		_		55.05			\dagger	_	- يو		_			_	36 ::	_		_		_	92.27	_		_		Total Affrega	n (m)
-	220	_		_			- 6		_	_	5 8				_		_		2 1270			_		- 2	_		_		_					-	_							*	_	_		_		7 13.50					Total Prospir	-
-	7.25	_		_	_	<u>.</u>		_		-	7.25		7 15		_	_			70 7 11	_		_		-	-,	_	_		_;		7 25			t				_		8.80	_	•	_		_	7 15	_	7 20			-	~	 ,	-
	2 25			25.55	_		31.80		9	8	_	_	_	_	-	2 3	_		_	_		3			2 3 8		_	30 50	_	8 8		_	~	╁		8 8	_		28.00	_			_		200	27 00		_		;	2700	_	Temperature C)	(deg
	8				3	320	:	Š.	_	8	8	ğ	ě			8 8	3 2	8	80			ě	ě	. .	3 8	;	_		÷ :	6 6	8	_	3.70		3	ر ة ة			3 3	3 8	8	8	_			É	8	Ē					00 (mg/L)	_
		_	-		_	2		3	_	_	10.00	_	10	ŭ	_	5	- f		2	_	-	_		2	-	-		_	-		ě	<u>.</u>		=	ê 3			ű.	<u>.</u>	970	_	0.74			_	8	_	8 3	<u>.</u>	2	<u>.</u>	2	OUR (mg O2	L/mi
	13.100.00			12,750.00			-	2000	_	_	_	_	_	13,450,00	_		30000			11250 00		_			3000	_	2 Dec 00	10,560.00	1,550 00	10,500,00			14,400.00	+	_	550.00	18,800.00	15.300 00	_	7,440,00		16,100.00	17.150.00		_	18,450.08	7,300.00	_			_	18,790,00		
	9.700.00			9,800 00		380.00		00.00	450.00	3	7,960 00		8,250.00			200 00		3	8.550 00			10,500 00		7,300.00	8			8,000.00		7 700 00	250 00		200.00		9.800.00	Ì	8	_	1,100.00	00		150 00			700 00	11,800.00	_	13.800.00			12.050.00	2.000.00	ML VSS (mg/	u

Table C-2 ZenoGem Water Quality Data

•		8	8			8	8	_	 8	_		_				_	8		8		<u> </u>		8	_	 B	8		_	8		_	8	_		3	8		8		 8	_	8	-	8	_	- 8			_	8	_	٠	
٠.	PETABLE (MBV)	10,78	9200			8	8.550 00		9.500.00		8 350 00		8.150.00	2,000	_	_	7,900		8000	8		_	E 000 00	_'	8	9.350 00		_	9.500.00	90001	_	10,150,00			3	10,250		90.		9,350		97.00		9,300,00	_	7,750.00	_	8,550 00		7,850.00		,500	-
	(Jdm) 98794	13.950.00	12,350.00	15,900 00	12,350.00	13.400.00	00 005 (1	11.650.00	11,400.00	13.550 00	2000	00 059 00	10,800 00	11,150.00	12 600 00	11,200,00	10,400.00	10,950 00	10,950.00	10 800 00	12,500 00	11,850.00	00 000 01	10,550 00	12,450.00	12,750 00	13,300 00	10.400.00	00 006 21	60.51		13,900,00			14,000,00	14,000 00		12.250 00		00 050 00	11,100.00	10,000,00	10,200 00	10,850.00	9 150 00	10.450.00	12.060.00	11,350.00	9.400.00	0,550.00	10,250,00	0.000.01	N. Des
	(vim.liso gm) mua	17.0			-	?	98				8	!	8				290		ò				0.87		3				ŝ	8			_	į	0 82	3				0.74		Ř.			_			8					
	(7 0 w) 00	8 8	_		_	9 9	_		8	_	Ş			R S	-			_	8 8				_		\$ 5				\$		_		_		- 0	0.0		_	_	_	_	5.10		2 00		8	_	_	5			۶	
	rengeb) endenegnei (3)	8 6	31.80		- 1	28.5	2 2	8	91.00		2	8 8	32.00	8 8	8		£	32 00	8 8	3 8	3		32 00	8 :	£ 8	3, 40			ž							8	28 00		_	8	82	E 33	5	3,20		5	8	80.00	8.8	8 28		- 5	8
_	Hq	82				8	6.87				2	!	ž				ξ		7 18				7.15		71.	_			Ξ.	2	-				8	2			_	2 39	-	2				;		g				;	R.
	eveneriqueriti lete T (-Agm)					*					:	2					523						12.30						ş						8	_										9	!						Ē
	آخط نظاموهم (ميهار)					5.2					2						5						96 02						75 52						37.72					24	ì					2						,	3
•	(7/8w) HOLL				_	8 6					;	3					43 10						8	_					5.						37.80	_				5	3					8			_	_		-	8
	(Jem) H-ECHASON					8					8	3					100						200						0 (2						0.12	_				8	3					8	;			_			š
	MH3-H (mg/L) (ASL Check)																																																				
	(VGu) H-EHN	22.20	23.10			94 94 90	5	3	25.20		5	R C	23 00		33		24.00		22 10	5	9		22 50		9	0.0		•	28.20	Ş	0.5	23.30			22	800		22.50		8	3	22.10		900		£	?	2.50		8		-	£
9	(Jen) SST been	124.00	8			ş 8	ş		1,200		,	8	8		8		8	_	112.00		8		8		80	8			132.00	1	B P	8			8	8	3	212 80		8	3	90 90		8			3	8		90			8
ב	(76m) 10085 Peer	00.85	8			135.00	8	3	8	_	1	3	202 00		88	_	8		90 96		8 3.		8	_	8	4	3		8		8	5			69 00	8	3	135.00			8	67 00		ŝ 8			8	8	_	172.00			8
	(Agm) Oc	D. 70	8 9	-	_	0.80	8 8	3 2	95.0			8 8	8	8	8		1 10	2	8	8	2		980	8	9 1	8 8	-		80		_			_			8			_	8	0.80	0.80	8	_	- 5	8 8	2	0.00	8	_	_	Š.
	VEX (IMPE)	L				360 00				_	-	8			8			358.00			8		360.00	_												_				į	3		_	_			8		_			_	338.00
	(1/8w) 800	_				8											312 00	:			912 00					_	_	_	812.00		_	_				_				-	86. R6.												8
	(прусы)	2,000.00	8 8	R		1.9MS.00	1,729.88	1,910.00	2,000,00			8 8	8	1,941.00	1.920.00		1,778 00	1,757.00	0.926.0	2.080 00	2 (40 00		2,100,00		1,700 00	2.120.00	3		2,100 00	2,450.00		2.100.00	8		2,130.00	1.900.00	2070.00	2,180.00			2,080.00	2.114.00	1,739 00				8 8	679.00	1.643.00	1.628.00			1.601.00
	socifop) sungametros	30.00	S 5	3	_	23 50	90 90	8 8	28 50	_	_	8 8	29.80	30.00	90 00	_	8	28.50	29 50	30.00	29.00		8		8	_	_		30 00	_						_	8 8	_			8 8				_			2 2	_	29 60	_	_	30.40
	н	7.13				87.8	,	8				<u>5</u>	8				7.24		6.70	_			8.0		5,				2.20		7.23				2.13	;					Ŗ ,	7.15					7.07	7.04					82
	SEV-Mi sybudge MLVSS (Jegm					9,950.00						10.250.00					2 000 00						7,750 00						9,950.00								8.00	10,100,00			8,400.00							000000					7.850.00
	Scale species also (Agri			8		12,950.00		12.800 00	13.450.00			13.050.00	10,500.00		10,100.00		00 051 01	-	20000	_	11.550 00		10.400.00		12,700 00	-	8		13,650.00		3,300.00		3	_			3	80 95		_	8000	00 006 11	-	10,500.00			_	8	1	0,450 00		_	10.550.00
	Ti egbudg atent	=			_	5			- 2	-	—-		<u> </u>	_	<u>-</u>				ō		-		138	_		_	 ū		- B		<u>~</u>		_	_	2			Ľ	~		<u>-</u>		_		_			_	-	_=		_	ā Ē
	HNT egbull elem (Jape] 1				1240						240					<u>-</u>	_		_		_	230	_					080				_		7,				_		<u>-</u>	_			-			_					8
	(ydu	+			_	3220	_		_	_		000		_	_	-		 }			-	_	3280			_	_	_	3020		_	-		_	2920	_		_			13700		-		_			_				_	12400
	Marie Shudge COO	∤ _		8 2	. 8	24.73	92	8 1					2 2 2	-	17.81	28		_	22.26		22.20	2 2		_	28	2	1 :	. J							7 0051	I	8 8				Z :		_		22.26	- -	_	. :		4		19'81	781
	(eyab) THE mater	╀	_	8 3	R		—	_	17.81	-		5 5	χ Ω 		<u>=</u>	22 28	_	2	22.	2	22	: :			20 228	_	E :		: 		_	_			22	_		_			<u>.</u>			- 8	_	17.81	-		-	# P		<u>-</u>	-2-
	bleff agtur	╠			_	8	_	0.47		_		=	-		_	_		-	-				9		-		-				_			_	~	_		_	_		-	_	: 		_				_		_	_	_
l	otel times BOD, period (britisy)			<u> </u>		=		=	7	_		-	•	_	2			<u> </u>	=	_	_		Ę	_	_	_			=	_	=		_		21		=	: 		_			2				<u>:</u>		-		-		_ 5
	becuterf east top	2		- 9	•	2	2		2 2	•	~	2		. 21	Ξ	=	2:		• •	9	•	9 :	₽•	•	6	•	2	2 2	?						R	•	2				2 :	<u>.</u>	: :	= =	•	5		2 :	.	2 5	: =	=	=
l	most betraff agbu (big) årna? eruselme	8		r i	§ 12	8	ā	2	8 2	ž	8	<u>.</u>	8 X	Ř	52	ã	Ē	2 8	8	ã	ŝ	<u>s</u> :	3 8	š	š	Š	ŝ	ž ž	2				ē	3 9	ī	ā	8	3			38	ž ;	9 9	<u> </u>	. š	žī.		10	9 5	8 8	į	Ē	ĕ
l	meri betasif egbu (bag) árati mellene	2									ĝ																						2	3 8	35		8																
	SST knowled 9TW (Je	80 M.Z	2 6 .00	800	8 8	20	95 25	8	8 8	92,1	148.00	112.00	8 8	8	90 25	8002	8	8 8	8	8	96 98	8	8 8 8 8	8	212 00	00.00	8	8 8	8 8	8	178 90	8	8 8	8 8	28.00	200 002	8 8	8 5	130 00	128:30	116.00	8	8 8	8 9	30,00	124.00	116.00	00 24	8 1	8 5	8	8	32.00
١	WTP Influent CROD	20.00	90 08	8	8 8	8	8 85	214.00	8 8	8	8	8.8	24 80	8	199 00	216.00	210 00	8 8	8 2	22,00	278 00	22400	8 8	8	8	8	8 9	8 8	8 2	8	160.00	8	8	8 8	87.2	170 00	28.00	8 8	8 8	8 8	8	8 1	8 2	8 8	8	170.00	8 8	90.00	8	8 8	8	8	79 00
	H-CHM knowled 97W (Age			_	_		27.30	_		_		3.6			_	_	_	9 2						2 2	_					2 8	_				21 40	_	28		_		21.80	8	_	_	_		24.30		_	_		_	8
I	incial desires	+	2	8	8 5		_		8 :		3 3	_	8 5	8 8	9	3	_			8	8	8.		_	_	3	2	8 5	8 5	3	2	8.50	8 :	9 9			8	9 5	3	8	8	8	8	8 5	3 8	9	_	_	S	8 5	3 5	3	- S
1	(vi) amil m	18	_	8	3 5		8	8	_		3 3		8 8		_			_	5 8		8	2	8 1		3 37	8			_	35.7.56	_	Ē		200	_	3752 00	8	8			8	80 BL RC	80.00			04.80	90.990	95'130	80 /DI#	3 2 3	2 2	3	
	•	West Scrieber 27	Thu 6/17/86 27				Tue 6/22/4m 29	82 887278 PAM	Thu 4/24/10 29		Ser 427/8	Mon 6/26/98 30	7 = 4/29/10	The 27/20	Pet 7/2/80 31	See 775/00 31	Sum 7/4/88 31	27 Dayler 1/18/00 32	200	77 Jan 7 Jan 17	Frt 7/4/00 33									Tue 7/20/06 35			W 7/23/4	200		Tue 1/27/888 37						_	-		*				West British			200	Man City
	STAGE ÉVENT						_	_				-										-		_	_	_	_							-,										-				_		_	_		_
	ETAG																																																				

Page 3 of 10

		_	_	_	_	_	_		_				_		_		_	_	_		_	_		_		_				_							_	_	_	_	_		_		
==	=	= #				•	•								7		. ~	7	٠, ٠	. ,	•	•																				• •	• •	•	STAGE/EVENT
1977	ı		Ĺ	Mon (8/)1466		74 1000	170 107.0	Ī	18.3	See 10/2/4	<u> </u>	THE STATE	W 120	Han 8/27/86	Sum activities	S 225	77 ₁₀ 8/234	Many BUZZ/BE	100	35			ц	1	5 m 972/m	_1_	F# 910	Ц	ì		1	F-1	3	1 4 4 4 4	LL	Sat NZW	1	2	K I					Tue #177/	Spie
5586.00	5512.73	22.2	8		\$377.00	_	5324.25		52//41				5 00 6			5082.91	_		100						400 Se	_	1773.33			4877.06		600.06		561.08	_	514.08			_	28.58			4296.83	\neg	Run Time (hr)
8	8.8	8 8			8 8	8	56 56	_	8 8	8	8	ŝ		_		8 8	8	8		8	8	8 8	8	έ	8 8	8	8	8 8	8	8 8	ŝ	8 8	8 8			8 8	\$				· &	8	8	ŝ	
			25.10	_	_			3	26.66	_				24.00	_		_		8			_		_										2 8		_			26.80	6				25.40	WWTP Influent NH3-N (mg/L)
	80.78	_	_		_	_	182,00	_	8 8					É 5		224 08	_		_	8 8		8	_		_		_	8 8	_	700		_		201.00		228 00			_	201.00	8 8	78.00	8 8		WWTP influent CBOD (mg/L)
8 8	8 8	8 8	28	80.08	8 8	8.8	20.00	, <u>s</u>	7 8 8	8 8	8	8	8 8	1 E	8	8	8 8	200,00	8 1	8 8	36 .80	9200	3 2 8	8	8 8	82.08	8	8 8	5 8 8	20.00	8 8	8 8	8 £	<u> </u>	124.88	28	8 8	6.00	8	8 8	8	8	8 8	160.00	WWTP influent TSS (mgA.)
ž Š	ŝ	§ 8	ś		ğ ğ	ē			5	1 25					125					725						8							ē												Studge Wasled from Asration Tank (gpd)
Ď į	8	3 6	3	ş	8 8	8	ã		8 8	3 5	ន	ã	ž ž	śś	28	8	ē	ž	ś	É É	ğ	ซี		ŝ	ន៍ ន៍	ğ	Ē.	8 5	ğ	Ē Ē	Š Š	125	ž		5 8	(15 K	ś	Ř	ž		35	Б. É	ž ū	Skudge Wasted from Membrane Tenk (gpd)
8 8	5	# 1	27	2	= =	: =	۰		i	8 3	ı ü	3	≅ :	: 5	29		¥ 0	.	Ģ.	2 34	ő	=		=	ű ű	: 2	2	ت م	=	= ;	: :	ī2			5		. ,	z	ā	i3		σ,	6	5 6	Total Mass Produced (Mrday)
	25	i	<u>.</u>	=		=			=		í		ŭ	ĸ			_	=		5	_		-		 		ŭ	ĸ				ű						ű.		•		ñ	-	3	Total Mass BOD, Applied (lb/day)
	ž	i	Ě	Ŕ		8			š		 		2	ŝ			6	Ē							ž		Ŷ	8		1.5		8				;	91	9		š	_	0.51			Studge Yard
17.51	20.42	8	13.80	11.13	ž .	2 2	17.01		18.55	17.81	ī	13.81	17.01	įį	17.81	ž		÷	ž		ž	17.81		ř	į -	22.26	<u>6</u>	ž 5	Ť	17.61	7 5	17.81	20.65		ř		79.60	Ē	17.81	17.51		29 68	17.81	17.81	System SRT (days)
			i S			(0600)	_						17160												38		-			12300		3900								8000				12400	Waste Studge COD (mg/L)
_		_	3			- E	_		1	_		_	 123				-					_			1280					1070		1230		_				_		917		_			Weste Bludge TICN (mgA.)
_	•				_	127			\vdash			_	191		_		;			_		_		_	ź		_			š.	_	Ē		_						38	_	_		Ŕ	Weste Studge TP (mg/L)
_	7,050.00	_	9.850.00	7,650.00		7,800.00			13,650.00		14,050 00		12,050 00	12,300.00	_		1.50 00	11,750 00		13,200.00		11,950			13.750		12,700 00	5,050		10,450 00		12,750		_			12,500 00	11,850 00		11.500		10,750 00	_	10,950 00	Waste Bludge MLSS (mg/L)
_		_	8 	-		5,600.00			*	_		_		9.700		_	8	_ 8	_	9.660		8			10,500 00		8		3	7,800		9,400.00		_		_	8	8		8,550		8	_		Waste Studge MLVSS (mg/L)
		_	8 7.1	6.96		8			╁-	_			707	2	-	_	_	727		7.20					725		_		3	241		8				_		7.17	_	7.29	_		_	724	ьн
-	29.5		29.60		_	29.00	29.50		29 40	_	27 00	28.00		28.90			28.10		79 00			29.00		8 8		_	30.90		28.00		_	26 88	36				50.00				—	32.20			Temperature (degrees C)
_			1,671.00			8		_	Ť	_				1,924.00					2,150,00			ě			1 354 00		Ē	8	¥ %	š		Ē	18				1,544,00				_			1.654.00	T
_	8	_	8 8 •	8		- 8	8		+		- 8	. 8	636.00	8 8	8		8	8 8	8	8		8		8	38		8	8 8	8 8	8	_	8 158 00		_	_		8 8	3 8	8	~_		- 8		88	COD (mg/L)
_		_	8	3	_		_		+				8	_		_			340 00	_		_		_	8						_	8						_		-	_	_		_	ALK (mg/L)
_	 š	ŝ	8 8	8		0.00	0		8		-		ŝ	8 8			ž		00	 8		1 10		9	0 70		1.10	8	, i	1 10		í 8	8				0 8	. 8	8	ě :	ē	8		88	DO (mg/L)
	8	_		ž.		å			1,3	_	8		ž. 8		_		179 00	8		56 96		15 8 88	-		8 8		8		<u>.</u>	8		ž 8					§ 8	18		ã 08		152.00	_	153 OS	Food CBODS (mg/L)
	10.00		34.88	10. 18		ŝ	2	_	112.8	_	8		120 00		Ŕ B		20 00	ě		ë 8		156.00	_		6 8 68	_	56.00		š 8	8 8		ğ 8					132 ag	8		152 88		9 8	_	š 8	Pood TSS (mg/L)
_	Š		22.70	27.00		Ì	:		24 88		2	3	23.20		ž	_	8	3	3	8		20 56			22 36		20.60		2 8	26.80		22 00			_		22 46	30		24.6		23 50	_	25 10	9413-11 (Mg/L)
_								_	624																															_					PRIS-M (mg/L) (ASL Check)
_		_	8				<u> </u>		1	_		_	8					ê				_			ŝ	_				8		8								28					HOEMOS-H (mg/L)
_			ĝ		_		<u>.</u>		+				8					8				_			-					36.70		35.80			_		-			28.30			_		FICH (mg/L)
_			27.0						\downarrow	_			£	_			_	\$ -				_			8					39 79		35 83								28 50					Total Mirogen (mg/L)
_			š		_	-	•		\perp				8					<u>.</u>		_		_		_	5		_			å	_	ġ.						_		8					Total Phosphorous (mg/L)
_			708		<u>.</u>				708			N.	23		7 10 2		_		È	8					. u				7.25	. i			ш.					, w		ž	_			723	pH
_			31.00 5.00				29.50 6.70		_					3 10 3 10					1 8			3100			31.80 5.20	_			31.50 4.70				31 00 150					37 08 370							Tomperature (degrees C) DG (mg/L)
-	- 1	5 8	<u>8</u>	8 3	_		5 3	5	-10	_			5 167	_	ž		3		2 8	ē					2			٥	2	1			c				<u>q</u>		3 8	12				1.3	OUR (mg 02/Limin)
10,300.00	7,300,00	2,000.0	1,250.00		8.560.00	a. Mo. o	7,100,00	5,250.0	4,350.00	14,500.00	12,550.00	11,000 0	17,400,00			1 8008	11,350 0	0,050 00			12.200.00	0.500		-		192500	13.000	11,050 0	11.600.00			13,200,00	11.6000	_		13,9900	13,1500			12.180.80		13.000.00	9,9600	10,050.00	ALES (mgA.)
8	_		6,500.00	_	5 8 8		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	_	90 00 00			885000	9		7 050	<u>б</u>	90 8 4 400 US		888000	2 85c 00	8 8	2000			90000	5	8 8	_	7,900 00	7.50000		8 8 8 8		_		<u> </u>	9,650,00		73000	8 850 00		0 0000		7.50000	er Asis (milty)
		•	8		\$		•		. 18	•		o	8		8		ō		¢	6		•	•		ē		-		۰	ح							٥		~				•		

Table C-2 ZenoGem Water Quality Data

TO MT AND AT EVENT 12)	TO MT-EMBAT 11)	TO MT-EVENT 19	TO MT-EVENTS)	TO INTERNET 7)	CARENT EVENTS SAME	Characterity	B(HOPELAL)	ALAT & OPEN		•			•			•		>		l =	ž	.	<u> </u>	5 5	: :		ä	ā	ü		ı	=	=	
									MAX.	M	MARAN	МАХ	Ę	MEAN	MAX	2	E A	Ē	ECAN	н.	•	X :		Thu 10204	u		_	22	Fri 10/22/10	Thu 1921/50	Wed 10/20/88	10/19/00	Mon 10/16/98	Dale
_		_	_																	1			582.50	SE2 30		5756,50 5780 50	5731.50	5708 00	5683 00	5860.25	5625 75	5612.25	1580.75	Rum Time (hr)
5	8	6	8	50		ŀ	8 6	8	50	Ī		10,00			9.50	ğ		8 8	-	8	Ē	ŝ	8	6		5 8	8	8	8	8	ŝ	6.50	8	Permante Pleasure (gpm)
7	8	28.60		27.53	1	-!		\$1.53	37.36	24.00	27.46	32.80	21.00	26.40						31 00		-			3	8 8					_	31.36	29,00	WWIP Influent NG- (mg/L)
3	2	173.80	8	174.73	171.9	77.75	324.00	702.17	280.00	142.00	179.25	359.00	9	178.96	407.00	148.00	268	25.8	244.27	67 00 ·	8	ğ 8	21.08	8 8		7 4 8	8	8 8	8	171 00	178.00	8 8	152.00	WWIP Influent CBQ (mg/L)
	5 ,00	190,00	212.00	153.45	18.57	152.62	774.13	194.00	8	124.00	1	248.00	¥	152.32	296.00	8	77.13	2120.00	12.91	80.00	8	100	8	8 K		78.08	28 08	140.00	128.00	180 08	56.00	* 8	180.00	WWTP Influent TSS (Mg/L)
3	191.67	150.00	90.00	125.00		110.07	8	92.50	350.00	100.00	175.03	175.00	75.00	112.00	150.00	8	8	8 8	3	28	ğ	8	125	ž è	ŝ	ž ž	ŝ	125	ž	125	ŕ	ន៍	35	Swilge Wasted from Aeration Tank (gpd)
	237.50	225.00	112.50	1411	127.78	ž X	123.00	124.17	400.00	100,00	230,42	250.00	70.00	133.01	225.00	8	1	5 6 6 6 6 6 6	116.25	ŝ	ĝ	8	ğ	8 8	3 8	8 8	375	125	28	200	8	ě	ŝ	Bludge Wasted from Monthrane Tenk (pp
i	28.57	21.77	1.57	16.90	10. 2	3	1 27 12 12 14 12	17.85	ż	Š	24.82	42.87		14.42	42.33		77 15	E E	ě	33	å	27 2	.	i 6	iā	* £	ŧ	- 5	á	8	ä	ă	8	Total Mass Produce (Ib/day)
:	12.02	12.25	Ë	1215	72.KJ	1270	37.E3	16,40	16.70	252	1217	21.00	7.46	12.72	30.79	i i	10.37	10.00	17.57				17	=	:	ā	_					_		Total Mass BCO, Applied (Briday)
	ķ	2.00	3	Ę	î	=	3 8	à	ě	9	200	3.30	9.3	1.14	2.93	5	Š.	2 2	127				<u>.</u>	b	8	345				_		_		Bludge Yield
	13.29	14	20.03	15.65		19.78	18.70	10.01	22	Ē	ě	31.80	12.28	18.25	22.26	Ĉ:	3	í	27.28	8.16	8.71	3 6	i .	6.50		2 20	k	1781	3	16.89	ï	Ξ	6.28	System BRT (days)
	14400.00	13400.00	19800.00	17100.00	13,986,47	940.23			4.400.00	8,100.00	11,420.00	18,000.00	2,990.00	10,344.71						8100						0600							ğ	Weste Studge COD (mg/L)
	1004.00	879.00	M2.00	1280.00	1,184.67				1,004.00	734.00	200.00	1,740.00	883.00	1,181.65						754	_				_	971				_		_	6	Wasto Bludge TKN (mg/L)
	155.00	108.00	127.00	215.00		195.62			183.00	108.00		215.00	124.00	158.41						124	_	_			_	Ē				-			ź	Waste Studge TP (mg/L)
	7650.00	9650,00	7800.00	12670.00	19,000.00	12,200.00	16,371,43		9,880,00	7,380,00	1,242.75	15,950.00	10,100.00	12,123,51	19,150.00	13,250,00	10.00			9.400.00		-	7 700 00	8,350 00		7.360 00		_	_	_		_	_	Weets Mudge MLBS (mg/L)
7000		7480.00	5400.00	9425.00		9.003.33	_		7,450.00	5,800.00		١.		9,061.11						7.200.00				0.0000	_			_	_	_				Wnote Sludge MLVS (mg/L)
:		7.04		7.20	7.20	7	2 2	723	724	:		77	Ē	7.16	7.65	ş i	ž.	7 5	7.15	720				ì	_	- £			_	_				pH
•	29.08	2	29-25	28.71	5	20.02	8 7 8 6	25,52	2	27.90	28.74	32.90	27.00	29.65	30.00	8	27 03	2 2	25.45	28.10			20 :	20.20		28 20			_					Temperatura (dagra C)
	1585.00	1894,87	1796.50	1950.29		1904.04	2,137.84 1,875.00	1,982.00	1,960.00	1,471.00	1,638.54	2,450.00	1,255.00	1,586,48	2,840,00	1,560.00	2 128 28	8 8	1,758.43	1 716 00		1	539 00	8 8		1,590.00								Conductivity (u8/cm
		448.00			36 .08	OC.LIK	619.67	300.00	8	282.00	37G.00	112.00	156.00	362.74	730.00	428.00		780.00	530.00					_		292.00					_	_		COD (mg/L)
	220.08	360.00		34.00	8 1	2	122	19.8 19.8	8	120,00	HI. 10	380,00	330.08	348.18	542.00	1 S	17		425.50		_				_	96 08						_	320.00	ALK (mg/L)
	90.90	0.83	0.8	103	_	- 1	2 2	171 2	120	0.50		1.70 2		9.01			t			0 98				9 8		8		_	9. 8	8	8	ĝ	ŝ	DO (mpL)
	F 8	157.00 1	8.98	194.20 1		- 1	279.08 1 279.00 1	27.67 2	21480 5	72200		278.00 2	Ě	1 867291	•		- 1		244.27	28 00			8	8		8	_		_	_				Feed CBODS (mg/L)
	8	84.00	04.00	107.20		ı	15 E	ι	978.8	72.00		312.00							231.36	24 00	_		570 00	8	_	72.00	_		_	_		_		Food TSE (mg/L)
i	17.20	24.05	8	23.10		-1	# B #	26.03	2	17.20		29.00					- 1	8 8	27.06	28 30			22 00	8	<u>;</u>	8			_	_	_			HISH (mg/L)
						Ē	21.90 0					1		8.24 G			8			_					_					_	_		_	MMS-N (mgA.) (ASL Check)
	0.01 10.00	0.02 43.30	0.01 42.40	0.04 34.00		MC 29 BEO	0.17 74.87	L	202			1					- 1			001 48			_		_	ğ				_			0.01	H02NO3-H (mg/L)
:	16 M 20		8 4241	24.04		١		10.86	44.80 44.91	30.00		75.40 79.52	24		ĺ.		- 1			8						45.00			_	_	_		8	Litra (miler)
		2 22.23				47.76	78.04 14	110.08		10.00			23.56				- 1	18 PE 25	2	5-			_			150	_				_			Total Miregan (mg/L
: -	3.87	5.45	697	7.4	22	+	- G	+-	7.	1.87 E.	_	⊢			⊢	_	-+	41 80	_	8				_		8	_		_		_	_	3.07	[mgt.]
793	31.00	7 03 31.00	23.70	05 30.04		ı	7.12 28.08 7.39 24.80	724 28.11	7.27 31.00	6.07 28.		7.70 34.00	8.84 27.70	710 31.20			- 1	763		7 27 27	_	_	27 00	2 6	-	716 2800				_			_	jeli Temperatura (degra
	11	8	70 8.44	3.80		ı	DE 1.00	11 5.93	7.30	25.46 4.80	29.25 6.28	7.00					- 1	27.00 8.00		27 00 6 10	_			27 40 6 10			_		7 28	536	8	9	5 8	C) (me/L)
	_	1	•	Ē	Ē	ŝ	2 2	0.70	ŝ		1.07	š	Ē	ŝ	5	È	ş	7	8	8						8			_		Ç			OUR (mg OziLimin)
7716 21	7878.00	7770.00	8378.00	12100.00	10,361.11	11,867.38	18,078,08	15,528.79	10,300.00		7,228,00	18,800.00	7,900.00	11.777.44	19,380.00	11,500.00	18.7	26,280,00	13,777.43	7 400 00	\$ 200 00 00	8,800 00	7.560.00	6,850,00	7 1	8,750.00	,390 00	00 00	8.450 00	7,700 00	5,300 00	8,400.00	8.860 00	al SS (mg/L)
Ü				1		- 1		1			K418.73	11,100,90			1		- 1	19,900.00	_	5 550 00			5.000 00	_		4 950 00				_	_		_	t

ZenoGem Water Quality Da

,							_								_			_				_			_		_	_	_			_					_							
	sucronigeert & Inverser	94.52					91 93				8					98 58					23.12				_			8					8						8				ž	
	negatibl late? 4*						70.63				63 23					8					56 15							ž.					8						29 FB		•		22 28	
	A ALK Consumed	2				5 U				-	28					\$												59 5,		_			95.7		•								57.29	
MOVALS	evorant alnomin d	19:56	29.57				2 3	9	?		2 8	£		æ 8:		39.65	10 50	-	26.93		94 70						T	8		E \$	\$		26 86		R 2					5 5	8		96 88	
¥-	CEGOS Nomovel	29.62	3				8	8	}	_	£	8		E 8		89 68			8		5 g						T	5	:	28 88 88	8 27		8		8 8			96.59		25	8		\$	
-	Invested 000 A						Z 9		_	_						8									_		-	_	_				\$6.76	-					_				75.76	
-	Invented BET #	99.78	2		_		5	8			2	8	_	Į.		82 S6			2 8		2 8	_					t		}	8	36 95		# S		# 52 # #			28	_	£	25		i 2	
-	HAC (CLITMIT)	00:000.9	3,110.00								931.00	8 29	•			3,300,00	98		_		8 00	_					t	8	_	300 00			00 000.		_	_	_	02 005,		200000			3200.00	
-	(CPUNIOS INL.)	Ľ	8				8			_	8					3.	8				-	_					╁		<i>;</i> 	-			80 06		8			8	_	8			80	
-	(Chungo mil.)	\vdash	8		•••		- 8				8	8		_		00 61					8				_		+		3	_	_		8		8 		_	000		210.00			8	
- ا	(Japan Tobal Collions	2	_					_			5	-				8		_			2 280				_		+						0.18		2	_		- 8	20:0	ž		_	0.15	
	(Agm) requests lated automorphism lated	t <u>-</u> -	-,-			-	8				31.57	_							_		29.26						\dagger	—			_			-			-						- S	
-	(7/Ew) HOU	<u> </u>					200 25				2.17 31	_									306		•				+		5 	_			- 86				_		5					
-	(Agm) N-COMRON	ŀ									8					9			_		28.20 3.0						+		3	_			- 8						*				35.	
-	the Chlerine (mgA.)	├					۶ 	В	<u> </u>		8 :	8 8	8	8		= 8	8 3	. 8	8		~	_					+		8 8 8	<u>-</u>	8 8		_	_	8 8	8 8				8 8	5 8		2 8	
<u>.</u>	(Agm) antholic tate	-	_					8			_	8 8	_			_	8 3										Ì				3 98					8 8	_	_		8 2	_	_	8 8	-
ERMEAT	Heal (mgA) (ASL (sheek)	-							_								_										1	_	_			_		_										
ľ	(Jew) N-SH	- -	1.0				8 8		8		0.03	8		8		0.0	;	2	620		¥.		-				1	_	8	8	60		8	_	0.35	2 2		5	3	8	0.24		8	
	(76u) 52	+-	8.0				9		8		9	\$		ê		9		_	8		8,							_	8	8,	8				20			5		Ŗ	620		R	
١.	(1/8w) sqoe:	2 2	2.52					}	2		0			0.87		š.			0 72		0.58	_			_		+	_		160	2			_	2.72					0.0	8	_	<u>:</u>	
	sascheell emiste (Age	4-							_			_				_											1		_				- 5		360 00	_		į		86			Ř	-
	THE (MAN)	1 × ×				140.00					120 00					- 2 8			_		_						1		55 66			_	- 8	_	230.00				_				ž 8	-
	(1)flw) go	4_					- 2			_				_		2005		• «							_		- -		40 CO	·	۸ و	,	- 1		Cy.	vr •	,		1 =				1 00	
l	(RLIN) Aupton	+-	~				_	8 8				8 8					0.13				_	_					+	_			20 8	~_		8 8		8 8	 3				8 8		8 8	_
	(шаудя) Ацефопфио	ل	1,620.00			_	_	1.0000	_			1,880.00		1,710 00		_			00 002.1								_		300.00		1,710.0			1,700.00		1.670.00			1,740.00		1.750.00		780 00	_
	essides) empredue	28.00 28.00	27 00 72 74 7		_		25.00	3 95	5. 5.		25.00	26.00		28 00		29 27 00	28:00	8 5	26.80		_				_		4	_	22 28.08	£3 27 BK	27.50	-			28.00	27 00			2 2 2	28 08 2	2 2 2		744 29 80	5
ŀ	(TVRW) 9006	8	27					3	8		780.00		3	170 00		8		8	80		8	_	_	_	_		+	_	8			3		3	7 00:000	8		_	<u>`</u> _	7 00:000.1	8	_	920 00	-
		8						\$ 	8				ĝ 			- 8			061.1		96						4	. 8	8 07 07	1,120				3					§ 		9E,			-
	TABB (why)	9, tg	5				_	8	8,500 00		7.450 00		8	9.500 00		7,600 00		8.350.00	9.050.00		90000							7,800.00		9,900.00				0000	9,600.00				10.480.00	8,900 00	0.0000		8.756 00	-
YANK	(1 /Pu) 881	13,130 00	14,900.00	0.000.00	5.750.00	6.473.00	00 000.0	8	9,200 00		10,400 00		10:00	12 000 00		10 900 00		00 000 11	12,700.00	12,000.00	3,000	80.0	00000						10.050.00	13,750,00	14,100 00	25000		17,300,00	13650.00	13.250.00	900	15,700.00	13.650.00	1155000	11,900.00	13.050.00	11,850.00	17,550.14
APRATION TANK	(nimLASO gas) Fil	\top						3			75.0		2			8		9									1		8.0	80				80	2					20			8	_
	(300)	xa g	Ŗ	8 8	}	£	8	3 g	8		9 9	9.10	8 8	8		- 8	9.	8	8 5	_					_		1	_	8 8	3 8	Ŗ.	R -	_	8 8	8	8	e 6		9 9	8	8 5		8	2
	ээхийэр) алгалайы	8 2	8 2	S 5.			2 20	22.00	26 40		8	23.00	8 5	8		8	8	8	2 2					_	_			_	8 8	3 37	8	8		8 8	8	27.00	2 20		2 2	8	8 8		2	28.82
-		# 3	_	8			_	8	8	_	7.09		8			78	_	8 7	-		_	_					\prod		7.12	7.33		2	_	R .	7.37	2			8	8.81 E.81	8	_	7.11	_
	(1)4ml 1000	8						725 8	ğ		9		8	1,490 00		8	_	<u>\$</u>	80.08			_							80	1.60		1,570.00		1.070.00	3	2,100.00			1,760.00	1,460.00			300 00	-
	(M) andT a			2 23		2 2 3 3 3	8	217.08	241.08	8	30.00	8 75	8	, 8	8 7	8 8	8	8	9 5	5	5 3	9	60 03	2 2	663.00	80.09	60.00	\$ 3 6 5	25.		26.	2 3		2 1			8 1	1013.5	100 de	8	1708.33	1157 56	1205.04	122
	•	Mon Zymys	Tue 2/8/4	Thu 2/11/8	See 2/13/8	Sun 2/14/16 Mon 2/15/19	Tue 2/16/90	Wed 2/17/94	Fel 2/18/6	See 2750	New 2/2 1/2	Tue 272376	Wed 1/148	F11 2724.	A 277.75	344 27288	Tue 3/2/8	Med Sold		5	A. 277	1	Wee 2/10/8	Mark and	7	Mon STERN	Per Per	See Month	Man 3/23/81	Tue 3/25/8	The 3/25/5	1	327	Mary Printer	Wed 3/21/98	Thu 41/8	E S			Wed ATT	1	Se 4105	25.5	14 4 5 W
ŀ		+			_		_	-									_								_	_	-															.—	_	_
																																				_								
	New York		•																									-							-	-								
- [1																																										

				-				一				u-		Т		e					-	_	-	_						p				_	_			~
_	auchachtearff a'			97.93				8				92 56		_		- S					2			2						38.77			2					8
	negotifilistol a Isvanofi			76.37				8				57.71		_	_	65.78					\$			36.38						6: 81			65 45					£ 25
M	Permunad XJA %			65 87				ě				37.57				60 09				\$ F				5					9				58.33					\$
EMOVAL 3	romefi alnommA if	85.78	3	57.58	18 87	\$		47 50	15 26	92.00	2	8 2:	8	Ī	3	2	;	5	ŝ	5 65	2	ķ	8	8		£	\$		ş: B:	\$6 60	_	8	8	,	\$ \$	95		26 78 20
_	levomen 20083 #	\$7.86	\$	8	98.86	\$		2.	\$	8		59 65	8		S:	35.75	26.66	į	3	98.73	9	,	98.86	30		3	ğ.		ŝ	J.		85 66	8.	-	2	g g:		
-	is cod Removal						-	26 96								3								3									26					
-	iavomeli 887 2	23 85	2 8	39.55	28	8		 8	89 66	. 2	 }		8		g g		\$					3 k	F. 8	_			88			_	_		ē	_	 B S			÷
	ньс (сълчет)	2500.00		3,000 00	3.400 00			3.200.00	3,000,00			200 00				00 0091	2.200.00			00:000:+		3		9	90 005				9	3	2 200 00		1 900 00		8 15			_
-	Fecal Coliform (CPL/100 mL)	90.00		92 26	8			Š.	8 2			8	5	3		00.61	96			2 08		 8		- 8	8 22						_							20.00
-	Tetal Collion (CFL/100 mL)	30.00		90 00	00 05			8 8	25.00		_	8		3		25.00	8 2			22 20		8			8 8				_		_		22 00					8.6
	aucroriqaoffi ialoT (Agrii)	-		0.28		-		98				75.0				- Ke					6.23	_								376	_	13,	37					2.72
-	Ngen) negoziki kata T			2 43				14 28				9	······								30.14				 }	-				95 02			8					5
	TKN (mg/L)			50 40				01.61				97.53	:			Ę					3					_		•		- 8			8			_		8
-	HOTWOON (WOL)			- 8		_		•						-		- 04 61				•	\$									9	_	_	8					2.61
-	Jem) anholds em?	├-	70.0		5 B	3 5	?	- 70.	g 8	3 3 3	 §		8 8 1	8 8	£6.0		8 8	20.0	E	8	28	* 8	86		3 8	8 8	300		80		8	50.0	14		8 3	8 8		2000
-	Figur) entroid:3 ia201	-			_	3.5				8 8 8			3 8				8 8					6 8			8 8	-					31.0		30			3 3		3 3
ERMEAT	CIPPER)					- 9			5		_										_						_						_					_
-	(Jam) H-CHH	- -	2.18	6.93	52 kg			4.20	- 92		3.	9	3	R.		<u>e</u>	9		20.0	200		8	20:0		<u> </u>	0.07	200		0.07	<u>2</u>		ă	8		B0 0	0.07		027
_ _	(Jen) 881	ş	0.20	0.60	250	5	ş	0.20	8	3 3	3	5	5	0.20	Š		0.0		8	8		8	0.20			0.0	8		_				8	,	8			8
-	(76m) 10010	90	0.24	0.08	236		ò	-	2		<u>*</u>	8		0.22	-	E	<	<u> </u>	7	1.0	_	8	2.07			980	8		8	;	;	90	0.0		0.62	5		
_	searchast materials	_		382.00				338.00				ş	Ř							8	_				8 8 ——					88			8	<u> </u>				
_	ALK (mg/L)	1_		326 00				260					3 5			90.04					_				8					<u>8</u>	_		8					<u>8</u>
_	(76m) 000	L						1300																	8 E						_	_	- 8	!				
-	(UTN) yMbidiu)	8	8 8	- 8	8 8	07.0	8		-	8 8			8 8		00 u 23	8	8 8	3 8	8	- 8	8	8 8			8 8	8 9			90		3 8	8	8	8 8		0 0 24		9 9 15
-	Conductivity (uS/cm	- P			1.880	- 350	1.920	1.674	188	1,672	5		3 3	2 5	ğ		2 8	88	178	98	3	22 52	2		8 3	5	3 %		56			8	96	8	98	8 2		1,510 00
-	compositive (quilibre	1 ×	8 8			8	8 5	29 00		2 8 2 2 3 2	29 00		8 8		28 00)		90.00		8			8 8	29 50	_	8 8 8 8	29 00	8 8		32.80	_	3, 5	31.00	- S			8 8		3 8 8
┝	4-4-11-1-11	8	8	8:	5		8			8	8		8	8	8			<u> </u>	8		3	# 180			8 	8			00 010		€ 	8		`	8			8 ,
-	(Julius) \$008;	=	0 1,140	0 1.370	-		Š	1,180			0.57		§ 		026	<u>8</u>		1	§		}	1 020	8		2	8	1300			_	<u> </u>	5	70.00		91500	*		25
	(JOW) BEAT	9.850.00	10,900 00	11.600 00	92.5		10.450.00	9,509 00			12 050 00	14,500 00	9 900 00	7.950 00	00 000	350.00		8	6.550 00	5	8	6.300 00	7,750.00		6.000.00	7.350 00	7,000 10		7 000 00		888	7 850 00	50		8,700 00	9,000,00		8,550 00
¥	('Vew) EST	8					0 0				-			8 8	2 8	E 0			8 8	8 8	8 8	8 8	8	8 8	_		e 0	8	8.8	8	10.000 00	10.450.00	13.800.00	8 8	11,300 00	11,600,00	13,900,00	1,300 00
È.		13,766.00	15.200.00	12,850.00	15.300 00	14.300.00	14,400,00	13,500 00	13.800 00	13,150,00	11,950.0		13,200.00	11,650,00	00 000 11	00 000 11	9.700.00	8,250.00	9 100 00	8.150.00	8.00	0.150.00	10.450 00	10,100.00	8.100 80	9.650.00	9.600.00	11,350 00	9.150.00	10.300	<u> </u>	. ž	Ω 5					
AERATION TANK	(nimLASO gm) Rib	+	14,700,00	12,850.00	15.300.00		14.800.0	15,000 00		0.00 13,150,00 17,000,00	11,950.9			0.49 11,450,0	9.850	11,400		9.400	9001	81.50	_	0.56	10.450		8,100 0	9 57 9.650.00	9,600	11,350	0.46 9.150		0.01			2 z z	960			38
AERATION I		S .		0.71				690						5				ş		3	\$	_			_	15.6		11,380	\$		2	3 8	3	3	986	8 8		9 R
-	(Jan) O	0 06.		120 06:1	57	<u> </u>	23	69D R-	8		ē		E .	1.80	62.1	9		8 R	\$		8 8	2.80	R.		9	256 912		36.11	\$	54	8.		9	8 8	080	8		
-	(Jages) Stutenegers (Jages) O (And LASO gen) Stute	7.09 2840 190 059	2890 190	17.0 00:1 00.72 02.7	07.1 08.75	38.00	29.00 2.00	120 049	8 00 90	6.83 29.00 1.90 0.61 29.00 1.90	28.70 1.80		7.33 28.79 1.50 0.73	29.50 1.80 0.49	20.20	88	96.2 25.96	696 2980 300 040 2980 430	30.00	4	29.00 4.70	703 3100 290 0.56	PZ-1 000 X		704 3050 430 048	256 012 050F \$0;	3010 390	360	707 1200 120 0.48	51	550 00: 00:1	3 8	9	95 - 95 - 95 - 95 - 95 - 95 - 95 - 95 -	685 32.00 150 950	08 50 08 50		7.25 31.80 1.40
-	(Jages) Stutenegers (Jages) O (And LASO gen) Stute	1,226.00 7.09 28.60 1.90 0.59	2890 180 1590 00 28.00 1.90	120 001 0022 002 000961	27.50 1.70	26.00	1 720 00 29 00 2 10	1,546,00 6.94 23,00 1.20 0.69	8 9 9	1 420 00 6 40 29 00 150 0 61	28.70 1.80		2900 120 073	2650 180 0.69	1 - Main 28.20 1.20	895	R 2 55 00	23 80 430 040	30.00 1.60	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	20000	1070 00 7 00 31 00 2 90 0.56	1240,000 1230		300.00 7.04 30.50 4.30 0.48	750 012 0500 501 000601	390		1 096 00 1 00 21 70 1 00 046	8	1 440 00 771 1100 130 053	02 1 00 11 00 00N	99	20000	1 20 00 6 85 32 00 150 9 60	3.16		745 00 7.25 37 80 1.40 3.20
-	hengeb) antrocente [(JApm) O (minLASO gm) RUs	(253 0a 1,220 00 7 09 28 60 1 90 0 59	1277.06 28.90 1.90 1.00 1.00 1.00 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 28.00 1.90 28.0	1349 56 1369 06 1 960 00 7 32 27 00 1 30 0 71	07.1 02.75	26.00 1.50	1489 58	1517.0A 1527.33 1 540.00 6.94 29.00 1.20 0.69	00 00 00 00 00 1951	1505 09 1 420 00 6 43 29 00 1 50 0 61 1 10 160 1 150 1	1434.0N 2 630.00 28.70 1.60	Treat on	1725.08 1 106.00 7 33 28 70 1 50 0 73 1725.08 28 00 1 20	1753 06 1 110 100 6 853 30 00 1 40 0 49	000 000 000 000 000 000 000 000 000 00	895	R 2 55 00	23 80 430 040	30.00 1.60	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	20000	1070 00 7 00 31 00 2 90 0.56	1240,000 1230		300.00 7.04 30.50 4.30 0.48	750 012 0500 501 000601	390		2377 96 1 096 00 7 07 12 00 1 20 0.46	2401.08	2425.04 1 440.00 7.21 31.00 130 0.53	2473.08 NB0 00 31.00 1.20	\$0.102	256904 20000 736 3700 140 038	2593.64 1 20.00 6.85 32.00 1.50 9.60	2617.08	5665 06	2713.09 745.00 7.25 31.80 1.40 2726.80
-	(Agm) 2008	41449 (25304) 1,20.00 7.09 2880 190 059	1277.06 28.90 1.90 1.00 1.00 1.00 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 28.00 1.90 28.0	120 001 0022 002 000961	07.1 02.75	26.00 1.50	1 720 00 29 00 2 10	1517.0A 1527.33 1 540.00 6.94 29.00 1.20 0.69	00 00 00 00 00 1951	1505 09 1 420 00 6 43 29 00 1 50 0 61 1 10 160 1 150 1	1434.0N 2 630.00 28.70 1.60	1856 08	1725.08 1 106.00 7 33 28 70 1 50 0 73 1725.08 28 00 1 20	1753 06 1 110 00 0 683 30 00 1 40 0 49	000 000 000 000 000 000 000 000 000 00	895	R 2 55 00	23 80 430 040	30.00 1.60	4	20000	1070 00 7 00 31 00 2 90 0.56	1240,000 1230		300.00 7.04 30.50 4.30 0.48	750 012 0500 501 000601	390		2377 96 1 096 00 7 07 12 00 1 20 0.46	2401.08	2425 36 1 460 00 7731 31 00 130 0 53	2473.08 NB0 00 31.00 1.20	2521 08	256904 20000 736 3700 140 038	2593.64 1 20.00 6.85 32.00 1.50 9.60	2617.08		2713.09 7.25 31.80 1.40 2734.80 7.25 31.80 1.40
	(Mgmt) adder (Agmt) adder (Agmt) adder (Agmt) (Agmt) (253 0a 1,220 00 7 09 28 60 1 90 0 59	1277.06 28.90 1.90 1.00 1.00 1.00 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 28.00 1.90 28.0	1349 56 1369 06 1 960 00 7 32 27 00 1 30 0 71	07.1 02.75	26.00 1.50	1489 58	1517.0A 1527.33 1 540.00 6.94 29.00 1.20 0.69	00 00 00 00 00 1951	1505 09 1 420 00 6 43 29 00 1 50 0 61 1 10 160 1 150 1	1434.0N 2 630.00 28.70 1.60	Treat on	1725.08 1 106.00 7 33 28 70 1 50 0 73 1725.08 28 00 1 20	1753 06 1 110 100 6 853 30 00 1 40 0 49	000 000 000 000 000 000 000 000 000 00	895	R 2 55 00	23 80 430 040	30.00 1.60	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	23.00 4.75	1070 00 7 00 31 00 2 90 0.56	1240,000 1230		300.00 7.04 30.50 4.30 0.48	750 012 0500 501 000601	390		2377 96 1 096 00 7 07 12 00 1 20 0.46	2401.08	2425.04 1 440.00 7.21 31.00 130 0.53	2473.08 NB0 00 31.00 1.20	\$0.102	256904 20000 736 3700 140 038	2593.64 1 20.00 6.85 32.00 1.50 9.60	2617.08	5665 06	2713.09 745.00 7.25 31.80 1.40 2726.80	
	(Mgmt) adder (Agmt) adder (Agmt) adder (Agmt) (Agmt) (253 0a 1,220 00 7 09 28 60 1 90 0 59	1277.06 28.90 1.90 1.00 1.00 1.00 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 28.00 1.90 28.0	1349 56 1369 06 1 960 00 7 32 27 00 1 30 0 71	07.1 02.75	26.00 1.50	1489 58	1517.0A 1527.33 1 540.00 6.94 29.00 1.20 0.69	00 00 00 00 00 1951	1505 09 1 420 00 6 43 29 00 1 50 0 61 1 10 160 1 150 1	1434.0N 2 630.00 28.70 1.60	Treat on	1725.08 1 106.00 7 33 28 70 1 50 0 73 1725.08 28 00 1 20	1753 06 1 110 100 6 853 30 00 1 40 0 49	000 000 000 000 000 000 000 000 000 00	895	R 2 55 00	23 80 430 040	30.00 1.60	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	23.00 4.75	1070 00 7 00 31 00 2 90 0.56	1240,000 1230		300.00 7.04 30.50 4.30 0.48	750 012 0500 501 000601	390		2377 96 1 096 00 7 07 12 00 1 20 0.46	2401.08	2425.04 1 440.00 7.21 31.00 130 0.53	2473.08 NB0 00 31.00 1.20	\$0.102	256904 20000 736 3700 140 038	2593.64 1 20.00 6.85 32.00 1.50 9.60	2617.08	5665 06	2713.09 745.00 7.25 31.80 1.40 2726.80	
-	(Mgmt) adder (Agmt) adder (Agmt) adder (Agmt) (Agmt) (253.0a) 1,220.00 7.09 28.60 1.90 0.59	1277.06 28.90 1.90 1.00 1.00 1.00 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 1.90 28.00 28.00 1.90 28.0	1349 56 1369 06 1 960 00 7 32 27 00 1 30 0 71	07.1 02.75	26.00 1.50	1489 58	1517.0A 1527.33 1 540.00 6.94 29.00 1.20 0.69	00 00 00 00 00 1951	1505 09 1 420 00 6 43 29 00 1 50 0 61 1 10 160 1 150 1	1434.0N 2 630.00 28.70 1.60	Treat on	1725.08 1 106.00 7 33 28 70 1 50 0 73 1725.08 29 00 1 20	1753 06 1 110 100 6 853 30 00 1 40 0 49	Frighting 1901 (8) 1 (5) (3) (3) (4)	895	R 2 55 00	23 80 430 040	30.00 1.60	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	23.00 4.75	1070 00 7 00 31 00 2 90 0.56	1240,000 1230		300.00 7.04 30.50 4.30 0.48	750 012 0500 501 000601	390		2377 96 1 096 00 7 07 12 00 1 20 0.46	2401.08	2425.04 1 440.00 7.21 31.00 130 0.53	2473.08 NB0 00 31.00 1.20	\$0.102	256904 20000 736 3700 140 038	2593.64 1 20.00 6.85 32.00 1.50 9.60	2617.08	5665 06	2713.09 745.00 7.25 31.80 1.40 2726.80	

Γ	avererigeoff # lavomafi			12.69					\$				5										21.98					8				9					_	£1. 69					\$ 93
~	nego viki eden Removel			96039					2 5	_				!		_		20 58					2					£ 0					7				_	17.18	_				88
-	Permenco XJA %			:					91. 29			:	_	F6 48		: S	_	5								_	_					1	£					17.59					25 98 26 25
SJAVO.	evomeñ alnommă 🔏	E 8	19 64	ŗ.		li be	\$ 72		p:	£		;				50 26	_	8	:	£ 8	75 66		8	- 1	E .	ie g		P. 8	¥: 66	3		_	 \$ \$	69.66		5 66		2 \$	5	3	2.5	_	
₽-	A CBODS Removal	58:82	28 88 			Z8 85	8			8					18 86	8	_				¥6	_	8	- ;		8		£	8 8				2 2 2	 E 8		8 8	_	26.62	6				16 66
-	* COO Vennoval	_		97.64	_							-				12.6							12'16										F.		_	_	_						2.2
-	lavomen &ET #	59.00	23.62			38 BE	3.8		18 66	- 8					\$	 E	_		_	EN 66	6		28 88	-	2 \$	99 83		58 66 66	F .		? ?		£.	0H 6+		_		¥.	8				
-	Hac (CLOWF)	000000		8	?		_	-	20 00.		 ;				00 000		_	8	_	90 04													2,000 00	00 000	_		_	90'00		3			00 000
-	(Selving mt.)	8				5	_		60	 E					£ .					900				-									8	- -				8 2		_			300
-	Total Collions (CFL/190 mil.) Fecal Collions	20 02				5		_	906	- 8					<u>.</u>					2.00									-				8	20 00 2	_			1200		·			8
-	aueneriqueerit inte (.f.gm) (.f.gm)	-		9					2.42		-	_		e					_	-			2		-			ç			-	-	ž					720		-			27.2
] -	Agen) negatifi lata:				3		_		. 0 4					 B	—		_		2				96.01					22 30					8 8		_	_		67.0			_		8
-	("Ngan) Min)				3				8					<u>.</u>					8		_		90 2					2 00 2	_	_			~ %		_			200					86.2
-	NOSWO3-N (wek)	-			· R	_	_		1540					2007		_			2									20.30					26.81				_	9 70 2					. 8
-	Free Chlotine (mgA.)	50:00	B 0		3 3	500	8 6 6			8 8	3 8			_	3.	8 8			8 8	3 0	3				8 0 0	8	_		8 8	50	3.0		70.0		80	50 0		_	60	8 8	800		80
w	Total Chlorine (mg/L)	-			8 8	_					3 3	_			3	_			8 8			_			2 0) 8				900	_		_				\$ 8			200
ERMEAT	JEA) (Agm) N-EH Chock)					_		_					_					-	8	¥0.0							_		_				_										_
	(YBw) (F)	80.0	8		è	9.03	20:0		40.0	- 1	9	0 13		8	Ę	3			Ê	ě	2	}	8		Š	80.0		8	88		8		200	60.0		8	_	8		8	900		0.0
	(JAgen) \$21	-	8		8 _	0.20	9		0.20		R			2 ~	90	£	_		920	0.70	020		020		040	80		200	9		5.		0.50	920		_		8	_	0.20			_
1	(76m) 9008;	8	0.29		8	ä	- 8		728.50 0.02			95		0.03	£ .	8			8	0.38	- 2	5	- 8		6 6	900		8 0	\$				60	0.20		0.0	_	9.13		å			-8
	seenbuck mulaig.	_			8 8				8			8		100 001		8	3		<u>ş</u> 8														8			-		8					312 00
	77K (MB/F)	 —			8 8 2			_	3	8		8		90 1	_	90 1							8										8			_		Ę				-	17.00
1	(UTM) vilibida.	١	. 8		51.0	61.0	¥ E		- 51.0		0 :	2.0		940	? •	R 3			910	5.0		2			4.0		_	<u>.</u>	5 C C C C C C C C C C C C C C C C C C C	6.0	21		51 700	8 5	5.13	=	_	22		91.0	8		0 14
	conductivity (uS/cm)	8 8			0.35.00	8			8		8 8	00 009:		90 0051	8	8778	3		8 8 8 8 8 8	8	8	3		-	8888			8	8 8 8	8	8		187.00	8 8		9		8	8	8 8	8		00 50#1
1	(:	8 8					8 8 8 8 8 8					32.20			8 8	_			32 00 25			В		3		-				25 000	-			25 00 25				_		8.8			3
L	H mmberature (degrees	<u>-را</u>		_	9 6	7.51	<u>я к</u>		337		, H	н		0 ,	7 41	ж -	_		7.45	7.35		<u> </u>			3		_	98	286				98 75	22	_		_	8 3		9 2			38
	(Jem) 1008	1.020.00	00000		940.90	365.30	8		720 00		965.00	Discussion Compa		1,100 00	810.00	8	3		642 99	775 00		8	5	Ř	1.040.00	810.00		00'089	8		745 00		915 00	8	300	770 00		905 00		90 009	755.00		620.00
	FARR (WBF)	9,300.00	9.400.00		9.150.00	9.000.00	R.750 00		6.450.00		2,300.00	2,450 00		6,400 cm	7 100 00	9			0,700 00	7 500 00		8 90 90	5	3	9,150.00	9 950 00		8,250 00	00 001 6		8 950 00		9,300.00	8	3	00 000 00		00 058	_	2,450.00	00 000		9 300 00
TANK	1782 (wôy)						11,700 000						10.300.00						9.050.00				00.001.01		12.550 00	8 95		8			00 056			8.750.00						10,190.00		9,850.00	
AERATION	(nim.Aso gm) Au	1_	= 2		8 C	3				_	5 2	•		ž ;		-		=	6 2/0						790	_=	_	17.0	2 2		-		8		-	. =		e e		8.	: •		2.2
		-	R 8	_			8 8	_			\$ 8 -	9			2 2	8					8	8		<u>.</u>					8 8	_			8	_		5 5				8 8	3 2		
	seedlep) surquedus	3 8					02 25			_					8 8 8 8		_		8 22			9 E		- - -						8 8				_		9 9				31.10			8
	•	4 ² .			7.53	, B.			6, 7		<u>.</u>			£	7 20	_			7.24	, ,				71.7	7 10			8	:				7.21	_	7 29		_	1.		8			<u>:</u>
	(1y8w) 900s	-	1.130 00	_	620 00	00 090	92.09	2	98		90 001 1	86 28 8		1.220.00	915.00		8		98 10	8		1.120 00		8 \$	1 140 00	8 6:		90 06:	9		8		822 750		8	832.30		00 000		125.00	847.90		712 00
	(म्() कार्या स		2784.83 2809.08	285658	2881.06	2929 08	297758	2899 BG	B2 250T	307306	312158	314508	316838		3241 OB		2000	3362 00	3385 06	343 58	3457.08	348108	352808	8 50 50	380106	364958	36730	3745	375208	3745.08	36190	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	300.00	391608	3839 08	3987.08	4013 OH	4004 83	2,780	107.06	129 58	5.	42.55 S. S.
	•	Wood Grische	Fri \$110	Sun 6/70/99	Mon 6/71/Fe	Wed 523/99	Thu 6/24/88	Sat 6/20/98	Sun 6/27/98	Tue 6/29/99	Thu 77599	Fri 7/2/F	Sec 773/98	Mon 7/5/90	Tine 7/6/89	The 7/8/99	Feb. 74	Sun 7/11/8	Mon 7/12/8	Wed 7/14/88	The Miles	Sec 777 200		Tim 1/70/00	Wed 7721.00	The 7/22/94	Set 7/24/80	Mon 7/24/94	Tue 1/27/98	Th. 725-0	Frd 7/30/98	Set 7/31/86	Mon 4/2/84	Tue 6/2	404 P/40	1	Set MYAN	Sun every	The seriors	Wed British	Fri STANS	See arional	Sun 8/15/90
		+				_					_				-				_																								
DI STATE OF A STATE OF																																											•
ı,	•	1																																									

Pege 8 of 10

_			_	_	_						_				_				_		_		_	_			_	-	_			_	-			_	1	_		_		_	_		_	
_	eueroriquerity &	_				23.65								86			\$					8 83							64.88	_							_			\$ 5	_					
_	negotišti kato T d kvomeri					55 44								47.28			19 47					51 68							E.	_				Ř Š						52 13			;	\$ \$		
9 -	% ALK Consumed																											‡				909		_				_				\$			_	
TEMONAL	evomen alnomma X			7.86		10 06		?	20 66							_	E 8	\$		\$ \$		ž g			38 56		85 O	ž	-	28.33		30 67	5	3	76.37		7			77 86			-	£ 8	8	_
-	lavomeR 20083 X	5	_	8		8	;	×	99.93		_			8,28			8	98 64		86 86		£			28 85		\$ #6	5	} \$	8		26 66			39 63		56 66			66.66		26 66	-	8 8	8	
-	Seromen 000 %													5								22.26		_										‡ }			1							S 2		
-	tevoment &2T /	8				8			39 85					8	!			29 65							28 66		8	:	8	8		\$	3	3			29.65					8	:	\$ \$	\$	
	ньс (съпчт)																					5,700.00						9.100.00	31016			90 00		2			00 006					3.400 00		88	_	_
-	Feed Collors																				_	12 00	92					8 1				8		8		_	8				_		_	8		
-	Total Colfform (CPUV100 mil.)				_		•				_											1,0071		_				8 2			-	. 20 24		` 8		•	8					8		8		
-	Total Phosphoreus (Ages)				_	3.10								8		-	8	_			_	262						-	-					B				-		91.6				<u>.</u>		_
-	(Jem) negoziiii laioT				_	15.70		_			_						66.5				_	5.17	_		-				a			_								20.00				8		
١.	("Agm) HUIT				_	2.50	_									_	2 00 2	_				82	_						- 5					• 			_			8:		_		8	_	_
·	NOSWOżne (wilk.)					- oso											R. E.	-				317									_						_			1830		_		1350		_
-	(mg/L)	80.0	3 8	8.0	_		80	8 8	8 8		_			800			8 0	3 8	80	0.27		8	ă		9.0	_	200	8	8 8	3 3		6	8		200			-		. F		8	_	200		
پر	(Jem) enhold3 late1	800	3 8	80			8		_					2 8	_		8	-				80	Ē	_	800		_	8					906	-						3 8	—			8 5	_	
PERMEA	Check) (Mg-N (mg/L) (ASL					_												_	-			_					_								_	_		Γ					_			
	(Jem) N-EHV		8	90 0		8		9.0	0.22					_			8	3		800		ě		_	60:0		ş			0.15		0.0		90	9.72		6.24		_	50.0		120		8		
	(V6m) 881		2			20		-	3 0.20		_				\$ -		_	0.00	_	c		-		_	2 0 50		0.40		20.2	0.20		2 020		8 8			8	_			_	- 5		0.20	0.50	
-	CBODE (MB/r)	-	<u> </u>	98.0		8		5.0	0.13						-	_	60	8	-	5		ĩ		_	0.12	,	2 33	328 00	0 12			001		-	0.18	-	90.0	-		100		8	-	0.2	0.10	_
ŀ	(Agm) NJA	-		_	_								_				_	-	_		_				_			8				9.6	—					-				00011			_	
	(75w) 000	-	_									_			8			_			_	8		_			_	<u>F</u>						8				L	_		.—			- 28		
	(UTH) (HINISTO)	0.15	8 8	0.07		-,00	80.0	900	2 3	:				£			800	8 8	- 0	61.0	-	710		_			0.29	0.21	91.0	2 0 0		8			8 8		_	-	- !	9 :		9		_	D 0	
	(пауст)	1.408.00	8 88	1,370,00		00 276	1,210.00	310.00	8 8					1.378.00	888		1,463.00	279.00	34800	1,515.00		00 969	90 159		705.00		728.00	1,631,00	90.00	1.582.00		724 00	1,652 00	.692.00	1,784.00					288.00		80	1,517.00	1,442.00	8 90	
	congob) studentemes	8		32.50	_		8	31.80	ç _		_			31 00	9			_	2 26		_	- 8	22 70		8		31.00			28.00		30.40	_		28 82	_	28	-		30.20						
Ļ	#	+−	R		_		_	ž.				_	_	_			ž				_	28		_			8	-	8			7	_	ž		_	_						_	7 11	_	
	(V ⁶ W) 9008:		80	900 000		705 00		702 00	9	3					8		618 00	;	8	815.00		820 00			690 00		720.00		792 00	90		8		88	00 006		1.000.00			360 00		\$	3	375 00	545 00	
	PAZE (why)	Γ	90.00	7,200 00		20000		7,150.00	7 900 30	8					90000		6.500.00	1	8	3,150.00		00 009 8			90 006		2,100 00		7,000.00	2.450.00		55.4		73%000	7 950 00		2000			980 00		809		8,000,00	00 00+	
TANK				00.054.8	750.00	8 9 9 9		9.850 00		00.09221	8 5					8002	8,750 00				920 00	1,65000					9750.00			10,150,00			10.000.00		0.00000	11,200 00	13.400.00		00.00	00 000 9						910001
AERATION TANK	(nimLASO gan) MA	1-	8		=	<i>5 5</i>	_	2	o :	- 2	=	_			= :		*		\$ <u></u>	6	12	8		_		2	95	_	8	5 5		9 2	_	01 521	= 0	=	==	+		* *		- 6		160		- N
۲	(n/6w) o	↓_		3 8			8 8		8 8					B	8				8 9	· 8	_		2	_	ş					& 9 2 -					8 8		2			8 8	i.			8		
		, ,	9 29	3 3	_		8 18			_		_	_	- Si			_	_	8 8		_		12.00		- 06 57				_	24.10 2					29.00		5	-		4 00 62 00 62				2000	_	
	н		7.20	_	_	-		7.18	_		_	_		_		_	1 19		22	_		5		_					~ E					2.			2	2	_		_		· ·	,0 t	_	
ſ	(Jew) scot	3	00:010	790.00		8	3	962.00		886					90.2%		772 90		8	950 00		90			902.00		8	3	978 00	90		5	3	385 00	00 080		9	í		8	Š		900	976.00	5	i i
T	(W) emiT su	1 2	4272 83	2 02	934.08	100.50	641708	į	3	8 6 6	138.00	\$ 980	8 8	7.	90 00	0 0	4877.08	470175	23.23	47.133	8 24	2 × ×		16.29	4862.16	16.1.91	5 5		-5 PG	2003	5082 91	160115	\$156	518016	5204 41	£23	3277 41	530341	\$305 66	52.525	27.200	\$305.25	2 2	2468.50	\$482.25	55.78.25 55.78.25
		1 A	West Arthres	505		Sun B/22/80	Tue 8/24/28	MATELIA POM	1.00 m	A 87275		# P.3078		MATERIA PALL	2		200	M 8778		Frd W100	¥ 17	Sun 8/12/99	74 ST		17.14	Set W18/8		21/4	4 972/8	The \$72500	5	Sun Brzeine	Tue 828/98	96/62/8 PMA	BALLAN PA	102/1	3un 100378	1	Wed 106/96	Thu 107798		10/10/8	10/12/10	1073799		
		ľ	ş :	<u> </u>	4	<i>a</i> :	, ž	*	£ '	- 3		i	2 \$	_		* .	* #	_	* -	_	<i>3</i>	2 3	1.2	¥	£ 4	<i>.</i>	3 }		*	ě ů		3	2 2	¥	£ *		3	∦ <u>*</u>	*	£ 2				}	<i>}</i> :	
RMY	i																																													
PACERVENT		-	•	٠.																					•				•	٠.		•	•	•				•			• =	•	: :	•	= :	:::
ľ	•	1																																												

#
43.20
61.25
\$
69'66
2
1600.00
9.00
2.73
22.10
8
20.10
10.0
0.02
9 0.14
0.17 0.20
300.00 0.17
124.00 36
2
6.13
1447.50
8
2 8
4400.00
900 0069
•
8
8
9

Opportunal, Writh CYCLED AN TO MY EVENT 119 DROPHILAL, WITH CYCLED AN

::: :

222222

5555555

::::::

Table C-3 RO Operating Date

££££££

ž ž

Table C-3
RO Operating Date
(Date History)

	, ,	And Stage 2 on 67: Chris Anti Bugs 1 on 67: Caustia Stage 1 on 67:0	•
981 67 981 67 982 70 983 70 98		`` -	_
2018 1189 2 20 2018 1189 2 20 2018 1189 2 20 2018 1189 2 20 2018 1189 2 20 2017 1189 2 11 2017 1189 2 11		THE WEST AND STREET	
1467 1467 1467 1467 1467 1467 1467 1467		13	_
Junes 30000 20000 27100 27100 27100 27100 27100 27100 27100 27100 27100 27100 27100 27100	*********** **************************	1100	
3156 2756 2760 2870 2870 2870 2870 2870 2870 2870 287	#\$#\$##################################	34.76	
្ត្រី និង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុង ក្រុ ក្រុង ក្រុង ក្	\$	<u>.</u>	
825226828844588	********** ****************************	z -	_
~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~		: ::	_
00000000000000000000000000000000000000		2	-
U W W W W W W W W W W W W W W W W W W W			
::::::::::::::::::::::::::::::::::::::	***************************************	1 2	~
		: ::	_
マントンフィンマン 原来のである	000000000000000000000000000000000000000	: :	
525522228 <b>8</b> 88	######################################	2	_
~~~ <u>~~</u>		š.	_
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	\$\$\$\$\$\$\$\$\$\\\\\\\\\\\\\\\\\\\\\\\\\\\\\		_
	988888008 111111111111111110000000111111100000001111	-	-
388228322222		š ž	_
455688888685555	######################################	E 8	-
4 6 2 6 6 6 7 4 2 2 D 8	######################################	8 :	
	***************************************	2 8	
P		Ē j	-
мявыянчия в ч ч ч <u>« « « « « « « « « « « « « « « « </u>	***************************************	e -	_
***************************************		: :	

		ž.
		Even
		, , , , , , , , , , , , , , , , , , ,
**************************************		46.00
		5 5 8
100 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		i i i
254 254 254 254 254 254 254 254 254 254	######################################	interactings 2615
25		Conc 2618
***************************************	## 0 F 8 K 6 8 F K F K F K F K K K K K K K F F F F F	Tot Pura
2 2 3 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	<u> </u>	Sampiralra 76
23232232222222	**************************************	7 7 E
277777772885888888		RO Feed
	***************************************	Concentral 5 8
	######################################	- i
	***************************************	Tol Pura
***************************************	**************************************	33
38222222255 322 255	######################################	37.0
		derritage
33223333333333333333	######################################	ŸřŽ
<u> </u>	######################################	Stage 1 Stage 2
+877833333333555533		2 Sept. 1
	######################################	310
2222222222222222222		22.5
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	***************************************	7um 1987
######################################	######################################	255

		:::1

Table C-3
HO Operating Data
(Data History)

I E		::	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	n voc	200000000000000000000000000000000000000
		3 7		5:00.0	P#sc:::::995::::905::::9:9:9::::::::::::9:9:9::9:::9:
i i	8995855855	57	9598985895858555	25 g g g g	
Turbidey	222222222222	23	356688836683	*****	
2 mg =	**************************************	8 P	22222222222222	22222	
RO Feed		22	250000000000000000000000000000000000000	22222	112128000000000000000000000000000000000
PDC (provgerni') Stage 1	. 由北海河建设西西南部北西北海南江		本名在第四百百里里里里在10里里的名	\$ 6 5 4 5 5	paasasaseBessassasepsassasepsepsaevassvascvecoBaseBaseas
Stage 2			おおかないないない おおおおおおおおお	: 0 1 1 2 2	•••••••
Slage 1	~ **********		**********	:-:::	
Come	12033333333333		\$ 5 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	\$ \$ 7 R A S	######################################
Pseure (4P4)			68 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	25.50	#######################################
3	52 52 52 52 52 52 52 52 52 52 52 52 52 5		8 6 5 7 8 8 8 6 7 8 8 8 8 7 8 8 8 8 8 8 8 8 8	92333	888888888333333333333333333333333333333
80	ត្តាស្តីស្ត្រស្តិត ស្ត្រ ស្តាស់ស្តីស្តីស្តីស្តីស្តីស្តីស្តីសុខ ស្តីសុខ សុខ សុខ សុខ សុខ សុខ សុខ សុខ សុខ សុខ	35	9990000000000000000		\$8800800041888888808088888888880000000000
Flow (Lpm) Tot Parm		= =		5:55%5	770-101-1071-1-1-1-1-1-1-1-1-1-1-1-1-1-1
1		22	22222222222222222	127177	?;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;;
Consponingle	୦ ମାଜ୍ୟାର୍ଥିବି ଅଧିକଥାରେ ଅବସ୍ଥିତ ହେଉ ୧୯୧୯ ଅବସ୍ଥିତ ଅବସ୍ଥିତ ଅଧିକଥା	::	*************	0 0 4 9 9 N	
PO Perc	ないもちゃりなららまりのから なって アファファファラ 自由 音楽器	22	**************	*****	
Na fa	. ************************************	2.5		*****	TREATER STREET S
Samplite abra	% ជាជាបានស្នាក្នុងស្នាក្នុងក	* 3	化大环共聚苯苯甲基甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲甲	នាខេះដីដ	ត្តភាពការក្ដីដូចស្ដីដូចសាល់ពេលបានគាត់ការសង្គិតស្ដីដូចសាល់ពេលបានជាការការការការការការការការការការការការការ
(of Perm	************	5.5	552225555555555555555555555555555555555	131313	:8288**********************************
Cene	1720 1720 1720 1840 1840 1840 1840 1840 1840 1840 184	3392	1508 1518 1518 1518 1518 1518 1518 1518	*****	
nierate 6	25.00 20.00	2951	2842 2842 2842 2842 2842 2843 2844 2845 2845 2845 2845 2845 2845 2845	25 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	
1	17.20 17.27 17.27 16.17	1728	1779 1810 1810 1810 1810 1810 1810 1810 181	888939	
ી ફે	2006.1980.1284 10.000.1981.1984 10.000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.00000.1981.1984 10.0000.1981.1984 10.0000.1981.1984 10.00000.1981.1984 10.0000.1981.1984 10.00000.1981.1984 10.00000.1981.1984 10.00000.1984 10.00000.1984 10.000000.1984 10.00000.1984 10.00000.198	E # #	0.007.000 15.0 0.007.000 >0.007.000 15.0 0.007.000 15.0 0.007.000 15.0 0.007.000 15.0 0.007.000 15.0 0.007.000 15.0 0.007.000 15.0 0.007.000 15.0 0.007.0 0.007.000 15.0 0.007.000 15.0 0.007	07/06/1969 1/35 07/06/1969 1/35 07/06/1969 1/35 07/06/1969 1/35 07/06/1969 2/33	
Clapsed Class (bys)	\$7.5 \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	111	227575757575757575757575757575757575757		
			A. with pat ifteed	 ` E	1
1			both Stegme (at 4 de with p		
Ì			G G		•

Page 5 of 17

			Singe
			. Everi
			Elapare Time (hn
	27/17/1990 27/17/1990		Desertion 37:12:1969
E E E E E E E E E E	1000 1000 1000 1000 1000 1000 1000 100	***************************************	
2.861 2.862 2.802	2000 2000 2000 2000 2000 2000 2000 200		Jolecula Jolecula
300+ 3511 4183 4211 4211 4211 4211	4630 4630 4637 4637 4637 4637 4720 4720 4734 4731	**************************************	Conductive Cone
F * \$ 5 5 5 5 5 1 8	99525245929856	***::*********************************	V (uSum)
2122222	**********	ななな異点な点はは未来のなななななからないないないないなれまれたのとなるなななななななななななななななななななななななななない点点のにはままれれ	Samplival
~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	***********	232223242444422222223442344444444444444	But Fac
# \$ # \$ 8 8 8 8 8 8 8 - 4 0 0 0 0 0 0 0	化安全 化安全 医自然 医自然 医安全氏管		2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
# # # # # # # # # # # # # # # # # # #	**************************************	>=====================================	Consentrat
111111111	***********		ī
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	11512111111111111111111111111111111111		Tel Perm
	or short or any short or or or or or or or or or or or or or	00000000000000000000000000000000000000	Conc
625 662 762 763 772 772	7 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	######################################	5 1
\$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50 \$1.50	674 674 677 677 677 687 687 687 687 687 687	893919979311138999444444999999999999999999999999	Interretage
\$5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	22222222222	848486448888888888888888888888888888888	8 2
********	3243353465345	34	Slage
121111111	32233323333333	222222222222222222222222222222222222222	Sing
9 4 4 9 \$ 4 \$ 5 £	* * * 7 % % % % % % % % % % % % % % % %	***************************************	Stege 1
*****	8688888888		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
688888888	***********	**************************************	ا ا تا تا
000000000000000000000000000000000000000	800001000000		Tubiday
ស្តីគូស្គីស្គីស្គីត្	<b>ୁଷ୍ୟାନ୍ତ୍ର ହୟନ୍ତ</b> ୍ରିଷ୍ଟ		100
ಕ್ಷಿಕ್ಕಿ ಕನ್ನಲ್ಲಿ ಇ	202220000000		5 = 2
*******	************	eseccecci et	: 12.

	·			
<u> </u>	となっていませる 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本	អ្នកស្ត្រស្នាក់ ក្រុ	# ************************************	***************************************
E S	2	******	~~•!:::::::::::::::::::::::::::::::::::	2 • • • • • • • • • • • • • • • • • • •
Portigi Inde	8584 88878389383888	# 4 4 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	######################################	***************************************
Turbally	227722222222222222222222222222222222222	707777N		
E M	22222222222222222	2243434255 46454545	22222222222222222222222222222222222222	
NO Fee	232222222222222222222222222222222222222	288888888	*************	
PDC (pai/gem.) Stage 1	919171818888818858185	**************************************	88888888888888888888888888888888888888	CARREST SANGUES SANGUES CANCELER CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR
Stage 2	- 577 ~ FR % % & \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	*******	**************	***************************************
Slage 1	D&& + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 + 5.5 +	3722324277	**********	\$\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\
ag ag	\$ 5 \$ 5 \$ 5 \$ 5 \$ 5 \$ 5 \$ 5 \$ 5 \$ 5 \$ 5	\$23535 <b>3</b> 33	828585868585858585	\$2,500\$333\$24173\$\$\$\$\$\$\$\$000\$800\$\$00\$50505050\$60\$800000000
wasure (kPs) Intermege	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	25 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	*****	\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$
, B	75.2 2.4 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5	E 25 7 7 7 8 9 9 9 9	5328158843843448	7650907727277777778888888888888772222222222
Cone	**************************************	**********	\$ 0 > 4 4 4 4 4 4 8 8 4 4 8 8 8 8 8 8 8 8 8	000000000000000000000000000000000000000
Flow (Lpm) Tot Perm	いくいきゅうきゅうさいもののものもつてそろうは、 ちょうくかなるものを発出を避れる。 まてき	04000000000000000000000000000000000000		3.20111011111111111111111111111111111111
3	***************************************	P. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2.	***************************************	***************************************
Concentrate	不存在他会就会就会被自身就不下下了的。	所作的是 100 年 10 年 10 年 10 年 10 年 10 年 10 年 10	<b>多くつゆごはするが! アンスのうらく でくちゅう ロックロンはっちゅう アンション 日本 ロック・アンス こうらく うてき ウック・アンス ロック・アンス >	**************************************
RO Feed	- 4 9 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		WWG.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.4.	
1	**************************************			**************************************
Samphealve	8888255255588888855 	222223333	· · · · · · · · · · · · · · · · · · ·	K A A KA KA KA KA KE E E E E E E E E E E
Skem) Tot Perm	8 1 8 2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	* 2 2 2 2 2 2 2 2 2 3 2 3	\$\$ * \$\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	6
Cone	465 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2 247 2	200 200 200 200 200 200 200 200 200 200	2 8 2 4 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	98.8:599858859299588158988898588855685511888886883
of and and	1111 1122 1133 1134 1135 1135 1135 1135 1135 1135	1282 2870 1102 1103 1104 1104 1104 1104 1104 1104 1104	200 M	
3	1822 1834 1834 1935 1735 1739 1739 1739 1739 1739 1739 1739 1739	22 1 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	665 665 665 671 671 672 673 673 673 673 673 673 673 673 673 673	200758825994159852886788585255853865558883388688888
The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s	200000000000000000000000000000000000000	*********		
1				
Ι.		- (1000)		
] ]			i	
L	I			

71 Mz 7 aga 9

		ži g
		E
		-
	8	201
		2/ 2/1/1999 15 08
		. i
N 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	***************************************	1701
	\$454566405666666666666666666666666666666	£ 5
Q Q Q Q Q R R R R R R R R R R R R R R R	\$370785551012335180008053800Q156**45581288188128628862881118£6388888	2 2 7
***************************************	ವಿರುತನವರ ನಿನೇವೆ : ೧೭೯೩ ನಿರ್ದೇಶಕ ನಿನಕ್ಕೆ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರಾಹ ನಿರುವ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರುವ ನಿರ್ವಹ ನಿರ್ವಹ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರವಹ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ ನಿರುವ	S2 21
111110111111111111111111111111111111111	x2000000000000000000000000000000000000	::
- 0 - N - 2 - 4 - 4 - 4 - 4 - 4 - 4 - 4 - 4 - 4	**************************************	::
	***************************************	::
######################################		::
		5.5
	0 × 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	555
4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	# \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	2 H
294328 <b>6944496388864</b> 686833888338344	8088223240007800001988222002850000002839520500233458682828080000	e e
######################################	5114-69-60110001-460-000-61024-61-61-6-6-6-6-6-6-6-6-6-6-6-6-6-6-6-6-	ន្តដ
	403334444444444444444444444444444444444	3.5
######################################		12
\$989922222223333346222233333569632433	######################################	127
######################################	***************************************	==
######################################	######################################	r x
<b>888888888888888</b> 888888888888888888888		62
***************************************		ě
		. : :
***************************************	***************************************	

Table C-3 RO Operating Data (Data History)

	Sie 4
	Eveni
	Elapsed Time (hrs. 2231 47
	Defections (ACC) 1945 Ave.
	1457
	Distance of the Control
	Conductively Cone 5007
ននានាអត្តន៖ « » » » » » » » » » » » » » » » » » »	Tot Perm
K CARA	Sampuvaive 230
	Rew Food
***************************************	HQ OH
	Conceedings 6.0
	: ë l
	Flow (Lpm Int Parm
***************************************	- 0
	; ≅ <b>i</b>
201880881888888888888888888888888888888	Interplate 100
***************************************	£ # 5
***************************************	Singe :
\$::::6668\$66276776776866686666666666666666666	Stage 2
	Steps 1
**************************************	30 T
######################################	=
***************************************	Turbid#y
5-5-5-5-5-6-6-6-6-6-6-6-6-6-6-6-6-6-6-6	1 10
***************************************	= = =
	::1

Table C-3 RO Operating Data (Data History)

_				
<u>.</u>		- <b>.</b>	र व्यक्षक्षक्षक्षक्षक्षक्ष र व्यक्षिक्षक्षक्षक्षक्षक्ष	***************************************
Pos		****		P
Particle	8552 88825283258625868 2	11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	######################################	######################################
Turbidity				
- General	. 4	*******	***********	
Tamper RO Feed	222222222222222222222222222222222222222	2222222	**************	
PDC (pairgpm ) Stage 1	31813188888888888888	28 8 8 4 9 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	# A & F # & & W C F R R R R R R R R R R R	
Stage 2	*************************************	******	**************	ERROLENTE : 1771, 1771, 1771, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871, 1871,
Stage 1		222224277	********	***************************************
ğ	**************	\$255 <b>55</b> 333	£285856 <b>85858</b>	3540653335555555555555555555555555555555
tasure (kPa)	65 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	25.5 25.5 25.5 25.5 25.5 25.5 25.5 25.5	# # T # # # # # # # # # # # # # # # # #	5:886:3768893866888888888888888888888888888888
1	753 7746 7746 775 775 878 878 878 878 878 878 878 878	25 C 25 C 25 C 25 C 25 C 25 C 25 C 25 C	2952112513595595	A6549000000000000000000000000000000000000
š	52 59 59 59 59 59 59 59 59 59 59 59 59 59		**************************************	
Flore (Lever)		**************************************	200000000000000000000000000000000000000	3
Į	***************************************	5556665455 5556665455	**************	***************************************
Concentrate		· 电线 电线 电 电 电 电 电 电 电 电 电 电 电 电 电 电 电 电	日本のはマイラコ EIフサ 名称のアアアラック・ログルル・ファック・ファック・ファック・ファック・ファック・ファック・ファック・ファック	
Ho C	ならちの自身がある場合をアファファ 前の代 ようなのの こころ ごうちょう はんしゅう はない こうかい はんしゅう はい はい はい はい はい はい はい はい はい はい はい はい はい		N N T T T T T T T T T T T T T T T T T T	
		*********	するできなり そうこう アファイ・アファイ・アファイ・アファイ・アファイ・アファイ・アファイ・アファイ・	**************************************
Semalited	8888544444444444	*********	<b>東西にはなる中央中央のはまれる対象は受賞</b>	na rang ka né a a a a a a a a a a a a a a a a a a
LEVER)	· 图 · · · · · · · · · · · · · · · · · ·	* 5 5 5 7 5 5 5 5 7	*************	0404805350050550505555555555555555555555
nauctivity.	2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2 2,2,2,	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	200 C C C C C C C C C C C C C C C C C C	985855555555555555555555555555555555555
ŭ	25 25 25 25 25 25 25 25 25 25 25 25 25 2	2922 2970 2970 1122 1124 1125 1125 1125 1125	248 20 20 20 20 20 20 20 20 20 20 20 20 20	
	1622 1623 1623 1715 1716 1716 1716 1716 1716 1716 1716	25 4 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	
			0.772.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072.1999 1 4.072	100 100 100 100 100 100 100 100 100 100
- Freeze	### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (### ) ### (#### ) ### (#### ) ### (#### ) ### (#### ) ### (#### ) ### (#### ) ### (#### ) ### (#### ) ### (#### ) ###  ##########	200 200 200 200 200 200 200 200 200 200	44000000000000000000000000000000000000	
	. (************************************			]
	### ### ### ### ### ### ### #### ######			The second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second secon
-	<u>, , , , , , , , , , , , , , , , , , , </u>			
L				

Page 7 of 17

		ş
		Ewan
######################################		Time (hra
	7772 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	0419/Time 3/29/1999 15 04 6770-1999 15 04
	************************************	÷ 5 2
2	***************************************	1000 1000 1000 1000 1000 1000 1000 100
	36255825689988589888888888888888888888888	5659 5659
	#3149\$65614133318000\$6003\$66856\$#*43\$\$\$\$\$\$\$\$\$668\$666888\$\$\$\$\$\$\$\$\$\$\$\$\$\$	2 2
	\$0\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	Samplivatva 51
	***************************************	Part Field
**************************************	11272222222222222222222222222222222222	70 F
	***************************************	Concentrate
		== 1
	**************************************	10 Pa
A	2 4 4 2 5 6 5 6 5 6 6 6 6 7 4 8 4 4 4 7 7 4 4 8 4 7 6 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6	5 0 0
<b>7.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3.3</b>	*5:53493485534853485545855428563564835648565486666666666666666666666	्र ≟ <b>१</b>
::::::::::::::::::::::::::::::::::::::	84882222220887888886508842200282092820028208264468264488868888888888888888	
* # # # # # # # # # # # # # # # # # # #	£\$\$\$555\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	2 E E
228888988888888888888888888888888888888	**************************************	: :
445888888888888888888888888888888888888	22000000000000000000000000000000000000	15 12
	122333555555555555555555555555555555555	
# # # # # # # # # # # # # # # # # # #	**************************************	22
######################################	L22575555555555555555555555555555555555	* *
••••••••••••••••••••••••••••••••••••••		; 2 2
######################################		ž Š
***************************************		
	***************************************	_

Table C:3
RO Operating Data
(Data History)

	00000
	00000
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	2
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	*****
	2222
	erre.
	55555
	£ £ £ £ 5
TINGENERAL DELIPTION OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PR	*****
<ul><li>「このますと見れただけだけだけです。</li><li>「これにはなる。</li><li>「これにはないできます。</li><li>「これにはないだけできます。</li><li>「これにはないだけできます。</li><li>「これにはないだけできます。</li><li>「これにはないできます。</li><li>「これにはないだけできます。</li><li>「これにはないだけできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできます。</li><li>「これにはないできまするできます。</li><li>「これにはないできまするできまするできまするできまするできまするできまするできまするできまする</li></ul>	
0.00.00.00.00.00.00.00.00.00.00.00.00.0	
	2222
-	25553
	20113
* 1	
**************************************	
・	**1 % 8
	22222
	25831
[P8866885500068835055385888858888888888888	3 \$ 8 5 5
	04/13/1984 0.15 04/13/1984 1.15 04/13/1984 1.15
Y. S. S. S. S. S. S. S. S. S. S. S. S. S.	
-	

7. 56 sond

		Sing
		-
		Even
		Time I'm
		Data/Time
		-
	* 18. A	1
		ŀ
ងពេលសមាន ការក្នុងសម្តេច នេះ ជាជា សមាន សមាន ក្រុម គឺ ខ្លួន ខែង គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ		190
		S
ត្តិត្តិស្ថិត មាន មាន មាន មាន មាន មាន មាន មាន មាន មាន	\$ 12:00:000000000000000000000000000000000	Spirrates
	3 270334332777333172332333333337777773333333333	Ram Food
	* *************************************	50 Fast
***************************************	7 7000000000000000000000000000000000000	Concerning
	· · · · · · · · · · · · · · · · · · ·	5 2
		io Perm
	* *************************************	: 5
######################################	(d damagagagagagagagagagagagagagagagagagaga	7
	: 053585358888888888888888888888888888888	620
. * * * * * * * * * * * * * * * * * * *	: ####################################	₹ 2
		- 15
		10
************************		
######################################	(* 20228336528.48.862888888825528.88.8255682625568255555	
######################################	** ###################################	=
\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	** ************************************	0.2
:#####################################	\$4 4 5543848844455533355444485444654465844658	ŝ
::4:6866:::::::::::::::::::::::::::::::		-
***********************	** ************************************	5
		$\perp$

Table C-3
HO Operating Data
(Data History)

	(//2,5/	51.0
		-
		Even
		Time (hra)
		Date/Time
		ï
		biergieg
81184927398688888888888888888888888888888888888		Conc
######################################	***************************************	I'd Poin
		Sampervaire
***************************************		Raw Food
		RO Feed
	ない くく ちょう くく ないかん しゅう かかか かから かり りゅう ちょう しょう しゅう かまま きょう くう くう くり しゅう かん かん ちゅう しょう しゅう しゅう しょう しょう しゅう しゅう しゅう しゅう しゅう しゅう しゅう しゅう しゅう しゅ	Concentrate
	\$ \$ 6 \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	i
		Tot Paris
		٦,
::	\$ = 5 2 2 3 3 5 5 5 6 5 6 5 6 5 6 5 6 5 6 5 6 5 6	ě
	1133112223335522233362223232323232323232323232	Interpta ge
**************************************	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	SE Conc
	 	ű ga
.::::::::::::::::::::::::::::::::::::::		Slege 2
######################################	***************************************	Steps:
**************************************		20 Family
**************************************	***************************************	17
		Lipson
\$- <b>\$55000000000000000000</b> 00000000000000000		ğ
		: 2 3

Table C-3
RO Operating Data
(Data History)

	T.	***************************************	တွေလာ များသာသာသာသာသီတွေသည် မွေးသောသီတော်သီတော ကြည်တွေသီလေး ကြောက်တွေသည် မွေးသောတိတ်သော		
	E C		*16==5==================================	•	555641F725577P9999•555575555555599
	Particia		***************************************	Ē	******************************
	Turbedly			r c	
	Res	2222244444444	222222222222222	2	
	RO Feed	***************************************	222442222222222222	2	
	PDC (peripper 7	***************************************		16.2	2586533535358923333538568866889883
	Drop (pee) Stage 2	99990555555555595999555555555555999999	£2200000000000000000000000000000000000	8	**************
	Stems	******************	======================================	٠	***************************************
	Contract		528888888888888888888888888888888888888	ž.	35553\$655555555555555555555555555555555
	Interestings	77887888888888888888888888888888888888		•	# 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
	]		8627 788 778 8627 788 778 8627 8623 8623 8623 8623 8623 8623 8623 8623	\$	######################################
	٤	***************************************	#0 N O D O O O O O O O O O O O O O O O O O	8	200840444444444444444444444444444444444
	Tot Perm		∨ 2 д и и и и о и и и и и и и и и и и и и и	:	*N4NN4NNNNNNNNNNNNNNNNNNNNNNNNNNNNNNNN
	]		000180000000000000000000000000000000000	-	337777777777777777777777777777777777777
	Concessionia		不是否定于古代的的自然的的情况的的意识。	ê	
	1 3		. 47 N D P 4 4 4 5 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	\$	
		***************************************			
		安全の表示を表別は実際なる事情を表示を表示を表示の表情的の意识を含む。 おはあだれてガスなのだだだ	************	E	្តិកាន់និងនិងនិងនិងនិងនិងក្នុងការប្រភព្ធភាពនាស្ថិននិងនិងនិងការប
	na/cm)	######################################	202 202 202 203 203 203 203 203 203 203	E	
### Common	Appellant	265866888888888888888888888888888888888	25	ž	: # # # # # # # # # # # # # # # # # # #
	Į,		2000 1100 1100 1100 1100 1100 1100 1100	2308	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
	:		1 8 9 8 7 6 6 6 6 8 8 8 9 8 9 8 7 8 7 8 7 8 7 8 7 8 7 8 7	à	4001468888888888888888888888888888888888
The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s	-		20000000000000000000000000000000000000	78-02:1999 14.33	
211 21111	Eleptrod		3 3 4 4 4 5 4 5 4 5 4 5 4 5 4 5 5 5 5 5	£ 13.7	
			Committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the committee of the commit	M. Carry (Carry )	The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s
	-				

2. 10 Z. abag

RO Operating Data (Data History)

These Light		01: 02: 03: 04: 04: 04: 04: 04: 04: 04: 04: 04: 04	2252 2252 2252 2252
Figs (Figs   Figs   F		8 C	88.65
Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care		3.5	8855
Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care   Flower Care		5.5	5555
Float (Lond)   Personne (EPs)   Person	######################################		
Flow (Lynn)   President (EPs)   President (EPs	35555355555555555555555555555555555555	3 8	3338
Flow (Lynn)   President (EPs)   President (EPs			
Flow (Lynn)   Prostaure (Ebs)   Tof Burn   Conc.   Feed   Interdage   110 44 751 657 657 110 48 774 678	**************************************		
Flow (Lynn)   Prostaure (Ebs)   Tof Burn   Conc.   Feed   Interdage   110 44 751 657 657 110 48 774 678			1111
Flow (Lprn)     Tol Parm Cone Feed Inte	######################################	2.5	1212
Flow (Lpm) Tol Perm Conc. 110 44	98886888668886886686868686868666777788888666888888	£ <del>?</del>	\$ E \$ E
Tol Perm	######################################	2.8	1553
²		2.2	32
And Concentrate Food 59 153	00000000000000000000000000000000000000	2.2	5555
Concentrate 5 0 6 7		7.7	2222
* I		8.80	N 40 40 C
5 2		2.2	3232
Raw French		50 SO	****
Samplication 2.	ಇಳು ಎಳಕು ಕಾತಕಾರಿಕು ಎಲಲಲ್ಲಿ ಸಹಸಗಳ ಸಹಸಗಳ ಸಹಸಗಳ ಸಂಪರ್ಧಿಸಿದ್ದರು. ಇತ್ತಿ ಕಾತಕಾರು ಕೈ ಪಾತ್ರವಾಗಿ ಸಂಪರ್ಧಿಸಿ ಕಾರ್ಯವಾಗಿ ಸಹ ಪ್ರಕ್ರಿಸಿಕ ಪ್ರಾಥಾಗಿ ಸಂಪರ್ಧಿಸಿ ಸಹಸಗಳ ಸಹಸಗಳ ಸಹಸಗಳ ಸಂಪರ್ಧಿಸಿದ್ದಾರೆ. ಇತ್ತಿ ಸಹಸಗಳು ಸಂಪರ್ಧಿಸಿ ಪ್ರತಿಕ್ರಿಸಿಕ ಪ್ರಾಥಾಗಿ	*1	2100
10 Perm 107	6xx86;278660;58668xxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxx	5.8	\$ 2 2 5
Cone Cone 5645		53	<b>2323</b>
Menstage 1488		* 8	386 3872 3872 3872
1 2 8		3 ŝ	# 10 m
Date/Time 04:18:1999 7:43 04:18:1999 8:43			11111
! ├			
Front			
İ	Š Š		

7. 10 11 mb g

Į.			***********
ě	*********	pro::200000000000000000000000000000000000	222222 <b>2866</b> 6
Particia	********	BORCERNER STREET STREET STREET BEST OF BORK STREET STREET STREET STREET STREET STREET STREET STREET STREET STR	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$
Turbudity	ыя фокууст - висорбан		5055555555555
5			885588888888
RO Fee	******		25558888888
POC (psettom )	2 5 5 6 6 5 6 5 5 5 5	***************************************	<b>克曼基尼尼恩基尼尼瓦尼克</b>
Stage 2	~~~~~ <del>*</del>	***************************************	***********
Presenta Stage	1112211111		**********
Cone	7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.		25.03.05.05.05.05.05.05.05.05.05.05.05.05.05.
Transmire (MPs)	元素保存在放展的最	######################################	
į	25252525		59575555555
ě	722222222	. B B AL DA BANAN BANANAN NENGA 20 00 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	**********
Flow (Lemi		02125688888888888888888888888888888888888	**********
]	5555455555		848448848484
Concentrate	N 4 B C N C N B N N	- D & N N A B N N B B N N N N N N N N N N N N	<b>电子音像设定式下向电影员工作电影</b>
1		***************************************	- 不当等实际企业的企业的企业
	**********	ZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZ	キャステントできます。
	C # W # # # # # # # # #	អ្នកពេលក្នុងស្គ្រស់ស្ត្រិក្នុងស្នាស់ស្នងស្នងស្នងស្នងស្នងស្នងស្គងិក្សេង បានសង្គម នេះ សង្គម នេះ សង្គម នេះ សង្គម ន 	2000年20日本日本日本日本日本日本日本日本日本日本日本日本日本日本日本日本日本日本日本
u Svem)	記載發音養養型 <b>整</b> 簽次	######################################	********
dudlivity	25 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		7746 7746 7746 7746 7746 7740 7740 8777 8777 8777 8777
Can.	1721 1785 1785 1773 1877 1877 1885 1885	5603864868558585858585855858533358533335355553333535535	2004 1700 1700 1700 1700 1711 1711 1510 1510
};	707		12 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
	000251000124 000251000124 000251000184 000251000184 000251000184 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025100025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 00025 0		1004/1999 11 19 1004/1999 11 19 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 12 1004/1999 11 1
			1900 1900 1900 1900 1900 1900 1900 1900
	No.	**************************************	4.5.5 4.5.5
	f		2
_	<del></del>		

Triposi aped

	<u> </u>		
or Feed P	Another Extra		Î
		3176 70 2377 80 2377 80 2380 20 2380 2	t inpred
10 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Comp	10 + 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 100 - 1	Detections
	*******************************	1634 1642 1702 1702 1702 1702 1702 1702 1702 170	ï
3776 3587 4786 4786 4786 4786 4786 4786 4786 47	***************************************	3544 2530 3537 3683 3683 3706 3706 3706 3706 3706 3706 3706 370	
4022 4022 4022 4022 4022 4022 4022 4022	***************************************	7012 7041 7179 7179 7227 7227 7275 5600 6104 6474 7090 7090 7090 7090 7090 7090 7090 7	Cone
0 = 8 % T M M M O O O O O O O O O O O O O O O O	# 14 # 4 # 8 8 9 1 1 1 1 2 2 5 6 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	781 # # # # # # # # # # # # # # # # # # #	(utien)
5. 15. 15. 15. 15. 15. 15. 15. 15. 15. 1	在中心中的企业的企业的企业,但是不是有一个企业的企业,但是不是有一个企业的企业,但是是是有的企业的企业。	2	Semplinaive
	%1000010000000000000000000000000000000	コンコンととととこととととこととと コンコンとととののののなりのと 単音点	Pow Ford
**************************************	2257517751227552852855275777587777 *************	00000000000000000000000000000000000000	70 P
おくらの事かのとなりをなるとなってなく とくくく	4405***********************************	かしないまとのようなのののからを作るようとなる。	Concentrate
33345555555555555555555555555555555555	113635533635636464433663346433664346434664444	*************	
11111111111111111111111111111111111111	25422222224468402222222225652223680 29922222222	11111111111111111111111111111111111111	Flow Itpm)
			n a
1974 188 188 188 188 188 188 188 188 188 18	511488818888888888888888888888888888888	9 2 3 3 5 5 6 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	ì
######################################	***************************************	222222222222222222222222222222222222222	Preseure (ki
22855555555555555555555555555555555555	4:444444444444444444444444444444444444	723 723 723 723 723 842 723 723 723 723 723 723 723	Conc
3282838822888322228 <b>3</b> 0		***************	Siage 1
• 5 5 5 • • • • • • 5 5 5 5 • • • • • •	***************************************		Drop (par) Steps 2
£414466555655655555	t#30100000000000000000000000000000000000	######################################	PDC (bavgem )
*********	######################################	88888222222222 <b>88</b>	RO Feed
888882222882822		********	2 5
			Turbiday
***********	ប្រសាសប្រាស់ពី ខែជាស្ថិតស្ថិតសម្រាជនា និងសម្ព័ស្តី ប៉ុន្តែ សិងសមានសង្គារៈ បានសេស	555555555555555555555555555555555555555	Particle
	588555555446666555555566665556666666666	======================================	P
<del></del>			1 0

3323	-			-	Ē																																						Siage
	AVERAGE	AVEHAGE	<del>-</del>	<del>-</del>	DANLERI	End Inc in Face P			•	•				•		•	-		•		-										_												Eveni
i					1715.41	_	3709 11	3708 1	3705 11	3702 11	30 20 20	1697.78	25 Sept.	3644 19	2 1	1 2	36.00	100	3637 19	36.5	1834 19	36.52 19	3630 10	200	367	342 2 2 2 3	3624.0	£ £	3421 10	2 1 2	85.8	¥ 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	1000	X67 41	36.55	10 E	3602 SE	3601 81	3590 83	3597 93	3595	3590 93 10 10 10 10 10 10 10 10 10 10 10 10 10 1	Time (Ara)
					Full 8661 123.	221-1988 5 55		:021-1996 2 55		54 22 6661/02/0:		1		1	65 6 666 AB: AD	07 10 1960 7 59	0.0000000000000000000000000000000000000	0 1 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	10/18/1999 3 59	0 10 10 10 10 10 10 10 10 10 10 10 10 10	C/10/1996 0 59	1217/1909 22 59	10/17/1989 21 59		1317 1999 1758			1017/1990 12:50		10 17 1999 5 44 14 5 896 7 110	317/1909 4 64	1017-19961-44	1017:1900 o at	10:16:1909 22 44	10:0:0:000:0:0		1016/1999 17 44	101019991644	PT C1 0461-91/0.	101619991244	P 01 6561-91/0.	11 6 5051 51 51	Date/Time
1 3 3 X	14	_	79 8		ŝ	ž	įį	į,	í	i	é		146		Ĕ	į į	ž.	ý ;	1	į	1973	ě	1 6	i	i	1 1 2	į.	į		6.6	Ę,	. í	1 6	É	ž 8	ś	; iš	.526	1519	527	1525	1300	ì
2007 M	2 3364.51		16408.57	1	.  -	17.5		3274		122			100		2 2	ěě	1	212	ě	2 2 6	213		229	2	225	2 2	229	2256	725	221	22	2 23	27.5	2	2 2	¥	řř	ž	 3 %	ç		2200	)riorn
- 1			1	1	-	7		2		~ 2 2					~ ·	55						_	_	_	_	_	_	_			_		_	_	_	_		_	_	_			-{
1017.43 4977.43	5286.61 1		022.64		ŕ	7	2 8	*	3 :	83		2 8	5 3	13	\$ :	8	t:	9 1	3 3	R =	1	3 :	57 8		ŧŧ	29	£	řŧ	8	9 5	2	1 2	27		_	_		_	_	_	7071	_	1
102.67 117.67 117.67	106.13		198.23		ě	*	2 2	7	2 2	# 8	: :		8.8		21	e r	X.			2 8	81	2 2	28	2	3 2	88	2	2 2	2	2 6	2 :		2 1	2	Ē Ē	Ē	ēş	9	ŠŠ	\$	<u>.</u>	₫ g	1
	14.93	į	10.2	1	ě	÷	<b>.</b> 2	2	* 3	36	: t :	ŧ	ŕ	: \$	<b>z</b> :	6 2	2	72	1 2	3 5	ē:	Ē	ž S	207	21.7	2	223	216	204	# 20 # 20	20	212	2 6	ž¥	ěŷ	247	7 %	3	2 2	236	22 22	2 2	200
1231	7.47	i	33	: 1	ï	7.7	77	77	~ ~	3 2	: 2.	a de	7 6	::	75	7 2	2	- :	: :	22	: :	::	73	73	22	7,	7.	7 7	7	75	7.	: :	2:	: :	2 ;	: :	7.7	7.	7.5	7.6	7.6	~ 0	
::::	6.72	1			-		• :			-					2	67		P :		• •	::								*	- u	5	57	56				5 5	2	9 15		<b>.</b>	5.5	
			165		, ,	7.4	* 6		7 0	2			62	78	7.0	22	7.5	7		75	: 3		2				::	::	66	2 0	70		5	* o			• •		<u>.</u> .	6.2	3.2		
1328	1	-	řž		2 0	ć		į.	× ×	<u> </u>	: :	- :	5	5.2	·	ú S	ı,i	į.		, i	5	ة ة ن م	ú	íź	ű ú	ŭ,	ž	ŭ 1	ź	5.5	15.3	ű É	ē	- 5	5 1	i iš	5 5	15.0	55	ï	خ ن	3 0	
2225	ş	1	ž ž i	,	100	23	55	22	ē i	2	125	źź	ű	á	12	ń ń	5	ž.		5.5	: 23	55	12.2	:5	2 2	5	i ž	12.5	123	125	12.5	7 2	ii i	5 %	ź	5.5	125	ű	50	12.5	123	22	1
	์ ชี		2 2		1	2.1		2		1 7		3 5	2 7		ï		::	ï		= :	32	2 2 5	52		: :			300		300	30	5 5	30	3.0	20		5 5	d E	2 2		200	300	·
101.24	103.56		22.1		i i	979	÷ §	Ŧ	řš	ž.	Š	: 5	Ę	1213	1216	70	ŝ	ž	įį	ž į	1127	ŝ	ŝ	1023	000	2	3 8	3 8	ě	979	97	2 %	ž	5 F	ŗ	\$ <b>\$</b>	920	ř	ž ž	953	ž ž	3 1	g
#### ####	*	ļ	12 11	1	1270	800	877	ī	ğ ü	3		5 E	97	11.33	ź	26	1	1108	0 10	1076	Ē	100	3	Ę	ī į	8	8 8	8 6	8	0.9	ī	žŧ	9		26		II	857	2		5 <b>5</b>	3	806
	Ī		į	<u> </u>	121	į	626	8	150	8	7 2	777	ž	1078	Ê	<u>.</u>	ő	65	ÉÉ	1017	į	3 5	E	E	5 £	Į,	Ę	5 }	Ę	8.37	Ş	8 5	3	. 6	Ř	žž	ž	į	9 9	i	3 0	920	200
1111	1			5		:	ű i	ī	::	á	: :	: :	ž	=	: :	= 4	iń	12	<b>5</b> =	ű,	i =	= =	=	: :	= =	=	: :	= :	: =	= :	: :	ē =	=	ó :	= :	::	= :	: :	53	15	= 5	2	~
			ž į	14.74	ž.		• •	•			• ~		, ,			• •		•	• •		0 E	• -			<b>▼</b> ö					• 7	5 6	5 5	ő	ë ë	ĕ.	ő •		•				• ;	ē
			124	É	5	- 2	ē	8	2 4	Ē	3 2	į	į		ā	š (	: :	š	ĒĀ	. 1	É	ě	8	ě ÷	ē	É	k K	÷	ž	£ .	: 8	ī :	ž	25		<u>.</u>	ř.	ž	ź.		ēŝ	t	-
			# # #	2	ž ,	×	27	2 2	2 2	3 23	¥ 2;	11 1	: 2	* *	2 22	2) 2	2 2	27	2 2	2:	2 2	22	: 2:	8 8	8 9	: 2	t t	2:	: :		: :	22	: 15	# #	: 15	<b>5</b> 5	: 2 1	: ::	× 5	: 2	2 2	2	=
1111	,		1 2	٤	2	t	2 ;	2 %	2 2	¥ ¥	≈≆	2 2	2 2	23	2	2 3	2 2	à	ಜಜ	2	2 2	2 2	2	2 2	<b>2</b> 8	*	<u> </u>	8	5 5	8 :	ಕಕ	8 8	8	= =	: 5	22	: 23	# #	7 :	==	8 8	<b>8</b>	ક
1988	;		===	8	7 2	í	á.	• •			<b>.</b> .		. č	2 h	20	20	20	0	200	0	200	~ ~	200	700	200	20	700	2	N NO	2	200	20	?	20	: 3	2 0			<u>.</u>			ž	
****			1 1 E	į	į,	ś	ž	· ·	ž	ž	3 5	8	- g	i	, 2	r	* 2	: 1	3 5	. 2	e e	ť	įŧ	::		s e	z s	£	2 8	1 2 :	: :	3:	: 1	\$ \$	2 2	ខា	t g	: 2	. 2 :	<b>5</b> 5		: 1	ť
1			£ 5 5	Ē	1307		يد .	a k	۵.		<i>د</i> م	٠.	دد			- 43	ಸ	i z	4.5		ಪ ಪ	٠.	ತ ಪ	4.4		: 2	Z 4	: 2										5 4					-
			:::	<u> </u>	1									,				-		. ,		•							٠.	::								٠.					-

Table C-3 RO Operating Data (Data History)

-	-	A	SlagerEve
Stages 1 and 2)	TESTING.		
	11111111111111111111111111111111111111		Elapsed Time (hrs.)
M. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green, S. J. W. 1. Green,	\$2,000 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	515 55 55 55 55 55 55 55 55 55 55 55 55	STime
202244444446000000000000000000000000000	10000000000000000000000000000000000000	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Ĩ
6 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	######################################	######################################	Interatage
では、 日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日	2	68 00 00 00 00 00 00 00 00 00 00 00 00 00	Con
	55555152185523818555528888888818618696868886886868686868686868	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	To Prod
2 2 8 2 8 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		3 6 8 8 4 4 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	Rejection
10 1 1 2 0 0 1 1 1 1 1 1 1 1 1 1 1 1 1 1	5 18 5 7 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	
888888888888888888888888888888888888888	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	888888888888888	(VICE-VpCp/Vc)/C
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	12/18/07/2/17/2/16/3/17/2/2/2/2/2/2/2/2/2/2/2/2/2/2/2/2/2/2/	22 22 22 23 24 24 25 25 25 25 25 25 25 25 25 25 25 25 25	Salt Rejection
17 50 17 18 17 17 18 17 17 18 17 17 18 17 17 18 17 17 18 17 17 18 18 18 18 18 18 18 18 18 18 18 18 18	# 20 9 9 4 4 5 7 7 7 8 8 7 8 8 8 7 7 7 8 8 8 8 8 8 8	2 60 2 55 2 55 3 22 3 22 3 22 3 22 3 22 3 22	Saft Pansage
96 45 45 45 45 45 45 45 45 45 45 45 45 45		648 677 648 648 698 698 698 1920 1920 1920	NDP
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	<b>发展的过去式和复数形式的现在分词 人名英格兰 化二甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基</b>	25687755552 <b>2222</b>	
2.26 2.25 2.25 2.25 2.26 2.26 2.26 2.26		11093 11093 1112 1114 1171 1200 1200 1150 1150 1150 1150 1150 115	TCF
2 2 3 2 3 2 3 2 3 2 3 2 5 5 5 5 6 5 6 5 6 5 6 5 6 5 6 5 6 5 6	4 \$ 4 5 4 4 4 5 5 5 5 5 5 5 5 5 5 5 5 6 5 6	5 8 8 8 7 7 7 2 2 2 2 2 2 2 2 2 2 2 2 2 2	J (L m-3nr-1alm-1
2.2 日本の本の日本のは、1.2 日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日	2	22 22 25 25 25 25 25 25 25 25 25 25 25 2	NPF (L/man)
\$28 <b>618</b> 8888888888888888	00000000000000000000000000000000000000	3 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	NPF (gpm)
100 P 0 A 0 M 0 7 7 7 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8		199 199 199 199 199 199 199 199 199	Stage
2 4 4 4 5 2 4 4 4 4 4 4 4 4 4 4 4 4 4 4	82,22,22,22,22,22,22,22,22,22,22,22,22,2	915 915 915 915 915 915 915 915 915 915	Slage 2
52334444444444			-
# 22 22 22 24 25 25 25 25 25 25 25 25 25 25 25 25 25		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1,

												_																																			
Recurery	51 83	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	25.25	52.78 52.88	25.33	88	55 55 55 35	\$2 ES	2 5 2 5	52 32 52 88	52.5	2 2 2 2	82	32	P. P.	67 75	6.00 6.70 8.70	F 75	67.75	8	23	388	3 H	22	56 39 E 86	2.2	8 8	5 t t	12.5	22	2 2 3	C R S	2 2 2	222	12:	; %	55.41	9 5 5 2 8 5	255	25.55	33	3. S.	5 R 2	RR. Kt	# # : 3	3 2 3 3 3 3 3	8 2
T.	0.62	200	12	6 B	333	22	20	200	2 2	0.0	26 ES	- 0 - 0 - 0	0 0 0 0	£ 8	8 8	8 8	<b>9</b> 0	800	92	25	8		2.5	. 32	ē.	167	307	2 6 2	8 8 3	2 2 2 2 2 2	2 2	2 2 2	8 8	<b>2</b> 2 6		2 0	090	5.5	250	280 280	0.00	200	225	22.50			2 2
Slage 2	20 6	200	2.5	28.1	27.6	52.5	27.4	7.5	283	28.3	2 2	24.7	2.5	5.5	5 5	. v		2 2	202	1.	17.0	2 %	23	20 4	2.5	::	~ =	5.4		. ·	• •	. ·.	1 2	12	5 2	23.2	230	223	222	388	2 2	234	523	22.2	243	Z Z S	žž
E S	į		2 2	* 2	225	23	2 7	24.0	5 F F	5 Z	<b>.</b> .	<b>8</b> 9	20 B	20 0	2 2	602	3.2.5	. 5. 5	22.	, <u>,</u>	5 .	7	W 00	2.5	2. č.	0.4			e m	ž P	7.7	* 40 t	8 ZZ	2.5	212	ŝ	, e	200	SE.	វត្តិនិ	5.5	23.8	ž ž	វត្ត	23.	223	222
NPF (apm)	es s		88.8	5.50	25.5	25.4	5.59	2.3	87 ES	2. S. S.	925	2.2	\$ 83	545	62.5	80.0	. 5 6	. 6. 6	4.5	f	9:	187	2 2	25	2.82	5.0	= 5	2.	560	240	2 3	980	9800	2 2 1	3 5	2 2	2.97	26.2	5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	168	22	2 30	2.75	2 67	\$ \$ 7 .	2 59	2.53
NPF (Ummi)	20.88	8 58 5	20.08	20 68	20.25	2 2 2	22.	8.5	20 62	20 24 20 27	20.30	2.38 3.38	22.28	20 66	29 61	22 :	: 2	125	2.0	: £	18 47	2 2 3	1 2 3	2.2	90 11	80.0	2 5	383	3,73	2 5	339	327	3 23	8 8	£ \$	20 8	8 t :	2 8	280	10 85	1 2 3	10 67	5 5 3 3	8 : 2	1007	\$ E	25.
1 (1, m-2he-1 efm-1)	5 44		\$ <del>\$</del> \$	85 S	5 4 6 5 5 1	3 5 5	25.3	<b>3</b> %	<b>\$</b> 5 E S	527	\$ 2.9	1 %	5.55	836	: C 8	100	3 2 3	155	8.5	2 <del>.</del>	ş	385	3 5	988	9 20	2	8 2	8	0.94	<b>26</b> 00	5 B	0 0 88 88	580 0	E 5	2 00 8	80 × 50	2.97	2 2 2	582	2 83	2 t c	2 78	22.5	<b>8</b> 2 <b>3</b>	3.5	55 22	2 5 5 2 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 5 3 5 3
	581	2	20.50	276	1238	15	3	3.50	123	208	8 5	202	27.0	9.5	582	17.	200	22.5	25.5	5 5	8	202	2	5.5	27.5	E	28.	8	\$ 50 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	23.53	22.22	2 5 2 5 2 5	229	23.23	7 5 7 5 7 7	1257	200	2.5	2 7	25.25	2 9 8	222	20.20	2 2 2	202	52	2 4 5
	\$	<b>9 9</b> :	3 2 5	2 2	2 2	883	8.8.8	; # S	==	==	<del>-</del>	- X 22	9 8	3.5	. 2 :	2 3. 3	9 38 3	R G 5	2 25 25	<b>7</b> 8	33	233	8 8 3			2	2 2 1	B <u>5</u>	<u> 8</u> 8	8 6	ēŝ	£ 5	និន	š.ž	13	· ·	r 2	<b>.</b>	# 1:1	- E E E		. 6 8	22	£ # #	2 2	8 X	2 52 55 
ş	160	27.5	27.5	21.2	565 264	ž ž		88.	27.5	281	282	- Z	2 2	8.5	35	8	6 8 8	- - - - - - - -		§ Ę	, 5	\$ \$ :	¥ \$ \$	756	3 3	772	25.	182	8 8	82 5	1323	1315	1327	6 %	5 5	3 8	2.2	3 3	8 5	583	253	1 15 35	\$ 5 8	S 38 8	£ £	8 S	8 S S
Call Designed	8	6.0	9 7 6	38.5	83	8 2	787	3 2 5	5 5	712	207	, c =	7.5				B E E	2 6 7	256	÷ 4	196	22	1027	2 2 3		13.97	8:	* # : :	# # = =	8 8	10 26	10 61	1 8 2 9	1 02	8 5	2 1	7 265	7.87	8 42	929	881	22.4	7.26	88	1 28	2.5	7.65
Care Balantiton	5ek 7epetimen 92 94	2 22	23 SE 28 28 28 28 28 28 28 28 28 28 28 28 28	2 2 2	8 8	5 5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	F F S	22	22	92.58	86.28	8 8	2 2 3	121	2 6	2 2 :	28:		. <b>.</b>	5. J 5. 5	B. 56	£ \$ ;	8 % 5 L	8 8 8	8	* S	2 9 :	# #	2 1	2 2	\$ Z	8 2	2 2	55 ES	92 40	75 27	22.35	22 te	2 <b>3</b>	8.2.3 2.2.3	8 5 5	22.5	25.50	25 25	2 2 2	32	25 25 25 25 25 25 25 25 25 25 25 25 25 2
A STATE OF THE PERSON NAMED IN	(VIC)-VIPCIPACINCE	8 8	888	388	88	88	8 8	888	888	88	8 8	388	383	8 5	8.8	8 8	888	88	888	88	8	88	88	888	8 8	8.8	88	8 8	88	8 5	88	8 8	88	88	8 8	8 1	888	88	88	888	88	888	88	88	8 8 8	88	888
	Т	0.08	560		200	 - 96 - 0	8.8	88			58 .	. 8 6	260			560	28.0	900 000	0 0 0 0 0 0 0 0 0	260	860	0.07	¥ 5	8 8 8	9 -		. 6 . 6	= =	2 8	2 3	2.5	15.0	25.0	8 8	800	88 0	260	22	88	2 2 :	8 8 3	200		0 0 C	3 8 5	8 5	ā ē ē
-	Rejection	56.0	2 2 2	980	25.0	\$ \$ \$	98.0	8 8 9		500	5 6 6	500			286	989	<b>S</b> S S	2 3	\$ <b>\$ \$</b>	8 6	*	2 2	3.3	8 8 8	3	8 6	2 0	2 2	2 2	83	980	2 00	25	\$ \$ B	2.60	1	25.5	5 6	2.5	1 5		8 5 5	500	5 5	6.5.5	5 5	5000
1	Tot Prod	260	13:	8 8 8	8 =	5.5		= 2	500	2 6	8	883	3	2.2	= =	÷ 8	25	2 2	***	7.5	5	= 6	2 2	2 2 3	* &	5 5	<u>.</u> 3	1 2	2.2	E	5.5	2 5	2 5	200	7 2	•		7- 2-	2.5	8 %	20.	- 5 9	2 2	38	86	2.5	- 2
	Contr	24.08	2.23	28 27	2.7.2	22.2	27.28	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	. A .	8 8 8	121	283	3 52 5	2 18 2	2 2	7 8 7 0	9:2	5 2 5 3	2	8 6 6 F	12.13	25.22	27 45	8 E E	8 3	2 2	5 2 2 3	2 Z	2 8	32.5	86 35	35	72.27	88	2.8	29 82	 	8.8	2 2	823	2 2	- 9.5 2.2.5	8 8	28 74	50.2	3 2 2	888
	Interutage	23 EZ	# E	5 58 52 00 53 00	2 22 22	26 16	22 52 23 28 24 25	22 22	2 2 2	2 2 2	32	2 2 2	22	27 52	: 8	# ? 5 5	2 2 2 2	200	222	2.8	28.21	# X R R	2 P	2 to 1	2 <b>2</b>	5 Z 2 Z	2 2 2	* ¢	2.2	 	8 1	2 2 2	8 9	22.2	22	1 %	2 2 3	8 8	\$ 8 8 8 8 8	20.00	3. S 2. R	2 2 2	26.5	# 8 # 8	2 <b>8</b> 8	2 2 2	A 3:
	3	25 E	2 2 2 3	8 9	1 1 1	1 2	3 K 2 2	2 : 2 :	2 2 3	90	3 2	3 92	2 2	2 E	# # ! !	3 A 2 2	2 2	2 2 2	2 2 2	3 3	2	22	22	2 2	2 1 2 1	5.53	5 5 7 4	8 5	2.5		2 2 3	3 3	2	2 2 3	8 2	15 16		2 2 2	25.55	2.5	15 27	2 2		2.3	2 8 3	26.5	8 2
	STIME	\$30.00 7 13 AM	MA 51 01 99-002	52070 11 13 AM	5/30/96 2 13 PM	\$3000 \$ 13 PM	52079 6 (3 PM 52079 7 (3 PM	\$3099 6 13 PM	53090 11 13 PM	521/00 3 13 AM	MA 61 8 89 152	\$31.99 7 42 AM	\$21.99 10 42 AM	531/99 12 42 PM 5/31/99 1 42 PM	\$3198 342 PM	501.98 7.42 PM	V31/08 10 42 PM	ALTON 12 42 AME	61 99 2 42 AM	61795 5 42 AM	77 00 10	8/2/90 7 13 AM	MA EL 18629	6/2/99 4 13 PN 6/3/99 7 18 AM	67299 12 18 PM	63/99 5 15 PM	6239 6 15 PM 6239 9 15 PM	MAST OF GRADA	SUA 20 12 15 Adm	61.99 4 15 AM	MA 21 5 6944	MA 21 B 69-1-3	64-90 9 35 AM	64.00 to 15.44	A.e.99 1 22 PM	6.4.99 3.22 PM	6.5.79 8 50 AM	MA 92 11 99/20	55599 2 59 PW	Nd 65 9 6659	65.599 7 59 PW	64.09 to 50 PM	A44.99 2 59 AM	646799 4 54 AM	646.99 7 15 AM	5450 10 15 AM	6-8-99 1 15 PW
_	_				_	_			_	_					_	_		_	\$ 8 3						_							_													_		8 5
	Comments	$\vdash$		-						-	_					_					Shell Charles with	i i			_				_		_																
	Stage/Erent	-				_							_			_					<u># U (</u>		_		_				_	_	_				• • • •												
	2					_		_			_		_		_											_		_					_														

Page 2 of 19

	n	-	Stage-Event
	Open at Son	and Leasuring (C.III) And Stage Z on Gar, Citize And Days I on 60; Caudit Bays I on 60; And Caudit Bays I on 60; And Caudit Bays I on 60; And Caudit Bays I on 60;	Comments
	544 551 551 551 551 551 551 551 551 551	5 23254445555555555555555555555555555555	Firms (firs)
1179   18   18   18   18   18   18   18   1	221222	6-60-90 115 PM 6-60-90 115 PM 9-60-90 115 PM 9-60-90 115 PM 6-70-90  \$Time 6/5/29 5 15 PM 6/5/29 6 15 PM	
# # # # # # # # # # # # # # # # # # #	111111	1 1111111111111 1 211111111111111111111	5 5 E
	28 51 62 77 28 63 85 19 62 77 28 63 85 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19 63 19	20 20 20 20 20 20 20 20 20 20 20 20 20 2	inlaretage 30 84
\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	222222	24 25.25.25.25.25.25.25.25.25.25.25.25.25.2	20 20 20 20
8	2000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Tot Prod
	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		Rejection
		0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	200
** ***********************************	888888	8 888888888888888	1 00 1 00 1 00 1 00 1 00 1 00
26 853729897774988774767947478777877787778777887778	2222222	2	Saft Rejection 91 51 91 40
2	4 4 2 3 8	6 6 5 5 6 5 7 7 7 7 7 7 7 7 7 7 7 7 7 7	Sall Passage 8 49 8 60
AN PEREES TARKEN BERKER BERKER BERKER BERKER BERKER BERKER BERKER BERKER BERKER BERKER BERKER BERKER BERKER BER	*****	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	S 8 8
A		7 777799988888	223
		250 240 221 200 202 198 198 198 198 198 198 198 198 198	1 257 1 261 1 257
	222222	2 222222222222222222222222222222222222	J   L m-2hy-1alm-1 2 53 2 52 2 52
	2827288	# 10 M	9 71 9 84 9 86
29 77777777777775566899651768888878988788887888888888888888888888	222222	\$ 23855 2255 2385 2555 2555 2555 2555 2555	2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
## ###################################		2 88858888888	22 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
		238 240 240 240 240 240 240 240 240 240 240	24 0 - 24 0 1
	2000000	c 000000000000000000000000000000000000	2 5 5 T
	8 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	\$ 2625502 FAR FAR FAR FAR FAR FAR FAR FAR FAR FAR	222

	StagarEvant
	Comments
	Elapased Time (hm 651 70 653 70 653 70 655 70 656 70 656 70 656 70
6 (1986 1) 5 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1) 6 (1986 1)	88883388888
# # # # # # # # # # # # # # # # # # #	14.57 14.57 14.57 14.58 14.20 14.20
# THE FROR FRANCE OF THE CONTROL HERE SENT AND FRED CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CONTROL CO	Interstage 12 95 31 64 31 26 30 78 30 18 30 18
AMENARAN MANARAN MANARAN MENARAN r>MENARAN MENARAN  30 S S S S S S S S S S S S S S S S S S S	
	Tol Prod 9 58 9 55 9 54 9 52 9 51
	D 97 0 98 0 98 0 98 0 98 0 98 0 98 0 98 0
	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
	194C1 9pCpAVc)/Ci 0 96 0 96 0 96 0 96 0 96 0 95 0 95
######################################	96 0.2 96 0.2 96 25 96 25 96 35 96 37
######################################	Salt Passage 3 94 3 89 3 89 3 81 3 75 3 75 3 76 3 76 3 63
38883333334355348885348885336688855338855388868588685	49 49 49 VQ
医征抗性脓肿性结肠性 计数据 化双环 化硫酸 化聚苯基甲基苯甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基	3 77777 3
	TCF 1258 1247 1240 1240 1256 1276 1277
	J-(L-m-2hr; ) almr-1; 2-97 2-96 2-96 2-96 2-95
	##F (L'men) # 00 # 07 7 94 7 94
######################################	2 11 2 13 2 10 2 10 2 10 2 10
	\$100   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200   200
	Stage 2
	balance from Cot
######################################	7222332 7222757

E PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIES PROPERTIE																	
	2	22 22 22 23 23 23 23 23 23 23 23 23 23 2	2		01 54 24 35	# # # # # # # # # # # # # # # # # # #	25.00 62.00 52.03 52.03 52.03	26 25 25 25 25 25 25 25 25 25 25 25 25 25									
	nee from Col																
						4 4 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	1,0000	112 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4									
	-	4 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	22002222222222222222	. 77.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.		25.52.52.54.54.55.55.55.55.55.55.55.55.55.55.55.	4 % 00 00 00 4 4 % president	000-B000000000000000000000000000000000									
	APF (spm)	2 2 3 3 3 3 3 3 3 4 4 4 4 4 4 4 4 4 4 4	8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	25 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		5533362382368865	25.2 2.2 2.2 2.2 2.2 2.2 2.2 3.3 3.3 3.3 3	2 2 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5									
	HPF (Lmin)	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	0.500000000000000000000000000000000000	8 1 1 8 5 5 1 5 9 5 5 1 5 8 8 5 5 6 5 5 5 5 5 5 5 5 5 5 5 5 5 5		883355666655666666666666666666666666666	7 5 8 8 8 7 7 8 8 8 7 8 8 8 8 8 8 8 8 8	2									
	(Lm-2hr-tetm-t)	# # # # # # # # # # # # # # # # # # #	262885285358888886525 00244453588888886525	808838:00000000000000000000000000000000		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	4 52 4 46 4 73 4 77 4 52	2 4 4 4 4 4 4 8 8 4 8 8 8 8 8 8 8 8 8 8									
	Į,	2.55 2.50 2.50 2.50 2.50 2.50 2.50 2.50	1219 2223 2223 2223 2209 2209 2212 2212 2212 2212 2212 2212	202 202 202 222 222 222 222 222 222 222	1236	2.55 2.25 2.25 2.25 2.25 2.25 2.25 2.25	1.228 1.238 1.243 1.258 1.258	1212 2002 1191 1191 1198 1178 1178 1178 1178 1178									
	-	# # # Q Q Q Q Q Q R # R R R R R R R R R	************	**********		*****	482±44	222222223									
	đ <b>Ç</b>	E 25 22 25 25 25 25 25 25 25 25 25 25 25	######################################	9 50 50 50 50 50 50 50 50 50 50 50 50 50		646855555555555	E 55 55 55 55 55 55 55 55 55 55 55 55 55	25 25 25 25 25 25 25 25 25 25 25 25 25 2									
	obmind he's	* * * * * * * * * * * * * * * * * * *	484486548848848888888888888888888888888	44444444444444444444444444444444444444	8 =	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	767 763 736 797 797										
	Salt Reportion	2	28824488888888888888888888888888888888			4 1 1 2 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	22222	2									
10   10   10   10   10   10   10   10	VICEVPCp/Vcb/Ce			\$ NG 5 5 5 5 5 6 8 8 5 5 5 5 5 6 6 6 6 6 6 6	0.82	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	0 + 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	23 <b>2 2 2 2 2 2 2 2 2 2 2</b> 2 2 2 2 2 2 2 2									
Common					9.00		1 2 2 2 2 2	85 2 2 2 2 2 2 8 8 8 3 3 8 5 8									
Commands	R negeon				0.97 397		*****										
Commands	1979	00000000000000000000000000000000000000			0.75		26 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 -	22 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2									
	8	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		<b>建设设计划的基础的的的设计的</b> 1999年1999年1999年1999年1999年1999年1999年199	8.8	2. 18. 18. 18. 18. 18. 18. 18. 18. 18. 18	844240 955454	20.5. 3. 4. 4. 4. 4. 4. 4. 4. 4. 4. 4. 4. 4. 4.									
March   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Contro	Interalless	22 22 22 22 23 23 23 23 23 23 23 23 23 2	**************************************	**************************************	25 25 27 28 28	28 28 28 28 28 28 28 28 28 28 28 28 28 2	11786x	2 K R S R S K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X K C X									
Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments	L. 1				- Z 5	1											
Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments   Comments		627799 0 44 PA 627799 0 44 PA 627799 0 11 44 PA 627799 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0 12 44 PA 62789 0	THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE S	MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SENSON MAN SE SE SENSON MAN SE SE SENSON MAN SE SE SENSON MAN SE SE SE SE SE SE SE SE SE SE SE SE SE	77799 10 36 AM 77799 11 24 AM 77799 12 22 PM	M 9 1 1 9 9 1 1 1 1 1 1 1 1 1 1 1 1 1 1	76/99 11 35 AM 76/99 11 35 AM 76/99 24 11 PM 76/99 33 5 PM 76/99 33 5 PM	1996 12 3 44/ 1996								2 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	600 600 600 600 600 600 600 600 600 600
		Convenience				of Engard On-	o lo 80%, with pit	£ 3									
				<del></del>		1											

Page 5 of 18

Supple see
Comme
127777777777777777777777777777777777777
STIME  **Y-999-12-19-20-20-20-20-20-20-20-20-20-20-20-20-20-
1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
######################################
\$ \$ 8 9 8 8 8 9 \$ 7 \$ 8 \$ 8 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
s = 3 3 % \$ \$ \$ \$ 3 3 3 5 5 6 5 6 5 6 5 7 7 7 8 \$ 6 6 6 6 7 7 7 8 5 5 5 6 5 5 5 5 5 5 5 5 6 6 6 6 6 6 7 7 7 8 6 7 7 7 8 5 7 7 7 8 7 7 8 7 7 8 7 8 7 8 7
***************************************
\$ - 1 - 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2 - 2
######################################

							8
	7						ga/Evant
							Commente
1542 82 1542 82 1544 82 1546 82 1546 21 1546 21	15.25 82 15.25 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.26 82 15.	1497 78 1492 78 1493 78 1495 78 1496 78 1496 78 1500 78 1502 78 1504 78 1504 78 1504 74	1480 56 1482 78 1483 78 1485 78 1485 78 1487 78 1487 78	1455 55 1455 55 1455 55 1455 55 1457 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 55 1477 5	108 60 108 77 108 77 108 77 108 77 108 77 108 77 108 77 108 77 108 77 108 77	1352 76 1353 76 1356 76 1356 76 1357 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 76 1358 7	Elapsed Time (hrs
77298 9 43 PM 77298 9 43 AM 77298 10 43 AM 77298 10 43 AM 77298 10 43 AM 77298 10 40 PM 77298 20 40 PM 77298 20 40 PM 77298 20 40 PM 77298 20 40 PM 77298 20 40 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM 77298 20 PM	7 22:99 11 43 AM 772:790 12 43 PM 772:790 1 43 PM 772:790 2 43 PM 772:790 3 43 PM 772:790 3 43 PM 772:790 5 43 PM 772:790 7 43 PM 772:790 8 43 PM 772:790 8 43 PM	77,099 8.15 PM 77,099 7.15 PM 77,099 11.25 PM 77,099 11.25 PM 77,099 12.25 AM 77,199 12.25 AM 77,199 13.55 AM 77,199 13.55 AM 77,199 13.55 AM 77,199 13.55 AM 77,199 13.55 AM	7/20/98 7 22 AM 7/20/98 9 35 AM 7/20/98 13 35 AM 7/20/98 11 35 AM 7/20/98 12 35 PM 7/20/98 135 PM 7/20/98 235 PM 7/20/98 235 PM 7/20/98 235 PM	7 May 12 MA A A A A A A A A A A A A A A A A A A	20070000000000000000000000000000000000	7 1499 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7 17 3 FM 7	STime
2222222	2012232111	14450 14450 14450 14450 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14550 14500 14500 14500 14500 14500 14500 14500 14500 14500 14500	55555555	11 12 13 14 14 15 15 15 15 15 15 15 15 15 15 15 15 15	252 × 058 8 8 8 8 2 7 8 8	0 10 0 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Ī
2 8 8 2 8 3 8 3 8 5 8 5 8 5 8 5 8 5 8 5 8 5 8 5	**************************************	2222222222 222222222222222222222222222	22 22 23 25 25 24 25 25 25 25 25 25 25 25	20 08 08 09 17 09 17 09 18 09 17 09 18 09 17 09 18 09 17 09 18 09 17 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09 18 09	50 50 50 50 50 50 50 50 50 50 50 50 50 5	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Interslage
895228	**************************************	24 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	22844825 22848254 2288333	27 34 31 37 16 37 16 37 89 37 89 37 89 37 89 37 89	55555555555555555555555555555555555555	**************************************	Come
11122	1 - 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	00000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 73 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	8 - 8 5 1 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	Tot Prod
000000000000000000000000000000000000000		000000000000000000000000000000000000000	000000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	000000000000000000000000000000000000000	2 2 4 2 2 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	Rejection
0 1 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	00000000000000000000000000000000000000	5 2 8 5 5 <b>2 2</b> 5	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		000000000000000000000000000000000000000	
2022222	1111000000	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	0 0 0 0 0 1 1 0 0 0 0 0 0 0 0 0 0 0 0 0	報酬 報報 から 4 名 報 0 1 2 2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	998888899888	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	(MCI-Abcbyrchcy
8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	2 2 2 2 2 2 2 3 4 3 5 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	94 99 95 17 25 25 26 26 27 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 8 7 27 28 8 7 28 8 7 28 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 8 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7 28 7	# # 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Sall Rejection
9 9 3 3 5 5 6 5 7 7 9 9 3 6 4 5 6 4 5 6 4 5 6 4 6 4 6 4 6 4 6 4 6	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	BIS S & A & A & A & B & S & S & S & S & S & S & S & S & S	5 1 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	0.505 mm 0.005 5 2.65 mm 0.02 0.25 5.55 mm 0.02 0.25	9 4 9 9 4 4 9 4 4 9 7 8 9 9 7 8 9 9 7 8 9 9 9 8 9 8 9 8 9	\$ 5 5 5 7 7 8 8 8 8 8 9 9 9 8 8 8 9 9 9 9 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	Salt Parage
164 195 298 298 298	555	266 276 276 278 297 298 298 298 298 298 298 298	3 5 3 <b>2 5</b> 5 7 £	327 327 462 470 478 478	472 473 473 473 470 480 480 480 480 480 480 480 480 480 48	552555555555555555555555555555555555555	£ 5
56861222	1128888111	288444444448	5 3 8 2 8 5 5 5 6 7 8 5 5 5 5 5	70 70	3 <b>8 8 9 9 9 9 8 8 8 8</b> 8	***************	
1 2 2 4 1 2 2 4 1 2 2 5 1 2 2 5 1 2 2 7 2 7 7 2 7 7 2 7 7 2 7 7	1229 1229 1236 1256 1277 1277	1240 1233 1205 1205 1205 1191 1192 1193 1194 1196 1196	1 216 1 226 1 226 1 226 1 226 1 226 1 226 1 227	1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	1205 1196 1196 1196 1196 1196 1206 1206 1215 1215 1251 1261 1251	TCF
000 000 000 000 000 000 000 000 000 00	22 22 22 22 22 22 22 22 22 22 22 22 22	2 50 22 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		# K	J (L m-2hv-1acm-1)
20 B 20 C 20 B 20 C 20 C 20 C 20 C 20 C	10 02 10 01 9 81 10 16 10 16 10 11 4 84 9 48 9 75	10 12 12 12 12 13 13 14 15 15 15 15 15 15 15 15 15 15 15 15 15	00000000000000000000000000000000000000	5 7 2 5 7 8 8 7 7 8 8 7 7 7 7 7 7 7 7 7 7 7 7	ただされたななななななななななな 記念に含みないなどに 記念に含みないなどに 記念に含まる。	20000000000000000000000000000000000000	15.31 (Januar)
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	3 1 2 4 7 3 3 1 4 7 3 3 1 4 7 3 3 1 4 7 3 3 1 4 7 3 3 1 4 7 3 3 1 4 7 3 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4 7 3 1 4	20	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	10000000000000000000000000000000000000	## (ggm)
2 2 2 2 4 2 7 7 7 7 7 7 7 7 7 7 7 7 7 7	11150001111	***************************************	7772	000000000000000000000000000000000000000	22222222222	555555555555555555555555555555555555555	Stage
22 24 25 25 27 25 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 27 26 2	1115	2007U4086	130 130 223 274	11110000000000000000000000000000000000	22121211111111	6666611111111111	Fig. 7
							÷
6 8 8 8 7 7 8 6 7 7 8 8 8 7 7 8 8 8 7 7 8 8 8 7 7 8 8 7 7 8 8 7 7 8 8 7 7 7 8 8 7 7 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7	282222222 2822222222	22554887725888 22554887725888	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	88888888 \$2522235 \$25222355	66 66 67 68 68 68 68 68 68 68 68 68 68 68 68 68	6	2 2

Operating Data

Racovery	00 75 00 00 00 00 00 00 00 00 00 00 00 00 00	02253#88257#8837#8926666666666666883888888888888888888888
Conductivity balance from Col .		
Ž	222222222 2222222222222222222222222222	
2 spal2	5 4 4 5 6 4 6 6 5 6 6 6 6 6 6 6 6 6 6 6	######################################
NPF (gpm)	2	#R:###################################
NEPE (Umin)	19 89 17 84 17 84 17 84 17 14 17 14 17 16 17 56 19 92	98 m D D D D D D D D D D D D D D D D D D
J (L m-2Ne-1stm-1)		
Ď	284 284 284 284 284 284 284 284 284 284	8.5.3.8.6.5.6.6.6.6.6.6.6.6.6.6.6.6.6.6.6.6.6
	244448888	######################################
ĝ	22222222222	
Saa Persen	9 4 9 8 9 4 9 9 9 9 9 9 9 9 9 9 9 9 9 9	
See Resection	28 28 28 28 28 28 28 28 28 28 28 28 28 2	\$6883318888874887098658688887567858888311668888788688888888888888888888888
WELVBChVelvCe	2223222322 2223222322	884254444555555555555555555555555555555
	0000-000	
-		
1	10212211220 1021221122	# # # # # # # # # # # # # # # # # # #
1	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	CHMEST RIGES REPRESENTATION OF THE STREET AND AND AND AND AND AND AND AND AND AND
	12 12 12 12 12 12 12 12 12 12 12 12 12 1	
]	2222222222	
	31 mm 72 yes 9 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 72 yes 10 00 PM 73 yes 10 00 PM 74 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM 75 yes 10 00 PM	March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 March 19 Mar
1	1548.21 1548.21 1548.21 1548.21 1572.21 1572.21 1575.21 1575.21	
	Community	
	State of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state	•
L	<u>"</u>	

Page 8 of 19

	· · · · · · · · · · · · · · · · · · ·	StagerEvent
		Comme
		nta Time
	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	8
10000000000000000000000000000000000000	:	814
00000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	15 39
12   13   13   13   13   13   13   13	# 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	30 17
3855648888888888888888888888888888888888	++8888++++++++++++++++++++++++++++++++	41727
	\$48 \$5 \$6 \$6 \$6 \$6 \$6 \$6 \$6 \$6 \$6 \$6 \$6 \$6 \$6	0.92
		0.97
		161
	F \$ \$ 8 8 8 8 8 8 8 8 8 8 8 9 9 8 8 8 8 8	ANCT ABOUTABLE
######################################	######################################	9401
		96 5
588833884388843483887358578678848 #138888888833484504873	0.18%	ŝ
**************************************	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	: £
		1240
-177946666979664699-77749664596647776 -5777479-678-8696865	9948mama8345mada44828mma9a25mma927	27
######################################	8379 # # # # # # # # # # # # # # # # # # #	12
***************************************	23255555555555555555555555555555555555	3 70
		; <u>:</u>
	ស្តស្តស្តស្តស្តស្តស្តស្តស្តស្តស្តស្តស្តស	5.73
	%%% 4 6 4 8 6 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	2 2

•	StaganEvent
E P	Communica Communica
	Elapsed Time (hrs) 1951 : 9
**************************************	Ĩ
	Interstage 28 25
RESERVAGO DE MARINGE DE SERVE DE SECUTAÇÃO SE LO CRASA MADA NE PORTO CONTROL A SECUTA SE SECUTA DE COMBET É ESTE E CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTR	1 14 COME
00000000000000000000000000000000000000	O 69
	Assection 0.97
	3 5
\$ 8 8 8 8 9 9 9 9 9 8 8 8 8 8 8 8 8 8 8	1 DB 1 DB 1 DB 1 DB
RESTREES CONTRACTOR SERVING CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTR	Sall Rejection 94 87
	5 13 5 13
: \$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	1 60 PF
	2.2
	7CF 1 276
	J (L m-2hv-latm-1) 3 46 3 42
	NPF (L/man) 1327 1311
**************************************	3 50 3 46
	ž 2 3
	Tr
######################################	

		Stage/Everal
		Comments
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2000 00 00 00 00 00 00 00 00 00 00 00 00	71ma (bra) 2081 97 2082 97
10 10 10 10 10 10 10 10 10 10 10 10 10 1	221222222222222222222222222222222222222	8 8
14 A A A A A A A A A A A A A A A A A A A		12 45
2 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	75 66 25 53
\$\$\$\$\$\$\$\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	7112 030000000000000000000000000000000000	44 S S S
000000000000000000000000000000000000000		Tol Pros
		Repartion 097
\$ 4 0 8 0 8 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	7222	8 3
5 4 8 2 8 9 3 1 1 1 1 4 8 8 8 9 9 2 8 8 7 7 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	5978 8762827888889828229878892288882299	(VECE VPCP/VeXC
2222421554455153221553224532522222222222	CIAS TAGIFIFE COCCANTACOCCANTACE CANCACAN SEC	Sali Rejection
8851252128	**************************************	Sall Pastage 6 39 8 50
\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	826666888888888888888888888888888888888	\$ 1 6 E
\$ 5 5 5 5 7 7 7 7 7 8 8 5 5 5 5 5 5 5 5 5	######################################	382
**************************************		1226
# 8 6 6 7 9 8 8 2 7 8 2 8 2 8 2 8 2 2 2 7 7 7 7 8 2 8 2	***************************************	3 62 3 57 3 57
######################################	9245 288288888888888888888888888888888888	13 80 13 80
######################################	######################################	367 362
	######################################	1 1 1 E
		102
è	\$2\$%;2 \$	ļ
	KEESTA SANGESTESTESTESTESTESTESTESTESTESTESTESTESTE	77.55

	:	ő		Stage/E veri
on 68, Passacci on the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of the party of	Charming (California)	men en en en en en en en en en en en en e		ent Comments
2602 17 2708 10 2708 10 2708 10 2711 10 2712 10 2713 10 2714 10 2715 10 2716 10 2716 10 2716 10 2717 10 2718 10 2718 10 2718 10	3-1	250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9 1 250 9	221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 221/48 22	E lapsed Time (hrs.)
	+294235PM	2009 7 3 AA 2009 1 00 FM 2009  2000 14 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 10 PM 1		
00000000000000000000000000000000000000	12 49	22222222222222222222222222222222222222	# # # # 8 8 20 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Ĩ
28 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	2023	1982 22 22 24 24 25 26 26 26 26 26 26 26 26 26 26 26 26 26	\$ 4 4 5 6 5 6 7 8 6 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	interstage
1	26 10	22 22 22 22 22 22 22 22 22 22 22 22 22		Come
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	°£3	000000000000000000000000000000000000000		Tot Prod
	3 9 7	1		Rejection
	793	2000 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		
222223222222222222222222222222222222222	0 93		5-1-1-5-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1	INICI-ADCIMARIO
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	9	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	10810101088888888888888888888888888888	Salt Rejection
10 A A A S S S S S S S S S S S S S S S S	5 0 8	\$ 77 \$ 74 \$ 85 \$ 85 \$ 85 \$ 85 \$ 85 \$ 85 \$ 75 \$ 75	\$ 5 5 5 5 5 6 6 6 6 5 5 5 5 5 5 7 7 7 7 7	Sall Passage
284848488888888888888888888888888888888	ă	5.55 5.66 5.66 5.66 5.66 5.66 5.66 5.66	\$6\$8\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	NDP
:2238 <b>283282</b> 22555	t	<b>约他们为对对对对对对为为为为为为为为为的</b>	######################################	2
1 198 1 226 1 233 1 234 1 247 1 254 1 266 1 266	1 277	123 129 129 129 129 129 129 129 129 129 129		TCF
3 1 3 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	391	\$65888858888888 \$758888888888888	88388888777587735888888888888887756877768777	J (L m-2N-14mn-1)
5 G T T T T T T T T T T T T T T T T T T	į	6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	\$ 48 85 \$ 45 \$ \$ 45 5 7 4 5 8 5 5 5 5 5 5 7 5 5 5 5 5 5 5 5 5 5 5	NPF (Limin)
3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	¥	88888888888888888888888888888888888888	######################################	15 ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( ( (
	ě	64	K6863837K389SSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSSS	Siage -
~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~	22.5			_1~_
				17
\$ 5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	52 : 3	8 円 株 内 内 内 内 内 内 内 内 内 内 内 内 内 内 内 内 内 内	######################################	20

	Slage/Event
	Comments
	Time (hos
100 100 100 100 100 100 100 100 100 100	\$Time
0.00 # # # # # # # # # # # # # # # # # #	13 g
######################################	Interstage 33 57
# # # # # # # # # # # # # # # # # # #	Conc 35 70
\$ 5 8 3 3 \$ 7 \$ 7 \$ 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	Tot Prod
	Rejection
00000000000000000000000000000000000000	191
89888889881778598988778559898989898989898989889888755555555	(VICI-VPCp/Ve)/Ca
235511235125125125125125125125125125125125125125	Sale Rejection
	SaR Passage
\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	S S
. ខណៈនទននេះ ខណៈខណៈខណៈខណៈខណៈខណៈខណៈខណៈខណៈខណៈខណៈខណៈខណៈខ	28
	1CF 1 229
	2 55
:	New (Comm)
2554418468187878787878787888887888888888888	NPF (ppm)
	Stage )
	_ =
	4
	1

(Cabulations)

ā	ឆ	Stage/Eveni
; 5		Commente RO Unit down
		Canan due
3024 40 3040 97 3042 97 3042 97 3042 97		Time (hrs) 2829 65
92299 2 11 PM 92299 3 12 PM 92399 7 46 AM 92399 8 46 AM 92399 10 46 AM 92399 11 46 AM 92399 11 46 AM	100 100 100 100 100 100 100 100 100 100	51.09 12.27 PM
222222	07775388871778888777788888788888888888888	Ī
18522223	2 4 2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	intersuage
49 30 48 24 34 34 34 34 34 34 34 34 34 34 34 34 34	124542	Cone
000000000000000000000000000000000000000		Toi Prod
		Rejection
2 8 8 8 8 8 2 2 2 2 0 0 0 0 0 0 0 0 0		
761		VICT-VPCP/VCF/CC
188522222	AANSATENANTANTANTANTANTANTANTANTANTANTANTANTANT	2
**************************************	日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日本の日	Sak Panage
: K & Q <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> & S <b>I</b> &	***************************************	Q.
3 <b>238</b> 5555	######################################	:
1111111111111		rcF
2 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	18 18 18 18 18 18 18 18 18 18 18 18 18 1	J (L m-2hr-1 sim-1)
	######################################	HPF (Umm)
10000000000000000000000000000000000000	\$284945574915055855578555758554855555585888555555855555555	Nos (gpm)
33222233		S.
77878885	**************************************	Steps 2
		-
73 50 50 50 50 50 50 50 50 50 50 50 50 50	######################################	

Recovery	2	58 8888455545548 88 8333588533565	######################################
belance from Col			
į	ではないます 日本 ないしょう ののおう するでき ちょう ちょく とくとく くくくくくくくくくくくくくくくくくくくくくくく 人名 日本 日本 日本 日本 日本 とう ストラント	**************************************	
Suga	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2.5	288888888888888888888888888888888888888
NPF (gpm)	2 K X 8 6 6 7 X 5 K 8 6 8 9 7 7 8 7 9 6 7 6 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7		**************************************
NPF (Umin)		00000000000000000000000000000000000000	9248#41878;2649##\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$
J (L. m-2he-1atm-1)	# C # # & 4 # # # # # # # # # # # # # # # #	\$\$ \$\$\$55 <b>3</b> \$\$\$\$\$\$\$ 64 66656885766666	
þ	2	200 200 200 200 200 200 200 200 200 200	
	<b>《命心感心死行江淮门传题用作的目的为广通传行以记行方</b>	** ***********************************	スカボスはおけれれれないないないないないないないないは、 おいまればない はんかい はんまい はんかい はんかい はんしゅう はいまい はんしゅう はいまい はんしゅう はいしゅう はんしゅう はんしゅう はんしゅう はんしゅう しゅうしゅう しゅうしゅう しゅうしゅう
ş	\$4 \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	\$35\$ <b>\$4\$</b> \$\$\$6\$\$55\$53535\$\$\$\$55 <b>\$</b> \$\$55555555555
Salt Passage	T		
See Pasterion		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	
VICE VIEW CONTRACTOR	**************************************	82 38888888888	##
	018080111111111111111111111111111111111	2	
-			######################################
3		0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	
,	2 4 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	82 253 25 25 25 25 25 25 25 25 25 25 25 25 25	
		は	
	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	33 33151717171717	
	100 100 100 100 100 100 100 100 100 100	95299 1 0 044 95299 2 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95299 3 0 049 95	100 100 100 100 100 100 100 100 100 100
1		222222222222222222222222222222222222222	
	Comments C		
	Bapp C verk		

	ű		ī	Slagar Vand
	Routine Testing		CO Line design days to decreasing days	Commanté
3452 22 3458 18 3458 18 3458 18 3460 10 3460 10 3461 16 3462 16 3462 40 3464 40 3464 40	340 11 340 11 340 11 340 12 343 22 343 22 344 22 344 22 344 22 344 22 344 22 344 22 344 22 344 22 344 22 344 22 344 22 344 22	300 20 30 30 30 30 30 30 30 30 30 30 30 30 30	3188 9 9 1 3188 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189 9 1 3189	Time (hra)
22	7555	0.000 (C) (C) (C) (C) (C) (C) (C) (C) (C) (C)		2
22222222222222222222222222222222222222	00000000000000000000000000000000000000	0.222222222222222222222222222222222222	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	į
100 00 00 00 00 00 00 00 00 00 00 00 00	35 74 36 80 35 20 32 20 32 20 32 37 32 18 31 25 31 br>31 31 31 31 31 31 31 31 31 31 31 31	# 12	2	32 St.
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	53 99 57 50 60 57 50 60 57 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 58 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 60 50 50 60 50 br>50 60 50 50 60 50 50 60 50 50 50 50 50 50 50 50 50 50 50 50 50	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	28 82 Come
200100111111111111111111111111111111111	0 58 0 58 0 58 0 58 0 58 0 58 0 58 0 58	00000000000000000000000000000000000000		Tot Prod
				Rejection 0.98
110 113 125 127 128 128 128 128	1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	- 000000000000000000000000000000000000	8
222227557	9 \$ 8 22 2 2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	23232222222222222222222222222222222222	8 8887474755288888888888888888888888888888	T DI
2000年100日 2000年100日 2000年100日 2000年100日 2000年100日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10日 2000年10	######################################	2	の名ののおおは、日本では、日本では、日本では、日本ののは、日本ののは、日本のは、日本のは、日本のは、日本のは、日本のは、日	Salt Rejection
7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB 7 BB	55555555555555555555555555555555555555	998 # 8 4 5 8 9 8 9 8 9 7 7 4 8 9 3 8 9 3 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8	2	Salt Panange
	664 664 641 518 518 527 527 528 530 530 530 530	\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	\$190 \$190 \$190 \$190 \$190 \$190 \$190 \$190	S S
22222222222222	######################################	5 5 5 2 3 2 2 2 2 2 2 5 5 5 5 5 5 5 5 5	7	8 8
1 219 1 223 1 223	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		110 100 100 100 100 100 100 100 100 100	1178
	2 2 1 2 1 3 2 2 2 4 3 2 3 6 8 2 2 2 1 3 3 2 3 5 8 8 2 2 2 1 3 3 2 3 5 8 8 2 2 2 2 2 2 2 2 2 2 3 3 3 3 3 3 3 3		# ####################################	J (1 m-2hr-1atm-1 3.21 3.17
22222222222222222222222222222222222222	20 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 4 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	0.000000000000000000000000000000000000	12.30
3 76 3 58 3 58 3 58 3 58 3 58 3 58 3 58 3 58	3 H 1 3 3 7 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	382323232222222222222222222222222222222	2833488888888887339851734887	3 2 1
	######################################	8422224928482828282828	2	<u>.</u>
		**************************************		┪
2012 20 8 8 8 20 20 20 20 20 20 20 20 20 20 20 20 20	75 - 27 - 27 - 27 - 27 - 27 - 27 - 27 -	######################################	2	79.12

	Siagostiven
	Comm
	erki.
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	5 (179 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17 to 17
	20
4 4 4 5 5 5 6 6 6 7 7 7 7 7 7 7 7 7 7 7 7 7 7	######################################
ARRANDRESERVES SECTIONS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRACTORS CONTRA	######################################
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	
	1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 5 1 1 1 5 1 1 1 5 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
QQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQQ	
######################################	2 2 2 2 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3
# 1 = # 2	# 15 15 15 15 15 15 15 15 15 15 15 15 15
***************************************	\$ 55 57 57 57 57 58 58 58 58 57 58 57 58 58 58 58 58 58 58 58 58 58 58 58 58
មិកមិក្សីក្រុមិទ្រឹម្មិទ្ធិនិងសេសសេសសេសសេសសេស នេះ នេះ នេះ នេះ នេះ នេះ នេះ នេះ នេះ នេះ	222222222222222222222222222222222222222
	2 = 2 = 2 = 2 = 2 = 2 = 2 = 2 = 2 = 2 =
	1
	20 4 4 4 4 4 4 4 4 2 0 0 0 4 4 0 0 1 4 4 4 4 4 4 4 4 4 4 4 4
2=1=3838	# 1
	\$248823286855588888888888
######################################	2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2

0(42m) 0(42m) 0(70m)	0	C M(SOA) B(SOA) B(STT)	>																			Stagent ven
	AVERAGE	AVERAGE AVERAGE	AVENAGE	TESTING	END OF SPECIAL	_					-				_	_					†	Comments
				371541	371111	371011	3700 11	3708 11	3706 11	3705 11	3704 11	3701 40	3699 2	3696.29	3697.28	3696 26	3695 29	1	3843	3642	100	Elapsod Time (hra)
				10/21/99 10:13 AM	_	_				_	-		_	_	_	_	10/20/96 2 05 PM	_	_	10 18 00 0 50 AM	-+	STIME
				12.39			-			ž		_	-	_		_				= :	1	Ē
				30 67	28 76	28 51	28 92	29 17	29 52	29 67	29 63	29 01	24.67	2	20 47	28 14		8	5	ž :		Haleralinge
				66.37	25 91	8	67 25	67 87	\$	80 12	67 60	8397	2	2	62.31	2	i	5	ş ĕ	8	513	C
				055	20	054	ŝ	0 62	286	ŝ	071	ŝ	9	ŝ	0 66	0.67	i	2	å	t i		Tol Prod
9 2 2 8 8 5 3 3 5 6	9723	95 55 46 11 12 12 14	98 02	0 98	ŝ	098	098	0	0 98	0	9	ŝ	0 98	980	0	98			99	9	8	Relaction
				100	28	- 29	1 29	2	1 22	2	ī	117	=	=	1 28	2	-	9	9	9	30,5	
				7.65	122	122	121	121	ī	132	Ē	- -	127	1.17	1 29	=	-	3 1	Ē:	2 2	3	PAICT-VACANCA
24 82 27 27 27 28 28 28 28 28 28 28 28 28 28 28 28 28	\$3 <b>98</b>	8 8 3 8 3 2 8 8	2	95.56	2	3.5	85 13	8 B	2	28	1 37	£	24	1	r	ŗ		:	8	8 2	R	VICT-VECAVCYCZ SAR Rejection
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	601	10 74 8 35 4 10	507	144	ŝ	442	4.87	è	5 18	5 6	5	ŧ	ž	5	5 50	5			374	3 77	181	Sall Passage
					626	637	2	621	91.	ê	ŝ	ş	577	570	185	592		į	900	921	5	₹
					•	#	2	8	:	E	Ξ	8	r	r	3	3:	_	-	ř	ř.	3	
				1034	1 020	1031	034	1037	ž	200	1 055	1 074	1071	ē	1 056	ě	-		055	0	3	ī,
					327	315	317	3 22	ĭ	331	331	319	-	ž	ž	1			5	8 3		C # 200 1 1 1 1 1
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	5 8	8 1 3 8 8 2 3 8	i		12 54	12 10	12:0	ź	12 78	1270	2	12.22	1 08	ž	ž	7. <b>8</b>		:	2		t	NOF COME
28878	38	347	3 81		22	320	3 22	328	33	×	3 35	323	<u>.</u>	J.	ž	33			213	2 2	,	
				136	:	14.6	1.7	:	14.5	:	=	13.0	ĩ	:	ĩ	=		= :	=	= ;		Ş
				31	•	•	•	:	:	•		:	:	:	•;	:	:	:		::		ĺ
													_	_		_		_	_	_		-y-
22 <b>888</b>	71 51	\$ 10 C C C C C C C C C C C C C C C C C C	2	91 53		8	8	80 3		8177		5	:	8 6	8	8		79 03	7	79 03		_

Table C-3
RO Operating Data
(Calculations)

, [		_			_	_	_			_	2			_	_			_				_					_									_			_	_				_		<b>-</b>	Γ				s	tagarEvent
Menta Mil	Wed 63/39	Tum 6/8/98	Mon 6/7/98	Sun GANA	341 6/5/99	Fri 84478	Thu 6/1/90	Wed 6/2/99	Bering out	Hon 5/31/39	Sun \$20090	\$6,600 to 14	SELECT OF 1	Tan 5/7700	Tue 5/25/99	Mon \$7499	Sun 5/23/99	Sat 5/22/98	Frt 5/21/76	Thu 5/20/99	Wed 5/10/90	Tue 5/18/99	May 5/17/00	Series and	Sat 5/16/00	51671400	Martin and	West School	Time City See	Sun 5/9/99	Set 5/8/799	Fri 5/7/98	Thu 5/8/59	Wed 5/5/99	Tue 5/4/99	SECTS NOTE	Sun 5/2/98	Sec 571/99	Thu 4/29/98	M=0 4/29/94	Tue 4/27/99	Mon 4/26/99	66/52/a un S	Sat 4/24/99	Section 13	Wed 4/21/98	Tue 4/20/991	Man 4/19/99	Sun 4/18/99	Set 4/17/99	Fn 4/16/99	ate
1	504.00		456 00	432.00	108.00	384.00	360.00	336.00	312.00	288.00	2 2	2 6 8		_	8 8	120,00			8																_							_					-		-	<b></b> .		iun Time (hrs)
t		_		_						7.13					_	_			_				_					_	è	:		_				_			_		7 52		_				t	7 40	_	_	·	н
T										1.851.00																			.000	3											1,483 00							1,850.00		-	168000	Conductivity (uS/cm)
			6.17	•				•								o													9	_															- -	799	T				,	OC (mg/L)
		_				0.17	0.18	01		029				5 5	2			_	012	0 1			_		_		_	_	0 23	:											•				222	22	029	031		-	0.25	urbidity (NTU)
						٤	1 60	8		ś			č						- 60	1 40																									8 8	2 28	210	ž			*	iDi
	_					0.55	0.69	8	·	042			ē	8 8	- 5				1 22	=									5 5												214				5 5	Ē	1.73	96			ī.,	Total Chlorine (mg/L)
						0.06	004	0 07		005			Ś	007	3				010	0 12									5 6	;											015				- C	0 1	0.08	0.07	_		<u>.</u>	ree Chiarine (mg/L)
			1.031.00													á	3												5	9							-											966.00			997.00	TDS (mg/L)
l		_	200	_								_				_			_	•	_	-				_																			_				_			Total Colfform CFU/100 mL)
							_												_													_			_										_							Fecal Coliform CFU/100 mL)
		29000				2200							30000						96000																						68000				B000		2					Pseudomonas (1000 ⁻¹ CFU/100mL)
			6,000 00				1,500.00		3,900.00							_				_																,				_												HPC (CFU/mL)
										7 32																				7 60										_	7.73						T	7 68			7.85	pH
										3,420 00																				80 SS 08											3,380.00							4.120 00			6,060.00	Conductivity (uS/cm)
						0.23	041	0 31		0.26				0.46	98				ě	0.67			_						1 1	į.						_					089				0.75	0 70	0.95	120			0.98	Turbidity (NTU)
l																							_			_																										SDI
			2,272							2.016.00							7 7 8 8													4 776 00											8							5,752 00			5,668.00	TDS (mg/L)
		_								8									_				_							ŝ		_		_	_	_					6 35				_		1	5			5 79	рн
										96 00						_			_				_							8 8											8					\$		9.19			42 10	Conductivity (uS/cm)
			ć	6													0.50													050															0.50	į	25					TOC (mg/L)
						_	9			0.14			_	0.04	0.15	_			9	5		L	_					_	200	0											9	_			8		-1-	9			0110	Turbidity (NTU)
		_				0.20	8	ŝ		8				0.40	ŝ				8	2	3						_													_					ê	8 6	5					SDI
			į	8						8		_				_	8		_	_			_							8																		8	3		24.00	TDS (mg/L)
		_				ķ	2	0 92		0.46				105	960					; ;	- 77	L													_													_				Total Chlorine (mg/L)
		_				<u> </u>	8	0.05		8				0.07	0 05				ŝ	2 2	2						_																				1				_	Free Chiorine (mg/L)
								_									700				_							_	_																			S				Total Coliform (CFU/106 mt.)
															_																																$\downarrow$					Fecal Collions (CFU/100 mL)
		_	8			2	:						100 00		_				8	Š																					Š	Š			22 00		ŝ	3				Pseudomones (CFU/100mL)
				800			é		1 200 00			-	_		200 00		170 00	_			_						-	56 00		142 00																	8	8	3			HPC (CFUANL)
				91 96						_		_			_	_	91 )1					1	_							92 73	•	_	_												53 13		93 74		_			n, TOC Removal
			•	95 93				_									92 75						_							86 23		_	_	_																		% TDS Removal
			\$				3						5 45						•	٠ <u>٠</u>												_	•							_		2			š			30				Log Reduction
2	Γ						2 !	: :	:	-				75 00	4231				_	8	2 2	1						_	78 2	80 00								_				8 8	_		22.7	75 00	1					% Turbidity Removal

Table C-4
RO Water Quality Data

	_									_	_																	۰										_									_			Stage/Event
Fri ANNA		OKAN DEM	Tue Drawe	Service Cars	Sad 7/31/90	Fri 7/30/99	Thu 7/29/98	Wed 7/28/99	Tue 7/27/98	Mon 7/26/99	Sum 7/25/99	Set 7/24/98	68.0727 U-1	Thu //2299	777200	W 1771 1000	72000	100 7/10 PM	S.m. 7/17/90	Fri 7/18/59	Thu 7/15/99	Wed 7/1 4/99	1 me 7/1 1/96	Mon 7/12/99	Sum 7/11/99	Ser 7/10/99	F0 7/8/99	Wed 7/7/98	Tue 7/6/99	Mon 7/5/99	247/7 CPS	Fri 7/2/90	Thu 7/1/98	GEOLVS PRIM	66.62.9 en.t	Man scanne	Sal 6/26/99	Fri 6/25/90	Thu 6/24/98	Wed 8/23/99	Tue 6/22/99	Sun 6/20/90	San 6/19/99	Fri 6/18/799	Thu 6/17/99	Wed 6/16/29	WANTED HOME	Sun 6/12/99	Sal 6/12/99	Date
1872.00	3 2	8	12400	17/8.00	1752.00	1728 00	1704 00	1880 00	1656 00	1632 00	1608.00	1584 00	960	536.00	8 8	161000	148.00	8 8	18 8	1392 00	1368 00	1344 00	1320 00	1296 00	1272 00	1246.00	1224 00	1178 00	115200	1128 00	1104 00	1056.00	1032 00	1008 00	984 00	8 2	91200	98.00	964 00	840 00	816.00	758 00	744 00	720.00	696 00	672 00	3 8	600.00		Run Time (hrs)
			,							_					_			ŝ						7 39				_	Į	7 09						720			_		i	Š					•			pН
			2	87.83	_					_					_		-	8	_			_	_	1.635.00			_		-	1,544.00				_		1.569.00			_		-	8	_	_			20/20	3		Conductivity (uS/cm)
		_	-	2		_				_								711											L	682				•••							:	6 71					*			TOC (mg/L)
0.13	3	2	000	0			0.08	_		_			č	, ,	_	0 1				9.14	1	:	:	0 13			9 3	2 2	Ê	315		ā	1	315	0.12	013		16	3	0 16	0 15	·		0.21	0 16	0 22	2 2	-		Turbidity (NTU)
हैं है	5	ž	ś	70		ŧ	š	ŝ					ģ	: è	8	70	3	é		.50	70		_						180	2 20											ั้ย	ē					5	5		SDI
9	2	0.15	0.59	9		0.72	129	1.56	9.77				į	ŝ	6		9	S		5	3	1 57	121	122			<u>.</u>	7.	187	98		1 36	6	66	147	6		36	ŝ	2.06	214	۸ 4		1 73	ž	1.74	237	ŝ		Total Chlorine (mg/L)
0.00	0	9	8	2		012	6	6	0.15	_			ē	5 3	် မ	(12)	0 NB	29		0 20	017	0 15	0 08	0.08			0 1	3 3	0 6	0 13		9	012	0.16	0 12	9		0.07	0 53	8	0.5	3		0.16	0 12	010	- 6	3		Free Chiarine (mg/L)
				8	_						_							791 00						989 00						961 00 00						8						920 <b>0</b> 0								TD\$ (mg/L)
	_																																			_			8							8				Total Coliform (CFU/100 mL)
					_				_						_								_			_			$\downarrow$				_						8											Fecal Coliform (CFU/160 mL)
13000			74000			580000			280000				•	0006			900			70000			17000				15000		000eE			Š			380000			58000			14000			57000			150000			Pseudomonas (1980'' CFW/100mL)
																																							_			170 00				1.400 00				HPC (CFU/mL)
				ž						_								6.92						? 91						713			_			7 35						763						7 63		pH
				5,460.00														4,290 00						5 540 00						4,000 00						3.550 00						2,700 00						4 620,00		Conductivity (u8/cm)
8	9	0.32	0.36	2	_	2	0.28	0.27	2 8		_			93	9	0.33	0.45	0.35		22	2 3	2	0,30	9			0.29	3	0 17	0.20				0.1	016	8		0.25	8	0.32	0.20	0 25		0.27	0 23	0.26	ž	- -		Turbidity (NTU)
ž	128	210	1.66	2.70	_	ž			3								_				•		_		~-						_																			ISDI II
				3 066 00														2 756 00						3 720 00						8						2,114.00						1.548.00								TDS (mg/L)
	_			5 39														5 75						2.7						603	_					8			_			621						6 02		рН
	_			150 00	_													06 00						115 00						65 00						72 00						67 00				_		\$ 8		Conductivity (uS/cm)
	_			0 50	_										_			0 50												8												0 50	_				_			TOC (mg/L)
0 10	9.33	0.05	0	0 02	_	8	2	8	2	0 05	_			2	005	004	0	0.07			2 5	5	9	9	:		0	9	-+-	\$			9 9	8	600	0 63		ŝ	8	9				8	9	9	90	007		Turbidity (NTU)
	_				_					_					_		-		_										2	200											8									SOI
	_			8	_					_								3 <b>6</b> 00	_				_	8	}				1	8						5 00						8								TDS (mg/L)
0.27	0.02	0.15	8	8			8	c	ķ	9				125	121	1.23	15	69		i	ŧ :	: :	٤	5 5	·		ī	:	2	9	:			5 2	ű.	ž		8	8	217	214	257	_	¥	ž	÷	210	1 28		Total Chlorine (mg/L)
0 07	0 02	2	0.13	000					3	000				020	0.25	0.28	0.20	954		į	021	3 6		5 5	:		000	010	0	0 00			6 6		010	0 07		ş	2 3	9	015	006		9	0.13	210	900	8		Free Chlorine (mg/L)
																																				3 00			8							8				Total Collform (CFU/100 mL)
	_		_											_	_								_																_			2.00								Facal Coliform (CFU/100 mL)
<b>87 90</b>			8	•			8			J 00					8		8				36		-	ě			8 00			<u>ت</u> 8			16 08		00 00			:	27 00		8			á	3		290 06		_	Proudomonas (CPU/100mL)
		800		600 00																		;	 6 8	-	á				80 00	8		_			5	700 00						98	_			350 00				HPC (CFUIL)
	_	_		91 68										_	-		_	92 9/		_									1		3								_			92 55								% TOC Removal
				8	_							_						3 :0							ï					2			-	_		95 47	-					8								% TDS Removal
	_	_	697		_	•	714		_	693							9		_		6 33			0 11			6 27	_		<u>.</u>			6.23	_		:			۔۔۔۔ د	_	6				 5		571			% TOS Removal
23 0	ě		8 8	75.0	_		75.00	£2.50	5	5.5				 ان	9	77 %	6	53 33			2	2	2	2	<u>و</u> و		8	2 3	06 67	78 57	8		68 75	71 43	8 8	1 1			8 8	3 3	8	2			7 2	77 27	53 65	66		% Turbidity Removal

Table C-4 RO Water Quality Data

erut A		_	33.33		_	46 15		, 98 66				8	2 2 2	11.11	8 4		_				_			_	-	8 8	_			5	8	_	8000			8 8		2 2 2			1	7.	8 8	8		
ey Son		2 6 	_	*		_	5.54	_											_		_	_					20	!		_			_		_											
801 A	ž											\$ \$			_			_						_			_			*					-	Ř					93 72			_		
301.2		_				93 15	_									_								_						91 62	_						_		_			_	8			
13) DeH	11,000,00	1,000 00				8																								400 00											330 00		80 94 94			
Posturio)		90 00		67.00			92 00		5																		00.085	3											_					_		
Feed C																							_		_					_				_		_								_		_
S) MetoT INUNIO)								_						_	_				_						_					5											_			_		
Erse Ch	0.03	000	0 05	ş			900	0 02	0 05			90.0	600		000						_			_		91.0	0 0			800	900		0 05			0 0		0 12	912	_	305	900	003	. 8		
to mor	800	8 8	0.02	0.25			0.24	000	200	,		<b>2</b>	8 3		9						_		_			86.0	8 8	<u> </u>	_	0.65	0.50		ğ			860	-	1 10	£20		20:0	610	910	¥		
pm) 801	1 8			_		, ,						8	_						_											33.00						8		_	_		62 00			_	_	_
MbidnuT KG2	0.10	700	90.0	700	_		B 0	0.03	900			•00	0 02			:			_		_					00	8 8	 8		100	<b>9</b> 0.0	_	900			003	-	600	200		500	0.02	8 5	200	 !	_
m) 201						5	3																							020													8			_
Conduc	128.00			_		8	3					89.00															_			127.00						8	_				107 00					_
Hq	0 552		_		_						_	525			_						_		_		_	_	_		_	2 40				_		_					69.5			_		_
pm) 201	2,936.0		_			_	?					1160			_				_		_									3,7520			_			4.0120					5,186.0					
kÇS	- 5	0.50				_		80				080		8	8 8	3					_						8 9	-		0.80	080	5 90				8 5	2	2.30	8					- 25	-	_
pibidnu1		0.24	25	0.24				91.0	6	576			0 83	0 0	, ,	-		_		_		•				0.28	60	620					0.03				7	1	021				3 3	2 2	3	
Conduct	4.550.00					-	3.000.0	_				4 700 00																	_	5.930 00						2890.00	<u>.</u>				6.940.00					_
на	\$	- ~-	_			;	9					3.10			_															9 56			_			613	_				20.2	_				_
43) S4H			_			_					_	_			_								_		_			_	_	1,600 00											1,790 00	_	1.600 00			_
(1000., C		110000		2000			32000			9000																		94000																		
Pecal Co (CFU/100			•	_							•		_	-	_	_		_			•	-		_	_				-	8			_		_			_	-	_			-		_	_
ioo ideoT idenUFIO)											_										_						_			8			_					_	_	_		_		_		
gen) 201	8						968.00					91200																		962 00						1,008.00										
Free Chir	900	900	9 0	000	_		0 0	000	0.03	8		8	0.02	000	00	600	_		_		_		_		_	0.14	0.16	9.15		9000	8		204			8	8	900	5	_	0 05	8	9	2 5	6	_
100m CNJ	8	0.07	0.08	9 22		_	91.0	00	0.03	8	_	0.52	900		9.0	<u>.</u>			_	_		_		_	_	8	13,	=			_		200	:		8	5	195	0.82		8	9.0	8	Į :	ŝ.	
ю	8	-	8 9	8	205			8	080	8		5	8		8	S .			_		_						\$ 20	2.30		90	8	2 80				2	8	5	2.80							
(hbidan)	9	600	0.13	8 8	_		5 5	8	8	8		800	000	\$1.0	8	• •			_		_	_	_		_	000	0.12	901		-	\$		2		_	600	0.5		<b>8</b> 0 0		600	8	<b>8</b> 00	8 :	-	
70C (mg																		_					_								_												6.57			_
Conduction					_						_				_											_			_	Ē																
Hq		_	_		_		_			_				_				_	_	_	_			_		_	_	_				_			_				_				_	_	_	_
									_				_																								_									3264 00
1	Sun Brange	28	Š	5 5	See British	115/1	5	\$ 5	5	Fr 8/20/99	Set 6/21/8	Mon 8/23/79	Tue 8/24/98	*25	2	F# 8/27/86		900	6.154	Med 9/1/88	W	Ş	\$		Š	Ş	Š	2016	5		\$158	66/51/6 Pem	5	Sar Brillian	2	Mon 9/20/99	Tue 9/21/99	Thu \$/23/88	F# 9/24/89	W25V	Sun 9/24/99		Wed sizers	9308	F# 101/39	102/1
****		3	Med British	Thu 6/12/99	3,	Sun 8/15/99	Mon British	1	Thu Brisking	E		3	3	3	Ē	Œ.	3	į	3	ż	£	ű	ä.		2	*	Ě	Ε	š	5 5	,5	š	ŧ.		9	ŝ	5 ;	Ē	Ē	ž	5	1	*	Ĕ	*	•
	Long to the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control o	201 7. 170 (Creduction of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character of the Character	25. 23. 25. 25. 25. 25. 25. 25. 25. 25. 25. 25	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	200	1000000	201	1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.000   1.00	1	201	1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985   1985	100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100	1	1   1   1   1   1   1   1   1   1   1					March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   Marc			March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   Marc		March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   Marc			March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   Marc	New York		Note								The content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the		The content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the	The content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the		The content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the	The content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the	The content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the	The content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the content of the

Page 3 of 4

	0			n			•			>							Stage/Event
MAX.	Ę	MEAN	MAX	E	MEAN	MAX	¥.	MEAN	WAX	ž Z	MEAN	Fri 10/8/99	Thu 10/7/29	Med 104/99	Tue 10/5/99	Mon 10/4/98	Date
			L									3408 00	3384.00	3360.00	3336.00	331200	Run Time (hrs)
7.39	-	6.22 1	7.48	7.09 1	7.30	7.13	7.13	7.13	7.52	7.46	*	L					рН
.893.00	1,211.00	563 44	.573.00	S#1.80	560.00	.651.00	1,651.00	1,651.00	630.00	,483.00	,556.50	l					Conductivity (uS/cm)
7.30	6.01	6.62	6.82	6.71	6.77	6.18	6.17	-	7.99	2	754						TOC (mg/L)
0.24	0.06	9.11	0.22	9.3	0.16	0.29	0.12	0.18	0.44	0.16	0.25						Turbidity (NTU)
22	0.80	ž	2.50	8	Ē	1.80	6	1.66	2.30	1.90	2.07		1 60				SDI
7	0.02	0.70	2.64	1.10	1.71	1.41	0.42	0.92	2.14	1,24	1.62	Γ					Total Chlorine (mg/L)
2	0.02	0.13	0.18	8	0.12	0.12	8	0	0.15	0.10	0.12		_				Free Chlorine (mg/L)
.006.00	791.00	898.67	961.00	920.00	943.33	1.031.00	966.00	998.50	929.00	929.00	929.00						TDS (mg/L)
8	8	8.08	8.00	8	<u>\$</u>	2.00	2.00	2.00									Total Coliform (CFU/100 mL)
8	3.8	8	2.00	2.00	2.00												Fecal Coliform (CFU/100 mL)
580000	š	97636	380000	3600	87950	96000	2200	39300	68000	8000	38000						Pseudomonas (1000° CFU/100mL)
1.700.00	1,000.00	1 444 35	4,400.00	170.00	864.87	6,000.00	1,500.00	3,274.18								1.000.00	HPC (CFU/mL)
7.61	3.10	8	7.63	7.13	7.44	7.32	7.32	7.32	7.73	7.60	7.67						рН
6 946 00	4,290.00	5 364 67	4,620.00	2,700.00	3,717.50	3,420.00	3,420.00	3,420.00	6,250.00	3,380.00	4,815.00			_		•	Conductivity (u5/cm)
ž	0.14	0.36	1.62	0.14	0.32	1.40	0.23	2.0	1.35	0.70	0.97						Turbidity (NTU)
8	0.30	1.57															SDi
5,186,00	2,758.00	3,503,22	2,114.00	.44.8	1,702.00	2,796.00	2,016.00	2,341.33	4.776.00	11.00	2,393.50						TD\$ (mg/L)
ž	5.25	2	6.21	6.00	6.07	6.00	8	9.00	6.35	6.01	6.16						рH
56.00	71.00	109.58	72.00	4.00	62.50	86.00	98.00	86,00	80.00	9.04	11.11						Conductivity (uS/cm)
8	0.50	8	0.50	0.50	950	0.50	0.50	0.50	0.50	0.50	0.50						TOC (mg/L)
=	0.02 2	8	0.07	0.03	8	0.15	0	0.08	8	ŝ	9.				_		Turbidity (NTU)
			0.50	Š	2	8	20	0.33	9.56	ŝ	0.47	L			_		<b>S</b> DI
62.00	29.00	5.11	56.00	34.00	ŧ	70.00	8	\$1.00	35.00	35.00	35.00	L					TD\$ (mg/L)
5	0.02	0.72	2.57	<b>1</b>	1.71	1.37	8	0.90				L		_			Total Chiorine (mg/L)
ï	0.02	0.11	0.19	9	0.11	0.09	0	0.06				L					Free Chlorine (mg/L)
8	8	ē	8	8	2.2	7.88	8	7.00				L					Total Coliform (CFU/100 mL)
			2.00	2.00	2.00							L					Fecal Coliform (CFU/180 mL)
380.00	7.00	68.57	1,700.00	<b>9</b> .06	270.75	100.00	30.00	50.25	22.00	9	13.50						Pseudomones (CFU/100mL)
1000.00	10.00	274.43	700.00	.08	85.18	1,200.00	10.00	110.28	142.00	32.00	76.67					350 00	HPC (CFUINL)
93.15	97. <b>6</b>	92,40	92.67	92.55	92.61	91.91	91.90	91.96	93.74	92.73	93.34			_			% TOC Removal
3.9	93.72	<b>8</b> 5.56	30	<b>9</b> 4.17	M .32	95.93	92.75	ĭ	96 23	M.23	<b>36</b> ,23				_		% TD\$ Ramovai
7.1	4.47	5.97	82.0	4 18	5.79	6.51	5	5.67	713	5.54	5.35	Γ			_		% TDS Ramovai
88	Ξ	57.29	<b>30.00</b>	53.65	=	75.00	25.00	54.14	H 16	72.73	78.47		_			_	% Turbidity Removal

Table C-4 RO Water Quality Data





CH2M HILL

Applied Sciences Group

2300 NW Walnut Blvd

Corvatlis, OR

97330-3538

P.O. Box 428

Corvallis, OR

97339-0428

Tel 541.752.4271

Fax 541.752.0276

September 22, 1999

McAllen WWTP #2, City of

149462.A1.ZG

RE:

Analytical Data for McAllen WWTP #2, City of

Applied Sciences Group Reference No. 9964

Dear Angie Fernandez/PHX:

On August 18, 1999, CH2M HILL Applied Sciences Group received four samples with a request for analysis of selected parameters.

The analytical results and associated quality control data are enclosed. Any unusual difficulties encountered during the analysis of your samples are discussed in the case narrative. Subcontracted analyses reports are attached.

Under CH2M HILL policy, your samples will be stored for 30 days after reporting. If you have not given us prior instructions for disposal, we will contact you if any samples require disposal as hazardous waste.

CH2M HILL Applied Sciences Group appreciates your business and looks forward to serving your analytical needs again. If you should have any questions concerning the data, or if you need additional information, please call Ms. Kathy McKinley at (541) 758-0235, extension 3120.

Sincerely,

Kelly Ensor

Senior Administrative Assistant

Mugneer

**Enclosures** 

## CLIENT SAMPLE CROSS-REFERENCE

## CH2M HILL Applied Sciences Group Reference No. 9964

Sample ID	Client Sample ID	Date Collected	Time Collected
996401	ZGP	8/17/99	7:30
996402	ROP	8/17/99	7:30
996403	ROC	8/17/99	7:30
996404	WWTP#2Effluent	8/17/99	7:30

# CASE NARRATIVE GENERAL CHEMISTRY

Lab Reference No.: 9964

#### Client/Project: McAllen WWTP #2, City of

I. <u>Holding Time</u>:

All acceptance criteria were met.

- II. Analysis:
  - A. Calibration:

Bromide recovery (132%) in final calibration verification exceeded acceptance criteria. All other acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>Matrix Spike Sample(s)</u>:

Bromide matrix spike recovery (200%) exceeded acceptance criteria. All other acceptance criteria were met.

D. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

E. <u>Lab Control Sample(s)</u>:

All acceptance criteria were met.

F. Other:

Not applicable.

IV. Documentation Exceptions:

None.

V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by:

Reviewed by:

#### CASE NARRATIVE METALS

Lab Reference No.: 9964

Client/Project:	McAllen	WWTP	#2,	City of	ρf
-----------------	---------	------	-----	---------	----

I. <u>Holding Time</u>:

All acceptance criteria were met.

II. <u>Digestion Exceptions</u>:

None.

- III. Analysis:
  - A. <u>Calibration</u>:

All acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>ICP Interference Check Sample</u>:

All acceptance criteria were met.

D. Spike Sample(s):

All acceptance criteria were met.

E. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

F. <u>Laboratory Control Sample(s)</u>:

All acceptance criteria were met.

G. <u>ICP Serial Dilution</u>:

Not Required.

H. Other:

None

IV. <u>Documentation Exceptions</u>:

None

V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by: _	Que	2010	
Reviewed by:		WUSH	

Client Information

Lab Information

Client Sample ID: ROC

Lab Sample ID: 996403

Project Name: McAllen WWTP #2, City of Project Manager: Angle Fernandez/PHX

Date Received: 08/18/1999 Report Revision No.: 0

Sampled By: R. Trevino Sampling Date: 08/17/1999 Analyzed By: MG/DK/MS

Sampling Time: 7:30

Type: Grab Matrix: Water Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
N-Nitrate	0.20	35.4		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.72		mg/L	EPA 351.4	08/25/1999
Total Dissolved Solids	5	3,230		mg/L	EPA 160.1	08/23/1999
TOC	5.0	33.7		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.25	9.89		mg/L	EPA 365.2/4	08/19/1999

Client Information

Lab Sample ID: 996404

Client Sample ID: WWTP#2Effluent

•

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Date Received: 08/18/1999 Report Revision No.: 0

Lab Information

Sampled By: R. Trevino Sampling Date: 08/17/1999 Analyzed By: MG/DK/MS

Sampling Date: 08/17/ Sampling Time: 7:30 Reviewed By:

Type: Grab Matrix: Water

Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
N-Nitrate	0.04	2.96		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	08/25/1999
Total Dissolved Solids	5	799		mg/L	EPA 160.1	08/24/1999
TOC	0.50	8.39		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.25	2.98		mg/L	EPA 365.2/4	08/19/1999

Client Information

Lab Information

Client Sample ID: ZGP

Lab Sample ID: 996401

Project Name: McAllen WWTP #2, City of Project Manager: Angle Fernandez/PHX

Date Received: 08/18/1999 Report Revision No.: 0

Sampled By: R. Trevino Sampling Date: 08/17/1999 Sampling Time: 7:30 Analyzed By: DK/MG/MS/JJB
Reviewed By: 3

Type: 7:30
Type: Grab
Matrix: Water
Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
Alkalinity (as CaCO3)	2.0	121		mg/L	EPA 310.2	08/23/1999 -
Bromide	0.020	0.132		mg/L	EPA 300.0-B	08/19/1999
Chloride	1.0	160		mg/L	EPA 300.0-A	08/23/1999
Color (APHA) Apparent		22		color units	EPA 110.2	08/18/1999
Fluoride	0.10	1.07		mg/L	EPA 300.0-A	08/23/1999
N-Nitrate	0.10	9.55		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	08/25/1999
Silica-React.	0.40	15.1		mg/L	SM4500-Si D	09/01/1999
Sulfate	1.0	150		mg/L	EPA 300.0-A	08/23/1999
Total Dissolved Solids	5	774		mg/L	EPA 160.1	08/23/1999
TOC	0.50	7.48		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.25	2.48		mg/L	EPA 365.2/4	08/19/1999
UV-254	0.009	0.129		asb/cm	SM5910	08/19/1999

Client Information Lab Information

Client Sample ID: ZGP Lab Sample ID: 996401

Project Name: McAllen WWTP #2, City of Analysis Method: SW 8260B Project Manager: Angie Fernandez/PHX Units: µg/L

Project Manager: Angie Fernandez/PHX
Sampled By: R. Trevino
Date Received: 8/18/99
Date Collected: 8/17/99
Date Analyzed: 8/27/99
Time Collected: 7:30
Dilution Factor: 1

Type: Grab Report Revision No.: 0

Matrix: Water Reported By: MCB

Basis: As Received Reviewed By: SAN

Analyte	CAS#	Reporting Limit	Sample Result_	Qualifier
Duranahla Valatilan				
Purgeable Volatiles	75-01-4	1.0	1.0	U
Vinyl Chloride			· · ·	
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	U
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	Ų
1,1,1-Trichloroethane	71-55-6	1.0	1.0	U
Carbon Tetrachloride	56-23-5	1.0	1.0	U
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	1.0	U
Dibromofluoromethane	1868-53-7		94%	SS
1,2-Dichloroethane-d4	17068-07-0		89%	SS
Toluene-d8	2037-26-5		103%	SS
p-Bromofluorobenzene	460-00-4		103%	SS

E=Estimated value above instrument calibration range

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

SS=Surrogate standard

**Client Information** 

**Lab Information** 

Client Sample ID: ZGP

Lab Sample ID: 996401

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Analysis Method: SM 5710.D

Sampled By: R. Trevino
Date Collected: 8/17/99
Time Collected: 7:30
Type: Grab

Date Received: 8/18/99 Report Revision No.: 0 Analyzed By: BDW

Matrix: Water
Basis: As Received

Analyzed By: BDW Reviewed By: 2494

#### SDS-HAA/THM Formation Potential Test Conditions

	Target			Contact	Chlorine	
Set-up Date/Time	Contact Time (h:mm)	Initial pH	Contact pH	Temperature (°C)	Dosage (mg/L)	
8/23/99 9:34	72:00	7.7	7.8	23	10.10	

#### Chlorine Demand Test Results

Take-off Date/Time	Actual Contact Time (h:mm)	Measured pH	Measured Temperature (°C)	Chlorine Residual (mg/L)	
8/26/99 13:10	75:36	7.8	23	0.68	

**Client Information** 

Lab Information

Client Sample ID: ROP

Lab Sample ID: 996402

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Date Received: 08/18/1999 Report Revision No.: 0

Sampled By: R. Trevino Sampling Date: 08/17/1999 Sampling Time: 7:30

Type: Grab Matrix: Water Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
Alkalinity (as CaCO3)	2.0	14		mg/L	EPA 310.2	08/23/1999 -
Bromide	0.020	0.020	U	mg/L	EPA 300.0-B	08/19/1999
Chloride	0.10	9.73		mg/L	EPA 300.0-A	08/23/1999
Color (APHA) Apparent		5	U	color units	EPA 110.2	08/18/1999
Fluoride	0.10	0.32		mg/L	EPA 300.0-A	08/23/1999
N-Nitrate	0.01	1,11		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	08/25/1999
Silica-React.	0.40	0.65		mg/L	SM4500-Si D	09/01/1999
Sulfate	0.10	4.00		mg/L	EPA 300.0-A	08/23/1999
Total Dissolved Solids	5	33		mg/L	EPA 160.1	08/23/1999
TOC	0.50	0.63		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.05	0.10		mg/L	EPA 365.2/4	08/19/1999

**Client Information** 

Lab Information

Client Sample ID: ROP

Lab Sample ID: 996402

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Date Received: 8/18/99
Report Revision No.: 0

Sampled By: R. Trevino Sampling Date: 08/17/99 Reported By: JG Reviewed By:

Sampling Time: 07:30 Type: Grab Matrix: Water

Basis: As Received

Analyte	MRL	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
						7.1
Aluminum, Al	45.6	45.6	U	μg/L	SW6010B	08/27/99
Arsenic, As	3.9	3.9	U	μg/L	SW6010B	08/27/99
Barium, Ba	0.81	0.81	υ	μg/L	SW6010B	08/27/99
Cadmium, Cd	0.38	0.38	U	μg/L	SW6010B	08/27/99
Calcium, Ca	21.3	714		μg/L	SW6010B	08/27/99
Chromium, Cr	7.2	7.2	IJ	μg/L	SW6010B	08/27/99
Iron, Fe	2.8	9.9		μg/L	SW6010B	08/27/99
Lead, Pb	2.3	2.3	U	μg/L	SW6010B	08/27/99
Magnesium, Mg	41.0	197		μg/L	SW6010B	08/27/99
Manganese, Mn	1.0	1.0	U	μg/L	SW6010B	08/27/99
Mercury, Hg	0.25	0.25	U	μg/L	SW7470A	08/23/99
Potassium, K	181	1360		μg/L	SW6010B	08/27/99
Selenium, Se	6.8	6.8	U	μg/L	SW6010B	08/27/99
Silver, Ag	8.0	8.0	U	μg/L	SW6010B	08/27/99
Sodium, Na	593	13000		μg/L	SW6010B	08/27/99
Strontium, Sr	28.6	28.6	U	μg/L	SW6010B	08/27/99
Zinc, Zn	2.3	7.2		μg/L	SW6010B	08/27/99

Client Information	Lab Information

Client Sample ID: ROP Lab Sample ID: 996402

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Sampled By: R. Trevino Date Collected: 8/17/99 Time Collected: 7:30 Type: Grab

> Matrix: Water Basis: As Received

Analysis Method: SW 8260B

Units: µg/L Date Received: 8/18/99 Date Analyzed: 8/27/99

Dilution Factor: 1 Report Revision No.: 0 Reported By: MCB Reviewed By: >474

Analyte	CAS#	Reporting Limit	Sample Result	Qualifier
Purgeable Volatiles				
Vinyl Chloride	75-01-4	1.0	1.0	U
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	U
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	Ŭ
1,1,1-Trichloroethane	71-55-6	1.0	1.0	U
Carbon Tetrachloride	56-23-5	1.0	1.0	U
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	1.0	U
Dibromofluoromethane	1868-53-7		96%	SS
1,2-Dichloroethane-d4	17068-07-0		96%	SS
Toluene-d8	2037-26-5		104%	SS
p-Bromofluorobenzene	460-00-4		103%	SS

E=Estimated value above instrument calibration range

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

SS=Surrogate standard

Client Information

Lab Information

Client Sample ID: ROP

Lab Sample ID: 996402

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Analysis Method: SM 5710.D

Sampled By: R. Trevino
Date Collected: 8/17/99
Time Collected: 7:30

Date Received: 8/18/99 Report Revision No.: 0 Analyzed By: BDW

Type: Grab Matrix: Water

Basis: As Received

Analyzed By: BDW Reviewed By: SA2

#### SDS-HAA/THM Formation Potential Test Conditions

	Target			Contact	Chlorine	
Set-up Date/Time	Contact Time (h:mm)	Initial pH	Contact _pH	Temperature (°C)	Dosage (mg/L)	
8/23/99 9:42	72:00	6.0	7.8	23	1.30	

#### Chlorine Demand Test Results

Take-off Date/Time	Actual Contact Time (h:mm)	Measured pH	Measured Temperature (°C)	Chlorine Residual (mg/L)
8/26/99 13:14	75:32	7.8	23	0.24

	Formation Potential Test Conditions										
		FP	Free	Free	Total	FP	Measured	FP	FP	FP	FP
Client ID	Lab ID	Dose	Residual	Demand	Residual	Temp.	pН	Start	Take-Off	Time H:M	Time (Hour)
McALLEN-ZGP	996401	10.10	0.68	9.42		23	7.78	8/23/99 9:34	8/26/99 13:10	75:36	75.60
McALLEN-ROP	996402	1.30	0.24	1.06		23	7.77	8/23/99 9:42	8/26/99 13:14	75:40	75.67
					·						
			<del></del>								!

Formation Potential Trihalomethanes (THMs) Disinfection By-Products, (ug/L)										
		FP	FP	FP	FP	FP				
Client ID	Lab ID	CHC13	BDCM	DBCM	CHBr3	TTHM				
McALLEN-ZGP-3D	300301	150	38.8	9.5	<l< td=""><td>198</td><td>CHCl3 = Chloroform</td></l<>	198	CHCl3 = Chloroform			
McALLEN-ROP-3D	300302	3.7	1.7	<1	<l< td=""><td>5.4</td><td>BDCM = Bromodichloromethane</td></l<>	5.4	BDCM = Bromodichloromethane			
							DBCM = Dibromochloromethane			
							CHBr3 = Bromoform			
A STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STA										
							EPA TTHM Stage 1 MCL = 80 ug/L			
					1		EPA TTHM Stage 2 MCL = 40 ug/L			
			1							

			Formation Pot	ential Haloac	etic Acids (HAA	s) Disinfection B	y-Products (ug	/L)			
		FP	FP	FP	FP	FP	FP	FP	FP		
Client ID	Lab ID	MCAA *	MBAA *	DCAA *	TCAA *	BCAA	DBAA *	HAA5	HAA6		
McALLEN-ZGP-3D	300301	8.6	1.4	49.9	57.3	12.8	1.6	119	132		
McALLEN-ROP-3D	300302	<2	<l< th=""><th>1.1</th><th>&lt;1</th><th><l< th=""><th>&lt;1</th><th>1.1</th><th>1.1</th><th></th><th></th></l<></th></l<>	1.1	<1	<l< th=""><th>&lt;1</th><th>1.1</th><th>1.1</th><th></th><th></th></l<>	<1	1.1	1.1		
						ļ					
			·		ļ	<del> </del>					
					<b>†</b>						
											1
		MCAA = Monoc	hloroacetic acid	-	BCAA = Bromo	ochloroacetic acid	1	EPA HAA5 Stage 1 l	MCL = 60 ug/L	1	
	·	MBAA = Monot	romoacetic acid		DBAA = Dibromoacetic acid		EPA HAA5 Stage 2 h	MCL = 30 ug/L		1	
		DCAA = Dichlo	roacetic acid		* These compos	unds make up the	HAA5				
		TCAA = Trichlo	roacetic acid		= Estimated var	lue					

Client Information

Client Sample ID: McAllen-ZGP-3d

Lab Sample ID: 300301

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Date Received: 8/26/99 Report Revision No.: 0

**Lab Information** 

Sampled By: B. Warloe
Date Collected: 8/26/99
Time Collected: Not Indicated

Analyzed By: DAH Reviewed By: mbos

Type: Grab Matrix: Water Basis: As Received

Analyte	CAS#	MCL*	Reporting Limit	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
Haloacetic Acids								
Chloroacetic acid	79-11-8		2.0	8.6		μg/L	SM 6251.B	9/3/99
Bromoacetic acid	79-08-3		1.0	1.4		μg/L	SM 6251.B	9/3/99
Dichloroacetic acid	79-43-6		5.0	51.4		μg/L		9/16/99
Trichloroacetic acid	76-03-9		5.0	56.0		μg/L	SM 6251.B	9/16/99
Bromochloroacetic acid	5589-96-3		1.0	12.8		μg/L	SM 6251.B	9/3/99
Dibromoacetic acid	631-64-1		1.0	1.6		μg/L	SM 6251.B	9/399
HAA5	001 04 1	60	5.0	119		μg/L	SM 6251.B	9/16/99
HAAS		00	3.0	110		µg/L	ON 0231.D	3/10/33
2,3-Dibromopropanoic ac	i 600-05-5			116%	SS			
Trihalomethanes								
Chloroform	67-66-3		5.0	150		μg/L	EPA 502.2	9/1/99
Bromodichloromethane	75-27 <b>-</b> 4		1.0	38.8		μg/L	EPA 502.2	8/31/99
Dibromochloromethane	124-48-1		1.0	9.5		μg/L	EPA 502.2	8/31/99
Bromoform	75-25-2		1.0	1.0	U	μg/L	EPA 502.2	8/31/99
	75-25-2	90			U			
TTHM		80	1.0	198		μg/L	EPA 502.2	9/1/99
1,2-Dichloroethane-d4	17068-07-0			102%	SS			

U=Not detected at specified reporting limit *=MCL according to Stage 1 of D/DBP rule SS=Surrogate standard

Client Information Lab Information

Client Sample ID: McAllen-ROP-3d Lab Sample ID: 300302

Project Name: McAllen WWTP #2, City of Date Received: 8/26/99
Project Manager: Angie Fernandez/PHX Report Revision No.: 0
Sampled By: B. Warloe Analyzed By: DAH

Sampled By: B. Warloe
Date Collected: 8/26/99
Time Collected: Not Indicated
Type: Grab

Matrix: Water
Basis: As Received

Analyte	CAS#	MCL*	Reporting Limit	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
Haloacetic Acids								
Chloroacetic acid	79-11-8		2.0	2.0	U	μg/L	SM 6251.B	9/3/99
Bromoacetic acid	79-08-3		1.0	1.0	U	μg/L	SM 6251.B	9/3/99
Dichloroacetic acid	79-43-6		1.0	1.1		μg/L	SM 6251.B	9/3/99
Trichloroacetic acid	76-03-9		1.0	1.0	U	μg/L	SM 6251.B	9/3/99
Bromochloroacetic acid	5589-96-3		1.0	1.0	U	μg/L	SM 6251.B	9/3/99
Dibromoacetic acid	631-64-1		1.0	1.0	U	μg/L	SM 6251.B	9/3/99
HAA5		60	1.0	1.1		μg/L		9/3/99
2,3-Dibromopropanoic ac	i 600-05-5			115%	SS			
Trihalomethanes								
Chloroform	67-66-3		1.0	3.7		μg/L	EPA 502.2	8/31/99
Bromodichloromethane	75-27-4		1.0	1.7		μg/L	EPA 502.2	8/31/99
Dibromochloromethane	124-48-1		1.0	1.0	U	μg/L	EPA 502.2	8/31/99
Bromoform	75-25-2		1.0	1.0	U	μg/L	EPA 502.2	8/31/99
TTHM		80	1.0	5.4		μg/L	EPA 502.2	8/31/99
1,2-Dichloroethane-d4	17068-07-0			9 <b>9</b> %	SS			

U=Not detected at specified reporting limit *=MCL according to Stage 1 of D/DBP rule SS=Surrogate standard

Reviewed By: mbos

#### CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Walnut Boulevard Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0278

Project	<u> </u>	_							urcl		- ^	nda:	. #				<del></del>	_											COC #		
Project	*								чи	168	• •	IUOI	#				1	<u> </u>			Requ	ested	Analyti	Cal Met	thod #			THIS AREA F			NLY
Project	Mana							L	_								-											Lab#	- ['	Page	of
Project M C Compa	Name		0.	. 11.	^*	1	). /		1	$\zeta_{\mu}$	١,	1.					O	ł				- 5			73	20		4464			131
1110	<u> 1411e 1</u>	<u>l</u>	Ke	u	re.	$\mathcal{L}$	/ /(	<u>77</u>		<u></u>	uc	4					<b>-  î</b>	Ι.				NO2	2 3		800	0 3		Lab PM		Custody	Review
Compa	y Name	F	/	'n	n I	Ι.							•					13	7	ر در در	n a	7 2	5 5		2 0	7 6			- }		
<u> </u>	y O Manager	+	_/_	110	7411	el	<u>ν</u>	Τ.										26	າ ເ	4 6	4 E	50	25		50	8 3		Log In		IMS Var	ification
-	•			tact	& PI	юпо	₩.	1	epo		•						F	İ		HAAS, THMS	SDS HAAS	TKW 1803-1802	KW, NO3-NOZ)	0.5	THOSPHOLOUS	KU, NO3-NO2	· ~	Log		LING VOI	mounon
Kalh	Mik	nl	ey					14	all	4		lck	41	ı/a	4		S	?	ا ا د	505 205	5.5	2 0	ジュ	0	2,4	29	Q.				
Request	d Comple	tlor	Date	<b>e:</b>	Site	ID		_								isposal:	N T	~	2	Sp	SD	17	31	11-	보는	圣广	120	pН	1	Custody	Seals Y N
۸	~ N A				W	2. 1°	70	H	7				1	Dispo	•	Return	A	-				L'	]]		1	,		1	T ₁	ce	(YW
14	SAP	_	_		_	$\underline{\omega}$	11	-	<u>_</u>					42		<u> </u>	→ N	<u> </u>				PR	eservat	IVE	1	T		QC Level 1 2		ther	
		T)	pe		trix	-											R	j	إر			7	_ <del>-</del>		7	<b>&gt;</b>	10	QO LEVE! 1 2	<del></del>		
Sam	oling	200	Ŗ	Ă   Š	ĵ				ENT							LAB		<	7	વ	ICE	SO	S	الع	S	Soy	3	Cooler Temperatur	• ,	4	
Date	Time	P	B	W S A C T E R	-   "			(9	CHA	RA	CTI	ERS	)			QC		۱ ۲	$\exists$	10	14	H2504	4054	17	H2504	H2.	H	Alternate De	scripti	 OD	Lab ID
<b></b> _		_		+	+	+	L	Т.	$\overline{}$	Т	$\neg$	Т	-				+	├-	7		-	<u> </u>	<del> </del>	' '	<del>  _</del>			Antomato De		-	
8/17/19		ļ	M	1	-	14	G	1		+	$\perp$						11	~	$\leq$	<del></del>	-	ļ	<del> </del>		-				:		
18/17/29	11		M	レ	1	R	0	1	0 <		4	je.	211	<u>.</u> 1	4				_	<u></u>											2
8/17/99	ij		<b>~</b>	4		7	9	f	<b>,</b> [	1	13	[c]	277	٠			11	ļ													
8/17/99	1		J	1		R		) (	2.								1					~									3
8/17/99	11			オ	+-	R	0			Ť	+	_		_			1;				,			1							ラー
	11	-			+	R		1		+	-	$\dashv$	$\dashv$				1	<del> </del>	$\dashv$							<u> </u>		<del>-</del>			323
8/17/19			M	-	+-				=  -	╁	-							$\vdash$					<del> </del> -	<u></u>	<del>                                     </del>						17
8/17/99	<u> 4</u>	_	4		4	2	G	f	4	- -	$\perp$	4						<b> </b>	-4		ļ		ļ	ļ	سا	ļ					- I I
8/17/20	14		M			W	N	1	o #	2	8	4	lu	en	<u>+</u>			<u>.</u>	_							1					4
1/17/59	11	ļ	レ			M	W	1		2	8			en			1,	ļ									سا	1			14
1-7-1						"			T	1		<u> </u>										· · · ·									
		-	ff	$\top$	-	1-	T	t		T	T	1					-[-	f	1		l		f		<del></del>						
Relingui	shed By	L	<u>.                                    </u>	L			<u>ــــ</u>						$\dashv$	Dat	te/Ti	tne	Receiv	red B			l	Emp	ty Bottle	<u> </u>	<u> </u>	<u> </u>	Date/T	lme		.=	1
Roo	shed By	U	a	Ke a	il_									8/17	199	1:25	XX		1		. •		9					8/17/99	07:	25	
Sample:	By and 1	ltie							n and p					o De	te/T	me 1:30	Relina	juishe	rd By				- 1	algn and pri	•		Deter	Ime   17/99 7:3	a		
Receive	<u>ー `し</u>	_				_			n ænd p		_	-		Da	te/T	me	Reling				·			on l	(CV) N	. 0					
Rope	e Vil	Ua	Ma	rl_	٩	<u> </u>	ie.	Ň	[ii]	AF	R	A		8)1	199	7:39	lu	<u>où</u>		<i>i Ma</i>	red	·	Rosid	e Vil	ARR.	EA)	Date/T	117/99			
Receive	d By						(Pleas	e elg	n end j	orint n	eme)			Da	te/T	me	Shipp UPS		d-E	· 1	Other _		8	Shipping	#			• •	<del></del>		
Special	nstructio	n <b>a</b> :											_				078	- 11								<del></del>					

# CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

**CVO** 2300 NW Walnut Boulevard Corvalits, OR 97330-3638 (541) 752-4271 FAX (541) 752-0278

Project #	Purchase Order	,	Requested Analytical Method #						THIS AREA FOR LAB USE ONLY			
-			<b> </b>			T				Lab # 0 / 1		of T
Project Name	0		T 0 T		c					19964	12	3
McAllen Reus	2 Pilot Stu	24	Å		97			60		Lab PM	Custody Re	vlew
Company Name	MAInni	:			\ \\		}	32	}			
City Of M Project Manager or Contact & I	hone # Report Copy to:		o F		1 .	1		8-	į	Log In	LIMS Verifica	ation
Kathy McKinley	Kashy McI	Vinley	i 1	707	S	70	70	3		ļ		
	I NOTAL THE	Sample Disposal:	C O N T	1-	0 6		j	000	}	pH	Custody Sea	als Y
No NA	- 0 <del>11</del> -	Dispose Return	À			<u> </u>				4	ice	(Y
	WTP#2		N E	<del></del> -	<del></del>	<del></del>	servati	ve	<del>'</del> -	QC Level 1 2 3	Other	
Sampling C G W 8	<u> </u>		R	3	4C-1	H2504	204	_				
MATI	CLIENT SAMPLE ID (9 CHARACTERS)	LAB QC		H2504	조 포	455	五	HC HC	ļ	Cooler Temperature		
Date Time R				<u> </u>	工	·		エ		Alternate Descri	ption	Lab II
8/17/19/7:30 8/17/19/7:30 8/17/19/7:30 9/17/19/7:30 8/17/19/7:30	299		2	V						<u> </u>		
8/17/99 7:30 / 1	ROP		2		<b>/</b>							2
8/11/197:30	ROP		2						·			22
V17/19 1:30 ~ 3	WWP +2 Efflu	cent	2			/ /						4
8/17/99 7:30	ROC		2			·	~					3
8/17/19 7:30	29P		2					V				
						<u> </u>						
						<u> </u>						
Relinquished By ROQUE VILLAM	1d	9/17/19 7:25 X	lecelye	d By	<u> </u>	Emp	ty Battles	8	Date/1	"8)17/99 7:	25	
Sampled By and Title	(Please sign and print name)		tellnaul	Ished By	·		(Please si	ign and print name)	Date/1			
Received By	(Please sign and print name)	Date/Time R	telingul	Ished By	<del></del>		(Please si	m TICVINO	Date/1	ime .	)	
Received By	COSIE VIII NERENI (Please sign and print name)	1 18/17/99 7:39	Logo	<u>rie V</u>	<u>Mane</u>	al	Kosie	Villaresh	<u> </u>	8/17/99		
	(countries selles in an brank criticies)		JPS 	Fed-Ex	Other			inhhiiñ z				
Special Instructions:				·				:: - <del>-</del>				

# CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

**CVO** 2300 NW Walnut Boulevard Corvails, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

Project (								P	urch	220	Orde	r #			<del></del>	7			loguesto.	1 4	tion) Ma			77.110		C#	Supplies Up
Fiojecti	•							•	4101		<b>V.4</b> 0	•				ŀ			Requested				<del></del>		AKEA FU	H LAB USE	ONLY
Project i	Mame							l							┤ぇ		<u> </u>	ن ا		ر کے		1		Lab #	44	Page	3
Mc/ Compan	$n / l_{\Delta n}$	ľ	101	(	, p	1: 1	1	ς	In	1,					O T		, Ca, Fe, Mg, Mn, Sr, As, Cd, Cr, 1, Se, As, 2n	3	1 1 2	ں ج	西元	3 3 3		1.	0	<u></u>	\
Compan	y Name		<u> </u>	بر		1 /	۱,		y v (c	4					<b>⊣</b> Շ		50 5	2	्येदं र	راچين 2	<u>6</u>	15 TO 15		Lab PM		Custod	y Raview
1:1	u n	t.	m	. [	مالا	41									•	١	15 X 4		. 27	= 15,7		15 43 .	5			1	
C; 4 Project R	/anage	ror	Con	tact	& P	hon	e#	R	epo	rt Co	py to	:			ᅴ 알		हें ूं अ	3	3400	ن کی ا	, v	2000		Log in		LIMS Ve	rification
								L	1/1	<b>.</b>	na I		,				A1, Ba, Ca, Fe, K, Na, Sr, As, Pb, Hg, Se, A5	ا ا	Browde, Chlor de Fluoride, Sultate,	Aliba, Ca, Fe, Mg, Mn,	Pb, H5, Se,	Brimide, Chloride, Fluoride, Sulfale,					
Kath	4 1110	<b>占</b>	1/	10	1	ID		]F	ayı	41	TICK	JA	1ec	/ Disposal	ON N		25 2	3	100	202		Kal La	)	рН		Cuetod	y Seals Y N
		Juoi	n vac												T		<u>م</u> ہر <del>م</del> ے	Ā	8 12 6	Z C A	4 14	A 2017 9	2			·	y Seale Tyly
AS	AP				l	IW	177	0 H	2			"	lepose L	Return	I N				P	reserv				<b></b> _		Ice	
			/pe	Ma	atrix						<del>,</del>			1	E		~				_		1	QC Level	1 2 3	Other	
Samp	ling	COMP	G R A B	W A T	B A I						IPLE TERS			LAB	s		HND3		3 8		HN03	3		Cooler Ten	perature	4	· w
Date	Time	P		R	-			,			,	•					<b>Y</b>	İ	<del>                                   </del>	<b>W</b>	丰			Alte	nate Desc	ription	Lab ID
\$ 17/29	7:3a	Γ	u	7		Ta	0	1	्र		П	T	$\top$		1		\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \										2
8/17/99			V			R	1	Г				-			<u> </u>												2
		┢	T		+	15	7 7	- [			-			<del> </del>		-		-		WA		<del>                                     </del>					1
8/17/29		-	1			1	<u>ا</u>	f	+	+	$\  \cdot \ $	$\dashv$				Ц				Mu.	Y-		<u> </u>	·			.   .[
8/17/99	7:30		4	7	$\perp$	12	16	$\int f$	_	$\bot$					#1	Ц				_			ļ				<b>1</b>
				4	$\perp$	1_	_	_	-	-	_		_	_		_							ļ		····-		
]										$\perp$	$\square$																
										-						ŀ	i i										
								-																			
		1-	$\dagger \dagger$	$\dashv$		T	+	╁	1	-	-			<del> </del>	1	-				-							
		╁	$\square$	+		╁	-	+	<del></del>			$\dashv$		<del> </del>						-			-	<b>.</b>			
		-	1-1				-}-	-	$\dashv$		}_}	-					}							<b>]</b>			
Balla sula	h a d 914						Щ.					_	Pote		1800		ed By			pty Bot	4400		Deta 6	<u> </u>	·		
Relinquis	inea by	V.	ill	$\alpha$	uoa								Date/ 8/17/	1900 19			· — E	<u> </u>		ipty bot	1		Date	Ime, 8/17/99			
Sampled	By and 1	itte		<u></u>		_ 1			end p			7	Date	Time	Refi	nqı	ulshed By				se sign and p		Date/T	lme	/	20	
Received	<u>۔ ک</u> ۱ Bu	<u></u>	<u> </u>			_KØ		Ţ	rev	IN C	<u> </u>			11 7:30 Time			1 ulshed By	<u> </u>	• • •		se sign and p	Trevino	Date/T	8)17/99 Ima	07:	37	
Logi	e Vu	Ш	an	al	7 						0) L <i>e 1</i> 3			9 07:39	L	00	zie Vi	Ula	neal		e Vil	MRREAL	- Jaior I	8/17/99			
Received	Ву						(Pleas	ne elg	n and p	rint naer	<b>(a)</b>	$\Box$	Date	Time	Ship		od Via Fed-Ex	Oth	<b></b>		Shippin	g f					•
Special i	nstructio	ms:							<del>,</del>						J Vra	•	i og.ex	- Out				-			<u> </u>		

as\$ te Violo



Ms. Anne McKee-Robbins CH2M HILL/CVO 2300 N.W. Walnut Blvd. Corvallis, OR 97330

> Columbia Analytical Services Report City of McAllen D9901502/D1227

> > September 13, 1999

Submitted by:

Beyon Jones

Bryan Jones

Project Manager/Client Services

## **TABLE OF CONTENTS**

#### CAS Lab Reference No.: D1227 Level 1

	Page
	No.
Organic Data Qualifiers	i
Organic Sample ID Qualifiers	ii
Sample Identification Cross-Reference	iii
GC ORGANOCHLORINE PESTICIDES	1
Case narrative	
Sample results	
Chain of Custody Documentation	17

## **Organic Data Qualifiers**

- A-- This qualifier indicates that a TIC is a suspected aldol-condensation product
- **B--** This flag is used when the analyte is found in the associated blank as well as the sample. This notation indicates possible blank contamination and suggests that the data user evaluate these compounds and their amounts carefully.
- C-- The "C" flag indicates the presence of this compound has been confirmed by the GC/MS analysis.
- **D--** This qualifier is used for all the compounds identified in an analysis at a secondary dilution factor. "D" qualifiers are used only for the samples reported at more than one dilution factor.
- E-- This flag indicates that the value reported exceeds the linear calibration range for that compound. Therefore, the sample should be reanalyzed at the appropriate dilution. The "E" qualified amount is an estimated concentration, and the results of the dilution will be reported on a separate Form I.
- I— The qualifier indicates that the reporting limit to the "I" qualifier has been raised. It is used when the chromatographic interference prohibits detection of a compound at a level below the concentration expressed on the Form I.
- J- Indicates an estimated value. It is used when the data indicates the presence of a target compound below the reporting limit or the presence of a Tentatively Identified Compound (TIC).
- N-- This qualifier indicates presumptive evidence of a compound. This flag is only used for Tentatively Identified Compounds (TIC), where the identification is based on a mass spectral library research. It is applied to all TIC results. For generic characterization of a TIC, such as chlorinated hydrocarbon, the "N" qualifier is not used.
- P-- This qualifier is used for Pesticide/Aroclor target analytes when there is a greater than 25% difference for detected concentrations between the two columns. The lower of the two values is reported on Form I and flagged with a "P".
- U-- Indicates the compound was analyzed for but not detected. The number adjacent to the "U" qualifier indicates the reporting limit for that compound. The reporting limit can vary from sample to sample depending on dilution factors or percent moisture adjustments when indicated.

## **Organic Sample ID Qualifiers**

The qualifiers that may be appended to the Lab Sample ID and/or the Client Sample ID for organic analysis are defined below:

- **DL--** Diluted reanalysis. Indicates that the results were determined in an analysis of a secondary dilution of a sample or extract. A digit to indicate multiple dilutions of the sample or extract may follow the "DL" suffix. The results of more than one diluted reanalysis may be reported.
- **MS--** Matrix spike (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- **MSD-** Matrix spike duplicate (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- R-- Reanalysis. The extract was reanalyzed without re-extraction. The "R" is not used if the sample was also re-extracted. May be followed by a digit to indicate multiple reanalysis of the sample at the same dilution.
- **RE--** Re-extraction analysis. The sample was re-extracted and reanalyzed. May be followed by a digit to indicate multiple re-extracted analysis of the same sample at the same dilution.

GC ORGANOCHLORINE PESTICIDES

# CASE NARRATIVE GC ORGANOCHLORINE PESTICIDES

CAS	Lab	Reference	No./SDG.:	D1227

Project: City of McAllen

#### I. RECEIPT

No exceptions were encountered unless a Sample Receipt Exception Report is attached to the Chain-of-Custody included with this data package.

#### II. HOLDING TIMES

- A. Sample Preparation: All holding times were met.
- B. Sample Analysis: All holding times were met.

#### III. METHOD

Preparation: SW-846 3520C

Cleanup: NA

Analysis: SW-846 8081A

#### IV. PREPARATION

Sample volume may vary based on the amount of sample received per container.

#### V. ANALYSIS

- A. Calibration. In the ending CCV, toxaphene, exceeded 15%D however the average of all analytes was within therefore no corrective action was taken.
  - 1. Retention Time Windows: All analytes were within criteria.
  - 2. Degradation: All acceptance criteria were met.
- B. Blanks: All acceptance criteria were met.
- C. Surrogates: All acceptance criteria were met.
- D. Internal Standards: All acceptance criteria were met.
- E. Spikes: All acceptance criteria were met.
- F. Samples: Sample analysis proceeded normally.

I certify that this data package is in compliance with the terms and conditions agreed to by the client and Columbia Analytical Services, both technically and for completeness, except for the conditions noted above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or designated person, as verified by the following signature.

SIGNED: Jerry Watega 9/10/99 Reviewer: Athr Weller 9-10-99

Scientist, GC Organics

PWB10820

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227 Lab Sample ID: PWB10820

Matrix: WATER Level: LOW Lab File ID: B0904010

Sample Wt/Vol: 1.000 L Date Received:

Extract Vol: 10 ML Date Extracted: 08/20/99

Column: DB5 Date Analyzed: 09/04/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8	gamma-BHC (L Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.020 0.040 0.50	ם מ מ

PWB10820LCS

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227

SDG No.: D1227

Lab Sample ID:

PWB10820LCS

Matrix: WATER

Level: LOW

Lab File ID:

B0904008

Sample Wt/Vol: 1.000 L

Date Received:

10 ML

Date Extracted:

08/20/99

Column: DB5

Extract Vol:

Date Analyzed:

09/04/99

Extraction Type: Continuous

Dilution Factor: 1.0

CAS NO. CC	MPOUND	Units: ug/L	MDL	RL	RESULT	Q
58-89-9ga 72-20-8En 72-43-5Me 8001-35-2To	ndrin_ thoxychlor_	ndane)	0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.56 0.52 0.46 0.50	

PWB10820LCS

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227

Lab Sample ID:

PWB10820LCS

Matrix: WATER Level: LOW

Lab File ID:

B0904009

Sample Wt/Vol: 1.000 L

Date Received:

Extract Vol: 10 ML

Date Extracted: 08/20/99

Column: DB5

Date Analyzed: 09/04/99

Extraction Type: Continuous

Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8	gamma-BHC (L Endrin Methoxychlor Toxaphene	· <del></del>	0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.090 0.075 5.1	<b>U</b>

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

ZGPERMEATE

Case No.: D1227 SDG No.: D1227 Lab Sample ID: D1227001

Matrix: WATER Level: LOW Lab File ID: B0904011

Sample Wt/Vol: 1.000 L Date Received: 08/18/99

Extract Vol: 10 ML Date Extracted: 08/20/99

Column: DB5 Date Analyzed: 09/04/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8	gamma-BHC (L Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.024 0.020 0.040 0.50	U U

CLIENT ID.

ROPERMEATE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227 Lab Sample ID: D1227002

Matrix: WATER Level: LOW Lab File ID: B0904012

Sample Wt/Vol: 1.000 L Date Received: 08/18/99

Extract Vol: 10 ML Date Extracted: 08/20/99

Column: DB5 Date Analyzed: 09/04/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8	gamma-BHC (L Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.020 0.040 0.50	ם מ

### 2C WATER SEMIVOLATILE SURROGATE RECOVERY

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227

			S1	S2	S2	TOT
	LAB ID	CLIENT ID.	#	#	52	OUT
	==========	=======================================	=====	======	=====	===
01	PWB10820LCS	PWB10820LCS	107	86		
02	PWB10820LCS	PWB10820LCS	105	72		0
03	PWB10820	PWB10820	102	76		0
04	D1227001	ZGPERMEATE	105	74		
05	D1227002	ROPERMEATE	68	47		0
06 07						
07						
09						
10					<del></del>	
11						
12	<del></del>					
13						
14						
15						
16						
17						
18						
19 20						
21						
22	<del></del>					
23						
24						
25						
26						\
27						
28						
29						
30						

QC LIMITS

= Tetrachloro-m-xylene = Decachlorobiphenyl (45-125)(34-133)

# Column to be used to flag recovery values
* Values outside of contract required QC limits

D Surrogates diluted out

page 1 of 1

FORM II

SW846

### 3E WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227 Column: DB5

LCS - Sample No.: PWB10820

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
gamma-BHC (Lindane)	0.5000	0.0000	0.5583	112	73-125
Endrin	0.5000	0.0000	0.5193	104	43-134
Methoxychlor	0.5000	0.0000	0.4603	92	73-142

# Column to be used to flag recovery and RPD values with an asterisk

*	Values	outside	of O	C 1	imits
	varues	Outside	OT O		・エル・コ

RPD: 0 out of 0 outside limits

Spike Recovery: 0 out of 3 outside limits

COMMENTS:	

## 3E WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227 Column: DB5

LCS - Sample No.: PWB10820

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
Toxaphene	5.000	0.0000	5.095	102	41-126

# Column to be used to flag recovery and RPD values with an asterisk

*	Values	outside	of	OC	limits
	varues	Outside	$\circ$	$\sim$	エエニニー

RPD: 0 out of 0 outside limits

Spike Recovery: 0 out of 1 outside limits

COMMENTS:	_

SW846

# SEMIVOLATILE METHOD BLANK SUMMARY

Client ID.

PWB10820

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227

Lab File ID: B0904010

Lab Sample ID: PWB10820

Date Extracted: 08/20/99

Extraction Type:

CONT

Date Analyzed:

09/04/99

Time Analyzed:

2010

Matrix:

WATER

Level: (low/med)

LOW

Instrument ID:

GCB

THIS METHOD BLANK APPLIES TO THE FOLLOWING SAMPLES, MS and MSD:

	CLIENT ID.	LAB SAMPLE ID	LAB FILE ID	DATE ANALYZED
01 02 03 04 05 06 07 08 09 10 11 12 13 14 15 16 17 18 19 20 21	PWB10820LCS PWB10820LCS ZGPERMEATE ROPERMEATE	PWB10820LCS PWB10820LCS D1227001 D1227002	B0904008 B0904009 B0904011 B0904012	09/04/99 09/04/99 09/04/99 09/04/99
22 23				

# PESTICIDE CONTINUING CALIBRATION CHECK

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Instrument ID: GCB

Case No.: D1227 SDG No.: D1227

Lab File ID: B0904005 CCV Date/Time:

09/04/99

1605

GC Column: DB5

ICAL Date/Time (1st pt): 08/22/99

1725

ICAL Date/Time (Last pt): 08/22/99

2040

Units : ug/mL

COMPOUND	AVERAGE RF	RF	CURVE	%D	MAX %d	
Toxaphene (2) (3) (3)	0.044 0.047 0.050	0.038 0.039 0.048	AVG AVG AVG	-12.0 -17.6 -4.3		<-

# 7B PESTICIDE CONTINUING CALIBRATION CHECK

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Instrument ID: GCB Case No.: D1227 SDG No.: D1227

Lab File ID: B0904020 CCV Date/Time: 09/05/99 0417

GC Column: DB5 ICAL Date/Time (1st pt): 08/23/99 0959

ICAL Date/Time (Last pt): 08/23/99 1314

Units : ug/mL

	AVERAGE				MAX	
COMPOUND	RF	RF	CURVE	%D	%d	
alpha-BHC	2.751	3.182	AVG	1 5 7	15.0	
beta-BHC	- 0.871	0.968	AVG		15.0	<-
delta-BHC	2.640	2.951	AVG		15.0	
gamma-BHC (Lindane)	2.495	2.825	AVG		15.0	
Heptachlor	2.542	2.917	AVG	1	15.0	
Aldrin	2.351	2.658	AVG		15.0	
Heptachlor epoxide	2.134	2.365	AVG		15.0	
Endosulfan I	1.886	1.963	AVG		15.0	
Dieldrin	- 2.243	2.438	AVG		15.0	
4,4'-DDE	- 1.919	1.922	AVG		15.0	
Endrin	1.972	2.030	AVG		15.0	
Endosulfan II	1.832	1.892	AVG		15.0	
4,4'-DDD	1.503	1.543	AVG		15.0	
Endosulfan sulfate	1.801	1.684	AVG		15.0	
4,4'-DDT	- 1.717	1.732	AVG		15.0	
Methoxychlor	0.903	0.864	AVG		15.0	
Endrin ketone	1.951	1.960	AVG		15.0	
Endrin aldehyde	1.334	1.342	AVG		15.0	
alpha-Chlordane	2.115	2.222	AVG		15.0	
gamma-Chlordane	2.117	2.223	AVG		15.0	
=======================================	-		======		====	
Tetrachloro-m-xylene	1.075	1.249	AVG	16.2	20.0	
Decachlorobiphenyl	1.920	1.792	AVG	-6.6	20.0	

## PESTICIDE CONTINUING CALIBRATION CHECK

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Instrument ID: GCB

Case No.: D1227 SDG No.: D1227

0506

GC Column: DB5

ICAL Date/Time (1st pt): 08/22/99

1725

ICAL Date/Time (Last pt): 08/22/99

2040

Units : ug/mL

COMPOUND	AVERAGE RF	RF	CURVE	%D	MAX %d	
	=======	========	****	=====	====	
Toxaphene	0.044	0.039	AVG	-10.4		
(2)	0.047	0.036	AVG	-24.2		<-
(3)	0.050	0.043	AVG	-12.5	15.0	
						ĺ

FORM VII

## $\mathbb{C}\mathbb{S}$ PESTICIDE ANALYTICAL SEQUENCE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227

Instrument ID: GCB

CLIENT SAMPLE NO.	LAB SAMPLE ID	DATE ANALYZED	TIME ANALYZED
	SAMPLE NO. PSTD#3 PEST PSTD#3 TOX PWB10820LCS PWB10820LCS PWB10820 ZGPERMEATE ROPERMEATE PSTD#3 PEST	SAMPLE NO. SAMPLE ID  PSTD#3 PEST PSTD#3 PEST PSTD#3 TOX PSTD#3 TOX PWB10820LCS PWB10820LCS PWB10820 PWB10820 ZGPERMEATE D1227001 ROPERMEATE D1227002 PSTD#3 PEST PSTD#3 PEST	SAMPLE NO. SAMPLE ID ANALYZED  PSTD#3 PEST PSTD#3 PEST 09/04/99 PSTD#3 TOX PSTD#3 TOX 09/04/99 PWB10820LCS PWB10820LCS 09/04/99 PWB10820 PWB10820 09/04/99 PWB10820 PWB10820 09/04/99 ZGPERMEATE D1227001 09/04/99 ROPERMEATE D1227002 09/04/99 PSTD#3 PEST PSTD#3 PEST 09/05/99

**CHAIN OF CUSTODY DOCUMENTATION** 

CH2MHILL Analytical Services
CHAIN OF CUSTODY RECORD
AND AGREEMENT TO PERFORM SERVICES

LMG 2567 Fairlane Drive Montgomery, AL 36116-1622 (334) 271-1444 FAX (334) 271-3428

☐ LRD 5090 Caterpillar Road Redding, CA 96003-1412 (916) 244-5227 FAX (916) 244-4109

FILKW Canviro Analytical Laboratories, Inc. 50 Bathurst, Unit 12, Waterloo, Ontario, Canada N2V 2C5 (519) 747-2575 FAX (519) 747-3806

Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

coc#9801827

Project #	Purchase Order #			Requested Analytical Me	thod #	THIS AREA FOR	LAB USE ONLY	
			lane, Taxopher une, Toxaphene			Lab#	Page o	of
Project Name		0	dane, Texaphe ane, Texaphen			D1227		
MiAllon Relise Pilot	Study	T A	Lindane, hlor, Taxagane, indane,			Lab PM	Custody Rev	/lew
		L	10 050 1				screened	
City of McAllen	1	*	hisk holy				BY 8/18/	199
Project Manager or Contact & Phone #	Report Copy to:	O F	272			L99 18W 1 19	LIMS Verifica	tion
Kathy Mckinley	Kathy McRiniey	/ c	10 X 6 X			Just 8/11.		
City of McAllen Project Manager or Contact & Phone #  Rathy McKinley  541 /758-0235#3144		O N	Endrin, Lin Methoxychlor Endrin, Lina Methoxychlor			pH	6	
Requested Completion Date: Site ID	OF M. Alless Sample DI	sposar.	2525			<b> </b>	Custody Sea	
ASAP NUTA		Return N		Preservative	<del></del>		Ice	YN
Type Matrix		E R				QC Level 1 2 3	Other	
Sampling C G W S A O I M A T I I R P B E L R	CLIENT CAMPLE ID	S				Cooler Temperature	2 <b>ċ</b>	
M A T I R	CLIENT SAMPLE ID (9 CHARACTERS)	LAB QC			1 1	Cooler remperature	2	
						Alternate Descrip	otion	Lab ID
8/17/1907:30 1 26	Permeate Permeate	2						1
8/17/19 07:30 V RD	P) cme ote	2						2
			V					
					<del></del>			
			1 1					
								·
<u> </u>	<del></del>		- <b> </b>  -	<del></del>				
l	<u> </u>				·		·	
Relinquished By . , Empt	y Bottles Date/Ti	me Receiv	ved By	Empty Bottles	Date/1	Time		
Relinquished By Empt	4 07:25	8/17/54 X P	<u>- ~ ~ </u>	4		8/17/99 07:2	5	
Sampled By and Title (Pleas	e sign and print name) Date/Til N Trovino 0730 \$		quished By	(Please sign and pri		8/17/99 07:39	9	
Received By (Pleas	e sion and print name) Date/Ti	me Relina	guished By	(Please sign and pri	int name) Date/T	ime .		
Kopin Vellaneck Posis	e VillARRES DI 07:39 B	117/29 ROD	rie Villar		P.P.FA	8/17/99		·
Received By (Pleas	e sign and print name) Date/Til		ed Via (Fed-Ex) Oti	Shipping	<b>;</b> #	1.00		
Social Instructions:	8/18/97	1000 073	(Ted-LX) OII	8	129007252	.67		
1								

ENERGY
LABORATORIES

BillingsCasperGilletteRapid City

ENERGY LABORATORIES, INC.'S CHAIN OF CUSTODY RECORD Mail Only:

PO Box 3258 • Casper, WY

82602-3258

voice

toll free 1-888-235-0515 307-235-0515

UPS/FedEx Deliveries:

2393 Salt Creek Highway •

Casper, WY •

82601

307-234-1639 fax

For Sa	For Sample Tracking Purposes, Please Provide Contact Name and Telephone #'s as Indicated (SEE BACK OF FORM FOR EXAMPLES AND INSTRUCTIONS)										
Project	Name /	Loc	ation	/ Purchase Order # / Bid #	1						Special Requests
MeAlle	nuallen Reuse Pilot / McAllen, / NO. P.O.#				C Other		Type o	f Analys	ses Req	uested	Stud TAT
<u></u>	tud y			' IX. /	Line C. C.	رقم	<del></del>				 
Name	/ Phone	# /	Fax	x# /	zin v	22	228,	ł			
Kathy CH2M	McKinl Hill	24		41-758-0235#3144/541-766-2852	Cont (W) S Segeration	adium	2 43				
Date	Time	composite	sample	Send Invoice to: Kathy McKinky CH2M Hill Applied Sciences Group  Ciall Dabove phore number  Send Report to:  Same as above	Number of containers Sample Type: A (W) S V U O Air Water Soils/Solids Vegetation Urine Other	4 5	226, Radium. Alpha				
		сош	grab	Send Report to:  Same as above  Sample I.D.	I Sa Air <u>W</u> aren	Radium Gross A					Comments, Special Instructions, etc.
8/17/99	07:30		/	ZenoGem Permeate	1	Х					
1 1	07:30		/	RO Permeate			X				
				ARS AT							
									-		

1	1. Sampler: (signature)	Date	Time	Received by: (signature)	2. Relinquished by: (signature)	Date	Time	Received by: (signature)
l	R-2.	8/17/99	07:30	Rosie Villaneal	Resie Villaned	8/17/99		
	3. Relinquished by: (signature)	Date	Time	Received by: (signature)	4. Relinquished by: (signature)	Date	Time	Received at Laboratory by:
						8-18-94	10:15	Krisponit

Project	Name / Thunde	Loi erbas	in	ENERGY LABORATORIES, INC.  Mail Only: PO Box 3258 •  UPS/FedEx Deliveries: 2393 Salt Creek  Turposes, Please Provide Contact Name and Telephone #  / Purchase Order #  Town of Hope No PO #	Casper, W k Highway	Y Ca	826 Isper, W EE BAC	02-3258 /Y •	826 ORM FO	OR EXA	MPLES	voice 307-235-0515 fax 307-234-1639  SAND INSTRUCTIONS)  Special Requests  Please fax results
Name / Phone # / Fax #  Jeff Jones @ (307) 555-1515, (307) 555-5555 fax   Send Invoice to: Jeff Jones PO Box Nowhere Hope, WY 80000  Send Report to: Bob Brown PO Box Somewhere USA, WY 81111		Number of containers Sample Pype: A W S V U O Air <u>W</u> ater Foils/solids <u>Vege</u> tation <u>U</u> rine <u>O</u> ther	Asbestos - TEM	IOC's - RADs	NO ₂ , NO ₃ , F	VOCs - 502.2	50cs - 504, 505, 508	50cs - 515,531.1	results as soon as possible Thank you.  Comments, Special Instructions, etc.			
1005	<u> </u>	↓_	ļ	Sample 1.D.				ļ		<u> </u>	ļ	
1995	1	<del> </del>					<u> </u>		<u> </u>	<u> </u>	<u> </u>	
5/28	11:35	<u> </u>	X	Entry to Distribution	4	X	<u> </u>	<u> </u>	X		<u> </u>	Phase II SDWA Primary
5/28	11:45		X	Distribution Tap	9		Х	X		X	X	4
5/28	11:45		X	Distribution Tap	9		X	X		X		X

1.Sampler: (signature) <b>Jeff Jones</b>	Date 5-28-95	Time <b>12:05</b> p	Received by: (signature) Harry Truckers	2.Relinquished by: (signature) Harry Truckers	Date 5-28-95	Time 13:15p	Received by: (signature) Sheryl A. Garling
3. Relinquished by: (signature)	Date N/A	Time N/A	Received by: (signature)	4. Relinquished by: (signature) Sheryl A. Garling	Date 5-28-95	Time 14:00p	Received at Laboratory by: Roger A. Garling

#### Instructions:

- (1) A completed Chain-of-Custody must be submitted with all samples
- (2) Special Requests area can include (but not limited to) the following:
  - Turnaround status, Rush status, Due Date, etc.
  - Special mailing instructions:
    - send copy of Report and/or Invoice to a second party
    - send copy of Report to a Government Agencies (EPA, etc.)
- Public Water System (PWS) Number
- Do you want samples returned to you or disposed of?

### Scope of Work/Instructions

## CH2M HILL Point of Contact for Final report/Invoicing

CH2M HILL Kathy McKinley 2300 NW Walnut Blvd. Corvallis, OR 97330

Phone: 541/758-0235 ext. 3144

FAX: 541/766-2852

### **Analytical Methods/Prices:**

Radium 226 by EPA 903.0 for \$40 per sample Radium 228 by EPA 904.0 for \$50 per sample Gross Alpha by EPA 903.0 for \$35 per sample

Sample Delivery: \$25

Return Cooler/Samples: \$6.40

The laboratory shall clearly and completely document and justify the preparation and analysis procedures when modifications to the methods have been made/requested.

**Holding Times:** Samples must be analyzed within EPA holding for each analytical method specified. CH2M HILL will deliver samples to the laboratory in a timely manner to facilitate the meeting of holding times.

**Quality Assurance/Quality Control Requirements:** QA/QC procedures will follow the protocols set forth in the EPA methods.

**Data Package**: A final data package must be submitted to CH2M HILL. The package will include: a lab narrative and data summary.

The laboratory narrative will include:

A description of any deviation from the prescribed methodologies or protocols as discussed in this SOW.

Summarization of quality control information exceeding the laboratory's acceptance criteria, a discussion of possible reasons for these discrepancies, and a description of corrective action taken.

All blank values exceeding three times the average method blank will be addressed.

A synopsis of all holding times achieved.

A discussion of any other analytical problems that may have been encountered.



Turnaround Time: Standard (3 weeks)

## CLIENT SAMPLE CROSS-REFERENCE

## CH2M HILL Applied Sciences Group Reference No. 3089

		Date	Time
Sample ID	Client Sample ID	Collected	Collected
308901	ZGP	09/14/1999	08:50
308902	ROP	09/14/1999	08:50
308903	WWTP#2Effluent	09/14/1999	08:50
308904	ROC	09/14/1999	08:50

## CASE NARRATIVE **VOLATILES**

Lab Reference No.: 3089

Client/Project: McAllen WWTP #2, City of

I. Holding Times:

All acceptance criteria were met.

II. Analysis:

> Calibration: A.

> > All acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

D. Spike Sample(s):

All acceptance criteria were met.

Surrogate Recoveries: E.

All acceptance criteria were met.

F. Lab Control Sample(s):

All acceptance criteria were met.

G. Other:

None

Ш. **Documentation Exceptions:** 

None

IV. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or designee, as verified by the following signature.

Prepared by:

Reviewed by:

A Hande

### CASE NARRATIVE GENERAL CHEMISTRY

Lab Reference No.: 3089

Client/Project: McAllen WWTP #2, City of

I. <u>Holding Time</u>:

All acceptance criteria were met.

II. <u>Digestion Exceptions</u>:

None

- III. Analysis:
  - A. Calibration:

All acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>Matrix Spike Sample(s)</u>:

All acceptance criteria were met.

D. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

E. <u>Lab Control Sample(s)</u>:

All acceptance criteria were met.

F. Other:

Not applicable.

IV. <u>Documentation Exceptions</u>:

None.

V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by:

Reviewed by:

### CASE NARRATIVE METALS

Lab Reference No.: 3089

Client/Project:	McAllen	<b>WWTP</b>	#2,	City of
-----------------	---------	-------------	-----	---------

I. Holding Time:

All acceptance criteria were met.

II. <u>Digestion Exceptions</u>:

None.

- III. Analysis:
  - A. <u>Calibration</u>:

All acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>ICP Interference Check Sample</u>:

All acceptance criteria were met.

D. <u>Spike Sample(s)</u>:

All acceptance criteria were met.

E. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

F. <u>Laboratory Control Sample(s)</u>:

All acceptance criteria were met.

G. ICP Serial Dilution:

Not Required.

H. Other:

None

IV. <u>Documentation Exceptions</u>:

None

V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by:	Aud Labor	
Reviewed by:	-(VWW)	



CH2M HILL

Applied Sciences Group

2300 NW Walnut Blvd

Corvallis, OR

97330-3538

P.O. Box 428

Corvallis, OR

97339-0428

Fax 541.752.0276

Tel 541.752.4271

October 26, 1999

McAllen WWTP #2, City of

149462.A1.ZG

RE: Analytical Data for McAllen WWTP #2, City of

Applied Sciences Group Reference No. 3089

Angie Fernandez/PHX:

On September 15, 1999, CH2M HII request for analysis of selected para

The analytical results and associate difficulties encountered during the narrative.

Under CH2M HILL policy, your shave not given us prior instruction disposal as hazardous waste.

CH2M HILL Applied Sciences ( serving your analytical needs agaif you need additional information extension 3120.

Sincerely,

Kelly Ensor

Senior Administrative Assistant

**Enclosures** 

Group received four samples with a tached.

ısual : case

ting. If you nples require

rward to ning the data, or 758-0235,



CH2M HILL

**Applied Sciences Group** 

2300 NW Walnut Blvd

Corvallis, OR

97330-3538

P.O. Box 428

Corvallis OR

97339-0428

Tel 541.752.4271

Fax 541.752.0276

October 4, 1999

McAllen WWTP #2, City of

149462.A1.ZG

RE:

Analytical Data for McAllen WWTP #2, City of

Applied Sciences Group Reference No. 3089 & 3113

Angie Fernandez/PHX:

On September 15, 1999, CH2M HILL Applied Sciences Group received four samples with a request for analysis of selected parameters. From two of these samples, CH2M HILL Applied Sciences Group generated two samples with a request for analysis of selected parameters.

The analytical results and associated quality control data are enclosed. Any unusual difficulties encountered during the analysis of your samples are discussed in the case narrative.

Under CH2M HILL policy, your samples will be stored for 30 days after reporting. If you have not given us prior instructions for disposal, we will contact you if any samples require disposal as hazardous waste.

CH2M HILL Applied Sciences Group appreciates your business and looks forward to serving your analytical needs again. If you should have any questions concerning the data, or if you need additional information, please call Ms. Kathy McKinley at (541) 758-0235, extension 3120.

Sincerely,

Kelly Ensor

Senior Administrative Assistant

Melenaux

**Enclosures** 

## CLIENT SAMPLE CROSS-REFERENCE

## CH2M HILL Applied Sciences Group Reference No. 3089 & 3113

		Date	Time
Sample ID	Client Sample ID	Collected	Collected
308901	ZGP	9/14/99	8:50
308902	ROP	9/14/99	8:50
308903	WWTP#2Effluent	9/14/99	8:50
308904	ROC	9/14/99	8:50
311301	ZGP-3D	9/20/99	
311302	ROP-3D	9/20/99	

# CASE NARRATIVE DBPs/ORGANICS

Lab Reference No.: 3089 & 3113

Client/	Project	: McAllen WWTP #2, City of				
I.	Holding Times: All acceptance criteria were met.					
II.	Analys	<u>iis</u> :				
	A.	Calibration: All acceptance criteria were met.				
	B.	Blanks: All acceptance criteria were met.				
	C.	<u>Duplicate Sample(s)</u> : All acceptance criteria were met.				
	D.	Spike Sample(s): All acceptance criteria were met.				
	E.	Surrogate Recoveries: All acceptance criteria were met.				
	F.	Lab Control Sample(s): All acceptance criteria were met.				
	G.	Other: None				
III.	Docum None	nentation Exceptions:				
clie abo	nt and Cove. Rel	at this data package is in compliance with the terms and conditions agreed to by the CH2M HILL, both technically and for completeness, except for the conditions detailed ease of the data contained in this hardcopy data package has been authorized by the Manager or designee, as verified by the following signature.				
Prepare	d by: _					
Review	ed by: _	_ <del></del>				

Formation Potential Test Conditions											
		FP	Free	Free	Total	FP	Measured	FP	FP	FP	FP
Client ID	Lab ID	Dose	Residual	Demand	Residual	Temp.	рH	Start	Take-Off	Time H:M	Time (Hour)
ZGP	308901	10.00	0.21	9.79		23	7.9	9/17/99 12:05	9/20/99 13:17	73:12	73.20
ROP	308902	1.60	0.71	0.89		23	7.7	9/17/99 12:12	9/20/99 13:21	73:09	73.15

Formation Potential Trihalomethanes (THMs) Disinfection By-Products, (ug/L)											
Client ID	Lab ID	FP CHCl3	FP BDCM	FP DBCM	FP CHBr3	FP TTHM					
ZGP-3D	311301	105	77.6	51.5	9.5	244					
ROP-3D	311302	2.9	2.9	2.5	<1	8.3				· · · · · ·	
	CHCl3 = Chloroform			-	EPA TTHM Stage 1 MCL = 80 ug/L						
		BDCM = Brom	odichlorometha	ne		EPA TTHM Stage 2 MCL = 40 ug/L					
	DBCM = Dibromochloromethane										
		CHBr3 = Brom	noform		Ι						

Formation Potential Haloacetic Acids (HAAs) Disinfection By-Products (ug/L)											
		FP	FP	FP	FP	FP	FP	FP	FP		
Client ID	Lab ID	MCAA *	MBAA *	DCAA *	TCAA *	BCAA	DBAA *	HAA5	HAA6		
ZGP-3D	311301	7.5	3.2	39.8	31.3	22.8	8.8	90.6	113		
ROP-3D	311302	<2	<1	1.1	<1	<1	<1	1.1	1.1	1	
		MCAA = Monochloroacetic acid			BCAA = Bromochloroacetic acid			EPA HAA5 Stage 1	MCL = 60 ug/L	-	ļ
		MBAA = Mono	bromoacetic aci	d	DBAA = Dibromoacetic acid EPA			EPA HAA5 Stage 2	MCL = 30  ug/L		
		DCAA = Dichle	oroacetic acid		* These compou	inds make up th	e HAA5			İ	
	1	TCAA = Trichl	oroacetic acid		1		1				1

212 Set LOC +WNTPEHIL

Client Information

Client Sample ID: ROC

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Sampled By: R. Villareal Sampling Date: 09/14/1999 Sampling Time: 8:50

> Type: Grab Matrix: Water Basis: As Received

Lab Information

Lab Sample ID: 308904

Date Received: 09/15/1999

Report Revision No.: 0

Analyzed By: MG/MAS/DHK

Reviewed By: -----

		Sample			Analysis	Date
Analyte	MRL Resul		Qualifier Un		Method	Analyzed
General Chemistry						
N-Nitrate/Nitrite	0.20	24.4		mg/L	EPA 353.2	09/20/99
N-Total Kjeldahl	2.0	3.6		mg/L	EPA 351.4	09/21/99
Total Dissolved Solids	10	4,330		mg/L	EPA 160.1	09/20/99
TOC	5.0	22.6		mg/L	EPA 415.1/2	09/21/99
Total Phosphate-P	1.0	10.5		mg/L	EPA 365.2/4	09/21/99

Client Information

Lab Information

Client Sample ID: WWTP#2Effluent

Lab Sample ID: 308903

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Date Received: 09/15/1999

Sampled By: R. Villareal

Report Revision No.: 0

Sampling Date: 09/14/1999

Analyzed By: MG/MAS/DHK Reviewed By: ------

Sampling Time: 8:50 Type: Grab

Matrix: Water

Basis: As Received

		Sample			Analysis	Date	
Analyte	MRL Result		Qualifier	Units	Method	Analyzed	
General Chemistry							
N-Nitrate/Nitrite	0.04	3.94		mg/L	EPA 353.2	09/20/99	
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	09/21/99	
Total Dissolved Solids	10	1,060		mg/L	EPA 160.1	09/20/99	
TOC	0.50	6.10		mg/L	EPA 415,1/2	09/20/99	
Total Phosphate-P	0.10	1.78		mg/L	EPA 365.2/4	09/21/99	

Client Information

Client Sample ID: ZGP

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Sampled By: R. Villareal Sampling Date: 09/14/99 Sampling Time: 08:50 Type: Grab

Matrix: Water Basis: As Received **Lab Information** 

Lab Sample ID: 308901

Date Received: 09/15/1999

Report Revision No.: 0
Reported By: JG
Reviewed By:

Analyte	MRL	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
Analyte	WIFLE	nesuit	Qualifier	Units	Metriod	Allalyzeu
Aluminum, Al	100	100	U	μg/L	SW6010B	10/14/99
Arsenic, As	10.0	10.0	U	μg/L	SW6010B	10/14/99
Barium, Ba	25.0	61.6		μg/L	SW6010B	10/14/99
Cadmium, Cd	5.0	5.0	U	μg/L	SW6010B	10/14/99
Calcium, Ca	500	<b># 86900</b> /		μg/L	SW6010B	10/14/99
Chromium, Cr	10.0	10.0	U	μg/L	SW6010B	10/14/99
Iron, Fe	100	#100 § f	U	μg/L	SW6010B	10/14/99
Lead, Pb	3.0	3.0	U	μg/L	SW6010B	10/14/99
Magnesium, Mg	500	<b>\$25600</b> /		μg/L	SW6010B	10/14/99
Manganese, Mn	10.0	17.0		μg/L	SW6010B	10/14/99
Mercury, Hg	0.3	0.3	U	μg/L	SW7470A	09/28/99
Potassium, K	2000	29900		μg/L	SW6010B	10/14/99
Selenium, Se	7.0	7.0	U	μg/L	SW6010B	10/14/99
Silver, Ag	10.0	10.0	U	μg/L	SW6010B	10/14/99
Sodium, Na	1000	<b>253000</b> 🕯		μg/L	SW6010B	10/14/99
Strontium, Sr	100	2000		μg/L	SW6010B	10/14/99
Zinc, Zn	20.0	54.4		μg/L	SW6010B	10/14/99

That Set IPR

Analyzed By: MG/MAS/JJB/DHK

Lab Information

**Client Information** 

Client Sample ID: ZGP

Lab Sample ID: 308901

Project Name: McAllen WWTP #2, City of Date Received: 09/15/1999 Project Manager: Angie Fernandez/PHX Report Revision No.: 0

Sampled By: R. Villareal Sampling Date: 09/14/1999 Sampling Time: 8:50

Reviewed By: m 32 34 Type: Grab Matrix: Water Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units_	Method	Analyzed
General Chemistry						
Alkalinity (as CaCO3)	2.0	153		mg/L	EPA 310.2	09/24/99
Bromide	0.020	0.322		mg/L	EPA 300.0-B	09/20/99
Chloride	2.0	281		mg/L	EPA 300.0-A	09/22/99
Color (APHA) Apparent		17		color units	EPA 110.2	09/15/99
Fluoride	0.10	1.14		mg/L	EPA 300.0-A	09/22/99
N-Ammonia	0.10	0.10	U	mg/L	EPA 350.3	09/23/99
N-Nitrate/Nitrite	0.04	7.90		mg/L	EPA 353.2	09/20/99
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	09/21/99
Silica-React.	0.4	16.1		mg/L	SM4500-Si D	09/23/99
Sulfate	2.0	247		mg/L	EPA 300.0-A	09/22/99
Total Dissolved Solids	10	1,950		mg/L	EPA 160.1	09/20/99
TOC	0.50	5.90		mg/L	EPA 415.1/2	09/20/99
Total Phosphate-P	0.10	2.89		mg/L	EPA 365.2/4	09/21/99
UV-254	0.009	0.126		asb/cm	SM5910	09/15/99

### Client Information

Lab Information

Client Sample ID: ZGP

Lab Sample ID: 308901

Project Name: McAllen WWTP #2, City of

Analysis Method: SW 8260B

Project Manager: Angle Fernandez/PHX

Units: µg/L aceived: 9/15/99

Sampled By: R. Villareal Date Collected: 9/14/99 Time Collected: 8:50

Date Received: 9/15/99
Date Analyzed: 9/27/99
Dilution Factor: 1

Type: Grab Matrix: Water Report Revision No.: 0
Reported By: MCB

Basis: As Received

Reviewed By:

		Reporting	Sample	
Analyte	CAS#	Limit	Resuit	Qualifier
Purgeable Volatiles				
Vinyl Chloride	75-01-4	1.0	1.0	U
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	U
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	U
1,1,1-Trichloroethane	71-55-6	1.0	1.0	U
Carbon Tetrachloride	56-23-5	1.0	1.0	U
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	1.0	U
Dibromofluoromethane	1868-53-7		103%	SS
1,2-Dichloroethane-d4	17068-07-0		94%	SS
Toluene-d8	2037-26-5		115%	SS
p-Bromofluorobenzene	460-00-4		95%	SS

E=Estimated value above instrument calibration range

SS=Surrogate standard

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

Client Information

Lab Information

Client Sample ID: ROP

Lab Sample ID: 308902

Project Name: McAllen WWTP #2, City of

Date Received: 09/15/1999

Project Manager: Angle Fernandez/PHX

Sampled By: R. Villareal

Report Revision No.: 0

Sampling Date: 09/14/1999

Analyzed By: MG/MAS/JJB/DHK

Sampling Time: 8:50

SM4500-Si D

EPA 300.0-A

EPA 160.1

EPA 415.1/2

EPA 365.2/4

09/23/99

09/22/99

09/20/99

09/20/99

09/21/99

Type: Grab

Matrix: Water

Basis: As Received

0.4

0.10

10

0.50

0.10

0.9

5.31

72

0.52

0.10

Sample **Analysis** Date MRL Result Qualifier Units Method Analyzed **Analyte** General Chemistry Alkalinity (as CaCO3) 2.0 16 mg/L EPA 310.2 09/24/99 Bromide U mg/L 0.020 0.020 EPA 300.0-B 09/20/99 Chloride 0.10 15.2 mg/L EPA 300.0-A 09/22/99 Color (APHA) Apparent ---5 color units EPA 110.2 09/15/99 Fluoride 0.45 mg/L EPA 300.0-A 09/22/99 0.10 U mq/L EPA 350.3 09/23/99 N-Ammonia 0.10 0.10 N-Nitrate/Nitrite 0.01 mg/L EPA 353.2 09/20/99 1.08 U N-Total Kjeldahl 2.0 2.0 mg/L EPA 351.4 09/21/99

U

mg/L

mg/L

mg/L

mg/L

mg/L

U=Not detected at specified reporting limits

Silica-React.

**Total Dissolved Solids** 

Total Phosphate-P

Sulfate

TOC

**Client Information** 

Client Sample ID: ROP

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Sampled By: R. Villareal Sampling Date: 09/14/99 Sampling Time: 08:50 Type: Grab

Matrix: Water Basis: As Received

## Lab Information

Lab Sample ID: 308902

Date Received: 09/15/1999

Report Revision No.: 0 Reported By: JG

Reviewed By: 34

Analyte	MRL	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
Aluminum, Al	100	100	U	μg/L	SW6010B	10/14/99
Arsenic, As	10.0	10.0	U	μg/L	SW6010B	10/14/99
Barium, Ba	25.0	25.0	U	μg/L	SW6010B	10/14/99
Cadmium, Cd	5.0	5.0	U	μg/L	SW6010B	10/14/99
Calcium, Ca	500	833		μg/L	SW6010B	10/14/99
Chromium, Cr	10.0	10.0	υ	μg/L	SW6010B	10/14/99
Iron, Fe	100	<b>2</b> 100	U	μg/L	SW6010B	10/14/99
Lead, Pb	3.0	3.0	U	μg/L	SW6010B	10/14/99
Magnesium, Mg	500	<b>₹500</b> 📝	U	μg/L	SW6010B	10/14/99
Manganese, Mn	10.0	10.0	U	μg/L	SW6010B	10/14/99
Mercury, Hg	0.3	0.3	U	μg/L	SW7470A	09/28/99
Potassium, K	2000	2000	U	μg/L	SW6010B	10/14/99
Selenium, Se	7.0	7.0	U	μg/L	SW6010B	10/14/99
Silver, Ag	10.0	10.0	U	μg/L	SW6010B	10/14/99
Sodium, Na	1000	₹16200 ¹		μg/L	SW6010B	10/14/99
Strontium, Sr	100	<b>37100</b> 7	U	μg/L	SW6010B	10/14/99
Zinc, Zn	20.0	20.0	U	μg/L	SW6010B	10/14/99

### Client Information

Client Sample ID: ROP

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Sampled By: R. Villareal Date Collected: 9/14/99 Time Collected: 8:50 Type: Grab

> Matrix: Water Basis: As Received

## Lab Information

Lab Sample ID: 308902

Analysis Method: SW 8260B

Units: µg/L

Date Received: 9/15/99 Date Analyzed: 9/27/99

Dilution Factor: 1
Report Revision No.: 0
Reported By: MCB

Reviewed By:

And	010#	Reporting	Sample	0 1:0
Analyte	CAS#	Limit	Result	Qualifier
Purgeable Volatiles				
Vinyl Chloride	75-01-4	1.0	1.0	U
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	U
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	U
1,1,1-Trichloroethane	71-55-6	1.0	1.0	U
Carbon Tetrachloride	56-23-5	1.0	1.0	U
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	0.6	J
Dibromofluoromethane	1868-53-7		110%	SS
1,2-Dichloroethane-d4	17068-07-0		102%	SS
Toluene-d8	2037-26-5		115%	SS
p-Bromofluorobenzene	460-00-4		104%	SS

E=Estimated value above instrument calibration range

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

SS=Surrogate standard

#### CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Walnut Boulevard Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

COC # Purchase Order # Project # Requested Analytical Method # THIS AREA FOR LAB USE ONLY Project Name McAllen Reuse Pilot Study
Company Name
City Of McAllen
Project Manager or Contact & Phone # Report Cop Lab PM **Custody Review** O F Log In LIMS Verification CONTAIN pН Custody Seals Y )N NWTP#2 ASAP Preservative QC Level 1 2 3 Other H2504 C Q W S A O I M A T I R P B E L H2504 So Sampling **CLIENT SAMPLE ID** LAB **Cooler Temperature** (9 CHARACTERS) QC Time Date **Alternate Description** Lab ID GP 0 14/99 08:50 114/49 08:50 0 114/99 08:50 0 4 **Empty Bottles** Received By Date/Time Ropie Villanca 4/14/9 08:32 9/14/99 08:30 Date/Time Relinquished By (Please sign and print name) Date/Time Sampled By and Title (Please sign and print name) 08:55 Javier Hingiosa 1114199 08:50 Date/Time Date/Time 9/14/99 Relinquished By Received By n/1444 08:55 Rusie VILLARREA Proie Villant Rosie VillanasHI Shipped Via Shipping # Received By (Please sign and print name) Other Special instructions:

# CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Wainut Boulevard Corvailis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

COC # Purchase Order # Project # Requested Analytical Method # THIS AREA FOR LAB USE ONLY Page, Project Name McAllen Re USE PILOT Study 60 Lab PM **Custody Review** 260 N  $\boldsymbol{\omega}$ City of meallen

Project Manager or Contact & Phone # Report Copy to:  $\dot{\omega}$ Log In LIMS Verification TOC Kathy McKinley Kathy McKinley

Requested Completion Date: Stie ID Sample Disposal: Custody Seals Y ĀIN W.W.TP.#Z ASAP Preservative E QC Level 1 2 3 Other Type Matrix Hzsoy H2504 4252H H2504 C G W S A O I R B E L Sampling **CLIENT SAMPLE ID** LAB **Cooler Temperature** #C1 FC. OC (9 CHARACTERS) Time **Alternate Description** Lab ID Date લ 9/14/99/08:50 RO 3 9/14/99 08:50 RO 2 4/14/99 08:50 NWT P#ZECF Went 4/14/99 08:50 ٥ 2 hy 199 08:50 2 9/14/9908:50 Religquished By Lillangel Received By **Empty Bottles** Date/Time Date/Time 9/14/19 08:30 1/14/19 ON:30 X Jani Duni Relinguished By Sampled By and Title Date/Time (Piesse sign and print name) (Please sign and print name) Date/Time 1/14/69 08:50 Savier Hindissa larier Hinoissa Pate/Time Relinquished By Louis Vallaned Date/Time Received By (Please sign and print name) Rosie VIII ARREAL Rosie VILLARKEH Shipping # (Please sign and print name) Shipped Via Other -Fed-Ex

### CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Walnut Boulevard Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

COC#

Cition Introduction

Project #	Purchase Order #			Requested Analytic	al Method #	. [	THIS AREA FOR L	AB USE ONLY
Project Name		7	RI, Ba, Ca, Fe, Mg, Ma, K, Nb, Sr, As, Cd, Cr, Pb, H5, Se, Ag, Zn	Alkainity 1705, Color, Branide, Chloride, Fluoride, Sulfate, Ceachive Silica Al, Ba, Ca, Fe, MS, Mn, K, Na, Sc, As, Cd, Cr,	Pb, Hg, Se, Ag, Zn Alkelinity, TDS, Color, Bramide, Chloride, Fluoride, Sulfate, Reactive, Silica		3089	Page of
McAllen ReUse Pil Company Name City of McAl Project Manager or Contact & Phone #	6+ Study	O T A	M, Ba, Ca, Fe, Mg, M. K, Na, Sr, As, Cd, C Pb, H5, Se, Ag, Zn	Alkainity 705, Color, Bromide, Chloride, Fluoride, Sulfate, Geogrive Silica Al, Ba, Ca, Fe, Ms, Mn, K, Na, Sc, As, Cd, Cr,	Sey Ag , Zn 1, TDS, Color Chloride Sulfate Silica	l li	Lab PM	Custody Review
Company Name	· · · · · · · · · · · · · · · · · · ·	] [	5 0 8	2 24 75 0	8 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3			•
City Of McH/	lew		17 E 2	हि से १० १० में स	Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Sent / Se		Log In	LIMS Verification
<b>,</b>	· ·	ř	300	रे येते बेब भे	2 2 2 2 3	[ [	LOG III	rimo vernication
Kashu McKinley Requested Completion Date: Site ID	Kathy MKinley	CON	3 2 ₹	La Se Line	7 19 18 18			
Requested Completion Date: Site ID	Sample Disposal:	N	2 3	지 기를 하는 것	Pb, 14g, 9 Alkalinity, Branide, Fluoride, Reactive,	1	PH	Custody Seals Y N
ASAP NUT	P#2 Diapose Return	Î		Preservati	ve			ice YN
i tabe i morrer t		ER					QC Level 1 2 3 (	Other
	CLIENT SAMPLE ID LAB (9 CHARACTERS) QC	s	H N03	I Ce Huo,			Cooler Temperature	2
Date Time P B E L	·		] ]	H	JH		Alternate Descript	ion Lab ID
9/14/99 08:50 LC R G 9/14/99 08:50 LC R G 9/14/99 08:50 LC R G 9/14/99 08:50 LC Z G	o e	1						Z
9/14/99 08:50 4 20	ρ	1		\ \				2
9/14/99 08:50 12 0	P	1		J				
7/14/94 08:50 44 26								Ì
1/1/1/05/39								
	<del>                                      </del>	<del>                                     </del>	<del> </del>				······································	
		<del> </del>					<del></del>	
		<del> </del> -						
Relinquished By . ; , / /	Date/Time	Recely	ed By	Empty Bottles	<u> </u>	Date/Tim		
Relinquished By Willamed	9/14/99 08: 30	X	Wished By	may 1	gn and print name)	9	114/19 08:30	
X Aven Juera Javi	er Hinnisa 19/14/9908:50 )	X	Mari He		R Hinoipsa	9	114/99 08:55	
Sampled By and Title  X Augus Guera Javi  Received By (Pleas  KALL V. JAMPA RES)	e sign and print name)  ON ARCA 91449 6:55	Reling	water Vu	Vanel Rusic	R Hindiasu Ign and print name) VIII PARE 191	Date/Tim	lulga	
Received By Pleas	te sign and print name)  VITTO 122	Shippe	ed Via	SI	hipping #			
Special instructions:	<u> </u>	UP8	Fod-Ex	Other				
Separation and and separate	,							



Ms. Anne McKee-Robbins CH2M HILL/CVO 2300 N.W. Walnut Blvd. Corvallis, OR 97330

> Columbia Analytical Services Report City of McAllen D9901720/D1454

> > October 20, 1999

Submitted by:

Karen Sellers Project Manager/Client Services

## **TABLE OF CONTENTS**

## CAS Lab Reference No.: D1454 Level 1

	Page
	No.
Cover Page	i
Table of Contents	ii
Organic Data Qualifiers	iii
Organic Sample ID Qualifiers	iv
Sample Identification Cross-Reference	v
GC ORGANOCHLORINE PESTICIDES	
Case narrative	2
Sample results	3
Chain of Custody Documentation	9

(This report contains a total of 16 pages.)

## **Organic Data Qualifiers**

- A -- This qualifier indicates that a TIC is a suspected aldol-condensation product
- B -- This flag is used when the analyte is found in the associated blank as well as the sample. This notation indicates possible blank contamination and suggests that the data user evaluate these compounds and their amounts carefully.
- C -- The "C" flag indicates the presence of this compound has been confirmed by the GC/MS analysis.
- This qualifier is used for all the compounds identified in an analysis at a secondary dilution factor. "D" qualifiers are used only for the samples reported at more than one dilution factor.
- E -- This flag indicates that the value reported exceeds the linear calibration range for that compound. Therefore, the sample should be reanalyzed at the appropriate dilution. The "E" qualified amount is an estimated concentration, and the results of the dilution will be reported on a separate Form I.
- I -- The qualifier indicates that the reporting limit to the "I" qualifier has been raised. It is used when the chromatographic interference prohibits detection of a compound at a level below the concentration expressed on the Form I.
- J -- Indicates an estimated value. It is used when the data indicates the presence of a target compound below the reporting limit or the presence of a Tentatively Identified Compound (TIC).
- N -- This qualifier indicates presumptive evidence of a compound. This flag is only used for Tentatively Identified Compounds (TIC), where the identification is based on a mass spectral library research. It is applied to all TIC results. For generic characterization of a TIC, such as chlorinated hydrocarbon, the "N" qualifier is not used.
- P -- This qualifier is used for Pesticide/Aroclor target analytes when there is a greater than 25% difference for detected concentrations between the two columns. The lower of the two values is reported on Form I and flagged with a "P".
- Indicates the compound was analyzed for but not detected. The number adjacent to
  the "U" qualifier indicates the reporting limit for that compound. The reporting limit
  can vary from sample to sample depending on dilution factors or percent moisture
  adjustments when indicated.

## **Organic Sample ID Qualifiers**

The qualifiers that may be appended to the Lab Sample ID and/or the Client Sample ID for organic analysis are defined below:

- **DL** -- Diluted reanalysis. Indicates that the results were determined in an analysis of a secondary dilution of a sample or extract. A digit to indicate multiple dilutions of the sample or extract may follow the "DL" suffix. The results of more than one diluted reanalysis may be reported.
- MS -- Matrix spike (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- **MSD** -- Matrix spike duplicate (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- R -- Reanalysis. The extract was reanalyzed without re-extraction. The "R" is not used if the sample was also re-extracted. May be followed by a digit to indicate multiple reanalysis of the sample at the same dilution.
- **RE** -- Re-extraction analysis. The sample was re-extracted and reanalyzed. May be followed by a digit to indicate multiple re-extracted analysis of the same sample at the same dilution.

### Sample ID Cross-reference Table

CAS Lab Sample	ID.	Client Sample ID	Collect Date Sample Matri	x Additional	Description	
FS = Field	d Samp	ole				
D1454001 D1454002	FS FS	ZGPERMEATE ROPERMEATE	09/23/99 Water 09/23/99 Water	ZGPERMEATE ROPERMEATE		

The above lab sample ID's and cross reference information apply to samples as received by the laboratory. Modifiers to the lab sample ID may be added for internal tracking purposes. Any modified sample ID will be reflected in the appropriate case narrative only.

GC ORGANOCHLORINE PESTICIDES

#### CASE NARRATIVE GC ORGANOCHLORINE PESTICIDES

Project: City of McAllen

#### I. RECEIPT

No exceptions were encountered unless a Sample Receipt Exception Report is attached to the Chain-of-Custody included with this data package.

#### II. HOLDING TIMES

- A. Sample Preparation: All holding times were met.
- B. Sample Analysis: All holding times were met.

#### III. METHOD

Preparation: SW-846 3520C

Cleanup: NA

Analysis: SW-846 8081A

#### IV. PREPARATION

Sample volume may vary based on the amount of sample received per container.

#### V. ANALYSIS

- A. Calibration. All acceptance criteria were met.
  - 1. Retention Time Windows: All analytes were within criteria.
  - 2. Degradation: All acceptance criteria were met.
- B. Blanks: All acceptance criteria were met.
- C. Surrogates: All acceptance criteria were met.
- D. Internal Standards: All acceptance criteria were met.
- E. Spikes: All acceptance criteria were met.
- F. Samples: Sample analysis proceeded normally.

I certify that this data package is in compliance with the terms and conditions agreed to by the client and Columbia Analytical Services, both technically and for completeness, except for the conditions noted above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or designated person, as verified by the following signature.

SIGNED:	J. Water 10/20/99	Reviewer: The More
	Jerry Watega	
	Scientist, GC Organics	$\sim$

CLIENT ID.

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

ZGPERMEATE

Case No.: D1454 SDG No.: D1454 Lab Sample ID: D1454001

Matrix: WATER Level: LOW Lab File ID: B1001024

Sample Wt/Vol: 1.050 L Jate Received: 09/24/99

Extract Vol: 10 ML Date Extracted: 09/27/99

Column: DB5 Date Analyzed: 10/02/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8 72-43-5	gamma-BHC (I Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.11 0.093 0.040 050	J U U

CLIENT ID.

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

ROPERMEATE

Case No.: D1454 SDG No.: D1454

Matrix: WATER Level: LOW 📝 Lab File ID: B1001025

Sample Wt/Vol: 1.050 L Date Received: 09/24/99

Extract Vol: 10 ML Date Extracted: 09/27/99

Column: DB5 Date Analyzed: 10/02/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8 72-43-5	gamma-BHC (L Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.0.0 0.0.0 0.0.0 0.0.0	ט ט ט

CLIENT ID.

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

PWB10927

Case No.: D1454 SDG No.: D1454 Lab Sample ID: PWB10927

Matrix: WATER Level: LOW Lab File ID: B1001023

Sample Wt/Vol: 1.000 L Date Received:

Extract Vol: 10 ML Date Extracted: 09/27/99

Column: DB5 Date Analyzed: 10/02/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8	gamma-BHC (I Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.020 0.040 0.50	บ บ บ

### 2C WATER SEMIVOLATILE SURROGATE RECOVERY

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1454 SDG No.: D1454

		· · · · · · · · · · · · · · · · · · ·				
		t	S1	S2	S2	TOT
	LAB ID	CLIENT ID.	#	#	1	OUT
	LIMB ID	CLILIANI ID.	#	#	1	LOOT
	=========		=====	=====	=====	===
01	PWB10927LCS	PWB10927LCS	93	74	Į.	
02	PWB10927LCS	PWB10927LCS	92	80		0
03	PWB10927	PWB10927	96	89		
04	D1454001	ZGPERMEATE	112	73	i	0
05	D1454002	ROPERMEATE	106	62		l ol
06					i ———	
						ll
07						
08			<del></del>		<u> </u>	
				l		
09						
10	-					
						<u> </u>
11	- <u></u> :					
12						1
13						
			·			
14						
15	-					
16		<del></del>				
17						
18						
					<del></del>	
19						
20						
21						
21					<del></del>	
22						
23						
23						
24						
25						
22						
26						
27			į			
28						
					I	
29	1	l	i			1
30						
J 5						'

QC LIMITS

= Tetrachloro-m-xylene S1 (45-125)= Decachlorobiphenyl (34-133)S2

# Column to be used to flag recovery values
* Values outside of contract required QC limits

D Surrogates diluted out

page 1 of 1

FORM II

SW846

### 3E WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1454 SDG No.: D1454 Column: DB5

LCS - Sample No.: PWB10927

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
gamma-BHC (Lindane)	0.5000	0.0000	0.5002	100	73-125
Endrin	0.5000	0.0000	0.4876	98	43-134
Methoxychlor	0.5000	0.0000	0.4194	84	73-142

# Column to be used to flag recovery and RPD values with an asterisk

* Values outside of QC limits

RPD: 0 out of 0 outside limits

Spike Recovery: 0 out of 3 outside limits

COMMENTS:	

SW846

### 3E WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1454

SDG No.: D1454 Column: DB5

LCS - Sample No.: PWB10927

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
Toxaphene	5.000	0.0000	4.895	98	41-126

# Column to be used to flag recovery and RPD values with an asterisk

* Values outside of QC limits

RPD: 0 out of 0 outside limits

Spike Recovery: 0 out of 1 outside limits

COMMENTS:	

CHAIN OF CUSTODY DOCUMENTATION	



# **CHAIN OF CUSTODY**

5090 Caterpillar Road • Redding, CA 96003 • Phone: (530) 244-5227 • FAX: (530) 244-4109

coc# Nº 990802

Project #	Purchase Order #				Requeste	d Analy	lical Metho	d#		THIS AREA FOR LAB USE ONLY				
			25						Li	ab#	Page of			
Project Name	- 1 1	Ţ	797	704		1		1 1	17	D1454				
MAKEN REUSE PILOTS Company Name City OF McAllon Project Manager or Contact & Phone # 541-758-	tidy	O T	7 3	Methoxych	} }	]	]		L		Custody Review			
Company Name	•	L L	Lindane,	ž 🗐	1				7	ag. Vengela	1			
City of Michillan	/	*	200	13 E	1 1	ſ		1 1	1	og Ih	LIMS Verification			
Project Manager or Contact & Phone # 541 - 758-	Report Copy to:  Kathy McKinley  Site ID Sample Disposal:			→ "F	1 1	İ	1	1 1	1					
Kayly MKinley 0235 Requested Completion Date:	Site ID Sample Disposal:	Ç.	Endrin, Joxaphene	Foxephen:	1 1			] ]	pl	н	Custody Seals N			
Requested Completion Bate:	The of	CONTA	nd f	ई दे		ļ					Ice ON			
4	14 0 f MAHEN Dispose Return	Ä	<u>ي اچا</u>	0 K	11						·			
ASAP u	INTP#2   H	Š		Pre	servative (	to be fill	ed out by co	ustomer)	°	OC Level 1 2 3 Olf	ner			
Sampling C.G.W.S.A	Ì	R	_ 0	70	1 1		ļ		C	cooler Temperature				
	CLIENT SAMPLE ID LAB	Ĭ		5	]		j		<u> </u>	5.0	<u> </u>			
Sampling C G W S A O I M A T I R P B E L	(9 CHARACTERS) QC		H ₂	H25		l				Alternate Description	Lab ID			
	Permeate	4	/								-1			
9/2/99 V Z G		4									-2			
					11									
<del>├──┼──┼┼┼┼┼</del>	<del>}-}-}-</del>	$\vdash$	-			-			<del></del>					
<del></del>	<del>                                     </del>	-	<del>  </del>						<b></b>					
		<u> </u>												
		Ĺ												
		1		Ì		3								
<del>├───<del>╎</del></del>	<del>-   </del>	╁		<del></del>	-}		<del> </del>		<del></del>					
<del>   - - - - - - - - - - - - - </del>	<del></del>	<del> </del>		<del></del>										
		<u> </u>			1	L								
Sampled By and Title	(Please sign and print name) Date/Tim	ne Non-	Relingu	ished By	1		(Please sig	n and print r	ame)	Date/Time	) 0 110			
Hecebert By	(Please sign and print name) Qate/Tim	(3.3℃ ie	Relinge	ished By	JAN 1		(Please sig	ne fer	C2	9/23/99 Q	8:40			
Sampled By and Tille  Received By  RUDIE VIlland	Please sign and print name)  Please sign and print name)  Posic Villarran 9/3/99	8:4	o la	Held By	llaned	<u> </u>	Kosic	VILLARI	24/	Date/Time 9/24/99				
Heceived By	(Please sign and print name) Date/I im	)6 /41	Shippe	d Via	Other		Shipping #	81291	Δ77.	C 117				
Special Instructions:  Semples were	and I among the 17-17-17	•						10	<u>~ (                                   </u>	INVOICE INFO	RMATION			
Samples were	collected on 9/23	5 /	77							P.O. #				
										Bill To				
[														



5090 Caterpillar Road

Redding Ca., 96003

Phone: 530-244-5227

Fax: 530-244-4109

# **SAMPLE RECEIPT EXCEPTION REPORT**

	ple Batch Number: D 1454	Client/Project: City of McAllen
Samp	ole Batch Number: D 7434	Client/Project: City of McAllen
		Comments:
	No custody seal as required by project.	2) No time sampled recorded on COC. Time taken from container
/	2. Analysis, description, date/time of collection not provided.	labels.
	Samples broken or leaking on receipt.	
	Temperature of samples inappropriate for analysis requested.	
	Container inappropriate for analysis requested.	
	6. Inadequate sample volume.	
9.1	7. Preservation inappropriate for analysis requested.	
	8. Samples received out of holding time for analysis requested.	
	Descrepencies between COC form and container labels.	
	10. Other	

Corrective Actions Taken:

wore Regured

8N 9/28/99

# Sound Analytical Services, Inc.

ANALYTICAL & ENVIRONMENTAL CHEMISTS

4813 Pacific Hwy East • Tacoma, WA 98424 (253) 922-2310 • FAX (253) 922-5047 e-mail: saincl@uswest,net



#### TRANSMITTAL MEMORANDUM

DATE: September 23, 1999

TO: Kathy McKinley City of McAllen 4100 Idela McAllen, TX 78503

PROJECT: McAllen Re-Use Pilot Study

REPORT NUMBER: 84099

Enclosed are the test results for two samples received at Sound Analytical Services on September 15, 1999.

The report consists of this transmittal memo, analytical results, quality control reports, a copy of the chain-of-custody, a list of data qualifiers and analytical narrative when applicable, and a copy of any requested raw data.

Should there be any questions regarding this report, please contact me at (253) 922-2310.

Sincerely,

Daria Powell
Project Manager

Client Name
Client ID:
Lab ID:
Date Received:
Date Prepared:
Solids
Dilution Factor

City of McAllen
ZENOGEM PERMEATE
ZENOGEM PERMEATE
34099-01

9/15/99
9/21/99
9/22/99
9/22/99

### Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

			Recov	ery Limits
Surrogate	% Recovery	Flags	Low	High
2,4-Dichlorophenylacetic acid	86.4		48	124

Analyte	Result (ug/L)	PQL	MDL	Flags
Milailice	(49:4)			
2,4-D	ND	0.096	0.084	
Silvex (2,4,5-TP)	ND	0.096	0.077	

Client Name Client ID: Lab ID:

**Dilution Factor** 

Date Received: Date Prepared: Date Analyzed: % Solids

City of McAlien RO PERMEATE 84099-02 9/15/99 9/21/99 9/22/99

10

## Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

**Recovery Limits** Low High Surrogate % Recovery Flags 124 48 2,4-Dichlorophenylacetic acid 73.6

Result Analyte (ug/L) PQL MDL Flags 0.1 0.087 2,4-D ND Silvex (2,4,5-TP) ND 0.1 0.081

Lab ID:

Method Blank - HB885

Date Received:

9/21/99

Date Prepared: Date Analyzed:

9/22/99

% Solids

**Dilution Factor** 

10

## Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

			Recov	ery Limits
Surrogate	% Recovery	Flags	Low	High
2,4-Dichlorophenylacetic acid	67.8		48	124

Result

MDL **Flags** Analyte (ug/L) PQL 0.1 0.087 2,4-D ND 0.081 ND 0.1 Silvex (2.4,5-TP)

## Blank Spike/Blank Spike Duplicate Report

Lab ID: Date Prepared: HB885 9/21/99

Date Analyzed: QC Batch ID:

9/22/99 HB885

## Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

	Blank Result	Spike Amount	BS Result	BS	BSD Result	BSD		
Compound Name 2,4-D	(ug/L) 0	( <b>ug/L)</b> 5	(ug/L) 4.73	% Rec. 94.6	(ug/L) 4.48	% Rec. 89.6	RPD -5.4	Flag
Silvex (2,4,5-TP)	0	5	5.44	109	5.17	103	-5.7	

ANALYTICAL & ENVIRONMENTAL CHEMISTS

4813 PACIFIC HIGHWAY EAST, TACOMA, WASHINGTON 98424 - TELEPHONE: (253) 922-2310 - FAX: (253) 922-5047

### DATA QUALIFIERS AND ABBREVIATIONS

- B1: This analyte was detected in the associated method blank. The analyte concentration was determined not to be significantly higher than the associated method blank (less than ten times the concentration reported in the blank).
- B2: This analyte was detected in the associated method blank. The analyte concentration in the sample was determined to be significantly higher than the method blank (greater than ten times the concentration reported in the blank).
- C1: Second column confirmation was performed. The relative percent difference value (RPD) between the results on the two columns was evaluated and determined to be < 40%.
- C2: Second column confirmation was performed. The RPD between the results on the two columns was evaluated and determined to be > 40%. The higher result was reported unless anomalies were noted.
- M: GC/MS confirmation was performed. The result derived from the original analysis was reported.
- D: The reported result for this analyte was calculated based on a secondary dilution factor.
- E: The concentration of this analyte exceeded the instrument calibration range and should be considered an estimated quantity.
- J: The analyte was analyzed for and positively identified, but the associated numerical value is an estimated quantity.
- MCL: Maximum Contaminant Level
- MDL: Method Detection Limit
- N: See analytical narrative.
- ND: Not Detected
- PQL: Practical Quantitation Limit
- X1: Contaminant does not appear to be "typical" product. Elution pattern suggests it may be ______.
- X2: Contaminant does not appear to be "typical" product.
- X3: Identification and quantitation of the analyte or surrogate was complicated by matrix interference.
- X4: RPD for duplicates was outside advisory QC limits. The sample was re-analyzed with similar results. The sample matrix may be nonhomogeneous.
- X4a: RPD for duplicates outside advisory QC limits due to analyte concentration near the method practical quantitation limit/detection limit.
- X5: Matrix spike recovery was not determined due to the required dilution.
- X6: Recovery and/or RPD values for matrix spike(/matrix spike duplicate) outside advisory QC limits. Sample was reanalyzed with similar results.
- X7: Recovery and/or RPD values for matrix spike(/matrix spike duplicate) outside advisory QC limits. Matrix interference may be indicated based on acceptable blank spike recovery and/or RPD.
- X7a: Recovery and/or RPD values for this spiked analyte outside advisory QC limits due to high concentration of the analyte in the original sample.
- X8: Surrogate recovery was not determined due to the required dilution.
- X9: Surrogate recovery outside advisory QC limits due to matrix interference.

5	

# Sound Analytical Services, Inc.

ANALYTICAL & ENVIRONMENTAL CHEMISTS 4813 Pacific Hwy East • Tacoma, WA 98424 (253) 922-2310 * FAX (253) 922-5047

e mail, saine bit uswest net

2

TURNAROUND REQUEST-	(business days)
Standard (10 days)	
RUSH: 24 hrs 48 hrs	5 day

CHAIN OF CUSTODY/R	EQUEST	FOR L	ABORA	ATORY	ANAI	LYSIS	3
MiAllero	Analys	es Requ	ested				
	T-7			1	7		_

Project Name:					Analys	es Keq	ueste	ed										
												T		1			Γ	1
McAllen Re-Use Pilot Study					ļ	2,4-0,2,45-TP	۵										į.	
McAllen Re-Use Pilot Study Contact: Kathy McKinley - Applied Sciences Phone No: 541-758-0235 #3144						F >	2,4-0,2,4,5-TP Sivex						-					
Phone	NO CR - DILL	A tiest	rience ;	,	S	14.7	\(\mathbb{E}_{\overline{\chi}}\)		ĺ	ĺ				1	1	l	1	ł
Env No	541-754-023	<u> </u>	<u> </u>		Containers	77,	7.3					1				ŀ	1	1
Fax NC	541-766-28	<u>52                                    </u>			밀	1.5	7.		l		į	-						
Email:	Kmckinle@ ci	2 m	CAM	`	ပိ	<u> </u>	19	ĺ	1		1	1	İ	Ì			l '	
LEBU				1 (	<b>*</b> 0#	<u>जं</u>	<b>5</b>				l			ļ		}		
Use Only	Sample ID			Matrix	**	7	7	<u> </u>	<u> </u>	<u> </u>		<u> </u>	l	<u> </u>				
1	Zenogem Permonte	9114/19	62:50	Liquid	١	1					1		ľ	1				
	lenogen Permonte RO Permonte	9/14/19	a 2:50	Lieuid	1		1											
Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Contro	1	1		1-17									$\vdash$					
						<del>                                     </del>	<del>                                     </del>	<del> </del>		├	<del> </del>	-	· · · · <del>- · ·</del>					
ernan ing kanaga Marahasa ya ya kanaga Marahasa ya kanaga ka	<del></del>	-	<u></u>	<b>i</b>		ļ	<b></b>			-	-		<del> </del>					
Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Contro				<u> </u>									<u> </u>		<u> </u>			
		ļ		]														
Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Control of the Contro																		
		<del> </del>		<b>——</b>		1	<del></del>						<del> </del>				<del>                                     </del>	
						ļ	-			ļ	-	<u> </u>	├─-	<b> </b>		<b></b>	┝╼┥	
****						L						<u> </u>	<u> </u>					
				1 1													j	
						_												
	<del>_</del>																	
				† <del></del>						<u> </u>							-+	
		-		<b> </b>	,	<b> </b>			ļ <u>.</u>		ļ		<del> </del> -			<del></del>	-	
		ļ				L				L		<b></b>	<u> </u>					
		]																
0.00	<u></u> ,,																	
**************************************				$\vdash$														
Accessorably Constitution	,	1		1		Ì	I 1			i			l		١	. 1		l

	Signature	Printed Name	Firm	Time/Date	Special Instructions
Relinquished By:	tan Han	Janes Hinojosa	City of Aut Hen	08:55	
Received By	logie Villand	Posse VillArest	NiA/bn	08:55	
Relinquished By:	Rosie Villami	for VillARKERA	Cotto F CAMer	4114144	
Received By	Ceiana	Giana	SAS	9/15/99	DAnn
Relinquished By:	d	.0			"//
Received By				Ţ	

COC No	Page	of



### **ENERGY LABORATORIES, INC.**

SHIPPING: 2393 SALT CREEK HIGHWAY . CASPER, WY 82601

MAILING: P.O. BOX 3258 • CASPER, WY 82602

E-mail: energy@trib.com • FAX: (307) 234-1639 • PHONE: (307) 235-0515 • TOLL FREE: (888) 235-0515

## **CASE NARRATIVE**

**DATE:** 

October 5, 1999

TO:

Kathy McKinley

FROM:

Sheryl Garling

RE:

CH2MHill Water Samples

SAMPLE NUMBERS: 32965 001 through 002

Samples Zenogem Permeate and RO Permeate were received on September 15, 1999. Samples were shipped using Energy Laboratories, Inc. contract service with UPS. The overnight option was used for shipping the samples to the laboratory. Samples were in good condition and properly preserved.

No analytical problems were indicated for this sample delivery group.

The methods used are methods published by US EPA for drinking water analyses. The methods used are as follows:

Radium 226 - EPA Method 903.0 (alpha emitting),

Radium 228 - EPA Method 904.0, and

Gross Alpha -EPA Method 900.1 (gross alpha minus uranium and

radon).

The standard detection limits for these methods are 0.2 pCi/L, 1.0 pCi/L, and 1.0 pCi/L, respectively. The initial e-mail response incorrectly identified methods and detection limits.

If additional information is required, please advise.



## **ENERGY LABORATORIES, INC.**

SHIPPING: 2393 SALT CREEK HIGHWAY • CASPER, WY 82601

MAILING: P.O. BOX 3258 • CASPER, WY 82602 E-mail: energy@trib.com • FAX: (307) 234-1639 PHONE: (307) 235-0515 • TOLL FREE: (888) 235-0515

### LABORATORY ANALYSIS REPORT - CH2M HILL

Project:
Sample ID:
Laboratory ID:
Sample Matrix:
Sample Date/Time:
Date Received:
Report Date:

e Pilot Study					
gem Permeate RO Permeate					
32965-002					
er					
/0850					
-99	-				
4, 1999	: '				
	RO Permeate 32965-002 er 9/0850 -99				

Radiometric		Method	Reporting Limit	Units	Res	sults
Radium-226	²²⁶ Ra	903.0	0.2	pCi/L	< 0.2	< 0.2
Radium Precision ±					-	-
	<u></u>					144
Radium-228	²²⁸ Ra	904.0	1.0	pCi/L	<1.0	<1.0
Radium Precision ±					-	-
			programme and the			
Gross Alpha	Gross α	900.1	1.0	pCi/L	<1.0	<1.0
G. Alpha Precision ±					-	-



### RADIOCHEMICAL QUALITY ASSURANCE REPORT - CH2M HILL

Laboratory ID Range: Sample Matrix: Sample Date / Time:

> Date Received: Report Date:

32965-001-002	_
 Water	_
 09-14-99/0850	_
09-15-99	_
October 4, 1999	_

	Method	Relative Percent Difference ¹	Spike Recovery (Percent) ²	LCS Recovery (Percent)	Method Blank (pCi/L)	Date Analyzed	Analyst
Laboratory #:		32996-002	32880-022		GA-40		
Gross Alpha:	900.1	0.0	104	106	<1.0	10-01-99	RS
Laboratory #:		32880-001	32880-022		RA-206		
Radium-226:	903.0	0.0	100	101	< 0.2	09-29-99	RS
Laboratory #:		32880-010	32880-020		228-235		
Radium-228:	904.0	0.0	79	77	<1.0	10-04-99	LMH

- (1) These values are an assessment of analytical precision. The acceptance range is 0-20% for sample results above 10 times the reporting limit. This range is not applicable to samples with results below 10 times the reporting limit.
- (2) These values are an assessment of analytical accuracy. They are a percent recovery of the spike addition. ELI performs a matrix spike on 10 percent of all samples for each analytical method.

Report Approved By: DIRacla

Reviewed By:

Log In No. 99-32965

lmh r:\Reports\Clients.99\CH2M_Hill\Water\rc32965-001.xls

ENERGY LABORATORIES, INC.'S CHAIN OF CUSTODY RECORD BillingsCasperGillette 82602-3258 Mail Only: PO Box 3258 • Casper, WY UPS/FedEx Deliveries: 2393 Salt Creek Highway • Casper, WY • 82601 • Rapid City

toll free 1-888-235-0515 voice 307-235-0515

fax 307-234-1639

For Sai	nple Tra	cking	Pur	poses, Please Provide Contact Name and Telephone	r's as Indicated	d (Si	EE BAC	K OF F	ORM F	OR EX	AMPLE	ES AND INSTRUCTIONS)
Project McAller P.W. S.	n lellse	/ Me	ation 19/len as		Type of Analyses Requested							Special Requests
Name	/ Phone	/ 4	Fax 541- # 3)	758-0235 / 54-766-28 <b>25</b> 52 44	containe W S V	ros Alpha	Gross Alpha,					
Date	Time	composite	sample	Send Invoice to: Kathy McKinley  CH2M HILL Corvallis OK.  Santas abac	Number of containers Sample Type: A W S V U O Air <u>W</u> ater Soils/solids <u>V</u> egetation <u>U</u> rine <u>O</u> the	m 226, Gras Alpha , 228	24, 4005			-		
Date	Time	тиоо	grab s	Send Report to:  Sample I.D.	N San <u>A</u> ir <u>W</u> ater	Radium	Redium 2 Redium					Comments, Special Instructions, etc.
9/14/55	08.50		/	Zonogem Permeate		<b>V</b>						
9/14/99	08:50		/	Ro Permeate	<u> </u>		<b>/</b>					
. ,												
				UPS-Al								
					<u> </u>				L			,
					:							•
												i
								:				

	1. Sampler: (signature)	Date	Time	Received by: (signature)	2. Relinquished by: (signature)	Date	Time	Received by: (signature)	ĺ
	clavi Hingosa	9/14/99	01:50	RopieVillanal	Ropie Villanel	9/14/99	<del>08:35</del>		Į
	3. Relinquished by: (signature)	Date	Time	Received by: (signature)	4. Relinquished by: (signature)	Date 9/15/95	Time	Received at Laboratory by: (sign ture)	1
•						· · · · · · · · · · · · · · · · · · ·	<u> </u>		

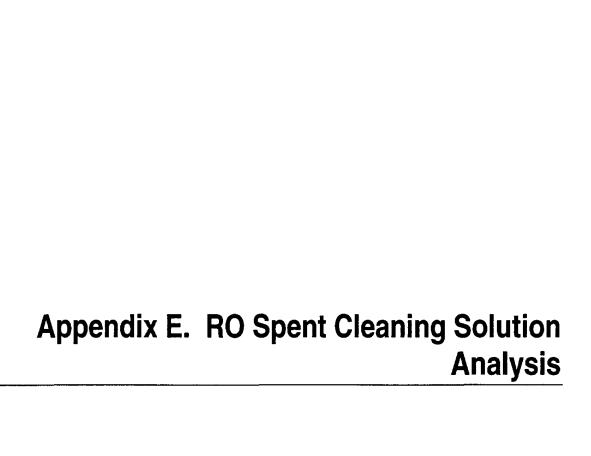
Project Name	Thunde	rbasi # /	Fax P (3)	/ Purchase Order #  Town of Hope No PO #  D7) 555-1515, (307) 555-5555 fax  Send Invoice to: Jeff Jones PO Box Nowhere	Number of containers Sample Type: A W S V U O dir Water Soitstoids Vegetation Urine Other	- TEM		of Analy	SO2.2	504, 505, 508	5, 531.1	Special Requests  Please fax  results  as soon as  possible  Thank you.
Date	Time	composite	grab sample	Hope, WY 80000  Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D.	San San Air <u>W</u> aer	Asbestos	IOC's - RADs	NO ₂ , NO ₃ , F	VOCs - 50	90Cs - 50	50Cs - 515,	Comments, Special Instructions, etc.
1995				\	;							
5/28	11:35		x	Entry to Distribution	4	×			Х			Phase II SDWA Primary
5/28	11:45		X	Distribution Tap	9		Х	Х		Х	Х	*

1.Sampler: (signature) <b>Jeff Jones</b>	Date 5-28-95	Time 1 <b>2:05</b> p	Received by: (signature) Harry Truckers	2.Relinquished by: (signature) Harry Truckers	Date 5-28-95	Time <b>13:15p</b>	Received by: (signature) Sheryl A. Garling
3. Relinquished by: (signature) N/A	Date N/A	Time N/A	Received by: (signature) N/A	4. Relinquished by: (signature) Sheryl A. Garling	Date 5-28-95	Time 14:00p	Received at Laboratory by: Roger A. Garling

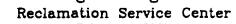
### Instructions:

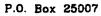
- A completed Chain-of-Custody must be submitted with all samples (1)
- (2) Special Requests area can include (but not limited to) the following:
  - Turnaround status, Rush status, Due Date, etc.
  - Special mailing instructions:

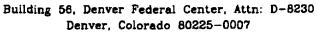
    - send copy of Report and/or Invoice to a second party
       send copy of Report to a Government Agencies (EPA, etc.)
- Public Water System (PWS) Number
- Do you want samples returned to you or disposed of?



# United States Department of the Interior Bureau of Reclamation Water Treatment Engineering and Research Group









# **FAXOGRAM**

Date:
To: Jim Lozier / Angre Formandez
Company: CH2MH1)
Fax Number:
From: Michell USBR
Fax Number: (303) 445-6329 Telephone Number: (303) 445-2245
Number of pages(including cover sheet)
Message: Copy of the Cleaning Solution
analysis. They are sending out
for the Soy, I'll let you know.
Mahell
·
<del></del>

# DATA TRANSMITTAL FAX COVER

uunhuzhubbb lub:54

Environmental Research Chemistry Laboratory, D-8240
US Bureau of Reclamation - Technical Service Center
PO Box 25007, Denver CO 80225-0007
Margaret Lake, Laboratory Manager, 303-445-2181
Douglas Craft, QC Officer, 303-445-2182
FAX 303-445-6326

DATE: 6/10/99
FROM: Dard Frost PHONE: X2190
TO: Michelle Chapman MAIL CODE:
OFFICE: FAX NUMBER:
PROJECT: McAllen DO LAB NUMBERS: \$5313-1
SAMPLES COLLECTED ON: 61199 NUMBER OF SAMPLES:
ANALYSES PERFORMED BY: BF VM
This is an electronic transmission of analytical results. The final data and memorandum with appropriate formal review and requested QC reports will follow. The data in the attached report has been reviewed by the laboratory QC Officer (or designate) and meets TSC Chemistry Laboratory precision and accuracy requirements unless qualified in the section below. Please review your data and let us know if there are problems that require corrective action.
QUALIFIERS: The following issues may affect the usability of your data:
Ca biased low by 20.5% CCV
was acceptable.
MESSAGE: Contract Soy and yind memo will Jollow.
APPROVAL Barb Frost Barb 9705 6/10/99 Client Representative For OC Officer Date
PAGE 1 OF REVIEWED-QUALIFIED SEE COMMENTS
LAB QC OFFICER DATE

## SAMPLE LOG-IN SUMMARY

## USBR ENVIRONMENTAL RESEARCH CHEMISTRY LABORATORY

Denver, Colorado

Job Control No: McAllen-99

Project Name: McAllen W-R

Login Date: 6/3/99

Description: Cleaning Solution

Client Reps: Barb Frost

Client Name: M. Chapman-Wilber

Chem Client Lab# SampleID

Sample Analysis

Sampled Date

6/1/99

Due Date

6/10/99

COC#

K5313-1

McAllen

unfiltered/unacidified, SO4/Ca/Fe/Al/Ba/Si

200.7_ICP

ICP Metals

300.0_ANIONS 365.1,365.2_totP ion chromatography of anions

Type

cleaning soln.

total phosphorous by Perstorp autoanalyzer

SAMPLE SUBMITTAL REQUEST FORM	SHEET 1 OF						
Environmental Research Chemistry Laboratory U.S. Bureau of Reclamation - Technical Service Building 56, Room 2340, Denver Federal Cente Margaret Lake, Laboratory Manager, 303-445-2	e Center er, PO Box 25007, Den 2181						
Today's Date: $\frac{\sqrt{2}/99}{24}$	Report Data By:	10/99					
Today's Date: 4/2/99 Samples Submitted By: Michele ChomunW	Wellephone: XZZ	44					
Mailing Address: D-8>30 U	FAX/LAN:	<u></u>					
Project Name: McAllen W.R	Job Number/WOII	DS945					
Sample Collection Location: Mallen		-					
Sampling Date(s): $\frac{6/1/99}{1}$ Type of Samp							
Samples Filtered? No Samples Preserved?		ody Form Required? No					
Official Data Report To: Michello C L	Olbert.	<u> </u>					
Copies To:	QC	Report Requested?					
Special Instructions:	erium, Salta	te, Silica, Phos					
7	Requested	Method or					
SAMPLE IDENTIFIERS	Analyses	Det Lim					
1. Calcum							
2. Iran							
3.							
4,							
5.							
6.							
7.							
8.							
9.							
10.							
11.							
12							

Report	of Chemical Analyses			McAllen W-R Collected: 6/1/9:	9	· <u>-</u>	- '		<u>-</u> -		 	
PO Box 250	lment of the Interior - Bureau of Rei 007, Building 56, Room 2300, Denv 80225-0007		enter					 		····		
Laboratory	<b>y</b> -	SiO2	TP-P									
Number	Sample ID	mg/L	mg/L					 			 	
K5313-1	McAllen	2.53	11.9					 			 	
	Detection limit:	0.02	0.005									
1	Date Analyzed:	6/9/99	6/7/99							Γ	T	
	Analyst:	bf	vm									
	EPA Method:	200.7	365.1									

Chem Lab#: K5313-1

Station ID: McAllen

Sample Type: cleaning soln.

MoreID:

Sampled Date: 6/1/99

Received Date: 6/2/99

Login Date: 6/3/99

Chain-Of-Custody:

Note: unfiltered/unacidified,

SO4/Ca/Fe/Al/Ba/Si

 Analyte	Method_Ref	Result	Units Qualifier	MDL	Date Extract	Date Analyzed Dilution	
Al	200.7 EPA	5530	µg/L	30		6/10/99	1
Ba	200.7 EPA	449	μ <b>g/</b> L	4		6/10/99	1
Ca	200.7 EPA	. 26	mg/L	0.03		6/10/99	1

U: Not Detected at Listed MDL.

J: Estimated.

MDL: Method Detection Limit.

Chem Lab#: K5313-1

Station ID: McAllen

MoreID:

Sampled Date: 6/1/99

Received Date: 6/2/99

Login Date: 6/3/99

Chain-Of-Custody:

Sample Type: cleaning soln.

Note: unfiltered/unacidified,

SO4/Ca/Fe/Al/Ba/Si

Analyte	Method_Ref	Result	Units Qualifier	MDL	Date Extract	Date Analyzed D	ilution
Fe	200.7 EPA	722	µg/L	4		6/10/99	1

U: Not Detected at Listed MDL.

J: Estimated.

MDL: Method Detection Limit.



Table F-1
ZenoGem Permeate Scale Potential

Parameter	Units	6/9/99	6/11/99	6/14/99	6/16/99	6/21/99	6/23/99	Average
General Chemistry	独有机构				1.41		. 7.4	
Alkalinity	mg/L as CaCO ₃	150		190		158		166
Total Phosphorus	mg/L as P			2.72		2.26		2.49
Sulfate	mg/L	250	214	214				226
Metals	194						111	
Aluminum ^a	mg/L	0.1	0.1	0.1	0.1	0.1	0.1	0.1
Barlum	mg/L	0.06	0.06	0.06	0.05	0.05	0.06	0.06
Calcium Hardness	mg/L	360		348		360		356
Iron ^a	mg/L	0.1	0.1	0.1	0.1	0.1	0.1	0.1

^aNot dectected at specified reporting limits for each sampling event.



#### SPIRAL WOUND MEMBRANE ELEMENT AUTOPSY

#### PURPOSE AND LOCATION OF AUTOPSY

Purpose of Autopsy: McAllen, TX Wastewater Reclamation Project: Determination of scaling in end element.

Date and Place: October 29, 1999, USBR WTER Pilot Plant Lab, Denver, CO.

Date of This Report: 12/30/99

#### Names of Observers:

Frank Leitz Bill Boegli Michelle Chapman Wilbert Kim Linton Qian Zhang

ELEMENT IDENTIFICATION				
Manufacturer:	Hydranautics			
Element Location:	Housing #6, 2nd element			
Serial Number:	x03529			
Element Dimensions:	2.5 in. x 40 in.			
Number of Leaves:	2			
Size of Leaves:	92.1 cm x 71.1cm Total Area 84.5 cm x 63.5cm Active Area per side (2.1 m² per element or 22.1 ft²)			

#### OPERATING HISTORY

The RO system was operated for six months on site at the McAllen, TX South Waste Water Treatment Plant. Screened de-gritted sewage was first treated in a Zenogem bioreactor/microfiltration system, then chlorine and ammonia was added and the Zenogem effluent was forwarded to the RO system. The RO element array was a 2x2x1x1 and had 3 elements per vessel for a total of 18 elements in the system. RO recovery rates were set from 50% to 80% of 15.2 L/min feed flow.

Sulfuric acid and antiscalent were added to prevent scaling. However, due to changes in the chemical character of the Zenogem effluent, or excessive gas formation in the acid tank which caused the acid feed pump to loose it's prime, the pH was not controlled well at all times. This resulted in a loss of permeate flow from the last vessel.

Also, traditional constituents used in an RO projection do not include phosphorous compounds. The researchers involved in this project began to suspect that phosphorous salts were the cause of excessive scale problems due to the nature of waste water treatment. Attempts at adjusting the pH to control phosphorous salts included running a projection with non-RO software to determine the potential for phosphate scaling. A range of pH settings and two control points for pH were tested in an attempt to control the scaling problems. The pH ranges tested were from 5.5 to 7 on the feed, and 5.5 to 6 on the concentrate. The lower pH control ranges were in response to this non-RO projected information.

Scaling also caused operators to clean the system approximately 4 times with a low pH solution at a pH of about 3. A high pH solution was not used to clean the membranes as there was no indication of biofouling and the system's performance was recovered using the acid cleanings.

#### DESCRIPTION OF EVENTS LEADING TO AUTOPSY

This element was subjected to one needle hole to help evaluate the integrity test methods.

Subject element was the second to last element of the last vessel (vessel #6). Permeate recovery flow from the last vessel varied from 1.4 L/min to 0.01 L/min. The last fouling was a result of turning off the acid feed pump for approximately 8 hours.

This autopsy was primarily done to determine how deep the hole in the membrane leaves had penetrated, and to determine the general nature of the scaling composition.

#### NARRATIVE DESCRIPTION OF AUTOPSY PROCEDURE

Fiberglass wrapping was cut open and peeled or pried off.

Picture shows the compressed air saw and other autopsy materials.



Anti-telescoping devices were removed and tape wrap was unwound.

Unwound membrane and separated spacer material from first leaf.

Measured leaf dimensions and active area.

A squeegee was used to wipe both sides of one leaf. DI water was used to liquefy the fouling substance

Applied congo red dye to the first leaf.

Samples were cut from the feed and reject ends of the second leaf for SEM analysis. Feed side is Sample 2 and the reject side is Sample 3.

#### **OBSERVATIONS**

There was a crack, ~2 cm long, ~10 cm from the feed end.

Sample #1 is the piece of fiberglass with the crack.

The brine seal was in good condition; it was saved as Sample #2

There was extra glue, possibly rubber cement, under the tape at the ends of the element-- probably to keep the end caps tight. Sample #3 is a bit of the glue peeled away from the end.

There was no evidence of the crack extending into the membrane material.

Picture was taken of the feed end of the rolled element.





Hole location was marked on the outer fiberglass cover from where a needle had been poked into the membrane. Picture taken of hole location in element. The hole location is shown in the fiberglass wrap and in the number 9 of the tape wrap.



At least 2 leaves had holes which were identified using a

magnifying glass (10x). The hole on the on the outer leaf was a cresent shape which is the same shape that would be formed by the tip of the hypodermic needle used to inflict the damage. The second hole protruded out, which would also be consistent with the direction the needle would penetrate.

The glue line appeared to have attracted more fouling material than the active area of the leaf. This may be due to the excessive use of glue.

Dye test on the second leaf with congo red dye took evenly over the membrane surface. This could be damage from low pH. There was no evidence of the hole extending beyond the tape wrap.

Test and Test Objective: No additional tests were done on this element.

#### DISCUSSION AND CONCLUSIONS

This element had at least two holes from the needle puncture which penetrated the active area of the membrane. The visible damage was configured in such a way that it can be attributed to the needle. One of the holes was cresent shaped and poked inward. The hole on the opposite leaf protruded outward.

#### SPIRAL WOUND MEMBRANE ELEMENT AUTOPSY

#### PURPOSE AND LOCATION OF AUTOPSY

Purpose of Autopsy: McAllen, TX Wastewater Reclamation Project: Determination of scaling in end element.

Date and Place: October 29, 1999, USBR WTER Pilot Plant Lab, Denver, CO.

Date of This Report: 11/21/1999

#### Names of Observers:

Frank Leitz Michelle Chapman Wilbert Kim Linton

ELEMENT IDENTIFICATION				
Manufacturer:	Hydranautics			
Element Type:	LFC1X 2540			
Element Location:	Housing #3, 2nd element			
Serial Number:	x03531			
Element Dimensions:	2.5 in. x 40 in.			
Number of Leaves:	2			
Size of Leaves:	91.8cm x 72.4cm Total Area 83.8cm x 62.8cm Active Area of one side (2.1 m² per element or 22.6 ft²)			

#### OPERATING HISTORY

The RO system was operated for six months on site at the McAllen, TX South Waste Water Treatment Plant. Screened de-gritted sewage was first treated in a Zenogem bioreactor/microfiltration system, then chlorine and ammonia was added and the Zenogem effluent was forwarded to the RO system. The RO element array was a 2x2x1x1 and had 3 elements per vessel for a total of 18 elements in the system. RO recovery rates were set from 50% to 80% of 15.2 L/min feed flow.

Sulfuric acid and antiscalent were added to prevent scaling. However, due to changes in the chemical character of the Zenogem effluent, or excessive gas formation in the acid tank which caused the acid feed pump to loose it's prime, the pH was not controlled well at all times. This resulted in a loss of permeate flow from the last vessel.

Also, traditional constituents used in an RO projection do not include phosphorous compounds. The researchers involved in this project began to suspect that phosphorous salts were the cause of excessive scale problems due to the nature of waste water treatment. Attempts at adjusting the pH to control phosphorous salts included running a projection with non-RO software to determine the potential for phosphate scaling. A range of pH settings and two control points for pH were tested in an attempt to control the scaling problems. The pH ranges tested were from 5.5 to 7 on the feed, and 5.5 to 6 on the concentrate. The lower pH control ranges were in response to this non-RO projected information.

Scaling also caused operators to clean the system approximately 4 times with a low pH solution at a pH of about 3. A high pH solution was not used to clean the membranes as there was no indication of biofouling and the system's performance was recovered using the acid cleanings.

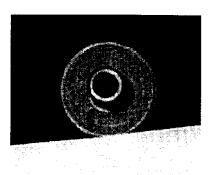
#### DESCRIPTION OF EVENTS LEADING TO AUTOPSY

Subject element was the second element in housing #3, one of two vessels that received flow first. Permeate recovery flow from this vessel varied from 2.8 L/min to 2.3 L/min. This element was subject to two holes punctured with a hypodermic needle. The fouling on the membrane was a result of turning off the acid feed pump for approximately 8 hours.

This autopsy was primarily done to determine the size and extent of damage resulting from the hypodermic needle. In addition, the general nature of the membrane and scaling composition is of interest.

#### NARRATIVE DESCRIPTION OF AUTOPSY PROCEDURE

Fiberglass wrapping was cut open and peeled or pried off. Sample #1 is the fiberglass with the 2 holes marked.
Anti-telescoping devices were removed.
Photographed the feed end of the element.



X03531

Tape wrap was unwound.

Measured the total area and active area of one side of one leaf. Applied congo red dye to the first leaf. Photograph of the dye stained membrane.



Sample #2 is a cutting from the leaf with the 2 holes in the glue line.

#### **OBSERVATIONS**

There were no cracks in this element fiberglass casing.

Two needle holes were visible in the fiberglass and tape wrap at a distance of 17.75 cm (~7 in) from the reject end.

The membrane was wound backwards - which probably makes no difference in performance, but does make autopsy confusing.

There were little black flecks on the membrane surface.

Glue lines were all solid.

Dye test showed no pin hole damage. There were only 2 holes in the glue line, neither of which extended through the hard, thick glue.

Test and Test Objective: Chemical analysis of fouling material on leaf 1

Organization Performing Test: USBR Chemistry Lab

Date: Submitted November 1, 1999

#### Observations from Test:

The analysis methods used for TDS, TSS, SO4, and Cl do not used acid to digest the samples. The method used for SO4 and Cl was EPA method 300.0A, ion chromatography. The other metals, except for phosphorous were digested with nitric acid and analyzed using the ICP (inductively coupled plasma) EPA method 30.15. Phosphorous is also digested, but under EPA method 365.1.

The results from both housing #3 and #6 are shown for comparison.

Analytes	Housing #3	Equivalent	Equivalent	Housing #6	Anions =>	Cations =>
-	concentration	Anions =>	Cations =>	concentration	Ox. State *	Ox. State *
	(mg/L)	Ox. State *	Ox. State *	(mg/L)	Conc. / At.	Conc. / At.
		Conc. / At.	Conc. / At.		Wt.	Wt.
		Wt.	Wt.			
Total P	36.69	-3.6		135.2	-13.1	
Al	2.52		0.3	9.1		1.0
Ba	7.02		0.1	20.8		0.3
Fe	1.1		0.1	3.8		0.2
Ca	76.5		3.8	298.0		14.9
K	2.7		0.1	4.8		0.1
Mg	4.07		0.3	13.4		1.1
Na	21.3		0.9	38.0		1.7
Si	2.46		0.4	7.4		1.1
SO4	15.7	-0.3		20.6	-0.4	
CI	21.6	-0.6		33.7	-1.0	
Totals		-4.5	5.9		-14.5	20.3

#### DISCUSSION AND CONCLUSIONS

The holes did not penetrate through the heavy glue line into the permeable membrane surface.

The solids precipitated onto the membrane surface originally come from a saturated solution. When the autopsy is done, de-ionized water is used to rinse the scrapings from the surface of the membrane. Since the samples are scraped from the membrane using DI water, the concentration expressed as a value in milligrams per liter is not meaningful as a concentration unless it is expressed in equivalents.

When the concentrations are interpreted as equivalents, it can then be shown in both housing #3 and housing #6 that there are roughly the same number of equivalents of calcium and phosphorous in each housing. This indicates that the predominant form of what was left on the membrane was most likely calcium phosphate (hydroxy apetite). Housing #6 had a larger amount than housing #3 resulting in the flow almost ceasing in housing #6.

When dye was applied to the element from the 6th housing, it did not adhere. That membrane element was the second membrane from the end of The membrane in the 3rd housing at the front end of the the system. system absorbed the dye indicating damage to the membrane surface. One possible reason why is that the acid solution was stronger at the front end of the system, especially if there was a problem with the chemical feed system and the pH dropped towards 2. Another possible explanation is the phosphate scale acted as a buffer to protect the membrane surface from the sulfuric acid in the end of the system. Phosphoric acid is a weaker acid than sulfuric. Using the 1st ionization constants, phosphoric acid would be a pH of about 3, and sulfuric is less than 2. Using the second ionization constant, phosphoric acid would be a pH of about 8, and sulfuric would still be about 2. As the water became more saturated with calcium phosphorous, the sulfuric acid became buffered significantly.

#### SPIRAL WOUND MEMBRANE ELEMENT AUTOPSY

#### PURPOSE AND LOCATION OF AUTOPSY

Purpose of Autopsy: McAllen, TX Wastewater Reclamation Project: Determination of scaling in end element.

Date and Place: October 29, 1999, USBR WTER Pilot Plant Lab, Denver, CO.

Date of This Report: 12/30/1999

#### Names of Observers:

Frank Leitz Michelle Chapman Wilbert Kim Linton

ELEMENT IDENTIFICATION				
Manufacturer:	Hydranautics			
Element Type:	LFC1X 2540			
Element Location:	Housing #6, final element			
Serial Number:	X03536			
Element Dimensions:	2.5 in. x 40 in.			
Number of Leaves:	2			
Size of Leaves:	92.1cm x 72.7cm Total Area 82.6cm x 62.2cm Active Area per side (2 m² per element or 22.1 ft²)			
OPERATING HISTORY				

The RO system was operated for six months on site at the McAllen,TX South Waste Water Treatment Plant. Screened de-gritted sewage was first treated in a Zenogem bioreactor/microfiltration system, then chlorine and ammonia was added and the Zenogem effluent was forwarded to the RO system. The RO element array was a 2x2x1x1 and had 3 elements per vessel for a total of 18 elements in the system. RO recovery rates were set from 50% to 80% of 15.2 L/min feed flow.

Sulfuric acid and antiscalent were added to prevent scaling. However, due to changes in the chemical character of the Zenogem effluent, or excessive gas formation in the acid tank which caused the acid feed pump to loose it's prime, the pH was not controlled well at all times. This resulted in a loss of permeate flow from the last vessel.

Also, traditional constituents used in an RO projection do not include phosphorous compounds. The researchers involved in this project began to suspect that phosphorous salts were the cause of excessive scale problems due to the nature of waste water treatment. Attempts at adjusting the pH to control phosphorous salts included running a projection with non-RO software to determine the potential for phosphate scaling. A range of pH settings and two control points for pH were tested in an attempt to control the scaling problems. The pH ranges tested were from 5.5 to 7 on the feed, and 5.5 to 6 on the concentrate. The lower pH control ranges were in response to this non-RO projected information.

Scaling also caused operators to clean the system approximately 4 times with a low pH solution at a pH of about 3. A high pH solution was not used to clean the membranes as there was no indication of biofouling and the system's performance was recovered using the acid cleanings.

#### DESCRIPTION OF EVENTS LEADING TO AUTOPSY

Subject element was the last element of the last vessel (vessel #6). Permeate recovery flow from the last vessel varied from 1.4 L/min to 0.01 L/min. This fouling was a result of turning off the acid feed pump for approximately 8 hours.

This autopsy was primarily done to determine if phosphate salts were of primary concern, or not. In addition, the general nature of the scaling composition is of interest.

#### NARRATIVE DESCRIPTION OF AUTOPSY PROCEDURE

The membrane was inspected during the autopsy at every step. First, the fiberglass wrapping was cut open using an air-powered cast saw set to cut at a shallow depth. The wrapping was then peeled or pried off. Anti-telescoping devices were removed from both ends of the membrane. Finally, the tape wrap was removed.

A squeegee was used to wipe both sides of the first leaf. DI water was used to liquefy the fouling substance. The material was collected in a sample jar labeled as Sample 1.

Researchers then applied a strong red red dye, congo red, to the second leaf.

Samples were cut from the feed and reject ends of the second leaf for SEM analysis with DI water added to the baggie to keep the membrane supple. Feed side is Sample 2 and the reject side is Sample #3.

The material was collected from the first leaf was funneled into a sample jar labeled as Sample #4.



#### **OBSERVATIONS**

The scrapings from the first element were a brownish pink color. The pink may be dye. No visible scaling was apparent.

Dye test on the second leaf with congo red was negative indicating no structural damage or biofouling on the membrane surface. Dye will highlight biofouling as the dye adheres to a surface ripe with organisms.



Test and Test Objective: Chemical analysis of fouling material on leaf 1

Organization Performing Test: USBR Chemistry Lab

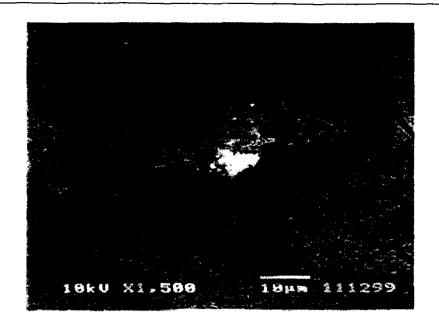
Date: Submitted November 1, 1999

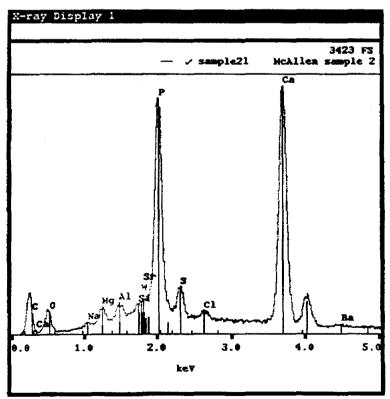
#### Test Results

Analytes	Housing #3	Equivalent	Equivalent	Housing #6	Anions =>	Cations =>
,a.y.cc	concentration	. •	•	concentration	Ox. State *	Ox. State *
	(mg/L)	Ox. State *	Ox. State *	(mg/L)	Conc. / At.	Conc. / At.
	, -	Conc. / At.	Conc. / At.		Wt.	Wt.
		Wt.	Wt.			
Total P	36.69	-3.6		135.2	-13.1	
Al	2.52		0.3	9.1		1.0
Ва	7.02		0.1	20.8		0.3
Fe	1.1		0.1	3.8		0.2
Ca	76.5		3.8	298.0		14.9
K	2.7		0.1	4.8		0.1
Mg	4.07		0.3	13.4		1.1
Na	21.3		0.9	38.0		1.7
Si	2.46		0.4	7.4		1.1
SO4	15.7	-0.3		20.6	-0.4	
CI	21.6	-0.6		33.7	-1.0	
Totals		-4.5	5.9		-14.5	20.3

#### Observations from Test:

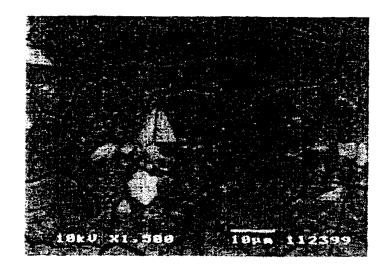
The analysis methods used for TDS, TSS, SO4, and Cl do not used acid to digest the samples. The method used for SO4 and Cl was EPA method 300.0A, ion chromatography. The other metals, except for phosphorous were digested with nitric acid and analyzed using the ICP (inductively coupled plasma) EPA method 30.15. Phosphorous is also digested, but under EPA method 365.1.

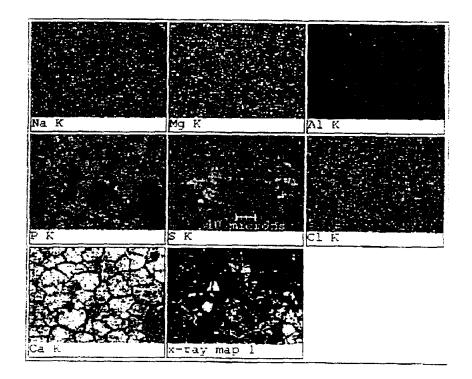




Test and Test Objective: SEM/Elemental Analysis of membrane samples from the second leaf to determine the nature of the scalant for element number X03536.

Organization Performing Test: USBR Date: Submitted November 1, 1999





SEM Distribution map of sampled elements for membrane # X03536

#### DISCUSSION AND CONCLUSIONS

#### SEM Test:

The X-ray display peaks should be interpreted as a qualitative analysis, not a quantative one. This analysis captures the energy spikes from the entire picture, not just the particle in the middle. The sample was hit with 10 kV of energy and magnified 3,500 times. Certainly, phosphorous and calcium are prevalent peaks. Barium and sulfur also show strong peaks on other samples not shown as part of this report because they are redundant to the information captured in the body of this report.

Although no visible scaling was apparent to the naked eye, this analysis clearly shows a fine silt-like layer covers the surface of the membrane. It appears from the distribution map that there is an even covering of these elements across the face of the membrane. The particle in the middle does not seem to be of a different character as compared to the rest of the scale layer.

#### Chemical Analysis of Scraping:

The solids precipitated onto the membrane surface originally come from a saturated solution. When the autopsy is done, de-ionized water is used to rinse the scrapings from the surface of the membrane. Since the samples are scraped from the membrane using DI water, the concentration expressed as a value in milligrams per liter is not meaningful as a concentration unless it is expressed in equivalents.

Using equivalents, it can then be shown in both housing #3 and housing #6 that there are roughly the same number of equivalents of calcium and phosphorous in each housing. This indicates that the predominant form of what was left on the membrane was most likely calcium phosphate (hydroxy apetite). Housing #6 had a larger amount than housing #3 resulting in the flow almost ceasing in housing #6.



The enclosed materials are considered proprietary property of ZENON Environmental Inc. No assignments either implied or expressed, of intellectual property rights, data, know how, trade secrets or licenses of use thereof are given. All information is provided exclusively to the addressee for the purposes of evaluation and is not to be reproduced or divulged to other parties, nor used for manufacture or other means or authorize any of the above, without the express written consent of ZENON Environmental Inc. The acceptance of this document will be construed as an acceptance of the foregoing conditions.

# **ZeeWeed® Tertiary Treatment System**

# BUDGET PROPOSAL for a ZeeWeed® Membrane Filtration Tertiary Filtration Treatment System for the City of McAllen, Texas Proposal Number #374-98 Rev. 2.0

Submitted to:

CH2M Hill 1620 W. Fountain Head Pkwy. #550 Tempe, AZ 85282

**Attention:** 

Jim Lozier / Fair Miller

Submitted by:

ZENON Environmental Systems – Municipal Division 845 Harrington Court Burlington, Ontario L7N 3P3

**December 7, 1999** 

Copyright[©] ZENON Environmental Systems 1999

### **Table of Contents**

1.0	COMMERCIAL INFORMATION	3
1.1 1.2 1.3	PRICING SUMMARY  STANDARD TERMS AND CONDITIONS  ZENON STANDARD TERMS AND CONDITIONS	3
2.0	SYNOPSIS OF THE ZEEWEED® TERTIARY TREATMENT PROCESS	8
3.0	FEATURES & BENEFITS OF THE ZEEWEED® SYSTEM	9
4.0	ZEEWEED® TERTIARY TREATMENT PLANT	. 12
5.0	MAJOR EQUIPMENT	. 14
6.0	ATTACHMENTS	. 16

#### 1.0 COMMERCIAL INFORMATION

#### 1.1 Pricing Summary

The budget pricing to supply equipment and services as described in this proposal is as follows:

ZeeWeed® Membrane Tertiary Treatment System including membranes, permeate pumps, membrane air scour blowers, instruments and control system & equipment F.O.B. McAllen, Texas.

Four (4) Train ZeeWeed® Membrane Tertiary Treatment System to treat a maximum daily hydraulic capacity of 8.5 MGD.

Process equipment will be supplied loose, i.e. not on skids, for installation by others.

**Fixed Capacity Flow** 

8.5 MGD

**Budgetary System Price** 

US \$5,075,000.00

#### Validity

Pricing is for budgetary purposes only and does not constitute a final offer of sale.

#### **Taxes and Duties**

No taxes or duties or brokerage are included in the above pricing. Any taxes, duties, tariffs of any type are for the account of the Purchaser.

#### **Field Service**

The equipment pricing above includes Field Service from ZENON Technicians for assistance with the equipment installation, commissioning, operator training and process start-up assistance.

Any additional days of Field Service required will be at ZENON's Standard per diem rate of US\$650 per day plus living and travelling expenses.

#### **Terms of Payment**

The budgetary pricing quoted in this proposal is based on the following payment terms

- 15% with Purchase Order
- 25% on submission of General Arrangement Drawings

- 50% on shipment of equipment or notification that equipment is ready to ship (partial shipments permitted)
- 10% within 30 days of equipment start up or within 60 days of equipment shipment whichever is sooner.

#### Performance & Maintenance Bonds

The cost of providing performance or maintenance bonds is not included. If required these will be at additional cost.

#### **Equipment Shipment and Delivery**

A typical drawing submission and equipment shipment schedule is indicated below. Drawing submission milestones and equipment shipment periods are quoted from the date of acceptance of a formal signed Purchase Order:

Submission of GA Drawings:

8 to 10 weeks from acceptance of P.O

Drawing Approval:

3 weeks from submission of drawings 24 to 26 weeks from acceptance of P.O.

Equipment Shipment:

2 weeks after shipment of equipment to site

Plant Operation Manuals: Operator Training:

When preferred by Customer but no later than

2 weeks prior to the scheduled plant start-up

The above estimated delivery schedule is presented based on current workload backlogs and production capacity. If a formal purchase order is not received within the period of validity of this proposal, the delivery schedule is subject to review and adjustment.

The estimated delivery period quoted is presented based on review <u>and approval</u> of equipment shop drawings within a two (2) week period. Any delay in approval of shop drawings may affect the proposed shipment schedule.

#### **Quality Basis**

For the purposes of establishing a quality basis for equipment supply, reference is made herein to particular equipment manufactured by certain suppliers. The term "or equal" where used herein shall be deemed to mean "ZENON Approved Equivalent". ZENON reserves the right to substitute equipment that ZENON considers to be of equal quality and suitability for the intended application from alternative suppliers to those named herein. With regard to determining the suitability or otherwise of any particular manufacturer's equipment for inclusion as part of the ZeeWeed® system, ZENON's decision shall be final.

#### 1.2 Standard Terms and Conditions

ZENON's Standard Terms and Conditions apply.

#### 1.3 ZENON STANDARD TERMS AND CONDITIONS

Seller desires to provide its Customers with prompt and efficient service. However, to negotiate individually the Terms and Conditions of each Sales contract would substantially impair Seller's ability to provide such service. Accordingly, Products and Services furnished by Seller are sold only on the Terms and Conditions stated herein. Notwithstanding any terms or conditions on Customer's order. Seller's performance of any contract is expressly made conditional on Customer's agreement to Seller's Terms and Conditions of Sale unless otherwise specially agreed to in writing by Seller. In the absence of such agreement, commencement of performance and/or shipment shall be for Customer's convenience only and shall not be deemed or construed to be acceptance of Customer's Terms and Conditions, or any of them. If a contract is not earlier formed by mutual agreement in writing, acceptance of any Product or Service shall be deemed acceptance of the Terms and Conditions stated herein. All contracts for the Sale of Products shall be construed under and governed by the law of the location of Seller's plant at Burlington, Ontario, Canada.

#### **QUOTATION AND PRICES**

All quotations are subject to the Terms and Conditions stated herein as well as any additional Terms and Conditions that may appear on the face hereof. In the case of a conflict between the Terms and Conditions stated herein and those appearing on the face hereof, the latter shall control. Seller's prices and quotations are subject to the following:

- a) All published prices are subject to change without notice.
- b) UNLESS OTHERWISE SPECIFIED IN WRITING, ALL QUOTATIONS EXPIRE THIRTY (30) DAYS AFTER DATE THEREOF, MAY BE TERMINATED EARLIER BY NOTICE AND CONSTITUTE ONLY SOLICITATIONS FOR OFFER TO PURCHASE; further, budgetary quotations and estimates are for preliminary information only and shall neither constitute offers, nor impose any obligation or liability upon Seller.
- c) Unless otherwise stated in writing by Seller, all prices quoted shall be exclusive of transportation, insurance, taxes (including, without limitation, any sales, use, or similar tax, and any tax levied on or assessed to Seller after Product shipment by reason of Seller's retention of a security interest as provided herein), license fees, customs fees, duties and other charges related thereto and Customer shall report and pay any and all such shipping charges, premiums, taxes, fees, duties and other charges related thereto, and shall hold Seller harmless therefrom, provided that, if Seller, in its sole discretion, chooses to make any such payment, Customer shall reimburse Seller in full upon demand.
- d) Stenographic, typographical and clerical errors are subject to correction.
- e) Prices quoted are for Products only and do not include technical data, proprietary right of any kind, patent rights, qualification, environmental or other than Seller's standard tests and other than Seller's normal domestic commercial packaging unless expressly agreed to in writing by Seller.
- f) Published weights and dimensions are approximate only. Certified dimension drawings can be obtained upon request. Manuals, drawings or other documentation required hereupon must be referenced specifically.

This is merely a quotation, and the technology disclosed herein may be covered by one or more ZENON Environmental Inc. (ZENON) patents or patent applications. Any disclosure in this offer does not hereby grant, and nothing contained in the offer shall obligate ZENON to grant, an option to obtain a license to any technology or any other rights under any patent now or hereafter owned or controlled by ZENON.

#### TERMS OF PAYMENT

Unless credit is granted or otherwise specified in writing, payment is due upon shipment. All payments on approved credit accounts

shall be due in full thirty (30) days from date of invoice. Past due balances shall be subject to a service charge of 1-1/2% per month (18% per annum), but not more than the amounts allowed by law. Partial shipments will be billed as made and payments therefor are subject to the above terms. Payment shall not be withheld for delay in delivery of required documentation unless a separate price is stated therefor, and then only to the extent of the price stated for such undelivered documentation. Seller may cancel or delay delivery of Products in the event Customer fails to make prompt payment therefor, or in the event of an arrearage in Customer's account with Seller. Seller hereby retains a security interest in the Products finished until Customer has made payment in full in accordance with the terms hereof. Customer shall cooperate fully with Seller to execute such documents and to accomplish such filings and/or recordings thereof as Seller may deem necessary for the protection of Seller's interest in the Products furnished.

#### TRANSPORTATION AND RISK OF LOSS

Transportation will normally follow Customer's shipping instructions, but Seller reserves the right to ship Products freight collect and to select the means of transportation and routing when Customer's instructions are deemed unsuitable. Unless otherwise advised, Seller may insure to full value of the Products or declare full value thereof to the transportation company at the time of shipment and all freight and insurance costs shall be for Customer's account. Risk of loss and/or damage shall pass to Customer at the FOB point, which shall be the point of manufacture or such other place as Seller shall specify in writing, notwithstanding installation by or under supervision of Seller. Confiscation or destruction of, or damage to, Products shall not release, reduce or in any way affect the liability of Customer therefor. All Products must be inspected upon receipt and claims should be filed with the transportation company when there is evidence of shipping damage, either concealed or external. Notwithstanding any defect or nonconformity, or any other matter, risk or loss and/or damage shall remain with the Customer until the Products are returned at Customer's expense to such place as Seller may designate in writing. Customer, at its expense, shall fully insure Products against all loss and/or damage until Seller has been paid in full therefor, or the Products have been returned, for whatever reason, to Seller.

#### PERFORMANCE

Seller will make all reasonable effort to observe its dates indicated for performance. However, Seller shall not be liable in any way because of any delay in performance hereupon due to unforeseen circumstances or to causes beyond its control, including, without limitation, strike, lockout, riot, war, fire, act of God, accident, failure or breakdown of components necessary to order completion, subcontractor, supplier or customer caused delays, inability to obtain or substantial rises in the price of labour, materials or manufacturing facilities, curtailment of, or failure to obtain sufficient, electrical or other energy supplies, or compliance with any law, regulation or order, whether valid or invalid of any cognizant governmental body or any instrument thereof whether now existing or hereafter created. Performance shall be deemed suspended during, and extended for, such time as any such circumstances or causes delay its execution. Whenever such circumstances or causes are remedied, Seller will make, and Customer shall accept, performances hereupon. In addition, Seller's inventories and current production must be allocated so as to comply with applicable Government regulations. In the absence of such regulations, Seller reserves the right, in its sole discretion, to allocate inventories and current production and substitute suitable materials when, in its opinion, such allocation or substitution is necessary due to such circumstances or causes. No penalty clause of any kind shall be effective. As used herein, "performance" shall include, without limitations, fabrication, shipment, delivery, assembly, installation, testing, and warranty repair or replacement as applicable.

#### **ACCEPTANCE**

The furnishing by Seller of a Product to the Customer shall constitute acceptance of that Product by Customer, unless notice of defect or nonconformity is received by Seller within thirty (30) days of receipt of the Product at Customer's designated receiving address; provided that, for Product for which Seller agrees in writing to perform acceptance testing after installation, the completion of Seller's applicable acceptance tests, or execution of Seller's acceptance form

by Customer, shall constitute acceptance of the Product by Customer. Notwithstanding the foregoing, any use of a Product by Customer, its agents, employees, contractors or licensees for any purpose, after receipt thereof, shall constitute acceptance of that Product by Customer. Seller may repair or, at its option, replace defective or non-conforming parts after receipt of notice of defect or nonconformity.

#### ASSIGNMENTS AND TERMINATIONS

Any assignment by Customer of any contract hereupon without the express written consent of Seller is void. No order may be terminated by Customer except by mutual agreement in writing. Terminations by mutual agreement are subject to the following

- Customer will pay, at applicable contract prices, for all Products which are completely manufactured and allocable to Customer at the time of Seller's receipt of notice of termination.
- Customer will pay all costs, direct and indirect, which have been incurred by Seller with regard to Products which have not been completely manufactured at the time of Seller's receipt of notice of termination.
- Customer will pay a termination charge on all other determined costs and other charges. To reduce termination charges, Seller will divert completed parts, material or work-in-process from terminated contracts to other Customer's whenever, in Seller's sole discretion, it is practicable to do so.

#### PATENTS AND OTHER INDUSTRIAL PROPERTY RIGHTS

Seller will hold Customer harmless, as set forth herein, in respect to any claim that the design or manufacture of any Product in Seller's commercial line of Products, or manufactured to specifications set by Seller and furnished herein, constitutes an infringement of any by Seller and furnished herein, constitutes an infringement of any patent or other industrial property rights of the United States or Canada. Seller will pay all damages and costs, either awarded in a suit or paid, in Seller's sole discretion, by way of settlement, which are based on such claim of infringement, provided that Seller is notified promptly in writing of such claim of infringement but there is no liability whatsoever herein with respect to any claims settled by Customer without Seller's prior written consent. In the event that Seller is required to hold Customer harmless hereupon, Seller will, in its sole discretion and at its own expense, either procure for in its sole discretion and at its own expense, either procure for Customer the right to continue using said Product, replace it with a on-infringing product, or remove it and refund an equitable portion of the selling price and transportation costs thereof. THIS SHALL CONSTITUTE SELLER'S ENTIRE LIABILITY FOR ANY CLAIM BASED UPON OR RELATED TO ANY ALLEGED INFRINGEMENT OF ANY PATENT OR OTHER INDUSTRIAL RIGHTS. Customer shall hold Seller harmless grainst any expense loss goes or damages resulting from claimed against any expense, loss, costs or damages resulting from claimed against any expense, loss, costs or damages resulting from claimed infringement of patents, trademarks, or other industrial property rights arising out of compliance by Seller with Customer's designs, specifications, or instructions. SELLER DISCLAIMS LIABILITY FOR U.S. OR CANADIAN PATENT OR COPYRIGHT INFRINGEMENT ARISING FROM USE OR MANUFACTURE BY ANYONE OF INVENTIONS IN CONNECTION WITH PRODUCTS OR SERVICES SOLD, USED, OR INTENDED FOR SALE OR USE, IN PERFORMING CONTRACTS WITH THE UNITED STATES OR CANADA. OR CANADA.

#### WARRANTY

Unless otherwise agreed to in writing, Seller warrants its Products to be free from defects in material or workmanship for a period of 12 months from the shipment of Product by Seller, provided that such Product are used, cleaned and maintained in accordance with the Seller's instructions. This warranty does not apply to normally replaceable parts or components such as

- filter cartridges, pump seals, membranes etc., (see below for membrane warranties)
- Customer undertakes to give immediate notice to Seller if goods or performance appear defective and to provide Seller with reasonable opportunity to make inspections and tests. If Seller is not at fault. Customer shall pay Seller the costs and expenses of the inspections and tests.
- 3. Seller's obligations under this warranty is limited to the repair or replacement at its factory, or any device or part thereof which shall prove to have been thus defective. If Customer asks Seller to replace defective parts at Customer's premises, Customer agrees to pay for any traveling time and expenses, plus the Seller's labour to complete the replacement/repair.
- Goods shall not be returned to Seller without Seller's permission. Seller will provide Customer with a "Return Material Seller will provide Customer with a "Return Material Authorization" number to use for returned goods. All returns are F.O.B. - Burlington, Ontario, Canada.
- 5. Warranty on the membranes applies only if the membrane element(s) has been operated and cleaned according to Seller's instructions. When either permeate or concentrate flow drops by 10% from the original rates at the same operating conditions, cleaning must be initiated or the warranty will be null and void. Elements must be clean and be kept moist. They should be shipped to Seller in water-tight bags and must be protected from freezing. WARNING – if element conditions of use given in Seller's instructions are not followed, the warranty will be null and void.

IMPLIED WARRANTIES, INCLUDING, BUT NOT LIMITED TO, WARRANTIES OF FITNESS FOR PARTICULAR PURPOSE, USE, OR APPLICATION, AND ALL OTHER OBLIGATIONS OR LIABILITIES ON THE PART OF THE SELLER, UNLESS SUCH OTHER WARRANTIES, OBLIGATIONS OR LIABILITIES ARE EXPRESSLY AGREED TO IN WRITING BY SELLER, ARE NULL AND VOID.

#### DAMAGES AND LIABILITY

SELLER'S LIABILITY FOR DAMAGES SHALL NOT EXCEED THE PAYMENT, IF ANY, RECEIVED BY SELLER FOR THE UNIT OF PRODUCT OR SERVICE FURNISHED OR TO BE FURNISHED, AS THE CASE MAY BE, WHICH IS THE SUBJECT OF CLAIM OR DISPUTE. IN NO EVENT WILL SELLER BE LIABLE FOR INCIDENTAL, CONSEQUENTIAL OR SPECIAL DAMAGES, OF ANY KIND, HOWEVER CAUSED, ARISING OUT OF, OR IN ANY WAY CONNECTED WITH, THE PRODUCTS FURNISHED BY SELLER TO CUSTOMER.

#### **DISPUTES**

All disputes under any contract concerning Products not otherwise resolved between Seller and Customer shall be resolved in a court of competent jurisdiction for the location of Seller's plant at Burlington, Ontario, Canada, and no other place. Provided that, in Seller's sole discretion, such action may be heard in some other place designated by Seller, if necessary to acquire jurisdiction over third persons, so that the dispute can be resolved in one action. Customer hereby consents to the jurisdiction of such court or courts and agrees to appear in any such action upon written notice thereof. No action, regardless of form arising out of, or in any way connected with, the Products or Services furnished by Seller, may be brought by Customer more than one (1) year after the cause of action has occurred. If any part, provision or clause of the Terms and Conditions of Sale, or the application thereof to any person or circumstances, is held invalid, void or unenforceable, such holding shall not affect and shall leave valid all other parts, provisions, clauses or applications of the Terms and Conditions remaining, and to this end the Terms and Conditions shall be treated as severable.

# 2.0 SYNOPSIS OF THE ZEEWEED® TERTIARY TREATMENT PROCESS

ZeeWeed[®] ultrafiltration system is a proprietary ZENON process technology that produces high quality treated water by drawing raw water through immersed ZeeWeed[®] membrane modules. ZeeWeed[®] "Outside-In", hollow-fibre membranes are manufactured ultrafiltration (UF) pore size. The ZeeWeed[®] UF Membranes have an absolute pore size of 0.1 microns and thus ensure removal of particulate matter greater than 0.1 microns in size such as most particulate matter, including bacteria, solids, Giardia cysts and Cryptosporidium oocysts, cannot enter the treated effluent stream. The ZeeWeed[®] Membrane ensures removal of a large percentage of impurities. The ZeeWeed membranes produce a high quality effluent, optimal for post-treatment by reverse osmosis.

The membranes operate under a slight vacuum created within the hollow membrane fibres by a permeate pump. Treated water is drawn through the membranes, enters the hollow fibres and is pumped out to the treated water storage tank (or distribution system). Air flow is introduced at the bottom of the membrane modules to create turbulence which scrubs and cleans the outside of the membrane fibres allowing them to operate at a high flux. The aeration also oxidizes iron and organic compounds, resulting in a treated water quality that is better than that provided by ultrafiltration alone.

ZeeWeed® membranes are immersed and therefore can tolerate high levels of solids. This is a main advantage when used as a tertiary treatment plant, since the ZeeWeed plant continues to operate well even when the upstream clarifier is upset and rejects solids to the UF. The capacity to handle solids also means that there is no need to pre-treat the clarified effluent, avoiding therefore the costs of sand filters or cartridge filters often required by other membrane technologies.

ZeeWeed[®] membranes have the additional benefit of being chlorine resistant up to concentrations of 1,000 mg/L. Therefore, influent water can be pre-chlorinated or the membranes can be easily cleaned, even when heavy fouling occurred.

The ZeeWeed® Membrane Technology process consistently produces high quality water, as the membranes are not subjected to stress, pressurization or rapid pressure fluctuations. Membrane cleaning by backpulsing is achieved by reversing the permeate flow and backwashing the fibre's lumen with permeate at low pressure (due to the high permeability of the ZeeWeed® membrane, the backpressure during backpulsing is low). The small variations in operating pressure occur smoothly over relatively long periods so that at no time is the membrane stressed. This, in turn, results in a membrane filtered permeate with the lowest sustainable particle count on the market.

#### 3.0 FEATURES & BENEFITS OF THE ZEEWEED® SYSTEM

#### High Treated Effluent Quality

ZENON's ZeeWeed[®] Membrane Tertiary Treatment System is a cost effective method for membrane filtration removal of solids and is particularly recommended for treatment of the following contaminants in water:

# Feed Water Element Suspended Solids

<u>Treated Water Quality</u> ≥ 6 log removal

Average Turbidity

≤ 0.1 NTU

Particle Counts

Average  $\leq 5/mL$ , size range > 2 microns

Note: The information provided in this section of the proposal is general only and is intended only to indicate what is capable of being achieved with ZeeWeed® Membrane Water Treatment Technology based on consideration of specific raw water qualities and the type of treatment processes utilized.

Since the presence of air is continuous or semi-continuous in the process tank, materials which will readily oxidize, such as iron in its ferrous state, will be micro-precipitated and separated by the membrane, therefore producing a better quality water than if treated by ultrafiltration alone.

#### Advantages of an "Outside-In" Immersed Membrane

#### a) Single Step Treatment

The ZeeWeed[®] membrane is an outside-in membrane where the flow of water is from the outside of the membrane to the inside of the hollow fibre. This means that the inside of the membrane only comes in contact with clean, filtered water. The solids to be removed remain outside of the membrane where they do not cause fouling and plugging.

#### b) Low Energy Requirement.

Being immersed allows ZENON's ZeeWeed[®] Membranes to operate under a slight vacuum instead of under a high positive pressure, as do other membranes on the market. The ZeeWeed[®] Membrane operates under a differential pressure of 5"Hg to 18"Hg (5-20 ft H₂O) vacuum. This operational energy is very low and to ZENON's knowledge is the lowest in the membrane market.

#### c) Ability to Operate in a High Solids Environment

The ZeeWeed® membranes are immersed within the process tank, where suspended solids can exist without interfering with membrane operation. The operating flux rates of ZeeWeed® membrane modules are, for all practical purposes, independent of the solids content and turbidity of the raw water supply. This reflects in its capacity to operate well in a solids environment seen when the clarifiers get upset.

#### d) Stable and Low Particle Counts in the Effluent

The low energy backpulse of an immersed membrane does not produce significant expansion of the membrane pores. Expansion of the membrane pores, which results from high energy air backpulsing of the membranes as utilized in some types of membrane systems, can result in high particle counts immediately following backpulsing. This expansion of the membrane pores may potentially permit the passage of particles of larger sizes through the membranes until the membrane fibre fully relaxed from the expansion induced by the backpulsing process. Such systems cannot reliably use particle counters to verify the membrane integrity.

With the ZeeWeed® Membrane system expansion of the membrane pores is insignificant and the ZeeWeed® process consistently produces high quality treated water, which remains stable at all phases of plant operation.

#### Resistance to Oxidizing Chemicals

The ZeeWeed® membrane is resistant to chlorine and other typical water treatment plant oxidants (such as chlorine dioxide and potassium permanganate) in concentrations as high as 1,000 mg/L. This means that it is possible to pre-chlorinate the water without having to add a de-chlorination step such as Granular Activated Carbon (GAC) or bisulfite injection, which not only requires periodic chemical filling and maintenance, but also adds an unnecessary compound into the water. Where prechlorination is desired, chemical resistance also provides protection against dechlorination equipment failure, which could lead to severe damage of a chlorine sensitive membrane. Finally, chlorine resistance also allows for easy disinfection of the membrane and the plant should this be required.

#### Exceptional Membrane Durability

The ZeeWeed® membrane has been designed to be exceptionally durable and resistant to breakage. To achieve a high level of membrane durability ZENON utilizes a patented internal support on which the membrane is caste. This provides resistance to the membrane and protects it against tearing and breakage without reducing its flux capacity.

#### Simplicity of Operation

The ZeeWeed® process is an easy and inexpensive system to operate both in terms of maintenance costs and personnel requirements. Since treatment is a single stage process, there is no need for coagulants (except for colour and organics removal), clarifiers or sand filters as with some other membrane systems. Instead the plant operators are only required to ensure they maintain proper membrane permeating conditions by maintaining the permeate pumps and blowers in operation.

#### Ruggedness of Operation / Operational Flexibility

The ZeeWeed® Treatment Process consistently produces high quality treated effleunt irrespective of seasonal, operational and weather related variations in the source raw water quality, since the membranes can operate equally well in low or high solids concentrations and at varying temperatures:

without clogging

- without the need for pressurized air backpulsing cycles which consistently stress the membranes and lead to premature failure
- without any detrimental effects on the membrane flux since the ZeeWeed® membrane was developed for environments of high solids concentrations
- without breaking since the hollow fibre membrane is a composite developed to be both highly durable structurally as well as chemically resistant to outside elements

# 4.0 ZEEWEED® TERTIARY TREATMENT PLANT

#### Design Parameters

The table below summarizes the main design parameters on which the proposed ZeeWeed® Tertiary Treatment System has been designed.

Design Flow

Design Flow
Fixed Capcity Flow

Paw Water

Preated Water

Treated Water

Preated Water

Treated Water

8.5 MGD

Note 1: The plant should be able to operate at 95% recovery, however, the recovery equipment has been sized for 90% and the average given above at 90%, is to allow for operations flexibility.

## 4.0 ZEEWEED® TERTIARY TREATMENT PLANT

#### Design Philosophy and Equipment Selection

ZENON proposes to offer a four (4) Process Stream Membrane Treatment Plant with each process train designed to produce a continuous treated water output of 1/4 of the required capacity of the plant. In the event of any type of operational problem or failure with one train the plant will function at 75% of the nominal average day flow design capacity, by adjusting the vacuum applied to the operating membrane modules. Future plant expansion, if and when required, can be achieved by adding additional treatment units.

The equipment proposed is designed for simplicity of operation. All plant operations are automatically controlled via a PLC. There are no normal operations that require manual operation of valves, pump speeds, etc. The system design philosophy is to reduce as far as possible the potential for system problems caused by operator error.

The treatment system proposed by ZENON does not include a chlorine dosing system to add residual chlorine to the treated effluent.

#### CONCRETE, EQUIPMENT LOOSE

The ZeeWeed® Membrane Tertiary Treatment System is designed with major process equipment supplied loose for installation on concrete pads. The ZeeWeed® membranes are supplied for installation in concrete tanks (by others) within Zenon supplied membrane support beams. The membrane air scour blowers are supplied loose for installation within an acoustically insulated blower room to minimize the noise transmission to the rest of the plant. Reject water will flow by gravity to the disposal point. The plant control panel will be supplied loose so that it can be either wall mounted adjacent to the plant or located in a separate control room depending on the Owner's preference.

#### 5.0 MAJOR EQUIPMENT

The list below summarizes the major equipment and the quantities of items included for the ZenoGem® plant design.

SCOPE OF SUPPLY SYNOPSIS			
for the ZeeWeed® Plant			
Item	Size	Units	Quantity
Raw Water Feed			
Raw Influent Feed Pumps			Not Incl.
Inlet & Discharge Isolating Valves			Not Incl.
Discharge Check Valves			Not Incl.
Piping Manifold			Not Incl.
Wet Well Level Switches			Not Incl.
VFD's			Not Incl.
Raw Water Screening			
Raw Influent Screen			Not Incl.
Raw Influent Grinder			Not Incl.
Raw Influent Flowmeter			Not Incl.
Raw Influent Flow Control Flowmeter			Not Incl.
Raw Influent Flow Control Valve			Not Incl.
Membranes/Membrane Cassettes			
Individual Membrane Modules			640
Membrane Cassettes			80
Process Tanks & Frames			
Membrane Support Frames			Incl.
Process Tanks			Not Included
Permeate Collection Headers			4
Air Scour Headers			4
Permeate Pumps			
Permeate Pumps	2,497	USgpm	5
VFD's/Control Valves	50	HP	4
Piping Manifold			Not Incl.
Valves			Incl.
Air Extraction System			
Air Removal Separation Columns			4
Vacuum Pumps	24	scfm	3
Backpulse System			
Backpulse Water Storage Tank	6,480	USg	2
Hypochlorite Storage Tank	106	USg	1
Hypochlorite Feed Pumps	6.9	USgphr	2
Item	Size	Units	Quantity

Air Blowers  Membrane Air Scour Blowers incl. Silencers	5,129	Scfm	3
	3,129	Scim	
Inlet & Discharge Isolation Valves			6
Discharge Check Valves Inlet Control Valves		<del> </del>	3
			Incl.
Chemical Addition System (if required)		<u>-</u> -	<u> </u>
Chemical Storage Tank			Not Incl.
Chemical Feed Pumps			Not Incl.
CIP System		<del> </del>	<del></del>
CIP Chemical Storage Tank			Incl.
CIP Chemical Feed Pump			Incl.
Instruments			
Permeate Flowmeters			4
Permeate Header Pressure Transducers			4
Process Tank Level Transmitters			4
Process Tank Level Switches			16
pH Transmitters			Not Incl.
Turbidimeters			1
Particle Counters			4
Membrane Blower Flow Switches			3
Permeate Pump Pressure Gauges			4
Membrane Air Scour Blower Pressure Gauges			3
Control Panel			
PLC-based Control Panel			1
Back-Up PLC			Not Incl.
Electrical			
MCC Panel			Not Included
Miscellaneous			
Air Compressor			2
Air Drier			1
Monorail for Cassette Removal			Not Incl.
Field Service Allowed			Days
Installation Supervision			5
Mechanical Checkout			5
Operator Training			2
Process Start-Up			3
Commissioning			5
TOTAL MAN-DAYS			20
TOTAL No. TRIPS			3
Freight			
Delivery to Site			Incl.

#### **6.0 ATTACHMENTS**

Plant Power Consumption and Estimated Yearly Operating Cost

Table 9.1.1 Connected Power and Estimated Power Consumption at Average Day Flow

City of McAllen Eff Filtration Rev 2

Average Day Flow 8,500,026 USgpd 32,173 m3/day **Maximum Day Flow** 8,500,026 USgpd 32,173 m3/day

ITEM #	TOTAL QTY	EQUIPMENT DESCRIPTION		# Operating Pumps Blowers etc.	Design Capacity	Discharge Head	Duty Point Efficiency	Equipment Operating BHP	Motor HP	Total Equipment BHP	Total Connected HP	Matar Efficiency %	Equipment kW	Hours / Day Continuous Operation	Energy Cost per year
		Raw Water/Wastewater Screen	n/a							-				24.00	
	4.00	Permeate Pumps	By Zenon	4.00	1,664.32 USgpm	35.00 ft	81.00	18.44	30.00	73.76	120.00	91.40	60.18	22 40	36,901
3	4.00	Backpulse Pumps	r/a	4.00	- USgpm	30.00 ft	31.00	10.44	30.00	75.70	120.00	31.40	00.10	6.40	30,301
- <del>d</del>		Recirculation Pumps	n/a		- USgpm	10.00 ft	55.00		<del> </del>			<u> </u>		24.00	
5		Sludge Wasting Pumps	n/a		- USgpm	30.00 ft	50.00	<del></del>	-					2.00	
-6		Reject Water Pumps	n/a		mapsu -	25.00 ft	55.00	<u> </u>	<del>                                     </del>	<del>                                     </del>		<del></del>	····	24 00	
7	3.00	Membrane Air Scour Blowers	By Zenon	2.00	3,840.00 scfm	4.25 psi	n/a	110.49	200.00	220.97	600 00	94 60	174.19	24 00	114,440
8		Process Air Blowers	n/a		- scim	6.00 psi	n/a			-		-		24.00	
9		Miscellaneous Air Blowers	n/a	-	- sc/m	6.00 psi	n/a	-	·	-	-		-	24.00	
10		Anoxic Zone Mixers	n/a	-			n/a	-	-		-	-	-	24.00	-
11	3.00	Air Separation System Vacuum Pumps	By Zenon	2.00	22.25 acfm	18.00 ins Hg	n/a	2.25	3.00	4.50	9.00	87.50	3.84	24.00	2,520
12	2 00		By Zenon	1.00	0.099 USgpm	50.00 ft	n/a	0.10	0.10	0.10	0.21	100.00	0.08	3 20	7
13	-	CIP Wash Pump	n/a		- USgpm	30.00 ft	55.00	•	-	-		-	-	0.02	
14		CIP Chemical Metering	n/a		USgpm			-			-		-		
15	-	Chemical Feed #1 System #1 - Metering	r/a	-	1.365 USgpm	50.00 ft	n/a	-	0.50	-	-	100.00	-	24.00	-
16	-	Chemical Feed #1 System #2 - Metering	n/a	-	0.101 USgpm	50.00 ft	n/a	-	0.03	-	-	100.00	-	24.00	-
17	-	Chemical Feed #1 System #3 - Metering	n/a	-	0.057 USgpm	50.00 ft	n/a		0.03	-	-	100.00	-	24.00	-
18	-	Chemical Feed #1 System #4 - Metering	n/a		0.101 USgpm	50.00 ft	n/a	-	0.03	-		100.00	-	24.00	
18	2.00	Air Compressors	By Zenon	1.00	52.00 scfm	100.00 psi	n/a	18.75	25.00	18.75	50.00	91.30	15.31	6.00	2,515
19	2.00	Air Driers	By Zenon	1.00	75.00 scfm		n/a	-	-	-		80.00		6.00	-
20	1.00	Controls & Instrumentation	By Zenon								1.34		1.00	24.00	657
21	1.00	Miscellaneous	By Zenon							-	1.34		1.00	24.00	657
			1 -												
		Total Connected Power		*							781.89	HP			
		Total Operating Power								318.09	ВНР		255.59	kW	
		Total Operating Cost				,				······································		······		US\$	157,696

Notes

Energy Costs based on

0.0750 US\$ per kW.hr

Power Consumption of other plant equipment required (raw water feed pumps, high lift pumps etc.) is not included by ZENON

Where operating efficiencies are not known, the equipment operating power is assumed to be 75% of the motor nameplate power rating

The operating hours for the permeate pump are corrected for the downtime during backpulse cycles (and Membrane Pressure Decay Test Cycles if applicable)

Permeate Pump Backpulses every 15 mins for 30 seconds 2,496 USgpm @ 30.00 ft TDH =

24.89 BHP

Motor Efficiencies indicated are typical only. Efficiencies used are usually within 2% of actual when motor is operating within 50-100% of its full load rating

Operation of Air Compressor is assumed to be only 25% of time

Operation of the Sodium Hypochlorite Pumps is intermittent - operation for 25% of time is used for energy calculation

Blower Energy Consumption Estimated as:

6.770 BHP per 1,000 scfm per psig.

The motor sizes in the above table are preliminary only and estimated based on the information available at the time of preparing this proposal. It must be understood that at the time of proposal preparation, final headlosses or pressure drops in piping systems have not been calculated accurately Motor sizes are subject to confirmation (and if necessary adjustment) during final design. Use of the above information for sizing or selection of any ancillary equipment is entirely at the USER's own risk. Whilst the motor sizes indicated above are ZENON's best estimate based on design criteria assumed during preparation of the proposal, ZENON accepts no responsibility for the absolute accuracy of the information contained herein.

Table 9.2.2 Estimated Total Annual Operating Cost
City of McAllen Eff Filtration Rev 2
Average Day Flow 8,500,026 USgpd
Maximum Day Flow 8,500,026 USgpd 32,173 m3/day 32,173 m3/day

lem			Cost per year	
Electrical Equipment - Zenon		Calculated at Average Day Flow	157,696	US\$
Electrical Equipment - Others				US\$
Backpulse Chemicals	Sodium Hypochlorite	Calculated at Average Day Flow	8,232	US\$
CIP Chemical #1	MC-1		3,211	US\$
CIP Chemical #2	Sodium Hypochlorite - 250 mg/L		4,435	U\$\$
CIP Neutralization Chemical #1			175	US\$
CIP Neutralization Chemical #2			117	US\$
Suggested Membrane Accrual			190,905	US\$
Estimated Total Annual Op	erating Cost		364,772	USS

Notes	Backpulse Chemical Consumption		Sodium Hypor	chlorite
	Sodium Hypochlorite Consumption		71.91	Litres per day
	Sodium Hypochlorite Consumption		26,248	Litres per year
	Sodium Hypochlorite Cost	US\$	0.31	per Litre
	oodiani iyyoonioma aaai			P
	CIP Cleaning Chemical #1		MC-1	
	Design Dosage		2,000.00	mg/L
	Solution Concentration		50.00	%
	Specific Gravity		1.240	
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tan	ks)	1,918.24	Litres
	Total Annual Chemical Consumption		1,918.24	Litres
	Chemical Cost	US\$	1.67	per Litre
	Chemical Cost	US\$	2.70	per kg
	CIP Cleaning Chemical #2		Sodium Hypod	chlorite - 250 mg/L
	Design Dosage		250.00	mg/L
	Solution Concentration		10.80	%
	Specific Gravity		1.168	
	Wash Frequency		12.00	times / year
	Chemical Consumption per Wash (all tan	ks)	1,178.52	Litres
	Total Annual Chemical Consumption		14,142.26	Litres
	Chemical Cost	US\$	0.31	per Litre
	CIP Neutralization Chemical #1		Sodium Hydro	xide
	Design Dosage		625.00	mg/L
	Solution Concentration		50.00%	
	Specific Gravity		1.520	
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tan	ks)	489.02	Litres
	Total Annual Chemical Consumption		489.02	Litres
	Chemical Cost	US\$	0.36	per Litre
	Chemical Cost	US\$	0.47	per kg
	CIP Neutralization Chemical #2		Sodium Blauff	ite
	Design Dosage		146.00	mg/L
	Solution Concentration		38.00%	
	Specific Gravity		1.290	
	Wash Frequency		12.00	times / year
	Chemical Consumption per Wash (all tan	ks)	177.11	Litres
	Total Annual Chemical Consumption		2,125.32	Litres
	Chemical Cost	US\$	0.06	per Litre
	Chemical Cost	US\$	0.55	per kg

12/07/1999 : 4:01 PM

The enclosed materials are considered proprietary property of ZENON Environmental Inc. No assignments either implied or expressed, of intellectual property rights, data, know how, trade secrets or licenses of use thereof are given. All information is provided exclusively to the addressee for the purposes of evaluation and is not to be reproduced or divulged to other parties, nor used for manufacture or other means or authorize any of the above, without the express written consent of ZENON Environmental Inc. The acceptance of this document will be construed as an acceptance of the foregoing conditions.

# ZenoGem®/ZeeWeed® BUDGET PROPOSAL for the City of McAllen, Texas Wastewater Treatment Plant

#### **BUDGET PROPOSAL # 374-98 Rev 1**

Submitted to:

CH2M Hill 1620 W. Fountain Head Pkwy. #550 Tempe, AZ 85282

Attention:

Jim Lozier & Fair Miller

Submitted by:

ZENON Environmental Systems – Municipal Division 845 Harrington Court Burlington, Ontario L7N 3P3

**December 7, 1999** 

Copyright® ZENON Environmental Systems

1999

#### **Table of Contents**

1.0	COMMERCIAL INFORMATION	4
1.1 1.2		4 7
2.0	ZENOGEM® PROCESS DESCRIPTION	10
3.0	ZENOGEM® ADVANTAGES	12
	Effluent Quality	12
	Compact Plant	
	Expandability	
	Simple Operation	
	Lower Sludge Yield	
	Process Reliability	13
	Advantages of an "Outside-In" Membrane	13
	Exceptional Membrane Durability	13
4.0	ZENOGEM® PLANT	14
5.0	MAJOR EQUIPMENT	17
6.0	ATTACHMENTS	20
	Plant Power Consumption and Estimated Yearly Operating Cost	20

#### 1.0 COMMERCIAL INFORMATION

#### 1.1 PRICING SUMMARY

The budget pricing to supply equipment and services as described in this proposal is as follows:

One (1) ZenoGem® Membrane Bioreactor Waste Treatment System including membranes, aeration system, pumps, blowers, instruments, control system and equipment, FOB McAllen Texas.

Process equipment will be supplied loose, i.e. not on skids, for installation by others.

**Fixed Capacity Flow** 

8.5 MGD

#### **Budgetary System Price**

US\$ 8,620,000.00

#### Validity

Pricing is for budgetary purposes only and does not constitute a final offer of sale.

#### **Taxes and Duties**

No taxes or duties or brokerage are included in the above pricing. Any taxes, duties, tariffs of any type are for the account of the Purchaser.

#### **Field Service**

The equipment pricing above includes Field Service from ZENON Technicians for assistance with the equipment installation, commissioning, operator training and process start-up assistance.

Any additional days of Field Service required will be at ZENON's Standard per diem rate of US\$650 per day plus living and traveling expenses.

#### **Terms of Payment**

The budgetary pricing quoted in this proposal is based on the following payment terms

- 15% with Purchase Order
- 30% on submission of General Arrangement Drawings
- 50% on shipment of equipment or notification that equipment is ready to ship (partial shipments permitted)
- 5% within 30 days of equipment start up or within 60 days of equipment shipment whichever is sooner.

#### Performance & Maintenance Bonds

The cost of providing performance or maintenance bonds is not included. If required these will be at additional cost.

#### **Equipment Shipment and Delivery**

A typical drawing submission and equipment shipment schedule is indicated below. Drawing submission milestones and equipment shipment periods are quoted from the date of acceptance of a formal signed Purchase Order:

Submission of GA Drawings:

8 to 10 weeks from acceptance of P.O

Drawing Approval:

3 weeks from submission of drawings

Equipment Shipment:

24 to 26 weeks from acceptance of P.O.

Plant Operation Manuals:

2 weeks after shipment of equipment to site When preferred by Customer but no later than

Operator Training:

2 --- also asiants the sale delta delta delta desta desta

2 weeks prior to the scheduled plant start-up

The above delivery schedule is presented based on current workload backlogs and production capacity. If a formal purchase order is not received within the period of validity of this proposal, the delivery schedule is subject to review and adjustment.

The delivery period quoted is presented based on review <u>and approval</u> of equipment shop drawings within a two (2) week period. Any delay in approval of shop drawings may affect the proposed shipment schedule.

#### **Quality Basis**

For the purposes of establishing a quality basis for equipment supply, reference is made herein to particular equipment manufactured by certain suppliers. The term "or equal" where used herein shall be deemed to mean "ZENON Approved Equivalent". ZENON reserves the right to substitute equipment that ZENON considers to be of equal quality and suitability for the intended application from alternative suppliers to those named herein. With regard to determining the suitability or otherwise of any particular manufacturer's equipment for inclusion as part of the ZeeWeed® system, ZENON's decision shall be final.

#### **Definitions**

For the purposes of defining milestone dates for payments, commencement of equipment warranties and turnover of responsibility for the operation of equipment from ZENON to the OWNER, the following definitions apply:

Commissioning

Commissioning of the plant is defined as the date when wastewater first flows through the plant.

Substantial Completion Substantial Completion is defined as the date when the equipment supplied first meets the required treatment quality and quantities as defined in accordance with Performance Warranties. In cases where the equipment supplied is designed for a future plant design capacity it is the responsibility of the Owner to provide wastewater in sufficient quantities for the performance tests within the time frame outlined in section 7.0 (Performance Warranties).

On the date Substantial Completion is achieved:

- Equipment and Process Warranties start. 1.
- 2. Responsibility for the plant operation transfers from ZENON to the OWNER.
- Holdbacks become due and payable. 3.

**OWNER** 

For the purposes of this document the term "OWNER" shall be also deemed to include the OWNER's appointed agents or assigns who will be responsible for the operation of the equipment / plant / treatment facility.

#### **Equipment Drawings, Plans & Specifications**

Unless otherwise specified, ZENON will furnish as part of this order the following types of drawings:

- 1. Process Flow Diagram
- Process and Instrumentation Diagrams 2.
- General Arrangement Drawings showing equipment dimensions and weights required for 3. the equipment foundations (foundations by others), and the utility requirements for the process equipment being furnished by ZENON with the System being supplied.
- Standard sub-vendors dimensional outline drawings for the items of major process 4. equipment (e.g. pumps, blowers, air compressors) which are necessary for the purchaser to complete its engineering and installation.
- 5. Standard sub-vendors equipment cut sheets for the major process equipment and other equipment items (major instruments and system components)
- 6. Electrical Drawings including Single Line Diagrams, Control Panel Layouts and Interconnecting Wiring Diagrams.
- 7. Assembly Drawings including General Equipment Layouts, deemed necessary by ZENON to be required for the Purchaser's field forces to erect the equipment.

#### Flow Definitions

For the purposes of defining membrane plant capacity after flow equalization, the following definitions shall apply:

Average daily flow. The average flowrate occurring over a 24-hour period based on total annual flowrate data.

<u>Maximum daily flow</u>. The maximum flowrate that occurs over a 24-hour period based on annual operating data.

<u>Maximum daily four hour flow</u>. The maximum sustained flowrate that occurs over a 4-hour period based on annual operating data.

<u>Peak hourly flow</u>. The peak sustained hourly flowrate occurring during a 24-hour period based on annual operating data.

<u>Minimum daily flow</u>. The minimum flowrate that occurs over a 24-hour period based on annual operating data.

<u>Minimum hourly flow.</u> The minimum sustained hourly flowrate occurring over a 24-hour period based on annual operating data.

<u>Sustained flow.</u> The flowrate value sustained or exceeded for a specified number of consecutive days based on annual operating data.

<u>Maximum monthly average flow</u>. This is the flow that is obtained by taking the month with the highest total flow and dividing by the number of days in that month. It provides information on the highest average flow that can be sustained for a one month period.

#### 1.2 STANDARD TERMS AND CONDITIONS

ZENON's Standard Terms and Conditions apply.

#### ZENON STANDARD TERMS AND CONDITIONS

Seller desires to provide its Customers with prompt and efficient service. However, to negotiate individually the Terms and Conditions of each Sales contract would substantially impair Seller's ability to provide such service. Accordingly, Products and Services furnished by Seller are sold only on the Terms and Conditions stated herein. Notwithstanding any terms or conditions on Customer's order, Seller's performance of any contract is expressly made conditional on Customer's agreement to Seller's Terms and Conditions of Sale unless otherwise specially agreed to in writing by Seller. In the absence of such agreement, commencement of performance and/or shipment shall be for Customer's convenience only and shall not be deemed or construed to be acceptance of Customer's Terms and Conditions, or any of them. If a contract is not earlier formed by mutual agreement in writing, acceptance of any Product or Service shall be deemed acceptance of the Terms and Conditions stated herein. All contracts for the Sale of Products shall be construed under and governed by the law of the location of Seller's plant at Burlington, Ontario, Canada.

#### **QUOTATION AND PRICES**

All quotations are subject to the Terms and Conditions stated herein as well as any additional Terms and Conditions that may appear on the face hereof. In the case of a conflict between the Terms and Conditions stated herein and those appearing on the face hereof, the latter shall control. Seller's prices and quotations are subject to the following:

- a) All published prices are subject to change without notice.
- b) UNLESS OTHERWISE SPECIFIED IN WRITING, ALL QUOTATIONS EXPIRE THIRTY (30) DAYS AFTER DATE THEREOF, MAY BE TERMINATED EARLIER BY NOTICE AND CONSTITUTE ONLY SOLICITATIONS FOR OFFER TO PURCHASE; further, budgetary quotations and estimates are for preliminary information only and shall neither constitute offers, nor impose any obligation or liability upon Seller.
- c) Unless otherwise stated in writing by Seller, all prices quoted shall be exclusive of transportation, insurance, taxes (including, without limitation, any sales, use, or similar tax, and any tax levied on or assessed to Seller after Product shipment by reason of Seller's retention of a security interest as provided herein), license fees, customs fees, duties and other charges related thereto and Customer shall report and pay any and all such shipping charges, premiums, taxes, fees, duties and other charges related thereto, and shall hold Seller harmless therefrom, provided that, if Seller, in its sole discretion, chooses to make any such payment, Customer shall reimburse Seller in full upon demand.
- d) Stenographic, typographical and clerical errors are subject to correction.
- e) Prices quoted are for Products only and do not include technical data, proprietary right of any kind, patent rights, qualification, environmental or other than Seller's standard tests and other than Seller's normal domestic commercial packaging unless expressly agreed to in writing by Seller.
- f) Published weights and dimensions are approximate only. Certified dimension drawings can be obtained upon request. Manuals, drawings or other documentation required hereupon must be referenced specifically.

This is merely a quotation, and the technology disclosed herein may be covered by one or more ZENON Environmental Inc. (ZENON) patents or patent applications. Any disclosure in this offer does not hereby grant, and nothing contained in the offer shall obligate ZENON to grant, an option to obtain a license to any technology or any other rights under any patent now or hereafter owned or controlled by ZENON.

#### TERMS OF PAYMENT

Unless credit is granted or otherwise specified in writing, payment is due upon shipment. All payments on approved credit accounts

shall be due in full thirty (30) days from date of invoice. Past due balances shall be subject to a service charge of 1-1/2% per month (18% per annum), but not more than the amounts allowed by law. Partial shipments will be billed as made and payments therefor are subject to the above terms. Payment shall not be withheld for delay in delivery of required documentation unless a separate price is stated therefor, and then only to the extent of the price stated for such undelivered documentation. Seller may cancel or delay delivery of Products in the event Customer fails to make prompt payment therefor, or in the event of an arrearage in Customer's account with Seller. Seller hereby retains a security interest in the Products finished until Customer has made payment in full in accordance with the terms hereof. Customer shall cooperate fully with Seller to execute such documents and to accomplish such filings and/or recordings thereof as Seller may deem necessary for the protection of Seller's interest in the Products furnished.

#### TRANSPORTATION AND RISK OF LOSS

Transportation will normally follow Customer's shipping instructions, but Seller reserves the right to ship Products freight collect and to select the means of transportation and routing when Customer's instructions are deemed unsuitable. Unless otherwise advised. Seller may insure to full value of the Products or declare full value thereof to the transportation company at the time of shipment and all freight and insurance costs shall be for Customer's account. Risk of loss and/or damage shall pass to Customer at the FOB point, which shall be the point of manufacture or such other place as Seller shall specify in writing, notwithstanding installation by or under supervision of Seller. Confiscation or destruction of, or damage to, Products shall not release, reduce or in any way affect the liability of Customer therefor. All Products must be inspected upon receipt and claims should be filed with the transportation company when there is evidence of shipping damage, either concealed or external. Notwithstanding any defect or nonconformity, or any other matter, risk or loss and/or damage shall remain with the Customer until the Products are returned at Customer's expense to such place as Seller may designate in writing. Customer, at its expense, shall fully insure Products against all loss and/or damage until Seller has been paid in full therefor, or the Products have been returned, for whatever reason, to Seller.

#### PERFORMANCE

Seller will make all reasonable effort to observe its dates indicated for performance. However, Seller shall not be liable in any way because of any delay in performance hereupon due to unforeseen circumstances or to causes beyond its control, including, without limitation, strike, lockout, riot, war, fire, act of God, accident, failure or breakdown of components necessary to order completion, subcontractor, supplier or customer caused delays, inability to obtain or substantial rises in the price of labour, materials or manufacturing facilities, curtailment of, or failure to obtain sufficient, electrical or other energy supplies, or compliance with any law, regulation or order, whether valid or invalid of any cognizant governmental body or any instrument thereof whether now existing or hereafter created. Performance shall be deemed suspended during, and extended for, such time as any such circumstances or causes delay its execution. Whenever such circumstances or causes are remedied, Seller will make, and Customer shall accept, performances hereupon. In addition, Seller's inventories and current production must be allocated so as to comply with applicable Government regulations. In the absence of such regulations, Seller reserves the right, in its sole discretion, to allocate inventories and current production and substitute suitable materials when, in its opinion, such allocation or substitution is necessary due to such circumstances or causes. No penalty clause of any kind shall be effective. As used herein, "performance" shall include, without limitations, fabrication, shipment, delivery, assembly, installation, testing, and warranty repair or replacement as applicable.

#### **ACCEPTANCE**

The furnishing by Seller of a Product to the Customer shall constitute acceptance of that Product by Customer, unless notice of defect or nonconformity is received by Seller within thirty (30) days of receipt of the Product at Customer's designated receiving address; provided that, for Product for which Seller agrees in writing to

perform acceptance testing after installation, the completion of Seller's applicable acceptance tests, or execution of Seller's acceptance form by Customer, shall constitute acceptance of the Product by Customer. Notwithstanding the foregoing, any use of a Product by Customer, its agents, employees, contractors or licensees for any purpose, after receipt thereof, shall constitute acceptance of that Product by Customer. Seller may repair or, at its option, replace defective or non-conforming parts after receipt of notice of defect or nonconformity.

#### ASSIGNMENTS AND TERMINATIONS

Any assignment by Customer of any contract hereupon without the express written consent of Seller is void. No order may be terminated by Customer except by mutual agreement in writing. Terminations by mutual agreement are subject to the following conditions:

- Customer will pay, at applicable contract prices, for all Products which are completely manufactured and allocable to Customer at the time of Seller's receipt of notice of termination.
- Customer will pay all costs, direct and indirect, which have been incurred by Seller with regard to Products which have not been completely manufactured at the time of Seller's receipt of notice of termination.
- Customer will pay a termination charge on all other determined costs and other charges. To reduce termination charges, Seller will divert completed parts, material or work-in-process from terminated contracts to other Customer's whenever, in Seller's sole discretion, it is practicable to do so.

#### AND OTHER INDUSTRIAL PROPERTY PATENTS RIGHTS

Seller will hold Customer harmless, as set forth herein, in respect to any claim that the design or manufacture of any Product in Seller's commercial line of Products, or manufactured to specifications set by Seller and furnished herein, constitutes an infringement of any patent or other industrial property rights of the United States or Canada. Seller will pay all damages and costs, either awarded in a suit or paid, in Seller's sole discretion, by way of settlement, which have done such claim of infringement avoided that Seller. are based on such claim of infringement, provided that Seller is notified promptly in writing of such claim of infringement but there is no liability whatsoever herein with respect to any claims settled by Customer without Seller's prior written consent. In the event that Seller is required to hold Customer harmless hereupon, Seller will, in its sole discretion and at its own expense, either procure for Customer the right to continue using said Product, replace it with a non-infringing product, or remove it and refund an equitable portion of the selling price and transportation costs thereof. THIS SHALL CONSTITUTE SELLER'S ENTIRE LIABILITY FOR ANY CLAIM BASED UPON OR RELATED TO ANY ALLEGED INFRINGEMENT OF ANY PATENT OR OTHER INDUSTRIAL RIGHTS. Customer shall hold Seller harmless argainst any expense less costs or demogras resulting from claimed against any expense, loss, costs or damages resulting from claimed against any expense, loss, costs or damages resulting from claimed infringement of patents. trademarks, or other industrial property rights arising out of compliance by Seller with Customer's designs, specifications, or instructions. SELLER DISCLAIMS LIABILITY FOR U.S. OR CANADIAN PATENT OR COPYRIGHT INFRINGEMENT ARISING FROM USE OR MANUFACTURE BY ANYONE OF INVENTIONS IN CONNECTION WITH PRODUCTS OR SERVICES SOLD, USED, OR INTENDED FOR SALE OR USE, IN PERFORMING CONTRACTS WITH THE UNITED STATES OR CANADA. OR CANADA.

#### WARRANTY

 Unless otherwise agreed to in writing, Seller warrants its Products to be free from defects in material or workmanship for a period of 12 months from the shipment of Product by Seller, provided that such Product are used, cleaned and maintained in accordance with the Seller's instructions. This warranty does

- not apply to normally replaceable parts or components such as filter cartridges, pump seals, membranes etc., (see below for membrane warranties).
- Customer undertakes to give immediate notice to Seller if goods or performance appear defective and to provide Seller with reasonable opportunity to make inspections and tests. If Seller is not at fault, Customer shall pay Seller the costs and expenses of the inspections and tests.
- 3. Seller's obligations under this warranty is limited to the repair or replacement at its factory, or any device or part thereof which shall prove to have been thus defective. If Customer asks Seller to replace defective parts at Customer's premises, Customer agrees to pay for any traveling time and expenses, plus the Seller's labour to complete the replacement/repair.
- 4. Goods shall not be returned to Seller without Seller's permission. Seller will provide Customer with a "Return Material Authorization" number to use for returned goods. All returns are F.O.B. Burlington, Ontario, Canada.
- Warranty on the membranes applies only if the membrane element(s) has been operated and cleaned according to Seller's instructions. When either permeate or concentrate flow drops by 10% from the original rates at the same operating conditions, cleaning must be initiated or the warranty will be null and void. Elements must be clean and be kept moist. They should be shipped to Seller in water-tight bags and must be protected from freezing. WARNING – if element conditions of use given in Seller's instructions are not followed, the warranty will be null and void.

IMPLIED WARRANTIES, INCLUDING, BUT NOT LIMITED TO, WARRANTIES OF FITNESS FOR PARTICULAR PURPOSE, USE, OR APPLICATION, AND ALL OTHER OBLIGATIONS OR LIABILITIES ON THE PART OF THE SELLER, UNLESS SUCH OTHER WARRANTIES, OBLIGATIONS OR LIABILITIES ARE EXPRESSLY AGREED TO IN WRITING BY SELLER, ARE NULL AND VOID.

#### DAMAGES AND LIABILITY

SELLER'S LIABILITY FOR DAMAGES SHALL NOT EXCEED THE PAYMENT, IF ANY, RECEIVED BY SELLER FOR THE UNIT OF PRODUCT OR SERVICE FURNISHED OR TO BE FURNISHED, AS THE CASE MAY BE, WHICH IS THE SUBJECT OF CLAIM OR DISPUTE. IN NO EVENT WILL SELLER BE LIABLE FOR INCIDENTAL, CONSEQUENTIAL OR SPECIAL DAMAGES, OF ANY KIND, HOWEVER CAUSED, ARISING OUT OF, OR IN ANY WAY CONNECTED WITH, THE PRODUCTS FURNISHED BY SELLER TO CUSTOMER.

All disputes under any contract concerning Products not otherwise resolved between Seller and Customer shall be resolved in a court of competent jurisdiction for the location of Seller's plant at Burlington, Ontario, Canada, and no other place. Provided that, in Seller's sole discretion, such action may be heard in some other place designated by Seller, if necessary to acquire jurisdiction over third persons, so that the dispute can be resolved in one action. Customer hereby consents to the jurisdiction of such court or courts and agrees to appear in any such action upon written notice thereof. and agrees to appear in any such action upon written notice thereof. No action, regardless of form arising out of, or in any way connected with, the Products or Services furnished by Seller, may be brought by Customer more than one (1) year after the cause of action has Conditions of Sale, or the application thereof to any person or circumstances, is held invalid, void or unenforceable, such holding shall not affect and shall leave valid all other parts, provisions, clauses or applications of the Terms and Conditions remaining, and to this end the Terms and Conditions shall be treated as severable.

#### 2.0 ZENOGEM® PROCESS DESCRIPTION

The ZenoGem® Process is a proprietary ZENON technology that consists of a suspended growth biological reactor integrated with a microfiltration membrane system, based on the ZeeWeed® hollow fibre membrane. Essentially, the microfiltration system replaces the solids separation function of secondary clarifiers and sand filters in a conventional activated sludge system.

The ZeeWeed® microfiltration membranes are typically submerged in the aeration tank, in direct contact with the mixed liquor. Through the use of a suction duty pump, a vacuum is applied to a header connecting the membranes. The vacuum draws the treated water through the hollow fibre microfiltration membranes and into the pump. Treated water is then discharged by the pump. The energy associated with permeate pumping is relatively small. An airflow is introduced to the bottom of the membrane module producing turbulence which scours the external surface of the hollow fibres transferring rejected solids away from the membrane surface. This airflow also provides a large portion of the process biological oxygen requirements; the remainder is provided by a diffused aeration system. Waste sludge is pumped directly from the aeration tank.

The ZenoGem® technology effectively overcomes the problems associated with poor settling of sludge in conventional activated sludge processes. The ZenoGem® technology permits bioreactor operation with considerably higher mixed liquor solids concentrations than conventional activated sludge systems which are limited by sludge settling. The ZenoGem® process is typically operated at a mixed liquor suspended solids (MLSS) concentration in the range of 8,000 to 12,000 mg/L. The elevated biomass concentrations allow for highly effective removal of both soluble and particulate biodegradable material in the waste stream. The ZenoGem® process combines the unit operations of aeration, secondary clarification and filtration into a single process, simplifying operation and greatly reducing space requirements.

Since the ZenoGem® process can be operated at elevated MLSS concentrations, extended solids retention times (SRTs) are readily attainable. Accurate SRT control is very simple since no solids are lost in the effluent. Many municipal ZenoGem® plants are operated with SRTs exceeding 25 days. These extended SRTs ensure complete nitrification even under extreme cold weather operating conditions. At extended SRTs, sludge yields can be considerably less than conventional aerobic processes, due to endogenous decay.

The ZenoGem® process is readily adapted for denitrification if total nitrogen removal is required. The elevated levels of biomass become readily anoxic in the absence of aeration, ensuring high denitrification rates. An upstream anoxic zone and mixer readily accommodates denitrification; this can be incorporated in the ZenoGem® tank design.

The ZenoGem® process is ideally suited for phosphorus removal, where required. Through the addition of metal salts such as alum or ferric chloride to the raw wastewater or mixed liquor, soluble phosphorus in the waste stream can be precipitated. The ZeeWeed® membranes have a pore size that provides an absolute barrier to the discharge of precipitated phosphorus. The phosphorus is retained in the mixed liquor and removed with the waste activated sludge. The ZenoGem® process can reliably achieve

significantly lower effluent phosphorus concentrations than conventional municipal treatment processes.

11

#### 3.0 ZENOGEM® ADVANTAGES

#### Effluent Quality

Depending on the specific application and design requirements, a ZenoGem[®] plant can achieve either high quality nitrified effluent or with the addition of an anoxic zone, high quality denitrified effluent. Phosphorus removal is readily achieved through the addition of metal salts to the feed wastewater or mixed liquor. Typically, ZenoGem[®] systems are capable of achieving the following effluent qualities.

 $\begin{array}{lll} BOD & <2 \text{ mg/L}^{\text{Note 1}} \\ TSS & <2 \text{ mg/L}^{\text{Note 1}} \\ TN & <10 \text{ mg/L}^{\text{Note 1}} \text{ (cool climate)} \\ & <3 \text{ mg/L}^{\text{Note 1}} \text{ (hot climate)} \\ TP & <0.1 \text{ mg/L} \\ Turbidity & <1 \text{ NTU} \\ Total \text{ Coliforms} & <100 \text{ cfu/100 mL} \\ Faecal \text{ Coliforms} & <20 \text{ cfu/} 100 \text{ mL} \\ \end{array}$ 

Note 1: The information provided in this section of the proposal is general only and is intended only to indicate what is the ZeeWeed®/ZenoGem® Membrane Wastewater Treatment Technology is capable of achieving. For the specific design treated wastewater quality, based on the consideration of specific raw wastewater characteristics and the required discharge criteria for the treated effluent, refer to Section 4.0.

#### Compact Plant

The ZenoGem® process can operate at mixed liquor suspended solids (MLSS) concentrations in the range of 8,000 to 12,000 mg/L, which is substantially greater than conventional activated sludge processes. This allows for conventional organic loading rates to be achieved with much lower hydraulic residence times. In addition, the ZenoGem® process requires a single tank in which aeration and solids separation are both achieved. If required, sludge digestion can also be accomplished in this tank. This single stage process results in an overall plant footprint substantially smaller than conventional tertiary wastewater treatment plants.

#### **Expandability**

Since the ZenoGem® equipment is modular in nature, plant expansion can be phased. Civil works can be designed for ultimate flow while membranes are added in phases as plant operating capacity dictates.

#### Simple Operation

Since the ZenoGem® process uses membranes to perform solid/liquid separation, there is no requirement for sludge to settle and thus no need for a secondary clarifier or polishing filters. Sludge is wasted directly from the aeration tank at a solids concentration in the range of 1.5 to 2.0 percent solids. The result is a single system which is simple to operate.

#### Lower Sludge Yield

The ZenoGem® plant can be operated at extended solids retention times (SRTs) allowing for lower net solids yields than conventional municipal treatment processes.

#### **Process Reliability**

Since the ZenoGem[®] plant is typically operated at low organic loading rates and the membrane provides an absolute barrier to particulate discharge, ZenoGem[®] effluent quality is not susceptible to hydraulic or organic surges which can negatively affect effluent quality in conventional activated sludge and fixed film plants. At periods of low flow (and organic load), the sludge within the reactor basin simply digests itself, without affecting the effluent quality.

#### Advantages of an "Outside-In" Membrane

#### a) Resistance To Fouling

The ZeeWeed® membrane is an outside-in membrane where the flow of water is from the outside of the membrane to the inside of the hollow fibre, meaning that the inside only sees clean, microfiltered water. The bacteria and inert solids to be removed from the wastewater remain outside the membrane and never enter the membrane to cause fouling.

#### b) Low Energy

Being immersed allows for the operation of the ZeeWeed® membrane under a slight vacuum (suction) instead of under positive pressure like other membranes on the market. The ZeeWeed® membrane operates under a vacuum of between -2 to -8 psi. The pump energy requirements to achieve this vacuum are relatively small.

#### **Exceptional Membrane Durability**

The ZeeWeed® membrane has been designed for exceptional durability and resistance to breakage. To achieve this high level of membrane durability ZENON utilizes a patented internal support to which the membrane is bonded. This support strengthens the membrane and protects it against tearing and breakage without reducing its flux capacity.

#### 4.0 ZENOGEM® PLANT

Firm Capcity Flow

The proposed ZenoGem[®] plant is designed to continuously treat an average daily flow of 8.5 MGD. The ZenoGem[®] plant is a six (6) train system and the capacity of each parallel train is .1.417 MGD.

The ZenoGem® plant is capable of producing an effluent meeting or exceeding the following criteria:

8.5 MGD

#### Design Parameters

<u>Parameter</u>	Influent		<u>Effluent</u>	
BOD	200	mg/L	≤2	mg/L
TSS	150	mg/L	≤2	mg/L
TKN	46	mg/L	≤3	mg/L
TN	46	mg/L	≤17	mg/L
TP	9	mg/L	≤1	mg/L
Wastewater Temperature	≥20	°C	≥20	°C

#### **Equipment Selection**

The main process equipment for the ZenoGem[®] plant, including permeate pumping equipment, membrane air scour blowers and supplemental aeration blowers, CIP membrane cleaning system, air extraction system, controls and other miscellaneous items, is designed for installation within equipment buildings (equipment buildings not included in ZENON's scope of supply).

The sizing of the main process equipment selected is as follows. Section 5.0 gives further details of the equipment items included by ZENON for this project.

#### Bioreactor (Process) Tank(s)

The bioreactors will consist of concrete tanks (concrete tanks not in ZENON's scope of supply). Six (6) individual process streams are required, each with the minimum dimensions of 160 ft long x 20 ft wide x 17 ft high (15 ft SWD). Each process tank will have an anoxic/aerobic and an aerated membrane zone separated by a baffle (baffle not included in ZENON's scope of supply).

Membrane cassettes will be supported by structural steel beams that will span between the concrete walls of the process tanks and will use the concrete walls as supports.

#### Process Tanks

Total Bioreactor Volume	2.154	MUS gallons
Design HRT	6	hours
Number of Membrane Trains	6	
Number of Bioreactor Tanks	6	
Volume of Each Bioreactor	359,000	US gallons

Length of Each Bioreactor	160	ft
Width of Each Bioreactor	20	ft
Side Water Depth of Bioreactor	15	ft

Note: Process tanks may be of concrete construction or fabricated steel tanks, whichever suits the client's preferences and are not included in ZENON's scope of supply.

Tank dimensions are preliminary only and may change slightly once final detail design commences.

#### ZW-500 Micro-Filtration Membrane Modules

Membrane Design Flux	11.55	gfd at Fixed Capacity Daily flow
Rate		
Minimum Design Liquid	20	°C
Temperature		
# Membrane Modules	1104	
# Membrane Cassettes	138	(8 modules per Cassette)

ZENON is committed to continuous development and invests continuously in research to develop better and higher flux membranes. For this reason ZENON reserves the right to change the number of membranes in its design, if by way of membrane technology improvements the permeability or operating flux rates of the membranes have been improved. This does not change the warranty since ZENON guarantees the design flow capacity and the operational performance of the membrane system.

#### Aeration System

The design air flow required for the fine bubble aeration system used with the ZenoGem[®] plant is approximately 5,550 scfm at the plant design capacity.

#### Aeration Blowers

Three (3) aeration blowers are included - two duty blower and one common stand-by unit. Each blower has a design capacity of 2,775 scfm. The aeration blowers are equipped with variable frequency drives (VFDs) to allow air delivery and dissolved oxygen levels in the wastewater to be controlled according to the system air requirements.

#### Membrane Air Blowers

Four (4) blowers are included for the membrane air scouring - four duty blower and one common standby unit The total required capacity of membrane air scouring is approximately 21,983 scfm. Each blower has a design capacity of 7,328 scfm.

#### Permeate Pumps

Seven (7) permeate pumps are included - six duty pumps and two shelf spares. Each pump is designed for a maximum permeate flow of 1,110 USgpm. The pumps will also provide backpulse flow at 2,880 USgpm The speed of the permeate pumps is controlled via VFD units according to the liquid level in the bioreactor tanks.

#### Sludge Recirculation Pumps

Seven (7) sludge recirculation pumps are included - six duty pumps and one shelf spare. Each pump is designed for a flow of 3,395 USgpm. The recirculation pumps are provided with VFD units to allow flow variation to allow optimization of the system process performance.

#### Sludge Wasting Pumps

Seven (7) sludge wasting pumps are included – eight duty pumps and one shelf spare. Each pump is designed for a flow of 207 USgpm.

#### Miscellaneous

No influent screening facilities are included. There must be existing screening and/or primary clarifiers upstream of what will become the ZenoGem® aeration (bioreactor) tanks. The screening equipment must be capable of screening particles down to 3.0 mm to prevent hair and other stringy materials from tangling with the membranes.

Equipment Installation cost is not included.

#### 5.0 MAJOR EQUIPMENT

The list below summarizes the major equipment and the quantities of items included for the ZenoGem® plant design.

SCOPE OF SUPPLY SYNOPSIS	<del>, 38</del>		
for the ZenoGem® Plant			
Item	Size	Units	Quantity
Raw Wastewater Feed	5120	Circo	Quarterly
Raw Influent Feed Pumps			Not Incl.
Inlet & Discharge Isolating Valves			Not Incl.
Discharge Check Valves			Not Incl.
Piping Manifold			Not Incl.
Wet Well Level Switches			Not Incl.
VFD's			Not Incl.
Raw Water Screening			
Raw Influent Screen			Not Incl.
Raw Influent Grinder			Not Incl.
Raw Influent Flowmeter			Not Incl.
Raw Influent Flow Control Flowmeter			Not Incl.
Raw Influent Flow Control Valve			Not Incl.
Membranes/Membrane Cassettes			
Individual Membrane Modules			1,104
Membrane Cassettes			138
Process Tanks & Frames			
Membrane Support Beam(s)			Included
Process Tanks			Not Incl.
Permeate Collection Headers			6
Air Scour Headers			6
Permeate Pumps			
Permeate Pumps	1,110	USgpm	7
VFD's	50	HP	6
Piping Manifold			Not Incl.
Valves			Incl.
Air Extraction System			
Air Removal Separation Columns			6
Vacuum Pumps	22	scfm	3
Backpulse System			
Backpulse Water Storage Tank	5,160	gallons	_2
Hypochlorite Storage Tank	106	gallons	1
Hypochlorite Feed Pumps	6.08	USgphr	3

Item	Size	Units	Quantity
DIP Tank Cleaning System			
DIP Tank			Not Incl.
Chemical Wash Pump			Incl.
Monorail & Pulley/Hoist for membrane removal			Not Incl.
Sludge Recirculation			
Sludge Recirculation Pumps	3,935	USgpm	7
Inlet & Discharge Isolation Valves			N/A
Discharge Check Valves			N/A
Piping			Not Incl.
VFD's	2.5	HP	6
Sludge Wasting		Ì	
Sludge Wasting Pumps	206.6	USgpm	7
Inlet & Discharge Isolation Valves			6
Discharge Check Valves			6
Piping			Not Incl.
VFD's			N/A
Air Blowers			
Membrane Air Scour Blowers incl. Silencers	7,328	scfm	4
Inlet & Discharge Isolation Valves			4
Discharge Check Valves			4
Inlet Control Valves			4
Aeration System Blowers incl. Silencers	2,775	scfm	3
Inlet & Discharge Isolation Valves			3
Discharge Check Valves			3
VFD's	200	hp	3
Biological Aeration System			
Fine Bubble Diffuser System			Incl.
Phosphorus Removal System (if required)			
Chemical Storage Tank	9,600	USg	1
Chemical Feed Pumps	112	USgphr	2
Instruments			
Permeate Flowmeters			6
Permeate Header Pressure Transducers			6
Process Tank Level Transmitters			6
Process Tank Level Switches			48
Dissolved Oxygen Sensors			6
pH Transmitters			N/A
Turbidimeters			6
Turbidimeter Calibration Kits			1

Membrane Blower Flow Switches		4
Aeration Blower Flow Switches		3

Item	Size	Units	Quantity
Permeate Pump Pressure Gauges			6
Membrane Air Scour Blower Pressure Gauges			4
Aeration Blower Pressure Gauges			3
Recirculation Pump Pressure Gauges			N/A
Sludge Wasting Pump Pressure Gauges			6
Control Panel			
PLC-based Control Panel			1
Back-Up PLC			Not Incl.
Electrical			
MCC Panel			Not Incl.
Miscellaneous			
Air Compressor			2
Air Drier			1
Field Service Allowed			Days
Installation Supervision			10
Mechanical Checkout			6
Operator Training			8
Process Start-Up			3
Commissioning			3
TOTAL MAN-DAYS			30
TOTAL No. TRIPS			3
Freight			
Delivery to Site			Incl.

#### 6.0 ATTACHMENTS

Plant Power Consumption and Estimated Yearly Operating Cost

Table 9.1.1 Connected Power and Estimated Power Consumption at Average Day Flow

City of McAilen (ZenoGem) Rev 1

Average Day Flow 8,500,132 USqpd 32,173 m3/day **Maximum Day Flow** 8,500,132 USgpd 32,173 m3/day

		EQUIPMENT DESCRIPTION		# Operating Pumps Blowers etc.	Design Capacity	Discharge Head	Duty Point Efficiency	Equipment Operating BHP	Motor HP	Total Equipment BHP	Total Connected HP	Motor Efficiency %	Equipment kW	Hours / Day Continuous Operation	Energy Cost per year
-, +		Raw Water/Wastewater Screen	n/a	<u> </u>					_			 		24.00	
	6.00	Permeate Pumps	By Zenon	6.00	1,109.56 USgpm	35.00 ft	81.00	12.29	20.00	73.76	120.00	90.20	60.98	22.40	37,392
3	- 0.00	Backpulse Pumps	n/a	0.00	2,880.00 USgpm	30.00 ft	74.00	29.94	40.00	73.76	120.00	90.20	00.96	6.40	37,382
- 4	6.00	Recirculation Pumps	By Zenon	6.00	3,935.25 USqpm	10.00 ft	55.00	18.35	25.00	110.08	150.00	91.30	89.91	24.00	59,068
5	6.00	Sludge Wasting Pumps	By Zenon	6.00	206.60 USgpm	30.00 ft	50.00	3.18	5.00	19.07	30.00	87.50	16 25	200	890
- 6	- 0.00	Reject Water Pumps	n/a		- USgpm	25.00 ft	55.00		0.00	13.07		07.50	10.23	24.00	
7 1	4 00	Membrane Air Scour Blowers	By Zenon	3.00	5,520.00 scfm	4.25 psl	n/a	153.32	250.00	459.97	1.000.00	95.00	361.05	24.00	237,213
8	3 00	Process Air Blowers	By Zenon	2.00	2,775.00 scfm	6.00 psi	n/a	114 89	150.00	229.77	450.00	94.20	181.89	24.00	119.501
9		Miscellaneous Air Blowers	n/a		- scim	6.00 psi	n/a		-	-	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		- 107.00	24.00	
10	6.00	Anoxic Zone Mixers	By Zenon	6.00			n/a		-	-	-	80.00	-	24.00	-
11	3 00	Air Separation System Vacuum Pumps	By Zenon	2.00	22.25 actm	18.00 ins Hg	n/a	2.25	3.00	4.50	9.00	87.50	3.84	24.00	2,520
12	3.00	Backpulse Sodium Hypochlorite - Metering	By Zenon	1.50	0.066 USgpm	50.00 ft	n/a	0.03	0.03	0.04	0.09	100.00	0.03	3 20	3
13	-	CIP Wash Pump	n/a		- USgpm	30.00 ft	55.00	-		•	-	-	-	0.03	-
14		CIP Chemical Metering	n/a		USgpm			-		-			-		•
15	2.00	Chemical Feed #1 System #1 - Metering	By Zenon	1.00	1.140 USgpm	50.00 ft	n/a	0.50	0.50	0.50	1.00	100.00	0.37	24.00	245
16	-	Chemical Feed #1 System #2 - Metering	n/a	-	0.101 USgpm	50.00 ft	n/a	-	0.03	-	-	100.00	-	24.00	
17	-	Chemical Feed #1 System #3 - Metering	n/a	-	0.057 USgpm	50.00 ft	n/a		0.03	-	-	100.00	-	24.00	-
18	-	Chemical Feed #1 System #4 - Metering	n/a		0.065 USgpm	50.00 ft	n/a	·	0.02	-	•	100.00		24.00	-
18	2.00	Air Compressors	By Zenon	1.00	52.00 scfm	100.00 psi	n/a	18.75	25.00	18.75	50.00	91.30	15.31	6.00	2,515
19	1.00	Air Driers	By Zenon	1.00	75.00 scfm		n/a	-	-	-	-	80.00		600	
20	1.00	Controls & Instrumentation	By Zenon								1.34		1.00	24.00	657
_21	1.00	Miscellaneous	By Zenon								1.34		1.00	24.00	657
1		Total Connected Power	1			<u> </u>					1,812.77	HP			
		Total Operating Power								916.44			731.64	kW	
		Total Operating Cost								0.0.77	"			USS	460,661

Notes

Energy Costs based on 0.0750 US\$ per kW.hr

Power Consumption of other plant equipment required (raw water feed pumps, high lift pumps etc.) is not included by ZENON

Where operating efficiencies are not known, the equipment operating power is assumed to be 75% of the motor nameplate power rating

The operating hours for the permeate pump are corrected for the downtime during backpulse cycles (and Membrane Pressure Decay Test Cycles if applicable)

Permeate Pump Backpulses every 15 mins for 30 seconds 1,664 USgpm @ 30.00 ft TDH =

16.59 BHP

Motor Efficiencies indicated are typical only. Efficiencies used are usually within 2% of actual when motor is operating within 50-100% of its full load rating

Operation of Air Compressor is assumed to be only 25% of time

Operation of the Sodium Hypochlorite Pumps is intermittent - operation for 25% of time is used for energy calculation

Blower Energy Consumption Estimated as :

6.536 BHP per 1,000 scfm per psig.

The motor sizes in the above table are preliminary only and estimated based on the information available at the time of preparing this proposal. It must be understood that at the time of proposal preparation, final headjosses or pressure drops in piping systems have not been calculated accurately Motor sizes are subject to confirmation (and if necessary adjustment) during final design. Use of the above information for sizing or selection of any ancillary equipment is entirely at the USER's own risk. Whilst the motor sizes indicated above are ZENON's best estimate based on design criteria assumed during preparation of the proposal, ZENON accepts no responsibility for the absolute accuracy of the information contained herein.

## Table 9.2.2 Estimated Total Annual Operating Cost City of McAllen (ZenoGem) Rev 1 Average Day Flow 8,500,132 USgpd Maximum Day Flow 8,500,132 USgpd

32,173 m3/day 32,173 m3/day

tem			Cost per year	
Electrical Equipment - Zenon		Calculated at Average Day Flow	460,661	US\$
Electrical Equipment - Others				US\$
Backpulse Chemicals	Sodium Hypochlorite	Calculated at Average Day Flow	8,232	US\$
CIP Chemical #1	MC-1		220	US\$
CIP Chemical #2	Sodium Hypochlorite - 250 mg/L		304	US\$
Chemical #1	Aluminum Sulphate (Liquid @ 48.5%)	Calculated at Average Day Flow	201,764	USS
Suggested Membrane Accrual			329,311	US\$
Estimated Total Annual Oper	ating Cost		1,000,492	USS

Esumateo	Total Annual Operating Cost			
Notes	Backpulse Chemical Consumption		Sodium Hypoc	
	Sodium Hypochlorite Consumption		71.91	Litres per day
	Sodium Hypochlorite Consumption		26,248	Litres per year
	Sodium Hypochlorite Cost	US\$	0.31	per Litre
	CIP Cleaning Chemical #1		MC-1	
	Design Dosage		2,000.00	mg/L
	Solution Concentration		50.00	%
	Specific Gravity		1.240	
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tan	ks)	131.54	Litres
	Total Annual Chemical Consumption		131.54	Litres
	Chemical Cost	US\$	1.67	per Litre
	Chemical Cost	U <b>S\$</b>	2.70	per kg
	CIP Cleaning Chemical #2		Sodium Hypoc	hlorite - 250 mg/L
	Design Dosage		250.00	mg/L
	Solution Concentration		10.80	%
	Specific Gravity		1,168	
	Wash Frequency		12.00	times / year
	Chemical Consumption per Wash (all tan	ks)	80.81	Litres
	Total Annual Chemical Consumption		969.76	Litres
	Chemical Cost	US\$	0.31	per Litre
	CIP Neutralization Chemical #1		Sodium Hydro	vide
	Design Dosage			ma/L
	Solution Concentration		50.00%	9-
	Specific Gravity		1.520	
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tan	ks)		Litres
	Total Annual Chemical Consumption	,	-	Litres
	Chemical Cost	US\$	0.36	per Litre
	Chemical Cost	US\$	0.47	per kg
	CIP Neutralization Chemical #2		Sodium Bisulfi	
	Design Oosage		•	mg/L
	Solution Concentration		38.00%	
	Specific Gravity		1.290	
	Wash Frequency		12.00	times / year
	Chemical Consumption per Wash (all tan	ks)	•	Litres
	Total Annual Chemical Consumption			Litres
	Chemical Cost	US\$	0.06	per Litre
	Chemical Cost	US\$	0.55	per kg
	Chemical Feed System #1		Aluminum Sul	ohate (Liquid @ 48.5%)
	Design Dosage		90.00	mg/L
	Solution Concentration		48.50	%
	Specific Gravity		1.335	
	Chemical Consumption		4,472.10	
	Chemical Consumption		1,632,315	Litres per year
	Chemical Cost	US\$	0.12	per Litre
	Chemical Cost	US\$	0.19	per kg

12/07/1999 : 3:59 PM ZENON - CONFIDENTIAL

## *PROPOSAL*

990212-M



845 Harrington Court, Burlington, Ontario, L7N 3P3 Tel. No.: (905) 639-6320 Fax No.: (905) 639-1812

DATE:

November 29, 1999

PREPARED FOR:

CH2M Hill

ATTENTION:

Mr. Jim Lozier

FROM:

Roland Lamoca

Re:

McAllen South WWTP

#### **ITEMS COVERED:**

Packaged water treatment plant incorporating Reverse Osmosis treatment.

The plant is to be designed for three trains, each with an effluent flowrate of 2.3 MGD of final product from the Reverse Osmosis system. The projected recovery rates from each unit operations have been established in the specifications provided CH2M Hill and are estimated at 80% - 85%.

The preliminary design criteria are:

One Reverse Osmosis Train

Effluent Flow (MGD)

2.3 MGD

System Recovery (%)

80 - 85 %

#### SCOPE OF SUPPLY:

#### Three Reverse Osmosis System Trains - Each:

- eighty-eight (88) 6 element long membrane pressure vessels, 400 psi rating, arranged in a 50:28:10 array configuration for optimal cross-flow conditions.
- five hundred twenty eight (528) Hydranautics spiral wrap high rejection type membrane modules. Six membrane elements will be installed in each membrane pressure vessel. A total membrane area of 192,720 ft2 is supplied,
- one (1) duplexed 5 micron prefiltration cartridge system, isolatable for cartridge replacement,
- one (1) horizontal, split case centrifugal-type feed supply pump, 1880 USgpm @530 ftH, 1780 rpm TEFC, Goulds or equal,

### **PROPOSAL**



990153-M

845 Harrington Court, Burlington, Ontario, L7N 3P3 Tel. No.: (905) 639-6320 Fax No.: (905) 639-1812

- one (1) sodium metabisulfite chemical injection system with chlorine analyzer, Prominent or equal,
- one (1) antiscalant injection system, Prominent or equal,
- one (1) acid injection system with pH probe and controller, Prominent or equal,
- one (1) lot process instrumentation for the RO system, includes feed conductivity, permeate conductivity, permeate flow transmitter, concentrate flow transmitter, concentrate pressure transmitter, membrane feed pressure transmitter, permeate pressure transmitter, feed supply residual chlorine analyzer, and feed supply pH.
- one (1) lot process valves for the RO system, Bray or equal,
- one (1) lot process low pressure piping Sched. 10 304 SS,
- one (1) lot process high pressure piping Sched. 10 316 SS,
- one (1) NEMA 4 PLC based control panel (Allen Bradley PLC complete with PanelView Operator Interface),

#### One Reverse Osmosis System Clean In Place Tank:

• one (1) skid mounted membrane cleaning tank with prefiltration cartridge system, and cleaning pump (316SS Goulds, or equal) and controls,

#### PRICE ESTIMATE:

US\$ 2,300,000.00

#### TERMS:

- All pricing in Dollars, FOB ZENON Burlington, Ontario.
- Duty, if applicable, is not included. Any Taxes, if applicable, are extra.
- Shipment shall be 20 24 weeks from receipt of order.
- Payment Terms: 15% with order, 25% on submission of drawings, 50% on equipment shipment, 10 % on start-up or thirty days whichever is less, all terms are Net 30.
- ZENON's Terms and Conditions as attached shall apply.
- This is a budgetary estimate only at this time, and does not constitute a binding offer of supply by ZENON.





JAN 18 2000



CH2M HILL PHUENIX Water for the World

Project Number: 990212-M

TO:

CH2M Hill

nemerop: naka tempetenan bila lebi ne

FAX:

480 966 9450

ATTN.:

Ms. Fair Miller

cc:

Jim Lozier - CH2M Hill

PHONE: 480 966-8577 x 249

Dave Bingham - ZENON

cc FAX:

DATE:

18 January, 2000

# OF PAGES

(Including Cover): 5

FROM:

Roland Lamoca

Manager, Technical Support Division

Industrial Wastewater Division

SUBJECT: McAllen Reverse Osmosis Operating Cost Estimates - Revision

Hello Fair and Jim;

The operating costs have been revisied based on our discussions today.

The higher pressure we had included previously accounted for a 5 year operation with a 10% flux decline/year. This is typical of ZENON's experience, but may not reflect recent experiences you have noted. As agreed upon, the following have been based on your experiences.

Please feel free to contact ZENON if you have any questions.

Regards,

Roland Lamoca

If you do not receive all pages, please call Lisa Ashton as soon as possible.

ZENON Environmental Systems Inc.

845 Harrington Court, Burlington, Ontario, L7N 3P3 Telephone: (905) 639-6320 Fax: (905) 639-1812 email: rlamoca@zenonenv.comhttp://www.zenonenv.com



#### **Operating Cost Summary**

**Assumptions** Annual Cost, US\$ Item (based on \$0.07 /kW-hr) \$357,495 /year **Power Consumption** Steam Consumption (based on \$5.00 /1000 lb) Membrane Replacement (every 5 years) (based on current prices, subject to change) \$190,179 /year Cartridge Filter Replacement (once per year) (based on current prices, subject to change) \$24,637 /year **Annual Process Chemical Cost** \$130,698 /year **Annual Cleaning Chemical Cost** \$15,144 /year

**TOTAL ANNUAL OPERATING COSTS** 

\$718,152 /year

Water Volume Produced Annually:

(based on 4800 USgpm)

2,522.9 Million gallons per year

**Operating Cost per Thousand Gallons** 

\$0.28 /1000 gallons



#### **Operating Cost - Power**

#### **Power Consumption**

<u>Unit</u>	# of units	Power/unit	Total power
Pre-treatment Chemical Mixers, 0.25 Hp	total of 6	0.2 kW	1.1 kW
1st Pass - R.O. Process Pump, 260 Hp	total of 3	194.0 kW	581.9 kW
Reverse Osmosis CIP Pump, 125 Hp	total of 1	93.3 kW	Intermittent use

RO process pump pressure is 165 psi @ 1883 USgpm each

Total Power Requirement		583 kW	
Operating period	Days / year	365 days	
	Hours / day	24 hours	
Utility	rate (\$/kW-hr)	\$0.07 /kW-hr	
Annual Power Consi	umption Cost	\$357,495 /year	



#### **Operating Cost - Elements**

#### Membrane Replacement (every 5 years)

Membrane Element

# of elements

Unit Price, US\$

Extended price, US\$

8" HYDRANAUTICS 8040-LFC1

total of 1584

\$600 each

\$950,894

Membrane pricing assumes negotiated pre-purchase price and is to be verified.

Membrane Replacement Cost

\$190,179 /year

#### Cartridge Filter Replacement (once per year)

Filter Cartridge

# of cartridges

Unit Price, US\$

Extended price, US\$

FILTERITE QMPT050-300USM8 FILTERITE QMPT050-300USM8

total of 324 total of 72

\$62 each \$62 each \$20,158 \$4,479

Cartridge Filter Replacement Cost

\$24,637 /year



#### **Operating Cost - Process Chemicals**

#### **Process Chemical Requirements**

<u>Chemical</u>	<u>Annual</u> <u>Consumption</u>	Unit Cost,US\$	Annual Cost, US\$
Sulphuric acid	10374 USgallons	\$0.04 /lb	\$5,745 /year
Sodium bisulphite	12288 USgallons	\$0.25 /lb	\$2,594 /year
Antiscalant	9892 USgallons	\$3.27 /litre	\$122,359 /year

Annual Process Chemical Cost

\$130,698 /year

#### **Operating Cost - Cleaning Chemicals**

#### **Cleaning Chemicals / Preservative Requirements**

<u>Chemical</u>	<u>Annual</u> Consumption	Unit Cost,US\$	Annual Cost, US\$
Organic Acid: MC-1	3788 kilograms	\$2.29 /kg	\$8,658 /year
Alkali Surfactant: MC-4	568 kilograms	\$3.06 /kg	\$1,738 /year
Sanitizer: MP-1	947 litre	\$5.01 /litre	\$4,748 /year

**Annual Cleaning Chemical Cost** 

\$15,144 /year

Appendix I. ZenoGem and ZeeWeed Cost Comparison

Item	7	ZenoGem*	ZeeWeed*
Fine Screening		20,000   8	
ZenoGem* / ZeeWeed* System ^a	\$	<u> </u>	\$ 5,075,00
Bioreactor/Equalization / ZeeWeed Tanks	-   \$	1,307,808	
Stored and Control of Taring		1,007,000	102,40
nstallation	\$	2,155,000	\$ 1,268,75
nstalled Costs Subtotal	\$	12,102,808	\$ 6,526,21
ZenoGem / ZeeWeed Equipment Building	\$	288,000	\$ 84,00
nstalled Costs and Building Cost Subtotal	\$	12,390,808	\$ 6,610,21
Unit Process Noncomponent Costs			
Yard Piping Allowance (10%)	\$	1,239,081	\$ 661,02
Site Electrical Allowance (8%)	\$	991,265	\$ 528,81
Site I&C Allowance (5%)	\$	619,540	\$ 330,51
Site Civil Allowance (5%)	\$	619,540	\$ 330,51
Unit Process Subtotal	\$	15,860,234	\$ 8,461,07
Contingency (10%)	\$	1,586,023	\$ 846,10
Contractor Overhead & Mark-up (10%)	\$	1,586,023	\$ 846,10
Total Construction Cost	S		\$ 10,153,29
Engineering & Administration (15%)	s		\$ 1,522,99
Total Capital Cost	s		\$ 11,676,28
Total Capital Unit Cost (\$/1,000 gallon)	s		\$ 4.9
Amortized Capital Cost (20yr @ 6.5%)	\$		\$ 1,059,69
Operation & Maintenance Costs			
Major Chemical Costs			
Backpulse Chemicals: Sodium Hypochlorite	\$		\$ 8,23
CIP Chemical #1: MC-1	\$		\$ 3,21
CIP Chemical #2: Sodium Hypochlorite (250 mg/L)	\$	304	\$ 4,43
CIP Neutralization Chemical #1: Sodium Hydroxide	\$		<b>\$</b> 17
CIP Neutralization Chemical #2: Sodium Bisulfite	\$	- !	\$ 11
Major Power Costs			
Screening	\$		\$ -
Aeration Basins	\$		\$ 419,00
Permeate Pumps	\$		\$ 36,90
Recirculation Pumps	\$		\$ 74,50
Sludge Wasting Pumps	\$		\$ -
Membrane Air Scour Blowers	\$	237,213	\$ 114, <u>44</u>
Process Air Blowers	\$	119,501	\$ -
Anoxic Zone Mixers	\$		\$ -
Air Separation System Vacuum Pumps	\$	2,520	\$ 2,52
Backpulse Sodium Hypochlorite - Metering	\$	3	\$
Chemical Feed #1 - Metering	\$	245	\$ -
Air Compressors	\$	2,515	\$ 2,51
Air Driers	\$		\$ -
Controls & Instrumentation	\$	657	\$ 65
Miscellaneous	\$	657	\$ 65
Membrane Replacement Costs	\$	329,311	\$ 190,90
Labor	\$	280,800	\$ 218,40
		4.070.505	4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4
Total Annual Operation & Maintenance Cost	\$		\$ 1,076,67
Total Annual O&M Unit Cost (\$/1,000 gallon)	\$		\$ 0.4
Total Annual Cost	-   \$   \$	3,065,924	
Total Annual Unit Cost (\$/1,000 gallon)		1.30	\$ 0.9



# DEMONSTATION TESTING OF ZENOGEM AND REVERSE OSMOSIS FOR INDIRECT POTABLE REUSE

## FINAL TECHNICAL REPORT ADDENDUM

City of McAllen, TX

by

James C. Lozier, P.E. and Angela M. Fernandez, E.I.T CH2M HILL

Cooperative Assistance Agreement No. 98-FC-81-0073

Desalination Research and Development Program Report No. 51 February 2000

U.S. DEPARTMENT OF THE INTERIOR
Bureau of Reclamation
Technical Service Center
Water Treatment Engineering and Research Group

D-8230 ACM-1.10

Mr. James C. Lozier, P.E. Project Manager, CH2M Hill 1620 Fountainhead Parkway Suite 550 Tempe AZ 85282

Re: Agreement Number 98FC810073, Desalination Research and Development Program Report No. 51, Draft Report Review Comments

Dear Mr. Lozier:

Thank you for presenting the data and results from the project titled "Demonstration Testing of Zenogem and Reverse Osmosis For Indirect Potable Reuse" on December 14, 1999. Ms. Angie Fernandez also deserves to be recognized for her valuable assistance in both the presentation and in overseeing the piloting activities.

Attached, for your consideration are select comments, both editorial and technical, which I believe will strengthen the final report's technology transfer capability.

If you have any questions on these comments, please do not hesitate to call at 303 445-2254.

Sincerely,

Robert A. Jurenka, P.E.

Attachment

cc: D-7810 (Mulligan)

cc: Mr. Wm. Bart Hines, City of McAllen TX,

bc: D-8230 (Price, Jurenka)

WBR:RJurenka:geg:xx/xx/xx:2254 Jurenka/rpt51comltr.wpd

Review Comments, "Demonstration Testing of Zenogem and Reverse Osmosis For Indirect Potable Reuse"

City of McAllen TX,

Cooperative Agreement No. 98-FC-81-0073

The following are suggested editorial comments:

- 1. Complete the acknowledgment page
- 2. Complete all missing appendices
- 3. Page 1-7: Shouldn't the last paragraph be indented?
- 4. Page 1-8 second line: delete "should".
- 5. Page 3-3, section 3.2.1: To the second paragraph: Third line, delete "...can (or may)" and replacewith "may";
- 4th line: add of after "value" and delete the parentheses;
- 5th line: move ">3 months" ahead of "infrequently" and replace"during" with "at";
  - 7th line: replace "insitu" to "in situ"
- 6. Section 3.2.2, last line: delete the parentheses.
- 7. Page 3-7: section 3.3.2:
- a. second paragraph: The lat 2 sentences seem redundent considering the previous section. Can they be rephrased?
  - b. third paragraph antiscalent is mispelled.
- c.  $5^{\text{th}}$  paragrpah: replace in the  $3^{\text{rd}}$  line, "can (or may)" with "may".

The following are recommended technical comments:

### 1. Page 1-1:

- a. To the first paragraph, add: This Program sponsors research in an effort to lower the cost of treatment technologies.
- b. The second paragraph describes UV treatment (also listed on page 1-5), however, there is nothing in the conclusions regarding it. Obviously the decision was made to use chloramines both in the pilot and in the projections of costs at full scale. Add sentences in the report describing why this disinfectant technique was replaced.

- c. Second paragraph, last sentence: define "intended purpose".
- d. Restructure the  $4^{th}$  paragraph by either using a colon and numbering the items, or make each point a separate sentence.
- 2. Page 1-3, re: El Paso Texas paragraph: Add to the end of the next to the last sentence... "because the increased pumping is lowering the aquifer level to the higher salinity water source."
- 3. Page 1-4: In section 1-2 the second sentence: It is recommended that "...from the Rio Grande River, water rights that it shares with multiple parties, including..." be replaced with, "...from water rights in the Rio Grande River that it shares with multiple parties including ..."

### 4. Page 1-6: Section 1.5.1,

- a. second bullet: List the WWTP effluent limits (as shown on page 4-1, section 4.1.1) and reference the table, by table number and page number, of the final values.
- b. The term maintenance clean or acid maintenance clean is used here and on pages 1-7, 1-9, 3-3, etc. Define this term prior to its use or add as a reference the page number where it is defined.

#### 5. Page 1-7:

a. First point: At the start of this point, replace "Flow Peaking" with "Flow peaking tests were run over a 24 hour period of time to simulate the types of peak loading conditions that typically occur in a conventional wastewater treatment plant. However, this (significantly)...

Also, at the end of this point add, "As a result, additional means must be provided such as ?? to ensure that slower changes in loading occur to give the membrane bioreactor system time to react to the change in loading."

- b. Second Bullet: Clarify what "intermittent aeration" is. Delete the words, "treatment conditions resulting in".
  - c. Third bullet: Add a reference to the table of results.
- d. Add a fourth bullet with the following: Per Table 5-16, Zenogem permeate was of lesser quality and the RO permeate was of greatert quality than the City's existing raw water source.
  - e. To the end of the fourth bullet add the following

sentence: However, the RO system always removed any remaining coliform regardless of the MF or UF pretreatment. Also, add the table number and page on which it can be found for the results supporting this conclusion.

- f. Add one last point about how cost effective and how much smaller the footprint area is as compared to a conventional treatment system.
- g. Section 1.5.2 RO System, Bullet 1, 4th line: Add "in the predominant form of monochloramine..." after "Continuos disinfection..." Also, add the table numbers and pages on which to be found for the results supporting this conclusion.

### 6. pages 1-7 and 1-8,

- a. RO System, bullet 2: If 80% is "higher" as stated, state what the normal or target recovery rate is. Also, clarify why the 80% recovery rate is described differently between bullet 2 and bullet 3. (I.E. higher vs design).
- b. RO System, bullet 3: Will blending the RO product water with Zenogem product water be acceptable in terms of final effluent quality? With MF not retaining all viruses, isn't there a concern over exposure to small viruses? Also, specify what type of limits are being described on page 1-8, line 2.
- c. Section 1.6.1.4 Replace the first sentence with: "This research project tested one MBR product, Zenon Corporations ZenoGem MF system The ZenoGem UF system should be retested at the 10g/L MLSS level. Also, other..."
- d. Section 1.6.1.4: Add to the end of this paragraph: "The Bureau of Reclamation is currently funding Montgomery Watson and the City of San Diego to perform research testing of this type, comparing the performance of ZenoGem and Mitsubishi systems.
- e. Section 1.6.2.1: add the approximate concentration of an aluminum based coagulant to complete the words in parentheses.
- f. Section 1.6.2.2 After the last word, "feasible", add "if the scale control can be resolved as discussed herein."
- 7. Section 2: There are many other RO treatment objectives which the Bureau would like to see listed. As shown in Jim's presentation graphic, these include:
- a. RO Feed: RO feed must be < 2 ntu; SDI<3; and heterotrophic plate count <500 cfu/ml.
- b. McAllen discharge limits: TSS<0.5 mg/L; CBOD5 <10 and NH3-n <3 mg/L.

- c. Reliability of Operation
- d. RO concentrate: Determine the impacts of the RO concentrate.
- 8. Page 3-1: Add consistency so that all figures are called figures and not exhibits.
- 9. Can a vacuum pump be added to Exhibit 3.2?
- 10. Page 3-3, section 3.2.1:
- a. State the complete downtime to the system for the backpulsing that occurs every 10 minutes? State the complete downtime for the maintenance cleans described as at least 75 minutes? Add the total downtime from the backpulsing and the maintenance cleans and clarify if a full scale plant must be slightly oversized to produce a given flowrate (ie plant reliability factor of 90-95%).
- b. Define permeation in the first paragrpah, second to the last line.
- c. To the second paragraph's 9th line: delete the first "membrane" in this line. Also, clarify ..." clean membrane initial level". Is the post-chemically cleaned TMP level reduced to a clean membrane level or restored to a new membrane level.
- 11. Page 3-4, 3rd line: Replace "The RO" with "The thin film composite RO". Section 3.2.3: Change the last sentence to read: This allows for a higher organic loading of wastewater in the treatment system.
- 12. Page 3-5: Specify the micron rating of the cartridge filter in the second line of the second paragraph. Also, in the second paragraph's  $4^{th}$  line, delete the first two "ands". Lastly, can the cleaning skid be shown in Exhibit 3.3?
- 13. Page 3-6: Change the TDS sum of ions values for 12/14 and 12/18 to 1465 and 1473. Also, to the second bullet, state the recommended antiscalent from the Hydranautics program.
- 14. Page 3-8: delete the parentheses in the first line. Also, clarify why in the last line, "Zenogem system" is in parentheses.
- 15. Page 3-9: Define stages A through D.
- 16. Page 4-1: Secton 4-1 item 4: Where in the report are the results of each of these tasks? Where are the air requirements summarized for the process for cleaning and for nutrient consumption?

- 17. Tables 4.1 and 4.2: Clarify under responsible party, what WWTP and WTP really means (ie who)?
- 18. Page 5-7: Add a figure, after Exhibit 5.2, of a complete project timeline that shows both the Zenogem and the RO stages. Then to all of the RO performance figures, modify the timeline hours to match this new complete timeline (ie RO start at 1200 hours instead of 0 hours). This will eliminate confusion arising from the fact that stages A-D differ depending on the equipment.
- 19. Section 5: Can a nitrification rate be determined and added? Also, on Page 5-8, from line 6 replace the second paragraph with:
- Table 5.5 presents the target and average operating conditions for th ZenoGem system during Stage C operation. At the beginning of this stage (after 1,783 hours of operation), the MLSS concentration was decreased to 10 g/L. From 4,130 to 4,158 hours (Event 3) and from 4,225 and 4,326 hours (Event 4) of operation, the permeate flow rate was increased by 46 percent (6.5 to 9.5 gpm) for a period of 6 hours (flow peaking) over a 24-hour period to simulate the types of hydraulic peak loading that typically occur in a conventional wastewater plant. This was done to determine if the MBR system could be operational in the same manner or if additional means would have to be provided to ensure slower changes in the loading to give the MBR time to react to the change in loading. After 4,876 hours of operation, the membrane module height was raised (Event 6) to minimize sludge accumulation in the module aerators during non-aeration periods. From 4,894 to 5,136 hours (Event 7) of operation, air was cycled to the membrane tank at an applied rate of 30 scfm for 10 seconds on and 10 seconds off to evaluate the effect of intermittent aeration on operations and membrane performance. From 5,136 to 5,187 hours
- 20. Page 5-14, Permeability Section: Replace the first paragraph with the following:
- Stages A C. Figure 5.3 illustrates changes in ZenoGem permeability as a function of operating time (TMP is also shown for reference). During Stage B, permeability (normalized to 20°C) steadily decreased as TMP increased, indicating membrane fouling at the higher MLSS concentration of 13 g/L. In contrast, at the lower MLSS concentration in Stage C, permeability increased and remained relatively constant as TMP very gradually increased. However during the flow peaking test periods (Events 3, 4 and 8), permeability sharply decreased as TMP increased. This showed that the MBR system must be provided with a means of ensuring slower changes in peak loading. The peak loading can not be raised as quickly over a 24 hour period as fast as a conventional wastewater treatment plant. These results also confirm that ZenoGem operation at 10 g/L MLSS concentration and constant flux provides

for very stable system operation.

- 21. Page 5-48, last paragraph: State why no useful data was obtained from the instruments. Section 5.3.3, RO Water Quality Impacts: Add to this section the table of RO manufacturer's membrane information and data, which Jim had shown in the presentation.
- 22. Page 5-50, section 5.4: Elaborate what is said in the very last paragraph. Define mass loading basis and be very specific here so non-technical readers can understand what is being concluded.
- 23. Page 5-51, section 5-5: change existing to exist in 1kine 1. Also, delete the s on parameters in line 7. Lastly add conclusions for the data being displayed in Table 5-16 and for any blending being contemplated.

### 24. Cost Section 6:

- a. Add text describing the overall conclusions of that can be derived from this study. Would a MBR system be cost effective or not, and under what conditions?
  - b. What labor rate was used in the cost estimates?
- c. Clarify if the costs presented are based to a certain month/year.
  - d. Where is the square footage of the building?

Bob Jurenka'- Re: RE: McAllen Integrity Report Status

Pagn 1

From:

**Bob Jurenka** 

To:

ibr8dm00;jlozier@[CH2M.com]

Date:

Fri, Feb 25, 2000 1:12 PM

Subject:

Re: RE: McAllen Integrity Report Status

Jim: Michelle is wrapping up the integrity report, having received internal review comments.

After receiving the final McAllen report, here are 4 final review comments which will need clarification. After you read these, lets discuss how best to finalize the report.

-1. Table 6.1: It is not clear why the Zenogem process needs 1.3M of new tankage.

2. Table 6.1: The economic analysis says @ 6.5% was the rate used. My tables of A/P values show a 7 % value was used.

3. Table 6.1: The total unit cost of \$2.10 per 1,000 is questioned. Explain how this was derived and not 1.98/1000 gallons.

4. Page 6-9, 3rd sentence: Provide more details to better justify the costs associated for new tankage, and the difference between \$1.3M vs \$0.1M for zeeweed.

Thanks

PS: We are still looking at ways to assist with autopsy work for Sherman. Hope the knee is doing better.

Bob Jurenka, 303 445-2254

### Fernandez, Angie/PHX

From:

Fboudkirk@cs.com

િ nt:

December 20, 1999 12:32 PM

Afernand@ch2m.com

Subject:

McAllen

Angie,

Here are a few editorial comments on the December 7, draft report. Bear in mind that the EPRI folks who take the time to read it will be starting from ground zero and the don't know ZeeWeed from break tank.

Page 1-1, UV is mentioned here but nowhere else in the report. I suggest deleting these references to UV as the project did not address its use.

Page 1-3 first paragraph; for the sake of current info, the San Vincente Reservoir recharge project was killed because of politics. It might be resurrected but as of August, 1999 the politicians killed it claiming it was an Anglo plot to make Hispanics drink dirty water!

Page 3-2. Somewhere we need to have a glossary for abbreviations like CIP. I know what it means but a person not informed about membranes might not. Also the term break tank is not is not self explanatory. On this page we have labeled an aerobic tank in the diagram while in the text a "aeration tank" is mentioned as well as "a 200 gallon calibrated receiving tank." These descriptions should be consistent with the diagram.

eye 3-3. In the first and second paragraphs a "process tank" is mentioned. I eye the words "membrane tank" should be used for consistency's sake. Also in the second paragraph it might be helpful to mention that the maintenance cleaning flush liquid is drained to waste.

The last sentence of this paragraph might confuse a first time reader as it seems to imply that maintenance cleaning is not a part of "normal" operation. I would suggest the sentence read "Maintenance cleaning is done insitu and is necessary to sustain the membrane flux." (Is it insitu or in situ?)

Page 3-4, I think adding the words "For pilot testing" to the beginning of the last sentence of the first paragraph sentence would avoid confusion about how a full-scale system would operate. The terms CBOD5, MLSS, MLVSS, SRT, etc., show the need for a glossary.

Page 3-5, The pore size of the cartridge filter would be informative as would be a few words about why the filter is required.

Page 3-6, I believe the samples were taken in 1998 not 1999 as the charts says.

Page 4-4, Again, since my audience is made up mainly of power plant types who are given job assignments outside their technical field of expertise, I would prefer the last sentence of the first paragraph of section 4.33 to "could adversely affect marine ecology." If that is indeed what we mean.

Page 4-5, ASL should be define in a glossary.

r age 5-18, Here we introduce an other CBOD term which I think is the same as CBOD5. If not it needs to be define in a glossary.

Page 5-20, Ditto for BOD5.

Page 5-52, Some explanation why some chemical element levels in the ZenoGem Permeate are higher than in the raw water would be helpful. Could these be a seasonal variation?

### **ATTACHMENT 1**

Texas Water Development Board Review Comments: City of McAllen Contract No. 99-483-276

Board Staff offers the following comments.

The study shows that effluent, and especially effluent with high hardness and high total dissolved solids, can be brought to drinking water standards for between \$1.24 and \$1.80 per thousand gallons. The study shows that using the Zenon technologies tested, that existing wastewater treatment plant capacities could be significantly increased (doubled or tripled) at costs similar to new plants (under \$1.5 per gallon/day of capacity). Savings may be realized by removing the possible impediments of new construction such as site location and additional distribution lines by utilizing the Zenon technology in existing wastewater treatment plants. The report also shows that Zenon technology can produce a higher quality treated effluent.

### Specific recommended changes to the report include:

- 1. Table 5.16 should be modified so that applicable safe drinking water act criteria are included in the table for reference.
- 2. The summary tables of water quality parameters compared to target values shown in the overheads at the Denver meeting should be included in the summary of this report.
- 3. The cost for the micro filtration process, including costs in dollars per thousand gallons should be broken out separately from the RO costs in Chapter 6.
- 4. 4.4.2 Sampling and Analysis: 1st paragraph, 3rd sentence (The WWTP....) mentions one of the samples collected is nitrate/nitrate nitrogen. This is redundant. This should be changed to read nitrate/nitrite nitrogen.
- 5. The Texas Water Development Board should be acknowledged as helping to fund this study.



### RECEIVED

JAN 2 4 2000

January 18, 2000

149462.A1.RP

TWOB REPF

**GRANTS MANAGEMENT** 

CH2M HILL

1620 W. Fountainhead Parkway

Suite 550

Tempe, AZ

85282-1843

P.O. Box 28440

Tempe, AZ

85285-8440

Tel 602.966.8188

Fax 602.966.9450

Proud Sponsor of

National Engineers Week 2000

Mr. Robert Jurenka, P.E. Grants and Cooperative Agreements Officer's Technical Representative Stop D-8230 Bureau of Reclamation Denver Federal Center Building 67 at 7th Street Denver, CO 80225

Dear Bob:

Subject: Transmittal of Final Technical Report

On behalf of the City of McAllen, Texas and in accordance with the Cooperative Agreement No. 98FC810073 entitled "Demonstation Testing of ZenoGem and Reverse Osmosis for Indirect Potable Water Reuse - City of McAllen, Texas", please find enclosed five (5) bound copies of the Final Technical Report, one unbound copy, and an electronic copy on compact disk in Word 97 format.

Sincerely,

CH2M HILL

Principal Investigator

Enclosures:

Final Technical Report (5 bound copies; 1 unbound copy)

Compact Disk

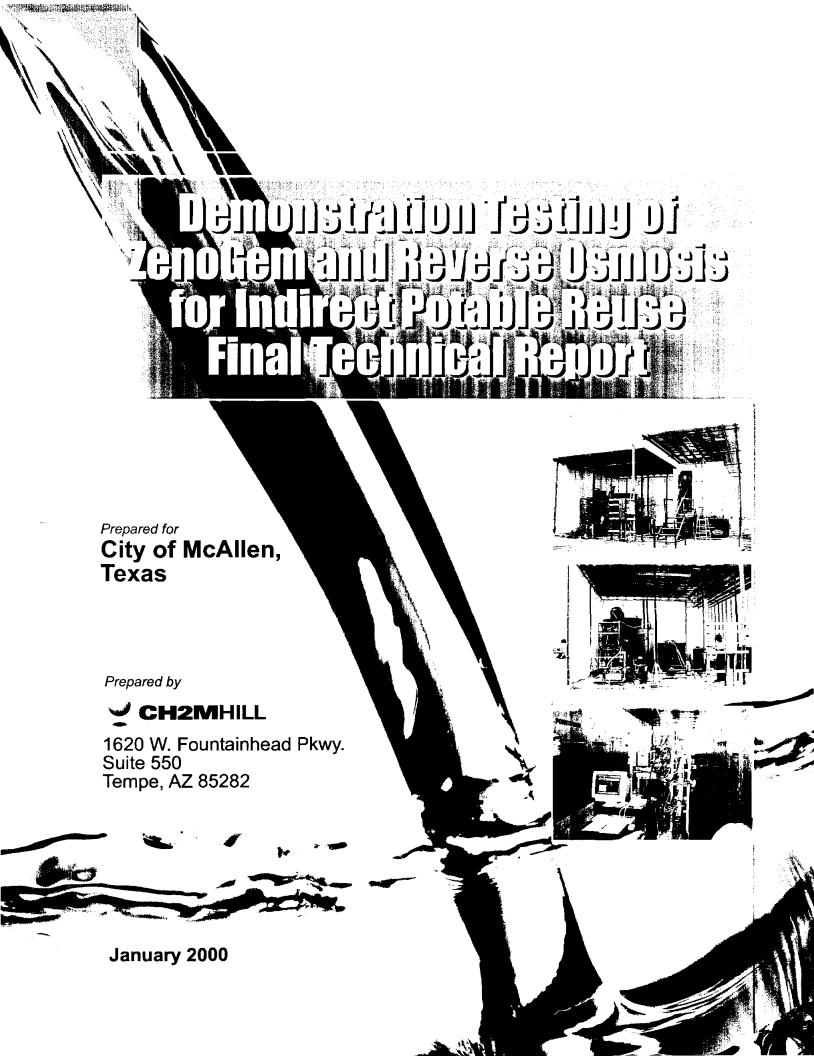
Cc:

Bart Hines/City of McAllen

Frank Oudkirk/EPRI Bud Clark/C&SWS Bill Hoffman/TWDB

Doreen Benson/ZENON Environmental Systems

Mike Anglea/CH2M HILL/SAN Angie Fernandez/CH2M HILL/PHX Glen Daigger/CH2M HILL/DEN



REPORT DOCUMENTATION PAGE			Form Approved OMB No. 0704-0188	
aintaining the data needed, and completing aggestions for reducing this burden to Was	ng and reviewing the collection of information. Send	d comments regarding this burden estimate of ormation Operations and Reports, 1215 Je	nstructions, searching existing data sources, gathering an or any other aspect of this collection of information, includin fferson Davis Highway, Suit 1204, Arlington VA 22202-4307	
1. AGENCY USE ONLY (Leave Blank)	2. REPORT NATE January 2000	3. REPORT TYPE AND BATES Final	COVERED	
4. TITLE AND SUBTITLE			5. FOUDING NUMBERS	
Demonstration Testing of Ze of McAllen, Texas	noGem and Reverse Osmosis for	Indirect Potable Reuse, City		
<b>6. AUTHORIS)</b> Jim C. Lozier and Angela M	. Fernandez			
7. PERFORMING ORGANIZATION NAME(S		<u> </u>	8. PERFORMING ORGANIZATION	
CHOM HILL			REPORT NUMBER	
CH2M HILL 1620 W. Fountainhead Parky	way Suite 550			
Tempe, Arizona 85282-184	Desalination Research and Development Program Report No. 51			
9. SPONSORME/MONITORING AGENCY	NAME(S) AND ADDRESS(ES)		10. SPĖNSERINE/MONITORINE	
Bureau of Reclamation			AGENCY REPORT NUMBER	
Denver Federal Center P.O. Box 25007				
Denver, Colorado 80225-00	007			
11. SUPPLEMENTARY NOTES				
os. DISTRIBUTION/AVAILABILITY STAT	TEMENT		12h. DISTRIBUTION CODE	
Available from the National 5285 Port Royal Road, Sprin	Technical Information Service, Ongfield, Virginia 22161	perations Division,		
to reclaim the City of McAll demonstration testing object drinking water regulations, (to control of membrane foul processed by composite RO MBR/RO system. The resul while meeting the City's cur filtrate that meets all drinkin	tration-scale testing of an integrate en's municipal wastewater to a quives include: (1) demonstration the 2) demonstrate reliable operationing through automatic cleaning, (3) membranes with minimal fouling, ts showed that (1) the ZenoGem p	pality suitable for use as a new mat RO product water meets all of the MBR on screened, deg B) demonstrate the MBR filtra, and (4) develop estimates of process is capable of producing requirements, and (2) the RO	Il federal primary and State secondary ritted sewage, particularly with respect te (RO feedwater) can be efficiently capital and operating costs for a g a filtrate suitable for RO treatment 0 system is capable of producing a nbrane cleanings.	
14. SUBJECT TERMS— wastewater reclamation; McAllen, Texas; ZenoGem; ZeeWeed; reverse osmosis; microfiltra			ation;	
membrane technology; indirect potable reuse; sewage			16. PRICE CODE	
17. SECURITY CLASSIFICATION OF REPORT	18. SECURITY CLASSIFICATION OF THIS PAGE	19. SECURITY CLASSIFICATION OF ABSTRACT	20. LIMITATION OF ABSTRACT	
I II	III	TIT.	Iπ	

Standard Form 298 (Rev. 2-89)

# DEMONSTATION TESTING OF ZENOGEM AND REVERSE OSMOSIS FOR INDIRECT POTABLE REUSE

## FINAL TECHNICAL REPORT

City of McAllen, TX

by

James C. Lozier, P.E. and Angela M. Fernandez, E.I.T CH2M HILL

Cooperative Assistance Agreement No. 98-FC-81-0073

Desalination Research and Development Program Report No. 51

January 2000

U.S. DEPARTMENT OF THE INTERIOR

Bureau of Reclamation

Technical Service Center

Water Treatment Engineering and Research Group

#### Mission Statements

### U.S. Department of the Interior

The mission of the Department of the Interior is to protect and provide access to our Nation's natural and cultural heritage and honor out trust responsibilities to tribes.

### Bureau of Reclamation

The mission of the Bureau of Reclamation is to manage, develop, and protect water and related resources in an environmentally and economically sound manner in the interest of the American public.

### Federal Disclaimer

The information contained in this report regarding commercial products of firms may not be used for advertising or promotional purposes and is not to be construed as an endorsement of any product or firm by the Bureau of Reclamation.

The information contained in this report was developed for the Bureau of Reclamation: no warranty as to the accuracy, usefulness, or completeness is expressed or implied.

### Researcher Acknowledgments

The authors would like to thank the Bureau of Reclamation (Bob Jurenka, Michelle Chapman-Wilbert, and Kim Linton), Texas Water Development Board (Bill Hoffman), Electric Power Research Institute (Frank Oudkirk), and Central and Southwest Energy Services (Bud Clark and Lance Orner) for sponsoring this research.

The authors would also like to thank the City of McAllen, Texas, specifically: Bart Hines, Public Utility Manager, and his Board for their finanical and management support; Joe Ibarra, Rey Palomo, Henry Perez and Javier Hinojosa and others at the South WWTP for their assistance in construction, operation, and maintenance of the demonstration plant facilities; and Rosie Villarreal, Ramon Trevino, David Garcia, Juan Morales and their respective staff for sample analysis.

#### Researcher Disclaimer

The information contained in this report regarding the performance of tested commercial products and the conclusions and recommendations drawn regarding such performance are based on testing conducted on wastewater sources from the City of McAllen, Texas, and are not to be considered an indication of the performance of such products on other water sources either at McAllen, Texas, or at other locations.

### **Bureau Point of Contact**

The Bureau of Reclamation's Water Reuse Task Manager for this work is Robert Jurenka. He can be reached in Denver at (303) 445-2254.

# **Contents**

Sect	Section		Page
1	Intro	oduction and Background	1-1
	1.1	Indirect Potable Reuse—Definition and History	1-1
	1.2	The Need for Indirect Potable Reuse for the City of McAllen	1-4
	1.3	Water Quality Considerations and Proposed Treatment Strategy	1-5
	1.4	Membrane Technologies in Indirect Potable Reuse	
	1.5	Conclusions	1-6
		1.5.1 ZenoGem System	1-6
		1.5.2 RO System	
	1.6	Recommendations for Further Research	1-9
		1.6.1 Membrane Bioreactors	1-9
		1.6.2 Reverse Osmosis	1-10
2	Testi	ing Objectives	2-1
3		onstration Plant Facilities	
	3.1	Raw Water Supply, Abstraction, Pumping, and Screening	
	3.2	ZenoGem Treatment System	
		3.2.1 Methods to Control ZeeWeed Membrane Fouling	
		3.2.2 Permeate Storage, Disinfection, and Pumping	
		3.2.3 ZenoGem Operation	
	3.3	RO Treatment System	
		3.3.1 RO Feedwater Characterization	
		3.3.2 RO Feedwater Pretreatment to Control Membrane Fouling.	
	3.4	Criteria for Treatment System Operation	
4	Test	ing Approach	
	4.1	ZenoGem Treatment System Tasks	
	4.2	RO Treatment System Tasks	4-2
	4.3	Additional Testing Activities	
		4.3.1 RO Feedwater Characterization	
		4.3.2 IPR Characterization	
		4.3.3 RO Concentrate and WWTP Effluent Characterization	
		4.3.4 RO Integrity Testing	
	4.4	Treatment System Monitoring	
		4.4.1 Operator Training	
		4.4.2 Sampling and Analysis	
	4.5	Data Evaluation	<b>4-</b> 8
		4.5.1 Filtrate Flow and Membrane Flux	
		4.5.2 Transmembrane Pressure and Permeability	
		4.5.3 Turbidity and SDI	4-9

	on	Page
5	Demonstration Testing Results	5-1
	5.1 Operations	5-1
	5.1.1 Startup Activities	5-3
	5.1.2 Operating Stages	
	5.2 ZenoGem Testing Results	5-7
	5.2.1 ZenoGem Operating Conditions	5-7
	5.2.2 ZeeWeed Membrane Performance	5-11
	5.2.3 ZenoGem Biological Treatment Performance	5-15
	5.2.4 ZenoGem Water Quality Impacts	5-22
	5.3 RO Testing Results	5-37
	5.3.1 RO Feedwater Quality	5-37
	5.3.2 RO Operating Conditions/Membrane Performance	5-39
	5.3.3 RO Water Quality Impacts	
	5.4 Impacts of IPR on Waste Discharges	
	5.5 Comparing Reclaimed and Existing Raw Water Quality	
	Cost Estimates Using ZenoGem, ZeeWeed, and RO Facilities	6-1
	6.1 Cost Assumptions	
	6.2 Cost Estimates	6-3
	References	7-1
.1	Results of RO Feedwater Characterization	
3.2	Operating Criteria for the ZenoGem System	3-8
.3	Biological Treatment Performance Criteria for the ZenoGem System	
		3-9
	Operating Criteria for the RO System	3-9 3-9
	Operating Criteria for the RO SystemBiological Treatment and Water Quality Sampling Schedule for the ZenoGerr	3-9 3-9 ì
.1	Operating Criteria for the RO System	3-9 3-9 1
1	Operating Criteria for the RO System  Biological Treatment and Water Quality Sampling Schedule for the ZenoGer System  Water Quality Sampling Schedule for the RO System	3-9 3-9 4-6 4-8
1 2 1	Operating Criteria for the RO System  Biological Treatment and Water Quality Sampling Schedule for the ZenoGer System  Water Quality Sampling Schedule for the RO System  Operating Stages and Events for the ZenoGem System	3-94-64-85-1
.1 .2 .1	Operating Criteria for the RO System  Biological Treatment and Water Quality Sampling Schedule for the ZenoGerr System  Water Quality Sampling Schedule for the RO System  Operating Stages and Events for the ZenoGerr System  Operating Stages and Events for the RO System	3-9 1 1 4-64-65-1
1 2 1 2 3	Operating Criteria for the RO System Biological Treatment and Water Quality Sampling Schedule for the ZenoGer System Water Quality Sampling Schedule for the RO System Operating Stages and Events for the ZenoGem System Operating Stages and Events for the RO System Stage A Average Operating Conditions for the ZenoGem System	3-9 14-64-85-15-2
.1 .2 .1 .2 .3 .4	Operating Criteria for the RO System  Biological Treatment and Water Quality Sampling Schedule for the ZenoGerr System  Water Quality Sampling Schedule for the RO System  Operating Stages and Events for the ZenoGerr System  Operating Stages and Events for the RO System  Stage A Average Operating Conditions for the ZenoGerr System  Stage B Average Operating Conditions for the ZenoGerr System	3-9 14-65-15-75-8
.1 .2 .1 .2 .3 .4	Operating Criteria for the RO System  Biological Treatment and Water Quality Sampling Schedule for the ZenoGerr System  Water Quality Sampling Schedule for the RO System  Operating Stages and Events for the ZenoGerr System  Operating Stages and Events for the RO System  Stage A Average Operating Conditions for the ZenoGerr System  Stage B Average Operating Conditions for the ZenoGerr System  Stage C Average Operating Conditions for the ZenoGerr System	3-94-64-85-15-25-75-8
.1 .2 .1 .2 .3 .4	Operating Criteria for the RO System Biological Treatment and Water Quality Sampling Schedule for the ZenoGer System Water Quality Sampling Schedule for the RO System Operating Stages and Events for the ZenoGem System Operating Stages and Events for the RO System Stage A Average Operating Conditions for the ZenoGem System Stage B Average Operating Conditions for the ZenoGem System Stage C Average Operating Conditions for the ZenoGem System Stage D (Alternative Operating Mode) Average Operating Conditions for the	3-9 14-65-15-75-8
1 2 1 2 3 4 5 6	Operating Criteria for the RO System Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System Water Quality Sampling Schedule for the RO System Operating Stages and Events for the ZenoGem System Operating Stages and Events for the RO System Stage A Average Operating Conditions for the ZenoGem System Stage B Average Operating Conditions for the ZenoGem System Stage C Average Operating Conditions for the ZenoGem System Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGem System	3-9 14-65-15-25-85-9
.1 .2 .1 .2 .3 .4 .5	Operating Criteria for the RO System  Biological Treatment and Water Quality Sampling Schedule for the ZenoGerr System  Water Quality Sampling Schedule for the RO System  Operating Stages and Events for the ZenoGerr System  Operating Stages and Events for the RO System  Stage A Average Operating Conditions for the ZenoGerr System  Stage B Average Operating Conditions for the ZenoGerr System  Stage C Average Operating Conditions for the ZenoGerr System  Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGerr System  Results of Biological Treatment Performance Analyses for the ZenoGerr System	3-94-65-15-75-95-10 em .5-15
.1 .2 .3 .4 .5 .6	Operating Criteria for the RO System Biological Treatment and Water Quality Sampling Schedule for the ZenoGer System Water Quality Sampling Schedule for the RO System Operating Stages and Events for the ZenoGem System Operating Stages and Events for the RO System Stage A Average Operating Conditions for the ZenoGem System Stage B Average Operating Conditions for the ZenoGem System Stage C Average Operating Conditions for the ZenoGem System Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGem System Results of Biological Treatment Performance Analyses for the ZenoGem System Results of Stages A and B Water Quality Analyses for the ZenoGem System.	3-9 14-65-15-75-85-9 em .5-15
5.1 5.2 5.3 5.4 5.5 5.6 5.7 5.8 5.9	Operating Criteria for the RO System Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System Water Quality Sampling Schedule for the RO System Operating Stages and Events for the ZenoGem System Operating Stages and Events for the RO System Stage A Average Operating Conditions for the ZenoGem System Stage B Average Operating Conditions for the ZenoGem System Stage C Average Operating Conditions for the ZenoGem System Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGem System Results of Biological Treatment Performance Analyses for the ZenoGem System Results of Stages A and B Water Quality Analyses for the ZenoGem System Results of Stage C Water Quality Analyses for the ZenoGem System	3-94-65-15-75-95-105-225-23
1.1 1.2 5.1 5.2 5.3 5.4 5.5 5.6 5.7 5.8 5.9	Operating Criteria for the RO System Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System Water Quality Sampling Schedule for the RO System Operating Stages and Events for the ZenoGem System Operating Stages and Events for the RO System Stage A Average Operating Conditions for the ZenoGem System Stage B Average Operating Conditions for the ZenoGem System Stage C Average Operating Conditions for the ZenoGem System Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGem System Results of Biological Treatment Performance Analyses for the ZenoGem System Results of Stages A and B Water Quality Analyses for the ZenoGem System Results of Stage C Water Quality Analyses for the ZenoGem System Results of Stage D (Alternative Operating Mode) Water Quality Analyses for	3-9 14-64-85-15-75-85-95-10 em .5-155-225-23 the
3.4 4.1 5.2 5.3 5.4 5.5 5.6 5.7 5.8 5.9 5.10	Operating Criteria for the RO System Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System Water Quality Sampling Schedule for the RO System Operating Stages and Events for the ZenoGem System Operating Stages and Events for the RO System Stage A Average Operating Conditions for the ZenoGem System Stage B Average Operating Conditions for the ZenoGem System Stage C Average Operating Conditions for the ZenoGem System Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGem System Results of Biological Treatment Performance Analyses for the ZenoGem System Results of Stages A and B Water Quality Analyses for the ZenoGem System Results of Stage C Water Quality Analyses for the ZenoGem System	3-9 14-65-15-75-85-95-225-23 the5-24

### TABLES CONT.

5.13 5.14	Average Membrane Performance Parameters for the RO System	
5.15	Comparative Loading of Critical Contaminants to Arroyo Colorado/ Laguna Madre	
5.16	Results of ZenoGem and RO Permeate Sampling for IPR Characterization	5-54
6.1	Order of Magnitude Cost Estimate for The ZenoGem and RO Alternative.	6-4
6.2	Order of Magnitude Cost Estimate for the ZeeWeed and RO Alternative	
6.3	Design Criteria Assumptions for the ZenoGem, ZeeWeed and RO Systems	
EXHII	BITS	
5.1	ZenoGem Operating Stages	5-4
5.2	RO Operating Stages	
5.3	Wastewater Discharge Characterization	5-50
FIGU	RES	
3.1	Demonstration Plant Feedwater Abstraction Point from WWTP No. 2	3-1
3.2	ZenoGem Treatment System Process Flow Diagram	
3.3	RO Treatment System Process Flow Diagram	
6.1	Existing WWTP Schematic	
6.2	ZenoGem Membrane Bioreactor and RO Facilities	
6.3	Conventional WWTP with ZeeWeed and RO Facilities	6-2
Zeno	Gem System	
5.1	Permeate Flowrate and Membrane Flux vs. Run Time	5-13
5.2	Transmembrane Pressure and Permeate Flowrate vs. Run Time	5-13
5.3	Normalized Membrane Permeability and Transmembrane Pressure vs.	
	Run Time	5-14
5.4	Hydraulic Residence Time vs. Run Time	
5.5	Solids Retention Time vs. Run Time	
5.6	Mixed Liquor Suspended Solids vs. Run Time	5-19
5 <i>.</i> 7	Mixed Liquor Volatile Suspended Solids vs. Run Time	5-19
5.8	Dissolved Oxygen vs. Run Time	
5.9	Oxygen Uptake Rate vs. Run Time	
5.10	Total Suspended Solids vs. Run Time	
5.11	5-Day Carbonaceous Biochemical Oxygen Demand vs. Run Time	
5.12	Chemical Oxygen Demand vs. Run Time	
5.13	Permeate Turbidity vs. Run Time	
5.14	Permeate Total and Fecal Coliforms vs. Run Time	
5.15	Ammonia Nitrogen vs. Run Time	
5.16	Percent Ammonia Nitrogen Removal vs. Run Time	
5.17	Nitrite/Nitrate Nitrogen vs. Run Time	
5.18	Total Nitrogen vs. Run Time	
5.19	Percent Total Nitrogen Removal vs. Run Time	

# **Acronyms and Abbreviations**

ACOE Army Corps of Engineers

ALK alkalinity

ASL Applied Sciences Laboratory

bio-P biological phosphorus

BOD biochemical oxygen demand BOR Bureau of Reclamation

C celsius

CBOD, carbonaceous biochemical oxygen demand

cfm cubic feet per minute CFU colony forming units

CIP clean in place

COD chemical oxygen demand CST capillary suction time

CSWS Central and Southwest Services

DO dissolved oxygen

DSVI diluted sludge volume index
EPA Environmental Protection Agency
EPRI Electric Power Research Institute

 $\begin{array}{ll} \text{ft}^2 & \text{square feet} \\ \text{g/L} & \text{grams per liter} \end{array}$ 

GAC granular activated carbon gfd gallons per square foot per day

gpd gallons per day gpm gallons per minute HAA haloacetic acid

HPC heterotrophic plate count
HRT hyraulic residence time
I&C instrumentation and controls

in Hg inches of mercury
IPR indirect potable reuse
KLT King Lee Technologies
MBR membrane bioreactor

MCL maximum contaminant level

MF microfiltration
mg/L milligrams per liter
mgd million gallons per day

mL milliliters
ML million liters

MLSS mixed liquor suspended solids

MLVSS mixed liquor volatile suspended solids

mm millimeter
N nitrogen

NH₃-N ammonia nitrogen

NPF normalized product flow
NTU nephelometric turbidity unit
O&M operations and maintenance

OUR oxygen uptake rate

P phosphorus

pCi/L picoCuries per liter
PDC pressure drop coefficient
PLC programmable logic controller

ppm parts per million

psi pounds per square inch

psig pounds per square inch gauge

RO reverse osmosis

scfm standard cubic feet per minute

SDI silt density index

SDS screened degritted sewage SDWA Safe Drinking Water Act

SI solubility index
SRT solids retention time
TDS total dissolved solids
THM trihalomethane

TKN total Kjeldahl nitrogen
TMP transmembrane pressure

TN total nitrogen

TNRCC Texas Natural Resources Conservation Committee

TOC total organic carbon
TP total phosphorus
TSS total suspended solids

TWDB Texas Water Development Board

UF ultrafiltration

UOSA Upper Occoquan Sewage Authority

UV ultraviolet

μg/L micrograms per liter

μm microns

μS/cm microSiemens per centimeter
WWTP wastewater treatment plant

# Introduction and Background

This report documents wastewater reclamation demonstration testing performed at the McAllen, Texas, wastewater treatment plant (WWTP) No. 2. The study was conducted under Task D: Water Recycling and Reuse of the U.S. Bureau of Reclamation's (BOR) Desalination Research and Development Program. The Program sponsors this research in an effort to lower the cost of treatment technologies. Testing was conducted from February 1999 to October 1999.

The results of previous pilot testing conducted for the City of McAllen (*Water Treatment Technology Program Report No. 26*) concluded that treating the City's wastewater with a membrane bioreactor (MBR) system (ZenoGem) followed by reverse osmosis (RO) and final disinfection (chlorination or ultraviolet [UV] light) may provide for a simpler, potentially less costly, treatment process for the reclamation of a portion of the City's wastewater to supplement current water supplies obtained from the Rio Grande River. The reclaimed water produced by the MBR/RO/disinfection process would in most respects contain significantly lower concentrations of most substances currently regulated under the Safe Drinking Water Act (SDWA), and as such, could improve the inorganic quality of the Rio Grande River water. However, unlike microfiltration (MF), which has been used extensively for RO pretreatment of secondary effluent, no testing has been reported on the use of the ZenoGem process to convert wastewater directly to RO feedwater for the purpose of producing a high quality effluent suitable for indirect potable reuse.

The purpose of this study was threefold: 1) to demonstrate the long-term operability and reliability of the ZenoGem system, 2) demonstrate the feasibility of RO treatment of ZenoGem permeate for the production of reclaimed water, and 3) determine if the MBR/RO process has operational, cost, and water quality benefits compared to the conventional WWTP/MF/RO in the context of indirect potable reuse (IPR).

This section addresses the following information:

- Defines indirect potable reuse.
- Explains the City of McAllen's motivations for considering implementation of indirect potable reuse to help solve their water supply problems.
- Describes the regulatory issues associated with implementation, and explains the reasons membrane processes, in particular MF/ultrafiltration (UF) and RO, are integral to its implementation.
- Presents conclusions and recommendations from this study.

## 1.1 Indirect Potable Reuse—Definition and History

Indirect potable reuse is the recovery of water from wastewater for the purposeful reintroduction into either a surface water or groundwater body that ultimately serves as a drinking water supply. Unplanned IPR has been occurring since humans first began disposing of wastewater into watersheds that are hydrologically connected to raw water supplies. Planned IPR began in the U.S. in the 1960s. A summary of some of the major milestones in the development of potable reuse as a viable component of a water resource management plan is presented below.

The Whittier Narrows Groundwater Replenishment Project, California. In 1962, the County Sanitation Districts of Los Angeles began spreading disinfected secondary effluent from a 10-million-gallon-per-day (mgd) (37.9 million liters [ML]/day) water reclamation plant to an underground potable water supply. The reclaimed water accounts for an annual average of 16 percent of the total inflow to the groundwater basin. The local population is estimated to be exposed to from 0 to 23 percent reclaimed water. An independent scientific advisory panel to the State of California conducted an extensive review of the project data and concluded that the Whittier Narrows Groundwater Replenishment Project was as safe as commonly used surface water supplies.

Orange County, California, Water District. Since 1976, the Orange County, California, Water District's Water Factory 21 has been reclaiming unchlorinated secondary effluent to drinking water quality and recharging it into a heavily used groundwater source to prevent salt water intrusion. The water recovery treatment facility is a 15-mgd (56.8 ML/day) facility that includes lime clarification, air stripping, recarbonation, filtration, carbon adsorption, slip-stream RO, and disinfection. It is estimated that less than 5 percent of the domestic water supply is comprised of the recovered water. The Orange County Water District has not identified any significant risk to users of the groundwater from the indirect potable reuse practice.

Upper Occoquan Sewage Authority Water Reclamation Plant, Virginia. In 1978, the 15-mgd Upper Occoquan Sewage Authority (UOSA) Water Reclamation Plant in northern Virginia began reclaiming wastewater for subsequent discharge to the Occoquan Reservoir. This reservoir is a critical source of drinking water for approximately 1 million people. The reclaimed water has accounted for as much as 90 percent of the flow into the reservoir. Treatment includes primary treatment, secondary treatment, biological nitrification, lime clarification and recarbonation, filtration, activated carbon adsorption, and disinfection. The plant has been expanded to 26 mgd (98.4 ML/day) and will be further expanded to 54 mgd (204 ML/day) by the year 2000. No negative health effects have been attributed to the plant or effluent discharges.

Potomac Estuary Experimental Water Treatment Plant, Washington, D.C. From 1981 to 1983, the 1-mgd (3.8 ML/day) Potomac Estuary Experimental Water Treatment Plant was operated with an influent blend of Potomac Estuary water and nitrified secondary effluent. The blend was designed to simulate influent water quality expected during drought conditions when up to 50 percent of the estuary flow may comprise treated wastewater. Treatment included aeration, coagulation, clarification, pre-disinfection, filtration, carbon adsorption, and post-disinfection. An independent panel reviewed the extensive testing performed by the U.S. Army Corps of Engineers (ACOE) and concluded that the advanced treatment could recover water from a highly contaminated source similar in quality to three major water supplies for the Washington, D.C., metropolitan area.

San Diego Total Resource Recovery Project, California. In 1983, a 1-mgd potable water recovery demonstration facility was commissioned as part of a total resource recovery

program established in San Diego, California. The purpose of the treatment system was to reclaim raw water from raw wastewater. The system included primary treatment, a water hyacinth aquaculture system, coagulation, clarification, filtration, UV disinfection, RO, aeration, carbon adsorption, and disinfection. An extensive chronic toxicity risk analysis showed that the risk associated with use of the recovered water as a raw water supply was less than or equal to the use of the existing raw water entering the City's Miramar Water Treatment Plant. The City is now planning to reclaim up to 20 mgd (75.7 ML/day) of secondary effluent for augmentation of their 90,000 acrefoot San Vicente Reservoir for eventual distribution to water customers.

El Paso, Texas, Fred Hervey Water Reclamation Plant. The 10-mgd (37.9 ML/day) Fred Hervey Water Reclamation Plant began operation in El Paso, Texas, in 1985. The recovered water is recharged to the Hueco Bolson drinking water aquifer where, over a 2-year period, the water travels to one of El Paso's potable water wellfields to become part of the potable water supply. The treatment system includes primary treatment, activated sludge/powdered activated carbon treatment, lime treatment, recarbonation, filtration, ozonation, and granular activated carbon (GAC) adsorption. Although no negative health effects have been correlated with the reuse practice, an increase in the total dissolved solids (TDS) content of the aquifer has occurred because the increased pumping has lowered the aquifer level to the higher salinity water source. Slip-stream demineralization will be included in future plant expansions to address the TDS issue.

Tampa Water Resource Recovery Project, Florida. The City of Tampa's Water Resource Recovery Pilot Plant began operation in 1986 with the purpose of evaluating the feasibility of reclaiming denitrified secondary effluent to a quality suitable for blending with existing surface water and groundwater sources for indirect potable reuse. Several treatments were evaluated, and one was selected for health effects testing. This treatment system consisted of aeration, high pH lime clarification, recarbonation, filtration, GAC adsorption, and ozonation. The results of the health effects testing coupled with the microbiological and chemical analyses performed during the evaluation indicated that the quality of the reuse water was equivalent to or exceeded the quality of the local raw water supply. The City of Tampa intends to develop a 20- to 50-mgd (189 ML/day) water resource recovery plant in the near future.

West Basin Water Recycling Program, California. From 1990 through 1995, the West Basin Municipal Water District conceived, designed, constructed, and began operation of the West Basin Water Recycling Program. This program includes reclaiming 5 mgd (18.9 ML/day) (expandable to 20 mgd, or 75.7 ML/day) of secondary effluent from the City of Los Angeles' Hyperion Treatment Plant for injection into the West Coast Basin Barrier Project. The West Coast Basin Barrier Project has historically received an average of 20 mgd of potable water for injection into the coastal reaches of local South Bay aquifers for mitigation of saltwater intrusion. Substituting reclaimed water for the potable water provides substantially greater water use efficiency in the area. Reclamation treatment includes predecarbonation, lime clarification, recarbonation, filtration, RO, postdecarbonation, and final disinfection. Based on hydrogeologic investigation and modeling of the West Coast Basin, it is anticipated that the reclaimed water will improve groundwater quality along the Barrier because of the high quality of the reclaimed water relative to the imported water and the native groundwater.

Reedy Creek Improvement District, Advanced Water Reclamation Program, Florida. In 1992, the Reedy Creek Improvement District began a pilot program to reduce phosphorus (P) and nitrogen (N) in the effluent from their WWTP to very low levels. Although the goal of treatment was not IPR, this was the first project to evaluate the feasibility of using MF and UF as a replacement to lime clarification, recarbonation, and gravity filtration for RO pretreatment. This approach was shown to be so effective that MF and UF have displaced lime treatment as the preferred means of RO pretreatment on subsequent IPR projects.

City of Scottsdale, Arizona, Water Campus Project. In 1994, the City of Scottsdale began pilot testing MF and RO for the purpose of reclaiming wastewater for ground-water recharge. The testing program, which has culminated in a 6.8-mgd (25.7 ML/day) IPR project currently under construction at the City's Water Campus site, represents the first planned IPR project in Arizona. During periods when demand for non-potable reclaimed water is low, product water from the MF/RO system will be blended with filtered surface water and injected into a potable aquifer using dry wells. The 6.8-mgd facility represents the first phase of a multi-year project designed to have an ultimate capacity of 25 mgd (94.6 ML/day).

City of San Diego, California, Water Repurification Project. As an outgrowth of their Total Resource Recovery Project, the City of San Diego began the Repurification Project to reclaim up to 20 mgd of wastewater for indirect potable use. The program is currently evaluating the feasibility of using the following advanced water treatment processes to re-purify tertiary effluent from the City's new North City Water Reclamation Plant to a quality suitable for direct discharge to the San Vicente Reservoir, one of the City's main raw water reservoirs: MF/UF, RO, ion exchange, and ozonation. The project represents the first surface supply augmentation IPR project in California and must satisfy stringent California Department of Health Services requirements regarding virus removal and real-time monitoring of individual processes for pathogen removal. If successful, the project will result in the construction of the largest IPR plant in the U.S.

# 1.2 The Need for Indirect Potable Reuse for the City of McAllen

The City of McAllen, Texas, is located in the Lower Rio Grande Valley near the United States-Mexico border, approximately 40 miles upstream from the mouth of the Rio Grande River. The City presently derives its water supply from water rights in the Rio Grande River that it shares with multiple parties, including other cities, water supply corporations, irrigation districts, and Mexico. The Lower Rio Grande Valley is a growing area with an existing water shortage problem. The Texas Water Development Board (TWDB) reports that all surface water resources in the area are 100 percent appropriated. Additionally, this semi-arid area often experiences drought conditions. Projected growth in population and water use indicates that the demand for potable water will exceed the City's authorized water rights by the year 2003. Consequently, alternative water supply strategies are necessary to ensure a safe, reliable source of potable water.

The two most feasible alternative sources are groundwater and re-purified wastewater. Many of the groundwater supplies in the Lower Rio Grande Valley have an elevated

dissolved solids concentration and require demineralization by RO or electrodialysis to make them suitable for potable use. Consequently, wastewater reclamation is considered by the City to be a desirable means of augmenting its water supply.

# 1.3 Water Quality Considerations and Proposed Treatment Strategy

In general, reclaimed water should be treated to a level where its quality exceeds that of the historical water supply. In Texas, public heath issues related to the use of reclaimed water fall under the purview of the Texas Natural Resources Conservation Commission (TNRCC). The preliminary requirements of the TNRCC with respect to IPR for the City are: 1) reclaimed water must be of equal or better quality than that of the City's current water supply, and 2) RO must be used to treat all of the reclaimed water prior to its reuse. Based on these requirements and in view of the City's desire to reduce the dissolved solids of its finished water to improve consumer acceptability, the following IPR treatment sequence was proposed for the City in 1997 and subsequently demonstrated via testing conducted in that year and reported in *Water Treatment Technology Program Report No.* 26:

- Primary and secondary treatment
- Chlorine disinfection
- MF/UF
- RO
- UV disinfection

This sequence not only satisfies the TNRCC's preliminary requirements, it also provides multiple treatment barriers to the passage of microbial, inorganic, and organic contaminants in the wastewater. The concept of "multiple barriers" has been adopted by the water supply industry to achieve the appropriate level of safety and reliability by providing redundant treatment steps for the removal of wastewater contaminants, primarily pathogens.

## 1.4 Membrane Technologies in Indirect Potable Reuse

A primary focus of one task of BOR's Desalination Research and Development Program is research on membrane processes for wastewater reclamation. In this context, three membrane processes (MF, UF, and RO) represent key treatment processes in the proposed treatment sequence for IPR at McAllen. RO has been applied for wastewater reclamation for more than two decades and is considered a proven treatment process. RO serves as the "workhorse" for the IPR process because it is efficient in removing nearly all contaminants of public health concern. Cost-effective RO operation on municipal wastewater requires a high degree of preliminary treatment to control membrane fouling. Such treatment is provided through the use of MF/UF to polish secondary effluent.

During the last 5 years, MF has been shown at demonstration- and full-scale to be a reliable process in the context of IPR. Production MF facilities are currently in operation in California and Arizona with additional facilities planned for Pennsylvania, Virginia,

and Georgia. UF technologies have also been demonstrated for the same purpose; however, to date none have been implemented full-scale. All of the MF/UF products at these sites have employed pressure modules.

During the 1997 pilot study at McAllen, pressurized MF was demonstrated for the treatment of effluent from the City's south WWTP using Memcor MF technology. At that time, a novel, immersed MF product (ZeeWeed) was tested and found to provide performance competitive with or somewhat superior to the pressurized MF approach. In addition, ZeeWeed was also evaluated in the context of a membrane bioreactor process (ZenoGem) and found to be feasible for direct treatment of the City's screened, degritted wastewater. Preliminary results indicated that the ZenoGem filtrate was of equivalent quality to both Memcor and ZeeWeed filtrate with respect to general water quality (TDS, total organic carbon [TOC], coliforms, and turbidity) but had significantly higher RO feedwater colloidal fouling potential (as measured by silt density index [SDI]). Longer term testing of ZenoGem coupled with a follow-on RO system was recommended at that time and is the subject of this research.

## 1.5 Conclusions

Conclusions drawn from the results of this study are presented below.

### 1.5.1 ZenoGem System

- The ZenoGem membrane bioreactor process successfully treated screened, degritted sewage (SDS) to a quality suitable for RO processing.
- The ZenoGem process produced a permeate (see Tables 5.8 through 5.10) that exceeded the City's effluent discharge requirements for carbonaceous biochemical oxygen demand (CBOD_s<10 milligrams per liter [mg/L]), total suspended solids (TSS <15 mg/L)), and ammonia nitrogen (NH₃-N <3 mg/L). This result was attained at all mixed liquor suspended solids (MLSS) concentrations and with both membrane types.</li>
- The ZeeWeed OKC MF (0.4-micrometer [μm] pore size) membrane exhibited higher sustained permeability than OCP UF (0.035-μm pore size) membrane at high MLSS levels (13 grams per liter [g/L]).
- Permeability of the MF membrane was sensitive to MLSS level. Permeability was stable at 10 g/L but declined at 13 g/L because of increased membrane fouling not adequately controlled by frequent permeate backpulsing or maintenance cleans.
- At an MLSS concentration of 13 g/L, simultaneous nitrification/denitrification and biological phosphorus (bio-P) removal occurred most likely because of the inability to completely transfer oxygen from the bulk liquid to the interior of the bioflocs at the hydraulic residence time (HRT) selected for this study (5.7 hours). The oxygen transfer limitations inhibited complete nitrification but promoted nitrogen removal.

- At an MLSS concentration of 10 g/L, the rate of oxygen transfer was sufficient to maintain complete nitrification and suppress denitrification and bio-P uptake.
- Flow peaking tests (i.e., permeate flowrate increased for a specific duration of time) were conducted over a 24-hour period to simulate the types of peak loading conditions that typically occur in a conventional WWTP. However, peaking significantly increased the rate of permeability decline and accelerated the fouling rate (fouling not reversed by backpulsing or maintenance cleans as defined in Section 3.2.1). As a result, normal diurnal variations in wastewater flow, in which peak hourly flows can equal 300 percent of average daily flow, must be dampened through flow equalization so that the ZenoGem process can operate at more or less a constant hydraulic loading (flux) rate.
- Intermittent aeration (i.e., air cycled at 15 minutes on/15 minutes off) to the aeration tank (at 6 g/L MLSS concentration) produced the greatest degree of total nitrogen removal (optimum simultaneous nitrification and denitrification).
- With respect to RO feedwater quality, ZenoGem permeate quality consistently exceeded goals for turbidity and SDI, and generally exceeded goals for bacterial concentrations.
- Per Table 5.16, compared to the City's existing raw water source, the ZenoGem
  permeate was of lesser quality with respect to TOC and many inorganic
  contaminants while the RO permeate was of better quality in nearly all respects.
- Coliform removal by the both membranes was less than 100 percent. MF membrane permeate contained significantly greater coliform concentrations at 13 g/L MLSS concentration than the UF membrane. Furthermore, coliform removal appeared to be a function of MLSS loading for the MF membrane. However, the RO system consistently removed any remaining coliform regardless of the MF or UF pretreatment.
- Cycled aeration to the membrane tank appeared to significantly increase the rate of membrane fouling (permeability decline) compared with continuous aeration.
   However, it is difficult to draw firm conclusions regarding aeration given the brief operating time with cycled aeration and its use in combination with other operating modifications (flow peaking, cycled aeration to the aeration tank).
- Footprint for ZenoGem facilities represents about 32 percent of the total area required for a conventional activated sludge plant providing comparable biological treatment and flow equalization.

### 1.5.2 RO System

- Membrane fouling by particulates and soluble organics in the screened, degritted wastewater was well controlled by the ZenoGem process as illustrated by stable first stage flux and salt rejection. Continuous disinfection, in the predominant form of monochloramine, with a low concentration of combined chlorine (approximately 1 mg/L) was effective in preventing biological fouling of the RO membranes as measured by stability of first stage feed/concentrate differential pressure (see Tables 5.12 through 5.14).
- Elevated concentrations of calcium and phosphate in the City's wastewater (and ZenoGem permeate) most likely caused precipitation of the calcium phosphate salt, hydroxyapatite, in the RO system second stage at feedwater pH levels designed to control calcium carbonate scaling. This precipitation caused rapid increases in RO feed pressures, rapid declines in normalized product flow, and marked increases in salt passage. The precipitate was readily dissolved using citric acid cleaning, and performance declines were consistently reversed by such cleanings. Further acidification of the RO feedwater to pH 5.0 (concentrate pH to 5.6) prevented such precipitation except at design (80 percent) recovery. A better control method may be to precipitate the majority of the soluble phosphorus in the wastewater during MBR treatment using a ferric or aluminum coagulant.
- RO permeate at design (80 percent ) recovery was very high quality: TDS <75 mg/L, TOC <0.5 mg/L, and turbidity <0.1 nephelometric turbidity units (NTU). Levels of these and other contaminants monitored for in the RO permeate were significantly less than the maximum concentrations permitted under federal drinking water regulations or indirect potable reuse guidelines established in certain states (e.g., California and Virginia). The exception being coliforms, which were consistently detected at low levels. From this standpoint, the RO permeate is of satisfactory quality for IPR use subject to additional disinfection (chlorination or UV). TNRCC has not established guidelines or regulations for IPR use at McAllen, however, their preliminary position is that RO treatment would be required. On the other hand, TNRCC may consider establishing quality requirements for IPR that use the quality of the existing raw water supply as the benchmark for treatment. In this case, it may be possible that an acceptable quality of reclaimed water can be produced through a blend or ZenoGem and RO permeate with post-disinfection.</p>

## 1.6 Recommendations for Further Research

The following recommendations are provided with respect to further research involving MBRs and RO in the context of indirect potable reuse.

### 1.6.1 Membrane Bioreactors

### 1.6.1.1 MLSS Levels and Membrane Flux

This research illustrated that membrane fouling and permeability is sensitive to MLSS level. Further research is needed to define the optimum combination of these two parameters (MLSS level/membrane flux) as they contribute to both capital and operating cost. Increased MLSS levels permit higher solids retention times (SRTs), reducing sludge yield, however their use may result in higher capital costs and operating costs associated with additional membrane area (reduced flux).

### 1.6.1.2 Cycled Aeration to Promote Nitrification/Denitrification

Optimize conditions of cycled aeration for the purpose of promoting simultaneous nitrification/denitrification. Testing in this study was conducted at only one on/off cycle (15 minutes on, 15 minutes off) to the aeration tank. No water quality parameters were measured at other cycles to determine if control at other cycles may be more efficient at achieving improved or complete nitrogen removal. Control methods need to be developed in conjunction with such testing.

### 1.6.1.3 Cycled Aeration to Reduce Membrane Air Scour Requirements

Aeration for control of membrane fouling represents a significant operating (power) cost. Cycling of air to the coarse bubble aerator integral to the membrane module (membrane tank) represents one way to reduce operating cost; however, aeration reductions must not come at the detriment of membrane permeability. Testing is needed to determine optimum airflow rates and cycle times to achieve the optimum balance of these two needs.

### 1.6.1.4 Alternative MBR Designs

This research tested one MBR product, Zenon Environmental System's ZenoGem using a MF membrane module. Other MBR products are available and have been installed for municipal wastewater reclamation both in Europe and Japan. Testing of these products is needed to assess their performance relative to ZenoGem and to determine if such products represent competitive technologies for application in the U.S. IPR and wastewater treatment market.

The BOR is currently funding research by Montgomery Watson and the City of San Diego to compare the performance of ZenoGem and Mitsubishi systems. Also, the ZenoGem UF system should be retested at 10 g/L and 6 g/L for comparison to the MF system at these concentrations.

### 1.6.2 Reverse Osmosis

### 1.6.2.1 Scale Control

For wastewaters containing elevated concentrations of calcium and phosphate, additional research is needed to determine the most cost-effective and operationally reliable means to control calcium phosphate scaling. Acidification has the advantages of low cost and typically being required for calcium carbonate scale control; however, its use to reduce pH to levels considered effective in this study (see Section 5.0) resulted in an aggressive RO permeate that was supersaturated with carbon dioxide (most likely requiring stripping). Ferric or aluminum coagulant addition to the MBR (or conventional plant) will reduce phosphorus levels in both the RO feedwater and concentrate. However, the doses required in the City's case (approximately 50 mg/L ferric chloride and 91 mg/L alum) produce additional solids in the MBR, potentially increasing membrane fouling and requiring acid maintenance cleans and reducing SRT for a given operating MLSS level.

### 1.6.2.2 Membrane Flux

RO testing in this study was performed at relatively low flux (10 to 11 gallons per square foot per day [gfd]). Given the low turbidity and SDI of the ZenoGem permeate, higher flux operation (reduced membrane capital cost) may be feasible if scale control can be resolved as discussed herein.

# **Testing Objectives**

The research to be conducted under this program has the following objectives:

- 1. Demonstrate feasibility and benefits of the ZenoGem process:
  - Produce a high quality RO feedwater (i.e., turbidity <0.2 NTU, SDI <3, heterotrophic plate count [HPC] <500 colony forming units [CFU]/milliliter [mL]).
  - Meet the City's effluent discharge permit requirements (i.e., TSS <15 mg/L, CBOD, <10 mg/L, NH,-N <3 mg/L).</li>
  - Operate reliably (i.e., sustained production).
- 2. Demonstrate successful RO treatment on ZenoGem permeate:
  - Reliable operation with minimal fouling and effective membrane cleanings.
  - Meet all drinking water/reuse standards.
- 3. Define design and operation and maintenance (O&M) requirements to develop full-scale ZenoGem and RO plant design criteria.
- 4. Develop cost estimates for current and proposed IPR advanced treatment processes for the City of McAllen.
- 5. Characterize ZenoGem and RO permeates relative to the City's existing raw water supply (i.e., Rio Grande River) based on:
  - Regulated drinking water contaminants.
  - State of Texas secondary drinking water requirement of TDS for 1,000 mg/L.
- 6. Determine impacts of IPR on waste discharges to the City's current discharge location (i.e., Arroyo Colorado/Laguna Madre).

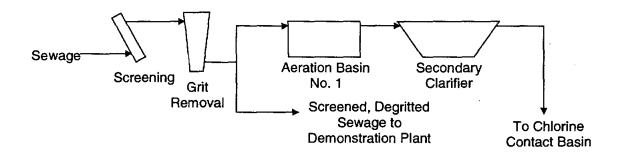
# **Demonstration Plant Facilities**

The demonstration plant facilities consisted of ZenoGem (MBR) and RO treatment systems. The plant also contained ancillary equipment, including a raw water supply pump, chemical feed systems, transfer pump, and associated piping, valves, and fittings for delivery of raw water (i.e., ZenoGem feed), transfer of processed water (i.e., ZenoGem permeate/RO feed), and disposal of discharge flowstreams (i.e., ZenoGem sludge, RO concentrate, and RO permeate) and membrane cleaning solutions to the WWTP. A description of the other components of the demonstration plant facilities is presented in the following sections.

# 3.1 Raw Water Supply, Abstraction, Pumping, and Screening

The raw water source (feedwater) to the demonstration plant was SDS from the City's South WWTP No. 2. SDS was abstracted from the influent splitter box (located upstream of Aeration Basin No. 1) and transferred to the ZenoGem system via a submersible pump located in the splitter box. The abstraction point relative to the WWTP processes is shown in Figure 3.1.

FIGURE 3.1
Demonstration Plant Feedwater Abstraction Point from WWTP No. 2

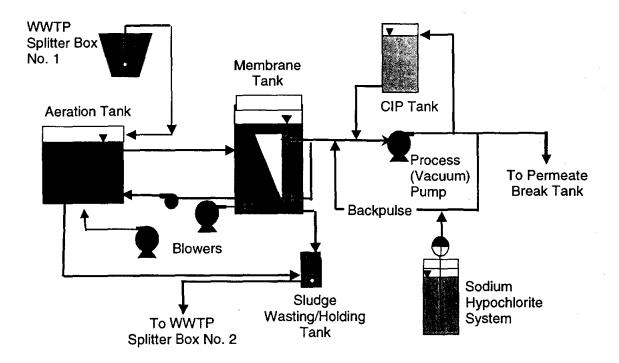


Raw water to the ZenoGem system was screened using a basket strainer and a 3-millimeter (mm) screen. Screening was necessary to prevent clogging of the inlet distributors of the membrane modules.

### 3.2 ZenoGem Treatment System

The ZenoGem treatment system is comprised of the following components: ZeeWeed Model MSTD ZW-4 unit, a 3,000-gallon aeration tank, auxiliary aeration blower, solids recirculation pump, and sludge wasting system (submersible pump located in aeration tank and 200-gallon calibrated sludge wasting/holding tank). The ZeeWeed unit consists of the following: 185-gallon tank containing the membrane module (membrane tank); one ZW-500 module containing 500 square feet (ft²) of hollow-fiber MF membrane with a nominal pore size of 0.4 microns (OKC membrane); permeate pump; membrane aeration blower; and backpulse/clean-in-place (CIP) tank¹. The ZeeWeed ZW-500 membrane module consists of loose fibers connected to a manifold rack system at either end, with the rack/fiber assembly suspended in the membrane tank and submerged in the mixed liquor. Treatment occurs when a vacuum of 1.5 to 9.0 pounds per square inch gage (psig) is applied to the filtrate side of the fibers using the process (vacuum) pump. The vacuum causes the water in the mixed liquor to flow from the feed side to filtrate side of the membrane in a direct filtration mode under a positive transmembrane pressure. A process flow diagram for the ZenoGem treatment system is shown in Figure 3.2. Photographs of the ZenoGem system are presented in Appendix A.

FIGURE 3.2
ZenoGem Treatment System Process Flow Diagram



¹During the commissioning stage of the testing (Stage A), a 0.035-micron UF (OCP) membrane module was installed in the membrane tank. This module was replaced with the 0.4-micron MF (OKC) membrane module to increase flow and reduce fouling.

During ZenoGem operation, biodegradable matter in the sewage (biochemical oxygen demand [BOD] and ammonia) is oxidized by the biomass maintained at high mixed liquor concentrations in the membrane and aeration tanks with air input to these tanks using coarse and fine bubble diffusers, respectively. MLSS levels and SRTs are maintained in the tanks through the frequency and volume of sludge wasted to a calibrated sludge wasting/holding tank. Waste sludge is returned to Splitter Box No. 2 using a submersible pump. The desired HRT is maintained by controlling the rate of permeate flow. Consistency of MLSS concentrations between membrane and aeration tanks is maintained by recirculating MLSS between the tanks using a submersible grinder pump located in the aeration tank.

#### 3.2.1 Methods to Control ZeeWeed Membrane Fouling

Control of solids buildup on the outside surface of the membrane fibers and related increases in permeate side vacuum are achieved in three ways. First, a blower is used to provide continuous air input (in the form of coarse bubbles) at 25 to 30 standard cubic feet per minute (scfm) into the bottom of the membrane tank directly below the membrane fibers. The air bubbles flow upward between the vertically oriented fibers, causing the fibers to agitate against one another. This results in mechanical cleaning through air scour.

Secondly, filtration is interrupted every 10 minutes and the membrane fibers are backpulsed repeatedly for 15 seconds with permeate from the backpulse/CIP tank. The system remains on-line during backpulsing and is in a backpulse mode for a total of 36 minutes per day. Typically, a low concentration of chlorine (<5 parts per million [ppm]) is maintained in the backflush water to inactivate and remove microbes (primarily bacteria) that colonize the outer membrane surface. Hydraulic cleaning via backflushing is accomplished using discharge head from the process pump, and backwash water is retained in the membrane tank.

Thirdly, three times per week, a 100-ppm sodium hypochlorite solution is added to the backpulse/CIP tank, and the membrane module is backpulsed repeatedly for 45 minutes in a procedure called a "maintenance clean." After the 45-minute in situ cleaning, the system is flushed with permeate for 15 minutes. An additional permeate flush to drain is performed for 10 to 15 minutes to purge the system of free chlorine once permeation (i.e., vacuum applied to filtrate side of membrane module) is re-initiated. The total system downtime during a maintenance clean is about 75 minutes.

The combination of air scour, backpulsing, and maintenance cleaning may not be completely effective in controlling membrane fouling, and with time, the pressure differential across the membrane (transmembrane pressure [TMP]) may increase to a maximum of value approximately 17 inches of mercury. When this condition occurs, which is anticipated to be (>3 months) infrequently at full-scale application, the membrane module is chemically cleaned with a 1,500 to 2,000-ppm sodium hypochlorite solution in a procedure called a "recovery clean." Recovery cleaning requires in situ full tank soaking and clean water flux testing. The chemical cleaning dissolves and removes the refractory solids, and reduces TMP to "clean membrane" initial levels (i.e., levels at startup prior to any evidence of fouling).

### 3.2.2 Permeate Storage, Disinfection, and Pumping

The ZenoGem permeate flows from the ZeeWeed unit to a permeate break tank that serves to balance the intermittent flow of ZenoGem permeate (resulting from backpulsing and maintenance cleans) with the continuous feed flow requirement of the RO system. After the break tank and prior to entering the RO treatment system, the permeate is dosed with combined chlorine (in the predominant form of monochloramine) using a solution tank and metering pump. Combined chlorine is batched using sodium hypochlorite and aqueous ammonia. The dosage is based on maintaining at least 1 to 2 mg/L of total chlorine residual and zero free chlorine residual. The thin film composite RO membrane material is intolerant to free chlorine, and any exposure will reduce the membrane life. Combined chlorine serves to prevent the low levels of bacteria that can be present in the ZenoGem permeate (primarily through contamination) from growing in the RO feed piping and on the membrane elements (biofouling). The addition of combined chlorine is not intended to serve as disinfection to eliminate pathogens. The "disinfected" ZenoGem permeate is pumped from the break tank to the RO system using a transfer pump. Excess ZenoGem permeate overflows the break tank through drain piping.

#### 3.2.3 ZenoGem Operation

The ZenoGem system is designed to operate at a constant flux with the TMP varying over time to maintain the design flux. The rate of filtrate discharge to the break tank is controlled to achieve the desired HRT in the membrane tank (bioreactor). Proper HRT control is required to achieve the desired degree of  $CBOD_5$  and ammonia removal by the biomass maintained in the bioreactor. Solids buildup in the bioreactor is controlled through daily manual wasting to achieve the desired SRT (concentration of MLSS) in the bioreactor. Unlike a conventional WWTP that operates at MLSS levels of 2,000 to 3,000 mg/L, the ZenoGem process is designed to operate at MLSS levels of 10,000 to 15,000 mg/L. This allows for a higher organic loading of wastewater in the ZenoGem treatment system.

Three modes of operation were employed during the study:

- Normal Flow: Permeate flowrate maintained at 6.5 gallons per minute (gpm).
- Peak Flow: Permeate flowrate increased to 9.5 gpm for 6 hours over a 24-hour period.
- Cycled Aeration: Air cycled to membrane tank at 10 seconds on/10 seconds off with or without air cycled to aeration tank at 15 minutes on/15 minutes off.

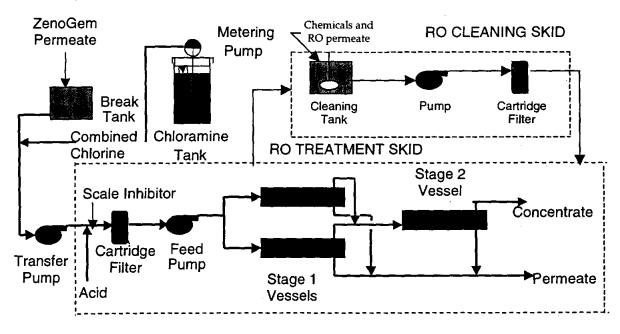
As detailed in Table 5.1, these operating modes are presented as specific operating events during ZenoGem operation.

## 3.3 RO Treatment System

The RO treatment system is comprised of the following components: a treatment skid and a cleaning skid. The treatment and cleaning skids are provided courtesy of the Bureau of Reclamation's Water Treatment Engineering and Research Group.

The RO treatment skid consists of the following equipment: chemical feed systems for the addition of acid and scale inhibitor, 5 micron cartridge filter, feed (high pressure) pump, two-stage pressure vessel array, programmable logic controller (PLC) and associated instruments and controls, piping, gauges, and valves. The cartridge filter serves as backup in the event of MF pretreatment failure. The RO elements, model LFC1-2540, are manufactured by Hydranautics and contain low fouling composite polyamide membranes. Stage 1 contains four pressure vessels each containing three 2.5-inch-diameter by 40-inch-long spiral wound elements in a "2:2" configuration. Stage 2 contains two pressure vessels of identical design plumbed in a "1:1" configuration. The two-stage array permits operation up to 80 percent recovery and simulates design of a full-scale RO plant using a "2:1" array with six-element vessels. A process flow diagram for the RO treatment skid and associated pretreatment equipment is shown in Figure 3.3. Photographs of the RO treatment system are presented in Appendix A.

FIGURE 3.3
RO Treatment System Process Flow Diagram



#### 3.3.1 RO Feedwater Characterization

Three separate samples of unchlorinated secondary effluent (from the City's WWTP) were collected prior to the start of testing to estimate the inorganic quality of the RO feedwater. (The inorganic quality of the WWTP effluent was considered to be a good simulation of that produced by the ZenoGem system given that both were designed to operate on the same feedwater and provided the same degree of biological treatment and nitrification.) The results are shown in Table 3.1.

TABLE 3.1
Results of RO Feedwater Characterization

	_		Sampling Date		
Parameter	Units	12/14/98	12/16/98	12/18/98	Average
Alkalinity	mg/L as CaCO₃	153	161	164	159
Bicarbonate	mg/L	187	196	200	194
Chloride	mg/L	388	359	378	375
Reactive Silica	mg/L	13.90	14.70	14.60	14.40
Sulfate	mg/L	327	305	332	321
Anion Sum	mg/L	1,069	1,036	1,089	1,064
Barium	μg/L	78.30	77.60	87.80	81.23
Calcium	µg/L	112,000	127,000	103,000	114,000
Magnesium	μg/L	29,100	29,700	26,800	28,533
Potassium	μg/L	17,100	18,900	19,400	18,467
Sodium	μg/L	236,000	271,000	233,000	246,667
Strontium	μg/L	1,260	1,310	1,380	1,317
Cation Sum	μg/L	395,538	447,988	383,668	409,065
TDS (Sum of lons)	mg/L	1,465	1,484	1,473	1,473

The mean values were then used with two software programs, King Lee Technologies (KLT) WaterWizard and Hydranautics' RODesign, to develop feedwater chemical conditioning requirements and establish product water recovery of the RO system based on the presence and concentration of sparingly soluble salts. The program outputs, shown in Appendix B, indicated the following design condition:

- RO feedwater acidification to pH 6.8 (with sulfuric acid)
- RO feedwater dosing with scale inhibitor at 2 ppm (KLT PreTreat 0100)
- Product water recovery of 80 percent based on 53 times saturation of barium sulfate in the RO concentrate

This condition served as the basis for target operating criteria for the RO system.

#### 3.3.2 RO Feedwater Pretreatment to Control Membrane Fouling

During extended operation, RO membrane elements are subject to fouling caused by both suspended and dissolved matter. Suspended matter includes organic and inorganic colloids and microorganisms. Sparingly soluble salts, such as carbonates, sulfates, and silica, can precipitate from solution because they are concentrated by the RO process. Suspended particles accumulate on the membrane surface causing biofouling and colloidal fouling, and can block feed channels thereby increasing the pressure drop across the system. These phenomenon reduce water permeability through the RO membranes causing flux decline and increased salt passage. The nature and rapidity of fouling depends on the condition of the feedwater. Fouling is progressive, and, if not controlled early, can impair the RO system performance in a relatively short time. For these reasons, fouling must be controlled.

Particulate fouling was addressed through the use of the ZeeWeed MF membrane. Scaling was controlled using acidification and scale inhibitor addition. Chloramines were batched and dosed into the RO feedwater to prevent biological growth (biofouling) on the membranes as discussed in Section 3.2.

The RO feedwater from the transfer pump enters the treatment skid where it is dosed with a scale inhibitor and sulfuric acid prior to entering the cartridge filter. The addition of scale inhibitor prohibits the precipitation of sulfate and carbonate scalants (specifically calcium carbonate and barium sulfate). KLT PreTreat 0100 was used for mineral precipitate control. Acidification further reduces the potential for calcium and carbonate to precipitate from solution. Sulfuric acid was used for feedwater pH control.

Chemically conditioned with King Lee PreTreat 0100 scale inhibitor and sulfuric acid, the filtered water is pumped to the RO vessels at a pressure needed to produce the design permeate flow. Target feedwater recovery is attained by adjustment of the concentrate flow control valve. The system operates in a constant permeate flow/constant recovery mode with feed pressure increasing to compensate for decreases in water mass transfer rate.

The combination of filtration, chloramination, scale inhibition, and acidification may not be completely effective in controlling membrane fouling, and with time, the pressure drop across the stages may increase with simultaneous decreases in permeate flowrate and feedwater recovery. Recirculating a citric acid solution (low pH cleaning) or an alkaline solution (high pH cleaning) containing a mixture of surfactant, detergent, and chelating agent from the cleaning skid through the RO vessels serves to chemically clean the RO system when fouling is apparent. Recirculation is coupled with soak periods to remove the membrane foulants and restore lost performance.

Cleaning was performed five times on the system throughout the study. Low pH cleanings using citric acid and sodium hydroxide (for pH adjustment) were performed to remove inorganic fouling, such as calcium precipitates (e.g., calcium carbonates and phosphates) and hydroxide precipitates (e.g., metal oxides such as ferric hydroxide). High pH cleanings using a caustic solution and sulfuric acid (for pH adjustment) were performed to remove calcium sulfates and organics.

## 3.4 Criteria for Treatment System Operation

Tables 3.2 and 3.3 present criteria that were established for operation and biological performance, respectively, of the ZenoGem system. Table 3.4 presents the initial operating criteria for the RO system based on RO feedwater analyses and projection results. These criteria reflect the individual manufacturer's experience with the systems. Some of the criteria were modified during the study to improve operability (i.e., reduce potential for membrane fouling) and biological treatment stability and performance. Detailed descriptions of the operating stages for each treatment system are presented in Section 5.1.

**TABLE 3.2**Operating Criteria for the ZenoGem System

Parameter	Units	Target
Aeration Tank Air	scfm	45
Backpulse Duration	sec	15
Backpulse Frequency	min	10
Biomass Recirculation Rate	gpm	36
Flux	gfd	18.7/27.3ª
Membrane Tank Air	scfm	25/30 ^b
Permeability	gfd/psi	5°
Permeate Flowrate before Backpulse	gpm	6.5/9.5ª
ТМР	psi	2.5 - 8.5
Vacuum before Backpulse	in Hg	5.1 - 17.3

^aTarget value during flow peaking.

^cExpected value based on control variables.

^bApplied rate increased to 30 scfm during intermittent aeration.

**TABLE 3.3**Biological Treatment Performance Criteria for the ZenoGem System

		Target					
Parameter	Units	Stage A	Stage B	Stage C	Stage D		
DO	mg/L	> 1.5	> 1.5	> 1.5	> 1.5		
OUR	mg O₂/L-min	1.0 - 1.5	1.0 - 1.5	1.0 - 1.5	1.0 - 1.5		
MLSS	mg/L	13,000	13,000	10,000	6,000		
Sludge Wasted Daily	gals	90ª	90ª	110ª	150 ^a		
HRT	hrs	6.2	6.2	6.2	6.2		
SRT	days	25°	25ª	20ª	15ª		

^aExpected value based on control variables.

**TABLE 3.4** Operating Criteria for the RO System

		Target					
Parameter	Units	Stage A	Stage B	Stage C	Stage D		
Acidified Feedwater pH		6.8	6.8	6.8	5.6ª		
Feedwater Flowrate	gpm	5	5	3	3 - 5		
Feedwater Recovery	%	80	80	50	50 - 80		
Permeate Flowrate	gpm	4	4	1.5	1.5 - 4.0		
Scale Inhibitor Dose	ppm	2	2	2	2		

^aSet target to concentrate pH during this stage (feedwater pH = 5.0).

# **Testing Approach**

The demonstration testing program was divided into two phases:

- Phase I: Operation of ZenoGem treatment system for 1 month to establish stable biological treatment performance and permeate water quality.
- Phase II: Operation of ZenoGem and RO treatment systems for 5 months to demonstrate project goals and objectives.

The demonstration plant operated 24 hours per day, 7 days per week except for chemical cleanings or planned and unplanned maintenance. Equipment was supervised on an 8-hour per day, 5-day per week basis and as required on weekends to ensure proper operation and data collection. Operating data were recorded at the beginning and end of the each shift. Water quality samples were collected at the beginning of the shift. The results of Phase I and Phase II testing are discussed in Section 5.0.

## 4.1 ZenoGem Treatment System Tasks

The ZenoGem treatment system tasks under Phases I and II were to:

- 1. Operate ZenoGem system to produce a permeate whose quality complies with the City's discharge permit (TSS <15 mg/L; BOD <10 mg/L; NH,-N <3 mg/L).
- 2. Characterize ZenoGem permeate relative to goals for RO feedwater quality, defined as follows:

Turbidity: < 0.2 NTU</li>

• SDI: <3

• Fecal coliforms: <1 CFU/100 milliliters (mL)

- 3. Characterize ZenoGem permeate relative to IPR water quality requirements and for development of RO feedwater design composition.
- 4. Measure O&M requirements for ZenoGem system (plant efficiency factor, labor hours required, energy consumption, and chemical and other consumable consumption); demonstrate reliable, long-term performance of the ZenoGem process; and develop criteria for design of full-scale ZenoGem system.
- 5. Develop information necessary for design of a full-scale ZenoGem plant. Design criteria to be developed as part of this task include the following:
  - HRT (at average and peak loading)
  - SRT
  - Aeration requirements, separately for maintenance of membrane flux (air scour) and for carbonaceous and nitrogenous removal

- Membrane flux rate
- Duration of operation between chemical cleanings
- Frequency and duration of backpulse
- Backpulse volume
- Chemical type and concentration (if any) needed in backpulse water
- Chemical cleaning regime, including chemical type(s) and concentration(s) and contact time to ensure maintenance of membrane
- Sludge production rate and characteristics to define and assess proper sludge handling, drying, and disposal
- 6. Evaluate the effect of flow peak testing (hydraulic peaking) on the ZenoGem process. The approach is to initially operate the ZenoGem process at a target SRT of 25 days and a HRT of approximately 6 hours to establish baseline performance. After a predetermined period of operation, the HRT will be decreased to about 4 hours. Following this change, system operation (membrane performance) will be monitored at the new HRT by tracking changes in TMP and permeability.
- 7. Evaluate the effect of intermittent aeration on operational (blower) costs and the ability to concurrently nitrify and denitrify in the ZenoGem process. This task includes cycled aeration to the membrane tank and aeration tank to determine the impacts on operational (blower) costs and biological nitrogen removal, respectively.

## 4.2 RO Treatment System Tasks

The RO treatment system tasks under Phases II were to:

- 1. Characterize RO permeate quality relative to IPR quality requirements.
- 2. Monitor RO system operating performance as measured by the following:
  - Feed and permeate conductivity
  - Feedwater recovery
  - Feed pressure
- 3. Assess changes in RO membrane performance caused by fouling of RO membrane and elements and by chemical oxidation of RO membrane surface by monitoring the following parameters:
  - Normalized permeate flow
  - Normalized conductivity passage
  - Normalized vessel differential pressure
- 4. Perform chemical cleanings as required when normalized performance parameters change by a pre-determined amount. Assess the efficiency of one or more chemical cleaning formulations/regimes to restore RO performance losses.

- 5. Confirm RO membrane manufacturer's projections of attainable feedwater recovery and document RO feedwater chemical conditioning requirements to control mineral precipitation.
- 6. Confirm effectiveness of RO feedwater chloramination as a means to control biological fouling of RO membranes.
- 7. Develop information necessary for design of a full-scale RO plant. Design criteria to be developed as part of this task include the following:
  - Feedwater chemical conditioning
  - Feedwater biological monitoring requirements
  - Feedwater disinfection (chloramination)
  - Feedwater pressure
  - Membrane flux
  - Feedwater recovery
  - Membrane composition
  - Cleaning frequency and regime
  - Post-disinfection requirements

### 4.3 Additional Testing Activities

Prior to and during the operation of the demonstration plant, several additional activities were required and performed, including RO feedwater characterization, IPR characterization of the ZenoGem permeate and RO permeate, RO concentrate/WWTP effluent characterization, and RO integrity testing. These activities are described below.

#### 4.3.1 RO Feedwater Characterization

Prior to testing, three sets of samples of unchlorinated secondary effluent from the South WWTP were collected to characterize the inorganic quality of the feedwater to the RO system. These analyses were required to estimate RO system operating conditions with respect to acid and scale inhibitor dosage and feedwater recovery. The samples were collected on December 14, 16, and 18, 1998, by the plant operating staff and analyzed by the CH2M HILL's Applied Sciences Laboratory (ASL). Results of these analyses were presented and discussed in Section 3.0.

#### 4.3.2 IPR Characterization

The overall goal of IPR is to produce reclaimed water of suitable quality for supplementing McAllen's current raw water supply. Thus, it was desirable to characterize the quality of the raw water supply as part of this study to compare it with quality of reclaimed water produced by MF treatment (ZenoGem permeate) and by RO treatment (RO permeate).

Raw water characterization of McAllen's current raw water supply was conducted during the previous pilot testing. With respect to the demonstration plant, samples of ZenoGem permeate and RO permeate were collected on August 18 and September 14, 1999, respectively, by the plant operating staff and analyzed by ASL. Results of these analyses are presented and discussed in Section 5.0.

#### 4.3.3 RO Concentrate and WWTP Effluent Characterization

RO will produce a waste stream (concentrate) containing elevated levels of most constituents present in the ZenoGem permeate, most notably TDS, TOC, and nutrients. Based on an assumed rejection of 90 percent for these constituents by RO and a feedwater recovery of 80 percent, the concentrate will contain TDS, TOC, and nutrients at four to five times their concentration in the ZenoGem permeate. It is anticipated that the RO concentrate will be disposed of by blending it with that portion of the South WWTP secondary effluent that is not reclaimed for IPR. This secondary effluent discharge point, the Arroyo Colorado, which flows into the Laguna Madre, a marine lagoon. Low freshwater inflows and variable salinity characterize the Arroyo Colorado-Laguna Madre system, which has TDS ranging from 3,000 to 10,000 mg/L. It is anticipated that TDS levels of the concentrate/effluent blend (which will be between 1,200 and 7,500 mg/L) will not adversely impact the ecology of the Arroyo Colorado-Laguna Madre system; however, there is concern that elevated nutrient concentrations in the blend could promote eutrophication and could adversely affect marine ecology.

Samples of WWTP effluent and RO concentrate were collected on August 18 and September 14, 1999, by the plant operating staff and analyzed by ASL and the South WWTP laboratory. The concentrations of the following constituents were measured to: 1) determine the suitability of discharge of the WWTP effluent/RO concentrate blend, and 2) develop requirements for treatment of the RO concentrate to ameliorate any constraints on discharge that are identified:

- TDS (gravimetric)
- TOC
- pH
- Total phosphorus
- Total Kjeldahl nitrogen (TKN)
- Nitrite/nitrate nitrogen

Results of these analyses are presented and discussed in Section 5.0.

### 4.3.4 RO Integrity Testing

The BOR performed an evaluation of RO element integrity test methods. This evaluation was outside of the scope of CH2M HILL's activities under their agreement with the City; however, activities conducted as part of the BOR's evaluation were closely coordinated with those conducted under this study and were, in large part, conducted by the City's operations staff. Furthermore, the results of the integrity method evaluation should provide useful information for future implementation of indirect potable reuse at McAllen and other locations where RO is used. Development of a field-applied integrity test method for RO elements will provide greater assurance that RO treatment is providing contaminant removal to the degree necessary to protect public health in this reuse context. Results of these analyses are presented in Appendix J.

## 4.4 Treatment System Monitoring

During the demonstration testing, various performance parameters were monitored to evaluate operation of the treatment systems and the quality of the water fed to and produced by the systems. The parameters that were monitored are presented in the following sections.

#### 4.4.1 Operator Training

The City provided two dedicated operators to supervise, operate, and maintain the demonstration plant during the course of the study. The operators were responsible for, but not limited to, equipment maintenance and operation, including manually recording operational data, saving RO system PLC data, batching chemicals, adjusting chemical addition rates, performing chemical cleanings, collecting routine water quality samples, and recording all demonstration plant activities.

Operating parameters for the systems were monitored daily to evaluate treatment system performance. ZenoGem system operating data were collected from equipment instruments and recorded manually on operations log sheets at least twice daily. RO system operating data were collected by two methods: 1) electronically via a PLC for a specified interval and duration (typically every hour over a 12-hour period), and 2) manually at the end of each operating shift from equipment instruments and panel readouts and recorded on operations log sheets. Method 1 was used for primary data collection; method 2 served as a backup source in the event of difficulties with PLC data downloading. Logbooks for each system were maintained to record all O&M events that occurred during the testing period including, but not limited to, date and time of chemical cleanings; type and amount of chemicals used during cleaning, cleaning temperature, and pH; downtimes; alarms or failures; and changes in any operating conditions.

The operating criteria (targets) were presented in Section 3.0. The actual average operating conditions, along with targets, are presented and discussed in Section 5.0.

### 4.4.2 Sampling and Analysis

The operators collected water quality samples from each treatment system on a routine basis. The South WWTP laboratory was responsible for performing selected physical/chemical and biological analyses. The WWTP laboratory was also responsible for collecting samples for TOC, chemical oxygen demand (COD), TKN, nitrite/nitrate nitrogen, and total phosphorous, and shipment of these samples to ASL for analyses. The central water laboratory, located at McAllen's Water Treatment Plant No. 1, was responsible for performing microbiological analyses.

Sampling activities commenced on February 8, 1999, for the ZenoGem system and on April 16, 1999, for the RO system. At these times, the operators began routine recording of system operating data and collection of water quality samples for each system. In addition, the water and wastewater treatment plants and ASL began routine sampling analyses. The biological treatment and water quality parameters, sampling location and frequency, and responsible analytical party for each treatment system are presented in Tables 4.1 and 4.2.

SECTION 4. TESTING APPROAG

TABLE 4.1
Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System

Parameter	ZenoGem Feed	Membrane Tank	Aeration Tank	ZenoGem Permeate	Aeration Tank Waste Sludge	Sample Day(s)	Responsible Party
Physical/Chemical							
ЭН	2/W	2/W	2/W	2/W	NONE	M & W	WWTP
Temperature ^a	1/D	1/D	1/D	1/D	NONE	M - F	OPERATOR
Conductivity	1/D	NONE	NONE	1/D	NONE	M - F	WWTP
Turbidity	NONE	NONE	NONE	1/D	NONE	M - F	WWTP
COD	2/M	NONE	NONE	2/M	1/W	M	СН2М
Total Chlorine	NONE	NONE	NONE	1/D	NONE	M - F	WWTP
Free Chlorine	NONE	NONE	NONE	1/D	NONE	M-F	WWTP
ALK	1/W	NONE	NONE	1/W	NONE	M	WTP
Biological							
DO ^a	1/D	1/D	1/D	NONE	NONE	M - F	OPERATOR
OUR	NONE	2/W	2W	NONE	NONE	M & W	WWTP
MLSS ^b	NONE	3/W	3/W	NONE	3/W	M,W,F	WWTP
MLVSS ^b	NONE	3/W	3/W	NONE	1/W	M or M,W,F	WWTP
DSVI	NONE	3/W	NONE	NONE	NONE	M,W,F	WWTP
CBOD ₅ ^b	3/W	3/W	3/W	3/W	NONE	M,W,F	WWTP
TSS ^b	3/W	NONE	NONE	3/W	NONE	M,W,F	WWTP

TABLE 4.1 Biological Treatment and Water Quality Sampling Schedule for the ZenoGem System

	Location and Frequency						
Parameter	ZenoGem Feed	Membrane Tank	Aeration Tank	ZenoGem Permeate	Aeration Tank Waste Sludge	Sample Day(s)	Responsible Party
NH ₃ -N ^b	3/W	NONE	NONE	3/W	NONE	M,W,F	WWTP
TKN⁵	1/W	NONE	NONE	1/W	1/W	М	СН2М
NO ₂ /NO ₃ -N ^b	1 <i>/</i> W	NONE	NONE	1/W	NONE	М	CH2M
T Phosphorus	1 <i>/</i> W	NONE	NONE	1/W	1/W	М	CH2M
Microbial						· · · · · · · · · · · · · · · · · · ·	
Total Coliform	2/W	NONE	NONE	2/W	NONE	M & W	WTP
Fecal Coliform	2/W	NONE	NONE	2/W	NONE	M & W	WTP
HPC	NONE	NONE	NONE	2/W	NONE	M & W	WTP

^aThese samples are to be taken at the same time. ^bOperator to analyze at sample location.

^{1/}D=once per day

^{1/}W=once per week

^{2/}W=twice per week

^{3/}W=three times per week

^{2/}M=2 times per month

ALK=alkalinity
CH2M HILL=CH2M HILL's Applied Sciences Laboratory (ASL)

DO=dissolved oxygen
DSV!=diluted sludge volume index
MLVSS=mixed liquor volatile suspended solids
OUR=oxygen uptake rate
WTP=McAllen's Central Water Treatment Plant Laboratory
WWTP=McAllen's South Wastewater Treatment Plant Laboratory

TABLE 4.2
Water Quality Sampling Schedule for the RO System

	Lo	cation and Freque			
Parameter	RO Feed	RO Permeate	RO Concentrate	Sample Day(s)	Responsible Party
Physical/Chemical					
pН	1/W	1/W	1/W	М	WWTP
Conductivity	1/W	1/W	1/W	М	WWTP
Turbidity	1/D	1/D	1/D	M - F	WWTP
SDI ^a	1/D	1/D	NONE	M - F	OPERATOR
TOC ^b	1/D	1/D	NONE	M - F	OPERATOR
TOC	2/M	2/M	NONE	М	CH2M
Total Chlorine	1/D	1/D	NONE	M - F	WWTP
Free Chlorine	1/D	1/D	NONE	M - F	WWTP
TDS	1/W	1/W	1/W	М	WWTP
Microbial					
Total Coliform	NONE	2/W	NONE	M & W	WTP
Fecal Coliform	NONE	2/W	NONE	M & W	WTP
HPC	2/W	2/W	NONE	M & W	WTP

^aOperator to analyze at sample location using auto analyzer.

CH2M=CH2M HILL's Applied Sciences Laboratory (ASL)

WWTP=McAllen's South Wastewater Treatment Plant Laboratory

WTP=McAllen's Central Water Treatment Plant Laboratory

### 4.5 Data Evaluation

Several of the operating parameters and water quality parameters presented previously were compiled, reduced, and analyzed to evaluate operational, biological, and membrane performance of the treatment systems. Evaluating the flux, TMP, and permeability characterized ZenoGem membrane performance. The primary water quality parameters used to evaluate the effectiveness of the ZenoGem treatment process in producing a high quality RO feedwater were turbidity and SDI. Evaluating the feedwater recovery, normalized product flow (NPF), and the pressure drop across the vessels characterized RO membrane performance.

^bOperator to analyze at sample location using monitor.

^{1/}D=once per day

^{1/}W=once per week

^{2/}W=twice per week

^{2/}M=twice per month

#### 4.5.1 Filtrate Flow and Membrane Flux

Membrane flux is directly proportional to the permeate (filtrate) flow rate as shown in the following equation:

Flux [gfd] = Permeate Flow rate[gpm] x 1440 / Membrane Area  $[ft^2]$ where [gfd] = gallons per day per  $[ft^2]$ 

As the filtrate flow rate increases, the membrane flux increases proportionately.

### 4.5.2 Transmembrane Pressure and Permeability

TMP represents the resistance to flow of water of 1) the membrane, and 2) the materials in the feedwater (foulants) that accumulate at the membrane surface or within the membrane pores. TMP at the start of testing (with a clean membrane) represents only the resistance of the membrane. As foulants accumulate and cannot be effectively removed by backwashing/backpulsing with disinfectant, TMP increases because of the resistance of flow exerted by the foulants. Thus, the rate at which TMP increases is directly proportional to the rate of membrane fouling.

Membrane permeability is inversely proportional to the TMP as shown in the following equation:

Permeability  $[gfd/psi] = Flux [gfd]*1.024^{(25-T)}/TMP$  [pounds per square inch (psi)] where T = feedwater temperature, °C

Permeability is a direct measure of the water flow through the membrane fiber and any foulants that have accumulated on the surface or within the membrane pores. The permeability equation includes a temperature correction factor to remove or "normalize for" the effects of changing temperature on membrane permeability. Increases in temperature increase water flow through the membrane because of decreasing viscosity. This effect must be removed to accurately assess changes in permeability with run time.

### 4.5.3 Turbidity and SDI

Traditionally, the RO membrane manufacturers have established the following as criteria for efficient RO operation:

Turbidity: ≤0.2 NTU

 $SDI: \leq 3$  (based on 15-min test interval)

# **Demonstration Testing Results**

This section presents the results of demonstration plant testing. All data collected during the study are presented in Appendix C as follows:

Operating data for ZenoGem System	Table C-1
Water quality data for ZenoGem System	Table C-2
Operating data for RO System	Table C-3
Water quality data for RO System	Table C-4

Results for water quality parameters routinely analyzed by the McAllen water and wastewater laboratories were communicated to CH2M HILL by facsimile on daily or weekly sampling logs. These data, along with CH2M HILL laboratory data, were tabulated and incorporated into Tables C-1 through C-4 in Appendix C.

## 5.1 Operations

A summary of ZenoGem and RO system operating stages and events is presented in Tables 5.1 and 5.2. Additional details regarding the specific operating stages are discussed below.

**TABLE 5.1**Operating Stages and Events for the ZenoGem System

Stage	Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
Α	-	2/6/99	0.00		Start of Testing (MLSS concentration at 13 g/L and OCP Membrane)
В		3/20/99	677.58		OKC Membrane
	1	3/31/99 - 4/1/99	915.58 - 941.00	25.42	Peak Flow Testing (9.5 gpm for 6 hrs over 24-hour period)
С		5/6/99	1783.00		Decrease MLSS Concentration to 10 g/L
	2	6/1/99	2406.08	2.42	Bubble Point Test
	3	8/12/99 - 8/13/99	4129.58 - 4158.33	28.75	Peak Flow Testing (9.5 gpm for 6 hrs over 24-hour period)
	4	8/16/99 - 8/20/99	4225.08 - 4326.25	101.17	Peak Flow Testing (9.5 gpm for 6 hrs over 24-hour period)

**TABLE 5.1 CONT.**Operating Stages and Events for the ZenoGem System

Stage	Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
	5	8/30/99 - 9/1/99	4561.08	51.50	Recovery (Full Tank) Clean
	6	9/14/99 - 9/16/99	4875.91	50.25	Raise Membranes
	7	9/17/99 - 9/27/99	4894.16 - 5136.25	242.09	Cycled Aeration to the Membrane Tank (10 sec on/off)
	8	9/27/99 - 9/29/99	5136.25 - 5186.91	50.66	Peak Flow Testing without Cycled Aeration
D		10/4/99	5303.41		Decrease MLSS Concentration to 6 g/L
	9	10/7/99 - 10/8/99	5328.75 - 5352.50	23.75	Cycled Aeration to the Membrane Tank (10 sec on/off)
	10	10/8/99 - 10/13/99	5352.50 - 5476.00	123.50	Peak Flow Testing with Cycled Aeration to Membrane Tank
	11	10/14/99 - 10/19/99	5476.00 - 5615.66	139.66	Normal Flow with Cycled Aeration to Membrane Tank
	12	10/19/99 - 11/2/99	5615.66 - 5948.25	332.59	Normal Flow with Cycled Aeration to Both Tanks (Aeration Tank at 15 min on/off)
	13	11/2/99	5948.25		End of Testing

**TABLE 5.2**Operating Stages and Events for the RO System

Stage	Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
Α		4/21/99	0.00		Startup
В		5/19/99	0.00		Start of Testing (Target Feed pH = 6.8)
	1	5/24/99 - 5/25/99	114.89 - 147.69	32.80	1st Cleaning (Citric Acid:Stages 1 and 2)
	2	5/30/99	256.41		Decrease Recovery to 50%
	3	6/1/99 - 6/2/99	305.9 - 328.42	22.52	2nd Cleaning (Citric Acid:Stages 1 and 2)
	4	6/8/99 - 6/10/99	475.88 - 526.38	50.50	3rd Cleaning (Citric Acid:Stages 1 and 2 followed by Caustic:Stage 1)
С		6/11/99	544.50		Decrease Recovery to 50% (Stage 2 Removed from Service)
D		7/7/99	1176.51		Stage 2 Returned to Service (50% Recovery)

TABLE 5.2 CONT.

Operating Stages and Events for the RO System

Stage Event	Date(s)	Run Time (hrs)	Duration (hrs)	Description
5	7/8/99	1196.78		Increase Recovery to 60%; Decrease Feed pH to 6.5
6	7/9/99	1208.73		Increase Recovery to 70%; Decrease Feed pH to 6.0
7	7/22/99	1532.92		Set Target pH to Concentrate pH = 5.6 (Feedwater pH = 5.0)
8	7/24/99 - 7/27/99	1578.67 - 1650.27	71.60	4th Cleaning (Citric Acid:Stages 1 and 2)
9	8/10/99	1985.17		Increase Recovery to 75%
10	8/30/99 - 9/1/99	2464.77- 2519.55	54.78	Unit Down due to ZenoGem System Recovery (Full Tank) Clean
11	9/2/99 - 9/8/99	2543.79 - 2687.50	143.71	5th Cleaning (Citric Acid:Stages 1 and 2); Acid Pump Failure
12	9/14/99 - 9/16/99	2830.65 - 2880.25	49.60	Unit Down due to Raising ZenoGem System Membranes
13	9/23/99	3041.97		Increase Recovery to 80%
14	10/4/99 - 10/6/99	3308.51 - 3359.81	51.30	Unit Down due to Decreasing ZenoGem System MLSS
15	10/8/99	3399.11		End of Routine Testing
16	10/21/99	3715.41		End of Special Testing

### 5.1.1 Startup Activities

**ZenoGem Equipment Commissioning.** ZENON field service technicians arrived at the plant site on January 11, 1999, and performed commissioning of the ZenoGem system through February 6, 1999. ZenoGem system commissioning included equipment installation; membrane bubble point and clean water flux testing; introduction and concentration of mixed liquor in the bioreactor tank; and operation on SDS to establish steady-state biological treatment (carbonaceous and nitrogenous oxidation) and membrane treatment. Operational activities included establishing target MLSS concentrations in both the membrane (process) and aeration tanks; air flow rates and dissolved oxygen (DO) levels in both tanks; solids recirculation rate between tanks; and membrane permeate flow (flux) rate. The ZenoGem system achieved steady-state operation on March 22, 1999.

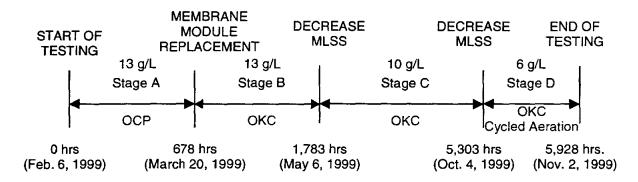
**RO Equipment Commissioning.** BOR project managers performed commissioning of the RO system during two site visits on February 2 through February 12, 1999, and on March 15 through March 19, 1999. During the first visit, RO system commissioning included installation of plumbing and electrical connections; delivery and storage of chemicals; modifications to the computer recording system; PLC programming; and installation of temporary membranes. During the second visit, additional RO system commissioning

included instrument calibration; SDI auto analyzer installation; system cleaning and disinfection; installation of permanent membranes and integrity tests. At that time, the RO system was scheduled for startup on March 22, 1999, coincident with steady-state operation of ZenoGem system. However, due to ZenoGem system special testing, replacement of defective chloramine metering pump parts, difficulties in attaining stable and effective chloramine stock solutions and residuals, combined with minor RO equipment problems, RO system start of testing was delayed until April 21, 1999.

#### 5.1.2 Operating Stages

**ZenoGem System.** The ZenoGem operating period has been divided into four separate operating stages as shown in Exhibit 5.1. The ZenoGem operating stages were as follows:

**EXHIBIT 5.1** ZenoGem Operating Stages



Stage A represents the start of testing using the OCP UF membrane and a target MLSS concentration of 13 g/L. During this stage, the aeration and membrane tanks were seeded with activated sludge from the WWTP and MLSS levels increased step-wise to the target level. The system accumulated 321 operating hours out of a possible 678 available hours, for an online factor of 0.47 (47 percent). This online factor includes two separate periods when the system was offline due to failure and subsequent replacement of the recirculation pump impeller, feedwater inlet level sensor replacement, and membrane module replacement.

The originally supplied membrane module, which used the OCP membrane, has recently been classified by ZENON as their drinking water membrane and is marketed primarily as an UF membrane for the treatment of natural raw water supplies to produce potable water. This membrane, which has a nominal pore size of 0.035 microns, has been found to have flux limitations when operated on high MLSS wastewaters and consequently is being phased out by ZENON in favor of the OKC MF membrane for wastewater treatment. The OKC membrane is more porous, with a nominal pore size of 0.4 microns. Initial in-house testing by ZENON showed the OKC membrane to operate at higher permeability and to benefit from a lower rate of fouling on wastewater, particularly when operating at peak loading conditions. Consequently, it was decided jointly by ZENON and CH2M HILL that the OKC membrane would be better suited for the

McAllen IPR application. After the OCP module was replaced with a new OKC module, the permeate flow rate was slowly increased to the target 6.5 gpm.

Stage B represents the period of operation using the OKC module and a target MLSS concentration of 13 g/L. During this stage, the system accumulated 1,077 operating hours out of a possible 1,105 available hours, for an online factor of 0.97 (97 percent). This online factor includes a short period of time when the system was offline due to replacement of a valve in the aeration tank. A single-day peak flow test was conducted during the latter part of this stage.

Stage C represents the period of operation at a target MLSS concentration of 10 g/L. During this stage, the system accumulated 3,416 operating hours out of a possible 3,520 available hours, for an online factor of 0.97 (97 percent). This online factor includes three separate periods when the system was offline due to bubble point testing, clean water flux testing/full tank soaking, and to raise the module height (in the membrane tank). During this stage, peak flow testing continued and cycled aeration (to the membrane tank only) was initiated.

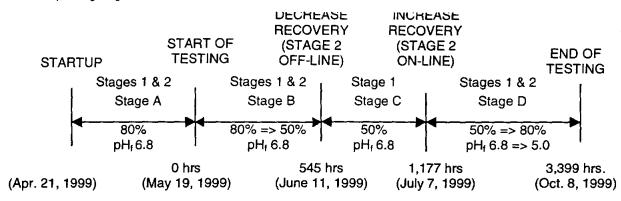
The target MLSS concentration was decreased from an initial target of 13 g/L to 10 g/L after 1,783 total available hours of operation following detailed discussions with ZENON technical personnel. Based on ZENON experience, lowering the MLSS concentration to 10 g/L provides for improved operability (lower membrane fouling) and more stable biological treatment. As discussed later in this section, MLSS reduction also improved oxygen transfer from the bulk fluid to the biomass, thereby improving nitrification efficiency and decreasing the degree of denitrification. Consequently, it was decided jointly by ZENON and CH2M HILL that the decrease in MLSS concentration would be preferred for the McAllen indirect potable reuse application.

Stage D represents the period of operation at a target MLSS concentration of 6 g/L. During this stage, the system accumulated 596 operating hours out of a possible 645 available hours, for an online factor of 0.92 (92 percent). This online factor includes a short period of time when the system was offline to decrease the MLSS concentration (i.e., wasting half the aeration tank volume) and subsequent aeration-only operation to reestablish proper biomass condition. Peak flow testing continued and cyclic aeration to the membrane and aeration tanks was also initiated during this stage.

The MLSS concentration was decreased from 10 g/L to 6 g/L after 5,303 total available hours of operation following detailed discussions with ZENON technical personnel. ZENON indicated that maintenance of stable membrane permeability during flow peaking would most likely depend on sludge filterability characteristics as indicated by the sludge capillary suction time (CST). Sludges with high CSTs are viscous and difficult to filter. The sludge generated in the ZenoGem process had a high CST (exceeding 100 seconds). ZENON indicated that for such sludge, reducing the MLSS concentration reduces the resistance to filtration and would maximize permeability during flow peak peaking. Consequently, it was decided jointly by ZENON and CH2M HILL to perform peak flow tests at a lower MLSS concentration in order to demonstrate maximum performance.

**RO System.** The RO operating period has been divided into four separate operating stages, as shown in Exhibit 5.2. Since the hour meter on the system was not functional, the online factor for each stage of operation was approximated by system downtimes recorded by the operators. The first two RO operating stages were as follows:

EXHIBIT 5.2
RO Operating Stages



Stage A represents the period of operation from startup to the actual start of steady state testing (commissioning phase). During this stage, the system was off line approximately 70 percent of the time due to numerous downtimes associated with PLC reprogramming and tuning to optimize control of feedwater flow and pH; failure and subsequent replacement of the scale inhibitor feed pump; de-commissioning of automatic sampling valves; and troubleshooting acid feed pump loss of prime. Data collected during this phase was considered representative of continued startup activities and system troubleshooting. By May 19, the system was successfully online, and the actual start of steady state testing was achieved.

Stage B represents the period of operation at a target recovery of 80 percent. During this 545-hour stage, the system was off line approximately 19 percent of the time due to three RO membrane cleanings and maintaining target pH.

RO Feedwater Pretreatment to Control Membrane Fouling. RO membrane elements are subject to fouling during extended operation caused by both suspended and sparingly soluble salts. Suspended matter includes organic and inorganic colloids and microorganisms. Sparingly soluble salts, such as carbonates, sulfates, and silica, can precipitate from solution as the RO process concentrates them. Suspended particles accumulate on the membrane surface causing biofouling and colloidal fouling, and they can block feed channels thereby increasing the pressure drop across the system. These phenomenon reduce water permeability through the RO membranes causing flux decline and increased salt passage. The nature and rapidity of fouling depends on the condition of the feedwater. Fouling is progressive, and, if not controlled early, can impair the RO system performance in a relatively short time. For these reasons, fouling must be controlled.

Particulate fouling is addressed through the use of the ZeeWeed MF membrane. Chloramines were batched and dosed into the RO feedwater at a target dose of 1 to 2 mg/L to prevent biological growth (biofouling) of the RO elements. As described in an

earlier section, mineral precipitation is controlled through a combination of acidification and scale inhibitor addition. The last two RO operating stages are described below.

Stage C represents the period of operation at a target recovery of 50 percent (operating first stage vessels only) to demonstrate that performance losses observed in Stage B resulted from mineral precipitation (as opposed to particulate or colloidal fouling). During this 632-hour stage, the system was online 100 percent of the time.

Stage D represents the period of operation at recovery of 50 to 80 percent (operating first and second stage vessels) and acidification of the concentrate stream to a reduced feedwater pH of 5.0 (concentrate target pH of 5.6) to control calcium phosphate and calcium carbonate precipitation. During this 2,222-hour stage, the system was off line approximately 10 percent of the time due to two RO membrane cleanings. It excludes three downtimes associated with ZenoGem full tank soaking, raising module height, and decreasing the MLSS concentration.

## 5.2 ZenoGem Testing Results

### 5.2.1 ZenoGem Operating Conditions

Table 5.3 presents the target and average operating conditions for the ZenoGem system during Stage A operation. The system operated at a target MLSS concentration of 13 g/L using the OCP UF membrane. After 678 hours of startup activities, the membrane was replaced with the OKC MF membrane.

TABLE 5.3
Stage A Average Operating Conditions for the ZenoGem System

Parameter	Target ^a	Normal Flow
Aeration Tank Air (scfm)	> 45	48
Backpulse Duration (sec)	15	15
Backpulse Frequency (min)	10	10
Biomass Recirculation Rate (gpm)	> 36	26.2
Flux (gfd)	18.7	17.3
Membrane Tank Air (scfm)	25	25
Normalized Permeability (gfd/psi)	5	20.8
Permeate Flowrate before Backpulse (gpm)	6.5	6.0
Permeate Flowrate after Backpulse (gpm)		6.0
Temperature (degrees C)		26.2
TMP (psi)	2.5 - 8.5	1.34
Vacuum before Backpulse (in Hg)	5.1 - 17.3	2.73
Vacuum after Backpulse (in Hg)		2.57

^aWhere target left blank, no target was established.

^bValues calculated when permeate flowrate reached 6 gpm.

Table 5.4 presents the target and average operating conditions for the ZenoGem system during Stage B operation. The system continued to operate at a target MLSS concentration of 13 g/L during this stage. After 916 hours of operation (Event 1), the permeate flowrate was increased for 25 hours to determine the short-term impact of higher membrane loading on permeability and TMP.

**TABLE 5.4**Stage B Average Operating Conditions for the ZenoGem System

Parameter	Target ^a	Normal Flow	Peak Flow (Event 1)
Aeration Tank Air (scfm)	> 45	43	42
Backpulse Duration (sec)	15	15	15
Backpulse Frequency (min)	10	10	10
Biomass Recirculation Rate (gpm)	> 36	38.3	39.5
Flux (gfd)	18.7/27.3 ^b	18.5	27.3
Membrane Tank Air (scfm)	25	25	25
Normalized Permeability (gfd/psi)	5	17.82	13.19
Permeate Flowrate before Backpulse (gpm)	6.5/9.5 ^b	6.40	9.50
Permeate Flowrate after Backpulse (gpm)		6.40	9.50
Temperature (degrees C)		28	25.8
TMP (psi)	2.5 - 8.5	1.2	2.1
Vacuum before Backpulse (in Hg)	5.1 - 17.3	2.66	4.17
Vacuum after Backpulse (in Hg)		2.59	4.12

^aWhere target left blank, no target was established.

Table 5.5 presents the target and average operating conditions for the ZenoGem system during Stage C operation. At the beginning of this stage (after 1,783 hours of operation), the MLSS concentration was decreased to 10 g/L. From 4,130 to 4,158 hours (Event 3) and from 4,225 and 4,326 hours (Event 4) of operation, the permeate flow rate was increased by 46 percent (6.5 to 9.5 gpm) for a period of 6 hours (flow peaking) over a 24-hour period to simulate the types of hydraulic peak loading that typically occur in a conventional WWTP. This was done to determine if the MBR system could be operational in the same manner or if additional means would be required to ensure slower changes in loading to the system. After 4,876 hours of operation, the membrane module height was raised (Event 6) to minimize sludge accumulation on the module aerators during non-aeration periods. From 4,894 to 5,136 hours (Event 7) of operation, air was cycled to the membrane tank at an applied rate of 30 scfm for 10 seconds on and 10 seconds off to evaluate the effect of intermittent aeration on operations and membrane performance. From 5,136 to 5,187 hours (Event 8) of operation, flux peaking was conducted without intermittent aeration to the membrane tank.

^bTarget value during flow peaking.

**TABLE 5.5**Stage C Average Operating Conditions for the ZenoGem System

			Peak Flow	Normal Flow with Cycled Aeration to Membrane Tank Only	
Parameter	Target ^a	Normal Flow	(Events 3,4,8)	(Event 7)	
Aeration Tank Air (scfm)	> 45	59	61	63	
Backpulse Duration (sec)	15	15	15	15	
Backpulse Frequency (min)	10	10	10	10	
Biomass Recirculation Rate (gpm)	> 36	48.2	47.5	44.6	
Flux (gfd)	18.7/27.3 ^b	18.7	26.6	18.7	
Membrane Tank Air (scfm)	25/30°	25	25	31	
Normalized Permeability (gfd/psi)	5	6.61	3.05	8.67	
Permeate Flowrate before Backpulse (gpm)	6.5/9.5 ^b	6.50	9.20	6.50	
Permeate Flowrate after Backpulse (gpm)		6.70	11.10	7.10	
Temperature (degrees C)		31.2	31.9	30.3	
TMP (psi)	2.5 - 8.5	2.8	7.5	2.4	
Vacuum before Backpulse (in Hg)	5.1 - 17.3	5.70	15.30	4.90	
Vacuum after Backpulse (in Hg)	<del> </del>	5.10	15.90	4.10	

^aWhere target left blank, no target was established.

^bTarget value during flow peaking.

Per discussions with ZENON, cycled aeration operation to the membrane tank was planned at 10 seconds on and 10 seconds off. However, a cycle time of 15 seconds on and 15 seconds off was implemented at the site due to communication and programming error between ZENON and the demonstration plant operators. ZENON Corporate Technology tested a number of different air cycle times at other pilot locations and concluded that 10 seconds off is the maximum allowable period before a decline in permeability is observed. Longer air OFF periods allow the mixed liquor solids to accumulate in the fiber bundle and are not subsequently removed by the air pulse during the ON cycle. Thus, the error in cycle time implemented is significant enough to cause the permeability decline observed during cycled aeration events as discussed in Section 5.2.2.

^cApplied rate increased to 30 cubic feet per minute (cfm) during intermittent aeration.

Table 5.6 presents the target and average operating conditions for the ZenoGem system during Stage D operation. At the beginning of this stage (after 5,303 hours of operation), the MLSS concentration was decreased to 6 g/L. From 5,329 to 5,353 hours (Event 9) of operation, air was again cycled to the membrane tank. From 5,353 to 5,476 hours (Event 10) of operation, flux peaking was conducted; however this time with intermittent aeration to the membrane tank. From 5,476 to 5,616 hours (Event 11) of operation, the flowrate was reduced to normal conditions and air continued to cycle to the membrane tank. From 5,616 hours to the end of testing (Event 12), air was cycled to the aeration tank at an applied rate of 45 scfm for 15 minutes on and 15 minutes off to evaluate the effect of intermittent aeration on biological treatment performance (i.e., to concurrently nitrify and denitrify).

**TABLE 5.6**Stage D (Alternative Operating Mode) Average Operating Conditions for the ZenoGem System

		Normal	Normal Flow with Cycled Aeration to Membrane Tank Only	Peak Flow with Cycled Aeration to Membrane Tank Only	Normal Flow with Cycled Aeration to Membrane Tank Only	Normal Flow with Cycled Aeration to Membrane and Aeration Tanks
Parameter	Target ^a	Flow	(Event 9)	(Event 10)	(Event 11)	(Event 12)
Aeration Tank Air (scfm)	> 45	65	66	64	66	65
Backpulse Duration (sec)	15	15	15	15	15	15
Backpulse Frequency (min)	10	10	10	10	10	10
Biomass Recirculation Rate (gpm)	> 36	47.3	48.0	47.0	46.2	43.1
Flux (gfd)	18.7/27.3 ^b	18.7	18.7	27.3	18.7	18.7
Membrane Tank Air (scfm)	25/30°	25	32	32	32	32
Normalized Permeability (gfd/psi)	5	7.27	7.52	3.25	3.86	3.42
Permeate Flowrate before Backpulse (gpm)	6.5/9.5 ^b	6.50	6.50	9.5	6.50	6.50
Permeate Flowrate after Backpulse (gpm)		6.90	6.70	11.50	6.90	6.90
Temperature (degrees C)		30.3	30.0	31.6	29.0	26.4
TMP (psi)	2.5 - 8.5	2.39	2.2	7.37	4.5	5.7
Vacuum before Backpulse (in Hg)	5.1 - 17.3	4.90	4.50	15.0	9.10	11.50
Vacuum after Backpulse (in Hg)		4.30	4.60	16.30	8.20	10.50

^aWhere target left blank, no target was established.

^bTarget value during flow peaking.

^cApplied rate increased to 30 cfm during intermittent aeration.

#### 5.2.2 ZeeWeed Membrane Performance

**Permeate Flow and Membrane Flux.** Figure 5.1 illustrates changes in ZenoGem permeate flow and flux as a function of operating time. During Stage A (prior to membrane replacement), flow and flux were increased in step-wise increments to "condition" the membrane fibers to the mixed liquor. This was done to prevent the fibers from becoming fouled. Permeate flow was held constant during Stages B through D except for five events:

- Event 1: Flow increased for 25 hours to determine the short-term impact of higher membrane loading on permeability and TMP; and
- Events 3, 4, 8 and 10: Flow increased by 46 percent (6.5 to 9.5 gpm) for a period of 6 hours (flow peaking) over a 24-hour period to simulate WWTP peak hydraulic loading.

The increases caused a corresponding increase in TMP and decrease in permeability; however both changes were reversed once the flow was decreased to the target level. Thus, the temporary flux increase caused only reversible membrane fouling and flow peaking for short (one-day) periods of time can occur in response to actual WWTP loading without causing a permanent increase in fouling.

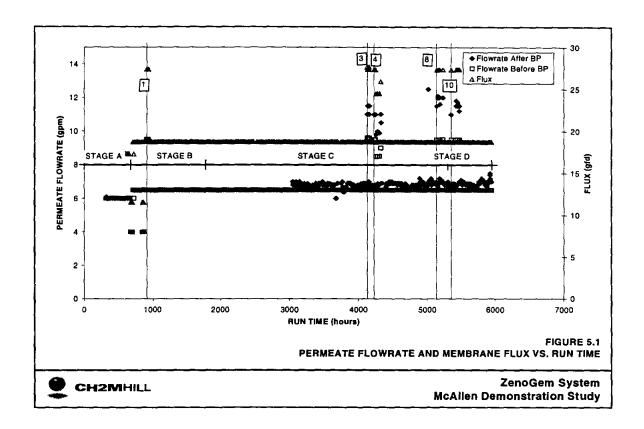
**Transmembrane Pressure.** Figure 5.2 illustrates changes in ZenoGem TMP as a function of operating time (permeate flow is also shown for reference).

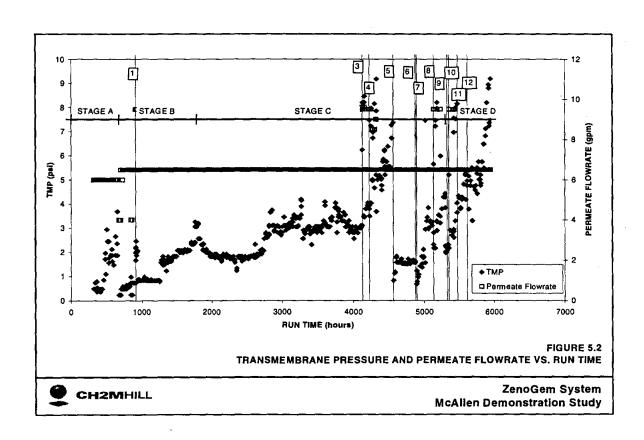
Stage A. TMP increased gradually as permeate flow was increased to the target value. The sharp decline in TMP that occurred at 653 hours was caused by continuous aeration of the module during the 12-day period when the ZenoGem system was offline due to recirculation pump failure and replacement. Continuous aeration in the absence of permeation was very effective in reducing membrane fouling.

Stage B. During the latter part of Stage B, TMP steadily increased even when permeate flowrate (and membrane flux) were held constant. This increase in TMP clearly indicates that membrane fouling was occurring at the higher MLSS concentration. The short-term flow peaking during Stage B (Event 1) caused a temporary increase in TMP that was reversed once flux was reduced.

Stage C. During operation at intermediate (10 g/L) MLSS concentration, TMP first decreased and then increased very gradually over a 1,000-hour period, indicating: 1) a very low rate of fouling, and 2) maintenance cleans were more effective in controlling fouling at the lower MLSS concentration. The step increase in TMP at ~2,700 hours was caused by a temporary loss of air scour in the membrane tank. Flow peaking during Stage C (Events 3 and 4) resulted in a more rapid rate of TMP increase, demonstrating that flow peaking of the membrane on a daily basis over an extended operating period caused a significant increase in fouling rate at the lower MLSS concentration. TMP increased to the maximum value (8 psi) which required a recovery (full tank) clean (Event 5) to reduce TMP to clean membrane levels (0.8 psi). At the end of Stage C, TMP rapidly increased when air was cycled to the membrane tank (Event 7) and again during flow peaking without cycled aeration (Event 8).

Stage D. During this stage, the impact of both flow peaking and cycled (intermittent) aeration was evaluated at low (6 g/L) MLSS concentration. The data in Figure 5.2 shows TMP increases were rapid when flow peaking and cycled aeration was practiced, consistent with flow peaking effect observed in Stage C. The impact of cycled aeration alone (no flow peaking) is more difficult to ascertain. TMP rise rate following Event 11 and the first part of Event 12 was low, but increased rapidly near the end of testing. The latter effect may be the result of operation at high TMP levels (significant fouling present) rather than from intermittent aeration. Future testing using intermittent aeration should be conducted with a clean membrane to more clearly determine its impact on membrane fouling. It should be noted that during flow peaking events, the vacuum after backpulsing was slightly higher than before backpulsing. This indicates that backpulsing had little effect in reducing the TMP (or increasing permeability) during flow peaking. During normal flow operation, post-backpulse TMP was always less than pre-backpulse values.



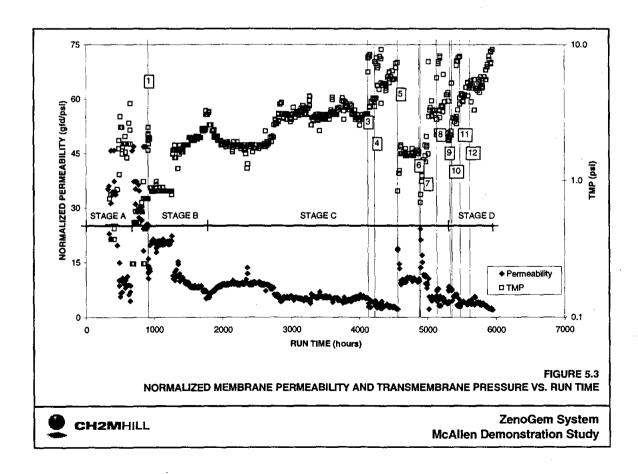


#### Permeability.

Stages A – C. Figure 5.3 illustrates changes in ZenoGem permeability as a function of operating time (TMP is also shown for reference). During Stage B, permeability (normalized to 20°C) steadily decreased as TMP increased, indicating membrane fouling at the higher MLSS concentration of 13 g/L. In contrast, at the lower MLSS concentration in Stage C, permeability increased and remained relatively constant as TMP very gradually increased. However during the flow peaking test periods (Events 3, 4 and 8), permeability sharply decreased as TMP increased. This showed that the MBR system must be provided with a means of ensuring slow changes in peak loading. The peak loading cannot be raised as quickly over a 24-hour period as in a conventional WWTP. These results also confirm that ZenoGem operation at 10 g/L MLSS concentration and constant flux provides for very stable system operation.

Following raising of the membrane module and subsequent aeration of the membrane tank without operation of the permeate pump (no permeation), permeability decreased (Event 7). Subsequent operation with cycled aeration to the membrane tank produced a rapid and significant decrease in permeability.

Stage D. Operation under conditions of cycled aeration and/or flow peaking generally caused more rapid declines in permeability than operation at normal (steady) flow and continuous aeration, consistent with results under similar conditions during Stage C. This performance indicates that cycled aeration is less effective than continuous aeration in controlling foulant accumulation.



### 5.2.3 ZenoGem Biological Treatment Performance

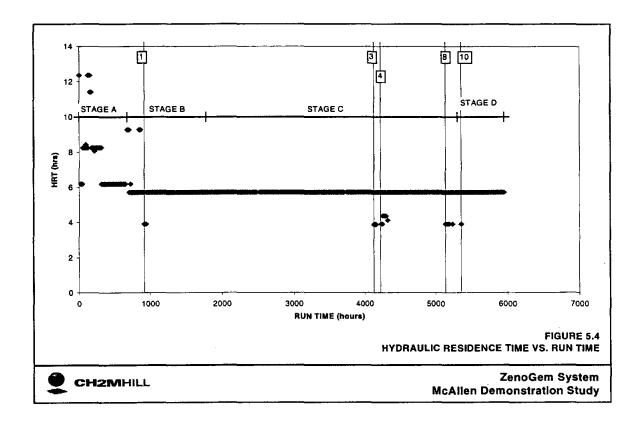
Table 5.7 presents the average conditions within the ZenoGem bioreactor (volume weighted composite of the aeration and membrane tanks) during each stage of operation.

TABLE 5.7 Results of Biological Treatment Performance Analyses for the ZenoGem System

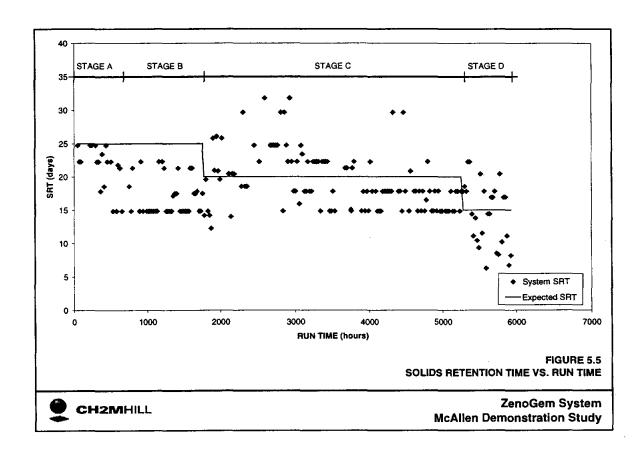
Parameter	Target ^a	Stage A	Stage B	Stage C	Stage D
DO (mg/L)	> 1.5	2.78	1.53	2.00	3.19
OUR (mg O ₂ /L-min)	1.0 - 1.5			0.87	1.34
MLSS (mg/L)	13,000 (Stage A & B) 10,000 (Stage C) 6,000 (Stage D)	11,454	14,070	10,634	6,661
MLVSS (mg/L)		8,339	10,243	7,655	4,873
Sludge Wasted Daily (gals)	90 (Stage A & B) 110 (Stage C) 150 (Stage D)	96	131	114	182
Sludge Yield		1.27	1.50	1.14	2.03
HRT (hrs)	5.7/3.9 ^b	6.2	5.8/3.9 ^b	5.7/4.0 ^b	5.7/3.9 ^b
System SRT (days)	25 (Stage A & B) ^c 20 (Stage C) ^c 15 (Stage D) ^c	21.29	16.79	19.25	14.04

^aWhere target left blank, no target was established. ^bValue during flow peaking. ^cExpected value based on control variables.

**Hydraulic Residence Time.** Figure 5.4 presents the HRT for the ZenoGem bioreactor. The average HRT for Stage A was slightly higher than the target range due to the step-wise increase in permeate flow to the target value of 6.5 gpm. HRT was held constant and near the target range during subsequent stages, except during flow peaking (Events 1, 3, 4, 8 and 10) when the HRT dropped by 32 percent (from 5.7 hrs at 6.5 gpm down to 3.9 hours at 9.5 gpm). A 6.5-hour HRT was selected to ensure sufficient retention time to achieve complete nitrification based on prior testing at McAllen and other locations. This compares with a HRT of 30 hours for the McAllen WWTP (3 to 4 g/L MLSS) and reflects the greater biochemical oxidation efficiency at the higher MLSS levels.



**Solids Retention Time.** Figure 5.5 presents the SRT for the ZenoGem bioreactor. The average SRTs were near expected values during each stage, except for Stage B. A higher SRT would be expected for Stage B (versus Stage C) given that the MLSS concentration in the bioreactor was higher and loadings were similar. A lower SRT during Stage B resulted from excess sludge wasting (average 150 gpd compared to the target 110 gpd) in an effort to maintain the target MLSS concentration of 13 g/L. The ZenoGem process has the capability to be operated at a longer SRT (15 to 25 days) than the McAllen WWTP (15 days) because it is not limited by sludge settleability that limits the maximum MLSS concentration that can be accumulated in the system when using clarifiers rather than membranes for biomass retention.

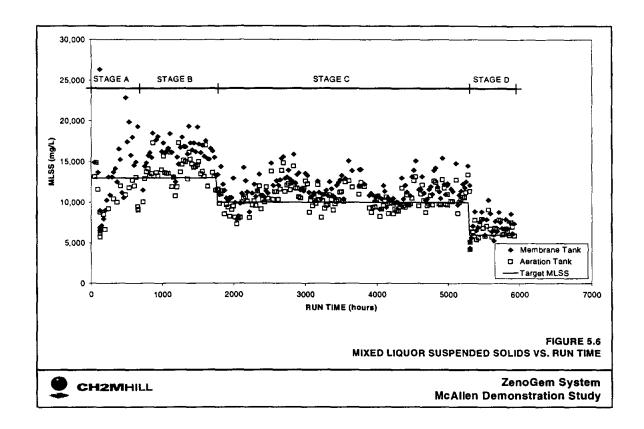


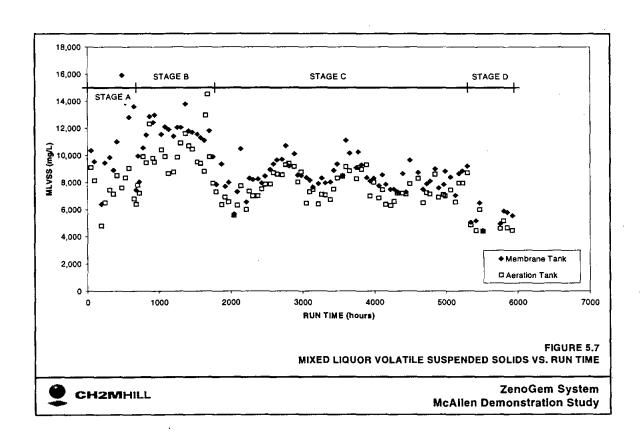
**Mixed Liquor Suspended and Volatile Suspended Solids.** The McAllen WWTP and the ZenoGem system both use the suspended growth process (activated sludge) to achieve biological treatment. Removal of carbonaceous organic matter in a suspended growth process is directly dependent on the concentration of biomass present in the mixed liquor (activated sludge). Biomass levels can be roughly estimated by measuring the concentration of either the MLVSS or MLSS in the treatment reactor. The latter is more practical for maintaining proper bacterial levels because it is an easier and more rapid method. MLVSS is a more accurate measure of bacterial content because it excludes some of the inert fraction of the suspended solids, however it requires an additional drying and weighing step, which adds time and effort.

MLSS and MLVSS levels measured in the ZenoGem membrane (bioreactor) and aeration tanks are shown in Figures 5.6 and 5.7. The concentration of both parameters should be the same in both tanks under ideal conditions (infinite sludge recirculation rate and exact sludge wasting rates). The average MLSS concentrations in the tanks were at or near target values during each stage. Lower MLSS concentrations in Stage A are representative of startup operations (seeding and MLSS concentration increase to steady-state conditions). Higher than planned MLSS concentrations in Stage B resulted in greater sludge wasting volumes and higher sludge yields. The most common range of MLVSS values for conventional air activated sludge systems is 2,000 to 2,500 mg/L (WEF, 1991). Although air based conventional systems can operate at somewhat higher MLVSS level (up to 3,000 mg/L in practice), sludge settleability decreases as MLSS levels decrease. Settleability is not an issue for the ZenoGem process because separation is not dependent on gravity settling but rather on membrane filtration. However, sludge dewatering characteristics are important as they directly impact observed membrane permeability.

The significance of the greater MLVSS levels is that the ability to remove CBOD $_5$  is directly proportional to bacterial density in the activated sludge tank (or bioreactor). By maintaining higher MLVSS concentrations, the ZenoGem process can attain comparable reduction in CBOD $_5$  at a much lower hydraulic retention time. This is clearly illustrated in Table 5.7, where the average HRT for ZenoGem is about 6 hours versus 30 hours for the WWTP. In fact, as discussed in the following section, CBOD $_5$  removal efficiency was slightly better for the ZenoGem system. In other words, the same, or even greater, degree of treatment can be accomplished in roughly one-fifth of the time or volume used by the extended aeration process used at McAllen. Assuming similar depths for an aeration basin and ZenoGem bioreactor, the tankage area of the ZenoGem process would require only 20 percent of the land area required for the extended aeration basins. It should be noted, however, that it is possible that acceptable treatment could have been achieved in the full-scale McAllen WWTP if another activated sludge process was used.

The average ratio of MLVSS to MLSS for the ZenoGem process was 0.73. This is at the lower end of the typical range (0.7 to 0.9) and reflects the absence of a primary sedimentation step ahead of the ZenoGem process to settle and reduce inerts.



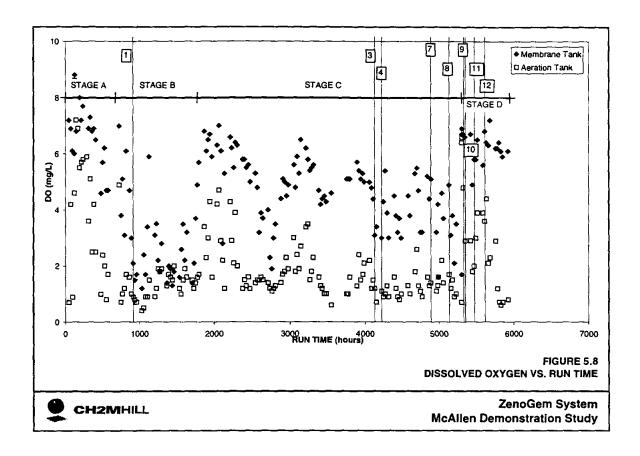


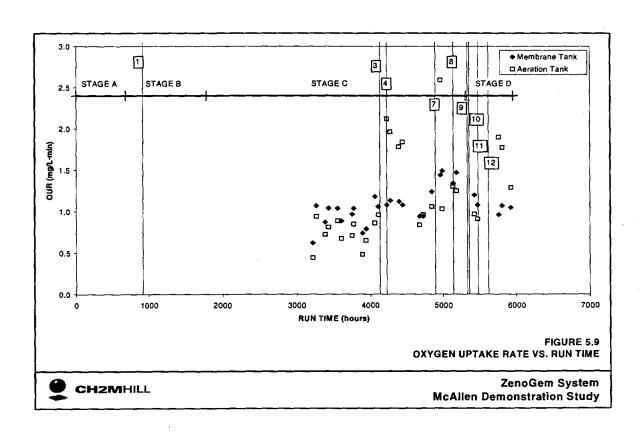
**Dissolved Oxygen.** Proper DO levels must be maintained in the activated sludge process to enable efficient degradation of both carbonaceous organic matter and organic nitrogen. Generally, DO levels in the activated sludge process should be maintained around 2.0 mg/L or greater to ensure that sufficient oxygen is present to achieve effective BOD₅ removal and nitrification (WEF, 1990). Lower levels will impede nitrification. DO levels of 1.5 mg/L or greater were targeted for the ZenoGem system.

DO levels in the membrane and aeration tanks are presented in Figure 5.8. DO levels were considerably higher than planned during Stage A as the air flowrate was optimized. Lower DO levels in the aeration tank than the membrane tank (38 to 58 percent lower throughout the study) resulted from inadequate air supply. Low DO levels in both tanks during Stage B resulted from high oxygen demand due to high BOD and TSS loading in the feedwater and to the higher MLSS concentration. Periodic increases in the ammonia content of the feedwater resulted in low DO levels during the other stages due to the increased oxygen demand required for nitrification.

**Oxygen Uptake Rate.** OURs in the membrane and aeration tanks are presented in Figure 5.9. OUR values were less than target from startup to the middle of Stage C due to error in the analytical method used. Samples were held for several hours prior to analysis (rather than being performed immediately), thereby decreasing oxygen uptake potential. After 3,216 hours of operation, OUR analysis was performed correctly and OUR values increased significantly.

**Sludge Yield.** Sludge yield coefficient, *Y*, is a measure of the amount of biological solids produced by a wastewater treatment process relative to the amount of organic matter removed. Ideally, the sludge yield should be as low as possible to minimize the need to dispose of sludge. For the extended aeration process used at the WWTP, *Y* is typically low because the microorganisms in the activated sludge operate in the endogenous phase based on the long mean SRT for this type of system (15 days). *Y* values for the ZenoGem system should be somewhat lower than the WWTP because the ZenoGem system operated at slightly higher SRTs; however this was not the case. The average sludge yield for the ZenoGem process ranged from 1.14 to 2.03 grams of sludge produced per gram of CBOD₅ removed. Based on the data available from the McAllen WWTP control logs, sludge yield for the McAllen WWTP was 0.73.





### 5.2.4 ZenoGem Water Quality Impacts

Several water quality parameters were measured to monitor the effectiveness of ZenoGem biological treatment and membrane filtration in improving wastewater quality. Table 5.8 presents the results of water quality analyses of the ZenoGem feed (SDS) and permeate during Stages A and B. The system operated at constant flow/flux during both stages, except for a brief 25-hour flow peaking period at the end of Stage B.

TABLE 5.8
Results of Stages A and B Water Quality Analyses for the ZenoGem System

					Stag	age B			
Parameter		Sta	age A	Norm	al Flow	Peak Flo	w (Event 1)		
Physical/Chemical	Permeate Target ^a	Feed	Permeate	Feed	Permeate	Feed	Permeate		
pH		7.23	7.33	7.22	7.59	7.12	7.58		
Temperature (degrees C)		25.6	26.3	27.1	28.2	26.0	26.5		
Turbidity (NTU)	< 0.2		0.17		0.24		0.34		
Conductivity (µS/cm)		1,986	1,714	2,138	1,716	1,975	1,765		
COD (mg/L)		300	5.0	620	15.0				
CaH (mg/L as CaCO₃)					331		360		
ALK		391	154	422	203		230		
Biological						<del>-</del> - <del>-</del> - · · · · · · · · · · · · · · · · · ·			
CBOD ₅ (mg/L)	< 2	228	1.77	230	0.85	276	1.98		
TSS (mg/L)	< 1	238	0.30	183	0.27	152	0.40		
T-Phosphorus (mg/L as P)		20.65	0.96	14.00	0.18				
NH ₃ -N (mg/L as N)	< 0.5	26.93	0.16	25.36	5.68	26.50	6.58		
TKN (mg/L as N)		111	3.31	75	9.73				
NO ₂ /NO ₃ -N (mg/L as N)		0.03	19	0.17	5.83				
Total Nitrogen (mg/L as N)		111	22	75	16				
Microbial					·				
Total Coliforms (CFU/100mL)	< 2.2		3.0		109.4		84.0		
Fecal Coliforms (CFU/100 mL)	0		4.5		41.9		175.0		
HPC (CFU/mL)	< 500		1,619		3,276				

^aWhere target left blank, no target was established. μS/cm=microSiemens per centimeter.

Table 5.9 presents the results of water quality analyses of the ZenoGem feed and permeate during Stage C. The system operated at constant flow/flux during this stage, except during three flow peaking events and a 242-hour period when air was cycled to the membrane tank.

**TABLE 5.9**Results of Stage C Water Quality Analyses for the ZenoGem System

				Pea	k Flow	Normal Flow with Cycled Aeration to Membrane Tank Only		
Parameter		Normai Flow		(Even	ts 3,4,8)	(Ev	ent 7)	
Physical/Chemical	Permeate Target ^a	Feed	Permeate	Feed	Permeate	Feed	Permeate	
рН		7.16	7.42	7.20	7.37	7.20	7.35	
Temperature (degrees C)		29.6	30.8	30.6	31.5	28.7	29.9	
Turbidity (NTU)	< 0.2		0.15		0.10		0.15	
Conductivity (µS/cm)		1,904	1,612	1,669	1,469	1,958	1,678	
COD (mg/L)		383.3	15.6	380	13.0			
CaH (mg/L as CaCO ₃ )			345		312		322	
ALK		352	128	336	158	334	176	
Biological								
CBOD₅ (mg/L)	< 2	164	0.57	161	0.08	156	0.54	
TSS (mg/L)	< 1	130	0.28	122	0.20	107	0.24	
T-Phosphorus (mg/L as P)		9.55	3.34	5.23	3.15		1.97	
NH₃-N (mg/L as N)	< 0.5	23.17	0.56	23.16	0.24	23.18	0.91	
TKN (mg/L as N)		47	2.94	37	2.20	38	8.50	
NO ₂ /NO ₃ -N (mg/L as N)		0.38	15.47	0.03	6.51	0.04	1.46	
Total Nitrogen (mg/L as N)		47	18	37	9	38	10	
Microbial								
Total Coliforms (CFU/100mL)	< 2.2		15.1		17.3		82.2	
Fecal Coliforms (CFU/100 mL)	0		8.9		8.8		26.1	
HPC (CFU/mL)	< 500		1,383		2,891		3,237	

^aWhere target left blank, no target was established.

Table 5.10 presents the results of water quality analyses of the ZenoGem feed and permeate during Stage D. The system operated in an alternative operating mode with a reduced MLSS concentration (6 g/L) and peak flow and/or cycled aeration to one or both tanks.

**TABLE 5.10**Results of Stage D (Alternative Operating Mode) Water Quality Analyses for the ZenoGem System

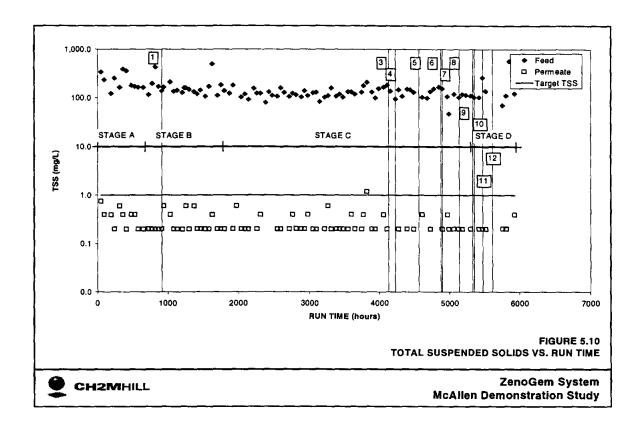
		Normal Flow with Cycled Aeration to Membrane Tank (Event 9)		Peak Flow with Cycled Aeration to Membrane Tank Only		with A to M	mal Flow n Cycled eration lembrane nk Only	Normal Flow with Cycled Aeration to Membrane and Aeration Tanks		
Parameter				(E\	vent 10)	(E	vent 11)	(Event 12)		
Physical/Chemical	Permeate Target ^a	Feed	Permeate	Feed	Permeate	Feed	Permeate	Feed	Permeate	
pH				7.06	7.13			7.13	7.33	
Temperature (degrees C)		29.3	29.8	29.4	30.3	29.1	31.0	28.1	26.6	
Turbidity (NTU)	< 0.2		0.12		0.10		0.13		0.14	
Conductivity (µS/cm)		1,796	1,533	1,695	1,487	1,595	1,448	1,575	1,338	
COD (mg/L)				448	15.0			292	14.0	
CaH (mg/L as CaCO ₃ )					280		300		316	
ALK				360	110	320	124	380	180	
Biological										
CBOD ₅ (mg/L)	< 2	146	0.03	157	0.15	154	0.17	154	0.37	
TSS (mg/L)	< 1	104		184	0.20	140	0.20	220	0.27	
T-Phosphorus (mg/L as P)		6.07	3.19	5.45	1.44	3.87	2.73	4.94	1.44	
NH ₃ -N (mg/L as N)	< 0.5	21.30	0.05	24.85	0.15	17.20	0.14	24.28	0.31	
TKN (mg/L as N)		42	2.0	43	2.0	39	2.0	47	2.85	
$NO_2/NO_3$ -N (mg/L as N)		0.01	18.30	0.02	13.5	0.01	20.10	0.01	3.96	
Total Nitrogen (mg/L as N)		42	20	43	16	39	22	47	7 .	
Microbial										
Total Coliforms (CFU/100mL)	< 2.2	·			8.5		9.0		6.4	
Fecal Coliforms (CFU/100 mL)	0				2.0					
HPC (CFU/mL)	< 500				2,102		1,600		2,458	

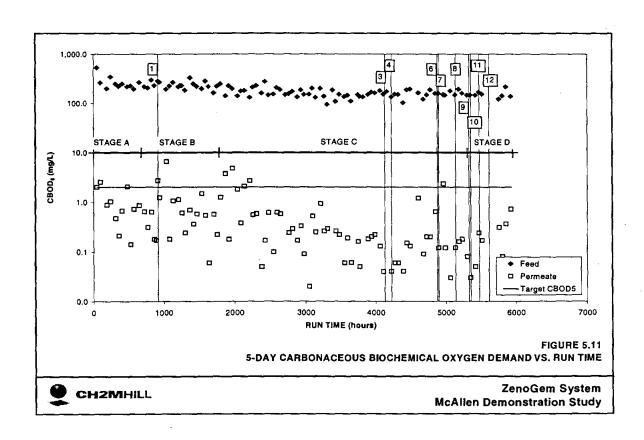
^aWhere target left blank, no target was established.

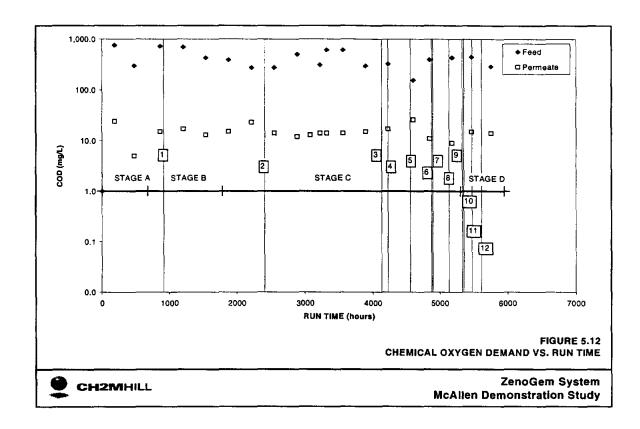
**Particle Removal.** The ZenoGem system achieved greater than 99 percent removal of TSS and CBOD during all stages of operation and was effective in reducing TSS and CBOD $_{\rm s}$  in the wastewater to below target levels as shown in Figures 5.10 and 5.11. TSS measurement is not sufficiently sensitive to detect potential differences in TSS removal as a function of MLSS concentration. Figure 5.12 illustrates that COD was consistently reduced to less than 20 mg/L in the ZenoGem permeate. COD removal efficiency was not impacted by MLSS concentration.

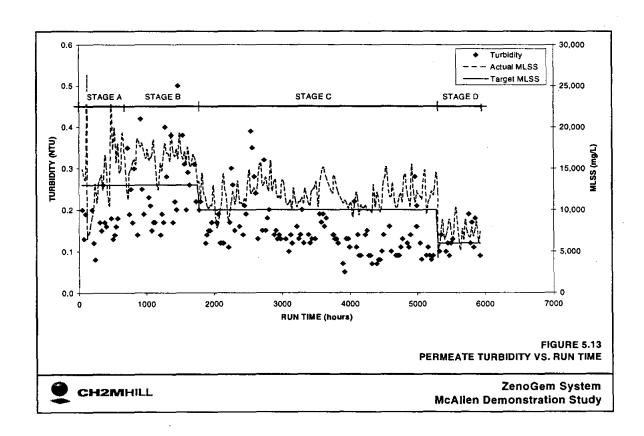
As shown in Figure 5.13 and Table 5.8, the average permeate turbidity was slightly higher in Stage B as compared to Stage A and to the target level of 0.2 NTU established for feedwater to the downstream RO system. This suggests greater particle passage through the OKC MF versus the OCP UF membrane at the higher MLSS concentration. Permeate turbidities were higher during Stage B than Stage C (see Table 5.9), suggesting that particle passage through the OKC membrane is greater at high solids loading (high MLSS concentration).

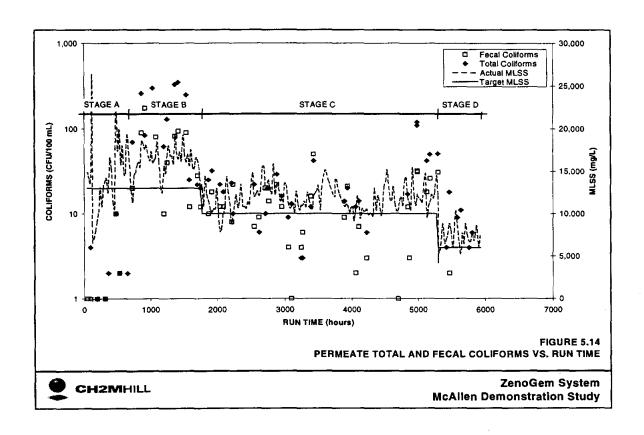
**Microbial Removal.** Trends observed for turbidity removal were also seen with microbial removal. As shown in Figure 5.14, the average total and fecal coliform levels were higher in Stage B as compared to Stage A. This suggests greater bacteria passage through the MF versus the UF membrane at equal MLSS loadings. The increase coliform levels observed in Stage B compared to Stage C suggest bacteria passage through the MF membrane is a function of MLSS concentration. The high HPC levels may reflect bacterial regrowth in the ZenoGem permeate piping in the absence of a continuous disinfectant. In general, total and fecal coliform levels exceeded the informally adopted goal of State of California "Title 22" regulations pertaining to unrestricted access (2.2 CFU/100 mL for total coliforms and 0 CFU/100 mL, respectively).











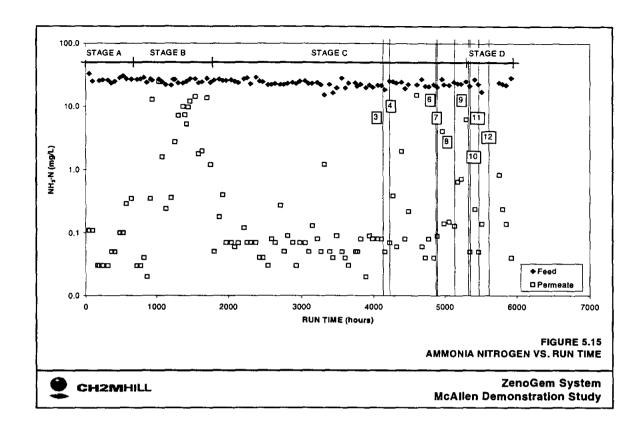
#### Nutrient Removal.

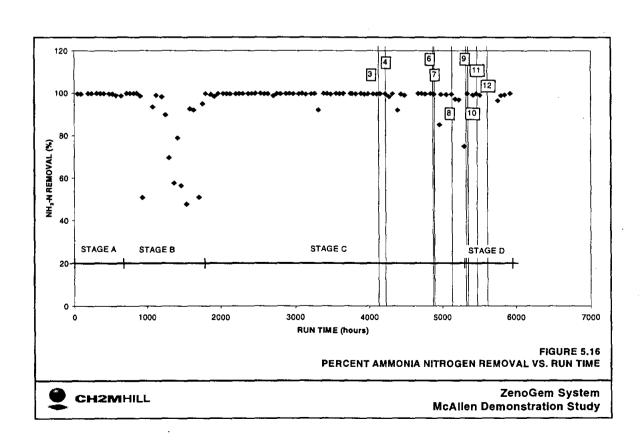
Nitrogen Transformation. At the long SRTs used in this study and the high wastewater temperatures, the activated sludge portion of the ZenoGem process should be able to achieve complete nitrification, i.e., the conversion of ammonia-nitrogen to nitrate-nitrogen. A potential constraint is the ability to supply sufficient oxygen to the process, given the relatively short HRT and the high volumetric organic loading rate. Assuming sufficient DO levels and a well mixed biomass, denitrification should be minimized. These were the expectations at the start of the study.

Ammonia Removal. Ammonia nitrogen feed and permeate levels and percent removal by ZenoGem as a function of operating time are shown in Figures 5.15 and 5.16. Feed levels were relatively constant, ranging from 15 to 30 mg/L. Permeate concentrations were less than the target of 0.5 mg/L at normal flow conditions, except during Stage B. Removals were essentially complete during all stages, except Stage B. Reduced removals (partial/incomplete nitrification) during Stage B most likely reflect impaired efficiency of oxygen transfer to the nitrifiers within the dense flocs present at the higher MLSS concentration (~13 g/L) and high wastewater temperatures. Although dissolved oxygen levels in the bulk liquid were within acceptable range to achieve nitrification (under conventional wastewater MLSS levels), transfer of this oxygen from bulk liquid to bacteria contained within the flocs was not sufficient to achieve complete nitrification at the provided HRT. The reduced nitrification efficiency at higher MLSS levels suggests that MBR operation at such levels may be constrained by oxygen transfer efficiency unless such a constraint can be overcome by increase air input or better gas-to-liquid transfer efficiency than attained in this study.

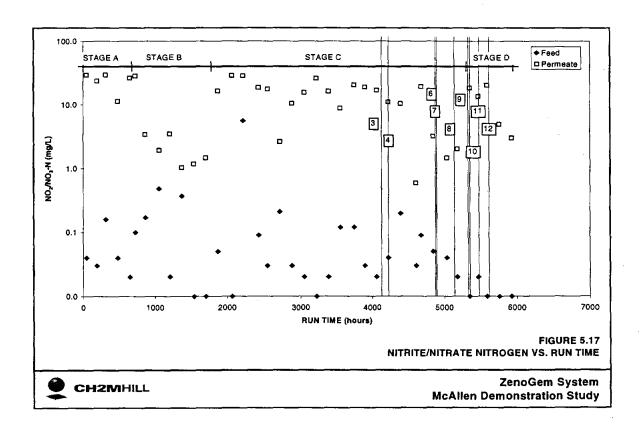
When comparing normal flow versus flow peaking in Stages B and C, nitrification (ammonia removal) was incomplete during peaking due to the decrease in HRT from 5.7 hrs to 3.9 hrs. Cycled aeration to the membrane tank had no real effect on nitrification efficiency in Stage C. Ammonia removal was reduced from 98 to 97 percent only. This result is not surprising as most of the oxygen for biological oxidation is provided in the aeration tank. During Stage D, flow peaking with cycled aeration to both tanks during showed no significant decrease in nitrification when compared to normal flow and full aeration operation.

During all stages, the rate of nitrification was calculated at 0.48 mg/L NH₃-N per mg/L MLVSS per day regardless of MLSS concentration or permeate flowrate. However, during cycled aeration to both tanks in Stage D, the nitrification rate increased to 0.72 mg/L NH₃-N per mg/L MLVSS per day.





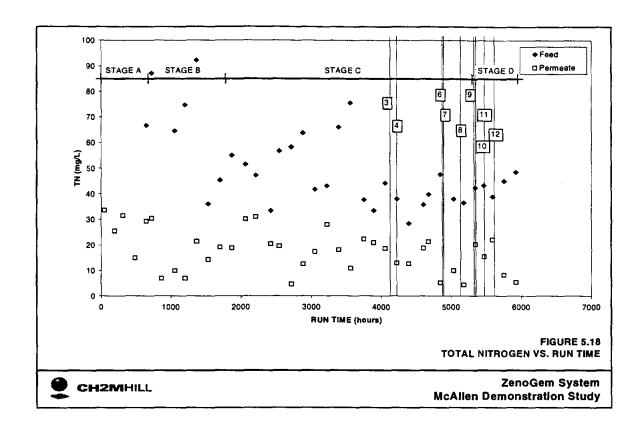
Nitrite/Nitrate Removal. Feed and permeate nitrite/nitrate nitrogen levels for the ZenoGem system as a function of operating time is shown in Figure 5.17. Feed levels were < 0.4 mg/L in all cases, as anticipated. Permeate levels ranged from 15 to 19 mg/L in Stages A and C. During Stage B and the end of Stage D, permeate levels were significantly less. Permeate levels are a function of the amount of ammonia and organic nitrogen converted to nitrite/nitrate (nitrification) and the extent to which this "converted" nitrogen is reduced to nitrogen gas by denitrifiers. In an aerated system, denitrification (nitrite/nitrate conversion to nitrogen gas) is not anticipated as the bacteria responsible for this reduction operate under anoxic conditions. During Stages A and C, denitrification was minimal yielding higher permeate nitrite/nitrate levels. However during Stage B and the end of Stage D, a significant fraction of the nitrite/nitrate generated from nitrification was converted to nitrogen gas, resulting in a condition of "simultaneous nitrification/denitrification" thus yielding lower permeate nitrite/nitrate levels. This result is consistent with the hypothesis offered under the Ammonia Removal discussion where reduced oxygen transfer creates micro anoxic zones within the mixed liquor, providing conditions conducive to the growth of denitrifiers. At the end of Stage D, conditions to produce this effect were put into place through cycled aeration in both treatment tanks. Such conditions were very effective for achieving a high level of both nitrification and denitrification, as illustrated by the data in Table 5.10 (Event 12) where permeate ammonia and nitrite/nitrate nitrogen concentrations were 0.31 and 3.96 mg/L, respectively.

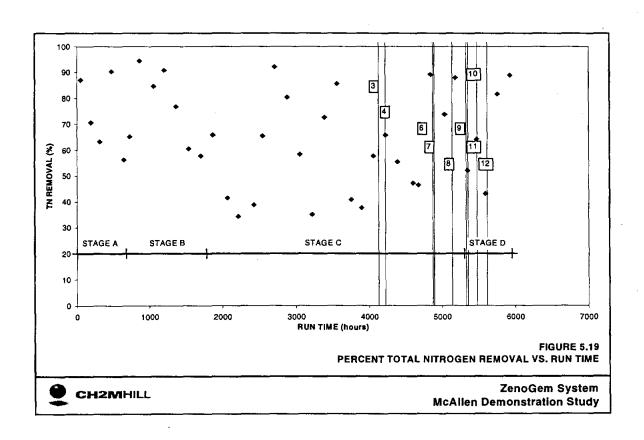


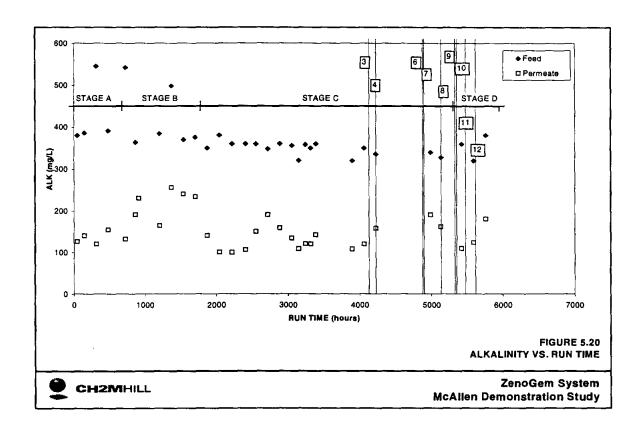
Total Nitrogen Removal. Feed and permeate total nitrogen (TN) levels and percent removal by the ZenoGem system as a function of operating time are shown in Figures 5.18 and 5.19. Feed TN levels were exceptionally high during Stages A and B, decreasing to the 38 to 47 mg/L range during the remainder of testing. As shown in Tables 5.8 through 5.10, highest permeate TN levels were observed at normal flow rates and at low to medium MLSS levels. Cycled aeration to the membrane tank had only minor impact on TN levels. TN removal was higher in Stage B as compared to Stage C due to nearly complete denitrification, in spite of the fact that partial nitrification (higher permeate ammonia and lower permeate nitrite/nitrate levels) was observed. TN removal decreased as a result of complete nitrification (lower permeate ammonia and higher permeate nitrite/nitrate levels) and reduced denitrification when the MLSS concentration was decreased in Stage C. The greatest degree of TN removal was observed at the end of Stage D (Event 12) during cycled aeration to both tanks. As previously discussed, such aeration is effective at maximizing simultaneous nitrification/denitrification. With a 15-minute on/off aeration cycle, the ZenoGem system was capable of reducing TN levels to 7 mg/L.

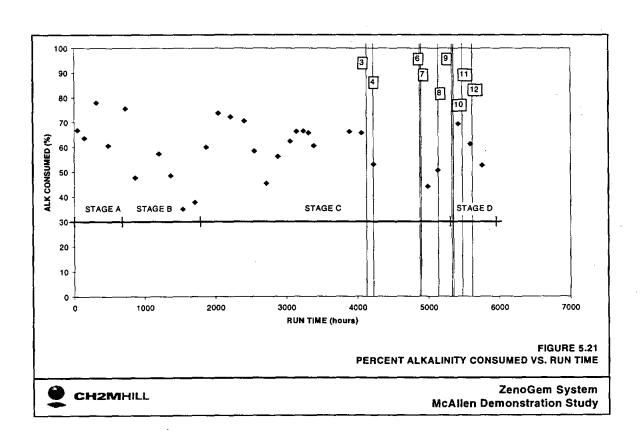
Alkalinity Consumption. During nitrification, alkalinity is consumed. During denitrification alkalinity is created. Assessing alkalinity reductions during the various stages of operation provides a means of "proofing" observed ammonia removals as well as providing a semi-quantitative measure of biological oxidation of non-ammonia organic nitrogen compounds. . Theoretically, 7.1 parts of alkalinity are consumed for each part of ammonia oxidized. As shown in Figure 5.20 during Stage B, alkalinity levels were reduced from an average of 422 mg/L as CaCO₃ in the feed to 203 mg/L as CaCO₃ in the permeate, yielding an alkalinity consumption of 219 mg/L as CaCO₃. In Stage C, levels were reduced from an average of 352 mg/L as CaCO₃ in the feed to 128 mg/L as CaCO₃ in the permeate, yielding an alkalinity consumption of 224 mg/L as CaCO₃. Based on an average ammonia nitrogen removal of 20 mg/L in Stage B and 23 mg/L in Stage C, 142 mg/L and 163 mg/L of alkalinity (as CaCO₃) should have been consumed in Stages B and C, respectively. The additional alkalinity consumption (77 mg/L as CaCO₃ in Stage B and 61 mg/L in Stage C) would have resulted from the biological oxidation of (non-ammonia) nitrogen compounds present in the wastewater. Ammonia nitrogen accounted for only 34 percent of the 75 mg/L of organic nitrogen (TKN) in Stage B and only 49 percent of the 47 mg/L of TKN in Stage C. These levels of TKN are unusually high for a domestic wastewater and indicate that nitrogen-rich discharges are present in the McAllen wastewater.

From previous discussions, nitrification was reduced and denitrification was significant during Stage B. Alkalinity changes between ZenoGem feed and permeate should reflect these differences; alkalinity removals during Stage B should be less than during Stage C as less alkalinity is consumed (from nitrification) and more is created (from denitrification). As shown in Figure 5.21, average alkalinity removal was 50 percent for Stage B and 64 percent for Stage C. Another way of comparing alkalinity consumption and nitrogen transformation is to correlate alkalinity consumption with total nitrogen removal. Lesser alkalinity consumption should occur with greater nitrogen removal as the ratio of nitrogen transformed from nitrate to nitrogen gas increases relative to the amount of organic nitrogen oxidized to nitrite/nitrate. Total nitrogen removal was 76 percent for Stage B and 58 percent for Stage C.

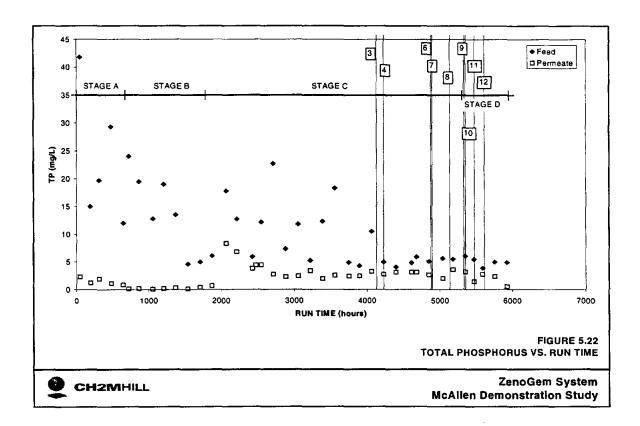


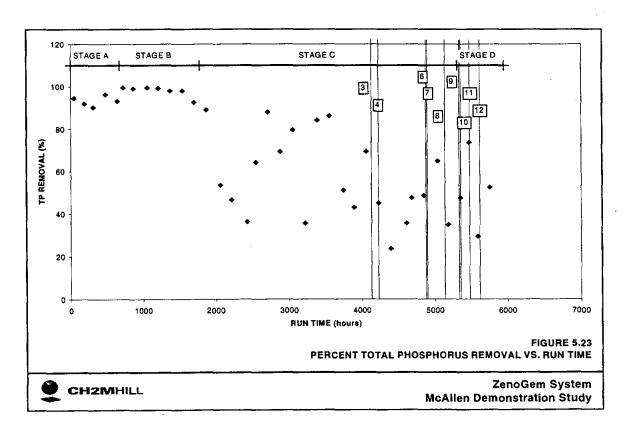






Phosphorus Reduction. Feed and permeate total phosphorus (TP) levels and percent removal by the ZenoGem system as a function of operating time are shown in Figures 5.22 and 5.23. Phosphorus reduction by the ZenoGem process was significantly greater in Stage B than in Stage C at 98 percent and 58 percent, respectively. At the higher MLSS concentration, oxygen transfer to certain zones of the aeration tank was most likely poor, resulting in anaerobic conditions within segments of the biomass producing favorable conditions for biological phosphorus uptake. When the MLSS level was reduced at the beginning of Stage C, these anaerobic zones were eliminated (or greatly reduced) and the phosphorus bound in these organisms was subsequently released, causing phosphorus removal to temporarily increase as shown in Figure 5.23. During the latter part of Stage C, the phosphorus levels in the permeate were in the 2 to 5 mg/L range, which is typical for the conventional wastewater treatment process using secondary treatment and nitrification. Phosphorus removal variability in Figure 5.23 reflects variability in the measured phosphorus levels in the ZenoGem feedwater. Also during Stage C, the phosphorus reduction decreased from 58 percent at normal flow/flux to 40 percent during flow peaking due to the decrease in HRT (insufficient time for phosphorus removal).





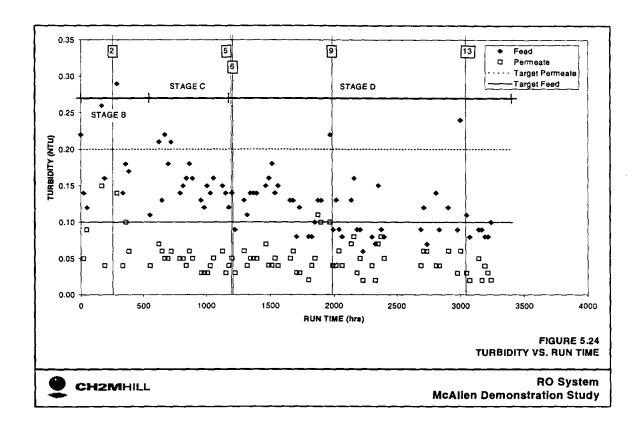
# 5.3 RO Testing Results

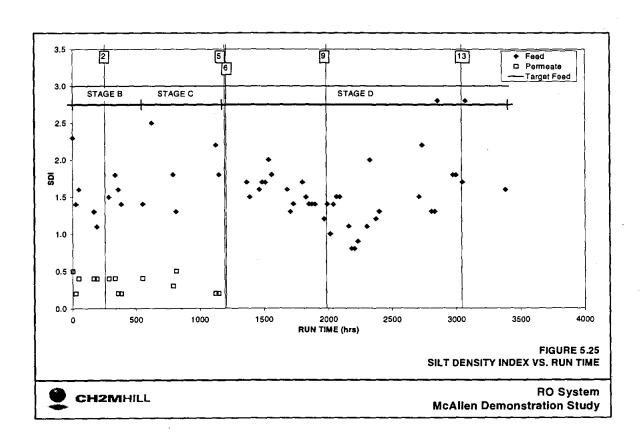
### 5.3.1 RO Feedwater Quality

Particulate Fouling Potential. Table 5.11 presents the average values for the RO feedwater quality parameters that reflect particulate and colloidal fouling potential (turbidity, SDI and heterotrophic bacteria). For all stages of testing, turbidity and SDI values were less than corresponding target levels, reflecting the low particle water produced by the ZeeWeed membrane. (Turbidity and SDI targets are those established by the spiral wound RO industry based on minimizing RO element fouling and cleaning. With a few exceptions, RO feedwater turbidity averaged less than the 0.2 NTU target (Figure 5.24). As shown in Figure 5.25, the ZenoGem system consistently produced a permeate with a SDI less than the target value of 3. The target of 500 CFU/mL for HPCs is an informal goal that is related to the acceptable level of HPCs in drinking water. There is not established correlation between HPC level in RO feedwater and degree of biological fouling, however, the greater the level the greater the potential to establish biofilms. Actual propensity to form biofilms depends on a number of interrelated factors, including organism type, level of nutrients, water chemistry, membrane material and flow hydraulics through the element. HPC levels were consistently above the target, however, as discussed in a later section of the report, there was no evidence of biological fouling. Taken together, the data in Table 5.11 indicate that the permeate from the ZenoGem permeate should cause little if any particulate fouling of downstream RO membranes.

**TABLE 5.11**Average RO Feedwater Quality Parameters

Parameter	Target	Stage B	Stage C	Stage D
Turbidity (NTU)	< 0.2	0.18	0.16	0.11
SDI	< 3	1.46	1.83	1.53
HPC (CFU/mL)	< 500	3,274	865	1,444





Mineral Precipitation Potential. Section 3 discussed the need for chemical conditioning of the RO feedwater to prevent the precipitation of calcium carbonate and barium sulfate, based on their levels in the WWTP secondary effluent and the degree to which their coions would be concentrated during RO treatment at target recovery. The mineral saturation calculations provided in the RODesign program (and also by the scale inhibitor suppliers contacted at the beginning of the project) estimate percent saturation for only the following sparingly soluble salts: calcium carbonate, calcium fluoride, barium sulfate, calcium sulfate, strontium sulfate and silica. Consequently, other sparingly soluble salts present in the effluent, including calcium phosphate salts, were not identified as being supersaturated as a result of RO treatment of the ZenoGem permeate. As discussed in Section 5.3.2 of this report, precipitation of calcium phosphate salts occurred during testing and required additional feedwater acidification to control. Analysis of spent cleaning solutions and materials removed from the membrane surface from element autopsies, showed that calcium carbonate and barium sulfate scaling was effectively controlled and that calcium phosphate was the major mineral precipitate.

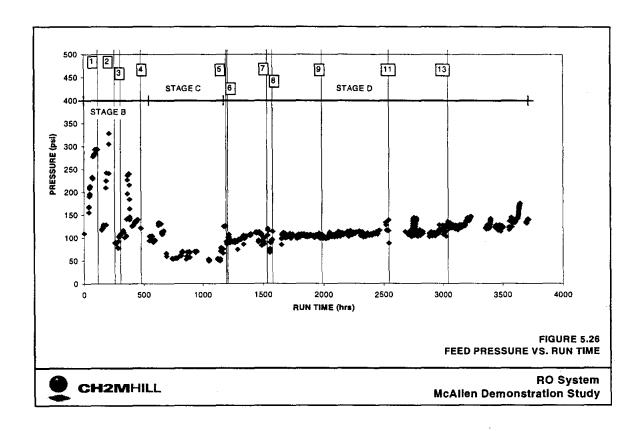
### 5.3.2 RO Operating Conditions/Membrane Performance

**Operating Conditions.** Table 5.12 presents the average RO system operating conditions for the following parameters: (recovery, flux, flow, pressure, and conductivity). With the exception of periods during Stage B, the RO system operated at or near target flowrates. Average feed pressure and permeate conductivity was significantly greater during Stage B operation at high recovery because of the increase resistance to flow caused by scaling in the second stage elements during this period. Feed pressure variations as a function of operating time is shown in Figure 5.26. This plot clearly illustrates the high feed pressure periods associated with scaling of the second stage membrane elements during Stage B. These effects were reversed by citric acid cleanings (Events 1, 3 and 4).

TABLE 5.12
Average Operating Conditions for the RO System

	Chamas In	Target	Actual	Flores		Flow (gpm)			Pressure (psi)			Conductivity (µS/cm)		
Stage	Stages in Operation	(%)	(%)	Flux gfd	Feed	Conc	Permeate	Feed	Interstage	Conc	Feed	Interstage	Conc	Permeate
В	1&2	80	70.4	10.37	3.98	0.94	2.85	231	220	213	1,608	4,408	3,729	182
8*	182	50	59.0	10.63	5.04	2.29	2.92	132	111	91	1,701	3,544	4,024	150
С	1	50	47.9	9.83	4.11	2.31	2.01	80	NA	65	1,636	3,167	3,330	71
D	1&2	50	48.9	7.71	5.45	2.67	2.95	125	100	63	1,798	2,958	3,520	104
D	1&2	62	63.8	10.03	4.33	2.76	1.45	90	76	63	1,814	3,510	5,017	148
D	1&2	70	68.1	10.50	4.24	2.89	1,41	101	86	74	1,741	3,408	4,998	118
D	182	74	72.6	10.62	4.02	2.92	1.12	110	97	87	1,549	3,187	4,970	95
D	1&2	80	79.3	11.89	4.12	3.27	0.86	128	115	107	1,731	3,841	7,210	105

^aTarget feedwater recovery decreased from 80 to 50 percent after 256 hours of operation (Event 2). NA=Not Applicable



Performance Parameters. Table 5.13 presents RO system target and average actual membrane performance parameters (NPF, salt passage and salt rejection) as a function of operating time. Figure 5.27 illustrates changes in flux as a function of operating time. Membrane flux varied considerably during Stage B, decreasing in proportion to the decline in system productivity. Although testing called for operation at constant flux, the rapid and severe increases in feed pressure make it difficult for the plant operators to provide such control. The step decrease in flux during Stage C was intentional and reflects an attempt to reduce RO fouling potential. Flux was steady during Stage D as mineral precipitation and feed pressure was more effectively controlled.

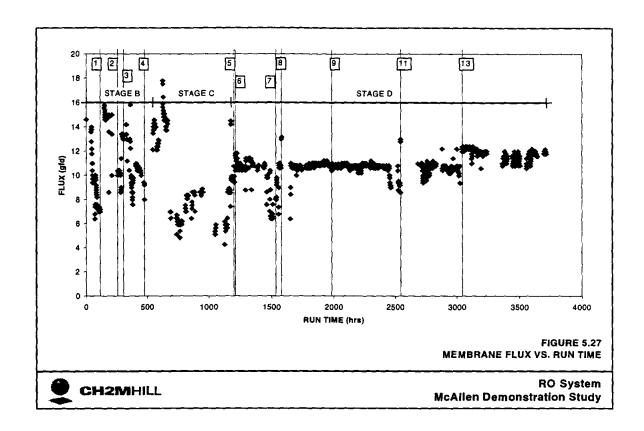
TABLE 5.13
Average Membrane Performance Parameters for the RO System

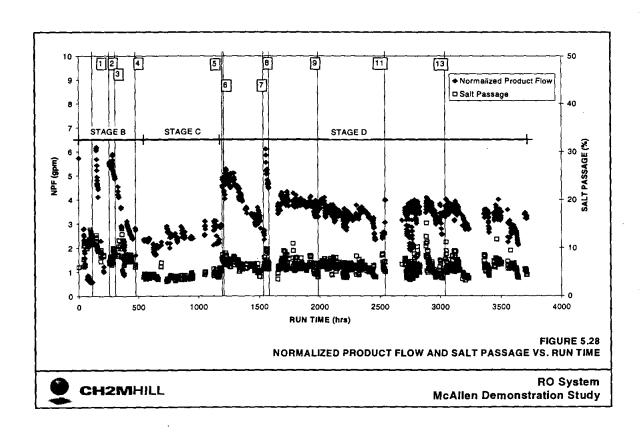
Stage	Stages in Operation	Target Recovery (%)	Normalized Product Flow (gpm)	Salt Rejection (%)	Salt Passage (%)
В	1&2	80	1.88	89.26	10.74
$B^{a}$	1&2	50	3.47	91.65	8.30
С	1	50	2.38	95.90	4.10
D	1&2	50	2.92	94.57	5.43
D	1&2	62	4.71	92.27	7.73
D	1&2	70	4.02	93.63	6.37
D	1&2	74	3.36	94.18	5.82
D	1&2	80	3.39	94.24	5.76

^aTarget feedwater recovery decreased from 80 to 50 percent after 256 hours of operation (Event 2).

Similarly, NPF showed severe and rapid declines during Stage B. As shown in Figure 5.28, these declines were readily reversible by citric acid cleanings, however operation at high recovery and feed pH (6.8) was not sustainable on a long-term basis. At lower recovery (Stage C), NPF was quite stable confirming that performance declines were recovery and scaling related. With return to two-stage operation and recovery of 70-75 percent (Stage D), NPF again declined but a lesser rate, reflecting the partial effectiveness of reduced pH (6.0-6.5) operation. However, stable performance could not be achieved until feedwater pH was reduced to 5.0, corresponding to a concentrate pH of 5.6. As recovery was further increased to 80, inability to effectively control concentrate pH at 5.6 again resulted in rapid NPF decline.

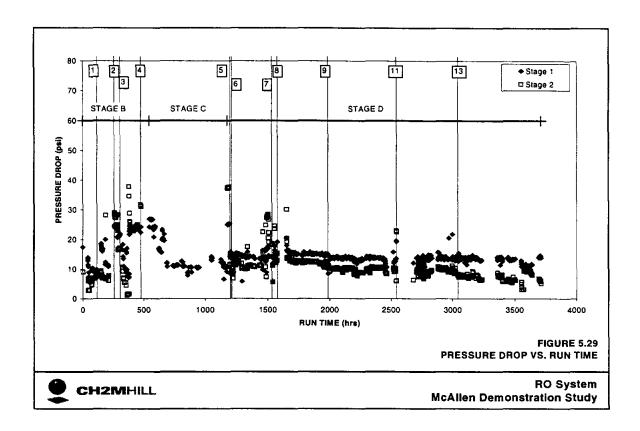
Normalized salt passage was less impacted by scaling than NPF, with the exception of Stage B operation when scaling was worst (Figure 5.28). Normalized salt passage was comparable at the very beginning of Stage B (6 percent at 4 hours) and at the end of routine testing (5 percent at 3,400 hours). This indicates no loss in salt rejecting capability by the RO membranes over the course of this testing despite repeated membrane scaling and citric acid cleaning.

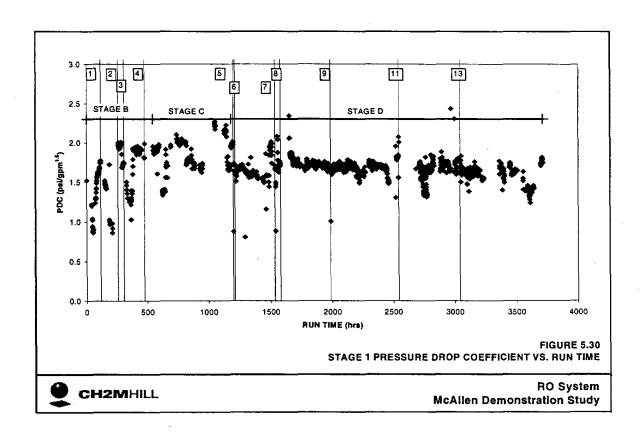




Figures 5.29 and 5.30 present vessel differential pressure (pressure drop) for each RO system stage during the testing as well as pressure drop coefficient for Stage 1 only as a function of operating time. In RO systems operating on MF-treated wastewater effluent or MBR permeate, pressure drop is monitored primarily to indicate the occurrence biological fouling, which causes a characteristic rise in Stage 1 pressure drop. Pressure drop reflects the resistance of water flow through the RO element feed spacer. As material accumulates within the spacer or on the membrane surface, pressure drop increases. Pressure drop coefficient accounts for changes in flow through the pressure and allows for a better comparison of systems operating at different recoveries. In general, the data in the figures indicate the absence of biological fouling. Stage 1 PDC was relatively unchanged, except during the beginning of Stage B. During the period considered most representative of a properly operated RO system (Stage D, 1,500 to 3,000 hours), both pressure drop and PDC were extremely stable. The very gradual decline in pressure drop during Stage C was associated with the decrease in recovery (lower feedwater flow through the feed channels).

¹Pressure drop coefficient (PDC) is defined as follows: PDC = pressure drop /(feed flowrate)^{1,5}





Calcium Phosphate Scaling and Its Impacts on RO System Feed Pressure and Productivity. During Stage B, NPF declined rapidly (see Figure 5.28). Cleanings with citric acid were effective in restoring performance losses (Event 1) but with subsequent operation, NPF again rapidly declined. At this time, mineral precipitation was considered the likely cause for loss of RO performance. Biofouling was unlikely based on stable pressure drop readings. A second citric acid cleaning was then conducted (Event 2) and a portion of the second stage spent cleaning solution was analyzed to better determine the nature of the mineral precipitant. Calcium, aluminum and phosphorus were present in elevated concentrations relative to the other metals. Calcium and aluminum phosphate salts were considered the primary scaling concern, as calcium carbonate precipitation was controlled by feedwater acidification. Appendix E presents results of the cleaning solution analysis.

To determine the exact type of scale, the ZenoGem permeate, which becomes RO feedwater after chloramination, was analyzed twice a week during the period June 9 through June 23, 1999 for ions that can form precipitable salts, including phosphorus and sulfate, and metals, including barium, aluminum, and iron. (Calcium hardness, alkalinity and phosphorus levels in the ZenoGem permeate were routinely analyzed as part of ZenoGem peformance monitoring protocol.) The analysis showed less than detectable levels of the oxidizable metals aluminum and iron (<0.1 mg/L). Barium and sulfate were present at concentrations less than their solubility (as barium sulfate salt) for operation at 80 recovery (0.06 mg/L and 226 mg/L, respectively). Phosphorus levels were significant relative to natural water supplies (14 mg/L). Given the high concentration of calcium hardness in the wastewater (356 mg/L), calcium phosphate scaling was indirectly suspected. Appendix F presents results of ZenoGem permeate ion analyses.

To further confirm that scaling and not fouling caused performance losses, the second stage was removed from service after 546 hours of operation and the first stage was operated at 50 percent recovery (Stage C). At the lower percent recovery and operating only the first stage vessels, the feed pressure and NPF decreased and remained relatively low and constant during Stage C. Performance stabilized at the lower recovery confirming that performance declines were a result of ion concentration and mineral precipitation. Calcium phosphate scaling is not commonly encountered in municipal RO operations because phosphate levels in most natural raw water supplies are not elevated. Furthermore, based on discussions between CH2M HILL and several scale inhibitor manufacturers (i.e., FMC, KLT, Permacare), calcium phosphate precipitation is not effectively prevented by commercially available RO scale inhibitors. Consequently, three scaling mitigation methods were considered to control the precipitation tendency in lieu of a specific inhibitor:

1. **Decrease RO feedwater pH.** The calcium phosphate solubility index was used to calculate the pH of the RO concentrate at which calcium phosphate concentration in the RO concentrate would be less than solubility (SI = pH-pH_c, where SI is <0). By trial and error iteration, the resulting pH was used to calculate corresponding feed

² The calcium phosphate solubility index (SI) is defined as follows: SI =  $pH - pH_c$ , where  $pH_c = 11.755 - (log calcium ions + log of phosphate ions = 2*log temperature)/0.65 (Green and Holmes, 1947).$ 

pH using Hydranautics RODesign and the design conditions discussed in Section 3.3.1. Although this approach would require significant acid dose (~100 mg/L), it has the added benefit of increasing the solubility of both aluminum phosphate and calcium carbonate. This approach was considered the easiest to implement for this study.

- 2. Chemically precipitate excess phosphorus from the screened, degritted wastewater during ZenoGem treatment. Addition of an aluminum or iron salt to the wastewater would produce highly insoluble aluminum or ferric phosphates easily filterable by the ZeeWeed MF membrane. It was calculated that a dose of 45 mg/L of ferric chloride would be required to reduce the phosphate concentration in the ZenoGem permeate to 0.5 mg/L. a level that would reduce the calcium phosphate solubility index to < 0 at 80 percent recovery. This level of coagulant addition would generate more sludge, increase MLSS concentrations, require a reduction in SRT to maintain the 10 g/L target MLSS concentration and potentially increase the fouling rate of the ZeeWeed membrane.
- 3. Biologically remove phosphorus by creating an anaerobic zone in the membrane bioreactor. This was done in an uncontrolled manner during ZenoGem Stage B operation but would require extensive testing to develop the necessary operating strategy relative to oxygen input. Such testing was beyond the scope of this project.

The second stage was returned to service after 1,177 hours of operation (Stage D) and the system continued to operate at 50 percent recovery. After 1,533 hours of operation and step-wise increase in recovery to 70 percent, a target pH of 5.6 was established for the RO concentrate (corresponding to feed pH of 5.0) to maintain calcium phosphate solubility (Scaling Mitigation Method 1). However, difficulties with both the acid feed pump and PLC pH control loop caused difficulty in consistently maintaining the pH during the remainder of testing. After 1,579 hours of operation, the fourth acid cleaning was performed. Feed pressure and NPF was reduced by the cleaning and remained relatively constant until feedwater was increased to 75 percent after 1,985 hours of operation. Thereafter, feed pressure increased and NPF decreased until another cleaning was performed at 2,544 hours of operation to restore performance. Increasing the recovery to 80 percent after 3,042 hours of operation resulted in a rapid increase in feed pressure and decrease in NPF. These results indicate that the decrease in RO feedwater pH effectively stabilized system performance and reduced fouling potential when operating at a feedwater recovery up to 70 percent. Stable system performance could not be maintained at the higher recoveries (75 to 80 percent), even with the decrease in RO feedwater pH.

Autopsy of the trailing element(s) from Stage 2 confirmed calcium phosphate as the primary precipitate (see Appendix G).

### 5.3.3 RO Water Quality Impacts

Control of Major Contaminant Categories. Table 5.14 presents the results of water quality analyses of the RO system feed, permeate, and concentrate during each stage of operation. These data are presented to illustrate the ability of RO treatment to reduce the concentration of particulate, microbial, inorganic and organic contaminants in the ZenoGem permeate (i.e., wastewater effluent). Per the objectives of the study, the following surrogate parameters were monitored through the study to demonstrate such removal capability: turbidity (representing particles), coliforms and HPCs (representing pathogenic bacteria), conductivity and TDS (representing inorganic) and TOC (representing organic).

TABLE 5.14

Average Water Quality Results for the RO System

Parameter			Stage B			Stage C			Stage D	
Physical/Chemical	Permeate Target	Feed	Permeate	Conc	Feed	Permeate	Conc	Feed	Permeate	Conc
pH		7.13	6.00	7.32	7.30	6.07	7.44	6.22	5.66	6.06
Conductivity (uS/cm)		1,651	86	3,420	1,560	63	3,718	1,668	110	5,367
Turbidity (NTU)	< 0.1	0.18	0.08	0.54	0.16	0.05	0.32	0.11	0.05	0.36
SDI		1.46	0.33		1.83	0.32		1.53		1.57
TOC (mg/L)	< 1	6.18	< 0.5		6.77	< 0.5		6.62	< 0.5	
TDS (mg/L)	< 500	999	51	2,341	943	44	1,702	899	73	3,503
Microbial										
Total Coliform (CFU/100 mL)		2.0	7.0		5.7	2.9		6.0	1.0	
Fecal Coliform (CFU/100 mL)	0				2.0	2.0		3.0	2.0	
HPC (CFU/mL)		3,274	110		865	65		1,444	276	

^aWhere target left blank, no target was established.

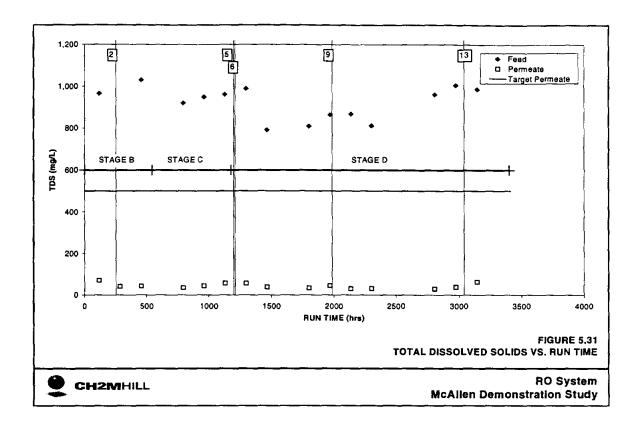
**Particulate.** As described in earlier in this section, turbidity levels in the RO feedwater were well controlled by ZeeWeed membrane (average of 0.15 NTU). Consequently, only minor improvements in turbidity were possible by the RO system. RO permeate turbidity was consistently measured at to 0.05 NTU. This compares with the target level of 0.1 NTU and the current Environmental Protection Agency (EPA) regulatory level of 0.3 NTU for conventional water treatment plants (95 percent of readings).

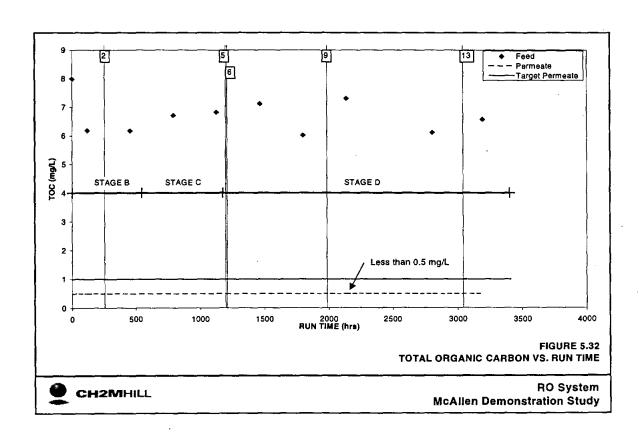
**Microbial**. The target level of coliforms was established at 0 CFU/mL. Coliforms were routinely measured in the RO permeate, typically at levels of 2 CFU/mL based on similar levels in the feed. This is surprising given the presence of a low level of monochloramines in the RO feed and permeate. HPCs were reduced by more than an order of magnitude by RO treatment, with permeate levels less than the drinking water trigger level of 500 CFU/100mL.

**Inorganic**. At the target 80 percent recovery (beginning of Stage B and end of Stage D), RO treatment produced an effluent (permeate) having an average TDS of 66 mg/L (in the absence of mineral scaling effects), significantly below both federal and State of Texas secondary drinking water standard for TDS (500 and 1,000 mg/L, respectively). The average RO permeate TDS compares very favorably with the 700 to 800 mg/L TDS level that is typical for the City's existing raw water supply (Lozier, 1998). As shown in Figure 5.31, permeate TDS was consistently < 75 mg/L (greater than 92 percent removal) throughout the study, despite periods of severe membrane scaling.

**Organic.** As shown in Figure 5.32, TOC levels in the RO permeate grab samples were consistently less than detectable (0.5 mg/L) based on a feedwater TOC range of 6 to 8 mg/L. This represents greater than 92 to 94 percent TOC removals. By comparison, TOC levels in the City's existing raw water supply average 3.8 mg/L (Lozier, 1998) and the California Dept. of Health Services TOC limit for direct injection of reclaimed water is 1 mg/L.

In association with RO membrane integrity studies conducted by the BOR and coincident with these research, permeate TOC levels were measured on-line using two low detection limit (20 ppb) analyzers provided by Sievers and Anatel on a short-term trial basis. Other sites using the Sievers instrument have shown RO systems treating microfiltered secondary effluent contain less than  $100 \, \mu g/L$  TOC.





# 5.4 Impacts of IPR on Waste Discharges

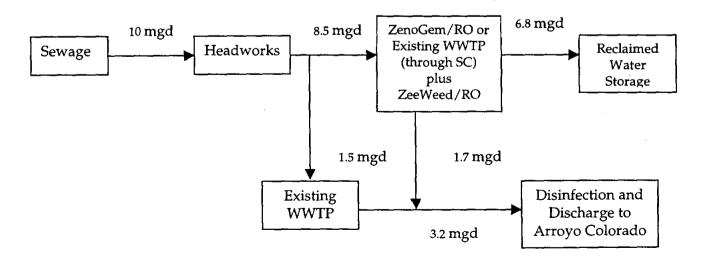
One of the objectives of this testing was to characterize the quality of the ZenoGem permeate and RO concentrate for water quality parameters important to the ecosystems of the Arroyo Colorado and Laguna Madre. The former is a non-perennial waterway to which the City currently discharges the effluent from the South WWTP. Flows into the Arroyo Colorado eventually empty into the Laguna Madre, an estuary that is connected to the Gulf of Mexico. Currently, the City's discharge is regulated with respect to three parameters: CBOD₅, TSS, and ammonia nitrogen. The limits for discharge are as follows:

CBOD₅: 10 mg/L
 TSS: 15 mg/L
 NH₃-N: 3 mg/L

As part of a reuse feasibility study previously conducted for the City, TNRCC expressed concern regarding the presence and concentration of nutrient and TDS in the waste stream(s) from a future IPR treatment system, as it would pertain to discharges to these water bodies. The IPR treatment system evaluated in this research would generate one waste stream, the RO concentrate. Sludge from the ZenoGem system would be dewatered and dried using existing WWTP facilities. For the purpose of this evaluation, it is assumed that 8.5 mgd of wastewater from the WWTP would be diverted to ZenoGem/RO treatment system or, alternatively, 8.5 mgd of WWTP effluent (from the secondary clarifiers) would be diverted for ZeeWeed/RO treatment system. With either alternative, 1.5 mgd (average flow) of undiverted secondary effluent would be disinfected and discharged to the Arroyo Colorado as is currently done. As shown in Exhibit 5.3, these assumed treatment scenarios would result in the following discharges:

- 1.5 mgd of effluent from the South WWTP
- 1.7 mgd of RO concentrate (20% of 8.5 mgd RO feedwater flow)

**EXHIBIT 5.3** Wastewater Discharge Characterization



In both alternatives, the 8.5 mgd of secondary effluent would be processed by RO to produce 6.8 mgd of final efffluent and 1.7 mgd of RO concentrate (waste). This waste concentrate would then be blended with the remaining 1.5 mgd of WWTP effluent (flow which bypasses IPR treatment), disinfected, and discharged to the current location. As shown in Table 5.15, concentrations of TDS, nutrients and TOC were then calculated for the 47:53 blend of WWTP effluent/RO concentrate using the data collected in Appendix D.

TABLE 5.15
Comparative Loading of Critical Contaminants to Arroyo Colorado/Laguna Madre

	(A)	(B)		
Parameter	RO Concentrate (mg/L) ^a	WWTP Effluent (mg/L) ^a	Composite Stream (Blend) Loading (Ibs/day) ^b	Existing WWTP Effluent Discharge Loading (lbs/day)
NO ₂ /NO ₃ -N	29.9	3.45	467	288
T-Phosphorus	10.20	2.38	174	199
TKN	3.16	2	70	167
TDS	3,780	930	65,227	77,562
тос	28.15	7.25	490	605

^aBased on average results of two sampling events.

Calculated as: 8.34*10*B where 10=existing average WWTP effluent flow (mgd).

The comparison shows that for each parameter, the concentration is much higher in the RO concentrate than the WWTP effluent. This reflects the concentration of each parameter by RO treatment and in the case of nitrate, a higher level in the ZenoGem permeate than the WWTP effluent. In some cases, agencies regulate contaminant discharges based on mass loading (pounds of contaminant per day) rather than concentration. Table 5.15 also shows the predicted mass loading for the RO concentrate/WWTP effluent composite stream (blend) verses the current WWTP effluent discharge. In contrast to the concentration comparison, mass loadings for the blend are higher only for nitrate. Consequently, it would be in the City's best interest to work toward establishing mass loading-based discharge regulations versus the current concentration-based regulations if they wish to discharge RO concentrate to the Arroyo Colorado/Laguna Madre ecosystem. If successful, the City could incorporate biological denitrification into the design of the ZenoGem system to control nitrate loadings at the current levels.

^bCalculated as: 8.34*(1.7*A + 1.5*B) where 1.7=RO concentrate flow (mgd) and 1.5=WWTP effluent flow (mgd).

# 5.5 Comparing Reclaimed and Existing Raw Water Quality

No federal regulations exist regarding the quality requirements for reclaimed water to be used in the context of indirect potable reuse. Currently, such requirements are established on a state-by-state basis. To date, the City has had preliminary meetings with TNRCC regarding such requirements. However TNRCC has not yet proposed regulations for McAllen, but have only referenced potential treatment techniques (e.g., treat all the reclaimed water with RO). To provide a basis for development of IPR regulations for this project, all primary and secondary contaminants currently regulated under the SDWA were analyzed in both the ZenoGem and RO permeates. Results of these analyses are presented in Appendix D. The results were then compared with data from similar characterization of the City's existing raw water supply (Rio Grande River) as sampled in 1997 during the Wastewater Reclamation Pilot Study, City of McAllen, Texas (1998).

Comparing the quality of the ZenoGem permeate to the City's existing raw water supply and to federal and state drinking water regulations as shown in Table 5.16, the following conclusions are drawn:

- The ZenoGem permeate contains greater levels (i.e., lower quality) of most inorganic contaminants than the City's raw water supply. The degradation reflects: 1) the inability of the City's water treatment plant and the ZenoGem process to remove such compounds, and 2) increases in these contaminants from the domestic water use/wastewater generation process. Consequently, the ZenoGem permeate, on at least one sampling event, exceeded the maximum contaminant level (MCLs) for chloride, color (APHA) apparent, and TDS.
- The ZenoGem permeate contains lower concentrations of certain metals (i.e., iron, manganese, aluminum, barium, and strontium) than the City's raw water supply and the MCLs as a result of their removal by oxidation or precipitation in both the WWTP and the ZenoGem processes.
- The concentration of dissolved organic matter (as measured by TOC) is significantly greater in the ZenoGem permeate than the City's raw water supply. Although there is not a current MCL for TOC, the greater the TOC level, the greater the potential for formation of trihalomethanes (THMs) and haloacetic acids (HAAs). These chlorinated byproducts have been shown to be carcinogenic and are regulated at very low levels (µg/L levels). This greater potential is illustrated by the significantly higher levels of HAAs in the ZenoGem permeate relative to the raw water supply. Further, the chronic health risks associated with identified organic compounds in wastewater are not well understood. For this reason, respected authorities in the field of IPR recommend that TOC levels be reduced. In the State of California, a TOC guideline of 1 mg/L has been established for reclaimed water used for surface water supplementation IPR projects.

Particle levels in the ZenoGem permeate are significantly lower than the City's raw
water supply based on turbidity measurements. This reflects the very small pore
size of the MF and UF membranes used with ZenoGem, which serves as a effective
barrier to the passage of most particles.

Comparing the quality of the RO permeate to the City's existing raw water supply and to federal and state drinking water regulations as shown in Table 5.16, the following conclusions are drawn:

- The RO permeate meets all established drinking water regulations as well as the TOC guideline of 1 mg/L.
- To produce reclaimed water meeting state and federal drinking water regulations and the State of California TOC guideline, both ZenoGem and RO treatment of the City's wastewater is required. Assuming an RO permeate TOC of 0.5 mg/L, greater than 90 percent of the wastewater would require RO treatment. If the TOC guideline were not considered, RO treatment would still be required, however, the percent of treatment would be reduced depending on the controlling contaminant (e.g., HAAs, nitrate or TDS). Assuming nitrate would be more cost effectively removed through biological denitrification, approximately 80 percent of the wastewater would require RO treatment to control HAA formation.
- Beyond simply meeting the drinking water regulations, experts involved in setting IPR policy strongly recommend the concept of multiple treatment barriers to ensure that the proposed treatment scheme adequately protect public health, particularly with respect to acute health risk from microbes. In this regard, the combination of ZenoGem and RO treatment provides two robust barriers to the passage of viral, bacterial and protozoan pathogens as opposed to relying on only a single barrier (i.e., ZenoGem only). An additional barrier or chlorine/UV disinfection may also be desirable while only marginally increasing costs.
- If TNRCC were to approach IPR guidelines for this project from the viewpoint that the reclaimed water must equal or exceed the quality of the existing raw water supply, a lower percentage of the ZenoGem permeate would require RO treatment. Based on the data shown in Table 5.16, it is estimated that about 50 percent of the wastewater would require RO treatment to have a reclaimed water match the TOC concentration of the raw water.

TABLE 5.16
Results of ZenoGern and RO Permeate Sampling for IPR Characterization

	Primary	Existing I	Raw Water	Zeno	Gem		
	MCL	_	plya	Perm		RO Per	meate
Parameter		3/11/97	6/2/97	8/17/99	9/14/99	8/17/99	9/14/99
General Chemistry						<del></del>	
Alkalinity (mg/L as CaCO ₃ )		130	106	121	153	14	16
Bromide (mg/L)		0.100	0.54	0.132	0.32	0.02 ^b	0.02 ^b
Chloride (mg/L)	250	155	207	160	281	9.73	15.20
Color Apparent	15	17	10	22	17	5 ^b	5 ^b
Fluoride (mg/L)		0.59	0.99	1.07	1.14	0.32	0.45
NH ₃ -N (mg/L as N)					0.1 ^b		0.1 ^b
NO ₂ -N (mg/L as N)				9.55	7.90	1.11	1.08
TKN (mg/L as N)				2 ^b	2 ^b	2 ^b	2 ^b
Reactive Silica (mg/L)		6.0	13.5	15.1	16.1	0.65	0.90
Sulfate (mg/L)	250	247	262	150	247	4	5.31
TDS (mg/L)	500 - 1,000	720	772	774	1,950	33	72
TOC (mg/L)	1 ^g	3.70	3.90	7.48	5.90	0.63	0.52
T-Phos (mg/L)		0.05	0.05 ^b	2.48	2.89	0.10	0.1 ^b
UV-254 (cm ⁻¹ )		0.112	0.092	0.129	0.126		
Metals							
Aluminum (mg/L)	0.05 - 0.2	1.22	0.248	0.111	1 ^b	0.046 ^b	0.1 ^b
Arsenic (mg/L)				0.004*	0.01 ^b	0.004 ^b	0.01 ^b
Barium (mg/L)		0.127	0.124	0.056	0.062	0.0008b	0.025*
Cadmium (mg/L)				.003	0.005 ^b	0.0004 ^b	0.005 ^b
Calcium (mg/L)		77	77.7	72.1	86.9	0.714	833
Chromium (mg/L)				0.007 ^b	0.010 ^b	0.008 ^b	0.01 ^b
Iron (mg/L)	0.3°	0.77	0.171	0.032	0.1 ^b	0.01	0.1
Lead (mg/L)				0.028	0.003 ^b	0.002 ^b	0.003 ^b
Magnesium (mg/L)		22.1	27.9	20.4	25.6	0.197	0.5 ^b
Manganese (mg/L)	0.05°	0.025	0.018	0.015	0.017	0.001 ^b	0.01 ^b
Mercury (mg/L)				0.0003 ^b	0.0003 ^b	0.0003 ^b	0.0003 ^b
Potassium (mg/L)		9	9.58	17.8	29.9	1.36	2*
Selenium (mg/L)				0.007 ^b	0.007 ^b	0.007	0.007 ^b
Silver (mg/L)				0.008 ^b	0.010 ^b	0.008 ^b	0.01 ^b
Sodium (mg/L)		102	140	157	253	13	16.2
Strontium (mg/L)		2.05	2.40	1.87	2	0.029 ^b	0.1 ^b
Zinc (mg/L)				0.463	0.054	0.007	0.02 ^b
Purgeable Volatiles							_
Vinyl Chloride				1 ^b	1 ^b	1 ^b	1 ^b
tran-1,2-Dichloroethene				1 ^b	1 ^b	1 ^b	1 ^b
cis-1,2-Dichloroethene				1 ^b	1 ^b	1 ^b	1 ^b
1,1,1-Trichloroethane				1 ^b	1 ^b	1 ^b	1 ^b
Carbon Tetrachloride				1 ^b	1 ^b	1 ^b	1 ^b
Trichloroethene				1 ^b	1 ^b	1 ^b	1 ^b

**TABLE 5.16**Results of ZenoGem and RO Permeate Sampling for IPR Characterization

	Primary MCL	Existing Raw Water Supply ^a		ZenoGem Permeate		RO Permeate	
Parameter		3/11/97	6/2/97	8/17/99	9/14/99	8/17/99	9/14/99
1,4-Dichlorobenzene				1 ^b	1 ^b	1 ^b	0.60
Disinfection Byproducts							
Trihalomethanes (SDS THMs)° (µg/L)	80	236.00	215.00	198.00	244.00	5.40	8.30
Haloacetic Acids (SDS HAA5) ^d (µg/L)	60	58.00	72.00	119.00	90.60	1.10	1.10
Semi-volatile Organics			·				
Lindane (µg/L)				0.024	0.011	0.02 ^b	0.02 ^b
Endrin (µg/L)				0.02 ^b	0.01	0.02 ^b	0.02 ^b
Methoxychlor (µg/L)				0.04 ^b	0.04 ^b	0.04 ^b	0.04 ^b
Toxaphene (µg/L)				0.5 ^b	0.5 ^b	0.5 ^b	0.5 ^b
Radiochemicals							
Radium-226 (pCi/L)				0.2 ^b	0.2 ^b	0.2 ^b	0.2 ^b
Radium-228 (pCi/L)				1 ^b	1 ^b	1 ^b	1 ^b
Gross Alpha (pCi/L)				1 ^b	1 ^b	<b>1</b> ^b	1 ^b
Chlorinated Herbicides							
2,4-D (μg/L)				ND	ND	ND	ND
Silvex (2,4,5-TP) (µg/L)				ND	ND	ND	ND

^aSource: Table 5.2 of Water Treatment Technology Program Report No. 26

ND =No Detection

pCi/L=picoCuries per liter

^bNot Detected at specified reporting limits.

[°]SDS THM - Simulated Distribution System Trihalomethanes (4 species)

^dSDS HAA5 - Simulated Distribution System Haloacetic Acids (5 species)

^eSecondary MCL

Secondary MCL: Federal = 500 mg/L; State = 1,000 mg/L

⁹Guildeline set by the State of California

#### **SECTION 6**

# Cost Estimates Using ZenoGem, ZeeWeed, and RO Facilities

This section presents the cost estimates for two advanced treatment systems to produce 6.8 mgd of reclaimed water that would supplement the City of McAllen's drinking water supply by providing a new source of raw water to the City's water treatment plant. The advanced treatment system would be located at the site of the City's south WWTP. The effluent from the advanced treatment system would be of a quality suitable for discharge to a new reclaimed water storage reservoir to be located in the vicinity of the City's existing water treatment plant. It is anticipated that the effluent from the advanced treatment system would receive additional disinfection depending on TNRCC requirements.

UV light disinfection or chlorination are two candidate disinfection methods. The most appropriate may depend on whether the effluent consists of 100 percent RO permeate or a blend of RO permeate and ZenoGem/ZeeWeed permeate¹. In the latter case, UV disinfection may be required because of the increased chlorine disinfection byproduct formation potential of the UF permeate. For the purposes of this exercise, costs for final disinfection have not been included because the method of disinfection has yet to be determined. Costs for disinfection of the UF permeate with chloramines (prior to RO treatment) have been included.

Estimates were developed for two alternatives:

- Treatment Alternative 1: ZenoGem MBR, UF permeate storage/disinfection and RO facilities treating screened, de-gritted wastewater
- Treatment Alternative 2: Extended aeration and clarification (existing), ZeeWeed system, UF permeate storage/disinfection and RO facilities treating secondary effluent from the existing south WWTP

For Alternative 1, a new ZenoGem MBR system would be installed to treat the screened, de-gritted wastewater and produce 8.5 mgd of reclaimed effluent. The UF permeate would be disinfected with monochloramines, stored, and then treated by the RO system (which includes acidification and antiscalant addition to the RO feedwater) to produce 6.8 mgd of RO permeate.

For Alternative 2, 9.4 mgd of effluent from the existing secondary clarifiers would be treated by the ZeeWeed UF system to produce 8.5 mgd of permeate. The UF permeate would then be disinfected, stored, and treated by RO as described for Alternative 1. For either alternative, wastewater flows in excess of those necessary to produce 6.8 mgd of RO permeate and would be processed by the existing WWTP facilities. Concentrate from the ZeeWeed UF system would be recycled back to the aeration basins, while sludge

¹ For purposes of the estimates, the ZenoGem/ZeeWeed permeate is referred to as UF permeate, as both processes use the same UF membranes.

from the ZenoGem system would be digested and dried using existing facilities at the WWTP. Both alternatives use existing headworks facilities for wastewater screening and de-gritting.

Figure 6.1 displays a schematic of the existing WWTP. Figures 6.2 and 6.3 are schematics of the two alternatives including existing facilities.

FIGURE 6.1 Existing WWTP Schematic

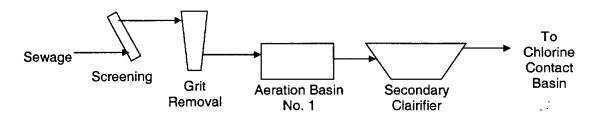


FIGURE 6.2
ZenoGem MBR and RO Facilities

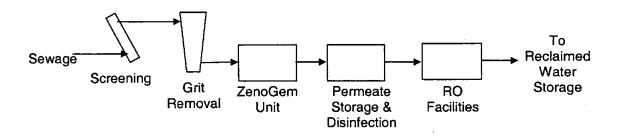
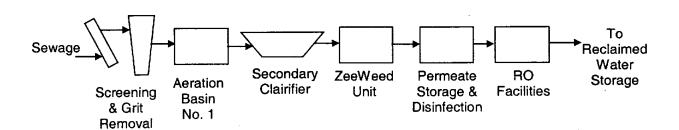


FIGURE 6.3
Conventional WWTP with ZeeWeed and RO Facilities



### **6.1 Cost Assumptions**

The estimates were prepared at an order-of-magnitude level to provide a relative and preliminary cost comparison between the two treatment alternatives and are based on information presently available. Order-of-magnitude cost estimates are defined by the American Association of Cost Engineers as an approximate estimate made without detailed engineering data. Final costs for each alternative will depend on such variables as actual labor and material costs, market conditions, project scope, implementation schedule, and will differ from the estimates presented. The costs are in present day dollars, and annual unit costs are based on ZenoGem/ZeeWeed permeate capacity of 8.5 mgd and RO permeate capacity of 6.8 mgd. The plant availability factor assumed for calculation of unit treatment costs (in \$/1000 gallons) is 95%. A higher availability factor is not required as the plant is intended to operate as a seasonally-average reuse production plant. ZENON budget proposals used in estimating ZenoGem/ZeeWeed and RO equipment costs are presented in Appendix H.

The estimates do not include costs for sewage screening and de-gritting (these facilities are currently being upgraded at the south WWTP) for either alternative. Alternative 2 does not include capital costs for extended aeration or secondary clarification, as these are existing. The costs related to ZenoGem, ZeeWeed, and RO equipment and required ancillaries are included. The ZenoGem system is sized to account for downtime associated with backpulsing and maintenance cleanings while the ZeeWeed system is sized to account for downtimes associated with backpulsing only. At the assumed RO feedwater recovery of 80 percent, 20 percent of the RO feedwater flow (1.7 mgd) becomes waste concentrate requiring appropriate disposal. For purposes of this estimate, RO concentrate is assumed to be discharged without further treatment to the Arroyo Colorado using the City's existing outfall. Consequently, costs are not included for concentrate disposal.

#### **6.2 Cost Estimates**

Estimates were prepared for the following cost categories:

- Installed equipment, total construction, total capital, total unit capital, and amortized capital
- Total O&M and total unit O&M
- Total annual and total unit annual

Tables 6.1 and 6.2 present the estimates for the Alternatives 1 and 2, respectively. The tables include the assumptions and references used in developing component capital costs and operating and maintenance costs. Table 6.3 presents design criteria assumptions used in developing the cost estimates for each major process. In addition, a line-item comparison of capital and O&M costs for the ZenoGem and ZeeWeed technologies is presented in Appendix I.

**TABLE 6.1**Order of Magnitude Cost Estimate for ZenoGem® and RO Alternative Capital and O&M Cost Opinion

Item		Cost	Assumption	Cost Reference
Fine Screening	\$	20,000	3-mm screen	CH2M HILL estimator b
ZenoGem® System®	\$	8,620,000		Zenon Budget Proposal
Bioreactor/Equalization Tanks	\$	1,307,808	6 tanks @ 170 ft x 21 ft x 23 ft (1.29 MG for equalization)	CH2M HILL estimator ^b
Permeate Storage	\$	70,000	180,000 gallons	CH2M HILL estimator b
Transfer Pump to RO System	\$	52,500	(2) 2,950 gpm @ 70 ft TDH pumps plus one stand-by	CH2M HILL estimator ^b
Chloramine Feed System				
Chlorinator	\$	30,000	50 lb/day duplex system	CH2M HILL estimator b
Ammoniator	\$	30,000	100 gai/day duplex system	CH2M HILL estimator b
RO System ^a	\$	2,300,000		Zenon Budget Proposal
nstallation	\$	2,730,000	25% of installed equipment costs	
installed Costs Subtotal	\$	15,160,308	, ,	
ZenoGem Equipment Building	\$	288,000	4,800 SF	CH2M HILL estimator b
RO Building	\$	390,000	6,500 SF	CH2M HILL estimator b
installed Costs and Building Cost Subtotal	\$	15,838,308		
Unit Process Noncomponent Costs				
Yard Piping Allowance (10%)	\$	1,583,831		
Site Electrical Allowance (8%)	\$	1,267,065		
Site I&C Allowance (5%)	\$	791,915		
Site Civil Allowance (5%)	\$	791,915		
Unit Process Subtotal	\$	20,273,034		
Contingency (10%)	\$	2,027,303	•	
Contractor Overhead & Mark-up (10%)	\$	2,027,303	i	
Total Construction Cost	\$	24,327,641		
Engineering & Administration (15%)	\$	3,649,146		
Total Capital Cost	\$	27,976,787	•	•
Total Capital Unit Cost (\$/1,000 gallon)	\$	11.87		
Amortized Capital Cost (20yr @ 6.5%)	<b>\$</b>	2,539,072		
Operation & Maintenance Costs				
Major Chemical Costs				
Disinfection: Chlorine			\$610/ton	Hill Brothers Chemical Co
Disinfection: Ammonia			\$370/ton	Hill Brothers Chemical Co
Backpulse Chemicals: Sodium Hypochlorite		\$ 8,232	2 \$0.31/Liter	Zenon Budget Proposal
CIP Chemical #1: MC-1		\$ 220	\$1.67/Liter	Zenon Budget Proposal
CIP Chemical #2: Sodium Hypochlorite (250 mg/L)		\$ 304	\$0.31/Liter	Zenon Budget Proposal
RO - Sulfuric Acid		\$ 5,745	\$0.04/lb	Zenon Budget Proposal
RO - Sodium Bisulfite		\$ 2,594	\$0.25/lb	Zenon Budget Proposal
RO - Antiscalant		\$ 122,359	9 \$3.27/Liter	Zenon Budget Proposal

**TABLE 6.1**Order of Magnitude Cost Estimate for ZenoGem® and RO Alternative Capital and O&M Cost Opinion

Item	С	ost	Assumption		Cost Reference
RO - Organic Acid: MC-1		\$ 8,658	\$2.29/kg	Zenon	Budget Proposal
RO - Alkali Surfactant: MC-4		\$ 1,738	\$3.06/kg	Zenon	Budget Proposal
RO - Sanitizer: MP-1		\$ 4,748	\$5.01/Liter	Zenon	Budget Proposal
Major Power Costs			\$0.075/kW-hr		
Screening	\$	•	Existing		
Permeate Pumps	\$	37,392		Zenon	Budget Proposal
Recirculation Pumps	\$	59,068		Zenon	Budget Proposal
Sludge Wasting Pumps		\$ 890		Zenon	Budget Proposal
Membrane Air Scour Blowers	\$	237,213		Zenon	Budget Proposal
Process Air Blowers	\$	119,501		Zenon	Budget Proposal
Anoxic Zone Mixers		\$ -		Zenon	Budget Proposal
Air Separation System Vacuum Pumps		\$ 2,520		Zenon	Budget Proposal
Backpulse Sodium Hypochlorite - Metering		\$ 3		Zenon	Budget Proposal
Chemical Feed #1 - Metering		\$ 245		Zenon	Budget Proposal
Air Compressors		\$ 2,515		Zenon	Budget Proposal
Air Driers		\$ -		Zenon	Budget Proposal
Controls & Instrumentation		\$ 657		Zenon	Budget Proposal
Miscellaneous		\$ 657		Zenon	Budget Proposal
RO - Pretreatment Chemical Mixers, Process Pump, CIP Pump	\$	501,591		Zenon	Budget Proposal
Membrane/Cartridge Filter Replacement Costs					•
ZenoGem	\$	329,311	1-yr warranty; 8-yr replacement frequency	Zenon	Budget Proposal
RO	\$	226,286	5-yr replacement frequency	Zenon	Budget Proposal
Cartridge Filter	\$	24,637	Annual replacement	Zenon	Budget Proposal
Other Costs					_
Maintenance	\$	63,750			ed South WWTP Costs
Permit Fees	\$	39,100			ed South WWTP Costs
Land Maintenance	\$	12,750	Replacement of sand in drying beds	Prorat	ed South WWTP Costs
Supplies	\$	61,200	Includes land application of sludge (\$31.50/dry ton)	Prorat	ed South WWTP Costs
Labor	\$	436,800	14 O&M personnel @ \$15.00/hr (9 ZenoGem; 5 for RO)	CH2M	HILL estimate
Laboratory	\$	141,100	Includes 4 lab techs, analysis, O&M, etc.	Prorat	ed South WWTP Costs
Total Annual Operation & Maintenance Cost	\$ 2	2,482,754			
Total Annual O&M Unit Cost	\$	1.05			

**TABLE 6.1**Order of Magnitude Cost Estimate for ZenoGem® and RO Alternative Capital and O&M Cost Opinion

ltem	Cost	Assumption	Cost Reference
Total Annual Cost	\$ 5,021,826		
Total Unit Cost (\$/1,000 gallon)	\$	ased on 6.8 MGD product water bw; plant availability factor = 95%	

^a Detailed listing of components comprising ZenoGem and RO systems are presented in Appendix H.

TABLE 6.2

Order of Magnitude Cost Estimate for ZeeWeed® and RO Alternative Capital and O&M Cost Opinion

Item	Cost	Assumption	Cost Reference
Fine Screening	\$ 20,000	3-mm screen	CH2M HILL estimator ^b
ZeeWeed® Tertiary Treatment System®	\$ 5,075,000		Zenon Budget Proposal
ZeeWeed Tanks	\$ 162,468	4 tanks @ 70 ft x 10 ft x 10 ft	CH2M HILL estimator ^b
Permeate Storage	\$ 70,000	180,000 gallons	CH2M HILL estimator b
Transfer Pump to RO System	\$ 52,500	(2) 2950 gpm @ 70 ft TDH pumps plus one stand-by	CH2M HILL estimator ^b
Chloramine Feed System			
Chlorinator	\$ 30,000	50 lb/day duplex system	CH2M HILL estimator ^b
Ammoniator	\$ 30,000	100 gal/day duplex system	CH2M HILL estimator b
RO System*	\$ 2,300,000		Zenon Budget Proposal
Installation	\$ 1,843,750	25% of installed equipment costs	
Installed Costs Subtotal	\$ 9,583,718		
ZeeWeed Equipment Building	\$ 84,000	1,400 SF	CH2M HILL estimator ^b
RO Building	\$ 390,000	6,500 SF	CH2M HILL estimator b
Installed Costs and Building Cost Subtotal	\$ 10,057,718		
Unit Process Noncomponent Costs			
Yard Piping Allowance (10%)	\$ 1,005,772		
Site Electrical Allowance (8%)	\$ 804,617		
Site I&C Allowance (5%)	\$ 502,886		
Site Civil Allowance (5%)	\$ 502,886		
Unit Process Subtotal	\$ 12,873,879		
Contingency (10%)	\$ 1,287,388		•
Contractor Overhead & Mark-up (10%)	\$ 1,287,388		
Total Construction Cost	\$ 15,448,655		
Engineering & Administration (15%)	\$ 2,317,298		
Total Capital Cost	\$ 17,765,953		
Total Capital Unit Cost (\$/1,000 gallon)	\$ 7.53		
Amortized Capital Cost (20yr @	\$ 1,612,374		

^b ENR CCI reference number 6126.79

TABLE 6.2

Order of Magnitude Cost Estimate for ZeeWeed® and RO Alternative Capital and O&M Cost Opinion

Item		Cost	Assumption	Cost Reference
6.5%)				
Operation & Maintenance Costs	_			
Major Chemical Costs				
Disinfection: Chlorine	\$	21,350	\$610/ton	Hill Brothers Chemical Co.
Disinfection: Ammonia	\$	9,620	\$370/ton	Hill Brothers Chemical Co.
Backpulse Chemicals: Sodium Hypochlorite	\$	8,232	\$0.31/Liter	Zenon Budget Proposal
CIP Chemical #1; MC-1	\$	3,211	\$1.67/Liter	Zenon Budget Proposal
CIP Chemical #2: Sodium Hypochlorite (250 mg/L)	\$	4,435	\$0.31/Liter	Zenon Budget Proposal
CIP Neutralization Chemical #1: Sodium Hydroxide	\$	175	\$0.36/Liter	Zenon Budget Proposal
CIP Neutralization Chemical #2: Sodium Bisulfite	\$	117	\$0.06/Liter	Zenon Budget Proposal
RO - Sulfuric Acid	\$	5,745	\$0.04/lb	Zenon Budget Proposal
RO - Sodium Bisulfite	\$	2,594	\$0.25/lb	Zenon Budget Proposal
RO - Antiscalant	\$	122,359	\$3.27/Liter	Zenon Budget Proposal
RO - Organic Acid: MC-1	\$	8,658	\$2.29/kg	Zenon Budget Proposal
RO - Alkali Surfactant: MC-4	\$	1,738	\$3.06/kg	Zenon Budget Proposal
RO - Sanitizer: MP-1	\$	4,748	\$5.01/Liter	Zenon Budget Proposal
Major Power Costs			\$0.075/kW-hr	
Screening	\$	•	Existing	
Aeration Basins	\$	419,000	18 motors @ 50 HP; 24 hrs/day	South WWTP info
Recirculation Pumps	\$	74,500	4 pumps @ 40 HP; 24 hrs/day	South WWTP info
Permeate Pumps	\$	36,901		Zenon Budget Proposal
Membrane Air Scour Blowers	\$	114,440	•	Zenon Budget Proposal
Air Separation System Vacuum Pumps	\$	2,520		Zenon Budget Proposal
Backpulse Sodium Hypochlorite – Metering	\$	7		Zenon Budget Proposal
Air Compressors	\$	2,515		Zenon Budget Proposal
Air Driers	\$	-		Zenon Budget Proposal
I&C	\$	657		Zenon Budget Proposal
Miscellaneous	\$	657		Zenon Budget Proposal
RO - Pretreatment Chemical Mixers, Process Pump, CIP Pump	\$	501,591		Zenon Budget Proposal
Membrane/Cartridge Filter Replacement Costs				,
ZeeWeed	\$	190,905	1-yr warranty; 8-yr replacement frequency	Zenon Budget Proposal
RO	\$	226,286	5-yr replacement frequency	Zenon Budget Proposal
Cartridge Filter	\$	24,637	annual replacement	Zenon Budget Proposal
Other Costs				
Maintenance	\$	63,750		Prorated South WWTP Cos
Permit Fees	\$	39,100		Prorated South WWTP Cos
Land Maintenance	\$	12,750	replacement of sand in drying beds	Prorated South WWTP Cos

TABLE 6.2

Order of Magnitude Cost Estimate for ZeeWeed® and RO Alternative Capital and O&M Cost Opinion

Item	Cost	Assumption	Cost Reference		
Supplies	\$ 61,200	includes land application of sludge (\$31.50/dry ton)	Prorated South WWTP Costs		
Labor	\$ 655,200	21 O&M personnel @ \$15.00/hr (16 exst. plant w/Zeeweed; 5 for RO)	CH2M HILL estimate		
Laboratory	\$ 141,100	includes 4 lab techs, analysis, O&M, etc.	Prorated South WWTP Cos		
Total Annual Operation & Maintenance Cost	\$ 2,760,698				
Total Annual O&M Unit Cost (\$/1,000 gallon)	\$ 1.17				
Total Annual Cost	\$ 4,373,072				
Total Unit Cost (\$/1,000 gallon)	\$ 1.85	Based on 6.8 MGD product water flow; plant availability factor = 95%			

^a Detailed listing of components comprising ZeeWeed and RO systems are presented in Appendix H.

**TABLE 6.3**Design Criteria Assumptions for ZenoGem, ZeeWeed, and RO Systems

Criterion	Value	
ZenoGem System		
Design Permeate Flow, mgd	8.5	
Hydraulic Residence Time, hours	6	
Solids Retention Time, days	. 17	
Mixed Liquor Suspended Solids Level, g/L	10	
Aeration Rate, fine bubble, scfm/mgd	647	
Aeration Rate, membrane air scour, scfm/mgd	2,586	
Aeration mode (both systems)	Cyclic	
Membrane flux, gfd	15.4	
No. of membrane trains	6	
No. of reactor tanks	6	
Backpulse interval, minutes	15	
Backpulse duration, seconds	30	
Backpulse pressure, psi	8	
Maintenance clean interval, hours	168	
Maintenance clean duration, minutes	60	
ZeeWeed System		
Design Permeate Flow, mgd	8.5	
Hydraulic Residence Time, hours	0.56	
Feedwater Recovery, percent	95	
Aeration Rate, membrane air scour, scfm/mgd	1,207	
Aeration Mode	Continuous	
Membrane flux, gfd	20.4	
Backpulse interval, minutes	15	
Backpulse duration, seconds	30	

^b ENR CCI reference number 6126.79

**TABLE 6.3**Design Criteria Assumptions for ZenoGem, ZeeWeed, and RO Systems

Criterion	Value				
Backpulse pressure, psi	8				
RO System					
Design Permeate Flow, mgd	6.8				
Feedwater pH, units	5				
Antiscalant dose, mg/L	Manufacturer dependent; 3 max				
Feedwater recovery, percent	80				
Membrane flux, gfd	12				
Membrane type	low fouling, aromatic composite				
Vessel array	three stage, concentrate taper				

Estimated total capital cost for the ZenoGem/RO approach (Alternative 1) is significantly higher than for the ZeeWeed/RO approach (Alternative 2), \$28.0MM versus \$17.8MM, a difference of nearly \$10MM. The difference reflects the higher cost of treatment for ZenoGem relative to ZeeWeed. Compared to the requirements for ZeeWeed, ZenoGem requires more membrane modules because a lower flux rate must be used to treat the significantly higher solids concentration of the mixed liquor (relative to the secondary effluent from the existing WWTP); larger tankage to provide wastewater flow equalization and the necessary hydraulic retention time to complete nitrification; and increased blower capacity to achieve carbonaceous and nitrogenous oxidation of the wastewater.

Estimated annual operating and maintenance costs for the ZenoGem-based alternative were slightly lower than for the ZeeWeed alternative (\$2.48MM/year versus \$2.76MM/year). This reflects lower energy and labor costs associated with operating the ZenoGem system versus those for operating costs for the extended aeration basins, secondary clarifiers and ZeeWeed system.

The significantly higher capital cost for Alternative 1 outweighs the slightly lower O&M costs. Consequently, total unit cost for Alternative 1 is higher (\$2.13/1000 gals versus \$1.85/1000 gals). Based on these estimates, it would be more cost-effective for McAllen to implement Alternative 2 (using ZeeWeed and RO to treat existing plant secondary effluent) to achieve their indirect potable reuse treatment goals. This reflects the cost savings of associated with the use of their existing flow equalization and secondary treatment facilities that are a sunk cost.

The disparity in capital cost between the ZenoGem and ZeeWeed alternatives could be reduced somewhat in the instance where a municipality's existing WWTP utilized concrete basins for aeration, rather than the earthen basins used at McAllen. Cost savings in this instance would result from avoiding the costs associated with constructing new concrete basins and instead retrofitting the membrane modules into the existing tankage. For the flow rate assumed in this cost comparison (8.5-mgd), the avoided cost would be \$1.3MM or 5.5% of the total capital cost for the ZenoGem alternative. Actual savings would be somewhat less due to the costs associated with basin retrofit. The \$1.3MM savings would reduce the difference in capital costs between the two alternatives, however, the ZeeWeed alternative would still be significantly less

expensive (by \$8.9MM). Additional capital cost savings could be realized if the blowers used for aeration in the conventional, concrete basin plant could be adapted and used where membrane modules are retrofitted into existing basins.

It was beyond the scope of this study to perform an order-of-magnitude level cost estimate for conventional treatment facilities (primary clarification, secondary [activated sludge] treatment and secondary clarification) followed by ZeeWeed in the case where no conventional wastewater treatment existed. However, based on design and costing of conventional treatment facilities that CH2M HILL has performed over the past 20 years, rule-of-thumb costs for 8.5-mgd of conventional treatment would be in the \$16MM -\$20MM range. Adding ZeeWeed costs of \$12MM results in a cost estimate of \$28-32MM. This compares with ZenoGem cost of \$22MM as estimated in this report. Based on these estimates, constructing a 8.5-mgd ZenoGem treatment plant to treat screened, de-gritted sewage would save \$6-10MM compared with the conventional treatment/ZeeWeed approach using the combination of rule-of-thumb and order-ofmagnitude cost estimates. This represents a significant savings potential and indicates that for municipalities considering indirect potable reuse and who would be starting with raw sewage, it should be considerably less expensive to construct a treatment facility using ZenoGem/RO versus conventional wastewater plant (through secondary treatment)/ZeeWeed/RO.

# References

- Green, J and J. Holmes. 1947. Journal American Water Works Association. Volume 39. p. 1090.
- Lozier, Jim. 1998. Water Treatment Technology Program Report No. 26. Wastewater Reclamation Pilot Study, City of McAllen, Texas.
- Water Environment Federation. 1990. Operation of Municipal Wastewater Treatment Plants. Manual of Practice 11, Volume II.
- Water Environment Federation and American Society of Civil Engineers. 1991. Design of Municipal Wastewater Treatment Plants, Volume I. WEF Manual of Practice No. 8. ASCE Manual and Report on Engineering Practice No. 76.

# **SI Metric Conversions**

English Unit	Multiply By	SI Metric Unit
ft²	0.0929	m²
gal	3.785	L
gai	0.003785	m³
gpm	0.06309	L/s
gpd/ft²	1.698	L/m²/hour
in	2.54	cm
lb	454	g
psi	0.0703	kg/cm²

**Appendix A. Photographs of Demonstration Plant Facilities and Associated Equipment** 

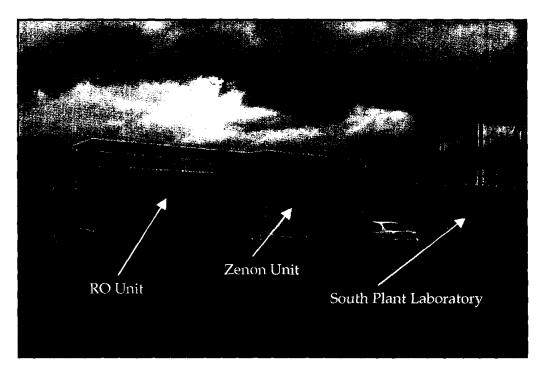


Exhibit A-1. Demonstration plant location (located to the west of the South WWTP laboratory).

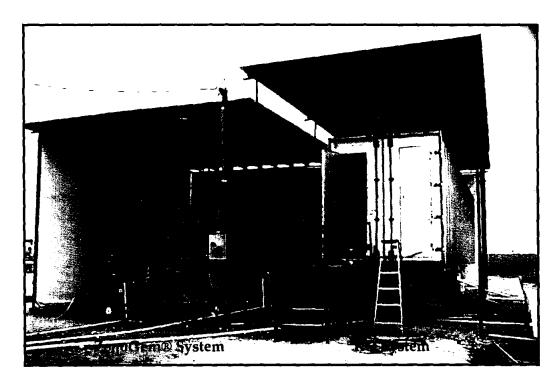


Exhibit A-2. ZenoGem® and RO treatment systems (looking west).

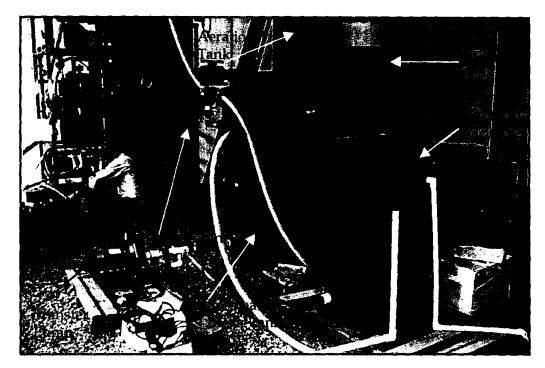


Exhibit A-3. Process tanks for ZenoGem system (operator Henry Perez in background).

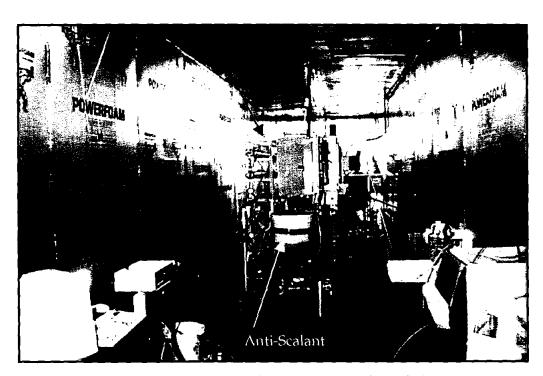


Exhibit A-4. RO system equipment (looking east inside trailer).



Exhibit A-5. RO data acquisition equipment (looking west inside trailer).

**Appendix B. RO Projections** 

HYDRANAUTICS RO SYSTEM DESIGN SOFTWARE, VERSION 6.4 (c) 1998 12/12/1999 BASIC DESIGN

RO program licensed to:

Stage Perm.

Flow

gpm

1545.2

7.8

TDS pН

Calculation created by: J. Lozier (CH2M HILL)

Project name: McAllen Phase II Permeate flow: 12.7 gpm 15.9 gpm HP Pump flow: Raw water flow: 15.9 gpm

80.0 8 (Stages !

Array

Recommended pump press.: 132.2 psi

121.4 psi 31.0 C(88F) Feed pressure: Permeate recovery ratio:

Flow per Vessel

Conc

gpm

1531.8

6.8

Feedwater Temperature:

Feed

gpm

Raw water pH: 7.80 Element age: 0.0 years Flux decline % per year: 56.9 H2SO4 Acid dosage, ppm (100%): 7.0

Acidified feed CO2: 57.9 Salt passage increase, %/yr: 10.0 12.0 gfd Average flux rate: Feed type: Wastewater

gfd

Flux Beta

Element

Type

7308.5

Elem.

No.

Conc.

psi

Press.

87.6

5.9

1-1 1-2 1-3 1-4	5.7 4.5 1.6 0.9	7.9 5.1 5.7 4.1	5.1 2.8 4.1 3.2	12.7 1. 8.8 1.	16 111.5 21 103.6 10 94.1 07 86.7	LFC1- LFC1- LFC1- LFC1-	4040 4040	6 2: 3 1:	x3 x3 x3 x3
+  Ion	+Raw   mg/l	water CaCO3	+Feed mg/l	water CaCO3	+Perme	caco3	+Conce	ntrate- CaCO	
Ca Mg Na K NH4 Ba Sr CO3 HCO3 SO4 C1 F NO3 Si02	140.0 29.1 332.0 17.1 1.0 0.1 1.3 0.3 293.0 327.0 388.0 1.0 1.5 13.9	349.1 119.8 721.7 21.9 2.8 0.1 1.4 0.5 240.2 340.6 547.2 2.6 1.2	140.0 29.1 332.0 17.1 1.0 0.1 1.3 0.1 224.0 382.8 388.0 1.5 1.5	349.1 119.8 721.7 21.9 2.8 0.1 1.4 0.1 183.6 398.7 547.2 2.6 1.2	2.3 0.5 25.2 1.6 0.1 0.0 0.0 25.5 6.3 25.0 0.1 0.5	5.7 1.9 54.8 2.1 0.3 0.0 0.0 20.9 6.6 35.3 0.4	690.9 143.6 1559.2 79.1 4.6 0.4 6.2 0.3 1017.8 1888.6 1839.8 4.5 5.7 67.7	1723.0 591.0 3389.5 101.4 12.8 0.3 7.1 0.6 834.3 1967.3 2594.9	0 0 0 5 4 8 8 3 1 6 6 3 3 3 9 3 8

	Raw water	Feed water	Concentrate
CaSO4 / Ksp * 100:	8%	10%	73%
SrSO4 / Ksp * 100:	5%	6%	42%
BaSO4 / Ksp * 100:	371%	428%	2994%
SiO2 saturation:	9%	9%	45%
Langelier Saturation Index	0.92	-0.19	1.73
Stiff & Davis Saturation Index	0.95	-0.17	1.35
Ionic strength	0.03	0.03	0.16
Osmotic pressure	13.3 psi	13.1 psi	62.8 psi

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYI	DRANA	UTICS	RO	SYSTE	M DES	IGN SC	FTWARE BASIC	. VERS	SION 6.4 SN	(c) 1	998	1	2/12/	1999
RO	prog	ram lic	cen	sed t	:0:									
		tion c				Lozie	r (CH2	M HILI	۵)					
		name:							ate flo	1747 *		1	2.7 g	nom.
		flow:					mqn		ater fl				.5.9 g	
		nded pu		nres	e · 1	32 2 5	ei .ei	210277	racer II	.ow.		1		Pitt
Fee	dne	essure:		בטוק	1	21.4 p	ei .ei	Darma	12to 705		:	0		
Foo	dunt.	er Temp		3 tura		21 A C	10051	rerme	ate rec	overy	ratio:	5	0.0 %	i
			JET.	acure	•	7.80	(001)	F1						
		er pH:	. <b></b>	/100	a. ) (	7.00	2504	Eleme	nt age:				0.0 Y	ears
		sage, p					2504		decline	* per	year:		7.0	
ACI	difie	ed feed	1 C	02:		57.9		Salt	passage	incre				
Ave	rage	flux r	at	e:	3	L2.0 gr	fd	Feed	type:	-	W	astewa	ter	
_	_	_		_		_								
Sta		Perm.			er Ves		Flux	Beta	Conc.		ement	Ele	m. A	rray
	F	Flow	1	Feed	Co	onc			Press.		Type	N-	ο.	
		gpm		gpm	gr		gfd		psi					
1-	1	5.7		7.9	5.		16.2	1.16	111.5	LFC	1-4040		6	2×3
1-3	2	4.5	5	5.1	. 2.	8	12.7	1.21	103.6	LFC	1-4040		6	2x3
1-3	3	1.6	5	5.7	4.	1	8.8	1.10	94.1		1-4040		3	1x3
1-4	4	0.9		1.1	3.	2	5.3	1.07	86.7	LFC:	1-4040			1x3
Sta	Elem	ı Fe	ed	Pres	Perm	Perm	Beta	Peri	n Conc	Concer	itrate	satura	ation	level
	no.			drop	-	Flux		sal				BaSO4		
				psi		qfd		TDS			<b>J-D0</b>	20201	D102	Daily.
		50	_	por	9p	9.4		100	2203					
1-1	1	121	Δ	4.0	1.0	17.0	1.13	28.4	1 15.0	12	7	504	10	0.0
1-1	2	117				16.1		31.2			8	602	12	0.2
1-1	3	114	-	2.6	0.9	15.2		34.7			10	733	14	0.4
T-T	3	TT-4	. 2	2.0	0.5	13.2	1.10	J4.	20.5	· 1/	10	133	14	0.4
1-2	1	108	5	2.1	0.8	13.7	1.17	39.3	24.3	21	12	903	17	0.6
1-2	2	106	-	1.6		12.7		44.8			16	1140	20	
1-2	3	104		1.2	0.7	11.5	1.21	51.5			20	1476		0.8
1-2	3	104	. 0	1.2	0.7	11.5	1.41	51.5	30.4	35	20	14/0	25	1.1
1-3	1	100.	6	2.6	0.6	9.8	1.10	55.9	40.7	40	23	1679	28	1.2
	2			2.0		8.6		61.1						
1-3		98.			0.5						26	1907	31	1.3
1-3	3	95.	. 9	1.9	0.5	7.8	1.10	66.6	49.9	52	30	2161	34	1.5
	4		^	1 7	0 4	~ 1	1 00	72 4	^			2410	2 -	
1-4	1	91.		1.7		6.1	1.08	73.4			33	2410	37	1.6
1-4	2	89.	_	1.5	0.3	5.0	1.08	81.0			37	2665	41	1.6
1-4	3	87.	. 8	1.3	0.3	4.5	1.07	88.6	63.9	71	41	2925	44	1.8

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYDRANAUTICS RO SYSTEM DESIGN SOFTWARE, VERSION 6.4 (c) 1998 12/12/1999 BASIC DESIGN

RO program licensed to:

1-2

3.1

Calculation created by: J. Lozier (CH2M HILL)

3.6

Project name: McAllen Phase II Permeate flow: 7.2 gpm HP Pump flow: Raw water flow: 14.4 gpm 14.4 gpm

Permeate recovery ratio:

73.2

LFC1-4040

50.0 %

2x3

Recommended pump press.: 100.5 psi

Feed pressure: 91.1 psi

31.0 C(88F) Feedwater Temperature:

5.2

7.80 Raw water pH: Element age: 0.0 years Acid dosage, ppm (100%): 56.9 H2SO4 Flux decline % per year: 7.0 57.9 Acidified feed CO2: Salt passage increase, %/yr: 10.0 10.2 gfd Average flux rate: Feed type: Wastewater

8.8

Stage Perm. Flow per Vessel Flux Beta Conc. Element Elem. Array Flow Feed Conc Press. Type No. psi gpm gpm gpm gfd LFC1-4040 4.1 7.2 5.2 11.5 1.11 81.9 1-1 6 2x3

1.12

+	+Raw	water	+Feed	water	+Perme	ate	+Conce	ntrate+
Ion	mg/l	CaCO3	mg/l	CaCO3	mg/1	CaCO3	mg/l	CaCO3
Ca	140.0	349.1	140.0	349.1	1.6	4.0	278.4	694.3
Mg	29.1	119.8	29.1	119.8	0.3	1.4	57. <del>9</del>	238.1
Na	332.0	721.7	332.0	721.7	18.0	39.1	646.0	1404.4
K	17.1	21.9	17.1	21.9	1.2	1.5	33.0	42.4
NH4	1.0	2.8	1.0	2.8	0.1	0.2	1.9	5.4
Ba	0.1	0.1	0.1	0.1	0.0	0.0	0.2	0.1
Sr	1.3	1.4	1.3	1.4	0.0	0.0	2.5	2.9
CO3	0.3	0.5	0.1	0.1	0.0	0.0	0.1	0.2
HCO3	293.0	240.2	224.0	183.6	18.3	15.0	429.6	352.2
SO4	327.0	340.6	382.8	398.7	4.4	4.6	761.1	792.8
C1	388.0	547.2	388.0	547.2	17.8	25.1	758.2	1069.4
F	1.0	2.6	1.0	2.6	0.1	0.2	1.9	5.0
NO3	1.5	1.2	1.5	1.2	0.3	0.3	2.7	2.1
SiO2	13.9		13.9		0.3		27.5	
TDS	1545.2	+	1531.8		62.4		3001.1	
pН	7.8		6.8		5.7		7.1	ĺ
++								+

Raw water	reed water	Concentrate
8%	10%	23%
5%	6%	13%
371%	428%	990%
9%	9%	18%
0.92	-0.19	0.65
0.95	-0.17	0.56
0.03	0.03	0.06
13.3 psi	13.1 psi	25.7 psi
	8% 5% 371% 9% 0.92 0.95 0.03	8% 10% 5% 6% 371% 428% 9% 9% 0.92 -0.19 0.95 -0.17 0.03 0.03

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

HYDRANAUTI	CS RO SYST	EM DESIGN S		E, VERSI DESIGN		(c) 1	998	1	2/12/	1999
RO program	licensed (	to:								
		oy: J. Lozi	er (CH2	M HILL)						
Project na				Permea					7.2 g	rpm
HP Pump flo				Raw wa	ter flo	w:		1	4.4 g	pm .
		ss.: 100.5 p								
		91.1		Permea	te reco	very :	ratio:	5	0.0 %	1
		e: 31.0 (	C(88F)							•
Raw water r	ρΗ:	7.80			t age:				0.0 y	ears
Acid dosage					ecline				7.0	
Acidified f		57.9			assage					
Average flu	ix rate:	10.2 g	lia	reed t	ype:		W	astewa	cer	
Stage Perm	n Flown	er Vessel	Flux	Beta	Conc.	គ14	ement	Ele	- Δ	rray
Flow		Conc	Liux		Press.		уре		A	rray
gpn		gpm	afd		psi	•	. y p.c	44.	<b>.</b> .	
1-1 4.1				1.11		LFC	L-4040	(	5 ·	2×3
1-2 3.1		3.6	8.8	1.12	73.2		-4040			2x3
Stg Elem	Feed Pres	Perm Perm	Beta	Perm	Conc	Concer	itrate	satura	ation	level
no.	pres drop	flow Flux	•	sal	osm	CaSO4	SrSO4	BaSO4	SiO2	Lang.
	psi psi	gpm gfd	•	TDS	pres					
							_			
1-1 1	91.1 3.5			39.0	14.6		6	486	10	-0.1
1-1 2	87.5 3.0		1.10	42.4			7	555	11	0.1
1-1 3	84.5 2.6	0.6 10.7	1.11	46.2	18.1	15	9	638	13	0.2
1-2 1	78.9 2.2	0.6 9.5	1.11	51.2	20.5	17	10	733	14	0.4
1-2 2	76.7 1.9			56.8		20	11	848	16	0.5
1-2 3	74.8 1.6	0.5 8.1	1.12	62.7	25.9	23	13	985	18	0.7
		<b></b>			=					

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

Brand Street

HYDRANAUTICS RO SYSTEM DESIGN SOFTWARE, VERSION 6.4 (c) 1998 12/12/1999 BASIC DESIGN

RO program licensed to:

Calculation created by: J. Lozier (CH2M HILL)

Project name: McAllen Phase II Permeate flow: 12.7 gpm HP Pump flow: 25.4 grpm Raw water flow: 25.4 gpm

Recommended pump press.: 140.9 psi

131.5 psi 31.0 C(88F) Permeate recovery ratio: 50.0 8 (Stage Feed pressure: 0.0 years 1 \$ 2

Feedwater Temperature: Raw water pH: 7.80

Element age: Acid dosage, ppm (100%): 56.9 H2SO4 Flux decline % per year: 7.0

Acidified feed CO2: **5**7.9 Salt passage increase, %/yr: 10.0 Average flux rate: 12.0 gfd Feed type: Wastewater

the territory water --- Food water --- Bermeate --- Concentrate

Stage	Perm. Flow	Flow pe Feed	r Vessel Conc	Flux	Beta	Conc. Press.	Element Type	Elem. No.	Array
	gpm	gpm	gpm	gfd		psi			
1-1	6.0	12.7	9.7	17.0	1.09	110.5	LFC1-4040	6	2×3
1-2	4.6	9.7	7.4	13.0	1.09	93.2	LFC1-4040	6	2×3
1-3	1.5	14.8	13.3	8.4	1.03	61.3	LFC1-4040	3	1x3
1-4	0.6	13.3	12.7	3.3	1.01	32.4	LFC1-4040	3	1x3

+	+Raw	water	reed	water	+Perme	ace	+Conce	ntrate
Ion	mg/1	CaCO3	mg/1	CaCO3	mg/l	CaCO3	mg/l	CaCO3
Ca	140.0	349.1	140.0	349.1	1.4	3.6	278.6	694.7
Mg	29.1	119.8	29.1	119.8	0.3	1.2	57.9	238.3
Na	332.0	721.7	332.0	721.7	16.2	35.1	647.8	1408.4
) K	17.1	21.9	17.1	21.9	1.0	1.3	33.2	42.5
NH4	1.0	2.8	1.0	2.8	0.1	0.2	1.9	5.4
Ba	0.1	0.1	0.1	0.1	0.0	0.0	0.2	0.1 (
Sr	1.3	1.4	1.3	1.4	0.0	0.0	2.5	2.9
CO3	0.3	0.5	0.1	0.1	0.0	0.0	0.1	0.2
HCO3	293.0	240.2	224.0	183.6	16.7	13.7	431.3	353.5
SQ4	327.0	340.6	382.8	398.7	4.0	4.2	761.5	793.2
Cl	388.0	547.2	388.0	547.2	16.2	22.8	759.8	1071.7
F	1.0	2.6	1.0	2.6	0.1	0.2	1.9	5.0
NO3	1.5	1.2	1.5	1.2	0.3	0.3	2.7	2.2
SiO2	13.9	}	13.9		0.3		27.5	
TDS	1545.2		1531.8		56.5		3007.0	·
рН	7.8		6.8		5.7		7.1	
++								+

	Raw water	Feed water	Concentrate
CaSO4 / Ksp * 100:	88	10%	23%
SrSO4 / Ksp * 100:	5%	6%	13%
BaSO4 / Ksp * 100:	371%	428%	990%
SiO2 saturation:	9%	9%	18%
Langelier Saturation Index	0.92	-0.19	0.65
Stiff & Davis Saturation Index	0.95	-0.17	0.56
Ionic strength	0.03	0.03	0.06
Osmotic pressure	13.3 psi	13.1 psi	25.8 psi

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics.
Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578
Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

Water Brown and

HYDRANAUTICS RO SYSTEM DESIGN SOFTWARE, VERSION 6.4 (c) 1998 12/12/1999 BASIC DESIGN RO program licensed to: Calculation created by: J. Lozier (CH2M HILL) Project name: McAllen Phase II Permeate flow: 12.7 gpm 25.4 gpm HP Pump flow: Raw water flow: 25.4 gpm Recommended pump press.: 140.9 psi Feed pressure: 131.5 psi Permeate recovery ratio: 50.0 % Feedwater Temperature: 31.0 C(88F) Raw water pH: 7.80 Element age: 0.0 years Flux decline % per year: Acid dosage, ppm (100%): 56.9 H2SO4 7.0 Acidified feed CO2: 57.9 Salt passage increase, %/yr: 10.0 Average flux rate: 12.0 gfd Feed type: Wastewater Stage Perm. Element Flow per Vessel Flux Beta Elem. Conc. Array Flow Feed Conc Press. No. Type mqp gfd gpm gpm psi 12.7 9.7 17.0 1.09 1-1 6.0 110.5 LFC1-4040 6 2x31-2 4.6 9.7 7.4 13.0 1.09 93.2 LFC1-4040 6 2x314.8 1.03 LFC1-4040 1-3 8.4 1.5 13.3 61.3 3 1x312.7 3.3 1.01 1 - 40.6 13.3 32.4 LFC1-4040 1x3Feed Pres Perm Perm Beta Stg Elem Perm Conc Concentrate saturation level pres drop flow Flux sal osm CaSO4 SrSO4 BaSO4 SiO2 Lang. no. gfd TDS pres psi psi gpm 25.6 -0.1 1-1 131.5 7.9 1.1 18.3 1.08 14.3 11 6 477 10 1-1 123.6 7.0 27.9 2 1.0 17.0 1.08 15.7 12 7 532 11 0.0 1-1 3 116.6 6.1 0.9 15.7 1.09 30.3 17.1 14 8 594 12 0.1 5.4 0.8 1-2 1 107.5 14.0 1.08 33.3 18.8 15 9 661 13 0.3 102.1 36.4 1-2 2 4.8 0.8 12.9 1.08 20.4 17 10 738 14 0.4 1-2 3 97.3 4.2 0.7 11.9 1.09 39.7 22.4 19 11 823 16 0.5 10.1 90.1 10.1 0.6 1.04 41.8 23.5 20 12 865 0.5 1-3 1 16 8.3 24.0 1-3 2 80.0 9.6 0.5 1.03 44.2 12 903 17 21 0.6 1-3 3 70.4 9.2 0.4 6.7 1.03 46.8 25.0 22 13 935 17 0.6 1-4 1 58.2 8.9 0.3 4.7 1.02 49.9 25.6 23 13 959 18 0.7 25.6 0.2 3.2 1.01 977 18 2 49.4 8.6 53.3 23 13 0.6 1 - 4987 1 - 43 40.7 8.5 0.1 1.9 1.01 56.9 26.2 23 13 18 0.7

These calculations are based on nominal element performance when operated on a feed water of acceptable quality. No guarantee of system performance is expressed or implied unless provided in writing by Hydranautics. Hydranautics (USA) Ph: (619) 901-2500 Fax: (619) 901-2578 Hydranautics (Europe) Ph: 31 5465 49335 Fax: 31 5465 49337

į

	Pertunability (gledpul) Pertunability Corrects Per Compension					52 74 50 30			35 16 22 72	34.38 32.79	_	22.74	174	2019 2004		26.00			8 081	_	90			20 20 20 20 20 20 20 20 20 20 20 20 20 2	105.48			_		105 48 101 80		263.77 270.04		_	90 00		31.56			23.44 22.8	21.98 21.46	2198 214		31.96 31.2	_			35.16			# 5 # 8			800			586 550
	(p=0) and				0.37	0.28	\$20	9.26	0.37	0.37	20	628	\$	0 12		6	6		8		3		8 :	02 :		2 6	22	0 12	0.25	0 12	0.12	\$0.0		33	910	2 :			970	0.74	0.70	9,0	037	30	Ĉ.	8	*	•	ò		3 3	2		, -	: 5	: E	2.95
	вического	START OF TESTING				grinners cheaning	Start sampling			ment cleaning				redded und			Describing surface			A colonial section of	C + C + 10 + 10 + 10 + 10 + 10 + 10 + 10			Distriction Market			Construction parents		mant cleaning								The control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the co					mant cleaning						marri Cleaning							mand classes	vetori le se savekt ett film seguep bennedn	Charges you was an extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive and extensive a
	Fraquency (min)	01	2 9	2 2	2	2	2	2	5	5	•	2	•	2	2	2	2 :	2 :	2 :	2 :	2 :	≥ :	2 :	2 5	2 9	2	: 2	2	2	5	9	9	9	2	2 :	2 :	2 2	2	9	9	9	è	2	•	2	2	2	e :	2 9	2 :	2 5	2 :	2 5	: =	: 9	: 2	: º
	(see) notiened 46	9.81	8 8	8 8	15.00	15 10	8	8	15 00	15.00	58	58	8.5	â.	ă 8	8	8 8	2 5	8 8	8 8	3 5	3 3	3 5	2 5	2 5	2 2	. 8	5 8	15 00	5 8	15 00	8 8	ž.		8	8 5	3 8	15.00	15 00	8	8	ē.	٠ 8	00 51	\$ 8	15.00	8	8	3 8	8 9	3 8	8 8	3 8			3 8	
	of) Till refin move by (in)		;	3 8	80	0.3	9.0	9 0	8	0.5	8	5	90	95	0.5		5 7	5		,	* 6	3 ;	: :	: :	; ;	3 3	; ;		50	3	0.3			50	6	63	0 6		01	0.		.5	0.8	80	ě	•	#P	• :					5 -	! #	: :		: 0
	المرسوور المناء عالمه والا (1979)	3.0	2	: :	:	•	<b>5</b>	<b>\$</b>	4.5	5	•	*	÷	ę	30	ş -	2 :	: :			: :	: :			: :		; ;	*	-	•	•	\$	ş	÷	¥ :	÷ :		: :	8	0	•	9	9	6.9	÷	•	•	9	2 9	; ;	:	2 :	2 2	; ;		: :	: :
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	Ann't Will at cook of (crosta)	13.0	ê 5		14.0	140	14.0	140	5	13.0	13.0	000	130	ŝ	ŝ	ŝ	2	3 :	2 5	2 :	-	2 :	-	0 0	<u> </u>	2 5	130	130	5	13.0	13.0	130	130	130	96	000	2 5	000	130	130	130	130	130	13.0	0.00	130	130	e :	2 2	2	3 5	2 :	2 2	-	: :		. 5
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	(led) stressed 46	3.0	2 :		30	30	30	30	=	9	3	£	33	ŝ	6	35	9 9	3 ;	7 .	5 6	9 0	7		9 :	1 2	7 5	3 .	2	30	<u>.</u>	3.1		35	Ę.	35	¥ ;		35	32	32	33	33	33	33	33	3	<u>-</u>	; ;	•	7 7	7 6		* :	; =	: =	. 6	32 ;
Commencione   1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1,	(by		5	3	6.75	8	95	5	5		\$	8	175	929		0.50	020	•	2	30.0	5 3	9	3 5	9 6	3 6		920	0.25	0 20	0.25	520	•		2	8		8 8	8		3	3	2	27.0	•	8	š	8	8 ;	\$ 8	2 2	3 8	3 5	, <u>,</u>	. 5		2.25	: :
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	anched shaft sharmed (mqg) 98	8	9 9	3	9	\$	4.5	\$	ş	7	÷	\$	5 7	8	30	6	0 0	3 ;	3 6			: :	: :	: :	: <b>:</b>	:		÷	Ę	÷	\$	ş	Ş	ş	•	:	•	•	9	¢	ê	9	•	ç	9	ŝ	9	9			2 5		3 9	, ,	; •	; 6	; ;
Comparison   1	Diomass Peckeuludo Rele (gpm)	24.0	<b>8</b> 8	2,0	28.0	21.0	8	150	91.0	ĝ	3.0	32.0		270	25.0	380	280		8 1		3 3	5 5	8 8	5 .	, 2	2	310	8	28.0	8	8	28.0	280	ĝ	20	8		38	2.0	62	360	27.0	2 <b>8</b> 0	27.0	6	ě	è 	240	2 2		5 5		č \$	2 2	26.0		, ĝ
Continues   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color	nie priemmental Air (cin	3.5	: :	1	\$	35	35	35	3	ŝ	35	3.5	3.5	3.6	3,	S.	5 5	2 3		:	£ ;	ç ;	9 9	£ 5	2 5	, ,	3 6	35	3.5	5.	98	3	e e	3.5	<b>S</b>			: :	35	35	3.5	35	32	35	35	<b>SE</b>	38	32	3 :	; ;	-	5 3	2 4	; ;	; ;	; ;	
Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communicatio	(cas) WS 44	250	8 8	2	\$2	25.0	220	52.0	250	250	25.0	25.0	25.0	52.0	520	- 25	200	ŝ	6 2	2 2	č :	ē :	2 :	82 8	÷ ;	2 2	. 8	520	250	55 0	25.0	25.0	250	25.0	25.0	25.0		250	25.0	280	52	25.0	520	25.0	25.0	320	520	8	Ĉ S	8	6 9	G :	3 2	ž	, ,	, ,	200
Community   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer   Computer	(generation) are the co	27.0	2 2	Ř	27.0	27.0	0 <b>8</b> 2	27.0	280	27.0	27.0	580	27.0	8	210	22.0	22.0	2	24.0	2	Ĉ i		2 1	2 3	0 2	2	92	2	26.0	ž	27.0	\$ *	280	5 5	2	2	, ,	2	**	280	582	240	240	260	260	57.0	280	260	8 5	27.0	9 2	2/2	Ĉ S	, ,	, ş	3 2	27.0
Colores   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore   Colore	(well) epitholy pee					_	_		_			_										_				_	_	_	_		_								_	_		_	_				_	_		_		_		_			
Community   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Co	Totalita Totalita Totalita			_	4367181	437333	437538.0	441298	443078	448030 (	4472980	_	_	÷	-	-	_		_	_		7		10200	700	200	474806	_	_	Ť	-	-	-	_		_	_	_									_	_					•••				
Commenter to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to compense to com	gathani windi wasi	5863		2500.0	3	9810.7	2811.7	\$45B	8	54517	56533	2668	5678 1	\$677	2005	570	5,007	3/6	2	2	2,6	66.6	,	27	, ,	200	5776.7	572	5796.7	5797.5	878	56.	- \$	2862	ž		5	5873.2	5884.2	\$	59120	28140	7 7185	5917.2	5035	2838	9565	505	1	i de			6000	****		100	60437
### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CONTINUES 1240  ### CO	(and) and primary evitations	80	5 5	Ę	47 28	87.8	2	28	4	95.25	97.50	101 00	122 54	122 58	127 %	*	1.69.17		8	8 5	8 1	8	20 1		1 2000	21.7	10 C22	241 08	243 08	34.5	247 08	265 28	85 88 2	280 28	283.00	3130	8 94	32.08	337.06	343.04	80.58	363.08	364 17	366 58	385 58	301.08	409 08	5	1 213	8 1	2 3		, 5 , 5	1 6	487.04	168.25	8
	(released) and?	\$100 AM	8 5	MA CIT	7.15 AM	1.00 PM	2.45 PW	7 30 AM	Md 00:	7-15-834	9 30 AM	1 00 PM	10-35 AM	9.00 AM	2 00 PM	9:00 AM	10 35 AM			96.	100	00.00	15.00	8 9	1000	200	2 2	2 30 AM	9 30 AM	11 00 444	1 30 PW	7:30 AM	12 00 PM	8 00 AM	30 44	8	216 7	3.30 PM	7 30 AM	1 30 PM	7 30 434	9 30 AM	10.35 AM	1 00 PM	B 00 AM	1 30 PM	7 30 AM	8 30 4	10.35 AM	20.		2	7 00 48	1 2 2	1 2 4	200	MA OF C
the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the part of the pa	••••	00:9 8881/80/00	02/19/06/19/0	C1-(1-04-1/2000	02/04/1964 7:15	00/08/1948 13:00	DE/08/1988 14:45	02/08/1968 7:30	ODICH BBS 13:00	81:2 8861/01/20	02/10/1998 B:30	00-11 888 IV-010	82/1/1988 10:36	02/14/1964 8:50	02/14/1988 14:00	00:4 844484/20	02/16/1999 10:35	10 mary 1000	C2/16/14/00 12:17	05.1946.70	00:11 #641.791/20	02/10/10/10/00	0001771888 7.15	02/17/1898 10:00	Will sentings	On the second state of	MOTOR 13:30	02/19/1999 7.30	DE 8 9041/41/20	00:11 0001/01/00	00:51 6661/81/20	02/20/1998 7:30	02/70/1999 12:00	00.8 8881/15/20	02/21/1988 11:30	02/22/1988 7:30	51.71	00.22/1999 15.30	OC 7 999172750	DE-11-0001/22/20	02/24/1999 7:30	02/24/1998 8:30	02/24/1999 10:35	00:01 6881772720	02/25/1999 8:00	02/25/1989 13:30	02/26/1989 7:30	62/24/1999 9:30	02/26/1999 10:35	05.01.0001.000.00	01.18461.1200	02/27/1888 11:15	027 200 Table 10.00	2.7	Open manifest	OF PLEASURED	OE / Sperioner
		Bat 2899	1 200	Am 2778	Man 20078	Man 2/8/70	Men 2/8/99	Tue 2/8/98	Twe 2/8/88	West 2/10/88	Wed 2/10/98	Wed 2/10/09	Thu 2/11/80	Sum 2714/98	Bun Z/14/90	Men 2/16/00	Mon 2/15/46	10 P	Mon 2/16/80	Tue 2/16/20	Tue 2/16/90	The Erithmen	Mary 2012 Days	West 2/17/98	West 2/17/No		The 2010s	Frizmene	Frd 2/18/88	FH 2/18/86	F# 2/19/90	Sel 2/20/98	8-4 2/20/ME	See: 2/31/80	Sur 2/21/10	Men 2/22/80	M.7272 word	Men 2/23/10	Tue 2/23/80	Tue 2/23/88	Wed 2/24/98	Wed 2/24/38	Wed 2/3479	Wad 2/24/98	Thu 2/25/19	The 2/25/99	FH 2/26/80	F1 3/24/98	Frt 2/26/99	F# 2/28/98	Ser 2/27/00	Sat 2/27/9	Sun 2/26/99		TOTAL STATE	Mary 2017	**************************************

Page 1 of 13

	т-			_	_	_			_		_	_	_	_			_								_				_		Т						_													_				_	_		_					_	_		_
Meli (Alies (kr)	=	173	17.3	17.3	17.3	17.3	173	17.3	-23		:	-	17.3	17.3	17.3	173	17.3	17.3	12.7	:												: :	ŝ	11.5	187	187	187		•	:		4	4	187	-	•	•	187	.0	.e.	187			: 5	:	:		r E	187	187	9	187	•	•	ì
tend (140	:	•	3	3	=	<b>8</b>		=		: :		=	=	=	£.	<b>8</b> 18	6 18			:											;		9.28	9.28	571	818	5.71					5.71	2.7	5.73	2.2	2.73	2	<u>.</u>	5.71	5.73	5 71	\$ 71	5.73		:			<b>8</b> 5 <b>8</b>	573	5.71	5.73	5.71	: :	2.3	2.11
Permentility Corrected for Temperature fronts (gridipel)	3	68	6.87	10.73	ž	125	8	8	3		2	8 82	=	=======================================	2	-29	60.9	77	2	Ĭ											1	9	£	2	37.20	35 16	31.00	5	37.00		2 !	28.87	96 93 93	23.28	£	3	30.27	78 87	26 57	30.27	30 54	30.27	24 22		;		ě	46 B3	£	24 BD	24 22	25.39		24 25	g 22
Permeability (phisped)	8	78	8	10.90	4.17	9 25	9.25	8.18	*	}	8	52	27 12	22 12	9.28	6.51	7.33	9		}											5		=	88 97	38 08	35 16	31.74	2	8	1 8		E	8	28.30	2	8	7. E	7. 16	27.23	2 6	31.75	31.74	36.30	90 91		9	2	46 88	25 38	25.39	25.39	25.30		52 38	25.39
(m) 401	* 2	2.4	7	15.	1,7		1.87	17			2	=	4	2	-	2 85	238	366	•	:											;	9 ;	8	958	5	970	0.59	3				8	970	3	e 25 0	2	950	80	590	0.59	850	950	9.74				6	950	7.	9.7.0	0.74	9.74	; ;	0	0 74
· ·			mant cleaning						conservation relation					mary flush					and followers on the second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second se																mentinane changeout		District Cleaning	and and			_			mater classing	ester cleaning					marri cleaning	after channey								Prateri chatring	after memi cleaning					_
(min) Youtherd (min)	٥	2	2	5	2	5	ş		٤	: ;	2 1	2	2	2	2	2	2	2	: 5	:											:	2 !	2	01	ē	2	ā	9		: ;	2 :	2	2	2	2	2	2	2	2	ē	9	2	9	: 5	: :	2 :	2	2	2	5	10	9	: :	2	2
(see) Aedirard 96	158	15.00	8	8	8	8 2	88	8	8		3	B .	B 2	8.8	8	15.00	15.00	951	8	3	_	_									3	3	8	15.00	500	90 51	15.00	8	,		3	8	8	8	8	8	8	8	8851	15.00	15.00	200					8	8	8	8	8	15.00	3 !	8	15.00
ni) 4di wata mwuzeV (g4	2	•	ŝ	;	*	=	:	0.7	9	: ;	;	86	33	33	38	2	9	ē		;											1	5 :	5	\$0	•	0.1	1.5	:	:	: :		-	1.2	2	- 2	2	2	Ξ	:	:	=	:	:	: :	: ;	3 :	n >	\$0	-	.5	1.5	-	: :	<u>.</u>	- 2
The rafts after Br. (1992)	3	9	2	2	\$	9	Ŷ	9	•	: :	:	•	\$	2	ş	•	9	9	9	3											,	:	D:	÷	¥0	9	9		:	:	3 :	£	\$	Ş	ş		8	9	9	9	5.9	9	8.5	:	: :		-	•	59	59	45 80	Ş	; ;	5	22
iouT 900 at and 90 (cred.)	13.0	13.0	130	9	13.0	39	13.0	0.51	130		3 ;	130	ŝ	130	0.51	130	130	130	92.	}		 									;	2 1	2	5	9	ě	180				1	92	20	5	130	200	90	5	ē	50	130	130	130	2	:	2	3	ě	ŝ	130	130	97	: :	2	130
(ped) namena. 44	?	32	32	*	32	32	32	32	:	: :	;	3.2	3	3.2	3.2	3.5	3.2	3.5	: :	;		 												*	22	2.8	2.8	:	;	: :	, :	* *	<b>\$</b>	*	. s	56	2	56	5.6	5.6	5.6	3.6		: :	: :	•	2	5.8	2.8	2.	88	33	; ;	27	38
ed) 48 profeed recursory (give	88	808	8	320	2	3.8	3.8	4.30	98	: :	3	8	8	8	380	5.40	8	5	8	1												8	8	250	5	8	1 20				3	£	8	5	2	2	2	1 20	9	20	22	2	5			3	3	3	8	2	2	95	3 :	2	95
protes that beautif	:	<b>\$</b>	•	<b>2</b>	9	:	:	9	9	: :	:	9	ş	ş	9	9	9	9	9	3		 		_							,	: :	;	÷	5	9	9	: :	:	: :		2	<b>5</b>	S:	59	£	£	•	ě	6.9	9	\$ 9	3		: :		•	9	e •	\$	8.5	9	; ;	5	65
notheres feetwarten (mag) ainf	ž	Ř	ğ	27.0	280	74°0	28.0	18.0	-		2	220	2.0	1,0	9	280															:	3	R	9	Ř	37.0	37.0	4	,	: :	,	×	37.0	8	Š	340	8	45.0	ž	37.0	37.0	8	<u> </u>	1		Ř :		8	ģ	ŝ	8	5	,	ž	9
(cf2) tå inhemotoppul	ä	¥	38	š	3.5	35	3	3	-	;	; ;	e P	5	38	38	35	3.5	35	91	;												; ;	Å	2	8	38.0	38.0	ş	<b>5</b>		ŝ	8	*	8	ose -	8	š 	ĝ	ŝ	38.0	350	38.0	7	, ,	: :		ì	380	ŝ	43.0	ê	929	,	÷	•
(was) MZ MY	ž	28.0	S2 -	25.0	230	20	28.0	28.0	20.00			2	25.0	92 -	28.0	25.0	25.0	25.0	9.6	:											;	è :	200	250	25.0	25.0	250		-	-	2	°2	320	250	320	ŝ	220	\$2 	2	280	250	25.0	25.0		:	2	250	250	250	250	250	25.0	: ;	280	25.0
(2 seesgab) WZ quia?	380	3 <b>9</b> 0	Ř	2,	380	220	200	280	280			2,0	27.0	22 n	27.0	27.0	27.0	27.0	8	Ì		 					_				ş		280	25.0	260	25.0	26.0	ž	,	;	2	280	27.0	380	280	ć.	57.0	2	280	27.0	27.0	27.0	97.6				ŝ	် 2	5 <b>6</b> 0	92	£	ž.	Ĉ :	27.0	250
(mqg) eternicit bec'i	_	_		_		_	_				_		_	_	_	_	_														ļ		_	_		_	_										280		_					2	_				230					_	_
technis? electron? (ing) galiane?	+-	\$ 150m25			_		512796	5701831										563 500													7-							_									6359912					646227 2			_							_			_
Property report areas	ž	7 250	- 60	9.00	2,00	100		6115.0	4117.0			20219	613	61412	61623	91842	6173	61783															62150	\$522	\$ 8528	9528	8280 9				8	5 282	Š	0,000	200	215	200	8	6352 5	ě	63653	95	6176					200	21.2	94130	212	277		653	3
Bedrando evitabendo (esti) emit	8118	529 00	22 125	2	E36.08	553.00	559 08	\$77.06	678.04			8	90 108	80 80	625 08	82.0	540 OB	3		3 2	2 2		8	80 80 80 80 80 80 80 80 80 80 80 80 80 8	653 08	923 09	65.0	80.00	46.53.04	2			3 2	20.55	706.06	725 54	728 17	770.7				35 26 26 26 27	2	776 83	778 08	20 E	187.58	8	821.33	853 28	824 83	827.58	97 270			8	3	865 09	867 58	80 08	871.58	80 000		98.98	91308
أتصب (أبريضا)	1:30 PM	7.30 AM	10:00 AM	100	130 PM	7:30 AM	130 PM	7.30 44	20			200	7:30 AM	10 30 AM	7:30 AM	11:30 AM	7:30 AM	10 30 AM	, m m			3	12 00 AM	12:00 AM	12-00 AM	12 00 AM	12 00 AM	12 00 AM	IS ON AM	7.00 AM		2	30.7	7 30 AM	(2 00 PM	7 30 AM	10.05 AM	9	20.00			2	30.7	10-45 AM	12 00 PM	300	7.30 AM	2 00 PM	7 15 AM	NA 00 6	10 45 AM	130 PM	2 20. 434				12.00	7 30 AM	10 00 AM	11 30 AM	2 00 FM	MA 07.	2	2 30 Ph	7:30 AM
· · ·	05:01.000	03/03/1946 7:30	OCHES/1998 10:00	00-11-0001/20/00	00:01949 13:30	001/ BBIL 90/02	02/04/1999 13:30	02/05/1888 7:30	OT-0 MONTON			03,01,048 13,00	02/1988 7:30	00:01 8441/90/00	02/19/06 7:30	02(11) 000(1/2000	03/08/1948 7:30	02:01:0001/00/00	2.1		000000000000000000000000000000000000000		00/12/1998 0:00	00.0 4441/61/20	03/14/1989 0:00	03/15/1998 0:00	03/16/19/06 0:00	03/17/1998 0-00	0.073/1868 0-00	2.00		2	02/20/1999 11:30	03/21/1998 7:30	03/21/1888 12:00	02/22/1999 7:30	90-01-909-12220	A-11			05.1 4441.47260	05/23/1998 13:30	02/24/1994 7:30	03/24/1889 10:45	03/24/1998 12:00	03/24/1898 15:00	03/25/1996 7, 50	00-F1 8661/52/E0	E1.7 0001/35/CD	03/24/1999 9:30	03/26/1909 10:45	03/28/1999 13:30	OF 1 0001/2/2/20	OF STREET, STREET		G1:01 8641/1750	03/21/18/81/2/CD	02/29/1999 7:30	03/29/1996 10:00	OC:11 6661/62/E0	03/2 - 1999 14:00	07.3041464	2	03/30/1996 14:30	03/31/1986 7:30
•••0	Tun 3/2/88	****	Wed arabe	West available	Wed britis	The payor	The Marte	FH 3/5/00	Ed World			2 P. P. P. P. P. P. P. P. P. P. P. P. P.	£ 750	Eat 246/00	Sun 3/7/96	Sun 2/7/80	Men 3/8/76	Men 346.00	1				847 K	Fet 3/1 // 18	Bur 27 e	Mon 1/15/Ne	Tue artices	Wast 2/17/89	The 1/10.00	10.00		77.00	5at 3/20/10	Sun 3/21/86	Sun 3/21/99	Mon 3/22/86	Mon 1/27/98				*****	Tue 3/23/89	Wed 1/2//00	Wed 3/24/88	MAN TAT POM	Wed 3/24/88	Thu 3/25/89	Thu 3/25/88	Frt 3/26/79	F# 324/96	Frt 3/24/29	Frt 3/26/99	201.107.00			THE PLANE	Sun 1/2 live	Mon 3/24/99	Non 3/28/99	Mon 3/29/99	Mor 329/99	Tise (C)000		Tue 270096	Wed 3/31/98
hw/Pagari																																																																	

	_		_							_	_		_			_								_		-	-	_	_		_	_		_	_			_			_				_					_	_	_		-	_											
Ziriz (Aller BP)	286	27.3			27.3	273	27.3	27.3	673	27.3	27.3	: :		6 / 2	27.3	•	18.7	12	•	ì	<b>18</b> 7	18.	1		(8.	:	:	è :	-	-	-	18.7	18.7	187	•	:		•		-	18.7	. <b>8</b> .		18,		18.7	18.7	£ #	187	187	4	:	è :	18 Y	187	187	187	187	18.7		•	è	92	18,	187	187
(zwi) Tilki	5.73			•	5	ē	3	3 91	38	3.6	ě			Ē,	56		5.7	5.75	-		5.71	2.	5.73	ĩ.	12.5					2.	2.5	2.5	5.73	573			; ;	,	571	5.73	5.71	1,75	5.71	7,4	\$71	5.71	571	5.71	5 21	5.71	5.73	. :	,	£ 7.1	571	5.71	5.71	12.5	5.71	:	; ;		25	2.5	571	- 25
Permentiliy Comected for Temperature Effects (gld/pol)	24.80	8	2 1	8	2	8 2	29 01	1327	13.97	13 82	7		E :	3	2	12.0	8 OZ	20 18	79.07	2	8	21.37	20.87	29 62	20.87		: :		8	8	20 87	20.38	20 87	16.71	20.00		. :	200	8	21.37	1, 61	20.38	96 61	20 67	96	20 38	20.38	20 87	20.38	20.38	9		807	8	20 87	20 87	20 87	22 17	- 2			3	20 02	12.40	.60	13 00
(majohit) (glidoneri)	*	h i	2 :	8 :	75.21	1237	5	28.51	14 65	13 82	25	:	R :	ę P	2	51 16	91 12	21 16	;		- 5	22.4	22.41	52.41	22.41				9	- -	ž	- Z	24	21 16	-				- 52	15 41	91 18	25 ¢:	17 22	17 22	17 22	5 2	3	17 22	22 41	22 41	22.41	-		÷ 2	15 62	15 22	22.41	23.81	8			 R E	529	12 70	1.20	12.70
(led) WIT	P. 0	î :		:	5	2	*	<u>.</u>	187	3	5 03		3 1	8	8	88 0	***	0 88	-	3	200	180	0.00	0 83	0.83				98	0 83	2	680	083	800				5	0 63	083	88 0	0 83	0.83	0.83	0.83	0.83	0.83	0 83	0 83	083	0.83		3	083	0 63	0 83	0.83	62.0	3.	:		è	1 82	1.47	1.67	-
Consulting			Annual Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the Country of the				maint cleaning	after mant cleaning		_					and back flow testing			Theird Contrato	Section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the sectio	After menni cheering				Brandell Sharan sandyla		-			_					mane cleaning															maer cleaning			-				mark channes							•			_
PP Frequency (min)	0 :	9 ;	2 :	2	2	2	2	2	2	2	<u>•</u>	: :	2 :	2	2	5	2	2	5	2	5	9	5	9	2	: 5	: :	? :	2	<u>.</u>	2	9	ō	٥	5	: :	: :	<u>.</u>	9	9	2	9	ê	9	2	2	2	5	õ	0.	2		2	2	9	2	2	5	9		: :	2	2	2	0,	10
(ma) position (age)	8 5	8 9	3 5	3 1	8	8	ž 8	8	8	8	8	1	3 1	č B	8	15.00	15 00	8		3	58	5 00	15 00	ž,	90 51		3 8	3 1	8	÷.	8	12 00	15.00	15.00	8		3 1	B	ž. 8	ž. 8	8 8	5 00	5 00	8	8	15.00	58	15.00	15.00	15.8	15.8		3	8	58	8	8	8	8			3	8 2	8	8	8 5
(D) 42 may (D)	2 :	3	: :		:	:	7	ŧ	•	Ŧ	<del>-</del>	: ;	: :	÷	÷	=	=	=		-	4	9	;	-	1.7	:		: :	-	-	1.7	1.7	11	-	-	: :	: :	:	,	1.1	1.1	÷	- 1	-	-	-	- 1		1.			: :	-	÷	-	-	-	-	5	: :	: :	n	e e	8 e	6.2	52
Til solle skill keerret (mm)	\$ :	= :	: :	: :		2	÷	\$	5	56	58	! ;	: :	•	5	6.5	9	5.0	-	•	¥	59	5	9	5 9		; ;	: :	0	5.	9	8 2	9	9	,	:	: :	<u>.</u>	5.	5	6.5	ş	6.5	9 9	6.5	\$ \$	9.0	Ş	ş	8.5	5.9	;		9	5	65	8 9	59	4	;	: :		un <b>4</b> 0	<b>9</b>	6.5	9.
hm? 413 st cost 44 (crest.)	9	12.0	2 1	1	25	ţ.	9	13.0	ŝ	6	9	: :	3	9	13.0	13.0	130	130	:	2	130	130	130	130	130	:	3	2	130	130	13.0	13.0	130	130		2 9	2 ;	3	5	ç	9	130	130	13.0	130	13.0	2	130	130	130	95		130	9	13.0	130	13.0	130	13.0	: :	: :	200	000	130	130	13.0
(jed) enceend dig	9.2	. :				2	2.8	2.8	7	32	: ::	: :	; ;	2	35	32	33	32		ş	33	5		3.1	Ē	; ;		, !	5	3.5	33	35	33	32	:		: :	ž	32	3.2	32	33	33	÷	35	33	3.2	32	33	3.2	:	: ;		35	33	31	33	3.2	E	: :	; ;	ŝ	35	3.7	3.5	38
III) 48 evolve emmery (84	95 4	3 40	3 1		3	3	95	8	3 80	8	01.		2 !	€	2	28	ž	8		2	- 70	1 70	1 70	ç	1 70			3	98	1 70	5	0.7	2.7	2		: :	2 :	2	2	0.7	1.80	0.7	4 70	5	5	5	5	1.70	1.70	1 70	1 70	:	2	20	2	2	22	2	320		: :	ê	2	8	3 40	300
evated alaft absorped (mag) %	53	9 :		: :	2	e:	-	5.	\$	5.0	2		: :	0	9	es T	\$ 9	8 5	:	•	ş	ş	ş	5 9	9	: :	; ;	: :	ç	ş	<b>9</b>	9.9	6.5	6.5		; ;		:	<b>5</b>	5	6.5	6.5	9	6.5	5.0	9	9	5.0	59	9	*	;	60	S 0	6.5	6.5	9 2	6.5	8.5	: :	: :	•	Ş	5 9	9	\$
notinississississississississississississis	0.04		;	3	,	8	0.27	ř	980	976	*	:		5	37.0	380	0 0#	380	į	·	980	430	37.0	32.0	31.0	, ş	, ,	2	e g	380	9	37.0	37.0	37.0	980	, ,	,	3	37.0	9	42.0	š	007	380	37.0	089	37.0	380	380	8	0.03	: :	3	37.0	\$	360	380	37.0	69	;		9./4	÷	9	380	380
(ml>) NA latnomotogue	6114	- :		2	•	0 0	0 24	007	0.09	9	47.0		2	7	63	o \$	42.0	10.79		=	ç	3	430	0 37	43.0	•			0.3	01	430	00	42.0	9	9	, ,	2 ;	?	•	62	100	0.24	9	0.29	0.00	42.0	45.0	45.0	9.27	410	9		ì	3	ç Ç	0	9	90	97	:		2	420	420	014	ŝ
(uga) MZ AY	25.0	320	6 :	62	è	250	250	250	25.0	25.0	35.0			Ĉ	320	25.0	25.0	05/	Ş	2	ę.	05.7	25.0	26.0	25.0		9 9		200	25.0	250	25.0	25.0	25.0			3	8	980	25.0	55.0	25.0	25.0	25.0	25.0	25.0	250	25.0	250	250	25.0		950	550	250	25.0	25.0	25.0	25.0	: :	: ;	200	250	750	250	2,50
(5 sorngob) WS grant	38.0	2	2	2	2	e <b>X</b>	942	27.0	27.0	250	250	: ;		2	270	<b>58</b> 0	27.0	27.0			œ R	27.0	280	280	280	:	:		B B	8	ŝ	280	982	ŝ	2		:	:	ŝ	27.0	280	0 82	8	580	8	8	200	280	2002	8	900		E	Ř	0 80	28.0	280	280	27.0		: :	e 8	5 <b>8</b> 0	260	280	54.0
Feed Flourain (gpm)	9 22	ž :	3		2 2 6	2	24 0	280	27.0	28.0	280			ž,	8	540	\$10	280		_		290	3,0		200				280	280	_	280				_		ŝ			ŝ	27.0	35.0	280	200		280	26.9	22.0	280			0 /2	520	28.0	280	27.0	180	100	: 1		_	Ĺ	290	280	240
Tomassio Totalizar Frankling (Bel)	678315.5	1000	2		2	6710910	621089	190089	680792 1	080360	6049070			581987 2	6818429	6927290	699074.0	700015	200100	700130	700878.2	706969 8	708255 5	71500075	714650 5				7246534	725391 2	7317849	7338260	7402656	740889 6	2			) CRG+ / -	750615	756881 8	757577	750067	759039 8	765389 9	7666162	773931 5	775279 9	782396	7834720	783667 8	784229 9		7 1506/	792718 5	799093 8	799815 8	B000028 4	8012828	907708			20 <b>5</b> 48	8164127	8165884	817218	623447 8
gritteef heeling	7 8519	9				9	979	100	ž	60709	2		2		9	54864	1058	6506.7		7058	8508.8	6828	6\$30 4	11559	6000				6576	65782	6596 7	6802 1	68201	6627	,,,,,			į	99202	4 / 299	6669	66710	66737	86514	199	6715.	67190	67388	67417	6742 5	4744.1		8/6	67681	67861	67881	4788.0	67924	ABORR			68023	6835 1	6838 9	6839 7	5.855 7
Britishand Grankman (end) andT	913.16	202		8	8	916.33	200	85033	951 08	251.32	35		2	3	ž	943 58	961 08	8		90	500	7	9.745 OB	1000 50	5		8 9 9 9	G :	1037.00	1027 08	1057 08	1063 08	1061 06	105108	-		9	55.00	1112 08	1129 08	1131 08	1133 33	136 08	1153 58	1157 04	177 58	1181 33	1201 08	1204 08	1205 50	1307.08		1225 08	1531 08	1249 08	1251.08	1252 54	1256 08	1277.04		8 1	296 82	1299 58	1301.08	1302 83	1320 63
(nim:sd) emil	7 35 AM	1 40 AH		8	10.29 AM	10 45 AM	- 08 AM	2 45 PM	330 PM	3-45 PM	76.00		3	8 6 6	- 28 AM	2 00 PW	7.30 AM	10 00 MM		<b>1</b>	<b>2</b> 00 L	7 00 444	10:30 AM	S no Alle	AN GO			3	2 S AW	1 30 AM	7.30 AM	1 30 PM	7 30 AM	9 30 AM	,		3		2 30 PW	7.30 AM	M 00	11 45 AM	2 30 PM	8:00 AM	11 30 AM	M 00 M	11 45 AM	7 30 AM	10.30 AM	MY 55 11	Md of		M 00 /	30 7	7.30 A.M	9 30 444	11 00 AM	2 30 0%	7.00			W S .	10 00 AM	11 30 AM	1 15 PM	7 15 AM
•••	86.7 8		_	_	_	03/31/1996 10:46	40:11 8881/1E/E0	02/31/1999 14:46	02/31/1999 15:30	_	_					04/01/1999 14:00	04/02/1998 7:30	_		_		04/03/1999 7:00	DARGO11998 10:30		-	_		_	_		_	04/05/1999 13:30		_			0.00	CACHE MAN TO A STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STA			04/09/1469 8:30	04/08/1999 (1):45	04/09/1999 14:30	Dr. : 4441/01/20	_	-	_		04/12/1999 10:30				DEL MANAGEMENT	00:01 8661421440	04/14/1999 7:30	04/14/1999 9:30	_		04115/1444 7:30			-	04/16/1998 10:00	04/15/1609 11:30	21:01 6561791/90	04/17/1989 7:15
	SAVIES PAR					MAN STATE	SAVIES PAIN	Wed 2/31/78	Wed 20179	SALES NO.				5	Thu MAN	Thu 40.00	Fet 42.00	64 42.70		F4 4/2/00	Frt 4/2/88	Bac 4/3/99	Bas 47/78	Cut CAN	Bun 444.80			-	Hon 4574	Mon 4599	Tue 4578	Tue 4470	Wed 47799	Wast 4779			P02		Thu 4/8/88	Erd APARE	Fri 4/8/86	Fri 49/00	Fri d'arte	See Aviores	See 4/10/90	Bun 4017/8	Sun 4511/78	Mon 4/12/98	Mon 4/12/78	Man 1/1 7/8	10.00		100 403/80	Tue 4/13/00	Wed 4/14/99	Med 471478	Wat 1/1/00	Wart 471478	1			F4 421628	<b>5</b> 5 ±	F# 41408	Fre 4/16/99	Sec. 67.778
programa		-	-	-	-	-	•	-	•	-	. •		-	•	-																																																			

(hel) @file (hel)by (minheamwi heranto (hel)by (minheamwi heranto (heranto (heranto minheamy) wi heranto (heranto (heranto)	11.20 11.20	18.24		182 1829 982	19 (C) (C) (S)					172 1088 1063 5	num cheming 177 1058 1009 571	162 1154 1075 \$71	147 1120 1019 571	162 1029 932 571		- 22	95.01	200	92.01	689	_	145 1029 914 571	545	907 825	200	200		200	2 1	939	907 796	1.96 9.52 9.66	2.06 0.07 8.25	208 903 808	818	905	3		200	300	2 1	55 8	908	& 25	407 865	2.06 #07 845 571	241 7.77 707	2.38 7.94 7.22	231 8.10 7.37 5.71	100 720	20 232	22 20 20 20 20 20 20 20 20 20 20 20 20 2	£ ;	236 784 /22	241 777 8:90	324 577 501	614 520	3.05 614 5.59	305 814 548	314 595 568		8	2.55 7.33 451 5.77	- E
(upu) Avenipera (upu)	Q.		- 9	CO TRAINE CHENTY	9.				2	•	10 manufact	9	•		0.		Ol Oliver		9	- 10	•	01	01	•		Of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Contract of Con	_	2 :			0-	_	10 mans clearing		9.	9	9		Contract breach		= :	2		- -	0	•	_	to mark cleaning	0.	- ·	- 01		2 !		10 mark cleaning	_	2	4	10 GAC 1419AF MLSS 10 10.000 mg/L	_	0,0		-	
(see) notherwO 48	15.00	8 8	8	8	85	8	8		8	8	15.08	588	15.00	9 51	8	885	5		8	\$ 8	8	\$	8	8	9	8		3 8	2 2	8	8	58	15.00	15 00	25.90	15.00	851	8	8		3 8	8	8 8	5 8	ž 8	5 9	5 8	15 00	8	500	15 00	8		3 :	8	8	15 00	8	15.00	15.00	8	1 1	3 1	8 8
(a) 98 volte muucel (git	32	5 5	32	7	33		:	: :	- =	50	37	33	3.5		96	38	: :	: :	5	•	32	33		7				: :	: :	:	2	36	96	=	-	-				:	: :	2	- -	7	2	3	;	;	9	4	•	. 9	: :	•	05	80	29	-	-	:	: :	2		
(mate)		::		•	\$	5	: :	; ;	0	6.5	5.0	5	9	5.0	9 9	19		; ;	•	\$	ş	5.9	45	9	4	: :	, ,	: :	: :		9.2	9.2	9	85	5 5	5	4		1 4	; ;	2 :	¢ :	•	99	6.0	5	ş	:	6.5	5	6 5	40	; ;	ç :	ç	9	6.5	65	92	9		: :	•	3
Me toos in Cif Tenii (credii)	96		130	13.0	130	951		; ;	90	130	130	130	130	13.0	130	130		? ;	0.52	130	130	130	30	130	1 2	: :		2 :	2	130	130	130	130	130	130	130	0.51	9		: :	? :	2	ě	13.0	ë -	13.0	130	130	130	130	130	130	; ;	2	9	20	130	13.0	130	130		2	2	2
(leq) others (leq)		; ;	: :	5	3.6	Š	: :	: :		39	35	36	3.6	35	90	36	ž	; ;	=	35	· -	3.6	36	3.8	-	: :	:	; ;	: ;	9	*	3.6	3.6	37	3.7	37	36	ç	- 2	, ,	9 ;		- E	1,0	37	'n	96	Ħ,	33	e F	33	*	: :	5		E.	3.8	38		39		; :	2	;
ri) 90 enched musel (git	9.0	2 :	328	3.70	25	ş	3	: :	R F	350	3.60	3.76	3.40	0, E	376	3.70	2,0	: :	P.	0.0	9.70	3.70	4.29	4.20	. 5			3 5	3 5		27	8	4.20	0Z <b>7</b>	9	<b>4</b> 30	30	8	0,7		2 5	2 ;	8	2	22	\$ 30	96	98	\$ 70	2.4	67.4	2	 ; ;	2	8	9	629	929	620	049		2	2.	25
protect state before BP (Spm)	<b>9</b>	:	9	5 9	6.5	5	:	: :	<u>.</u>	5	40	ş	9	5 8	6.5	59	:	: :	ŝ	5	5.9	5 9	5.9	59	. 2	: :	; ;			0	 9	s •	5			5	59			; ;	: :	2	5	¥0	9	 	59	6.5	5	99	9		; ;		92	5	6.5	9.5	\$ 9	9	: :	: :	0	2 :
notteturiseff equaniti (reqt) alef	98	9 6	9	ŝ	37.0	98	:	: ;	 2	90	ĝ	90	37.0	420	360	9		; ;	97.0	420	9	360	ş	96	Ş	. 5	;	9 9	;	0 2 0	9	350	ž	0	980	3	F.	: 5	3	3 8	3 9	9 :	÷	9		8	\$	g	g		3	g	; ;	: :	8	Ç	2	æ	4	4	•	:	₽ :	3
ومشخبانسوسیم چې (دزینه)	65	8	:	9	9	9		:	o M	ŝ	9	92	9	98	9	-00		-	•	99	9	04	005	49.0	9					=	\$	ŝ	200	0	084	9	45.0	9	Š	2 5	2 :	6	ê	ŝ	ŝ	90	0 67	0.83	0.87	8	200		; ;	8	•	S	0 94	480	8	900			2	200
(wu>) #12 17#	220	ŝ	25.0	25.0	25.0	200		: ;	520	320	25.0	0 3.5	032	25.0	9,40	25.0	. 4	-	oç.	ů.	?	35.0	9.5	25.0	. 5	35.0			0 0	e C	320	250	240	32.0	ŝ	52	×	×		: 2	0 1	e :	55	52	×	£	55	55	ĸ	×.	×		3 :	2	K.	×	52	52	52	25	. ;	. :	e :	ς .
(godiese C)	25.0	8	25.0	27.0	27.0	•		:	280	92	27.0	ŕ	200	27.0	30.0	280		:	2	3‡0	280	8	280	90			, ,	2 6	9 1	ĝ	S S	200	ê	90	596	g	20.5		: 8	3 5	R	S 82	2	8	22	2	8	58	8,	R	2	: 2	7	2	8	E	32	- 62	Я	22	; ;		8	29
(mqg) element bee?	2	8 1		280	2	070	. :		27.0	30	9	280	280	28.0	27.0	-		-	280	24.0	280	88	280	90	:			2 0	2 2	82	000	57.0	2	28.5	220	280	200		2 2	3	2	8	500	280	16.0	210	58.0	0 62	28 0	£	28.0			0 82	27.0	27.0	25.0	280	240	280	:	:	280	, ,
realisto? (199) generally	824880.0	12180	402404	0 620176	\$41239.0	Proposed in			2063	8 25025	457864 7	854270 (	0 89 1658	865396 5	8675489	87795.0	874807.	0 /000	874688 S	876/32 9	882359 6	6808583	890792.0	A92162.0	8004234			277.00	Refrance	9076104	8099735	9162334	915947 5	1 951.21	918137.0	924484 2	42KAIRO	D TORKE A	0.332.00	a de la constante	12/554	9	0120110	9425280	840871.5	951347 9	958517 0	959316.0	9595100	990215.0	946592 9	040407 2	7 /69694	9	976241.2	9764090	0 071778	9835108	985656.0	7 521286		00///66	882586	90394719
gamest with mark		2	1 200		_	_		_	_	21569	\$ 6283	# × 60	4853 7	6974 5	5 0869	_		_	_	_	_	6 5204	7045.0	_	_			30,00		_	_	71171	71181	****	71227	21404	19912	9			2 /91./	7169 2	8	7190 9	72117	72156	7235 7	72380	7238 7	7240 8	7558 7	136.0	7 1007/	72027	7284	75857	72879	7305.9	7312.0	7.729.9		375	73.02	ì
Commento Operating	EE #251	7 5	1000	1371 41	1372 63	M 3224			380	141708	141933	1621.33	10 0273	80 174	1447.06	1465.00			25.25	1472 08	1489 58	90 (81	15:3 08	16.7.0B	2 151			5 5	8 3	8	1567 58	1585.08	1587.00	1588 58	1591 33	80 00	1616.08			2 2	80 903	1638 58 1	- BO 9591	56 0991	1681 08	1885.08	1705.08	1707 56	1709 DB	1711.08	1729.08	1735.33	2 0	2015/2	1755.33	1757.33	1759 08	1777 08	1783 08	180108		000	88	85 9081
(nim:ni) and?	10.45 AM			- SS AM	_				_	_	9 45 AM	11 45 AM	_	_	_			_					_	_					_		_	_	9 30 AM	11 00 AM	_	_	_		_			_		-		_	_	_	30 AM	_				_	P 45 AM	11 45 AM	1.30 PM	7.30 484	130 PM	7.30 AM			11.30	8
	┝╌		_				_	_				_				_		-		_	-	_	-		_	_			-			-			_		_	_		_			-		-					_			_		-	-	_	_	-	-				-
<b>**</b> 0	-	00:4 8581/81/90	_		SETTEMBER 11:18	200		A	04/20/1988 13:30	04/21/1989 7:30	04/21/1996 9:45	27-11-0001/15/00	_	04/22/1999 7:30	04/72/1998 13:30	OF T BOOK TOWN			04/14/19/04 11:00	n4/23/1989 14:30	04/24/1988 8:00	_		-				WZC1966 11 30	_	-	04/27/1999 14:00	04/26/1998 7:30	04/28/1999 8:30	DO-11 445 L/L-C/NO	_	02/20/1966 7/30	A		200000000000000000000000000000000000000	a and a discount	00.11.00.100.100	04/30/1999 13:00	05,0171999 4:30	05/01/1998 10:45	05/02/1696 7:30	06.02/1999 11:30	05/01/1999 7:30	00:01 8811/20/30	05/03/1899 11:30	OS-01-1999 13-30	05/may1988 7:30	SP CT MODIFICATION	- MALADOCA	05/08/1898 7:30	05/06/1999 9-45	05/05/1999 (1:45	_	05,0521898 7,30	Ě	05-17-1989 7-30		m.a	05/07/1999 11:30	05/07/1999 13:00
<del></del>	AL 417/80			A 47.00					144 47078	West 421/78	West 4/21/89	Wed 4/21/84	Wed 4/21/80	Thu 4/22/98	Thu 4/22/86	1		-	F# 422/18	Fri 4/23/89	3m 4/3 c/m	Sat 42478	Bare 4250					Mon 425va	Mon 426/38	Tue 427/89	100 427/89	64-92-h ma	SETEP POM	94/32/p P4/A	AND PARTY.	7					HOLD P	Frt 4/30/08	\$4.51.09	See Grand	Bun \$/2/99	Sun \$7299	Man 67/78	Mon \$7399	Mon K3/M	Mon S7AB	T. 1. 5/6/20		11	MAI SCAN	Wed LAW	Wed Living	Mad S.Y.	Thu \$46.90	Thu S4/90	Fr. 47708			F4 \$778	14 EV 15 EV
mas Reguld																																																										i	ی					

	_								_								_					_			_					_				_			_			_									_	_	_		_					_	_
(as Mari) both	734	•	•	•	16.7	187	±	16,	18.7	18.7	187	187		#	4	÷	4	187	1.7		187	18.7		187	48.7		187	107			•	•	:	<u>.</u>	•	<u>;</u>	:			<b>1</b>	7.	7	11.7	18.7	<u>.</u>	<b>:</b>	18.7	187	187	18.7	18.7	187	181	187	18.7	181	18.7	1.	187
(and) THH	5					17.5	5.73	5.73	5.73		5.71	5.74	5 71	7.	5.73	5.71	5.71	5.71	5.71	5.73	5.73	5.74	5 71	5.71	5.71	5 7.4	5.71	5.73	5.7	2					2.5	, ,			5.71	5.71	5 71	5.71	5.71	5.71	17.8	5.71	5.71	5.71	17.5	5.71	2.75	5.71	5 71	17.8	17.5	571	5.71	5.71	5.71
Permanentify Controlme for Temperature Effects (girlyst)	5	2 5		8	1 68	2	8	7.87	8	8	4	*	2	92	9.6	8.8	60	8 72	2.0	8 42	7.	08	06.8	29 8	50	4 07	9 10	9.67				2 2		5	E .	g 5	Ç	. 69		50	98	š	9.28	19.67	6.0	20.6	*1.8	8 77	52.6	:		3 22	15 6	96.8	:	8 93	6 33	67 6	9 72
(heqibig) (filliamente'	7.33		-	2	2	104	404	60	95	9	25.	4 52	9 52	9 52	9 52	25 0	10 29	10 29	10 25	62 04	10.29	20 00	10.02	6.17	10.29	5		6.17	10.29	10%		2 2	8 8	3	10.29	2 5	2 2			10 29	10 29	10.29	10 29	77.0	40 24	28	10 29	10 29	10 29	10.29	10.58	10 88	55.0	85.0	10.73	10 29	9 01	8	- 2 2
(led) and	2.55		18.2	238	211	200	2.08	98	7=	12	8	8	ŝ	3	2	1 96	1 62	1 82	28	1 82	- 28	187	187	1 92	182	2	26.1	8	2	2	:	2 5	: :		# E	2 5	3 :	2	- 26	- 28	1 82	1 82	28 1	1 92	- 62	1.77	1 82	1.92	28	1 82	1.13	- 25	22	2	- 42	- 82	1 72	. 67	- 69.
				Sold State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State o						ment cleaning	•					maket cleaning								maint cleaning						Special Street				_			Consumer commen		ar flow mater broken					mand channed						grant closens						Dominos participation	•		_
(www.) Acceptancy (with)	2 :	2 5	. 9	. 5	2	5	5	2	2	9	5	ō	9	9	2	2	2	5	2	2	2	2	5	•	2	2	õ	2	: 2	: =	2 9	2 9	? ;	2 :	2 5	2 9	2 9	2 2	2	9	2	2	2	2	2	2	2	ē	۶	9	\$	5	2	9	2	2	9	2	5
Der Duradon (sec)	8 ;	3 5	8	8	8	5.00	58	5.0	15 00	15.00	15.90	8	8	5 8	8	8 8	5 00	8	8	15 00	15.00	15.00	15.00	15.90	5 00	8	20,51	50 ST	8	8		3 8	3 5	8 1	8 5	3 8	3 8	8 8	8	15 00	90 \$1	8 5	15 88	8	5.00	15.00	15.00	15.00	15.00	15.00	8	8	8 8	15.00	95.00	15 00	15 00	15.00	15.00
Vacuum after the (in		;	;		7	Ş	7	7	42	4.2	36	3	9	ê	•	9	46	3.1	3.7	3,	*	80	3.7	3.0	96	96	3.6	33	3.4	26	: :	; ;	; ;	; ;	7.	; ;	; ;			3,	3.7	37	3,7	3.7	36	3.5	3.7	37	3,7	37	36	34	36	96	37	3.7	33	33	26
18 raths shaft paramet (mag)	\$ 1	2 :	: :	: 2	2	**	80	90	\$	9	59	\$	\$	8 8	\$	*	9.2	8.5	9	90	9	8	9	65	92	9	3	\$ 8				. 4	; ;	: :	· •	: :				90	8 9	9.9	\$ 8	8 8	5	\$	5 9	5.50	5.0	88	\$	9	9	8 8	50	9		9	·
Amon Tel of second tell (prosel.)	13.0				55	22	13.0	130	130	13.0	130	13.0	130	130	000	130	130	130	130	13.0	13.0	130	130	130	530	130	0.61	130	130	130	: :	2 5	2 9		9 9	2 5	2 :	2 2	. 5	130	ů.	13.0	50	13.0	13.0	130	130	180	13.0	130	13.0	13.0	13.0	13.6	130	13.0	130	.00	130
(ing) amount %E	\$ ;	; ;			Ē	3.7	3.7	3.7	3.7	3.7	•	3.7	3.6	36	3.7	3.7	37	3.5	3.6	3.6	3.6	3.6	36	3.			3.7	3.7	7	9	: :		: :	; ;	* :	; ;	: :		36	36	96	36	90	9	37	3.	3.6	38	90	36	3.7	36	9	36	9	36	96	96	36
ni) % stoked musest	8 5		,0	9	8	4 30	£ 50	27	8	8	8	8	8	8	8	90 7	3 70	D 20	370	3 70	3.70	380	380	3 80	3.70	3.60	3.80	8	5,	3.70		2 5	3 5	2 :	2 5	2 5	2 5	130	980	3.70	3.70	3.70	370	8	3.70	360	3.70	9,20	370	3 70	3 60	8	360	3:60	3.70	3.70	92.0	340	340
enoted aloft absorbed (mag) %d	3 :	:		:	53	5 8	5 9	9.2	9	9	9	\$	50	\$	\$	92	•	÷	9.9	6.5	\$	\$	\$ 9	9	5	5 9	9	9	\$	8			; ;	: :	•			9	9	6.5	5 80	6.5	9 9	\$	\$	\$9	5	9	. 65	\$	8.9	9.2	9 8	65	8 2	8 8	•	9	6.5
nottekessinen manuetti (mag) sinfi	<b>8</b> 1	3		\$	28	3	s	8	5	- 5	ş	8	8	8	8	5	5	s	52	25	\$	š	25	25	5	28	7	ş	•	\$		: :	: :	:	ş :		;	; 5	•		7	\$	7	ş	9	\$	*	\$	\$	ş	\$	\$	Ŗ	ę	ş	٠	5	ş	9
(min) tiå lahveneigguð	6	•	9	· •	•	9	0.69	510	51.0	2:0	ž	52.0	55.0	910	80	\$2.0	210	50.0	619	909	625	200	51.0	20.0	51.0	200	9	929	820	52.0		200	1 5	2	8 5	7 5	2 3	9		_					_		_								9	260	35	98.0	280
(min) WX MA	2 :	0 ×	: *	1 12	*	33	22	22	52	22		22	52	22	82	£	×.	£	z	\$2	£	52	52	25	35	\$2	52	23	2 :		*	, y	: :	q :	\$ 1	0 8	\$ 1	. 10	. 12	5	52	£	52	22	22	52	×	22	52	£	ю	52	ĸ	52	52	ε	: 2	2	22
(O monthop) WZ double	8 :	3 7		8	8	×	8	Ħ	282	282	8	8	2		8	30.5	ŧ	æ	8	31.5	8	308	8	8	ħ	31.5	28	8	8	8	ء ا	1 2	; 6		F 8	,	6 8	R F	2	30.5	82	308	562	8	5	315	8	33	29.5	8	33	æ	29.5	35	8	6	31.5	32	<u>~</u>
(mig) elenwori bee i	2	3 5	3.0		200	540	280	22 0	21.0	280	23.0	260	200	280	280	280	27.0	5.	27.0	26.0	280	27.0	280	2	280	280	500	130	27.0	280					0 5	2 2	e :	3 2	280	290	280	56.0	280	ę,	980	26 0	260	240	26.0	22 0	280	2	280	25.0	27.0	2,0	500	280	27.0
vocinist dansared (40) galboof	1001845 5	10101	1017044	101	1018688.9	1019563 8	1028038 5	1028200	103460.0	1035320 0	1035581	1036456.0	10428100	1044986	10618484	1052370.0	1052500	1053386	1050804	10612621	1066343	1069785	1077017 6	1077844 2	91118/01	10788368	1085542 4	10876128	1003056	1094855 6	000			2000	11042013		2	1123300	0 908111	11201065	11271560	11286085	11356216	11383712	1136600 0	11374972	11441585	11462900	11526371	1153419 8	1153813 6	11546709	1161080 5	1163223 0	11697419	11705059	11706980	11715648	1178008 9
Bulliand seath seat	7367 2		7461.9	74034	7404 2	7408	7474 5	74304	7448.0	74500	74504	74534	74713	74773	7465 6	7497 6	74961	7,600 8	7518 6	1522 7	7542 1	1546	75866	75689	75699	7571 9	065:	7595 9	76139	78164	7617.2	76192	7637		76432	1	2	766	768.	76.87 8	77083	77123	7732.3	77343	7735.2	2737 6	77557	7761 6	7719 6	71817	7763.0	7785 4	7802 9	7809.0	7826 9	7829.0	7829 8	7832 9	7849.8
gottmeeto acrimento (end) essif	1829.06		1673.0	1075.33	1876 83	1879 33	1897 08	10 006)	1921 06	1823 08	1924 86	1927 08	1945 08	1951 08	1969 33	1871 33	85 2261	1975 08	1993 06	100 / 001	2016 58	2020 58	2041 08	2043 41	2045 06	2047.08	2065.33	2071 08	2080 08	2091.58	2003.08	2005.08	100000	3	211908	2130 50	00.416	2142.58	2161.08	2164 58	2185 04	2159 06	2213 08	2211 08	22125	2215 08	2233 08	2739 08	2257 08	2259.08	2261 08	2263 58	2281 08	2287 08	2305.08	2307.08	230658	2311 08	2328 58
(min:24) andT	11:30 AM	3 8 6	7.30	₩ \$4	1.15	1 S P L	7.30 AM	30.54	7 30 AM	9 30 AM	8 48	30 PL	7 30 ALL	1 30 PM	7.45 AM	9 45 AM	11 00 AM	NO OF	7 30 44	130 AM	7 00 AM	11 DO AM	7 30 AM	4 50 AM	11 30 AM	30 05	7 45 AB	1 30 FW	7 30 AM	10 00 AM		700			30 PM	1 00 M		Nd OF	7 30 AM	11 00 AM	7.30 AJA	130 AM	11 30 AM	9 30 AM	11 00 AM	1 30 PM	7 30 AM	30 PM	7 30 AM	9 30 AM	13 30 AM	7 00 PM	7 30 AM	1 30 PW	7.30 AM	9 30 AM	W 90 11	1 30 PM	7 99 AM
970			-		_	_	05/11/1988 7:30	05/11/1958 13:30	05/12/1998 7:30	06/12/14/8 P-30	-		DE/13/1989 7:30	05/13/1898 13:30	05/14/1986 7:45		_			06/15/1988 11:30			-		_		28-7 664 TURNO	_	-		00.100			_		-	00.01 00.010.00		_	_	_	_	05/24/1999 11:30	_		06/24/1989 13:30	DE:/ 4441/27/50	05.25/1999 13:30	DK 7 8881/35/20	05.26/1989 9:30	06.11.00012520	-	-	_		-		DE:51 999 13:30	
•••	- FE		200	<b>See 57 878</b>	Men 57 tree	Men S/10/68	Tue E/1770	Two Errivae	Wed S73/86	Wed Errane	West Errands	Wed 8/12/86	The \$73/00	The Sriabe	Fel STATE	Fri Bridge	Frt S71400	64 8148	Se 57.578	25 70	800 S1678	Sun Sri svis	Mon \$77.798	Mon S/1779	Mon 5/17/98	Mon 17778	The Literal	Tab Syleyse	Wed S/19/89	Med S/1988	1				The 50000	A COLUMN TO		- CA 123	844 5/22/98	Sel 5/22/99	Burn E/23/90	Bun 5/23/98	Mon 52 UNB	Mon \$2476	Mon 6/2 4/19	Hon t2499	Tue \$2550	Tue 5/25/99	Med SZGW	Med Sychts	Wed SZum	Wed M26/99	The 527.88	The \$27.84	Fri SZBAND	Fri Szans	Fri SZBV99	Fri Szanne	Set SZWM
programa																																																											

r	_						-				_		_			-				_				_																_				_	_		-					_					
SACT (SAIN SAIN) (SAIN)	÷	<u> </u>	<u> </u>	7.01	18.7	787	187	187	<u>#</u>	3	<u>.</u>	ì	•	187	<u>*</u>	187	18.7	18.7	18.7	-	.#1	18.7	-	18.	18.7	1	187	18.7	18.7		<b>1</b>		18.7	187		•	187	18 7	187	ì ;				187	187	187	187	187	-	187	18.7	187	187	187	187	187	187
(end) Title	17.5	5 5		\$ 7.1	\$73	5.73	5.73	5.7	5					5.7	5 71	5.71	5.71	5.71		: :					5	5.2	5.71		1.	5.73	Ţ	1.5	5.71	5.71	5.71	5.71	571	2.3	£ .				17.8	5.71	5.73	5		5.5		5 71	5 73	5 71	5 71	5.71	5.71	5.71	5.73
Permentility Corrected to Temperatura (glutper)	α.01	ž ;	ě	22	2/	878	9.	21	ž	8	2	S 0	22	1	1	20	4 67	683					: :			9 6	2	2 2	7 20	8	867	8 63	8 72	2	\$27	7 68	2 2	787	7 59	89 2	2 6	2	8	5.73	8	: 2			109	5.83	5.12	1.5	98.7	4 28	4.65	2 5	5 37
(ndpt) (sypposis	188	2 :	2	£ 29	£	BS 04	20 00	10.28	\$	20 30	8 :	# # = 5	8 8	623	10 68	10.00	86 01	10.28	5		8 9			9, 9,	10.01	10.07	2	. 5	0,10	50	77.6	10.23	5, 51	10 02	12.0	600	406	£0.	22			7.33	9	9 28	7 19		7.19	7.05	683	9	\$0.0		5 5	5 15	10.5	50.9	50.9
(bed) dist	157	2 !	3 2	25	2	- 1		2	2	28	2 1	2 5	2 2	2	22	2	22.5	28.		:	: :	: 2	: 2			•	2	- 2	2.31	1.7	8	26	- 82	à	26 1	5.06	238	8	:	8 8			2.75	28	98	. 5	2.60	2 65	2	2 15	3.09	3 0 5	3 63	3 63	373	3 09	906
																								_																_									_								_
				r				ij		2				ľ							•					2	•				2								2					Z						ē	,						
***********				main class				Priorie point		Train Clean				maent clean						Carde Chan						ment clean					maint clean								TAIN COM					maint clean						maint cleaning							
	İ							_																																																	
	_			_	_	_	_							_	_	_		_		_	_	_	_	_		_	_	_	_	_	_	_		_					_	_			_											_	_	_	_
(min) (min)	٥	2 :			0.	0.	•	2	•	0 :	-				2		2	-0		_				_								_		5			<u>-</u>	_		_	2 9	- 01	ē	5	5	_					- 0	- 2	- 5	- 0	- 0		_
BP Duration (sec)	15.0	9 5		5	15.00	5.	95	ŝ	ž		Ē :	8 8	0.00	15.0	5	15.00	15.00	15.0	2			15.0	15.00	9	. 4	15.00		8 9	15.0	95	15.0	90 51	8	- 65	150	15 00	15.0	15.0	8.8	8 8		- 50	ň	e či	.50			-	150	15.0	15.0	15.0	150	150	15.0	-	- 20
ni) 46 volte metros V	35		7 7	-	3.7	:	37	3.7	8	3.	\$ :	9 6	7 7	90	35	-		35		-	-	-	3 6	-	=	33	3.2	33	• •	33	:	:	3.4	6	3.5	;	:	6	;	: :	: :	133	- ~	7	42			-	: ;	÷	3,	*	:	9	63	52	<b>.</b>
The sales first about the	\$1	: :	: :	:	*	•	9	\$	5	40	: :		n 40		\$	88	8		: :	-	: :	: :					9	9 6	9	\$		•	8.5	8.5	5	9	6.5	ŝ	\$	•	0 4			8.5	5 4	. 4		9	8	\$	\$	•	9	9	9	69	6.5
99 bees in CP Teach (Fred2.)	130	9 9		0.51	65	<u>.</u>	ē	ŝ	6	2 1	2 5	2 5	2 6	69	13.0	130	13	130	13.0	95	130	25	5	5	- 6	13.0	13.0	130	13.0	0.63	130	130	130	130	136	13.0	130	13.0	130	2 5	3 5	130	130	130	(30		130	130	130	130	130	130	130	130	130	130	13.0
(jud) america dil	*	: :		*	î	38	*	ř	*	ŧ :	- :	* *		*	3,	38	ŝ	3.6	17		-			: :	-	9.6	36		37	36	36	37	36	36	36	34	**	36	37			34	3.8	3.7	38	: :		-		8	33	37	3	3	3	96	33
ni) 46 motos muusaV (gH	3.20	8 8	2 2	3.76	3.70	8	š	3.70	3.70	370	8 :	2 5	2 2	0.0	35	350	350	3,70	ş	2.2	475	3.70	2 2			180	3.70	3	2	980	8	3.70	3.70	380	8	420	4 20	₹ 50	8	2 5		5.20	8	5 70	\$ 30	: 5	9	97.5	95	2 60	6 30	\$ 30	7 40	7.40	160	92	6 30
moted state attended (megs) 95	\$	2 4	2	57	5	Ş	5.5	ş	ş		::	0 4	: :		ş	9	9 9	9	9	: :			9	1 10	9	: :	· •	3	9	8	ş	\$\$	9	\$2	\$0	50	\$	6.5	5			98	\$ 9	9	9	. 40			10°	\$ 8	\$	\$ 9	5	\$	59	5 9	65
nolitakeriseri sesansid (mag) sind	44	8, 1	; \$	4	7	\$	\$	4	4	<b>\$</b>	¥ :	ŧ \$	8	. \$	\$	\$	9	3	•	: 5	;	: \$	. 2	: 5	. 1	. \$	\$	: \$	\$	4	7	\$	\$		\$	7	\$	\$	#	ę :	3 9	25	ş	S	2	; ş	\$	\$	25	S	5	ŝ	15	5	5	22	5
(cff2) the technomologous	35	9 9	2 2	67.0	64.0	ž	95	9	8	\$	•	0 0		57.0	57.0	9	98	980	5	9	3	3	3				· ·		\$	87.0	*	35	980	0 85	0.78	0 85	58.0	97.0	\$	0.00		0 85	8	0.08	280			9	9	009	0.65	0 09	000	600	8	8	610
Are ZW (chim)	52	8 8	3 13	22	52	z	22	22	22	٤ :	κ :	5 8	3 5	×	52	35	52	25		, ×	: *	×	. %		: :	. 10	12	3 18	52	*2	52	52	22	12	×	52	23	ĸ	£	2 %	C %	: 2	\$2	23	25			, ,	: 23	25	. 22	*	ĸ	52	52	52	52
(2 corngal) WZ quari	31	8 8	i g	я	Ħ	g	8	×	8	ē :	<u>.</u>	g :	8 8	8	F	2	8	ě	5		; p	9	, 8	2	; ;	: =	. 2	3 2	8	25	8	ě	21	98	26	35	35	5	e E	E 1	3 5	2	8	315	32	3 22	, ,	. 8		31.5	æ	32.5	22	33	8	8	8
(angg) edanwoi'i bee'i	210		8	280	28.0	280	380	57.0	280	240	280	0 4	92	380	27.0	260	280	280		, ¥		2 2	782		27.0	. 8	240		380	27.0	28.0	280	27.0	260	27.0	230	160	260	24.0	08.		260	28.0	27.0	280	26.0	280	2	280	280	27.0	25.0	240	180	280	260	27.0
National description of the present (pre)	11796179		1199043.8	1186215 8	1186747 0	1197569.8	1203879 8	5057019	1211639 6	12123980	12127483	2199076	222180 4	12286310	1228781 3	1230260 0	1245297 8	12467360	0.02870.0	1 354590 1	2540e2 A	1255706.4	1282249 9	12642800	270977.5	1272151 6	1272231 5	12728801	12793168	1281004 9	1287364 9	12675074	1288947.2	1295761 6	12968584	1304758.8	13057383	13130486	13137884	3138729	1321086	1322954 2	13293410	1330078 0	1330280 0	171108 6	133,484 3	9 0796EE	1345407 5	346114 8	346234 8	1346945 6	13524612	1354839 7	13662129	13586251	1362984
Brittereff safeth world	2 15842	2		•	7801.3	7843 5	7921.5	7926 5	7942 7	į	9		2 22	7980 \$	7 000 7	2004	9000	80408	900	2	1	9046	BO84 1	9	9	=			1 1618	81362	75.6	0.55.0	37.	81778	4 0818	\$ 202B	82054	8 5228	8227.8	8228	0 072	9254	M272 0	8274.0	8274.8	122	8295	190	6317 7	8319.7	8320.2	8322.3	8 GPCB	977	83863	B356 0	8376.4
Britished Operating	2333.08	200	2377.08	2379 08	2380 83	2383 06	2401.04	2406 08	2425 08	2427 08	2428 61	80 577	2455.00	2473.08	2474 33	2478 58	2521 08	2525 06	2545.00	5	500	40.55	90	25.056	2503.04	2596.25	2597 33	2599.08	2617 08	2627 83	2641 08	2642 33	2646 16	2685 08	2663 06	2690 08	2692 58	2713 00	2715 08	2776.30	774.83	2743 08	2781 08	2763.08	2764 58	2768 83	2784 83	2778 83	2809 04	2811.09	2813 33	2814 33	2832 58	2838 08	2856 58	2860 66	5881 08
(minn:hd) and?	3			9:30 AM							11 20 AM		1 2			_				1		_		—				_	_	15 PA		B45 AW		_						00.1				9 30 AM	_			_	_		_	_			_	11 05 AM	_
															_								_	_													_			_						_		_						_	_	_	
****	0C:11 9861/8Z/90	04/30/1888 7:50 	06/31/1999 7:30	06/31/1988 9:30	21:11 0001/15/00	06/21/1999 13:30	04/01/1989 7:30	06/01/1008 12:30	06.7 9991/20040	06/02/1598 9:30	04/02/1999 11:20	00:01 8881/00/00	06/03/18/8 13:30	DE: 7 888 1'300	0E/04/1999 6:45	00.01.000.13.00	06.7 8887/80/80	06/06/1999 11:30	DESCRIPTIONS 7-50		W. 11 4841/2040	00.01.000.07.000	or:7 600 Calculator	DECEMBER 13.00	A. 7 1000 7 10	04.08/1996 10:40	04.09/1999 17:45	06.58 19.30	DE-7 888 F-01-00	24:E1 0041701700	7 8891711780	04/11/1999 A:46	DEAT 1/1 1999 12:35	06/12/1969 7:30	00:01 999 1/21/80	06/13/1999 8:30	06/13/1998 11:00	06:14/14/06 7:30	Servertible 9	00:11:00	A 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	04/15/1999 13:30	7.0001701700	06:16/12/12/120	11 888 11	Nevre/1999 13.15	7 8881/21/200	1 0001/21/200	06.7 8891/87/30	05-6 6941/21/20	UNIVERS TO	OE/11/1998 12:45	00:7 9981/81/90	06:19:1959 10:30	7 686 1/02/10	04/20/1898 11:05	D6/21/1995. 7.
	⊢	_			-															_				_			_					-								-		_				_				-					-		-
	944 (17979	5		154 mg	S .	Men 6/3 1/36	Twe Crin	Tee Sy	West 6/2/98	Š	Med 0.7/10		The extrem	F4 6/4/8	F4 8438	E-I SAZO	Per CANE					200	1-400				West Colors		The 6/10/96	Thu 67078	Fri days sales	F4 6/11/86	Feeting	Sat 8/1 2/90	Sed 6/12/	Sun Eritm	Stan Eri 3	5	Mon Erity	Non Co. Los	Tue contract	Tue	Wed 6/16	Mad 47 and	Mad Sylvan		Thu Avi 7.00	Day 6/17/86	Pri 671578	F4 61678	FECTOR	FA CYLENS	Set 6/19/98	Sat 6/19/99	Sun 6/20/99	Sun 6/20/99	Mon 6.71.
			_								_					_								_			_							_						_						_		_					_	_	_		-
i	i																																																								

(de sept)	,				_		_	_	_	_	_	_	_			_				_		•				_	_	-	9	·	-				, ,											4		_				_			
Sang.	*	= !			=	=	=	=	•	=	=	-		: :			: :	-	* *	8	=	ě	•	ţ.	ţ	2	2		<u>.</u>		8	•		2	_	-		<u>•</u>	•	2	<u> </u>	= :	2 9					2	Ş	2	=	19	<u>-</u>	<u>.</u>	
(and) Title	5.71	57	. 5	\$ 71	5.7	\$ 71	5.1	5 71	571	571	571	57.	22	5	; ;	; ;		27		5.3	571	5.71	5.71	5.71	\$ 7.1	5.7	5.7	571	5.71	5.71	571	5.71	5.7	5 5		5 71	571	5.71	\$ 23	5.2	5.71	5 5			5.73	5.71	5.71	5.75	2.5	5 71	5 71	5.71	ŗ	571.	
Permendilly Competest tot Temperature Effects (girl/pet)	2.24	9 :	: :	5.20	531	5 24	8	25	533	2.4	5.73	200	<b>3</b>	8 5	2 5		; ;	: :	5 12	5.29	2 40	5 33	91.5	5 76	8	5 20	5.23	5 16	<b>7</b> 80	67.4	\$	\$14	2	9 5	527	472	\$	\$27	215	4 65	4 6	R :		2 5	55	6.28	8	23	5.73	5.87	5 63	5 73	15.5	5.38	546
(solving) (processed	50.0	/50		-	9 09	\$	3	89 8	:	-	99 0	# ·	25 9	2 :	:				808	1	9 49	9	5 5	30	2 86	3	9.59	5.05	5.77	5 52	5.11	<u>.</u>	878	8 5	41.9	3	35		\$ 03	\$ 50	25 25	2		5 9	7.33	7.33	133	5	9	899	9	6 46	97.9	6.35	· ·
(pod)	90 0	2 1		8	308	886	2 80	2 80	8	3 05	2 80	9 2	20 1	2 2	2 5	3 8		ž	309	202	2 30	305	7	3.14	3.19	308	6	314	324	939	324	Sac.	3	1 6	305	344	3.	305	8	333	e i	RD .			1 15	2 55	2 55	2 30	2 80	2 80	2 75	2 90	2.85	ž	305
•	maint cleaning					-	maari claaming			increase back prite pressure to 6 9 and 7.0									many channed		-				markt cleaning					many closury						change OUR procedure (prior data incorrect)	many channing						Suppressor suggests							mand channing					
(unu) Assumbary ag	2 :	2 :	? \$		\$	5	2	2	2	01	õ	2	2 1	2 :	? 9	? \$	? 5	. 9	9	ē	5	5	5	9	9	9	ë	2	2	5	9	9	2 :	2 5	- 2	\$	Ş	ç	2	٥	5	2 :	2 5	? \$	2	01	ř	2	2	2	5	0	ē	01	- P
(see) Durantion (sec)	15.00	8 8		8	8	15 8	8	15.00	15 00	5 88	ŝ.	ž 8	8 5	B 8	3 5	3 8	2	9	15.00	15 00	15.00	15 00	15 00	15 00	15.00	5 00	5.00	8	8	8	ž.	8	8	8 8	8 8	8	8	15 8	1580	158	8	8 8	3 8	3 8	8	85	85	5 80	15 00	15 00	15 00	15 00	5 8	15 00	8 8
nt) 48 some american's (gri	= :	: :	; ;	4.7	Ş	;	7	Ŧ		;	35	·	: :	; ;	; ;	: :	; ;		Ç	5	4	<b>‡</b>	7	*	÷	7	:	÷	7	25	;	÷	9		; ;	:	3	4.7	5	23	25	: :	; ;	: :	\$	- 27	÷	÷	;	7.5	4.2	2	5.2	6	<u>.</u>
استون الماء على الآل (1949)	2 :	::					<b>40</b>	3	\$	\$	8 8	\$			: :	, ,	; ;			2.0	5	9	5	\$	9	7.0	ø	œ	<b>19</b>		٥,	•	5	D 1	; 5	:		o.	:	6.7	2	D :				89	29	6.7	è	ŝ	59	8.9	8.9	•	<b>8</b> 6
Ares 7 970 m cook 98 (ares)	13.0		2 2	0.0	000	9	(30	130	5	17.0	•	0	= :	•	:	:	:		•	061	180	180	180	981	9.	•	5	9	<b>8</b>	9		9				180	•	180	•		<u>=</u>		:				9	2	2	•	0.81	9		°	
(loq) onessert 40	<b>8</b>		: :	7	3.6	80	#	3.6	38	40	•	1.0	0, 1	• :		, ,	: :	: :	- 7	1.2	2.0	70	7		7.0	٠,	2.0	;	:	7.2	7.2	:	2.0	٤:	: 2	72	7.	7.1		7.3	7.3			2 2	7	7	7.2	7.3	7.3	7.3	7.2	7.9	2.5	7.2	7.3
ni) ma esched smuuseV (B [†] 1	630	8 8		27	00:9	630	\$ 70	5.70	420	8 20	5.70	8.70	2 80	9 5	2 6		2 5	2	90	\$ 30	280	0.20	8 40	6.40	9 20	6.20	0.0	9 40	2	ŝ	8	6 20	7.20	2 2	620	8,	7.00	B 20	£ 30	0.50	8	9 1	8 5		\$ 20	5.20	5.20	8	9	5.70	5 80	9 30	8	8	\$ 20
enched shaft steamer?	\$ :			÷	9	•	9	¥7	·	6.5	5 9	\$	9	9	, 4	, ,	, ,		. 6	9	6	15	6.5	40	9	\$	9.9	5.9	88	92	8	5 9	\$ :	6 6	9 6	9	8	8.8	5.9	\$	\$	:						9	59	9	\$	5	9 2	8.5	5 5 9
notiniconizefi esemeli (mqg) sinfi	5 ;	ā 2	: 3	a	25	25	2	25	5	2	a	æ	× :	2 5	: 5	2	: 5		\$	ş	\$	\$	5	5	8	3	s	8	8	8	8	ŝ	s :	R S	8	8	8	\$	8	9	9	: :	2 5	1	- 54	5:	8	\$	*	\$	25	ş	\$	\$	<b>\$</b> \$
(erto) NA temperated	9 5	9 9	ě	8	0.29	9	ŝ	8	ĝ	ŝ	ĝ	9	2	2 :	; ;			0.19	3	8	9	9	6.0	610	909	9	009	6	ŝ	95.0	9	280	629	620	8	0 29	610	610	5	530	8	2 3	9	3 9	82.0	019	009	ŝ	630	62.0	610	62.0	620	629	610
(was) WS NA	æ :	۶ ۶	8	2	2	2	z	52	52	\$2	33	52	¢ ;	e :	. x	: x	: *	Ý	. \$2	ĸ	\$2	52	58	58	52	25	52	22	52	52	52	52	£ :	8 8	3 8	32	52	52	ĸ	X,	× :	Ç ;	G K	: ×	52	: 12	8	52	25	52	38	\$2	×	25	3 32
(2 soengeb) WS gene?	s ;	£ £		Ħ	30.5	<b>F</b>	×	25	5	22.5	5	35	26	ę :	, ,	2	1 2		. #	35	32.5	ā	ā	5	æ	26	32.5	5	3	3.5	Ħ	35 2	8	; ;	3.5	F	315	3+5	35	ŝ	8	<b>á</b> :	- ×		'n	- =	<b>.</b> E	. R	8	30 8	e: E	g.	ē	n	3 22
(mqg) atmacali kee-i	2		300	20	27.0	280	28.0	27.0	280	27.0	280	280	27.0	2 2		_		2	. 82	27.0	28.0	27.0	982	962	982	210	200	27.0	2	28.0	27.0	98	500	E :	380	210	28.0	28.0	27.0	38.0	22	6 1	2 1		22	580	92	23 0	240	280	260	280	24.0	6	78.0
nezhalot etaeurre' (gal)	7 1000001	TOTAL	1374218.0	1376285 2	13629224	136361	1383784 2	1364606 0	1391160	13932264	1308418	1398954 9	3001040	3398888	0 00000	4147600	416740	142.6355	1423755 1	1423986.0	14246621	14313355	14397252	1439725.2	14404761	14407014	14414554	14481712	1448848 7	1456527.4	14567139	25814	1464487	1465934	1473504 9	1480569 1	1481155 6	14812259	1462618 5	146894 6	1490878	1487189	2000/601	2 Facet	1505219 6	1505657 1	1506289 0	1507037 2	15117199	1512031 5	1513231 5	1519228 4	1520826 0	1526498 9	1526596.4
Eniberry sateble second	8278.4		9	Pact 3	\$423.7	8428	87583	8478	1	BM52 6	87.78	Ē	1		1 10		9.00	2	175	\$245	85472	8568 7	8576.2	8568	15917	8582 5	3 MSB	8613.5	8418.5	0 /036	7 70	200	000		966	8706 4	8708.0	8708.5	87124	87310	8736 5	9	27582	2 6 6	87783	1,6778	8781 S	7 (3)	8797.4	1987	1902 2	1618	88239	9845	89483
Commission Operating (cnf) andT	2863.08	200	2904.83	2910 58	20.29 00	2931 08	2832 33	2934 58	2952 83	2958 58	2077 58	2979 08	2880 3	2862 50	2000	900	1004.04	90	3051 08	1052 58	3054 58	3073 08	3079 08	3087 06	3094.08	3100 58	3102 56	312158	3126 59	3145 08	314741	3150 58	3168 58	80 00 00	3195 58	3215 83	3217 50	3218 58	3222 58	3241 08	3246 50	2000	1268 58	3274 74	3789 08	1292 58	3294 €	3296 58	3313 08	3314 83	3318 54	3335 83	3340.33	3362 08	3364 58
(mer.nd) envit	9 30 AM	100	10.0	26 Pag	7.30 AM	8:30 AM	10 45 AM	M4 00 I	7 15 AM	1 00 PM	1 00 ALL	\$ 30 VIII	W 50 50	8	8	74	14 00.00	NV S	9.10 AM	11 00 AM	1 00 PM	7 30 AM	1 30 PM	7.30 AM	9.30 AM	11 00 AM	1 00 PM	8 00 AM	1-00 PM	7.30 AM	N 05 0	8	700 V	200	10 00 AM	8 15 AM	7 SS AM	MV 00 6	M 200 1	7 30 AM	8		3 2 2	7000	7.30 AIM	11 00 AM	12 50 PW	3000	av or c	B 15 AM	Md 00 4	6 15 AM	10 45 AM	R.30 AM	11 D0 AM
						_	_	_												_	_			_		-					_	_		-	_						_	_	-	-		_	_	-	_		_		_		
****	06/21/1988 9:30	0021/1900 11:00	04/22/1988 7:16	06/22/1888 13:00	04/13/1940	04/23/1999 9:30	04/23/1898 10:45	06/23/1898 13:00	0424/1998 7:15	04/24/1969 15:00	06/25/1888 8-00	04/21/1999 9:30	04/15/18/8 10:45	000000000000000000000000000000000000000	000000000000000000000000000000000000000	Ce. 7711000 8.00	A 11 10 10 10 10 10 10	OLCHARATE T. IO	04/28/1999 1 30	06/28/1999 11:00	06/26/1998 13:00	DC:7 8981/95/20	OE:21 B881/82/90	OC.1 884 F30-30	06/30/1999 9:30	06/30/1898 11:00	06/30/1998 13:00	07/01/1999 E:00	07/01/19 <b>09</b> 13:00	07/02/1988 7:30	07/02/1988 1-50	07/02/18 <b>18</b> 11:00	07/02/1998 7:00	DE IL BERTADATO	97704/1989 10:00	81:39 4:15	07/05/1999 7-55	07/05/1988 8:00	07/05/1969 13:00	07/06/1999 7:30	07/00/1969 13:00	0.7 898 77070	OTHER DESIGNATIONS	00.11.000177070	02.7 88613670	07/06/1999 11 00	07/06/1998 12:50	07/04/1998 15:00	07/09/1999 7.30	07/04/1999 9:15	07709/1999 13:00	81 9 66 12	07/10/1999 10 4S	07/11/1969 1-30	07/11/1990 11:00
<b>4</b> -0	Men 4/21/88		Tue 6/22/20	Tue 6/22/10	West 6/23/88	Wed 6/23/86	Wed 6/23/99	Wed 6/23/88	Thu arrange	Thu 6/24/90	Fri 8/26/88	Fri tersens	F4 47.54	14 6250			- CO - CO - CO - CO - CO - CO - CO - CO	Man 42 108	Mon 4/2 UVE	Men 4/28/99	Mon 6/2 8/96	Tue 6/29/98	Tue 6/29/98	MADES POM	Wed 6/30/98	Med 6/30/19	West 6/30/98	Thu 7/1/98	Thu 771/98	Frt 772/90	Fr 70/m	Frt 70/FF	Set 7/3/04	2017.00	Burn 7/4/78	Mon 7/5/Es	Mon 7/5/98	Man 7/5/99	Mon 7/5/89	Tue 2/6/99	Tue 7/4/52	111111111111111111111111111111111111111			Thu 7/8/99	The 7/8/79	The Patron	Thu 7/8/90	Fri 75499	Fri 7/8/9#	Fet 7,509	Set 7/10/96	Set 7/10/90	8us 7/1 t/38	Sun 7/11/99

Page 7 of 13

Page 8 of 13

Lag Angy) (pall) Maja	:		_			_	-		-							•	_	_		-	_				•	•	_ •	-	_	_	 =		-	_	-	•	**		-	E 0.		9.0	_					-	-		<u>.</u>		_	-	_	_	•	-		_			
	_		_	•	=	-	=		_	-	-	-	-	_	-	-	-	-	_	-	-	_	-	 	<u>-</u>	-	_	_	ē 	-	# 		E .	E	-	-	_	-	_	_		_	<u> </u>	e ;	, ; 	-	-		_		_	_	-	_	-E	- 8	-	_	-	_	_	_	
(md) 7mi	12.8	5.7			7.5	2.5	571	57.5		-			<u>.</u>		- 57	- 5	-	-\$	5.7	- 22	-		2		<u>.</u>	57	-	57.	386	391	- 3	5.71	5.7	386	391	571	577	- 57	5.73	57.5	- 52	57	- ·	- 57		-	_	_	2		- 57	<del>-</del> -	571	673	4 12	-	571	5.71	- 5		_		
Parmenhility Corrects for Temperature Ellente (gittipes)	\$ 12	\$31	• —	2	8 5	\$67	528	\$ 60	75		3	3	6 20	\$ \$	287	252	8	989	*	5	3	* .	ğ.	233	£	515	217	215	375	2.88	5 76	* 65	99 *	283	2 68	4 23	•	4 16	386	124	*	\$	303	5	328	200		2	5	2	385	15.2	312	0E <b>7</b>	2 79	2 33	328	2 93	5	3 5	-	328	
Hedding y Marketing	8	\$	2	:	3	?	:	3	3	:			E	\$ 	:	ž	\$	3	3			:	2	:	908	:	<b>8</b> 24	509	\$	7	133	*	3	337	324	135	4.95	4.76	59.	4 95	476	236	98		2.5	ì	: :	) e	<u> </u>	5	ē	8	3 29	208	330	282	373	363	9	; ;	3 5	2 2	_
(log) 467)	80.	ğ	2	g E	2	82	8	2.80	8	2	5	8	2 55	2	8	90 5	280	2 80	7 80			3	8	6	338	305	9	8	624	96	62.8	5	3	8 20	\$ 45	378	3.78	383	Ş	378	3 93	?	7.47	5	, 22		, ,	•	-		è	ž	\$21	3.58	7.85	818	10.5	5 7 6	, ,			\$0.5	_
<del>4/4</del>			Cultural Comment								Stantas Linu				_			mount channers							makeni cindering				marassi to 9 6 gpm @ 8 00 AM		reduce biologeasure to 3 8 and 3 9	maint cleaning	increase to 9 5 gpm ig 8 50 AM		_							mant cleaning	recease to 9 5 gpm at 10 AM		Acresse to 9 5 gpm at 6 PM	_		Company Communication	increase to 6 ppm at h PM			Workship 5 govern 8 AM	mant clearing		Increase to R 5 gpm at 6 PW							Contract Character	
(upu) Loueste (upu)	٩	•	•	2	2	<u>•</u>	2	•	2	: :	2 :	2	<u>.</u>	•	<u> </u>	2	2	2	2	9	: :	2	<u>•</u>	2	2	ē.	õ	9	2	2	ā	ç	•	<u>.</u>	9	9	٥	2	ē	10	9	2	٠	9 :	2	2 5	2 5	2	2	2	5	2	õ	2	ē	01	5	2	- 5		2 9	2	
(see) Durgition (sec)	8 54	58	8	8	8	8	15 8	5.00	851	3 5	8 :	8	8	8	8	6.8	15.00	8	8 52	8	3 8	3	8	8	8	9	5 00	28	5 00	15.00	5 30	8 5	25.00	5.00	8 51	8 5	8	8	8 51	8 5	15.00	8 00	8	8 5	8 :	3 8	3 8	8	8	8	8	8	15.00	15.30	8 8	8 5 8	15.00	15.00	2	3 2	3 5	8 9	
15+1 Leg anger secondes,	=	2	=	2	82	-	5.7	53	;	::	3	6	25	2	8	8	25	25	5				2	'n	2,	6	s,	**	12.5	16.5	9	:	6,	182	17.2	7.2	7.2	5	7.2	7.5	7.5	:	162	7.7	<u>.</u>	} ;	: :	2	2	2		17.7	4	2	15.7	17.7	6	8 5	: :	: ;		. 8	_
46 wife size Name (	=	4.	:	•		•	•	•	:	: :	:		è	2	:	8	67	2	•		: :	•	•	•	6.8	9	89	89	:	=	ş :	• •	0.	**	10	89	:	*	•	4	•	8.9	<u>•</u>		=	: :	: :	•	9	2	9	5	65	69	110	10.5		9		3 :	: :		
Anni 920 in con 98 (Thors)	•	•	•	•	•	•	9	180	180	; ;			<u>e</u>	•	9	ê	180	9	•	1 1		2	2	9	90	2	9	•	8		180	130	12.0	130	130	13.0	130	130	130	130	130	130	130	130	90	2 5	2 5		9	2	50	130	130	130	130	130	130	13.0		:		2 02	
(bed) exertence (bed)	:	7.5	s. _	<u>.</u>	:	:	•		7.4	: ;	. :		:	:	7.3	13	7.3		7.3	: :	: :	:	m.	: :			2	2	<u>.</u>	ř.			36	ş	÷	;	:	;	7	÷	;	05	÷	÷ :	÷ :	: :	: :	•	-	;	÷	6	6	20	÷	ş	6.	÷	•	; ;	; ;	•	
ni) ⁴⁸ enebod eniwasiy (g/s	8	P		8	5.70	8	3	8	8	; ;	3		8 5	570	8	8 20	5.70	5 70	5.0	5		2	9	8 20	8	ŝ	9	6.30	15.30	16.20	9	7.10	7.10	16.70	17.39	7.70	7.70	8	120	7.70	8	7.10	15.20	9.50	2	2 5	2 5	0.0	2	2	<u>0</u>	16.83	10 60	7.50	15 00	18 70	0.00	2	5	3 5	2 5	8 9	
proted dail casemer (mqg) TE	9	\$		:	<b>S</b>	ş	50	9	9	: :	: :		•	5	5 9	ş	59	\$	•	: :	, ,	:	9	so 10	5	9	9	<b>.</b>	*	5	6 2	9	· •	*	5 6	9	29	59	6.5	59	59	9	S	· ·	s :	£ ;	: :	\$	<u>.</u>	5	9.	un <b>80</b>	\$	8	8	•	9	9	*	; ;	. 4	: :	_
holiminorized pasmoili (mag) shall		8	; ~		8	58	2	8	4	: :	;		•	•	\$	3	=	ŧ	#	•	1 9	;	<b>=</b>	<b>\$</b>	2	7	<b>\$</b>	•	•	÷	\$	\$	•	•	47	÷	\$	=	٠	4	\$	8	•	ę :	•	* \$	: :	•	*	•	7	<b></b>	\$	*	*	7	9	\$		: :		;	
mis) the branching	8	920	ê	8	\$	ê	30.0	61.0	810	: :		À	ê	Š	ŝ	0 85	006	009	9	6	3 5	2	·	620	ŝ	00	ŝ	62.0	92.0	5	og Og	0.29	620	9	009	62.0	919	620	9	850	90 0	0.40	900	920	62	8 :		ĝ	9	8	620	0.65	619	ŝ	2	63.0	623	930	á	3 3	-	2 5	
(mda) WS 44	*	\$	к —	*	23	82	8	23	×	: :	s :	2	×.	£	\$2	\$2	52	٤.	25	. *	2 %	5	r:	r.	S.	×.	ĸ	£	¥)	ĸ	52	£	22	83	52	52	23	×	82	52	52	52	8	۶ :	ε .	٤ ٧	· ;	2	۰	e 	52	10	52	×	10	\$2	52	52	, ×	9 7	r #	: K	
(canb <b>53</b> , (40 lives (c)	æ	30.5	£	PF .	Ř	×	33.5	5	p	3 1	3 ;	F3	æ	25	8	31.5	5	g	4		? ;	; _	3,	F.	316	75.4	8	я —	2	32.5	8	E	315	32.4	8	3	87	30,7	32.5	3 17 2	भ	325	8	36	<del>,</del>	ŝ		Fi	32.5	PI	ŝ	32	E	22	æ	8	30.5	ä	: s	2 5	4 8	2 2	
(mage) attracted book	_	:	_	5E0	20	ŝ	280	_		_	_	_	<u>.</u>	27.0	380	360	280		_	_			9e	28.2	380		_	_	28.0	280	27.0	29.0	27.0	280	_	280	_	_	240	27.0	280	28.0	380	_	_		_	280	_	_	_	_	26.0	280		280			, ¥	_	_	2 8	
Torresse Totalizer Personne (pm)	1725130	1728988.4	172	730158	173071	1736878	17387213	17455343	1746708 9		ASSESSED	17471	125704	1025201	17602511	1781758	17681611	17647238	1768945 0	1 769640	1776308	20000	1778764	178482	1785682	1785919 6	17866456	1793284 6	1793478 2	1795109 0	1796062 6	1802867	1803089	1804336.8	1805306	1811805 5	18131876	18205402	1622361 5	1828424	1830336.2	14250466.7	18317468	957858	142388152			1829308	2	1820286	1857429 6	1,66004.3 5	186601	1866853 5	18671338	18683384	1875097 5	187770 \$	1884001.2		0 000	1893347.6	
golbtell Metall work	7 RSPG	\$4103	2			EMA MAG	Ī	25.5	9			2	9478	0462 2	Š	8206	9528 3	9528.2	9529	8	9	į	9226	95730	9575.5	95763	95783	82868	95973	9600 3	9602 1	96203	96212	96234	96252	96429	9646.7	96670	\$421	9661 9	98839	2 198	9696	97148	9715	200		97412	97418	0.20	9762 3	9768	97861	97862	9796.6	97867	9804.5	91189	9820		3	9855.5	
Communicative Operating	391606	3636.54	20 000		25 24 25 26 26 26 26 26 26 26 26 26 26 26 26 26	3960 58	3966 58	3985 08	3087.08		20 page	200	R9 <b>6</b> 00 <b>7</b>	4613 08	4032.58	4036 83	4057.08	4029 08	4060 58	87 C9UT	4000	2000	4087 58	41.04 SB	4107 04	45 BO 17	4110 58	4128 SH	4129.58	413258	4 26	415283	4154 33	415.6 53	4158 33	4175 09	1179 83	4200 08	4204 58	4225 DB	4227 08	4228 33	4230.58	424858	4249 58	5 5	10 7 7 7	427508	4275 33	£278.58	4236 83	F305	4379 58	4323 88	4324 98	4326 25	4344 08	4351 08	1 358 5.0	9 1	90300	4.395 OA	
(refer: std) send?	12.30 PM	7.00 AM	3	2	8	700 AM	3 00 PM	7 30 AM	MA OF 8		3	8	30.44	11 30 AM	700 /	13.8M	7 30 444	930 AM	18 8	100			- Mad 00 2	N 00 .	30.44	1 00 VM	7 60	7 90 AM	A 00 A AA	13 00 AM	M 00	7 15 AM	8 45 AM	MY 00 1:	12 45 PM	6 30 AM	10 15 AM	6 30 AM	1 00 10	7 30 AM	N 30 AW	10 45 AM	M-001	7 00 AM	W (8)	3		# G	W 545	8	7 15 AM	8 18	28 AL	13 00 AM	10.30 AM	12 40 PM	6 30 AM	30 95	200		1000	7 V	
9460	┢	_	-		_	09:14 886 1:50 09:14 886 1:50	00:01 0001/30/00		_	_	_	-	-	_		04/04/1999 11:15	DE/08/1999 7:30	OE-0 666 LBOYBO		_	_	_		DE/17/1888 7-00	_	-	_	_	_	00 11 4441/21/90	_		_	_				04757796				_	00:11.0001791400	_	_	08/1//1986 13:00	-	_	_	_	04/19/1999 7:15	00.Cr 899 1/41/20	-	04/20/1999 10:00		04/20/1999 12:40	06.30 444 17700	06/21/1999 13:30		_	_	08/23/1998 9:30	
***d	Two brams	West States			MAY O POM	Thu effre	The britis	Fet Britis	Eri Balansa				Set 80.00	1 a 17770	Sun MAN	Sun traves	Mon avega	Men GARGE	Mar 25.00		100000		Tes 67076	#4 67 1/3e	SEVILLE PRIM	Med art y/Je	24/1/2 Pa/A	Thu B/12/99	Thu 8/12/99	Thu Brigibe	Thu 6/12/86	FH 673/09	Fri 4/12/20	Fri Britine	Fri 6/13/98	Sed B/14/70	Set G1478	Sun 875/98	Sun 8/15/98	Mon 674/he	Men Critina	Mon S/14/79	Mon Miche	Tue 6/17/80	Tun 0/17/00	Total Ball Tyles		*** 5150			Thu Minns	The Milana	Fri g/20/19	Frt actives	Fri satovin	Fe actors	Set 8/21/70	Sec 8.21799		100 mar	1777	1000	
Proce Bridge																													•	•	•			•	•								•	,	-	•			•	•		-			•	-							

400	3	_		-		_	_	_	_	_			Fri &Z7/96 06	_	_		_	_	Men 6/30/16	_		_	_		-	_		_			_		_	_		_	_		_	_			En Stroves	_		_	Bun 9/12/99 DM	-		_		Mon 9/13/99 09	_			
****		DWZ3/1000 13 00	_	-	A CONTRACTOR	-	_	_	-	_		0a/27/10m6 4:45		00:3 884 1/32/80	_		_	_		00.7 8001/1500				09/02/1988 13:00		-	_	_	-		_		-	000001990 0:30	-		_	_	_		and and	_	08/10/1899 8:35	-	_	_		_						_	1 50:11 66813/100	_
(nintral) and(t	11:00 AM	8 9			2 2	2	8	8	15 4	1.00 PM	7 30 AM	100 548	1 00 PM	M-30 AM	₩ 80 F	8 30 AM	NA OE 01	7.00 AM	7 30 AM	300		M. 00	20 AM	1 00 PM	B DD AM	9 30 AM	11 00 11	12 45 PM	7 00 AM	10-00 AM	400 V	10 00 41	8	M 00 01	8	7 40 AM	# 00 PM	715 44	MY 57 W	12 45 PM	100	1 1 2 1 1	8.35 AM	700	7.00 AM	MY 00:11	6 30 AW	11 00 484	7 40 AM	9 30 AM	11 00 AM	12 45 PM	7 IS AM	9 30 AM	11 05 AM	12 45 PM
goldensegO septimical (end) semil	4300 Sg	23.00.7				3	1	2	2	44 70 58	BO 08**	4490 33	4 W S	4514.08	4516 58	4534 08	4540 08	4560 SB	45.61 OR	8 5	100	000	45.58	4587.08	4606.08	4607 58	4609 of	4610 83	4629 08	4632 08	465L 08	1658 08	101/0	46/8 28	468100	470175	4707 08	4725 33	4726 83	473083		200	4774 66	4767 08	4797 08	1987	482058	4825 08	4845 75	4847 58	4849 08	4850 83	4869 33	4871 58	4873 15	4874 83
gelined toldi mili	1996					7064	8	800	9623.8	30296	8	, mag	6 2500	90776	1 5260	7	8 1000	* k1001			7700	100243	10042 8	100483	100673	10064	10000	10071 4	6 8800 1	100927	101	101180	101377	10130	10143 6	(0)817	0.0101	101852	101861	101901	9000	10033	10233.2	1 (523) 7	102558	10260 3	102792	102837	10304.3	2 90001	10001	1 0308 5	10327.3	10329 5	19336.1	10332 8
State T alest grade (Ing.) grade and	18 864 8	9 9 7 9 9		T TOTAL OF			10103650		1917BG	1919945 1	1928842 4	1926768 9	1928342 4	1935467 3	1936345 9	1940127 1	19442201	1951462 4			000000	1952341.5	19588150	1960899 6	1967593.8	1968134 5	1963363 5	1968939 B	1975351 4	18784581	1984509 3	6 / P95461	982818	19933194	0047884	2001219 6	2 1600002	20085215	2004749.8	20111689	2010000	20084150	20263523.8	2027889 9	50342839	2038865.3	2042503 8	2044097.5	20513621	20520184	2052243 9	2052275 5	20593887	20601841	2060739 1	2051319.9
(mqg) stansoff boo'	e i	8 3	:					38	260	280	27.0	240	0.42			280	280	53.0		-		27.0	27.0	980	240	280	280	27.0	200	27.0	280	980	24.0	27.0		98	260					9 5	280	27.0	280	240				560	280	27.0	. 2	280	270	26.0
(2 moston) WZ speed	R :	F 5		* ;	ê i	ñ		×	20.	Ħ	- F	315	32 5	33	B	ñ	7			ş	2 2	7 2	300	32.5	8	ñ	æ		5	×	35	R	8	9 9	, F	. 8	30.5	8	30.5	ē ;	<u> </u>	9 8		35	<u> </u>	a	30.5		=	÷	33	32.5	305		3.5	2
(uuto) WZ MA	×.	× 1	0 :	c :	0 :	2	κ .	æ	×S.	ĸ	52	κ	25	\$2	52	ĸ	r.	٤.	_	<u>.</u>	0 K	: r	\$2	32	æ	۲.	71,	- 52	25	71,	52	52	R.	\$ 5	: *	. 2	ĸ	52	52	ς,	ς ;	C 1	12	52	×	52	×	52	52	я	Е	2	×	52	52	32
als) AA ist <del>nomeriya</del> Ak (ch	029	\$ \$		2	2	0 2	°		2	÷	930	<b>\$</b> 2.0	0	0.29	62.0	0 23	019	630			3 5		ŝ	019	059	0.29	0.29	950	620	0.0	0	0.5	o :	9 5		630	029	ŝ	0 2	0.0	2 2	3 2	039	009	620	0 09	0.29	0 69	0 29	0 1	010	0 00	e2 0	62.0	610	007
offshranicaft semmoid (mag) ess.f.		• :	•	. ;		÷		7	7	•	4	÷	7	÷	=	<b>\$</b>	=	÷				. \$	•	*	*	7	•	•	•	•	•	\$	2		: 5		•	ŧ	*	ę :		: :	: :	4	2	=		=		•	•	<b>\$</b>	\$	8	я	9
nched skill gleografi (mgg) Til	<del> </del>	_		2 ;						_				_	5		S	_					\$	_	÷	59	 9	6.5			_	<b>S</b>		S 4					_	2					_		_			_			9	•	· ·	- 1
f) 48 anohod wowen's (p/4	9.70		_		8 :	2.2	_	_		_	1300	1 20		8	8 :			29 62			2 5		230	_	8	3.70	3.20	320	3.20	320	200	330		9 6		_			_	2 :	2 9		_	3.0	310		_	330	330			320	3.20	930	330	92.0
DP Presence (pel)	-	_	•	_	-	06	-	_		_	-			_	- 6+	_	- 05	_			- :	3.8	_	3.6	-	39	÷	=  -	- 12	₽ 	# 		_		_	_	- 13	_	- 42	2 1	. :	; ;		_	42 13		_	_				_	- 13	-	- 27	-
(analy)	-	000	-				_		_	_			130 6.9	_	_		•					000	_		10	_	_	30 6	130 68	_		_		9 9	_		_	_	_	130 67	-	_	_	.0	- 08	90 - 08		- 01		96		9 061	10 67	_	10	
(men)	-	-	_	_	_	_	_	•	_	_			_	_	_	-	_	_				_			22	-			_		_	_	_	-	_		_				_			32	-	_		33	_	_	_	32	_	-	3.5	-
(see) moternió 48	-		3 :	-	3 1	-	_		_	8 8		_			-		_	8 8 8		-		98	_		15.00		_		8 8		-				2 2		_		15.8		3 8			95.5			_	_		_	-	_	_	15.00	_	-
(nin) Yacamper (nin)	L	_					_			_					_		•	•		-		2	9	₽	5	9	_		5	_			_	2 :			_			9 ;		_	_	_	_	_	_	_	_	_		2	9	ē	0	9
					-	Current Charles	_	-14	_	_	rrugest cleaning		_					just prior to full lank soak and flux test	begin full tank south and flux test	and flat tank soak and flux lest		_												mark meaning				maint cleaning				country server			_					granted plant			_	reading before CST lest	reading before CST tast	reading before C.S.T. fact
(pod) 4991	Ę.	-	-	-		ž	- 25	-	5.7	- 87	- -	25	- 55	5	, e	7.23		<u> </u>	_	-		-	=	-	-	-			-		-	-	-		-	-	-	15	-	25	3 .	ă i.	-	-	15		- 3	- 3	-	- 1	-			39	19	-
ndpy8) Aggreens	3.83			_		_				326		•				1 257	_			_		2			10.58	_		_		2 			_	2 2					_		_	2 5		_	_		_	_		_			_		= ~	_
Permembility Connection for Temperature Effects (globped)	9.	<b>8</b> 8		-	6	8	8	<b>9</b>	<b>2</b>	2 78	ž	582	2 82	5 B6	2.78	2 23	236	5 20	_	18.76	2 87		2		928	_	_			_	_	\$ 2	_		_	_	10 78	_		_	2			_	98 01	10.16		-	_	_	67.6			10 01	_	_
		5 5		-		5	- 2		5.7	571	- 57	5 71	571	5.75	571	57		571			-	\$ 2.5	5.71	571	571	5.73	- 57	571	17.0	57		_	_			57.	571	573	5.7	5.			. 25	5 7.1	5 71	571	5.7	5.71	577	- \$	- 57	 		_	6.7	_
	1				_			_			_				_																																									

elonome	une of the er 150 PM to make me		1 air to membrane lank, 10 s											mary clashing		high vacuum alarm			Taile channe								gavesio tries	American State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of State of Sta	minated Date work on a me and			end of peak liber systeng at 2 Ptu		many classing	rd peak flow testing at 10 4		end peak flow testing at 2 PM			The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s	And a second discount.							Control of Sp. 114 days and and and another special	om werklion tank MLSS to 6	usal ian imm 12 45 to 3 30 FM only		Starting unit at 12 40 PM	normal flow and full serator	
Fradesiny (min.)	0 20	2 :	01 01 10 10 10 10 10 10 10 10 10 10 10 1	2	9	9	01			2 2	2		2	2	•	•	-	2 5		-			. 2	2	0	2	0	9 9		. 5	. 0	9	9	ē	ē	2	0.	-	0 :	2 :			2 2		2 :	_	2 :	H	_	•	?	01	ò	- 01
(see) noterned %			8 8	15.00	8 8	8 8	98	8 8	8 8	8 52	8	98	1500	9 5	8	8 8	8 8	8 8	8 8	3 5	8 5	8	8 5	20 51	15.00	15.00	8	8 8	8 8	8 8	15.00	15.00	15.00	- 80 Si	00 51	989	- P0 G	8	9 :	3 8	3 8	8	3 8	3 8	3 :	8	8 8	8	8 :	8 8	3	98	. o si	15.00
(B)	┼		: 2	_				_			_		_		_			• •	_						_					_				23			_		2 1						-	_		ł		; ;			3.5	_
in with class of the life		;	70 7	:	20		۰,	. :	. :			67	67	8	eg	12.5	2 5	٠.			v ec			63	6.9	7.0	2				13.0	121	7.2	7.0	69	120	•	0 4 0		-						89	6 6		0.	on (	?	9	- 89	
P bees in City Tank (Sers)	4 3	2	2 20	130	130	0.61	0.61	130	2 :		130	130	130	089	130	130	2 5	9 9	9 2 2	2 :	2 2	: :	130	130	130	13.0	0.5	2 2	2 5	2 2	130	130	130	130	130	130	13.0	000	20	2 3	-		2 6	2 :		90	130		130	961	2	13.0	130	- 012
(leq) students (leg)	<u> </u>		: :	•	÷	Ç	7		: :	: ;	7	÷	ç	<u>د</u>	 \$	Ţ:	: :	•						•	9	÷	÷	ç ;	: :	, 4		÷	ş	ę	E 7	ş.	9	4	· !	; ;	. 4	: ;	. :	: :	 : :	-	÷:	; ;	•	ş :	•		9	- 4
ni) 48 anded anuses (gi		3	£ 5.	250	8	8	2 20	8 5	3 5	5 5	2 80	3 60	578	8	320	15.20	8 5	2 0	8 8		3 9		6 70	09.9	6 30	5.70	2.5	0. 0	. 5	3	2,2	15.20	07.0	99	8	18 20	16.70	7.20	7.20	2 5			2 2	2 5	2	0.0	8 8	2 5	98	9 9	-	2	8	 92
درماده ۱۳ (۲۰۹۹)	,	-	£ £	8.8	\$	5	5	::	::		9.9	\$:9	9	5 9	5 9	5 9	2 :	5		-			- 59	69	9 2	98	S .	\$ 4	0 9	: :		9.6	8.5	- s	5.	5 6		s 9	\$ 1	: :	2 4			n u	n :	 	5	2 :	· ·	v 1			- 50	- -
notiativotinafi essenci (mag) eta:	,	2	3 5	c	ŧ	ŧ	\$	<b>3</b> :	• •		-		ş	25	•	ş :	<b>.</b> :	<b>\$</b> :		: :	; ;	: 5	. \$	29	1	25	\$			, :		ç	9	ş	;	Ş	\$	•	ų į	ę :		. :	2 =	. ;	R :	\$	ţ:	:	7	<b>-</b>	;			\$
ento) sin instrumentation		3	3 3	ŝ	62.0	3	0.00	3 3			0.19	630	0 09	Ş	0 19	ŝ :	2 3	8 8		: :	62.0		3	075	°	2	9	0 0	2 6	2	029	62.0	63.0	ŝ	9	ş	ŝ	630	62.0	2	2 2		2 2		2	630	950		0 40	1 :	i	950	650	9.4
(m12) WX 1L	,	2	2 2	92	ū	8	2	e i	2 5	2 24	32	26	35	Ę.	۲	2		٠ :	~ ;	3 5	2 2	1 12	. 2	2	2	35	35	R 8	6 K	. ×	52	25	52	25	52	52	52	\$2	\$	C :	0 #	2 %	5 X	0 8	2	2	٤ :	3 8	- 32	£ 1	- C	25	52	52
(D eeergeb) WS quie	4 ;	g ·	8 8	R	g	8	E	8 3	4 8	2 8	R	Я	31.5	\$	8	8	á i	£ 1	e é	. 8	2 5	ě	8 2	я	F	R	8	S S	5 2		200	8	Š	8	8	28.5	285	28 2	29.5	Ç ;		2 5	3 8	3 8	g :	33	29.5	,	R	303	=	9	30 8	582
(mgg) amreofit bee	1	-	ž ž		240	0 92	280	2	2	0 %	380	27.0	28.0	976	27.0	0.82	0.62	380	5 2	0.20	280	976	0.02	ĸ	26.0	28.0	28.5	27.0			280	26.0	25.0	280	280	27.0	27.0	260	2	2	0 87		0 22			58.0	280	1		280	9.73	280		38.0
nestinato T vicentire: (mg) gráticos			200002	2069787.4	2070429 1	20788584	2078370 1	20059551	200	2004796	2096268 6	21025512	21044701	21103900	2110608 4	2111901.5	21.22.04	21102968	9197757	21200776	2129524 6	2136564	21371276	21425935	21436135	21506167	21514368	21515830	235250	2150704	2162311 5	2162858.4	21692294	21700901	21,70122 \$	2171428.5	21719604	21783998	21803980	S FERRAL 2	218/12/0	20000	3.02000		220422 3	2208035.2	2213000 5	221.2045.0	22138456	22144269	A 66.75.37	2215938.4	22183040	2222081 5
Bribeen week we			10001	100674	10074.5	10074 \$	10379.2	100489		10424.8	10428 7	104470	10457 \$	10469 7	10470	104742	6/20	7	106182	7 00	105238	108407	9776	10560 2	10563.0	10582 6	9,6	105855	10000	10604.2	106117	106127	10629 9	106323	10632.8	0.55301	106360	106535	106590	2//00/	6//90	7 0036	1071. 7	, , ,	10/236	107287	10748.4	0.0250	107509	107525		10757 3	107583	10774 6
geilanego evimienno: (and) emi	16,2,0		2 7 7 7 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	4898 16	4807 91	1 5 7 5 7 5 7 5 7 5 7 5 7 5 7 5 7 5 7 5	4010 66	101		4996 75	1860 91	91 8567	99 E867	10 9867	5012 41	\$016 DR	201/104	18 5005	90 40 50		5065 91	5080	5087 41	5110.91	511241	5132 18	2.5	5135 56	2 2 2 2 2 3	8 5	16 1915	516291	5130 16	5182 41	5183 66	5185 91	5186.91	5204	5509 61	9776	255	1 1 1 1 1	6255 11		127	5280 41	5300 18	2302	5303 41	5303 41	2000	5307.00	5308 00	\$324.25
(tru:A) maj	7.00 AM		***	1.5 AM		MY 00 B	10-45 AM	7.30 444		1 1	M- 00	7.15 AM	12-45 PM	8 00 AM	7 30 AM	1 10 AM	100	8	12.45 PM		MG 00	77	10 30 AM	10 00 AM	11 30 AM	7 15 AM	30 AM	10 45 AM	1000	70.00	8 P.	2 00 PM	7 15 AM	9 30 AM	10 45 AM	M 98	2 00 PM	7.30 AM	8 8	W 51 /	200		Mar 50 01	0 0	8 30 AM	20 MM	7 15 AAA	3000	10 30 AM	12.45 PM	200	Mdoo	100 PM	7 15 AM
	+			_	_	_	_	_			_		-	-	-				_					_			-		_		_			-						_	_	-			_			╁		_	-	-	-	_
	00/1 BRE 7:00		ON17/1888 7:11	21:11 86817/TAGO	06/17/1666 13:00	00.3 8991/21/20	ON/18/19/99 10:45	0E/18688 7.30		04207948 8-50	00-01-00-01-00-0	08/21/1898 7:15	08/21/1969 12:45	08/21/1888 4:00	06/22/1080 7:30	0472/1988 11:10	00.51 6661/22/60	00/2 V 1000 7:00	Charles 12:45		00.21.000.13.00	040501040	06/25/1898 10:30	08/24/1888 10:00	08/26/1999 11:30	0427/1999 7:15	06.9 988 11/2/20	09/27/1909 10:45	STATE BOOK IN COMME	OUT BEST TOTAL	08/2W/1889 13:00	08/28/1998 14:00	09/29/1999 7:15	06-28-1858 8-30	<b>ONZECTORS</b> 10-45	09/28/1999 13:00	00/26/1999 14:00	06-2 6681/00/00	00.11 6981/00/80	51 / 8681/1001	000146661/10001	100000000000000000000000000000000000000	TAMPO SON CO.		100011000	1003/1999 17:30	10/04/1999 7-15	CONTRACTOR AT LES	10/04/1999 10:30	10/05/1999 12:45	OF CLASSICAL PROPERTY.	10/06/1999 14:00	10/06/1999 15:00	10/07/1999 7.15
***	8	74 0.77		44/1/4	88//1/8	TA MIN				Man Moore	Mon M2074	Tue 9/21/90	94124	4 WZZ/40	H-22-M	Wed \$72/98	27.7	Par 0/23/80	The 872399		1070411	-	Bec 8/2 5/80	B45878 U	n 1276.90	Man 9/27/99	4 527/20	Men W27/M			Tue BZE/91	Tue trzave	Wed Warns	Wed brame	47250	West 9/29/39	Med S/2979	Thu troops	Thu traces		EN TOTAL		ACCULT THE	47.0	Sun 10/2/10	Sun 10/3/96	Mon 10/4/99		Men 10/4/10	Tue 10/5/99	- A	1040	Wad TOWN	Thu 16/7/89

,	Γ				_	_		_	_		_			_	_	_	_	_	_	_	_	-			_	_	_	_	-	•			_	-	_	_				_	_	_	_	_	,,	-	_	_					_
(atl many) load Eng	_	= =	•		Ä	= :				2	•	ä	96	ž ;	À i	4 5		- 8	32.2	ä	2	2		-	. 62	•	-	•	•	9	9	ž	-	-	<u>.</u>	•	<u>.</u>	•	-	5	196	•	<u>.</u>	193	ž	ě	Ž.	ē ;	2 :		. 2	Ŕ	ě
(sod) IPR	_	2 2			381		5 5	, 5	5.71	5.	571	38	39.	5.7	ē :			\$ 7.1	381	36	5.7	25	25		5.	5 71	5	ž,	i,	5	5.7		\$ 2.5		571	5 71	57	-		5.2	5.21	5		5.71	573	5	5.2	2.5	5 5				- 5.7
onneshility Corrected or Temperature (Secia (glidipal)	_	8 5	8		95 7	523				39.5	629	3.38	8	505	3.5	2 93	2 5	2 2	2.87	2 84	80	380	26.		866	8	348	337	3 51	152	7	6	377	348	3.63	7 98	343	9 9	2 5	5 5	8 29	397	378	01 +	3.75	3 56	333	ě	36.	325	, ,	2 2	375
(redpy) (pypermie)	_	2 :	3		225	= :		9	25	6.35	7 18	3.92	3 62	8	Z :	2 1	S 4	5 15	328	335	£ 33	ş;	9 9	2 5	;	66.4	3.89	3 89	65 E	<b>3</b>	*	56	3.77	3.46	2	\$6+	283		3 2	69 5	89 5	3 97	3.97	01. <del>†</del>	393	3.26	340	423	2 5	2 2	2.5		393
(pod) are.		2 16	218		\$21	2 80	0.0		2.85	2 95	2 60	6 97	35	350	5 ;			3 6	5.0	815	<b>+</b> 35	4.22	22.		-	4.27	8	÷	521	92 5	-	9/ •	3	2 9	919	9.78	4 78	9 5	2 6	23	62 €	7.15	472	4.57	4.76	526	5 50	25	7 1	2 3	5 5	125	• 78
Бритимпо	start cycled sension to MT at (1.45 AM			start peak flux leating from 11 45 to 2 00 PM						Duniesia husuu	started peak flow from 10 50 AM to 3 00 PM		started peak flow from 8 AM to 2 PM				O'Manage Seasons	Me Col MA 13 months from 14 Mo to 3 PM		and peak flow teeting to MT, continue internitient an			mant cleaning							many clearing					rharn clearing				edition) y learn								grand classes					OTTO AND AND AND AND AND AND AND AND AND AND	_
P Fraquency (min)		2 9	5 5		9	ę :	2 9	2 9	: 2	ő	2	9	2	2	ā	9 9	2 5	? 2	ě	ō,	ē	ō	9 9	2	2	5	2	2	2	2	9	2	2	. 5	•	ē	9	2 :	2 5	9	ē	9	9	2	5	5	ē	9	5 8	2 5	2 9		P
(see) notherud 4(	_	ž ;	15.00		98 51	8	8 8	3 5	8 5	50	15.00	15 80	8	8	5 8	8 9	8 8	8 8	15.00	8	8	8 8	8 8	8 8	8 9	8 5	15 00	15 00	15 90	15.00	88	8	90 91	8 8	15.00	15.00	58	8 5	8 8	8 52	8 2	15.00	5.00	15 99	15 00	8	5 8	58	8 8	8 8	8 8	9 5	25.00
nl) <b>di seka m</b> ucani (gi	_	::	*		10.7	:	- :	; 5	62	9	63	15.3	16.5	2	12.1	2	: :		16.2	19.2	9	8 2	85	: :	82		8	3.6	102	103	72	D Si	•	:	6	2.2	¥ .		5 6	; ;	:	7.3	7.3	8.6	۲.	10.2	102	8 3	2 6	0.01			82
To with sing morner (mage	_	F 6	: 5		î.	\$	: :			3	6	11.5	:	<b>10</b>	= :	· ;		2 0	112	315	20	:	e :		0	9	2	9	3	•	6	on eo	3		5	<b>\$</b>	4	: :			5	29	\$	6.7	5	69	5	69	70	· ;	: <del>.</del>		7.0
The loss in CIP Tenk (enail.)	_	£ 5	2 2		130	9	2 :	2 5	2 0 21	13.0	130	130	13.0	130	5	5 1	2 5	2	13.9	130	130	130	30	2 0	130	130	13.0	90	13.0	130	9	00	2	5 5	130	130	130	6	9 5	2	5	13.0	130	130	0.61	130	13.0	130	130	130	2 2	? 5	22
(leq) enuseered 98		::	; ;		•	; ;		; ;		;	-	9,	9	9	£ .	•	: :	; ;	\$	•	:	;	÷ ;	: :	-			÷	÷	=	<b>:</b>	•	*	7	•	20	ç :	5	: :		47	5	•	*	•	0	6:	e,	<b>5</b> :	: :	;	; <b>;</b>	•
ni) 98 esohed muusei (6)	_	\$ 5	97		900	20 1	8 5		8	8	\$ 30	14.20	5	6.70	5 30	8 3	0.00	2 2	6 60	ð. 8	8 80	9	9 5	2 6	3	9 70	e a	9.80	10 60	0.01	8	9 70	91 91	8 2	10 50	7 70	9.70	0 :	R 8	2.9	6.70	09.6	9 6	6 30	9.70	10.70	11 20	8	8 3	0. 5	200	990	9 70
eroted shall amenite'		*	: ÷		·		2 :		. 59	. 6	ě	<b>5</b>	5	9			: :		6	8.8	8	\$ 6	w 1	n ir	65	\$	9	\$	9	· ·	\$	e E	ž		ş	\$ \$	\$	s :			. 5	9	5 9	6.5	9	\$	\$	\$	e :			: :	£
nothkrziseň ggemel (mgg) alst		: :	: :		Ŧ	<b>5</b> :	• •	: 1	=	8	Ģ	ş	*	\$	<b>:</b> :		: 1	<b>*</b>	*	•	ę	\$	<b>5</b> 5	• •	- 5		37	\$	ę	•	7	3	1	. \$	=	\$	3	¥ ;	<b>.</b> .	: #	ę	ş	•	£	÷	Ę	\$	47	<b>\$</b> \$		? ?	; \$	<b>=</b>
(erita) siA labramoiqqui	_	<b>;</b> ;			î	ĵ	2 2		ŝ	98	0 86	650	ŝ	98	989	88	9 6	\$ \$	ŝ	2	93	3	670		0.78	980	68.0	65.0	980	089	6,0	0 69	ē		3	ŝ	200	·	3 4	9	8	66 0	99	68.0	20	0 99	95	689	3	8 3	1 2	¥	63.0
Unit ZW (crim)		8 8	1 2		<b>2</b>	2 :	3 5	; ;	25	¥	35	35	25	2 :	2 :	9 3	د د	. 2	2	₽	2	2:	2 5	3 2	2	24	35	Þ	25	a	2	3	5	. 2	35	32	žF	A .	3 6	33	26	32	32	32	35	71	2	č	35	9 8		· "	35
(O seemgeb) WZ qme	_	9 8	R		3.5	8 1	25 25	š	8	8	6	31.6	Ħ	8	=	31.5	۶ ۽	300	31.5	2	8	3.5	<b>R</b> 8	3 5	8	5	8	F	\$	25.5	25.5	£	ĸ	3 5	55	25.5	23	2 :	0 #	2 %		52	22	32	23	×	52	₽	£ }	5 5	° ×	3 52	22
(mdf) eletwol? pee	l_	27.0			2,		8 1	2.0							_					280			280				27.0	27.0			\$ ·		2	_	280	280			2 2		27.0	260	22 0	27.5					280			_	270
nesimio) amanmo' (ing) gelimo)		0 0219222		_	2222975 4								_		_	2269172	_					_	22031939	_		2303295 8	_			_	2320568 9		2378176 S				2353391 5			-			_				_	_	2377619 2	_		_	_
grafficer States tool	_	10780.3	10798 2		2	106217	6280	10460	108702	10872 1	108723	10873.3	10884 0	10690 5	50805 8	0 000	10016	0.1801	10919.0	10921	10937 4	10042 9	10001	10857.3	108745	(0078.0	110066	-1004	100	11025.6	110269	8	11061	11068	110716	11073 0	11002 5	1003		E 01111	11.231	11139 7	11143	111831	111688	1.88	111904	11190 9	6 26111	112113	112741	112363	11236 8
gniteració evitalumu: (evit) emil	5326.75	533000	5349 50	\$362.50	8 482	5372 00	2376.00	5	54.20 50	5422 50	5423 75	5426.25	5428 00	200	5449 75	8 5	05 0275	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	5473.75	8476 90	5402.55	5497.75	5515.75	5522.90	55.39.25	35.150	9565 00	\$570.25	5588 75	5590 50	5543 75	251262	\$618.06	5635 75	5638 50	5640 75	5860 25	5665 75	2025.00	5687 66	5691 50	5708 00	\$713.00	\$731.50	573650	5756 50	5754 75	226000	2,62,00	978030	Sanaso	5000.75	5508 00
(जसाम्म्) कान्	11 45 AM	M 00 -	8-30 AM	11-30 AM	130 PM	7.00 AM	100		7.30 AM	3 30 AM	10 45 AM	15 PM	3 00 PM	7.30 AM	7 42 br	Mar 00 2	77 97 97	10 45 444	12 45 PM	MJ 90 C	7 15 AM	12 45 PW	***	Nd 00 1	6 15 AM	1 S A	M 00 K	1.5 PM	7 45 AM	MA 00 6	12 S Pw	1000	8	6 45 AM	B 30 AM	11 45 AM	7 15 AM	200	3 8 8	10 40 AM	2 30 PM	7 00 484	12 00 PM	6.30 AM	11 30 AM	7 30 AM	***	W 8	M 00 1	1 30 AM	30.40	W 53 0	11 00 AM
440	├—	10/07/1990 13:00	10/00/1988 8:36	_	_		COLUMN TARREST				10/11/1998 10:48					_	0	_				_	10/15/1989 6:45	_	_	10/14/1898 11:30			_	10/18/1999 8:30	10/16/1999 12:45		00-11-00-12-00		10/20/1998 9:30			_	000000000000000000000000000000000000000	_		_	_	10/24/1999 4:30	_			_	10/25/1909 13:00	DE LA REAL PROPERTY.	06.7 8081/2001	10/7/1999 9:45	10/27/1999 11:00
	The 1077/91	The 16/7/20	F# 1084	Fri 104/89	pri source	Det 10/8/20	1	100,000	Mon 10/11/70	Mon 10/11/86	Men 10/11/86	Man 10/11/99	Men 1071 AP	Tue 18/12/80	14 10/178	Tue 10/12/86		20. DOL PHI	Wed TOTARS	West fort area	Thu 10/14/80	The 10/14/99	Fri 1015mg	10.157	Bat 10/14/99	\$44 TOTAN	Sen 19/17/86	Sum 10/17/99	Mon 107 mm	Mon 10/16/84	Men 10/18/99	100	Tam 10/16/88	Wed 10/20/W	Wed 10/20/99	Wed 10/20/99	Thu 10/21/96	Thu togathe	10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mary 10 mar	Frt 10727/98	Fr 1072279	Set 1073799	\$ar 10/23/80	Sun 1024/99	Bun 1024/99	Men 10/25**	Mon thrave	Mon 10/25/98	Non torstwe	Tue Undered	1077701	West 10/27/99	Wed 10/27/49
State State of	•			•	•							•	2	,	٠.	o.				. 0	=	<b>-</b>	= :	2 =	=	=	F	F	#	=	Ξ:	= :	: £		12	ŽĮ.	؛ د	<b>:</b> :	2 5	: 2	2	5	2	ũ	2	z	~	12	e :	2 :		: 5	ç
ı																																																					

				-			(w48)	6		(mis) sid	enched	uq) gg v	(10-	Mest	42 174	u) 41	(>0	(upu)			()edge;	:		
liver Bengeld	4440	-	(mina:ht) emili	Cumulative Op	and west	المستحدة (عبو) ودعائمت	olerwoi'i bee'	dep) MZ duej	(ento) WZ viA	Ememolyqua (	(codg) atof	5F (gpm) Ynched merany Ynchel	d) exnees(4 dg	ACC as east 4.6 (most.)	e alait heame'	ight	e) notiened %E	Tonouper's 94	Threeas	(pod) (pod)	A) Allegerence	ار آرمیهای را آمار آرمیهای بازد زیادهای روشایی	(evd) Title	(46 mpr) (pp)
21	West 16/27/50	10/27/1988 13:00	1-00 PM	3610 00	1 86211	2394194.8	280	27.5	35	089	5	06'6 5'	_	-	_	28	8.8	٥		*	2	363	17.8	ź
22	The sectories	10/20/1998 7:30	7.30 AM	9828 80	11257.2	2400783.5	0.02	26.5	35	3	•	11.7			7.0	10.7	8	2		5.75	3.24	3.14	5.71	Ę
**	The sectors	10/20/1988 12:46	12:45 PM	SECO. 75	11262.8	2402909.5	38.0		81	2	-				_	6	8	2		5.75	326	g	571	ē
2	PH 10/20/00	DE:/ #102501	130 Alta	5852.50	11281 2	2409099.4	38.0	22	26	65.0	*		_		_	117	15.8	2		7	2.89	2.75	5.71	ź
11	PH 10/25/00	10/28/1988 B:46	D:45 AM	505A.75	\$1283.5	2409652.6	280	72	35	ŝ	• •		_		_	12.2	8 51	2	maint cleaning	6 48	2.59	2 75		Ī
21	Frt 10/20/00	00:11:0001/02/01	11:00 484	200	11283.6	2419006.0	28.0	28.5	32	95.0	3	11.2	•	13.0	_	10.2	8	2		25	3.50	8	5 7.1	:
*	Fel terzenbe	10/29/1968 13:00	-00 PM	\$858 00	11285.7	ξ	280	592	- 22	029	2	1 20	-	ē		107	15.00	9		8	3.60	913	5.74	=
12	## 167978	10/20/1969 7:00	7.00 AM	5878 00	11300.7	2416855.9	220	<b>*</b>	32	5	· ·	\$ 13.8	•	13.0		111.7	15.00	9		883	2,74	2 61	5.71	2
2	14 10/30/99	10/20/1989 11:00	100	\$880.00	11307.9	24163123	\$0	<b>58</b>		0.29	2	14.5	•	30	_	11.7	15 00	2		7 12	28	2.45	5.71	6
11	Sen 10/31/F.	10/21/1969 B:16	3 5	\$29925	113269	2424672.0	240	 \$2		0 98		16.70	•	13.0	_	152	8 5	2		8 20	2 28	2.28	5.74	:
*	Sum 10/21/86	10/21/1960 12:30	12 30 PM	S905 Sn	113324		280	۲,		•	÷	15.6	_	130		ì	30 51	Đ.		7.76	5	2 30	6.7.9	204
*	Man 11/1/86	11/01/1988 7:30	7.30 AM	5924 50	113522	24	38.0	¥ *	_	0.99	=	9.				17.7	5.00	2		-	5 08	212	5.71	21.3
*	11/1/18	11/01/1999 9:45	9 45 AM	\$2.926	11354.7	2433858 8	280	9	32	ž	*	1780				:	15.00	<u>.</u>	Granded classical	8 78	2 12	90 Z	5.71	8
21	Men 11/1/88	11/01/1988 11:00	11 00 AM	5928 00	11355 2	2430905 0	28 0									(3)	8 5	₽		7 22	5 28	2 43	5.71	216
72	Men 11/1/88	91/01/1988 13:00	1 00 PM	9836.00	11357 2	*	27.0	58								14.2	8.8	2		7.37	35	237	5.71	213
1.2	Tee 11/2/96	11/02/1999 1-15	7 15 AM	5848 25	11375.4	24405922	280	25.5	4	-1	-	1	4	-	4	17.	1500	2	END OF TESTING	916	3 5	201	5.71	28.
	MEAN.							2								57	15.8	10.0		1,37	20.0	19.67	Ē	17.28
A(AT * GPM)	ı							34.0								95.0	15.00	0.0		0.37	4.80	4.47	5	17.27
	МАХ							200	-					}	١	8.8	15.00	9		*	2 2	46.78	=	17.88
	MEAN						25.5	27.0								2.73	15.0	0.01		137	1	17.45	5.07	2
τ.	i						9	21.0								070	9	6		978	£31	F-01	181	Ę.
	MAX						30.0	32.0						1	1	6.20	18.1	00.		124	#	# E	978	17.34
	MEAN						25.5	31.2								2.5	15.0	10.0		2	1.72	3	ş	# #
υ	ī						97	27.0								8	15.0	0.0		0.69	2.51	2.20	*	17.27
	MAX						Z.	34.0				1	١		١	88	15.0	200		=	27.21	74.17	12	11.00
	MEAN						Ī	£								7	15.0	100		7	4.57	Ş	1.45	8.2
Ď	ī						15.0	2								Ŗ	15.0	<b>1</b>		ž	2	2.01	1.9	Z.
	MAX						24.0	32.0			1					18.20	15.0	200		a.	1.52	2	5	11.00
A(AT & GAM)								24.2		Ì						2.57	15.0	10.0		13	20.05	18.57	5	17.24
BUNCHMAL MING							ş	24.0								2	15.0	90.0		0.25	-	<b>F.</b> 0	í	1.0
BENCHMAL MAX)	_						0,0	82.0								27	197	10.0		324	1	#	171	27.24
B(HOMMAL MEAN)							15.4	28.0								2.58	16.0	100		1.3	18.83	17.62	5	8
B(PEAK-EVENT 1)							ž	ž								4.12	18.0	100		2 05	13.46	13.19	100	27.34
C (NORMAL)							7 E	2 5								 	5 5 6 6	0.01		2.80	7.76	3 5	2.5	18.27
CONDIMINAL WITH C CLED AIR TO MT-EVENT 7)							×									Ş	18.0	10.0		2.4	7	4	5	5.0
C( HOMBAL)							£ ;	2								2:	92	9 5		2.3	17	12.	Š	18.81
DIPEAK WITH CYCLED ASH TO MT-EVENT 19							ž	i								Ş	9	9		7.37	1	77	:	1
DROPHIAL AND CYCLED AR TO MT-EVENT 15) DINOPHIAL AND CYCLED AR TO MT AND AT-EVENT 12)							7.7. 7.9.	2 2		653	76	25 25	::		33	7 6	9 P	6 5 6 6		\$ 5	17.	12	£ 5	2 2

The state	7. 2	5.90 16.150.00 13.150.00 3.10 0.74 15.550.00
Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Section   Sect	1	3.10 0.74
The control	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	8 5.
The contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract	Ma 20	06 6 6
Type	<del></del>	
Typing to	Manufaceria Man 1	7.12
Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   Typing   T		8
Type   1	(m) angoldit tale 1 (5) (6) (6) (7) (6) (6) (7) (6) (7) (7) (7) (7) (7) (7) (7) (7) (7) (7	69 72
Transference	(1.74m) HXIT	74 60
Third   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   State   Stat	(YAM) HESINEON 3 8 E 3 8 E 5	80
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C		
Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created Stromes   Created St	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	22 23
Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Campa   Camp	Categori 267 hours 5	8. 8. 1 8. 8. 1
Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Cambridge   Camb	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	266.00
Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Comp	<del></del>	
Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Company   Agranting   Compan	(196w) 1119 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	<b>8</b> 6
	8 8 8 500 mat/s	700.00
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	1.17 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2.150.00
Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Comp		
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C		7.18
### PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PATE OF THE PA	tybu	
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of the special states of	
Control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the cont		
Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The Control   The		
Cond-marked registered by Particle Registered by Particle Registered by Particle Registered by Particle Registered by Particle Registered by Particle Registered by Particle Registered by Particle Registered by Particle Registered by Particle Registered By Particle Registered by Particle Registered by Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Registered By Particle Register	Traffic Sanoth COD	
The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The state   The	(mph.) This material 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	22.26
The 20th of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the con	New	0.76
Column	Accordant to the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of t	ž 2
The State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the State of the		2 ± 2
The 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the 20th of the		888
The articles of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the c	and beganding equals 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	
Column	### ##################################	8 8
Column	2 2 3 5 5 6 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	265.00
CADO CADO CADO CADO CADO CADO CADO CADO	Change 25 25 82 45 84 84 85 85 85 85 85 85 85 85 85 85 85 85 85	88
The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s	B 5 5 7 8 8 8 8 9 9 9 9 8 8 8 8 8 8 8 8 8 8 8	2 2 3 3
The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s	Cum)	1129.08 1157.58 1161.58
	100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 20000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 2000000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 2000000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 200000 100 2000000 100 2000000 100 2000000 100 2000000 100 20000000 100 20000000000	
-   -   -   -   -   -   -   -   -		<del></del>

	(Agm) SEV.	90.050	20000	-	1	00000	00.008.1		11,700.00		17.550 00		8	100.00		- 8		00:006	I	7.850.00		350.00	7,780.00		8,000.00	_	5.650 00		7,300.00	0.500.00	_	800		00.000.0	97500.00		-	2000	00 056'2		8,480.00	8,950 No		00.050.0	9,650 00	_		90 002.6
IE TANK	(Jen) 82.h	00 05/	18,000 00	_		17.300.00			16,200,00	17,150.00			12.550.00	15,350 00	15.300.00	16.600.00	8 88 88	Ę		10.950.00		0000000				12.950 00	7,900.30		_	14,300,00	8	11,250,00		_	10,200,00			10.950.00	_	2	00 000 11	. 8		12 550 00		8		12.950.000 S
- BARA	Chert ASO gen) FIUX		= :		_	<u> </u>	91		-		7.0		2.5		-	- 5		29 0	+			E30	5 2 2			Ξ.	190		3			- :	_	*		-	_	7	- 530	-	_	22.0	_	670				
<b>I</b>	(1) <b>4</b> m) (c	-	8 8	!		8 8		š	8	_	_		8 8	8				6	8	2		_			8		8	_	6 10	8 8		_		_	9 9	_	_	8 8	_	8	Ş.	8	_		8 P	_		8 %
	;) jouducagns (qedic	100	2800	3	- 1	8 8	27.00	28.00	28 00		28.50	80	8 8	28 00		5	2800	55 <b>F</b> C	90	24 80		8 8	23 80	29.20	32 50		8	29 00	31 90	8 8		5	8 8	30 60	31.00		;	8 8	8	30.30	Ē	32.00	3.98	35	32 52 53	-		32 06
	н	8			;	8	7.18				8	-	E			į	3	8.78 E.78				23	ž				7 12		10.7			;		3.5			-	0	3.25			¥.		8 H5				25
	ménadeporte lato (-Agm				-	8					8					-	ì		7			<b>8</b>						17.80				5	:						8			12.25					7	E 22
(7/	Gus) wedangay jesa)	-	_	_		-	_	_			36 11						3		1			55.55					_	15.15	_	_	_			_	_	_	—	_	33.49	_	_	5	_			_		
<u> </u>	(JAges) NOI	-				 8 5					<u> </u>		-				_	_	+			85.						ş	_							_	_	_	33.40	_		E		_		_		<u> </u>
<u> </u>	(Tythus) H-SOHIZON	}-		_							96		_		_	- 3	_	—	+	_		50.0						130			_					_			600	_	_	5 00		_		_		- 58. 
-	(Noorl)	}-	_	_			11 30		8	_	•	_	8	_		-	>		+		_	c			_	_		-		_							_	_	_	_		۰		_				
_	JEA) (Jem) H-EHP	<b>├</b>			_			_	27.60	_	- 0	_		8	_	F			+	8	_	8			8		R		8				<u> </u>	<b>Q</b>			;		8		_	8	_	۶	8		_	
_	(Agm) N-EHN	1~	- 5	_	- 1	2	00 52 00	_	27.30	_	2 2	_	23.30	8			ï	34.00	4	26.05		5	00 25 60		Xi		26.30	_	25.00	23.70		- 8		28.40	22.90		_	_	25.00	_	24.40	00 22 90		8	23 03			 2 2 2
	(Jem) EST book	160.00	•			5	12.00	_	8		\$		822	98		- 5		ž	1	ĝ		124.00		_					120.00	92.00		-	<u> </u>	2				8	132	_	22.	ş	_	<u>š</u>	128.00	_		
-	76u) 50080 Pee,	231.00	3	-	_	66 66 	248 00	_	222.00		8.98		B B B B	219 00			<u> </u>	220 00	-	246.00		2.8	227.00	_	80.00		140.00	_	178 00	181		3	_	210 00	228.00		_	5	278 00		9	153.00		208 00	8			
_	(76m) OC	5	90 0	_	_	960	8	8	8	_		9	8 6	90		_	2 2	ŝ	8	8			0.70	8	98.0		00 0.70	_	0.80	2 6	_	- 8		8	98			8 8		96	8	80	080		8 8			080
-	итк (шек)	1			-					_	370.00				_	- 5			4			38			_		380									_		36				98						0.88
_	(1/6w) goo	<del> </del>						_			429.00		_			_			1			390.00								_			<u> </u>		_							276.00					_	
(tear	CONSUCERNIA (USA)	2,050.00	2,200.00		4	2,20,00	2,150,00	2,220,00	2.050.00		2,430 00	2.070.00	2.030.00	1.945 00		8	00000	2 330 00	940 00	2.040.09		1.982 00	911.0	380.00	00 566.1		00 BSB.0	1.836.00	1,825,00	8040		8	98.00	993 00	1,993.00			1,823.00	1.960.00	00 001 0	. a 70 m	2 113 00	1.980.50	2.300.00	2,200 00		1	1,940,00
	(Sep) Europyee	L	28 00			27 00 75	_	_	88	_				27.00		_		29 00	_1	28.3		29 00		28 50				28.00		28.00			3 2	28.50	28 50	_		30 00		29.50					2 20 20			29 50 30 00
_	**	1~		_	_	3	91.				8	_	, ,		_	_	•	7.23	1			26.9	98	_		_	10		% Z					58.83		_		, ,	ž		-	7.31		<u>.</u>		_		<u> </u>
_	Waste Sludge MLV	,-	_	_		_			_		_	_	_	_	_	_	_		1				_		_	_	_		_		_	_		_			_		_		_	_	_	8	_		-	9.600 00
	(7/6w	}-					8		8	_	00 05	_	B					8	+	8	_		00.08		90 09		_		_					_	- 8			3						8		_		
-	E.Mi agouit atselv	_				_	17,700 00		16 500.00	_		_ ;	00.008.61	15,300.00				13.250.00	-	8	_	11.100 00	10.75	_	-2 2 2			_	_				_	_	12,000			ž			_			1,78			_	12,300,00
_	TT agbuild ateath	_																_	1								_									_												 5
	Mate Skidge TKN Medic Skidge TKN																																											1502			-	1304
_	mgA.)															_								-							_					_	_							2880				9
_	er(ab) TRE resiev(	1 =	2 3	7	7.12		8		ž :		3	Į.	2 2	5	5 4 5			6	R	1960	Ŗ	2.25	- *60	209	0.85	9			;	9 9	20 42		_	_	28.85	958	5.0		_	24.73	22.76	-		31.80		- 73	E,	27.2
	Mary against	-				3	2	-	12.2		2.42	_	P.	-	_		_		+	8		8.	92	_	-			-					_		- F		_	_	_	_		_	_	5+0				
_	(mpped (popped)	-		_	_			_		_	<u> </u>	_		-			_	<u>.</u>	+		_	- -		_					-		_			·			_					_		<u> </u>	<u> </u>			
_	(Yeakey)	-	_	_	_					_			_			_			+		_	_		_						_				_	_	_			_		_	_	_	_	_	_	_	
	outpart sault late!	├-										_		_			_	_	1			_					_	_		÷ ₽	8	23				5				•	-			_		<u>~</u>	2 9	2 2
(pdi	of bereath egbuild g) and energinesh	ā	និ ខ	ě	8 5	8 8	28	- S	<u>8</u> 5	ž	š	<u>s</u>	8 8	š	ŝ	ž ž	3 5	ž	33	× ×	52	8 8	- 5	Ē	ž.	8.	Ē.			S 8	200	2 2		_	, K	ğ	<u>ج</u>	_		8	ā			2		8	8	8 8
(p	ani balasiw ngbuig agg) sinaT acdere#	ļ 1				. ž	8	ž	ទ ខ្	3 3	8	ž ;	8 8	125	52	<u> </u>	3 3	128	8	8 8	š	523	έ δ	75	8	ē ;	£.			3 2	8	ē.																
6	ST Imendial 97W9		3		20800	8 99	21200	204.00	172.00	00.00	116.00	00 1	8 8 8	180 00	78.00	8 8	00.00	90.00	172.00	00.00	176 00	20.00	172.00	160 00	90 09	180.00	16.00	172.00	240.00	8 8	8	12400	28.88	25.00	00.271	172 00	140 00	882	94.00	¥ 8	8 9	140 00	32.00	244 00	2000 2000 2000 2000	168.00	8.0	12 80 12 90
90	WITP Influence CB	278.00			80.00	26.00	368 00	268.00	296.00	222 00	146.00	368.00	8 64	283 00	256.00	90 20	8 8	238.00	230 00	8 88	225.00	00.96	25.00	218.00	8 8	212 00	288	212.00	230 00	8 8	202 00	8 20 3	8 8	208 00	242.00	238 00	82	8 8	329.00	179 00	20,00	90.991	98 98	212.00	204.00	204.00	190 061	98 90
	MATS INSURANCE INC.	-	_			R 8	—	-		_	8 8	_					9 9		1		_	27.20			_	_	_	27 80	_		_		2 8				_	8 8	_				24 40	_	_		_	22.50
-	(mag	⊬	S 5					9.50	8 8	2 2	_		8 5	3	25	_		_	3	8 8	_	_		8	8.5	3		_	8	8 8	8			3 :	8 8	8.50			-	8	8 5	_		9 :	3 3	8		3 S
_	(tri) enail? out	┖~	1277.00		1348.58	_		_	1465.08	_		_	80.00	_		8 8			8	901.08			192108				20196			2137.00	8	2185 000	_		5305.08		\$	8 8			247308		8	8	261708	8	8	2735.83
-		121 Mary 4714		Bat 4/17/80 13	2	2000	Wed 4/21/99		Fri 4723781				The 4/29/50 160		Sat \$71/99 183	Sun \$72/88 16				Sut Syllenger 15:		St. Gently not	61 66/Z1	62	Frt 5/14/00 194	81 Table 19	Sun Sileng 20			Frt 5/21/29 21:	722/10 2181	72399 21		Wad 5/28/99 22	Fri 5/28/99 2:30	72900 23	Sun \$70098 23	Tue 6/1/99 2401		Thu 6/2/99 24	Cur GRADO				Fri 6/11/89 26			Non 6/14/99 27
	4140	1	1	ă	5	2	*	ž.	Ī,		Hon &	100	2 2	Ī	28	5	1	*	2	E	Š	Ron	3 2	Thus	2.5	SI-S	S S	3		2 2	3.0	Sms	1 1 1	¥ 94 5	1 2	25	Se :	1	200	ž.	1 3	Mon	3	*		Sar	Sun S	Mont Tue S
ENT		-																_	1										_	_	_	_								_			_		_	_	_	_
BTAGE/EVENT																				ů																												
in		1																	1																													

Page 2 of 10

Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   Temple   T	
Third records	96 0 25 40 100 100 38 00 38 04 06 100 100 100 100 100 100 100 100 100
Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Control Cont	96 D 2540 0 0 M 38 D
March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   March   Marc	96 D 25 40 O 104 38 D) 38 C4 4 S5 7 2 3 34 D)
Teach   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Contro	96 D 25 40 O 104 38 D) 38 G4 4 S5 7 2 3 34 D)
Teach   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Control   Contro	96 DD 25 4G 0.014 39 0D 38 64 4 85 7.72
Cythol State   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.   Fig.	96 00 25 40 0.14 38 00 38 04
Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Company and Annual Property   Comp	96 00 25 40 044 38 00
Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communication   Communicatio   Communication   Communication   Communication   Communication	96 DO 25 40 0 114
Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Charlest State   Char	96 DO 25 40 0 114
Tright   State   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tright   Tr	8
A	8
The control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the co	
Company	8
Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Comp	
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	324 00 338 00
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	354 00
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	160100
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	7.29
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	7.850.00
COOK SET INVARIANT SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET OF SET	0.550
Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   Column   C	. <u>.</u>
COLD SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE S	
Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Company   Comp	15400
COECY AMERICAN STATE OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PR	
COLD SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE S	
ODES menderal with with the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control	
OCCUPATION OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF	
COCC	2 = = =
Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to proper   Spring Manual to	 មិនិនិនិ
8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	
	3 4 5 5 8 8 8 8
1	
**************************************	
(vo) control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control control c	156.00 156.00 176.00
	6.50 6.50 7.50 7.50 7.50 7.50 7.50 7.50
The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s	4204 58 6.50 (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (
le.	4204 58 6.50 (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (
STAGESTURAL CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR	4204 58 6.50 (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (18-00) (
<b> </b>	Set \$1.450

Page 1 of 10

	(7 ⁶ 4) 98AT		8	7,300.00		00 0988		7,300 00	9,650 00					250.00			7.500 00	600	3	8 8			5			90000		7,850.00	W 650 00	_	0,000		7.050.00	0,020,00	3	9,850 00	_	200.00	Г		900			5,150.00	6.500 00		8	
Į.		_	_		8 :						8							_		•	8	_					8 8	_				8					8 8	_	L									- 8
BRANE TA	(Jen) 82.34	] =		9,700.00	13,000.00	12,100,00		9,750.00	13,150.00	13,950.00	15,100 00			11,600,00	13.200	_	10,300,00			11,000 00	13,950,00	_	00 00 5 11	_		10.500 00	12,200 00		12,300 00		11,350 00	34,800 00	_	10,300,00		11,890 00	14 500 00	12,100.00	4,350.00	5.750 00	2,110,00	8.850.00	_	7.650.00		8,00.90	7,900.00	10.390
3.	(min/JSO (min/)	_	2 8	8	_	- 2		95 00	. 8				_	9 8			530	2 8		8			9 9			5		320 1.44	8 8	8	5		3	3.10		8			22	9 6	2 5	_		£ 8	. S	96 5		_
-	congob) entercopro) (5	<u> </u>		32.20				32.00	•					31 00			91 80		_				26 26			8		31.00		38.00					28.			30.70	-	3100 65						30.80		_
:	oospob) endersemel	<del> </del>	2 2 2 2 2	8	_	7.16	• • • • • • • • • • • • • • • • • • • •	22 22	ř	-						-	7.59	7.75		ē			5 E	_		F		7.02	F 8	-			7.18 29	2 3		22		8	8	F 8	8 8			6.9	38.	- S F	<del>-</del> -	_
H	('yeu	$\vdash$				2	_	_		-					3		5.88 7		_			-	_	_				r:		198			^	<u>.</u>				_	-		-		_	<del>-</del>	5.65			
١.	eucrarigacit'i latvi							_						-	-												_	_											-									—
١.	(Agm) segociti ialo					*									3		39.79					_	Ë							38.04				2					L						4330			
١.	(Jame) HOLI					28.30								ķ			39.70						3							8				 	8						9 67				43.30			
	(-1/6m) N-CON/COA					8								ç	\$		90.0						5					_		3									L		ć	_			ar.o			_
١.	JEA) (Agm) N-SH/ Moorie)	L														_				_																		8.24										
١.	(Jam) H-EHN		28.10	23.50		24.40		19.30	22 40					3	;		26.80	8	3	20 60			GF 27			2		27.00	22		21.80		24.40	23.20		23 00		58 80			23.30			2,00	22 20		62.7	
9	(Jgm) 88T beel		98.90	108.00		152.00		148.00	137.00					8	3		90 00	8	3	95 00 95		8	8			95		108 90	8		120 00		8	20 00		116.00		112 00			9			504.00	264 00	8	80	
E-	Leed CBODS (INBUT)	Γ	8	152.00		102.00		98.00	8					8	3	_	120 00	8	2	188.00			3			8		8 8	8		00 621		148.00	92 00	3	00 091		147.00			8			146.90	00:89		B X	_
-	(70m) 00	8		8		8 8	8							8 8	3		9 9		_	_		,	2 6			2		8	00 5	8	8			8 8	8	20		96			9 8				8	£ 5		
	YFK (WB/F)														·														340 00				328 00				•							360 00				
-	(Y ^e w) soc													8	3				•	•			e R												3										00:84			_
] -	Conductivity (utivers)	1.654.00	8 8 8	1,489.00		255.00	1,493 00	1537.00	544.00	- <del>-</del>		_		1,582.00	3		8 1	337.00	883.00	1,814 00			8 27 8			65300		2 020.00	2,150,00	975.00	1,834,00		1,993 00	1.924.00	2.140.00	2.010.00				- 1	80.86			1,742.00	87.18	1.812.90	5/8/0	_
	C) (omperature (degrees	J2 90		32 20				90 90						00 00		_	28.60		2 9				2 5			6162	_	23 20						28.90		27.03		29 40	_		02.52			29.20				_
-	H		7			82	_	7.14									7	2					ç				_	22	12.	_		•	6.7	200									_	8	1 10		<u>-</u>	_
	Watte Shidge MLVSS				_	9,550.00								0.00	, and		7,800 00	_	•				8					9.650 00		•	•		9,200.00								00 000 %				2,450.00			_
-	Weeks Studye MASS		00000	10,750.00		11,500.00		00 058.11	12,900.00					2,250			10,450 00	90.090	200	12,700.00						00 05611		13.290 00	92.5		14.150.00	••••	12.300.00	90	3	14,050.00		13 650 00	_		8			1,650.00	9.450.00		00 0597	_
-	₹1 sgbuit etesti (Jeni			_		<u> </u>		<u> </u>						5			ī5.	_					- -			_		_		215	-		_	-		_		-					_		\$		_	_
-	Marke Studge TKN	1150		•		Š							•	23	-		020					000	Ê							1780				9001	Š.						342				9,60			_
-	Weeks Studge COD (Agm)	12400				9000						-		50	1	_	12300					9								17100						_					9				13400			_
-	(syab) TRE metry5	19.		23.68		19 21	17.81	1 8	17.8		ž		20.85	2	1.0	1	E :	1 1	1 2	16.49	22.28	E :	: E			8 2	18.	ī	1 1	18 21	ž	1 2 1 2 1 2 1	ž	<b>2</b> 5	. 18	ž	5 5	18.55			17.81	92 22	<u> </u>	5 5	2 0	ω ₆	2 S	17.81
	blaff egbuild		8	0.51		5		1.	0.91					ž	3		51.15	ž	9	30			<u>.</u>					1.37	2	}	8		8	5	5	5.		98			8			20.	8	- :	3	
-	Cotal Mass BOD, Applied (Briday)		2	12		•		5	2					:	2		•	:	ž	ā		:	<u>`</u>					~	=	:	:		2		2	7		=		_	-			Ξ	5	- :	2	
•	Total blace Produced (yebidi	2	2 2			5	2	٠ -	. •		6			2	· •	:	= :	2 2		2	2	Ş :				= :	2 12	Σ	5 5	. 5	3	£	2	<b>z</b> s	2	ž	S 8	12			w :	:	6	2 6	. 8	<b>8</b> 1	ž 8	8
	meti belesili agbuli bag) árail enerámesi	ž.	ē ž	ĸ		8	125	ž i	2 2		ž		175	\$61	ž	8	2 5	8 5	8 8	ŝ	8	ž ;	ž <u>S</u>			E S	3 5	ž	§ §	8	<u>s</u>	8 1	ž	ž ;	5 5	ន	is is	3.5		-	K 8	8	ş	8 5	3 8	375	8 ž	ž
	mort helselff agbeit (bag) shaT notimeA						_						8							_	8						55	_				ž					តិ ខ				٤	8	<u>2</u>	ş	38	522	8 8	ŝ
-	BET Insulist 9TWN (Agm)		8 8	192.00	B 8	8 8	186.00	8 9	3 8	112 00	124.00	8 8	8	8 8	3 8	00 80	8 8	8 8	8 26	<b>1</b> 5	192 00	8	8 8	20.00	25.00	8 8	8	152.00	20.00	8 21	148.00	8 8	8	8.8	8 8	8	8 8	176 50	8 5	140 00	26.63	16,4 (0)	124 00	90 00	8 8	90 691	8 8	148 00
	WITTP Influenc CBOD	80 50	8 8	88.	80.00	8 24	130.00	8 8	8 8	228 00	178.00	200	208-00	9 9	8 8	8	00.21	8 8	8 8	178 00	324 00	178.00	8 8	174 00	88	8 8	8 8 8	98 90	8 8	8 8	178.00	24.8	8	8 8	8	99 92	25.58	140.00	221.00	280 00	92 90	200 00	98 98	8 8	8 8	00 5	200	00 05
	A-Shiri mandra Trivia (Ages)	25.40				28 40	26.80					8 8															-	32.60	92				8	26.20				28 60	25.30					28. 29	?			
	ciencii sizarci (mili	S.	3 9	8	3 :	3 5	3	8 8	8	8	8	8 8	10.00	8 5	2 2	9	8	8 9	3 5	8	8	8	8 8	3	8	8 9	8 8	8	8 5	3	<b>S</b>	8 8	9. 9.	8 8	3	S,	8 5	3 25	8	98	8 5	8	\$	ş 5	3 3	8	3 3	8
Г	(vr) sent and	42.44		4.00.5s	90 77	4363.06	4417.0B	8	8	4314 DB	4538.08	4561.06	4561.08	4581.56	4629.08	4854.08	4677 06	27.107.	4749.33	4773.33	4797.08	4820.58	C C 6969	4875.91	4875.91	4892.16	940	4964.16	4968.16	5005.91	5060.16	5110.91	\$132.16	20.00	5204.41	5229 41	5251 16	5300.18	13.00.21	5305 66	52425	2372 00	5386.25	\$420.50	3 3	5492.25	5515.75	5565 00
•	4400	Tue MITME		Fri BZDW	201	Mon 67378	Tue 8/24/96	Wed BZS/98	F11 12.77	Not british	Sun 8/29/86	Tue active	Wad Sride	Thu 9/2/99			Mon brings	Tue 9779	100	Frt Briorge	Sec W1788	Sun 1172	Tue Bridge	Wed MISSE				Mon 9/20/98 4	Tue 9/21/98	Thu 8/23/86 5	Frt 9/24/98 S	Son 9/2/99	Mon 9/27/98 5	Tue STEVES S	Thu Waden	Fri 10/1/99 5	See 10/2/88 5	Mon 1044786 S	Tue 10/5/98 S	Wed 104/09		Sai 10/9/90 s		Mon 10/11/99 5		Thu 10/14/90	Sat 10/15/88	Sun 10/17/99 5
STAGE/EVENT			• •	•				_																					٠.					• •					٥		•		2	2 5	: £	£ :	: =	=
L		1_																																					L					_				

	(7 <del>4m)</del> \$8A'W								4.950.00		5.900 00	_	S.RO0 00			5,550.00	11,063.64	6,400.00	15,900.00	11,350.00	7,450.00	13,800.00	1,486.77	5,650.00	11,100.00	5,418.75	4,450.00	6,300.00	12,883.33	11,217.50	8.808.27	1,760.00	7950.00	2050.00	5025.00	4450.00	\$550.00
MEMBRANE TANK	(7/Eu) \$57M	8,850.00	6.400 00	5,300 00	7,700 00	6.450.00	9,800.00	7,550 00	9.800 00	6.750 00	7,900 00	8.850.00	2,550 00	8,600 00	6.200 00	7,400.00	13,771.43	0.000.0	26,350.00	16,180.47	11,500.00	19,350.00	11,777,44	7,900.00	15,900.00	7,228.00		- 1	- 1	16,071.05			12100.00	6375.00	7770.00	7875.00	7219.23
MEMBE	(nimLASO gm) MUG	ட	_				_		96.0	_	1.07	_	_	_	_	1.06	99.0	4.0	0.74	9.76		0.87								0.7		122	1.42	_ ا	1.14	_	1.03
١	(7 <del>64)</del> 00	•	*	9	8.3	7.			8	27 80 6 20	0 8 40		5 50	_		6.10	99.0	8.4	00 8.80	2.83		DO T.00	28 4.67		7.00	25 6.29		- 1	1	8 5			3.90	29.70 6.65	50 5.80	85 6.18	27.27 6.31 1.03
	esengeb) eménegne)	-							28 00	22		27 40	27.00			27.00	7 25.94	6 24.50	2 27.00	4 27.50	25.00	7 30.00	6 31.26		- 1	4 29.25		1	- 1	22	1		30.04	8	3 31.00	30.85	- 1
ŀ	H ^c	-							7.0		7.23				_	727	71.17	*	7.42	-		7.47	├	_	-+	-	_	+	+	5 5	╫		7.05	Ļ	7.03	_	1.22
	Tetal Phosphoreus Tatal Phosphoreus	1 6							8					_		4.92	23.58	12.00	91.80	1,08		24.00			22.70	5.05	3.87	1	1	14.05	1	2.2	Ē	6.07	5.45	3.87	¥
	(Agm) negotilit late?	38.91				_	_		1054			_				48.51	18.81	66.72	155.04	75.04		125.17			75.52			П		75.02	47.78		38.04	42.41	43.32	38.91	46.78
	(Agm) KMT	8							\$5.00			_				48.50	86.55	64.70	155.00	74.87	36.10	125.00			75.40			ı	1	74 87	1	37.38	38.00	42.40	53.30	38.90	46.75
	(.Fgm) N-EOM/EON	3							5							0.0	90.0	0.02	0.16			3			5.62	0.01	0.0	20.0	- 1	0.17	0.38	0.0	PC'0	10.0	0.02	16.0	0.0
	MID-N (WBV) (VSF	L																				27.60	6.24	6.24	\$24			l	ı	28	6.24						
	(Jen) M-CHN								24 00		22 80		22 00			28.30	27.05	23.40	33.00	29.47	22.00	20.00	23.17	15.30	28.00	23,16	123	28.32	28.93	2 2	23.17	23.16	23.18	21.30	24.85	17.20	24.28
FEED	(Jen) 521 bee?								72.00		112 00		570 00			124.00	231.38	124.00	390.00	180.19	108.00	300.00	127.15	8.0	212.00	186.25	72.00	378.8	230.17	2 2	120	122.00	107.20	104.00	184.00	140.00	219.50
3	Feed CBODS (mg/L)								122 00		142 00	-	314.15	_	_	138.00	75.035	194.00	830.00	234.43	164.00	330.60	162.96		- 1	153.75	122.00		- 1	230.05	16.1	160.60	158.20	146.00	157.00	154.00	154.00
	(mg/h) 00	8	8	990	8	990			8	0.70		8	_			06.0	121	8.0	3.00	0.71	8.0	2.40	94		2			- 1	- 1	2	1		1.03	0.65	0.93	0.90	
	(Mgm) ALK	32000							380 00		_						92.50	380.00	\$45.00	11 22 17	363.00	\$42.00	349.16	320.00	380.00	353.33	320.00	0.00	381.00	422.17	342.20	336.00	334.00		360.00	320.00	380.00 0.71
	(YAW) gas	ļ	_						292 00		_	_					530.00	300.00	760.00	19.61	129.00	20.00			612.00			- 1	- !	29.61		380.00			00'844		292.00
	Conductivity (u.S.kcm)				_				00 065 1	1,570 00	00147	90.095	0.519 00			1,716.00	1,756.43	190.00	2,630.00	2,128.28	•	2,640.00			- 1			ı	-	2,137.64	П		1958.29	1795.50	1694.67	1595.00	1574.83
	(c)	-							28 20	28 40	27.90	28.20	28 00 1			28 10 1	25.49 1,7	24.50	26.40 2,0	27.03 2,1		30.00			1			1	- 1	27.10 2.	ŀ		28.71 15	29.25 17	29.40 16	29.05	28.13
	Hq neargeb) enutanequie?	-							6 96	~	7.24 27	-	*		_	7.20 28		5.81	7.32 26			7.65 30			27.7			-	- 1	722	ı	7.20	7 20 28	×	7.06 28	8	7.13 20
┝	( <b>7/6</b> w)	-							_							-	-	_	,	_		1	_		+		_	+	_		+	-	_	8			
	SSV-III egbuit eleaW	_							_		6.900 60		_		_	7,200,00					٠	٠			٠.			7,450.00		17	0 0 003 33		0 9425.00	3600.00	7450.00		7050.00
	Billis agains ataow (Agm)								7.356.00		8.950 00		7 .00 00			9.400 00				16,371.43	13,250.00	19,150.00			-1			9,650,00		16,371.43	12 200 00		12670.00	7600.00	6650.00	7630.00	6350.00
	TT ogbuit stasW	ī							5			_				(24							158.41	124.00	215.00	135.40	108.00	183.00				191.67	215.00	127.00	108.00	155.00	143.50
	Watte Sludge TKN	1001							126							5							1.191.65	893.00	1.740.00	890.00	754.00	1,004.00			1 194 46		1260.00	842.00	879.00	1004.00	862.50
	(wild) Moste Studies COO	14400							10800							8100							10,344.71	2,880.00	18,000.00	11,420.00	8,100.00	14,400.00			A 980 23	13,968.67	17100.00	10600.00	13400.00	14400.00	9350.00
	(eyab) TS2 molay8	879	ž	14.4	10.69	98 97	18.71	23	8.30	20 45	1021	16 89	18.83	11.13	£.73	B.16	21.29	14.0	24.73	16.79	14.20	22.28	19.25	12.25	31.80	14.04		П	19.91	2 5	1	1.1	15.65	20.03	14.40	13.29	22
١.	bledy aghuic	L							3.45		9,3		5				1.27	25	2.73	3	0.67	2.93	-	9	2	2.03		3	₹	8 5	=	0.84	1.14	0.98	2.00	ŭ	8
	Total Mane SOD, Applied (Widow)								9		=		ċ				17.57	10.00	38.16	18.37	1.00	30.79	12.72	7.40	21.08	12.17	9.52	2	18.40	7.52	12.79	12.53	12.15	11.38	12.25	12.02	12.43
	besulated Produced (yable)	9	ē	=	×	•	11	\$	ន	ē	8	•	•	22	\$	33	16.04		34.39	27.13	10.6	42.33	14.82		42.67	24.02	5.89		17.85	2 2	14.73	10.96	16.90	1.57	21.73	28.51	38.06
	mori belastiv epbuli Mondrans Tank (gpd)	8	8	8	8	S.	ž	375	98	8	8	90	50g	8	ş	400	116.25	90.00	130.00	148.15	100.00	225.00	133.01	70.00	250.00	239.42	100.00	3	124.17	147.30	132.35	127.78	143.16	112.50	225.00	237.50	265.38
'	most beteeff egbuild (bag) ánst nottemA	ş	š	8	125	Ē	ē	25	98	8	200	125	ž	8	328	280	93.64	90.00	130.00	30.00	8	150.00	112.00	75.00	175.00	175.83	100.00	3	92.50	30.00	11087		125.00	100.00	150.00	191.67	16231
	SET Insuffid 9TWW (Agm)	160 00	14,00	8	90.00	128.00	140.00	128 00	128.00	176.00	152 00	886	8	8	98	160 00	182.91	120.00	216.00	178.13	48.00	286.00	162.22	8	248.09	161.29	124.00	3	94.00	174.13	152.62	146.87	153.45	212.00	180.00	154.00	149.85
	WHITE PREPARE CROSS	152 00	180.00	178.00	171.00	8.1	163.00	142.00	8	170.00	00 891	147.00	214 00	8	90 181	187.00	248.27	163.00	135.00	258.30	146.00	67.00	178.94	8.3	359.00	179.25	142.00	8	283.17	254.00	2	7.8	174.73	180.50	173.60	11.83	169.00
	H-CHIN Imanified STVING (Jigni)	88	31.5						28.00	24.00		_	_			31.00							36 40	21.00	32.60	27.45	24.00	8	31.53	28.99	28.41	23.13	27.53		28.60	29.05	73.72
	atreed anneal	85	9	3	ş	9	8	8	9.50	9	8	95	9	8	50	6.50	8.18	3.0	8.00	2	8.4	8	6.53	6.30	90.00	9.30	2 :		8	9 8		8	8.8	95	8	2.2	8
l	(tot) entit met	5588.75	5412.25	87.96.78	5680.25	5000	5708.00	5731.80	5754.50	5780.90	5804.30	5828.50	5862.50	5876.00	\$800.25	5924.50																					
•	<b>490</b>	Man IQUIGNES		Wed 1020/86 S	Thu 16/21/86 St	F-1 10/22/80 54	Sel 10/23/94 5	_	Mon 19/25/PB 5:	Ton 10/20/1995 S.	Wed 19/27/98 St	The totaged sa	54 10/29/88 St	Set 10/30/86 54	Sum 10/31/88 St	ě	MEAN	T T	MAX	MEAN	Z	MAX	MEAN	Z	MAX	MEAH	N. S.	-									
\$TAGE/EVENT		=	=	2	=	2	-		2	2	2	=	•		2	12		٠	_					U			•		ALAY 0 OPER	SCHOMMAL)	CONOMINAL	COPEAR-EVENTS 3.4.8)	TO LET EVENT ?)	TO MY-EVENTY)	TO BIT-EVENT 109	TO MT-EVENT 11)	TO UT AND AT EVENT 12)

_		_					_									_											_		_				_		_								
	sucroniquents &	94.52					6163		_		Ř				96						200						L	88					99 OH			_		_ :	ţ		_		12 66
	negotilei latoT #						70 63			-	į				5.08	-	_				5. 2.							65.16					8	_					9467	_			280.82
· -	ALK Consumed	18.84				63 73				-	£				9	3												75.65					92.2										57 29
MEMOVAL	avomen pinomma 2	29'86	26.57				8	9	;		8	8 73	98	E .	8		29 64	Ş	£		;; 8							69 66		£	8		26.66	04 96	50 11		-		93.51		38 35		38 36
<del>-</del>	% CRODE Hemoval	29.65	8				95 86	5			 \$	8	5	?	8		86 8e	8	2		95 oc							0: 68		£	62.56		36.35	90 66	25 56		_	\$	26 66		G 6		94.48
-	PLOOD GOUDAN						96.84								5	-				-	_							_					16.76				_						75.26
-	invomen &21 %	87 89	128.66				89.66	8	-	-	Ē	96 98	8	:	3	-	99.76	3	 \$		66 66							\$		05 66	\$ 8		98 98	38 86	Ç 8			- F	99 RS		56 66 66		
	(THING) 34H	6,000.00	3,110.00				200				3	<b>€52.00</b>			3 330 30		0.365.00				3300 00			,				6,920 00		98			00:000					00 905	300 00				3,200 00
-	Feed Cofform (CFL/100 m/L)	8	8				8		_		 B						5 00		-								h	20 00					8 8	175.00		-		- S 081	20.00				8
-	Total Collions (CPU/199 mil.)		8				8				3	2 00			8	3	8		-		8							20.02				•	260.00	8				30000	210 00			_	62.00
-	Eucheldecous (Agm)						12				<u>.</u>				8		_				8							0.12	_				81.0						100			_	91.0
	Agm) negotiki lateT	33.58					25 55			;	è				8						29.26							30.38					6 63						66			_	A 85
-	(JApm) MUT	4.28					92			:	2.12				2	<u> </u>			_		8						-	8					5			_			6				ž,
-	HOZWOZH (WBV)	2930		-		_	23 50				 3				Ş	?	-				8							28 30					£ .						8	•			351
-	(Jem) enholds end				_		800	8 9			8 8	0,00	800	3	ž	8	800	8 8	8									8	ş	\$ \$	0.02		8	8 8	000	B 0		\$	8 8	Ş	ş		\$ 60 80
ATE.	Jem) entroid2 lateT						000	190	;		8 8	80	20 00	1	Š	3 8	20.0	8 8					_					21.0	800	2 2	900		909	8 8	900	900		ě	0.03	8	300		\$ 5
PERME	NH3-N (WBV) (VSF															_											L											_				_	
-	(76m) N-CHN	11.0	0.11			2	3 8	5			8	90 = 02	5		9		010				0. E. C.				_		_	9 9 93			0		2000		12.80			24 50	5		0.24		2
-	122 (mb/r) CBODE (mb/r)	ļ	90				0.60		_	_	-	021 040	- 200				014	- 5	_		0.36							0.65 0.20		5.0	0.50		8 .	272 020	73 660			654 0 10	0.18 0.20		98 0 50		200
-	Calcium Hardmass (Jigm)						•				•	•			•	-	•		-		٥		•		_			0					344.00	36030 2	_			332.00	340.00		-	_	324.00
-	ALIK (mg/L)	36.00	_			80 07			_		8				8				_		_	_		_			_	92 00		_		_	00 061	230 00			_	<u></u>					90 79
-	(76m) d00			_			24.00								8										_	_	-		_		•		5.00										00.71
-	(UTA) yilalarut	0.20			_			e :		_	510	7.	<u></u>	5	-	0 0		91.0	E .	_			_			_			9.19		S		9.0	0.42	9:0	61.0		5.					\$1.0 0.0
	Conductivity (uS/cm)	1,620.00	00 090				00:050	1,640 00			90000	00 097.1	200 00	800	8	000197	1,750 00	1,720 00	000				_					1.590.00	1,800 00	1,710.00	1,690.00		1.640.00	00000	1,870 00	00 069'1		00 017.1	1,740.90	1,650.00	9 9 2 7 2 9	_	1.580 00
-	cengeab) antikanaques (3)	26.10	27.50	27.00		8		25.50					2,38			_		25 50					_			_	-	_		27.80			58 00		27.30	27.60				28 ±0			8 8
L	Hq	7 10	7.47		_		2				R -	8	_		Ę	-	\$ 2		_									\$		S			8	38			_	2				_	ž
	(n#w) \$0080	00 001,1	1,050.00				908	247.00	<u> </u>	_	00.00	988	900	_	ş	3	1,150.00	200	200		1,040,00							1.070.00		1,120 00	1.360.00		1,090 ng		1,740 00			00.055.1	1,300.00		1,280 00		920 00
	(76u) SSATM	9,100.00	8,150.00				4,800.00				7.430.00	7,150 00	8	-	7 875 20		8,350 00		D 000 6		6.800.90					_	6.400.00	7.200.90		00:006	9 450 m		12,300.00	0.000	9.500.00	_		10 409 m	00000		8.650 00		8,750.00
TANK	(Jen) SS.M	13,133.00	11,600.00		6.475.00	9	6,650 00	0.000			10,440 00	10.100 00	5000		8		11,800 00	200	12,000 00	13.050.00	9.450.00	9.050.0				-		10 050 00	12,900 00	13,750,00	13.203 00	13.500 00	07,300,50	13.656.00	13,250 00		15,700.00	13.65¢ m	13.550.00	16.150.00	13.050.00	10,750 90	11,850.00
AERATION TANK	(nimh.Aso gen) RUO	_	6.43				ğ				•	7			9		87			_	—						-	98		59:0			0.40	290					9				3
-	( <b>1/6w</b> ) 00	0.70	2 8	8 8		8 8	8 8	5.70		8	8 5	5.	2 5	8	8	3 3	2 00	8 5	2	-			_					8	0.70	8 8	5.		8	8 6	98 0	6; 0		0.40	8 8	8.	8	_	96 0
\	ompob) endeneques (3)	2,00	3 5	27.50		5	25.8	25.00	ŧ		8 8	38.60	36 50	Я 8	5	8 8	56.00	25.50	2,									92	27 00	27.50	38 20		26.00	8 8	27 00	27.80		28 00	8 8	\$	8		29 60
Ľ	H	ž	8		_		7.28		_	_	7.01	7.78				9	7 62											7.12	_	7.33	_		7.23	733				7,47	•	-	-		
L	CB008 (wild)	1,020.00	2,820 00				725 00	9			8	1,040 00	-	-		<u>.</u>	1,660.00		8095		1,850.00						L	830 66		8 \$ -	1,570.00		1.070 00	20000				1,760 00	960		1,420 00	_	1.300 00
	(Vi) emit muñ	7 '				148 58		217.08		289 58	337.08		386.56			8 80	529 08	80 53	8 10	80559	80.00	80.03	623.08	8 3	653.08	653.00	82.778	25.55	749.58	<b>3</b> 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	82133	25 SE SE SE SE SE SE SE SE SE SE SE SE SE	965.08	913.08	936.58		1013.58		1057.08		1129 08	118158	1229 08
-	etag	Mon 2/8/99	Wed 2/10/80	The 271178	Sun 2714/8	Mon 2/15/80	Wed Z/1779	Thu 2/18/90	Set 2/20/8	Sun 2/21/98	Tue 2/23/88	Wed 2/24/90	Thu 275/19	Set 2/27/89	Sun 2/28/99	Tue 3/2/88	Wed 3/3/99	Thu 34	Se 36.78	Sun 3778	Non July	Wed 3/10/88	Thu 3/11/20	Set 3/13/80	Mon 3/15/89	Wed 3/19/80	Set 3/20/89	Non 3/23/99	Tue 2/2/59	Wed 3/24/99	Fri 3/26/90	Sun 3/2 (1/9)	Mon 379/89	Wed 3/31/90	Thu 4/1/99	Fri 4/2/88	Sur 44399	Non 4/5/99	Tue 46699	Thu 4/1/2	Fri 4/9/99	Sun 471/99	Non 4/12/99 Tue 4/13/99
STAGEFEENT		<b>-</b>	_								-																	_												-		_	

_		_					_													_		_				_											_		_			_	—		_	_				_
	ananadaonin'i X Iavometi					97.93					5	5					92 58						99 00						53.43	2				<b>\$</b> 6 \$4							36.27			64.18					9	 8
	negorbili latoT & isromefi					7£ 75					60.46	-					52			1			92.50	_	_				97 17	:				E E							38.79			5.43						
	Semuenco XIA &	-				£ £					7						33.33			†		_	90.00	_	_									22.22					_	9			_	58.33	_	_				÷
MOVALS	lavornest phonon &	12.06 12.00	-			95 75 25	78.84		\$6 41	_	- 5	3	92.51		82 00		8.		8 8	†	£ \$		26.93			2		,		96.76		55 25 26		95.85	-	<u> </u>	69.68	_	-		99 R4	_	200	98 86		79 66	02.00			E 25
1	% CSODS Removel	98.74	-	_		£.	8 85		7. 8		- 2		18 66		.666				8 8		 8	-	97.35			3	_	,	  	87 66		98 86 50 86		94.95	;					/6.56	76.56					02.56				
	WYCOD Removal	-				*		_	*		- 6		- ði		ъ. 		3-		3	+	ă.		5		•				-	-		ē:		2	ě		ъ.			<b>5</b> 5	-		*	34 33		*: 				
	FIRST VICTORIAL	69-63		<u> </u>		55 26	2		·	_	9	_	98.88		26 66		200	_	8	+	98		*						<del></del>	22		£		5			89 66			_			—			98 SB	—			
$\vdash$	FAMOUR 251 %	8	- 1	-		8	8	_	8:	-		3	- 8		8		8		8	+	\$	_	8	8					?	8		6		8	8	8	8	_				8	_	18 56 81			8			
١.	ньс (съличт)	2.500		_		8	3400				200		3,000				8		8	1			99.						§ 	7				1.400	8	_				000		2,000		1,900			0.61			
١.	Fecel Coliform (CFU/196 Int.)	40.00				82	8				8	3	12.00				28.00		5 8				10 00	8	ŝ			:	3	12 00				8	8									8		_ :	8			8
١.	Total Colitoria (Jrn 001/UTC)	130 00				8	350 00				25.0	ì	25.88				22 00		% %				22 00	5				Ş	T 27	18.90				2388	8									22 (0)			<u>S</u>		9	8
١.	auenoriqaeeii latei (Jem)					0.28					8	3					0.37						0.67						8 30	-				6.79							3.76		Ę.	4 37					;	
	(Agm) negetibl leteT					21 43					86.77						91.61						58.85						30.14					31.00							20 50			09 61					Ş	•
ľ	(mg/L)	-				20 42 20 42					-						17.70			1			2.45						2	5			_	2 20							200			2 00	_					8
-	HOZMO2-14 (W&A.)					8					3	?			_		÷			1			16 40						5	8				28 50							18.50			17 60						 5
-	(Agen) enhadd serif	20:0	3 8	Š		ě	80	3	s	_	2		800	g	0.03		8	0 03	6.0.0	88	8		0 03	200	3 8	900			50.00	3 3	900	0.0		8	8 8	8 8	2.0			3	90.0	<b>3</b> 00	900	0.03	_	8 .	ž ž	;	- 5	2 2
, E	Total Chlorine (mg/L)	20.0	A 6	9		ē	2 2	8.0	8		ş	1	8	8	8		8	20	8	8	8		g	8 8	9 8	800		5	3 8	6	500	Š		50.0	8 8	2 6	10.0			5	800	6 15	5 0	800		0 0	2 5	;	-	3 5
PERME	NH3-N (mg/L) (ASL Chack)						4.5		÷				3																								•													_
	(Agm) N-EHM	273	:	_		8 ×	3 5	978	£		5		1.76		8		1360		52		0.05		9.18	9	3	0.07			9	90.0		002		0.12	10.6	Š	0.07			è	9.0		Ş	0.03		6.0g	000	;		77.
	(Jen) 221	Ľ		_		9	6.0	-	0.20		020		020		06 940		2 0 50		2 333	-+-	£				5	30			8	0.20		020		۲.			0.40							0 0 50		2 020				2
١.	CBODE (WPVT) (WPVT)	09:0		-		90	96.0		0.57		5	ì	0.54		ç		000		820	+	-		57.00	-	-	4.72		- 8	-	8,0		202		340.00 2.57	-	3	97			9			0.61	0.10		0.62	5			8
-	ALK (mg/L) Calcium Herdnese	_				85 85											90		٠.	+			8			•••		- 1	8					8						128			_	38		_	_			B 8
-	(new)					£					240						23	_		+			15.00					- !	ji Bi					23.00						9			—	14 00			—			
-	(UTM) WINISHUT	21.0	8 8			98.0	- 8	8	95				. 2	62 0	93			22.		8	N.	_		7 5	- 42		_	;	- 9	2 2	21.0	2			2 5	38	51 4				-	0.51	2			2	* 0 5			2 86
ľ	сондподъць (паусш)	-	0007.			00 000			_		92.72	3 8	8	8	8		- 8	924 00	8	25.00	00.096.1			8 8					3 8		8	8			8 2 8		00 889°s			8		1,756.00					0000281		- 1	1.510 00
-	to		28 00			27.00							29.40						8	-4-	 88 	_		30.00							32 00 1.4					30.00		-		32.00		30.50		8			2 8 8 2 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	_		8 1 8 1 5 1
:	Hq sesgeb) authrognet	7 40 28	8 7			763 27	207		F		7.87		7.54	53	2		7.78		7.51	39	٤.		161 31	20 20		2			_	7.	_	2		R A	8 8		۶			š	32	8	=	3 91		7 411 32	2 8			5 E
Γ	CROOS (mpt)	00.080.0	9			1,370.00	1,140.00		00 0851		90		760 00		00 025,1		960 096		955 00		00 026		900 009	50.040		90 089		8	3	050 000		00 00		00 00	5		00 000'1			1000	160.00		760 00	270.00		915 00	965 00		-	 8 8
-	(w8v)	000	- 5	3		8	-8		8		- 8		8		8	90 90	3 8		۶	+	8		٤	8	3	8			 3	00:00		8	_	8		- - -	8	_		3	- 00 00		8	8		8	8	3	8	
ı.		986	8 8			98 8	00 10 700		80	8 :	8 8		9,400	8		12.950			7 950	-+	8 8	8	60 6,750	8 8		00 6.550	8		8 8	90 6.300		00 7,750	3 8	900.5	2		2.000	8		3 5	00 7.500		7.850	7,850		00 6,700	8 8		_	8 8
AERATION TANK	(Jyon) SS.JM	13,700.00	14,700.00	15.00	12,850 00	00 021.81	14,700 00	14,300.00	14,400 00	0000	00 000 00	13 800 00	13.150.00	17,000 00	11,950 00		13.650.00	13.200.00	11,450 00	11,600.00	9,850.00	11,400 00	8,550.00	9,700,00	8.250.00	9,100.00	9.500 00	8,150,00	8 8 8	8.150.00	10,000,00	10.450.00	10.100 00	3.100 00	540	10,150 00	9.600.00	11.350 00	12,900,00	00.000.00	10.900.00	11,850.00	12,800,00	10.350.00	11,300,00	11,300 00	11,600 00	13,900 00	14,850.00	12,100.00
AERAI	(mins/JASO gen) PAUO	650				20	90				9	5	190				5		9				150	9,0				97.0	5	95				9	5	ì			,	9	0.53			65.0		0.60			5	8
	(Jew) od	8	8 8			8 5	8	38	2.00		8	8	8	8	8		8	2	\$	\$	£		3	2 5	3 5	2			3 5	2 8	2.50	- 29		ş	8 9	8 9	8			2 5	8	8	5	1.40	8	3	& E		,	2 2
	Temperatura (degrees C)	28 80	8 8	3		2 2 8	27.00	28 00	8	_	8	90 90	28.00	29.00	28.70		5, 50	28 00	98 98	88	£ 8		06 OC	5 S	8 8	8			2 8	8 8	33 00	8	_	90 20	8 8	3 5	31.00			8	31 00	3,40	8 5	32.00	31.40	32 00	32.90	\$		9 5
Ľ	Hq	8	-	3	_	00 7.32	721		8	_	8		00 6 R3		8		7.		6.83	I	8		7.17	3						202		8		\$			8	_	-	8	721		_	86		6 85	8		_	<u> </u>
L	C800e (w8yr)	1,320	¥ .			<u>8</u>	1,320		1.720		5		00:028:)		2 630		8		1,110 00		8		00 OK.:	3	•	3 860 00			2	1.074		1.240 00		300 6		_	1,350	•		5	1,460		860 60	800		5	8	}		8
١.	(vd) seeff earth		1277.08	124.83	1349.58	106808	10,10	1441.08	1465.08	25	527.7	9	1505.00	1609.08	1634 08	1856 08	170508	1729 08	1753.08	1777 00	1801.08	25 976	1873.08	98.08	20 50 50	1969.33	1993 00	201656	2065	2069.08	211306	2137 06	2165.08	2213.08	2233.08	2281 08	2305 08	2328.58		20/02			247308	2545.08	2569 DB		261706	266508	2690 08	27.13.08 27.36.83
	****	BET LT POM	7 516e	Sec. 477.	M 5	Mon 4/18/86	3	Thu 4/22/98	F1 423	84 424	Sen 421	427	47287	Thu 4/29/88	FH 4/30/98	Set 571/84	TO SO	740 64698	Ward 6.5.00	784 M	5 5 5	5	Mon S/10/99	2 1 5 1 5 1 5 1 5 1 5 1 5 1 5 1 5 1 5 1	Thu 5/12/96	55 14	Sat 5/15/88	2 2 2 2	200	5	Pu 5/20/9	FH \$221/8	Sun 5/23/88	\$25 w	5 1	W \$22	FH 528/	Sar 5/29/9	Sun 570 <b>79</b>	The 6779	Wad 5/2/99	The 62/99	Fri GAME	Mon 4778	Tue ENVe	Wad 6/9/99	Thu Critical	Sat W12/99	Sun 6/13/89	Tue 6/15/99
1			_	_		-	*			~ ,	- 1	, -	*	_			_		_	1		_		- 3				:		*	_		· •	-	~ i	, F			· ;		_			_		_			w :	_
┢																				- 1																														
rend																																																		
STAGENENT																					U																													

	incomeration of a				69.21					79.49		_			56 56		_	_		:: E		_			21 98	_				\$1.02					\$ \$					69.33		_		_	45.05
-	levomeñ 				90.39		_			56.29			_		35.05 S		_			5					85 62 B					80.89			_	-						<i>E</i>					65.83
-	* ALK Consumed				1.98					96 29		;	 8		-					60.56					-					*					66.25					65.71 57					\$2.38 E
WALS		4	-					2	_	99.72	# # #		5  F		19:61	22 22	-	95 05 		25 25	£ \$		5 85		28 98		2 8	28 82		99 79	99.76	-;	i B		8	65.66		- 8		29 63	69 63		99.73		52 52
AEMO	wound enominal of	77:M6 98:77	86		17.88 78	59.87		8 2		8							_			8			ž.		¥6 54		è è	\$6.66		58 56	96 66		\$		8 8	98 88		98 66			76 66	_	<b></b>		76 56
-	* CBODS Removal	38:86	8		78.99.B7	39.82		8		8	\$		E 8		15 84 15 15	28	_	£ 8			94 75		8		£ 98		<u> </u>	8		8	\$				_	66		ŝ	_	66 66					_
-	Hyvame# 000 #				1 97.64					_					15.55	·		8 27		_			_	_	97		_	5		<u>.</u>	•		_	_	9493	6									94 75
L	levemen E&T #	89.68	8		8	8		9464		8	88			_	5 5	9	_	# 6		1866 0	59 69	-	8	_	99 85		E K	24.62		99.85	8.	9	Ė		99.85	08 66				\$.	99.89	_			_
_	HAC (CENTER)	8,000.0			2,500.00					700 00	500 002	_			-	1.360.90				1,000,00	9										_				2,000	00 000'1				1 490.00	4,200 (				1.900 00
$\Big _{-}$	Fecal Coliform (CPUVI 00 mL)	14.00			22.00		12 00			8	90.				5	8 8				92	99.99														8	21.00				8	7.08				8
	moliloa iato? (Jm 00NJP3)	20 00			% %		16.00			8	13.00					3 5				2.3	60.2														8 <u>*</u>	2002				ē 8	98				8
	enerariquesi bab'i (Agm)				2.28					2 42					£					8					2 54					Q *					2 \$					3.52				_	2.22
(•	Agm) negetiši latoT				12.50					17.40				_	88.38					0					10 86					22 30					20,22					18 79					1300
-	(Jam) HUIT				90 2					2.00					2 00					200					3	_				2.00					5.					2.00					33
-	NOSMOS-M (mgA.)				95 93					15.40					8.8		_			5 5					£					20 30					85 06 80					16.70					8
-,	Free Chlorine (mgA.	8	8 8		8 5	8 8	8	3		\$ 5	8 8	8	3	-	3	5 5	8	3		0 00	8 8	-	800		9.0	8	200	Š		100	8 8	0 00	đ d		8 8	3 3	80	ę g		0.03	8 8	0 03	60 03		0.63
, E	Agen) embolrið læteT	0.03	8 8		800	0.0	š	8		500	8 8	8 6	8		8 :		ž.	90		8	8 8		0.0		80.0	8 2		3		2 2	8	0.0	8		90.0		800	8		8	3 8	0.03	600		20 0
PERME	NH3-N (mg/L) (ASL Check)																			5	0.0																								_
	(TABLE) H-EHEN	90'0	0 08		0.07	0.03		0.07		000	900	- ;	0.13		ē	ş		2		6.0	Š		0.03		90.0		3	623		0.05	9.02		8		8	8		800		90'0	90.0		8		000
-	( <b>Jen</b> ) \$81	-	0.20		020	0.23		g G		020	0.50		e.		0.02 0.50	3.60		620		8	0.50		3.22		0.06 0.20		Ç	020		9.	- X		R .		8	0 20		2		9	250				<u>,</u>
-	(mg/L)	62	- 2		71.0			8		200 005	0.52	-;	8		-	3		8		96 OF			ë		ō		6	80		9.16	8				390.00 0 18	0.20		0 22		304.00 0.13	3				902
-	ALK (mgA)				980			_		328		—	8			3		8 02 00 00 00 00 00 00 00 00 00 00 00 00 0		W 27:		_		_	_										8					30 00					158.00 312.00 0.04
-	(1/6w) gpg				8					2 5	3	-	<u>.</u>		8	<u>.                                    </u>	_	8 2 2		÷		_			8	_	_	_							5					ž					90 Tr
-	(UTH) (Hbidau)	51.0	520		410	0 0	41.0	<u>c</u>		22	D 0	4.	÷		9 1	2 5		2 2		1			5.0		91.0	1.	5 5 5 5	ē.		ž :	7 2	E .	<u>.</u>		207 15	9 0	e :	=	_	226	= =	8	Š.		-
	Conductivity (usion	Ͱ	1,400.00		1.556.00			128 00		8 98	_	00 27			1,500 00			8 6		8	00 96391	_	96 Eg				8 8			22.00				_		00.677.1				06 2421		488 00			1,405 00
-	C)	8 1	8 8		8 8						8 8					3 20 20 20 20 20 20 20 20 20 20 20 20 20			_		9 9		8		8 6		2 2	-		2 :	27.00		-			8 8						32.00			32.40
Ľ	++	7.45 31	5 5		3.0	75.		~		737	, E				6.	4	_	е.	_	7.65	, X				7.55	_;	3	_		2.60	7.66	~			M 2	7.39		6		7.00	9			_	7.38
	CRODE (MBV)	1,020.00	1,000,00		00:040	965 00		735 00		720 00	965.00	. ;	800		1,100.00	810 00		6P) 00		642 00	275 00		00 <b>68</b> 8		8.85		8	810 00		680.00	768.00		245.00		61500	250 00		770.00		905.00	620 90		755.00		620 00
-	(Vin) SSV.M	\$300.00	9,400.00		9,150 00	9,000 00		8.750.00		B,45/3 00	7,300 00		7.45000		00 000 9	7,100.03	_	7 050 00	_	8.700 00	2 500 00		A 3000 DO		8.450 00	-	9.150.00	8.850 00		8,250 00	9,100 00		8000		9.300 00	7,000 00		00 000 0		6.850 00	7 450 00		6.400 00		6.300 00
TANK	(JABW) BSTM			14,450.00	11,700.00	10,500.00	11.550.00	11,700.00	2,250 00	9,759.00	9.550.00	10.650.00	9,856.00	00 000 01	8 150.00	925000	9.600.00	9 650 00	10,300.00	9.050.00	00 000 00	10,300 00	11,250.00	00 000 101	17 500 00		98080	11,850.00		10.950.00		_	8			9.350.00	9,450 00	10 300 00	8,250.00	9.150.00	9,500.00	10.650.00	8.600 00	9.950.00	_
AERATION TANK	(nimLASO gm) RUO				\$	3.0			_	\$	2	_			2	1	_			22.0			-		£ 0	_	190	_		120	880		-		<b>5</b>	0.65	-			<b>y</b>	8	_			2.12
-	( <b>'Y\$W</b> ) 00	9	8 8		\$ 5	5 8	2.30	<u> </u>		9 1	8 8	8	e R		9 :	2 2	ž	5	_	<u>\$</u>	£ 5	8	3		ş		_				3 8	Ē			2 2	9 9	2	2.0		8	8 8	2	D. C	_	č
-	Temperature (degree	92	8 8		31.20	25 25	32 20	8		32.50	8 8	8	8		9:20	8 8 8 8	9 a	9 8		35 68	8 9		3.45		31.40						90 00	28.00			98 55	2 8	9 5	3		32 30	8 8	93	35 00		32 50
Ľ	H	7,28			7.23	6.87		_		7.19			_		F 94	92,			_	7.24	5				7 12		7 10			8		_			121	7 29	_			?	8		_	_	722 00 7 13
L	(36m) 900E3	Ε.	1,30.00		620.00	1.060.00		802.00		755 00	1,100 00		8 2		1,270 00	858		20 592		88	8	_	1,129.00		86	_	90.0	878 00		790.00	910.00		8		852 00	28		87.00		820 00	8	2	8 (2		
_	(M) owell unit	2781.08	2808.08	2626.58	2001.00	2829 08	2952.83	296963	3002 54	305 00	3067.08	312158	3145.06	3192 06	321750	3245.0	3289.08	2225 83	3362.06	3385 06	3409 08	3457.08	3481.08	3503.83	3553.08	6	360108	3649 55	3673.08	3745.58	3771.08	3795 00	3644.06	3868 58	369: 06	3839	8	3967.08	406.83		4067.58	412958	415433	4204.58	4275
	****	West Critical	F	Sec 6700	Mon 6/21/8	Wed 6/237	Thu 624	Fri 6/25/8	#/2 to 10.8	Mon 6/26/9	Wed 6/30/9	ALL BALL	F4 77.	Sur 7/4	Mon 7/5	Wee 777	The 7/8/9	Frt 7/10/00	Sun 7/1 t/Be	Won 7/12/9	Tue 7/13/8	Thu 7/15/0	F4 7/167	San 7/17/88	Mon 7/19/9	Tue 7/20/	Wed 127 bow	FH 7/23/8	Sun 7/25/89	Mon 7/26/9	6/32/1 Pe/A	The 7/29/9	Set 7/31/99	Sun arra	Mon &2/98	Wed Every	Thu 8/5/0	11 64/90	Sur \$709	Mon & WW	Wed 5/1/99	Thu 6/12/8	Fri arraya	Sun Briston	Mon N16/9
- H		-						_											_																										
STAGE/EVENT																																										-	-		•
ľ																																													

_		ī					_		_						_			_		_	_											_	_	_			_	_	_	_		_					_
	aucradquodif d' lavornell					23 65								35.63	!		47.45					48 53							:	} !				34.91				1			:			55			_
	negorithi latol #					55 44								47.78			÷					89 15							;	79.87				87.96							7			64.22			_
s	A ALK Consumed																											\$1.12				5	Š			Ţ.							<b>7</b>	_			
EMOVAL	levomen sinowenh d	1	P	99.74		10 26		8	80								<b>8</b>	18 66		ş		8			95.66	_	20.00		28.37	25.33				97 20	2	È		76 7		5	: \$		2.8	99 78	_	61 66	_
*	CBODE Semonts	1	Ŗ	8 &		8		86	66.66					90.38			\$ 5	8		\$		8.			26 66		5		26 66	86 66		8	Ì	56 66	8	-	:	66		8	3		76 66	99 86		68 66	
	A COS Removal					_								17.79								52 76												37.94				Ť						59 96			_
	Havomañ 881 %	1	8			78.66			\$					ĝ				56.69							38.87		96		88 88	59 B3		9	Ē	58 63				86					F 106	46 66		98 86	
Γ	HEC (CENSUR)																					9,700.00	•					9,100.00	00-018				3	4 400 00	-			3.900 00					3,400:00	1 300 00			
	Fetal Collina (CFL/106 mL)												_				5					08 21	3,00					8 .				9	_	38				8						2.00			_
	Total Coliform (CPUV) (pt mL)													•					_			90						9 02	10.00			8	3	8		-		8					8	8			_
	aucrorigeoriti latot (Agen)					3.10								8			8					æ					_			3				55						- 5				17			_
	(Jigm) negotifil leJo?	_				12.70								68.8			8				-	5.17		-						g.				;				T		9	R R			15.50			
	(Agm) Nort					23								5			8					8								8				2.40		_		$\dagger$	_		8			2 00			_
	(Jen) N-con/con		_			10.50						_		9			S 2		_			3.17								£.				16.5				Ţ		8	8			13.50			_
	Free Chlorine (mg/L)	8 8	3 5	8		9.00	8	8 8	800					8 8			3 5	3	89.0	0 27		ğ	ş		ş		88	8	8	8 8			5 8	2	8 8	3		I		3 5	3		8 8	25 25	50	50.0	_
EATE	(Agm) enfrointi late?	8 8	3 8	90.0		9.0	8	8 8	0.03		_			8 8			8 8	8	80.0	16.0		8	8		ğ		90	8	000	8 8		5	3 8	90.0	8 8	3				8 8	3		8 8	9 8	0.00	00	_
PERM	MH3-N (mg/L) (ASL Check)	-	_	_					_									_		_		_			_		_		_				_			_		1			_						_
	MH3-H (mg/L)			0.08		- 38		8	0 0 22								8	10 0 Da		8		ş			60.0		- 5	_	R	0.15			2	0.65	5	-		Ž			6		30.24	90 0 005		0.14	_
	188 (mg/L)	2		88		0.20		ē.	013 020					121			80	0.20		0.20		ž			0.12 0.20		2.33		0.12 0.20	0.03				0.20	_		_	0.00		- 1	8		0.05 0.20	024 020		0.77 0.20	—
	Calcinin Maranas (Agm)	Ľ						J	c					_	-		0	o		0		e			٥		-	328.00	0					•				2		-	,		280.00			<u>-</u>	
	ALK (mg/L)																	_										190 00					3					$\dagger$			_		110.00				_
	COD (wêyr)													8								8												8										8			
	(UTH) (VIbidus)	-					900							o c			ë ë	_		ę.		2.0			2					2 6	_		, = e		8 9			1		6 6			_	3 6		-	_
	Conductivity (us/cm)	1.409.00	1365.00	1,370.00		1,143.00	1,210.00	1,356.00	1,294.00					1,378,00			7,463.00					1.696 00	1,651.00		1,705 00		1,728.00	1.631.00	00.099	1,682.00		2	1,652.00	1,692.00	1,883.00	8				1,586.00	3		1,502.00	1,442.00	1,479 00	1,416.00	
	eeengeb) enuterequee (2)	9 5		32.50				8 9 5 5	_					8 5			9 8	_		32.00		5	32.70		30.00			8	_	8 8					28 80	6		99.06		23 40	3			3 8	31 00	31.03	_
H	196	؛ ا	_	-	<del></del>	7.18		2									<u>ኝ</u> ድ	7.64		9		7.80					7.30		7.36	-				7.42		,		8				_	, ,	- 1	_	-	
	CBODE (wb/r)	•		900:00		705.00		282.00	950 00					830.00	! 		618.00	715.00		007518		62000			680 00		720.00		782 00	750.00		8 		858.80	8	<u> </u>		0000			9		260 00	832 00		8	
	(Jen) SZV.M	-	} 	7,200.00		7.200.00		8	7.900 00					300 00			9.500 00	7.250.00		7,150,00		8.600 00			6,900.00		7,100,00		7,000 00	7.450 00		3		7.956 00	200	Š		8.700.00		,	8		4,450 00	6.000.0		4.400.00	
N TANK	(76m) 587m	9,200.00	8,900.00	8,450.00	9 800 00	9.400.00	10,900 00	9.600.00	10.500 00	12.650.00	06 G			9,550.00	12,150.00	10,250 00	6.750 00 9 mm n	9.800.00	10.850 00	9,700.00	12,850 00	11 650 00	9,800 00		9,700.00	12.800.00	9,750	10,950 00	9,650.00	10.100.00		12,750.00	10,000,00	10.350.00	00 009 01	11.200.00	13,400 00	33000	8,100 00	6.800 00	7.800 00	5 400 30	5.650.00	2,950.00	6.850 00	5.850 00	9,100.00
AERATION TANK	(nimLASO gen) RUO	3	3			2.		ž									ž	96				8					2 59		8			ş	2	52				$\uparrow$					16.0	160			_
	(754) Od	8 8	9 8	98.		8	2	8	8				_	8 8			8 8	8	- 10	86		Ē	DE -		*		9	89	<u>B</u> :	2 9			8	3	8 8	3		0,0	3 8	8 8	ķ.		8 8	8 8	38	8	_
	eeengeb) sruitereepnes (3)	25.25	_	32.40				S 8						S 2		_	E 8	_		31.60			32.08		29.90			86 98		9 8			_	28 90	23 00				3 6	29.30	Ē.		30 80	2 26		30 50	_
F	***	1 5	_	8		7.18		8  	8	_							£ 2	7 22		۶.		7.38			8		8		<u>چ</u> 8	9				7 24		3	_	2.7			 B		6 97	707	_	8	_
L	(76w) 10083	33 1		780.00	<b>z</b> -	15 00 11 2 00		9	80.	<b>P</b> 1			9 .	ŝ			ğ	8		950.00	<b>z</b> -	96	2	= -	\$		<u>.</u>		82	940.00			3	985.00	ş	<u> </u>		00000			8		00.08	1.01		ğ	<del>K</del> 8
	(vr) sent aust	4248		4320.58	5 500	4793.00	4417.08	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	4489.08	4514.08	450 S	4581.08	4561.08	5 5 5	4629 08	4654.08	470175	4725.33	4749.33	4773.33	0.161	6945.73	4869 33	4675.91	4882.18	4914.91	100	984	1,586.91	5080.18	5062.31	5110.91	5156.4	5180.18	5204.41	5251.18	5277.41	2300.16	2005.64	5324.25	\$372.00		242030	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	\$492.25	5515.75	38.5
	990	Tax 61778	1	Fa brea	See Britis	Mon 9/23/	Tue 8244	Thu 6/26/8	F1 227	-	Non 679	Tue BF31/R	Wed S/1/A	124	1	Sen MA	Mon Mar	Sale bala	Thu self.	fi Brigh	ALL BOTTA	Men Will	Tue MIAM	Week MISA	Fri W17/	Sat 9/16/99	Mon Book	Tue 8/21/8	Wed 922.	FH 1244	N25/8 NA2	Sun #26/88	Tue WZW	Wed 1294	Thu \$304	Set 10/2/80	Sun 18/3/88	Mon low	Med 104/8	The 1978	Sel 10/MPs	Sun tortoge	Mon 1071/94	Wed 10/13/98	Thu 10/14/9	Fri 10/15/	Sun 10/17/00
-		$\vdash$													_													_										+						_			—
STAGEJEVENT																												•				٠.								• 1		2	• ;	2 2	=		= =
STAG		Ì																																													
1		l l																																				1									

STAGENENT						AERATION TANK	A TANK		_								PE	RMEATE								_			HEN	DVALS			
	aned	CSODE (mg/L)	на	Temperature (degrees	(76w) oo	(nimLASO gm) RUO	(Jem) 28JM	(Jegen) 82Y Jan	CRODS (mg/L)	PH Temperature (degrees C)	(из/си) Ацидэприод	(UTN) (NIU)	(76m) ggg	ALK (mgAL)	CBOD2 (WBV)	(Jen) 221	75Y) (76W) N-(HH	Check)	(Agm) entick(5 earl	HOSWOZ-M (mg/L)	(TABLE) MIXE	(Jgm) negatiii latoī	euerongeacht kabe (Agm)	molilo Coliforn (Jm 00 N/173)	Feeal Coliforn (Jrn 00 th/13)	mc (canwr)	la vomeA EST >	Memoral GOD A	CBODS Removal	lavorish alnommå 2	ALK Consumed	lavoment euonestandi d'	lavamen
Ξ	Mon 10/19/80 5588.75	L	L		130		6.750 00	-	r	-	L		٣	124.00 300.0	8		-	-	-	20.10	Ľ.	22.10	2.73	┝╌	+	00 009"		-	-	-	82	43.20 29.	
=	Tue 10/18/18 5612.25		_		360		5,750 00		_	_				_			_	_		_				_			_					_	
=	West 10/20/88 5635.75		_	_	9	_	6,100.00		_			_	_				_		_					1.00		1,800.00						_	
				-	2.10	_	00 058'9	_		_	_							_		_													
2	Frt 14/23/88 5683.00	_	_		2.00	_	6,700 00	_	_		_	_	_	_	_	_		_		_	_					_					_	_	_
2	Set 10/23/Pet 5708:00		_				7,850.00		_				_													_			_				
=	Sun 10/24/86 5731 50					_						_	_			_		_								-				_	_		
=	Men 19/25/86 5756.50	632.00	7 16		8	8	_	4,600 00	612.00 7	733 2500	1,414.00	6 0	8 E	180.00 315.00	00	0.30	830	0.0	_	76	330	8 24	5.38	8	_	300.00	2: 66	12.56	8 22 66	2.58	52.63	81 69 8	52.42
- -	Tue 10/26/70 \$780.50		_	57.50	0.2	_	_		_	27.90	1,515.00	21.0	_			_		9	_	_	_		_		_	_		_	_	_			_
77	Wed 10/27/99 5804.50	87.8	7.21	26.10	0.70	1.7	6.750 00	5,150 00	2 00 288	32 26 00	918.00	21.0		_	80	0.30	0.24	ő						83		2,500 00	28 66	•	8 86 66	56 98			-
ŗ	Thu 10/20/00 5628:50			27.40	90		6,500.00		_	27:10	1,316.00	-						000	20 0 03	_						-	_		_				_
	FH 10/20/70 5052 50	100.008	_	27.10	E 6	_	6,950.00	4,850 fm	897 (1)	22 00	1,324 00	E :			0.0		ž.	•										•	49.83	8.	_		_
•	3et 10/30/98 5676 00		_		_		2,550 00	_		_	_	_						_	_						_	_	_					_	_
-		_	_				7,000.00		_	_		_		_		_		_		_			_	_		_			_		_		_
22	Mon 11/1/99 5924 50	780.00	7 28	27.20	080	62	_	4.450.00	665.00	7.35 26.40	1,536 00	80			0.72	0 40	M 0.0	0.07	70.0	2 38	2.40	5.38	3.5		-		99-66	0.	- 87 66	88.88	16 88	-5	
	MEAN	1,460.45 7.14		26.13	3.90	0.47	10,061.33 7,566.36	_	144.09 7	7.40 26.19	1,675.63	0.16	14.50 135	135.00	1.05	0.38	0.11	0.05	95 0.04	23.96	3.01	76.97	34.	2.28	1.65	67.778	99.62	97.59	99.61	79 65.64	87.29 70.	70.09	93.24
•	Z S	725.00 6.84		24.50	0.70		5,750.00 4,600.00	_	508.00 7	7.10 24.00	1,550.00	0.0	5.00	120.00	0.14	0.20	0.03	0.02	12 0.03	11.40	2.00	1.98	0.82	1.00	90.	0.7	99.63	20.00	99.04	M.70 60	60.61 56.		90.30
	MAX	2,820.00 7.62		27.50	9.60	85	14,900.00 9,100.0		7 00:050'	7.63 28.00	1,886.00	0.76	24.00 15	154.00	252	0.75	0.35	0.22	22 0.10	29,40	4.28	33.58	2.29	10.00	10.00	00.000.0	16.51	98.33	99.94	9.89	77.96 90	90.35	98.28
	MEAN	1,518.00 7.14		28.02			13,862.20 \$,656.2				1,719.24	0.75	15.00 204		96.0	0.28	577 8				9.73	15.56	0.16	107.19	46.74	3,275.88			99 55 8	82.63 50		75.72 97	78.78
	Z	830.00					10.050 00 6,400.DC				_					0.20						6.85	20.0										92.56
	KAX	2,630.00 7.47	ı	90.00	-	2	17,300.00 14,500.00	-1	_	7.82 31.00	1,950.00	88	17.00 25	256.00 360.00	85	09.0	24.50 11.	- 1	2 0.08	28.30	20.40	30.38	0.37	350.00	180.00		- 1	- 1	28 97	99.92 75	-1	25.50	2.50
	MEAN	932.19 7.13			1.73				_		1,603					0.27				_		17.99	92.0	18.15		_	6.						54.93
٥	Z.	\$20.00 6.83			0.60						_					0.20						7	0.67			-							23.85
	MAX	1,460.00 7.36		Ţ	2	1			_		1	- 1	١.	- 1	- 1	2	Į	0.05	-1	- }	1	8	2	_	اـ	+	-1		-	-	-	Ì	8 3
	MEAN	2	-		2.38						-					0.23	ä	0.0		_		3	2.03	9									50.73
•		480.00 6.97		25.40	9 5	5 6	20000	0.000.00	200.00	7.11 25.00	918.00	600	90.41	110.00 240.00	90.0	8 6	<b>3</b> 5	10.0	100	8 S	2.8	F 5	0.92	8	9 6	00.000.1	99.00	8 2 2 2	2 2	7 E	52.63 43	43.20	2 2
Ave Ta costs		4 536 67 7 31		1	1	1		1	_		1-	1	1	1		5	91.0	3	1	1	1	2 2	3	8	!	╁		1	1	ı	1	ı	1
DINORMALI		1.485.00	2	1		ı	13,863,33 9,875,00	-	┰		1-	0.24	1	1	40 0.85	0.27		5.19 0.04	1	1	}	35.5	0.18	١.	[.	╁╌	ł	ı	)	ı	l	l	97.97
B(PEAK)		1,115.00	7.37				13,450.00 9,650.0		8			0.34		360		0.40					- 1			- 1		_			1				
CONORMAL)		57.74 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07 05.07	7 2	31.17	2 2	1.74	10,596.15 7,692.3 9,416.67 8.890.0		768.60 7	7.42 30.84	1,612.20	0.15	15.55 121	128.29 344.57	57 0.57	0.28	0.27 0.0	90.0 20.0 F0.0	90 000	1547	2.54	18,42	134	15.09	1 20	1,383.07	99.79	94.68 9	8 59.66	98.82 63	63.55 58 52.96 76	58.03 St	39.96
CONCREMENTAL WITH CYCLED AND			3						:		•												3										:
CONCOUNTS, WITH C TOTAL OF AN			5		2	1	- 1	l	+	20 68.0	Т		1		3			5	Т		3	2		П	ļ	:	2				ı	ı	Ī
TO ATT-EVENTS		490.00	_	29.55	3.85		P600.00	4650.00	260.00	29.80	1533.00	0.12			0.03		90.0	0.07	7 0.04	16,30	8	20.30	3.19					9	99.98	12	2	52.13 47	47.45
TO MT. EVENT 19)		848.00	7.02	70.77	2.23	76.0	6810.00	1225.00	496.00	7.13 30.33	1487.00	0.10	15.00 110	110.00 280.00	90 0.15	8	0.15	9.0	7 0.02	13.50	2.00	15.50	1,	6.49	2.00	2102 348	99.87	96.65	99.91	99.45 69	7 4.69	M.22 72	73.58
TO INT-EVENT 11)		\$80.00		30.60	3.60		6900.00	4400.00	\$45.00	31.00	1447.50	0.13	5	124.00 300.00	00 0.17	0.20	0.14	0.02	12 0.01	20.10	7.00	22.10	2.73	9.00		1600.00	99.86	•	99.89	99.19 61	61.25 43	43.20 29	29.46
TO UT AND AT EVEN. 12:		20,50	7 22	7, 72	174	1.65	6692.31	4712.50	764.00	7.33 26 57	1337.83	41.0	24.00	180.00 316.00	037	0 27	15.0	50.0	50 0 03	8	2.05	*	14	4.42	.,	2457 96	94 74	95.21	94.76	98.68	52.63 85	85.30	52.42
				ļ.	l	ı	L	l	1	1	L			1					П	L						ł	ı	ı	ı	ı	L	ı	1

Target H			n w w α ψ	****
Ž	2222222222222	######################################	************	555555
Partiele	2022222 33		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	<u>និន្ទិទិនិទិ</u> និ
Turbidity	00 00 00 00 00 00 00 00 00 00 00 00 00		00 d 0 d 0 d 0 d 0 d 0 d 0 d 0 d 0 d 0	6666000
R Ge	- 600 / 87 887 808 808		# 1 # 1 # 2 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	222222
RO Feed	######################################		22222222222222222222222222222222222222	555555
PDC (psi/gpm ¹ ? Slage 1	\$ C \$ 2 2 2 2 2 2 2 5 5 5 5 5 5 5 5 5 5 5 5	MRNAR 58 48 8 4 8 8 4 8 8 4 8 8 6 6 6 6 6 6 6 6	\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	8888888
Oraș (pul) Stege 2	<b>中国中央工作工作的</b>	***************************************	を見るとなれてこことによるなのののののも	222222
Stage 1	282222222242284	\$2\$\$\$2#FV###############################	物の作品でいたなどのはないないないできます。	222222
Conc	540 670 670 670 860 1150 862 2165 272 282 282 282		817 820 820 820 830 830 830 874 874 878 878 878 878 878 878 878 878	55 55 55 55 55 55 55 55 55 55 55 55 55
essure (kPs)	907 902 902 903 917 916 916 916 917 2186 634 484	44857788977777986648648886664888888888888888	######################################	1888321
1	1035 1032 1033 1035 1035 1030 1030 1030 1030 1030	*5=====================================	808 810 820 820 823 823 823 823 834 836 836 836 837 836 837 836 837 836 837 836 837 836 837 836 837 836 837 836 837 838 838 838 838 838 838 838 838 838	625 623 623 623 623
Control	· 《 · · · · · · · · · · · · · · · · · ·	\$ 4 8 4 5 4 5 4 5 5 5 5 5 5 5 5 5 5 5 5 5		2000000
To Per	# # # # # # # # # # # # # # # # # # #		######################################	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
]	25555557555 255555755555555555555555555	NNNOTY NO SYNAMONO DE L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE CONTRA L'ALLE C	65000000000000000000000000000000000000	222222
Concentrite	55515535535 251	•.•••••• <b>:</b> 88888.aaaaaaaaa.		4 4 4 4 4 4 4
F F	00000000000000000000000000000000000000	100000000000000000000000000000000000000		****
Rew Free	សមា ស្ថា បា បា ២ ២ ២ ២ ២ ២ ២ ២ ២ ២ ២ ២ ២ ២ ២ ២		医最级性 化了了了 化物物合物 化低性电子 化自然电台 化一口口 化邻分替氏管 化多种合物 医自身 医自动 医血管	0000000
Samplitabre	排放政治的公司 经经济股份 电电子 经经济	表面的需要素质量更更多更多的表面的表面的现在分词的现在分词可以不是有的的的表面或用,不是有效的。		232222
USicm) Tot Perm	****		######################################	1111111
Cone Cone	52.8 56.52 55.72 55.72 55.72 56.06 56.06 56.06 56.06 57.46 57.46 56.06 57.46 57.46 57.46 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 56.06 5		58.88 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000 6.000	3400 3503 3503 3503 3500 3500 3500
Interniege	13.00 13.70 13.70 13.00 13.00 13.00 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13 14.13	######################################	6 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	25 25 25 25 25 25 25 25 25 25 25 25 25 2
]	122 123 124 125 125 125 125 125 125 125 125 125 125		# 50 50 50 50 50 50 50 50 50 50 50 50 50	1500 1602 1602 1612 1630 1635
Date/Time	422-199 1-37 PM 4222-1990 1-47 54222-1990 1-47 54222-1990 1-47 54222-1990 1-27 54222-1990		0.525 (1990 of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 25 cm) of 2	05/20/1999 8 W 05/20/1999 8 W 10 05/20/1999 8 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/1999 W 10 05/20/199 W 10 05/20/199 W 10 05/20/199 W 1
Time (krg)		80666666666666666666666666666666666666	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	233.77 256.11 258.41 258.41 258.41 260.41 260.41
Event	STANTUP	Defense of Tables	on Circ Ad	Dec to BOX
3	≪		<u> </u>	~
Ľ				

(1 10 1 **ebs** o

	<del></del>		
E:::::::::::::::::::::::::::::::::::::		**************************************	
2 5 5 5 5 5 5 5 5	56558888****		FEEEEEEEEEEEEEEEEEEEEEEEEEEEEEEEEEEEEE
25 t 19 25 25 25 25 25 25 25 25 25 25 25 25 25	4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	\$\$1200000000000000000000000000000000000	988888888888888888888888888888888888888
7 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0			
1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	86888888888888888888888888888888888888	20100000000000000000000000000000000000	\$8555588835558888886555888888555588888888
	22 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		######################################
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	8 8 4 8 8 8 8 8 8 8 8 8 8 8 8 8 8 4 7 7 7 7		***************************************
2222222	**************************************	びいることのできるとと、「「」、これできたこととの関係的語彙が	RECECCORRECTED OF A TAX A A A A A A A A A A A A A A A A A
*******	***************************************	び物味ははいいまはいけいまままとうティックティネを対な対対対対	**************************
	\$ 2 3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2	33333333333333333333333333333333333333
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		200 C C C C C C C C C C C C C C C C C C
2555555	524 524 525 526 526 526 527 527 527 527 527 527 527 527 527 527	734 908 908 908 907 907 907 907 908 908 908 908 908 908 908 908 908 908	
200 000 000	7 / / / / / / / / / / / / / / / / / / /	**************************************	**************************************
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	00000000000000000000000000000000000000	от така така така така така така така та	*NNN****NNONAGONOOGEE##000000000000000000000000000000000
2222222	282822222222222222222222222222222222222	2.000011011	000000000000000000000000000000000000000
4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4			8000 0
	うちゅう (m) (m) (m) (m) (m) (m) (m) (m) (m) (m)	とうと聞いなととと、自然をおとれて自然なととなった。 かんきゅうかん ちょうしゅう 中央 中央 日本 アイカル 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本	
			RECEREREREREREREREXXXXXXXXXXXXXXXXXXXXX
Sample   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100	R 表 R 公 A R 公 R 化 R 公 R R S R R S R S R S R S R S R S R S	**************************************	***************************************
E 20 9 3 5 8 5	2	- F # 8 8 1 2 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	5:72528588\$T\$584858688;916889668782866888
972 972 972 972 972 973 973 973 973	1558 1558 1558 1558 1558 1558 1558 1558		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
2005 2005 2005 2005 2005 2005 2005 2005	2772 2772 2772 2772 2772 2772 2774 2772 2774 2772 2774 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2772 2	# 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	
12333233		\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	
E 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011999 1 0 00011	1999 1999 1999 1999 1999 1999 1999 199	
		**************************************	
Stage Event		Const Area (Stope 1	
<u> </u>			

Page 2 of 17

1	4484-	<u>81</u>	
Front	of Channey (Cities and Burge 1 or Bit.  Note And Shape 1  N BF; Caustle Stage on BF()		<del>-</del>
The least	28.5		60.00 00 00 00 00 00 00 00 00 00 00 00 00
Data/Time	06/08/1999 10 41		0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000
1	1713	<b>3393936488</b> 110000000000000000000000000000000000	1497 1539 1537 1537 1621 1621 1668 1586 1586 1586
Interstage	Ř	CHARAARAARAARAARAARAARAARAARAARAARAARAARA	3095 2699 2699 2717 2717 2717 2717 2717 2717 2717 27
Cone	X	######################################	0110 0110 0110 0110 0110 0110 0110 011
Tot Perm	Ē	SECRETARY SECRECASIONS OF THE SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRETARY SECRET	និង និង និង និង និង និង និង និង និង និង
Samplivalue	×		2017年第第四部特別日本北部
Rea Feed	7.5.	***************************************	************
I.		23111111111111111111111111111111111111	としてはなるななのでもなられない。 しょうしゅう ないごう でんぱん できまる はんしゅう はんしゅう はい はい ない はい はい はい はい はい はい はい はい はい はい はい はい はい
- Shreening			4 4 4 4 4 5 5 5 6 6 6 7 7 7 7 7
2	ē	ANNUNNUNNUN TOTTATTÄTERARRERRERRERRERRERRERRERRERRERRERRERRER	\$5555555555555555555555555555555555555
ŭ L			
T Per		3	153 788 788 788 788 788 788 788 788 788 78
Presector (RPs)	1689		
20	<del>-</del>	######################################	352222222222222222222222222222222222222
Stage 1 Stage 2	2		***************************************
Slage 1	8.		*************
2	6.26		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
E a	~ ~ ~	RESTRICTED FOR THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE STATE OF THE	22222222222222222222222222222222222222
Ture dity	20	30253330286355353555557785465658452557788463265778846326578787878787878787878787878787878787878	24 - 44 48 2 48 48 48 48 48 48 48 48 48 48 48 48 48
a section	Ē	######################################	%#38F#55559 <b>8</b>
ž	•	DO::::::::::::::::::::::::::::::::::::	У <u>л</u> иниментована В
	<b>\$</b> 1	***************************************	各外有所有 母母 化合金 医内内 电电子 医多丁乙丁乙酰 医络性性 经 医 电 电 电 电 电 电 电 电 电 电 电 电 电 电 电 电 电 电

Dags Johns

A H	::::	* = 0 * 0 * 0 * 0 * 0 * 0 * 0 * 0 * 0 *	***************************************	ସା ମଧ୍ୟ ସ୍ଥା ସମ୍ପ୍ରମଣ ସମ୍ପ୍ର ଅଧ୍ୟ ଅଧିକ ଅଧିକ ଅଧିକ ଅଧିକ ଅଧିକ ଅଧିକ ଅଧିକ ଅଧିକ
No.				ବ୍ୟର୍କ୍ତ ବ୍ୟବ୍ୟ ବ୍ୟବ୍ୟ
Particle	¥ \$ § §	256888888888888888888888888888888888888		\$\$ ; \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$
Turbidity	2000	**************************************		
e a	225		2.00.00.00.00.00.00.00.00.00.00.00.00.00	## 0 # P # 8 # 4 4 # 6 # 6 # 6 # 6 # 6 # 6 # 6 # 6 #
RO Fee	2222			252222222222222222222222222222222222222
PDC (per/gpm )	2427			######################################
Drop (pel)				
Predoute Stage -	====	2002200220022222222022 <b>0</b> 02 <b>0</b> 0202222		***************************************
teurs (MFs)	1828	**********************	9879886G\$178770:09846481:57209884860:57757514888	***************************************
1	2583	## ## ## ## ## ## ## ## ## ## ## ## ##	\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
Cone	2222	0/ = 44 0 = 44 4 4 4 4 4 4 4 4 4 4 4 4 4 4		у и в и и и и и и и и и и и и и и и и и
Flow (Lpfn)	****			**************************************
1	2772	\$255 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	000 1 1 1 0 1 1 0 0 1 0 0 0 0 0 0 0 0 0	p. 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
Conceptions	****	<ul><li>単本のの口口口口口口口口口口口口口口口口口口口口口口口口口口口口口口口口口口口</li></ul>		*****************
F 2	-250	# \$\\ # \$ # \\ # \$ # \$ # # # \$\\ # \$ # \$		физиканафицикафици физикари
Reve Feed	2222			
Sompthy aire	2222	######################################	ទនាក់នុកកាណក្នុកក្នុក នេះ ២ ខាន់ លុក លុក ខាងខាង គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ	***
L. Perm	2322	<b>新江鄉和內國內內公司內國鄉南國都都在公司公司的公司公司公司公司公司公司公司公司公司公司公司公司公司公司公司公司公司</b>	K K B & C & E & E & E & E & E & E & E & E & E	10. 10. 10. 10. 10. 10. 10. 10. 10. 10.
Cane	2 2 2 2	**************************************		2547 2547 2547 2547 2647 2647 2647 2647 2647 2647 2647 26
the reference	2615 2615 2631 2631			2535 2541 2641 2662 2663 2663 2663 2663 2663 2663 266
Į	3833	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
and line	2 2 2 2	100 (100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100 to 100	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	100 (100 (100 (100 (100 (100 (100 (100
		<del></del>		
**				
-				
1	L_	<del></del>		

Page 4 of 17

	:	てきょうことできますののはち からられるとう おか	\$ 20 40 70 70 70 70 70 70 70 70 70 70 70 70 70	\$88855888888888888888888888888888888888
	•	*********	66666668666688666 6178*8	\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$
	ž	2222288222223 2222222222222222222222222	96985358732182537 934 95	
	),	7.467.000.000.000.000		
	• 16	***************************************	22222222222222222222222222222222222222	
	, ii	22 337527532		
	175	200000000000000000000000000000000000000	・ はないできる。 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまでは、 ・ はないまではないまではないまではないまではないまではないまではないまではないまで	**************************************
			1937年 医医性肠管管性结合性结合性	
	ε	X=:=============	######################################	
		100111111111111	\$5555666666666666666666666666666666666	######################################
			# # # # # # # # # # # # # # # # # # #	\$886,63612366657123666666666666666666666666666666666666
	È	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	88888888888888888888888888888888888888
	1.0		EGG 251 151 151 151 151 151 151 151 151 151	######################################
	•			77811111111111111111111111111111111111
		5545565556546474 44	888888888888888888888888888888888888888	2-78-978-9788888888888888899999999999999
	5.	अ क के व क क के व क क क क क क क क क क क क		20 X 8 X 8 C 7 D 7 D 7 C 7 D 7 D 7 X X X X X X X 2 D 7 D 7 D 7 X X X X X X X X X X X X X X
		自己不不不不 医肾盂性脓肿 经 化谷		
	×.	*************	**************************************	ERILICERRERRERRERRIRRERRERRIRRIRRERRERRERRERRE
	æ	医克尔里奇耳氏征 计计算 计计算 化二甲基苯甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基	報報の日本 1 日本 1 日本 1 日本 1 日本 1 日本 1 日本 1 日本 1	эллын аддойбалып аччүнд на надалдыкалы өзүү кан түзү эмпетулга фаса
	ş.	***********	08::::::::::::::::::::::::::::::::::::	18:50:0:::::::::::::::::::::::::::::::::
I CPRIPATE AND CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL OF CONTROL	3510	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	88 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	2500120030100101000000000000000000000000
ARTITUTE STATE AND CONTROL OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF THE PROPERTY OF	3510		2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	
	₹.	1782 (688) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779) 1799 (779)	1770 1811 1811 1811 1811 1811 1811 1811	
	3 8 8	0.00 (1990) 1990 1924 1934 1934 1934 1934 1934 1934 1934 193		0.000 (1990) 1
TENTON DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DEL CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA CONTRACTION DE LA C	828	8888888888888888	SERVERERE PREFERENCE PROFES	777777777777777777777777777777777777
Back Stages Colors  1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1			ėξ ∉	<del>{</del>
				· · · · · · · · · · · · · · · · ·

1	2 52 525555	**	在在下面下面的人。 全面内的中部的图片
Į	P • P # P # P # P # P # P # P # P # P #		<b>₽</b> ♥ ☆ ☆ ☆ ☆ ☆ ☆ ☆
Particia		\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	¥ <b>3</b> \$ \$ \$ \$ \$ \$ \$ \$ \$ \$
Turbiens			~~~~~
S S	9 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	48 5555588868886	2443444554
NO Fee		88 455388888888	22222222
PDC (pre/ggm 1)		** **************	7 A A A A P A P A P A P A P A P A P A P
Stage 7			85535353
Stews 1	*1************************************		20111111
*	************************************	2	257 478 957 977 978 986 986 987 888 988 988 988 988 988 988 988
Internitive	######################################	65.2 65.2 65.2 65.3 65.3 65.3 65.3 65.3 65.3 65.3 65.3	21.2 25.5 25.5 26.5 26.5 27.5 27.5 27.5 27.5 27.5 27.5 27.5 27
1	<b>35234014601446666565665846618</b> 772286868468868848847222164868888	8 C	65.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5
ě			ខណ្ឌពស្ធិចាក់ជាត សម្មេសមិត្សសម
Flow (Lpm) Tot Perm		N	# # 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Į			* 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
Concentrate		20000000000000000000000000000000000000	<b>有事情有效的有价格</b> 有用表写为完全的
1.4 OF	**************************************	ба чения чения переда Съ. — — — — — — — — — — — — — — — — — — —	\$\$\$\$\$\$\$\$\$\$\$ 
Par Fee		0.00 DECEMBER PROFES	**********
Samplifyahre	- 発表を考別的なな対象性になる数では重要されながあるとのなった者はあれたがおいからことからようなからなったのではなかのであるというできた。 -	C	\$\$\$\\$\$\\$\$\$
Allem) Tot Perm	\$2856 <b>918828688</b> 68889918888888888888888888888888888	22 55588575558	# 5 \$ \$ \$ \$ \$ \$ \$ \$ \$
Come		4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	25 C C C C C C C C C C C C C C C C C C C
Internation		25 00 00 00 00 00 00 00 00 00 00 00 00 00	2813 28130 38130 38130 38130 38130 38130 38130 38130 38130
Į		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	X 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
Outs/Time		200 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	200 000 000 000 000 000 000 000 000 000
22		.444444444444444444	**************
free.			
ı			
ت		<del></del>	

Page 4 of 17

1				X = 0 = 0 = 0 = 0 = 0 = 0 = 0 = 0 = 0 =
ā	心と心をするとととなるとの色とととともの		~~*::::::::::::::::::::::::::::::::::::	C. • • • 120 DD C DD C DD C DD C DD C DD C DD C DD
Particis	\$583 8583 553 553 553 553 553 553 553 553	# 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	<b>88</b> 8 8 8 8 8 8 7 <b>8</b> 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	***************************************
Turbicity	N 7 W N W P M M M M P M M A A A A A A A A A A A A	# m # # # # # # # # # # # # # # # # # #	N N N N N N N N N N N N N N N N N N N	
Ren	***************************************	*******	233322222333333222222 23332222222233333222222	483 & & & & & & & & & & & & & & & & & & &
RO Feed	HARARARARARARARARARARARARARARARARARARAR	******	***************	
Stage 1	\$4\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	79-17-17-17-17-17-17-17-17-17-17-17-17-17-	8768888670777777	
Drup (ped) Mage 2	いないでは我は我は我はななななない。	988888	**********	\$885.1333.1331.1311.1311.131.00000000000000
Pressure Steps -	2.85.*57.0000000000000000000000000000000000	22222000	<b>海海海通过水汽油运运运运运运运</b>	
3	**************************************	\$23222111	£286898888888866688	868888888888888888888888888888888888888
Inharatage	068 653 977 977 977 961 961 962 963 976 976 976 976 976 976 976 976 976 976	625 630 630 631 631 725 727	3 6 3 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	(\$895133558058668588655888888888888888995555555555
1	753 574 774 774 775 578 578 578 582 582 582 582 682 683 683 683 683 683 683 683 683 683 683	725 727 727 727 727 727 800 800 801	623 623 623 611 611 611 620 620 621 621 621 621 621 621 621 621 621 621	
Conc	9 4 4 9 4 4 9 4 4 9 4 4 9 4 4 9 4 4 9 4 9 4 9 4 9 9 9 4 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	FFFFFFF	**************************************	^^\~ + ###################################
Flow (Lpm) Tot Perm	のていまなはならなるならなるなるできている。	9 4 5 8 8 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9		
1	15 5 5 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	7.622.232323		***************************************
Concembate	<b>化物质 医线性蛋白 医腹部骨骨 等于了才不见 服 化丁丁基基基基基基基基基基基基基基基基基基基基基基基基基基基基基基基基基基</b>	44 64 64 64 64 64 64 64 64 64 64 64 64 6	ちょうちょうしょうしゅう ちゅうしょくてく ちゅうしゅう ちゅうしょうしょう ひゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅう	255555555555555555555555555555555555555
HO Feed		<b>医生态人人名约之的人</b> <b>医生物的食物物</b> 不分别分	5 C G 4 C 4 C G 4 4 C G A G A A A A A A A A A A A A A A A A	200000000000000000000000000000000000000
1	医胃炎 医皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤皮肤		**************	::::::::::::::::::::::::::::::::::::::
Samplivalve	883855465554888855	¥#3\$\$3\$87	2	ರ್ವತಕ್ಕೆ ನಿಷ್ಣಿಯಿತ್ವ ನೆಗೆಗೆ ಸಸಸಸನಗಳು ಸಿಗೆ ಪಿರುತ್ತಿಕೆ ಪ್ರತಿಯ ಪರಿಕಾರಕ ಅಧಿಕಾರಿ ಕಲಕ ಕಾರ್ತಿ ಪ್ರವಹಿಸಿ ಸೆಸೆ ಸಿಗೆ
Tof Perm	B # 8 5 5 7 8 8 8 8 8 8 5 5 5 5 5 5 5 5 5 5	**********	. 20 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	>***801236888666666666666666666666666666666666
Conc	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	3886 3867 3722 3722 4738 4738 4738 4738 4738	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	
Con	25 25 25 25 25 25 25 25 25 25 25 25 25 2	2921 2970 3011 1126 1197 1197 1457 1775 1975	20 20 20 20 20 20 20 20 20 20 20 20 20 2	
1	1827 1827 1827 1827 1828 1828 1828 1838 1838 1838 1838 1838	1655 1672 1784 1791 1791 1701 1701 1701	1673 1683 1684 1700 1700 1700 1700 1700 1700 1700 170	
Date/Time	2010-091-091-091-091-091-091-091-091-091-	255555555	0773-1988 6.0 0772-1989 1.0 0772-1989  - 22 - 22 - 22 - 22 - 22 - 22 - 22 -	
		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	555 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR (558 PR	
1	ŀ	A Largest philoconc. a		Chris Anid (Stopped 2)
1	1	13		•
Ľ	1			

Page 7 of 17

	7
	[maj maj]
	Data/Time
	:
	history
	Conductive
***************************************	(uthin)
	Samplivere
	RG Fall
***************************************	Concentrate
	i
	Flow (Lan
ANALON MARINE NO 10 10 10 10 10 10 10 10 10 10 10 10 10	Come
anarananan kanan kanan kanan kanan kanan anan kanan kanan kanan kanan kanan kanan kanan kanan kanan kanan kanan	ī
	Procesure (ki
	2
,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	Pressure Stage 1
	Drop (sed)
338995855555599988355558585858588	POC (padigram )
	70 -
************************************	2
	T-umbheldh
	ſ
122323120232340272324023340233403234 7233403333333333400433004330043340433404	Particle
**** **********************************	ļ. ļ

Page 1 of 17

¥
4524264544646485404865408888893888446466888884416666666666888856886688568888888888
495235608257778805579160888538877055888888888888888888888888888
**************************************
全質で作品着ななってこうとうからかられるようのは、またないななななななななななななななななない。 
***************************************
xxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxx
11;0;4442;45444;4601;10;688;1144;10;6;6;6;6;6;6;6;6;6;6;7;6;;;;;;;;;;;;;
25288888885288888888888888888888888888
1
######################################
801110101010101010101010101010101010101
48553888488488888933555889888835558888888888
808888888888888888888888888888888888888
20 5 2 3 4 4 4 4 4 5 5 4 4 4 4 4 5 5 5 4 4 4 4
36555555555555555555555555555555555555

	2084 79 2085 74 2085 74 2081 79 2071 74 2072 74
	08/3/1990 15.35 08/13/1990 15.35 08/13/1990 17.35 08/13/1990 27.35 08/13/1990 27.35 08/13/1990 27.35 08/13/1990 27.35
######################################	168111
######################################	282 287 287 287 287 287 287 287 287 287
388458888888888888888888888888888888888	\$ 6 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
:	8 2 2 2 2 2 2
######################################	12 2 2 5 5 5 <b>5</b>
######################################	222222
:23224:3242525557533252555555555555555555555555	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
Z_22ZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZZ	2111111
######################################	200000
	*****
######################################	8822823
######################################	9993338
	*****
· · · · · · · · · · · · · · · · · · ·	
	1 667 1 7 66 1 7 67 1 7 6 1 7 6 1 7 6 1 7 6
**************************************	******
***************************************	****
	222222
	883333
	:======

Page 10 of 12

	ļ
	08/20/1998 14 16 08/20/1998 14 33 08/20/1998 14 33 08/20/1998 17 33 08/20/1998 17 33 08/20/1998 17 33 08/20/1998 20 18 08/20/1998 20 18 08/20/1998 21 33 08/20/1998 21 33
	3022 3022 3183 3184 3187 3187 3187 3187 3187 3187 3187 3187
::0:::::::::::::::::::::::::::::::::::	5007 3007 5194 5194 5172 5172 5174
ក្នុងសម្រេចស្រាប្រកួទ្ធី ដូច្នឹងសមានផ្លូវស្ថេចការសស់សមាសមាសសម្រេចស្រុខការស្វាស់សមាសម្រេចស្រុចសម្រេចសម្រេចសម្រេច សមាស្រុសសម្រេចសម្រេចស្រុកសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចសម្រេចស	*********
***************************************	253284111
***************************************	:::::::::::::::::::::::::::::::::::::::
	**********
	* * * * * * * * * * * * * * * * * * *
	555555555
**************************************	2 2 3 2 2 2 2 2 2 2 2 2
	######################################
808888873388888888888888888888888888888	* # # # # # # # # # # # # # # # # # # #
***************************************	
:::::::::::::::::::::::::::::::::::::::	
	តី ឌី គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ គឺ
	******
	****
	200000000000
1999-9-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-	\$25522222
	:::::::::::::::::::::::::::::::::::::::
	********

Page (1 of 17

	_ :			į
	Acid Sings 100 97 and Sings 2 on M4 Acid France Fallon on M5; Restart on at 2 PM	land south	TO design date of	
20		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	31183111111111111111111111111111111111	240175
	1999	17. 1669.17.00 18. 16. 16. 16. 16. 16. 16. 16. 16. 16. 16	007700710	3
	å á	1 8 2 2 4 4 4 4 6 4 6 8 2 5 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6		Ě
100 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2300	2920 9100 1106 200 200 200 200 200 200 200 200 200 2		ĩ
\$25 \$25 \$25 \$25 \$25 \$25 \$25 \$25 \$25 \$25	ĝ %	3555 5983 5785 5785 5795 5795 4477 4477 4477 4477 4477 447	28884488888888888888888888888888888888	1
型 編 表 2 2 2 2 2 1 1 1 1 2 3 2 1 1 1 1 1 1 1 1	3 2	2 Q Q Q B B B B B B B B B G Q Q G G G S S S S S S S S S S S S S S	V 4 M 4 4 4 M 8 8 8 8 8 8 8 4 4 4 5 5 6 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	. =
在在各個的項目的 化二氯甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基甲基	ē E	*************	**************************************	
	2 3	**************************************	37233333777777733723333733733723773377	
######################################			######################################	
スピーテロスト とうちゅう カント・ファン とくしょう できました できかい ストン しょう アントン しょう できまる ままま かんしゅん アントン ファント マーチ・アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・	· ·	おものもちもものものもちもられること アンコンファシャール ちゅうちゅう ちゅうしょう アンコン	***************************************	
	ž 9		\$5.4.\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	Ē
01111111111111111111111111111111111111	: :	名名に 20日本の日本の日本の日日日日日日 20日 20日 20日 20日 20日 20日 20日 20日 2	######################################	112
56286262626262111111212123666666	i ;	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	500000000000000000000000000000000000000	::
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	7 S	7 9 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	000000000000000000000000000000000000000	73
3533335535535553355735573555	2 3	77 77 77 77 77 77 77 77 77 77 77 77 77	444444444688668888888888888888888888888	892
\$ 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	<b>*</b> §	2888888888888323	825888888888888888888888888888888888888	ξĚ
000122222222222222222222222222222222222	.s =	% ಸರವಾದ ಪರವಾದ ಪ್ರವಿಷ್ಣ ಪ್ರವಿಷ್ಣ ಪ್ರಕ್ಷಣ	22.22.23.24.20.00.24.20.24.24.24.24.24.24.24.24.24.24.24.24.24.	
ଲେବର ବଳ ବଳ ଓ ପୁସ୍ତ ପ୍ରତ୍ତଳ ମଧ୍ୟ ନଳ ଓ ପୁସ୍ତ ପ୍ରତ୍ତ ହେଇଥା । ଜେବର ବଳ ବଳ ଓ ପୁସ୍ତ ପ୍ରତ୍ତଳ ମଧ୍ୟ ମଧ୍ୟ ବଳ ଓ ପୁସ୍ତ ପ୍ରତ୍ତ ପ୍ରତ୍ତ ହେଇଥା	. 23	ညီကေတည် <b>ခုစာယာသာယာသလယ္သလက္</b> သည်မ	•••••••	; ä
** 8 5 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	<b>6</b> 3	222288888888888888888888		2 8
486666655x2884228882258825888	= =	2222222222222222222	######################################	e ¥
5825555554444445546555555555555555555555	<b>5</b> 5	******************		3 25
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	0 0 N w	22552225232222222		3.2
### ##################################		221212121222222222	38,447,668,830,800,800,800,800,800,800,800,800,80	3 2
800000000000000000000000000000000000000	= •	+11114 + + + + + + + + + + + + + + + + +	********	: =
				::

41 Jr. 2. obro

s		<del></del>				T
<u> </u>	<u> </u>				<u> </u>	+
The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s		7 Page 2	,	nd in Feed P	į	ī
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	779 8 8 8 7 7 7 8 8 8 8 7 7 8 8 8 8 8 8	2775 64 2776 30 2778 30 2780 30 2780 30 2782 30 2782 30 2784 30 2784 30 2784 30 2784 30	2763 98 2763 98 2763 98 2764 60 2766 60 2766 60 2766 60 2760 60 2760 60 2771 60 2771 60 2771 60 2771 60	2740 16 2740 18 2750 18 2751 18 2752 16 2753 16 2753 16 2754 18 2756 18 2756 18 2756 18	276 G G	2742 18
GP16-1999-1-27 GR-46-1999-1-27		DW12/1998 6 29 DW12/1999 0 06 OW12/1999 10 06 OW12/1999 10 08 OW12/1999 12 08 OW12/1999 13 08 OW12/1999 13 08 OW12/1999 13 08 OW12/1999 15 08 OW12/1999 15 08 OW12/1999 15 08 OW12/1999 15 08 OW12/1999 15 08 OW12/1999 15 08	DRY 1/1999 1 0 29 DRY 1/1999 1 10 29 DRY 1/1999 1 12 19 DRY 1/1999 1 10 29 DRY 1/1999 1 10 29 DRY 1/1999 2 1 29 DRY 1/1999 2 1 29 DRY 1/1999 2 3 29 DRY 1/1999 2 70 DRY 1/1999 2 70 DRY 1/1999 2 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70 DRY 1/1999 3 70	ORY 11999 2:57 ORY 11990 4:57 ORY 11990 4:57 ORY 11990 4:57 ORY 11990 8:57 ORY 11990 8:57 ORY 11990 8:57 ORY 11990 8:57 ORY 11990 8:57 ORY 11990 8:57 ORY 11990 8:55 ORY 11990 8:55 ORY 11990 8:57 ORY 11990 8:55 ORY 11990 8:55	25 - 26 - 26 - 27 - 27 - 27 - 27 - 27 - 27	Deta/Time 09/10/1999 20 57
178) 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014 1 2014	11 12 12 12 12 12 12 12 12 12 12 12 12 1	7 7 7 7 8 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8			E 5 1 1 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	8
37 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20 May 20	375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 375.00 37	100 100 100 100 100 100 100 100 100 100	3394 3394 3508 3952 4160 4501 4501 4501 4506 4500	4314 4314 4314 4314 4314 3314 3314 3306 3421	3427 4427 4427 4427	100
2000 2000 2000 2000 2000 2000 2000 200	\$ 5 1 2 4 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	4 8 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	######################################		37 30 30 30 30 30 30 30 30 30 30 30 30 30	5
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	· 2.5 2.8 2.8 3.5 2.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3	253255333555	8 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1 1 1 2 2 2 2 2 2 2 3 2 3 2 3 2 3 2 3 2	52523	78
\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	488000	· 自己基本的基本的	***********	**************	55233	25
て着するのは、なりでも自動をなる中ではなっていません。	777777777777777777777777777777777777777	222222222	7777777777777777	72222222222	2222	7.6
3.55 A S S S S S S S S S S S S S S S S S S	⊼ k k k k μ k k k μ φ k θ μ δ φ φ μ θ φ φ θ α φ δ σ δ δ δ δ σ δ δ δ δ δ δ δ δ δ δ δ δ	# # # # # # # # # # # # # # # # # # #	,		22222	
84381480257258073873878878	228755888888888888888888888888888888888	() 医甲基氏反射 医甲基基氏 () 医甲基氏病	2222222222222	***************************************	22222	7.2
3343453344634546355463554655 3255000000000000000000000000000000000	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	************	*************	222222222222	55555	ŝ
1		2222222222	555555555555555555555555555555555555555		55555	0.6
					****	-
77.4 F. Z. Z. Z. Z. Z. Z. Z. Z. Z. Z. Z. Z. Z.		227722275	20 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	744 8 8 7 7 7 7 8 8 7 7 7 8 8 7 7 7 8 8 7 7 7 8 8 7 7 7 8 8 7 7 7 8 8 7 7 7 8 8 7 7 7 8 8 7 7 7 8 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7	55555	:
		35 55 55 55 55 55 55 55 55 55 55 55 55 5	944 881 881 881 881 881		25566	736
\$ 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4		********	28222333333323	*5584584868	2 2 3 3 3 3	8
*****************	*****************************	*********	=======================================		- ::::::::::::::::::::::::::::::::::::	-
435466446652363543652366	0 d d e n e e n e e e e e e e e e e e e e					,
X	7722287628886667778866666676688888	1 2 2 2 2 2 2 2 2 2 3 3 8 2 3 8 1 8 2 8 2 8 2 8 2 8 2 8 2 8 2 8 2 8 2	1882551882	1 8 4 4 4 5 4 8 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	# # # # # # # # # # # # # # # # # # #	
*****************	********************		262222222222		52555	2
23523488322388845235688233			3,3,3,5,2,2,2,2,2,2,2,2,2,2,2,2,2,2,2,2,	188444533333333	*****	Ŀ
	300000000000000000000000000000000000000	000000000000000000000000000000000000000		00000000000000000000000000000000000000	22222	0.7
######################################	\$\$2:52:22:23:38:25:53:22:32:32:32:32:32:32:32:32:32:32:32:32	14481424488	*******	2811622168	2 2 2 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	ź
**********************	000000000000000000000000000000000000000			:::::::::::::::::::::::::::::::::::::::	85865	ā
A IV IV IV IV IV IV IV IV IV IV IV IV IV	~ D D OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY OF THE OWN DAY			3. 17 18 18 18 18 18 18 18 18 18 18 18 18 18		2

Page 13 of 17

	C P P P P P P P P P P P P P P P P P P P	- Francisco
306.6 57 306.6 57 306.6 57 306.6 50 306.6 50 306.6 50 306.6 50 306.6 50		7919 FZ
999		Deta/1999 2 43 09/18/1999 2 43
1677 1677 1678 1678	84495511866888884841191818584888555 34488448888838888888888888888	872
37 ta 3690 3675	***************************************	3400
77.5 7.6	466166486494444661561818686546666	£ 5
884 85	\$\$1143#\$\$28886\$\$4\$3###\$\$2568###\$#################################	2 0
::::::::::::::::::::::::::::::::::::::	こうてきさらばらればないないには不かなこのなれなの後でなるのはなられない。 スカガルバネトだは不満になったがはははなればればればればればればればればればればればればればればればればないないないない	- :
77.5		7 2
222 22	[#####################################	55
	\$#####################################	2.5
44 4 5 5 <b>5</b> 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		ž 2
555 55		5 5
		::
228 22	# \$ # \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	28
700 77	A35388384422000288004837534248422008	9 8
482 65 65	######################################	8 8
	***************************************	= = =
	**************************************	= 0
krr is		1.72
1995 22		: = = [
::88 88		18 =
2010 -0	228770177877878787878787878787878787878787	222
230 110 98	15*8*8*8*8*9*4* ***884****884 66**;848\$* 65528453882788888 6288253388888888888888888888888888888888	: E =
3442 44	♥♥♥₹₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽₽	:== i
5 d		:  3

Page 14 of 17

:		
\$ <b>4</b>	the in Finance process of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the contract of the	
3300 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 St 3350 S		1100 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
1000/1999 11 19 1000/1999 12 02 1000/1999 12 02 1000/1999 18 02 1000/1999 18 02 1000/1999 20 02 1000/1999 20 02 1000/1999 20 02 1000/1999 20 02 1000/1999 20 02 1000/1999 20 02 1000/1999 20 02 1000/1999 20 02 1000/1999 20 02		************
1778 1784 1786 1790 1808 1775 1748 1772 1873	88.330.08888888800000000000000000000000	1600 1712 1712 1713 1714 1714 1714 1714 1714 1714 1714
3604 3700 3730 3739 3628 4044 3635 3711 3715 3711 3597 3597 3530 3420		3721 3765 3432 3432 3743 3874 3770 3898 3777 3880
5983 7745 7793 7397 7443 7443 7443 7443 7443 7443	161681111111111111111111111111111111111	7556 7556 7557 7557 7557 7557 7557 7557
122 122 123 124 124 125 127 128 128 128 129 129 129 129 129 129 129 129 129 129	877777777777777777777777777777777777777	#25 # # # # # # # # # # # # # # # # # #
282888888888888888888888888888888888888	ឯកក្រុកពុក្រុកកុខ តុស្សភ្លូក្នុកក្រុកក្រុកក្នុងបទិក្សក្សក្នុងក្នុងកុខសុសក្នុងក្នុងកុងក្នុងក្នុងក្នុងក្នុងក្នុង	212288888
7777777777777 20000077	***************************************	333222333
	252002000000000000000000000000000000000	**************************************
7. 保存者とことできましてでなるのとは	022222222200022022200222022222222222222	**************************************
**************************************		545465465
55555555555555555555555555555555555555	595888558868588885888888888888888888888	20000000000000000000000000000000000000
		2222222
9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	\$\$2446383348385858888866688338838838888888883388388888333888888	5122322331
4 7 2 2 3 3 4 7 7 2 2 3 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	\$125 <b>68886848186986848686</b> 848 <b>8</b> 084888888888888888888888888888888	2 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
569 592 593 704 704 725 727 727	338548385888333388888888888888888888888	772 773 773
	223223333333333333333333333333333333333	1012103111
******		*********
111111111111111111111111111111111111111		2 % 2 ប៉ុន្តិ
2222222222222	\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	28282288
255525555555	%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%%	2252888335
-00000000000000000000000000000000000000		
2 3 2 2 2 2 2 3 3 4 2 2 2 3 3 5		8488832844
5 <b>5564</b> 52253253	***************************************	ក្នុងដល់ជល់ក្នុង
3.01 in or or or or or or or or or or or or or		

Page 15 of 17

		*	
ite a face		Bod of Resident Servey	rea .
	######################################	2 2 2 2 8 2 1 2 3 5 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1	13/10 20 33/10 20 3381 20 3384 75
			Despitime 10/07/1999 4 90 10/07/1999 11 90 10/07/1999 11 90 10/07/1999 15 35
1572 1572 1572 1572 1572 1572 1572 1572	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		
2587 4482 4883 4884 4884 4884 4884 4884 4884	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	25 25 25 25 25 25 25 25 25 25 25 25 25 2	35.5
8229 8423 8423 8423 8424 8424 8424 8424 8424	77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00 77.00	7000 7000 7000 7000 7000 7000 7000 700	777 777
Q = % % % % % & G G G G G G G G G G G G G G	2 4 <b>2</b> 4 8 8 9 9 2 2 2 2 2 2 2 8 8 8 8 8 8 8 8 8	555555 BB86888855555555555 7888455585555	= \$ 3 8 8 B
33733333355443 x845	ភូនៈ១៩ឆ្ង១១៦៨១១៩៩% § ទើបប្រភពនិង១៩២៩២២១	公共元年	77 77 77 77 77 77 77 77 77 77 77 77 77
	**************************************		70
ഗർത്യത്തെയും ക്കുക്കുക്കുന്നത് ഉപ്പയാച്ചം — ഇച്ചധരിന്ന് എയ്യായിയി	линическим колициам голором и и и и и и и и и и и и и и и и и и и	うちゃく いいちゅうストイット・これがロロ りりじしゅうぎょしん じょうちゅう はいまない しょうしょう ちょうしょう しょうしょう しょうしょう はい はい はい はい はい はい はい はい はい はい はい はい はい	94845
**************************************		****** *******************************	Contraction
\$ 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	85588888888888888888888888888888888888	2000	និនិនិនិនិ
2255333333355335535 24600 80 80 80 40 40 40 40 40 40 40 40 40 40 40 40 40	: 22	05266 36612121286662622 2221212126666	33111
94900000000000000000000000000000000000		70000 x200000000000000000000000000000000	22225
944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 - 944 -	7 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	25555
772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 / 772 /	\$\$####################################		769 769 769 769
722 6944 752 752 752 772 772 772 772 772 772 772	0.18228888888888888888888888888888888888	######################################	2 3 3 3 2 2
<b>ಸ</b> ವನ <b>್ನನ ಕನ್ನೆ ಕರಣಗಳ ಕರೆ</b> ಕನ್ನಡ	100000000000000000000000000000000000000	40888 1111111111111111 01111111111111111	=====
<b>န</b> င်္ဂိုင္သိုင္သည္ လူလိုင္သည္ ကို လိုက္သည္ အေလ	лов чы довене в дер чели и очеден феферо з	засле чило чела пределения в пределения	
\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	***************************************	\$\$\$\$\$ 9433333338\$\$\$\$\$ 45\$446665 <b>\$\$</b> \$	
2224222333333333333	48455464655554445544655554		x = 8 R &
88888855333388883338	4 5 8 8 8 8 8 8 8 8 8 5 5 5 5 5 5 5 8 8 8 8 8 8 8 5 5 5 5 5 5 5		= 2 2 2 2 E
######################################	404088840000488844688888880000		000
සහසන් නිහා ව යුලු යුලු පිළිබි සි සි සි ව සි වි	បទសក្សបក្សបុខដូចជប្បស្និតស្ថិតស្ថិតស្ថិតស្ថិតស្ថិតសៀ		3 S = 5 S
. & = = = = = = = = = = = = = = = = = =	:48::::::::::::::::::::::::::::::::::::		=====
			3

Page :6 of 17

2222	ᆔ	0	Ē	7		1
	AVERAGE	AYERAGE	AVERAGE	AVERAGE	End on Micros	Meki
						1583 64
						1010
11111	Ē	1636.00	ğ .			1
3407.60 3407.60 3107.60	13.bett	. !	3801.02 4408.37	387.3		2200
3819 S4 6417 43 4967 59 7208 92	5264.17	- l	27720.20	1142		
12 A 12 A 12 A 12 A 12 A 12 A 12 A 12 A	100		10.0			-
36.01 36.01 37 52.00 57 52.01	¥.		7 7 7 7 7 7 7 7 7	,	# ####################################	-
7.65 7.65 7.65 7.65	7.07	3	S ž	ŝ	* 3223223232323222222222222222222222222	1
13132	5.72	2	5.2	Ē		: [
28245		9	==	ŝ		:
28282	2		ž ž	-	# 2222252222	Ē
12 2 2 2 2	ž		:::	ž	2 325872738888	
* 5 5 6 8	Ē		iŝŝ	ğ	- 1000000 - 100000	: = }
125,13 191,24 191,24 128,63	ž	3	22 77	Ę,	8 3988888 9388	ž
75 T 25 T 25 T 25 T 25 T 25 T 25 T 25 T	1	(	21.00	133.70		
12 12 12 12 12 12 12 12 12 12 12 12 12 1	14.4		L LIL	122,74		3
11.11.11.11.11.11.11.11.11.11.11.11.11.	16.35	Ē	1 5 5	88	. 1000110111111 10000000000000000000000	; ]
37.46 12.81 8.70	10.06	_	115	10,94		ő
1515	ž	1.83	3 - 5	1.55		
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	12.30	25.52	144	- H	# ####################################	: =
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1	ž	1 2 2	2027		_
2228	3	15.0	8 = 8	1.04		: ū
1330 134.80 134.81	122.75	116.8	1 2 2	11254	ន ដូច្នេះ «ដូច្នេះ ដូច្នេះ ដូចនេះ «ដាន់ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ «ដាន់ » នេះ » នេះ «ដាន់ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ » នេះ »	2 2
1 2 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	5,4	ě	141	78.67	4 447642644647 4474444647474646464646 <del>4667646</del> 676646864646	- 5
56128			:::		0 0000000000000 00000000000000000000000	,

Page 17 of 17

-	-	,	Staged verd
Stape 1 and 7	TEITRO		C
147 148 159 159 159 159 159 159 159 159 159 159			The (1-
20259 8 20 W 20259 8 20 W 20259 8 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 20 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12 W 20259 12	2000 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	47789 7 47 MI 47789 7 47 MI 47789 7 47 MI 47789 7 47 PMI 47789 7 5 0 AMI 57789 7 5 PMI 57789 7 5 PMI 57789 1 48 PMI	STime STime
200 20 20 20 20 20 20 20 20 20 20 20 20	10500000000000000000000000000000000000	10000000000000000000000000000000000000	ž Ž
40 24 40 25 25 40 40 40 40 40 40 40 40 40 40 40 40 40	おおおおれれなおいかはななのかれんらのいのまでまでいなられるのものでもありませる アリカリのない 日本の日の内内 アカリ はつれい それの 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本 日本	2223 # 25 # 2 # 2 # 2 # 2 # 2 # 2 # 2 # 2 #	Internations
경 한 한 한 한 한 한 한 한 한 한 한 한 한 한 한 한 한 한 한	######################################	50 00 00 00 00 00 00 00 00 00 00 00 00 0	Come
	222211111111111111111111111111111111111	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Tot Prod
2 0 1 0 0 0 0 1 0 0 0 0 0 0 0 0 0 0 0 0		2222222222222222	Rejection
100	0-A5-228-45-248-88-88-48-88-21-34-45-3-3-5-5-5-5-3-8-5-8-8-8-8-8-8-8-8-8-8-	0 0 0 0 0 1 1 0 0 0 0 0 0 0 0 0 0 0 0 0	0.08
\$ 2 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	888888888888888888888888888888888888888	888888888888888888888888888888888888888	(VICI-VPCp/Ve)/Ca
\$25550577777658555555555555555555555555555	2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	20 20 20 20 20 20 20 20 20 20 20 20 20 2	Salt Rejection
12 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60 11 2 60	0 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Salt Panange
398 377 377 377 377 447 447 457 457 457 457 457 457 457 4	23 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	877 877 877 857 848 848 848 805 807 807 1820 311 311	ş
28 C 28 C 28 C 28 C 28 C 28 C 28 C 28 C	\$\$\$0\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	85883 <u>7</u> 5958888	2
7.29 7.23 7.23 7.23 7.25 7.26 7.26 7.26 7.26 7.26 7.26 7.26 7.26	2022233322573388885322883333332257333388885323333333333	1100 1100 1100 1100 1100 1100 1100 110	4
0 27 20 27 27 27 27 27 27 27 27 27 27 27 27 27	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	5 6 6 7 7 6 5 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 6 7 7 6 6 7 7 6 6 7 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6	J (L m-2hx-1etm-1)
2 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		22 22 23 25 25 25 25 25 25 25 25 25 25 25 25 25	HPF (Union)
0	2 3 5 8 8 8 8 8 5 7 5 8 7 8 7 8 7 8 7 7 7 7	336 336 336 327 321 321 321 327 327 328 328 328	NPF (gpen)
110 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0 100 0	Stage 1
7766627777977777777866666666666666666666	228888888888888888888888888888888888888	905 73 73 80 80 90 90 90 90 90	Stage 2
\$239 <b>1</b> 02533888553653	122112222222222222222222222222222222222	122222222222222222222222222222222222222	-
80 99 90 90 90 90 90 90 90 90 90 90 90 90	######################################	の の の の の の の の の の の の の の	Aucon 79 Q

Page 1 of 19

·		7
949	The County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of the County of th	Date to 50%
84888888888888888888888888888888888888	9 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	71mma (hrs. 256, 41
MAY 12 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	50000 11 10 M 50000 11 11 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 500000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 11 M 1 M 50000 1	\$70/89 / 13 AM
\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	323520 20 20 20 20 20 20 20 20 20 20 20 20 2	i) Si
ARRITATION NA CONTRACTOR NO STATEMENT CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRACTOR CONTRA	8 1 2 2 2 2 2 2 2 3 3 3 3 3 3 3 3 3 3 3 3	23 12
	次次 対策報 びかいけい 2 対策 対策 2 対 2 対 2 対 2 対 2 対 2 対 2 対 2 対	24 R
2255519285577588888888888888888888888888888888	5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	C BS
		Rejection 0.95
3-1-3-1-3-1-3-1-3-1-3-1-3-1-3-1-3-1-3-1		0.89
	000000000000000000000000000000000000000	1 00 I
	1212111246488881144888888814488888888888	Sax rejection
148 458 488 188 188 288 488 888 888 888 888 888 888 888 8	# 0.00 # 0 # 0 # 0 # 0 # 0 # 0 # 0 # 0 #	Saft Phasage
\$4888888888888888888888888888888888888	15844588853758888323382888222888222888373333	272
្ត ពេលស្តេសស្តេសពេលបាយ ១១៧៧៧ ។ ។ ១៧៧៧ ៧៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣៣	的 的 的 心 点 点 表 表 表 的 的 的 种 就 就 就 我 计 计 计 计 计 计 计 计 计 计 计 计 计 计 计 计	à
	10 10 10 10 10 10 10 10 10 10 10 10 10 1	ž.
	- 8 - 8 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	5.44
0 T T T T T T T T T T T T T T T T T T T	5 - 5 - 5 - 6 - 6 - 6 - 6 - 6 - 6 - 7 - 7 - 7 - 7	20 ES
\$X\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$\\$	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	5 52
######################################		24.4
22222222222222222222222222222222222222	3535565655454888888888888888888888888888	ě
20000000000000000000000000000000000000	2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	ŝ
COSOSCETETE CENTRAL DE SANCE DA CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE CONTROL DE C	である。 では、 のいなななななななななななななななななななななななななななななななななななな	5

Page 2 of 19

•		1	Slagad vent	
	Strice Acid 1 on CS: 1 sugar 1 o	Manual franchis	Community	
	75 88	757244444444	9999	Elapas
	3m2 10 41 AM	66999 115 PM 66999 10 15 PM 67799 12 16 M 67799 12 16 M 67799 12 15 M 67799 2 15 M 67799 2 15 M 67799 5 15 M 67799 5 15 M 67799 7 12 M 67799 7 12 M 6789 8 14 M 6789 8 41 M 6789 9 41 M	57hme 5/6/99 5 15 6/6/99 6 15 8/6/99 7 15	_
27	å	111111111115 122583389832	1 2 2 2 E	
#Sで、 GOM # M 3 G 3 G 3 G 4 G 4 G 5 G 5 G 5 G 7 G 7 G 7 G 7 G 7 G 7 G 7	26 70	24 90 2 2 3 3 5 2 2 3 4 5 2 2 3 3 5 2 3 3 5 2 3 3 5 3 5 3 5 3 5	30 % 30 %	
######################################	\$	29 45 29 23 29 23 29 23 28 23 28 23 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 27 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 28 2	20 00 20 00 20 00 20 00	
288	98	127 117 117 117 117 117 117 117 117 117	7 1 3 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	
	0 85	3223323333333	Pejection	
	0 99	000000000000000000000000000000000000000	0 9 9 9	
00000000000000000000000000000000000000	8	8888888888888	1 00 1 00 1 00 1 00 1 00 1 00 1 00 1 00	
626 845019797571978584844487546487897840015454455555564988749888749818974544492468	93 83	2	91 51 91 60	_
25	6.47	7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	Spl Passage 8 49 8 80 8 95 8 40	
F2966844888888888888888888888888888888888	5	592 612 612 612 621 621 621 621 621 621 62	2 2 3 3 3 g	 }
	2	222222288888	# 3: 3: E	_
	1219	1240 1229 1212 1209 1202 1108 1108 1108 1108 1108 1108 1108	125 125 125 126	i 
	207	00000000000000000000000000000000000000		
	8	9 54 9 45 9 45 9 37 9 37 9 27 9 27 10 88 10 88 10 58	9 71 9 66 9 86 9 86	į
200	in in in in in in in in in in in in in i	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 56 2 55 2 55 2 56 2 56	
	2	22 5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	23.5	-
	31 1	334822222222 55722222222222	240 C 23 C 23 C 24 C 23 C 24 C 23 C 24 C 23 C 24 C 23 C 24 C 25 C 25 C 25 C 25 C 25 C 25 C 25	
	0.80		0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	balance from Col
MAN TO SERVICE OF SERVICE OF SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE SERVICE S	î		X E X E E	_

Page 3 of 19

20				
529 12 M M	100 0 0 7 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	321121222222222222222222222222222222222	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	28 28 28 28 28 28 28 28 28 28 28 28 28 2
# # # # # # # # # # # # # # # # # # #	11111111111111111111111111111111111111		2	0.00 M 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
2 4 4 4 5 4 5 5 5 6 5 6 6 6 6 6 6 6 6 6 6	22 25 25 27 27 28 28 28 28 28 28 28 28 28 28 28 28 28	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	23 24 25 25 25 25 25 25 25 25 25 25 25 25 25	32 00 31 04 30 43 30 43
2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2. 2	22 22 22 22 22 22 22 22 22 22 22 22 22	2 2 2 2 2 2 2 2 2 2 3 3 3 3 3 3 3 3 3 3		30 50 50 50 50 50 50 50 50 50 50 50 50 50
\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	882888888888888888888888888888888888888		18288264464	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
		7 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9
	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	23,23,23,23,23,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,24,25,25,25,25,25,25,25,25,25,25,25,25,25,	1 0000000000000000000000000000000000000	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
**************************************		8 2 8 2 8 2 8 2 2 2 8 2 2		2 3 3 3 3 3
	3.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 % \$ 2.8 %	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	\$ 8 8 8 8 9 9 1 1 1 2 2 3 5 1 1 1 1 2 2 3 5 1 1 1 1 2 2 3 5 1 1 1 1 2 2 3 5 1 1 1 1 2 2 3 5 1 1 1 1 2 2 3 5 1 1 1 1 2 2 3 5 1 1 1 1 2 2 3 5 1 1 1 1 1 2 2 3 5 1 1 1 1 1 2 2 3 5 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
8 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	3 2 2 2 3 3 4 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
2 2 2 2 3 2 2 2 2 2 3 3 3 3 4 5 5 5 5 5 5 6 5 6 5 6 5 6 5 6 6 6 6 6	188 222 222 222 221 221 221 240 260 260 260 260 260 260 260 260 260 26	***************	550 550 550 550 550 550 550 550 550 550	6 5 5 5 5
	5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1 1 2 2 1 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 2823332333333333333333	3 3333
222 222 223 234 245 255 265 265 265 265 265 265 265 265 26	1 205 1 205 1 205 1 205 1 205 1 205 1 254 1 265 1 265 1 265 1 265 1 265 1 265 1 265 1 265 1 265 1 265 1 265 1 265 1 265 1 265	1 250 1 243 1 243 1 243 1 273 1 273 1 273 1 273 1 273 1 273 1 273 1 274 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276 1 276	1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1 258 1 247 1 240 1 229 1 229 1 219 1 215
	3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	1	2 2 2 3 3 7 5 7 5 8 5 8 5 8 7 8 8 8 7 8 8 8 7 8 8 8 7 8 8 8 7 8	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		6 4 5 5 7 7 8 8 7 7 8 8 7 7 8 8 7 8 8 8 8 8	7 44 4 60 4 60 4 60 7 87 7 87 7 87 7 88 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62 8 62	3.00 8.07 7.98 7.98
アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・アン・ア	22222222222222222222222222222222222222	<b>2 計名の実施の数数数点計算数据的数分析表示を表示を表示を表示を表示を表示を表示を表示を表示を表示を表示を表示を表示を表</b>	- 0200000000000000000000000000000000000	2 2222
	11 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0			203 203 203 203 203 203 203
# \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$				

Page 4 of 19

•	•	•					Hogen ward
for to 70% with pi	hec to 80% with th	T Company	Both Stages On				Communit
1199 28 1290 74 1290 73 1200 73 1200 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 73 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 74 1210 7	19 19 95	1177 95 1177 95 1177 95 1178 95 1178 95 1178 95 1178 95 1178 95 1178 95 1178 95 1178 95 1178 95 1178 95	1172 56 1172 56	112 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 2 3 2 3 2 3 2 3 3 3 3 3 3 3 3 3 3 3 3	944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 944 00 946 00 946 00 946 00 946 00 946 00 946 00 946 00 946 00 94	The (No. )
78991 15 504 7899 7 15 64 7899 7 15 64 7899 7 15 64 7899 7 15 64 7899 1 20 7 44 7899	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	77799 3 15 PM 77799 3 15 PM 77799 4 15 PM 77799 4 15 PM 77799 4 15 PM 77799 9 45 PM 77799 1 1 45 PM 77799 1 1 45 PM 77799 1 1 45 PM 77799 1 1 45 AM	7/7/90 11 24 AM 7/7/90 12 22 PM 7/7/90 145 PM	76,99 3 24 OM 76,99 5 34 PM 76,99 5 54 PM 76,99 5 34 PM 76,99 9 34 PM 76,99 1 24 PM 77,99 2 4 AM 77,99 7.0) pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt. 10 pt.	62799 10 48 PM 62709 12 48 AM 62709 12 48 AM 62709 12 48 AM 62709 12 48 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 24 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 62709 12 AM 627	STime \$72799 9 48 PM	
######################################		55555555555555555555555555555555555555	ā î	######################################	224450 3000 3000 3000 3000 3000 3000 3000	53555555555522222 2852268853555226	1 2
30033345234533494 34624 3003345234533453494 34624 30033453453453494 34624 30033453453453494	33 35 36 36 22 7 3 2 2 3 5	26 40 26 40 26 40 26 40 26 40 26 40 26 40 27 40 28 40	25 g/ 25 8?	34 38 32 32 32 32 32 32 32 32 32 32 32 32 32	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 29 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56 20 56	29 75
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	4 5 35 9 5 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	2922222222	30 26	52855555555555555555555555555555555555	25727272727272727272727272727 \$ \$ \$ 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	22 22 22 24 25 25 25 25 25 25 25 25 25 25 25 25 25	Cone
110 1117 1117 1117 1117 1117 1117 1117	1 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		0.75	0 0 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	3 3 3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	0 67 0 67 0 68 0 68 0 68 0 68 0 68 0 68 0 68 0 68	Tot Pred
0 0 0 0 0 7 7 7 0 0 0 0 0 0 0 0 0 0 0 0	38 2943	2 2 3 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	0.97	000000000000000000000000000000000000000	230000000000000000000000000000000000000	000000000000000000000000000000000000000	Rejection 0.97
828181818181922 1239			19	2.3.0.0.0.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	000000000000000000000000000000000000000	2
2002110022233333	- 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	44 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	0.92	6 6 6 6 8 8 6 6 6 7 9 6 8 8 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9		00000000000000000000000000000000000000	(VICI.VpCp/Ve)/Ce
22822222222222 2382222222222 23822222222	22 1111 45 1758	2 2 2 3 3 4 5 5 5 6 5 6 5 6 5 6 5 6 5 6 6 6 6 6 6	95.09	98 8 2 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	数 12 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	3
### 7 ### ### ### ### ### ### ### ### #	ឧប ១១១១ ឧទ ចិដ្ឋាទីស៊ី	1 5 5 6 7 7 7 8 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8	184	4 56 4 57 4 58 4 58 4 59 4 4 59 4 4 59 4 4 59 5 6 5 6 6 7 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7		5 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Selt Pressage
293 274 272 272 273 273 273 274 275 275 275 275 275	53 9998	9222222222		313 302 303 303 303 303 303 303 303 303 30	3 2 3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	262 277 277 277 277 277 277 277 277 277	261 Ng
\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	85 8888	3 2 4 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		8846111111118	# 3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2222222222222222	¥
1243 1258 1265 1216 1216 1217 1217 1202 1148 1148 1148 1148 1148 1148 1148 114	1 2 1 9 1 2 1 6 1 2 1 6 1 2 1 7 1 2 2 9 1 2 2 9	1 258 1 258 1 258 1 275 1 275 1 275 1 281 1 281 1 281 1 282	1236	1 198 1 202 1 212 1 222 1 223 1 226 1 226 1 227 1 249 1 209 1 208 1 198 1 198 1 198 1 198	1 219 1 233 1 233 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206 1 206	1251 1240 1228 1228 1222 1215 1215 1215 1216 1217 1212 1212 1212 1212 1212 1212	125
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	F = 100000 6.7 2 2 3 5	2 N N N N N N N N N N N N N N N N N N N		308 308 308 309 311 311 311 311 311 311 311 311 311	5 1 2 2 3 3 3 3 5 5 5 6 2 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	4 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	J (L m-2h-1atm-
22252222222222 222882282222222 222882228222	5 3 2 8 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	11 12 12 13 14 15 15 15 15 15 15 15 15 15 15 15 15 15		3 6 8 6 7 2 6 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	9 22 9 23 9 23 9 24 9 25 9 26 9 26 9 26 9 26 9 26 9 26 9 26 9 26	1) NPF (Umin) 9.22
\$ 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	* * ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~	1 P 2 P 3 P 3 P 3 P 4 P 5 P 5 P 5 P 5 P 5 P 5 P 5 P 5 P 5		20 14 20 14 20 14 20 14 20 20 20 20 20 20 20 20 20 20 20 20 20	スペーションとのなる。 のは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、 のは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のでは、大学のは、大学のは、大学のは、大学のは、大学のは、大学のは、大学のは、大学の	7 7 7 8 5 5 7 7 7 7 7 7 7 7 7 7 7 7 7 7	MPF (gpm)
######################################	2222	233333333233			5 7 3 3 3 3 4 3 3 5 3 3 3 3 3 3 3 3 3 3 3 3	100 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Stage 1
11.7 9 0 1 1 1 1 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	11 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	222222222					Stege 2
							÷
52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50 52.50	32 4545 22 22 PR	242723233 2427233	1 2 7 =	50 9 50 9 50 9 50 9 50 9 50 9 50 9 50 9	2	2002 2002 2002 2002 2002 2002 2002 200	١.,

Page 5 of 19

	127 7 1 1 2 2 2 3 7 7 1 2 2 3 7 7 1 2 2 3 7 7 1 2 2 3 7 7 1 2 2 3 7 7 1 2 2 3 7 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2 3 7 1 2
100 100 100 100 100 100 100 100 100 100	222222222222222222222222222222222222222
	######################################
# # # # # # # # # # # # # # # # # # #	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
2 = 2 X F X E I E G 2 = 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G 2 E G	2 2 2 3 2 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4
54#85088#8548#8#########################	12288282832222
	D 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
	0 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
	\$ 1 2 2 2 3 2 5 2 5 5 5 5 5 5 5 5 5 5 5 5 5
	9
	7 7 7 8 8 8 2 2 2 2 2 2 2 2 2 2 2 2 2 2
***************************************	292 292 292 292 301 301 301 301 301 301 301 301 301 301
XXXLORCALMXXX & 0 28 8 & 2 & 2 & 2 & 2 & 2 & 2 & 2 & 2 &	463224684
	1 247 1 249 1 229 1 229 1 222 1 226 1 209 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200 1 200
	2 2 2 3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
244 5 5 5 7 7 8 5 8 5 7 8 5 7 7 7 7 7 7 8 7 8	1 0 1 0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5
	33222222222222

Page 5 of 19

·						š
	· ·				į.	- Event
	2.0 2.0 2.0 2.0 2.0 2.0 2.0 3.0 3.0 3.0 3.0 3.0 3.0 3.0 3.0 3.0 3					Comme
		***************************************			**************	} 
		140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 140 SS 14	*******		000000000000000000000000000000000000000	3 4
72399 8 43 AM 72399 7 43 AM 72399 10 43 AM 72399 10 43 AM 72399 10 PM 72399 4 00 PM 72399 6 00 PM	772299 17 43 AM 772299 17 43 PM 772290 24 PM 772290 24 PM 772299 343 PM 772299 443 PM 772299 543 PM 772299 743 PM 772299 743 PM 772299 843 PM	72094 6 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72095 7 72 Ak 72	777,949 E 14 AA 777,949 E 14 AA 777,949 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA 779,99 E 27 AA	7777699 24 AA 777899 34 AA 778899 34 AA 778899 34 AA 778899 34 AA 778899 34 AA 778899 34 PA 778899 34 PA 778899 34 PA 778899 13 AA 778899 13 AA 778899 13 AA	71,159 1.33 FM 71,1599 1.33 AM 71,1599 2.33 AM 71,1599 2.33 AM 71,1599 4.33 AM 71,1599 4.33 AM 71,1599 6.33 AM 71,1599 1.24 AM 71,1599 1.24 AM 71,1599 2.24 PM 71,1599 2.24 PM 71,1599 2.24 AM	STime
333111111	33555555 35555555 3555555 355555 35555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 355 3555 3555 3555 3555 3555 3555 3555 3555 3555 3555 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 355 35 3	######################################	77777777 777777777 77777777	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	15 22 15 22 15 22 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 25 15 15 15 15 15 15 15 15 15 15 15 15 15	Ĩ
25 53 25 63 26 63 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 73 27 27 27 27 27 27 27 27 27 27 27 27 27 2	25 25 27 27 28 27 28 28 28 28 28 28 28 28 28 28 28 28 28	<ul><li>※ 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2</li></ul>	23 25 25 25 25 25 25 25 25 25 25 25 25 25	マンス 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 8 8 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Interstage
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	30 98 30 98 30 98 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30 98 45 30	######################################	4 4 2 2 2 2 3 3 4 4 5 2 4 5 3 4 5 4 5 5 4 6 5 4 6 5 4 6 6 6 6 6 6 6 6	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Come
15 11 1 2 3 5 7 2 5 6 1 2 3 5 7	1 - 2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	00000000000000000000000000000000000000		0 + 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Tel Prod
0000000	000000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	. 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Rejection
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	00000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	1244 1444 1000 1000 1000 1000 1000 1000	: 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 9 9 7 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	
9 1 1 1 1 0 9 9 9 2 1 2 2 2 2 3 8	1 1 1 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	\$ 7 3 2 2 2 2 2 2 3 2 4 2 2 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	3 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	22888888228888		VИСЬ-¥9Ср/¥сИСс
91 23 94 05 92 53 90 28 90 28	92 21 52 52 53 53 53 53 53 53 53 53 53 53 53 53 53	121288888822111518182 121288888822111518182	2 2 2 2 2 2 2 3 3 3 3 3 3 3 3 3 3 3 3 3	4 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	20252222222222222222222222222222222222	Salt Rejection
9 9 7 7 8 9 9 5 7 7 8 9 9 7 7 8 9 9 7 7 8 9 9 7 7 8 9 9 7 7 8 9 9 7 7 8 9 9 7 7 8 9 9 7 7 8 9 9 9 7 7 8 9 9 9 9		5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	7 8 8 8 9 5 7 7 8 5 5 7 7 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	Sait Passage
79 29 30 22 50 52 50 50 50 50 50 50 50 50 50 50 50 50 50	555	463 463 463 463 463 463 463 463 463 463	475 476 476	477 477 470 489 480 480 480 480 480 480 480	\$ 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	ğ
55551222	2232222222	2、4、4、4、4、4、4、4、4、4、4、4、4、4、4、4、4、4、4、4	577 577 587 588 588 70	7 6 4 7 7 7 8 4 8 8 8 8 8 8 8 8	邻泊印印印络群群群群 化纸纸纸纸纸纸纸	
1 209 1 216 1 222 1 236 1 250 1 250 1 275	1 229 1 233 1 240 1 251 1 258 1 265 1 275 1 275 1 275 1 275	226 226 227 228 228 228 228 228 228 228 228 228	1 212 1 216 1 236 1 236 1 236 1 231 1 231 1 231 1 236 1 237	1 185 1 186 1 186 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205 1 205	1205 1195 1195 1195 1196 1296 1296 1296 1287 1287 1287 1287 1287	TCF
55 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2	7 0 2 2 2 2 2 2 2 4 2 5 5 5 5 5 5 5 5 5 5 5	> N N N N 의 의 의 의 의 금 등 등 호 및 등 및 및 및 및 등 등 급	9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	# # # # # # # # # # # # # # # # # # #	J (L m-2hr-1am-1)
22 0 95 22 0 95 22 0 95 19 12 19 12 19 18	10 02 10 01 9 91 9 93 10 15 10 11 9 48 9 75	5	111111111122 206288214	55555555555555555555555555555555555555	75555555555555555555555555555555555555	NPF (Lmm)
55 55 55 55 55 55 55 55 55 55 55 55 55	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2 2 5 8 2 2 8 8 M G	2 2 2 2 4 5 5 5 2 2 2 3 5 5 5 5 5 5 5 5 5 5 5 5 5	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	NPF (gpm)
77777777777777777777777777777777777777	1447 1347 1399 1109 1109	11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	7 G G G Z G G G G G G G G G G G G G G G	7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	3303030333722222	Stage 1
23 6 23 6 18 2 18 2 18 5 18 5 18 5 18 5 18 5 18 5 18 5 18 5	11116777244	107 248 130 140 170 170 170 170 170 170 170 170 170 17	11 1 2 2 3 3 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	32731212323131	600 8 6 7 7 7 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	_
						balance from Col
44 63 47 67 71 06 68 49 69 77	3858485888 885388888	2 2 3 3 3 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	238888825 2388 <b>53</b> 88	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	68 22 27 24 24 25 27 27 28 28 27 27 24 27 28 28 27 27 24 27 28 28 27 27 28 28 27 27 28 28 28 27 28 28 28 28 28 28 28 28 28 28 28 28 28	Recovery

Page 7 of 19

•		1
		Commanda
	1566 21 1567 21 1568 21 1568 21 1570 21 1572 21 1573 21 1575 21 1575 21 1577 67	These (Nes)
100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100   100	77-199 10 05 944 77-199 10 05 94 77-199 17 00 FM 77-199 17 00 AM 77-199 10 00 AM 77-199 00 AM 77-199 00 AM 77-199 00 AM 77-199 00 AM 77-199 10 AM	1
	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Ī
とは、「おおおかれ、「おおおおいない」となって、「おおおおないない。「おおおおおおおおおおおおおおおおおおおおおおおおおおおおお	31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77 31 77	Interntage
\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$\$	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	Cone
288 7 5 7 3 5 8 7 3 5 8 3 5 8 8 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	000000000000000000000000000000000000000	Tot Prod
	20000000000	Aejection
	0000-000-00	203
	228233838	(VICI-VpCp/Vc)/Ce
######################################	43	Sale Rejection
C C C C C C C C C C C C C C C C C C C	# 55 55 55 55 55 55 55 55 55 55 55 55 55	Sall Passage
BBBBBBBBBBBBBBBBBBBBBBBBBBBBBBBBBBBBBB	375 375 375 375 375 375 375 375 375	ğ
# C W T T M # W # C C C C M # C C C C C C C C C C C C C	222222	
	1 254 1 249 1 229 1 229 1 216 1 216 1 217 1 206 1 206	1 1
	58 % 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	J(Lm-2hr-1am-1
	17 17 18 18 17 18 18 18 18 18 18 18 18 18 18 18 18 18	NPF (Umin)
	4 4 6 7 4 4 5 5 6 4 6 5 6 6 4 6 5 6 6 4 6 6 6 6	MPF (gpm)
7 A C C A T T T T C C C A C C C C C C C C	0 10 10 10 10 10 10 10 10 10 10 10 10 10	Stage 1
2	55 0 8 8 0 7 7 8 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 8 0 8 0 8 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8 0 8	1~
		belance from Cor
DE LA CERTE CON CONCONTRE CON ENTRE CON CONTRE CON CONTRE CON CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CONTRE CON	7 6 6 6 7 7 7 7 8 8 6 7 7 7 7 7 8 8 6 7 7 7 7	7

Page # od 19

	Stryp-C vont
	Canada
	Elegand The sci field 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03 1278 03
	STIME AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE AND ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE ADDRESS OF THE STATE
00000000000000000000000000000000000000	2544782823777887488748748774474 254478282777887488748744774774747474747474
### ##################################	1
24000000000000000000000000000000000000	
227788887287288728726718978677477772677588878887777888	3
	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
* = 0 = 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	OFF. WEST AND A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE OF A STATE
######################################	1
22 X 28 X 28 X 27 X 2 X 2 X 2 X 2 X 2 X 2 X 2 X 2 X	
\$88::889:53:588 544334853:88530008538848	ND
***************************************	2 8 8 4 4 4 4 4 4 4 4 4 8 8 8 8 8 8 8 8
######################################	10 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	JC 1999-1488-1
######################################	2 C C C C C C C C C C C C C C C C C C C
18382377382377362877752878555578588778887788878887888788	NPF (gps)
######################################	**************************************
	7 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
	below from Col
######################################	74-4-4-4-4-4-4-4-4-4-4-4-4-4-4-4-4-4-4-

Page 9 of 19

	-	Stageoff von
	Re to Jan	Committee
200 200 200 200 200 200 200 200 200 200	100 100 100 100 100 100 100 100 100 100	100 100 100 100 100 100 100 100 100 100
MARKET STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE OF STATE	54 54 54 54 54 54 54 54 54 54 54 54 54 5	22222
~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	化化苯基化二氯酚化合物溶解中枢含物溶解中枢动物医尿管结合 经经验证据 经股份公司	122218
00000000000000000000000000000000000000	日本の (株式 (株式 (大田) (大田) (大田) (大田) (大田) (大田) (大田) (大田)	29 25 26 28 28 28 28 28 28 28 28 28 28 28 28 28
4 1 1 1 1 1 1 2 1 2 1 3 1 3 1 3 1 3 1 3 1	######################################	1 2 2 2 5 1 8 1 2 2 2 5 1 8 1 2 2 3 5 1 8
		7st 77ma
		Rejection 0 98 0 98 0 98
		20000
8 2 2 3 3 3 9 9 9 9 9 9 8 8 8 8 8 8 8 8 8 8 8		109 109 109 107 107
**************************************		548 Rejection 94 87 95 01 95 29 95 34 95 34
880000000000000000000000000000000000000	283.58.58.28.28.28.28.28.28.28.28.28.28.28.28.28	\$13 513 4.99 4.71
002234553655365566666666666666666666666666		\$ \$ \$ \$ \$ \$
**************************************	288844488833388338833888448884488883388883	
		1276 1286 1287 1283
		3.46 3.42 3.42 3.33 3.33 3.30
00000000000000000000000000000000000000	00000000000000000000000000000000000000	13.27 13.27 12.73 12.73
\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$		350 346 338 338
\$3,000000000000000000000000000000000000	*******===============================	9age 2 110 107 107 107
		+

Page 10 of 19

	SlagarEvers
	Communita
	7 mag (Arra) 2061 87 2062 97 2063 97 2066 97
100 100 100 100 100 100 100 100 100 100	2 6 6 6 6
ANDER OF THE STANDARD AND AND AND AND AND AND AND AND AND AN	1 24286
00410599134060778899798997989078898289888888888888888	75 83 25 83 25 83 25 83 25 83
ABBERTANDE SETTEMBERT AND CONTRACT CONT	22 A A A A A A A A A A A A A A A A A A
	320000
	Pojection 097 097 097 097
10004/00104/88804-80480404848484848488803844488494949494949494949494949494949494	9 9 9 9
20224477732489948877775598888828888888888888888888888888	102 102 101
######################################	Salt Rejection 93 61 93 50 93 12 93 12 92 90
	Sall Parage 6 39 6 60 6 60 7 70
	1 2 2 2 2 2 3
	5 2 2 2 2 2
	1236 1236 1237 1238
	J L m-2hr-1elm-1 3-62 3-57 3-57 3-84 3-61
	13.89 13.89 13.69 13.60 13.60
**************************************	NPF (gpm) 367 362 369 366
	138 138 138 138 138
**************************************	~
\$ \$24440 E	4
ENTRE CONTRACT CONTRA	

Page 11 of 19

	7234 5 7234 5 7234 6 7236 7 7236 4 7236 7 7236 7 7236 7 7236 7
2000 13 M M M M M M M M M M M M M M M M M M	A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM A2009 1 19 PM
41886477.23766666677766667776777676666666666677767776666	0202020202020 02020202020 020202020
######################################	77272222222 288252222 28825222
242110100000000000000000000000000000000	0 8 8 8 8 8 5 5 5 5 5 5 5 5 5 5 5 5 5 5
00000000000000000000000000000000000000	000000000000000000000000000000000000000
	000000000000000000000000000000000000000
	0 - 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
2 2 2 2 2 2 2 3 8 8 9 9 9 8 2 9 8 8 9 8 9 9 8 8 8 8 8 8	\$ 1 0 5 0 1 1 1 0 0 0 0 0 0 0 0 0 0 0 0 0
######################################	# # 5 # 5 # 5 # 5 # 5 # 5 # 5 # 5 # 5 #
	88 - 27 26 5 5 1
***************************************	888888888888888888888888888888888888888
	22228888
	1 290 1 290 1 290 1 290 1 290 1 290 1 270
	1 - 4 - 5 - 5 - 5 - 5 - 5 - 5 - 5 - 5 - 5
::::::::::::::::::::::::::::::::::::::	12 18 18 18 18 18 18 18 18 18 18 18 18 18
\$	0.00 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
	55555555555555555555555555555555555555

Page 17 of 19

	Acid and		80	Singuré vent
3.0	Azid Stage 1 on 9/2 and Stage 7 on 9/4] and Stage 7 on 9/4] Azid Pump Falture on 9/8; Restart on	Palaing Zoon nil buck sook	Remain das a	Comments
2682 17 2706 10 2706 10 2706 10 2710 10 2711 10 2712 10 2713 10 2713 10 2713 10 2713 10 2714 10 2718 10 2718 10 2718 10 2718 10 2718 10 2718 10 2718 10 2718 10	254.1.79	244 77 2818 34 2820 34 2820 34 2820 34 2827 34 2820 34 2820 34 2831 34 2832 34		Time (tes)
MARY A CORPORATION OF THE PROPERTY OF THE PROP	· ×	Philip II AM Print Conference of the Conference	600 10 10 10 10 10 10 10 10 10 10 10 10 1	SThrue
55	-: t	33555555555555555555555555555555555555	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	Ĩ
26 87 28 27 28 65 26 87 27 12 15 15 15 15 15 15 15 15 15 15 15 15 15	20 23	25 88 25 88 25 88 25 88 25 25 25 26 26 27 27 27 27 27 27 27 27 27 27 27 27 27	3 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Interstage
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	26 10	2004444444446222 20044444446222 20046284848486485	4 6 7 8 6 7 7 8 8 7 7 7 8 7 7 7 7 8 7 9 7 9 8 7 9 8 7 9 8 7 9 8 8 7 9 8 8 7 9 8 8 7 9 8 8 7 9 8 8 7 9 8 8 7 9 8 8 7 9 8 8 7 9 8 8 7 9 9 9 8 8 7 9 9 9 8 8 7 9 9 9 8 8 7 9 9 9 9	692
	3	000000000000000000000000000000000000000		To Prod
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 97	000000000000000000000000000000000000000		Hejection
20	ŝ	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		
21.5.5.1.0.2.2.2.2.2.2.3.4.	093	2 5 5 4 4 8 8 7 4 4 8 8 4 5 8 8 8 9 4 9 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	5 6 - 7 - 6 - 7 - 6 - 7 - 6 - 7 - 6 - 7 - 6 - 7 - 7	(Authorithment)
8 8 8 8 8 8 1 2 2 2 2 2 2 2 2 2 2 2 2 2	2	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	168518988888888888998889984588888888888888	MOGDERN XIES
34445555555555555555555555555555555555	3	3 87 17 18 18 18 18 18 18 18 18 18 18 18 18 18	\$8 5 4 4 8 8 8 8 9 9 7 5 5 7 7 8 8 7 7 7 7 7 7 7 7 8 8 7 8 7	San Parage
22888888888888888888888888888888888888	, <u>s</u>	\$55 \$56 \$56 \$56 \$56 \$56 \$56 \$56 \$56 \$56	\$ 3 5 6 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	1
7 7 7 7 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	: :		3 = 9 8 8 8 7 7 7 7 7 8 7 8 8 7 7 7 7 7 7 7	1
7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266 7 266	1277	1 233 2 256 1 257 2 258 1 258		ç
2 2 2 3 3 3 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		2	지 집 보고 있는 것 같지 않지 않는 데 그 때 있는 것 같다. 그 보고 있는 것 같고 있는 것 같고 있는 것 같은 것 같은 것 같은 것 같은 것 같고 있다. 그 보	7 (F 40-741-19411-1)
66522824232233555658	1	5 1 1 1 1 S 2 S 3 S 3 S 3 S 3 S 3 S 3 S 3 S 3 S 3	2 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1137
N 7 9 1 2 2 3 4 4 4 4 5 2 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	, j	**************************************	- N	
್ನನ್ನೆ ಪ್ರತಿತಿತಿತ ತಮ್ಮ ಕಡೆದ ಪರ್ಸ ೧-೨೦೪೮ ಎಂತರ - ೨೦೦೩ ೩೮೦ ಇ		# # # # # # # # # # # # # # # # # # #	000000000000000000000000000000000000000	
7 7 8 8 8 8 9 7 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	75	23 5 6 7 6 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9		
				1
22 22 22 22 22 22 22 22 22 22 22 22 22	9 1	56.77 71.86 88.88 71.86 70.77	\$ 6 6 9 9 9 9 9 8 7 7 7 7 7 7 7 7 7 7 7 7 7 7	

Page 13 of 19

	Shaper Street
	Commissed a
	2723 10 2723 10 2723 10 2723 10 2727 10 2727 10
10 10 10 10 10 10 10 10 10 10 10 10 10 1	355555
	282828
00000000000000000000000000000000000000	1/1/1/1/1/1/1/1/1/1/1/1/1/1/1/1/1/1/1/
	0 22 24 44 44 44 44 44 44 44 44 44 44 44
22 8 8 2 2 2 2 3 2 2 2 2 2 2 2 2 2 2 2 2	701 Prod
	78 en con con con con con con con con con co
	0 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9
8 - 8 - 8 - 8 - 8 - 8 - 8 - 8 - 8 - 8 -	(VKC)-VHCMVE)/Ce 1 1 22 1 1 7 1 23 1 08 1 04 0 04
######################################	8 m Rajection 98 33 98 34 98 57 94 57 94 57 94 57 94 57
	Sam P 367 367 367 367 367 367 367 367 367 367
**************************************	\$ 5 8 5 8 8 8 6
្នុក្ខ ខុខ ខុខ ១០ ២៩០ ២៩០ ២៩០ ២៩០ ២៩០ ២៩០ ២៩០ ២៩០ ២៩០ ២៩	******
	1226 1226 1216 1216
	J (L. m-2hr-1 atm-1 2-55 2-48 2-47 3-32 3-33 3-33 3-33 3-33 3-33
00000000111011101111111111111111111111	978 978 9.45 12.36 12.77
	NPF (gpm) 2 58 2 52 2 51 3 27 3 37 3 37
	3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3
***************************************	774 2 9 9 9 9 2 7 4 2
	Balance from Col
	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1

Page 14 of 19

5	å	:	SlagarEverd
Mc to 90%		NO Unit down du to raiging Zenon	Comments
3015 32 3017 32 3023 30 3024 40 3040 97 3042 97 3045 97 3045 97		2429 85	Fides (fore
5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	10 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		STIMe
1445 55 55 55 55 55 55 55 55 55 55 55 55	######################################	-	Ĩ
33 33 33 33 33 33 33 33 33 33 33 33 33	%314851421722292924842845484286248728882488798478476888247258272582725827488474884558488558	:	interstage
39 12 69 45 69 46 69 30	######################################	:	Conc
00-00-00 00-00-00 00-00-00 00-00-00 00-00-	98888888888888888888888888888888888888		Tot Prod
20000000000000000000000000000000000000			Aujection
101111111111111111111111111111111111111	VVVII 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8		[VICT-V#Cp/Vc)/Cc
2 2 2 2 2 2 2 2 2 3 3 3 3 3 3 3 3 3 3 3	**************************************		Salt Palaction
00 00 00 00 00 00 00 00 00 00 00 00 00	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$:	Sad Pastage
54.5 54.6 54.6 54.6 54.6 54.6 54.6 54.6	# % % % \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$		ş
22228888	# E # 2 # 2 # 3 # 5 # 5 # 2 # 2 # 2 # 2 # 2 # 2 # 2 # 2		
1188 1175 1182 1130 1141 1151 1161 1161			1CF
200547623 Y	20 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		J (L m-2hr-1stm-1)
13 45 13 14 15 16 16 16 16 16 16 16 16 16 16 16 16 16	**************************************		April (Limin)
7472457 S	\$;	MP# (gpm)
			Stage
7 / 8 / 8 8 8 5 9 8	**************************************	:	2 after
			-
7 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	e e e e e e e e e e e e e e e e e e e		Recov

Page 15 of 19

100 100 100 100 100 100 100 100 100 100	908.87 908.87 908.80 908.00 90	306: 87 306: 97 306: 97 307	3047 97 3048 97 3049 97
10 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	90599 50 144 90599 70 144 90599	82996 64 PM 92987 74 PM 92987 64 PM 92987 12 64 AM 92987	973992 46 PM 97399 3 46 PM 97399 3 46 PM
0 2 5 3 5 3 2 3 3 5 5 5 6 5 6 5 5 5 5 5 5 5 5 5 5 5 5	22 22222222222222222222222222222222222	22 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	3 3 3 15 3 2 3 15
984519877989348832934749852838888888888888888888888888888888888	######################################	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	3 1 1 5 3 12 13 5 3 12 13 5
ののでは、大力のなのなどを含む。 では、大力では、大力のないは、大力では、大力では、大力では、大力では、大力では、大力では、大力では、大力で	50 54 54 55 56 56 56 56 56 56 56 56 56 56 56 56	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	82 24 71 22 79 88
	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		1 0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
			097 097 098
			20 4 5 2
\$\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	Q (2) 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	0 0 1 2 3 3 3 3 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	107
11677800004641801504590999999447875875895959595959595959595959595959595	92	かい おいかい はい はい はい はい はい はい はい はい はい はい はい はい はい	8 2 2 8 8 3 2 8
	874984488944558	いいののほうのマロの G G G G G G G G G G G G G G G G G G G	17 20 8 72 5 95
4 4 8 ± 8 5 5 6 5 6 7 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	517 517 518 519 519 519 519 519 519 519 519 519 519	\$2.50 \$2.50	8 5 5 2
2 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	2	カルフロガス 神経 神経 野郎 対対 はない はい おいけい はい おいけい はい はい はい はい はい はい はい にい はい はい にっぱい はい にっぱい まいしょう しょうしょう しょうしょう しょうしょう しょうしょう しょうしゅう しょうしゅう しゅうりゅう しゅうり しゅうしゅう しゅう	8 2 3 8
	1 175 1 175 1 175 1 186 1 186 1 207 1 207 1 207 1 207 1 207 1 207 1 207 1 207 1 207 1 207	1222 1222 1212 1212 1212 1212 1212 121	1 198 1 219 1 217 1 222
######################################	が物物性 2000年	7 4 7 5 7 4 7 4 7 4 7 4 7 8 7 8 7 7 8 7 7 8 7 8	3 97 3 73 3 68 3 95
73125622552363535525555555555555555555555	3 3 4 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	5 3 3 3 3 3 3 5 5 7 7 7 7 7 7 7 7 7 7 7	5 H H S
	5 5 5 7 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		37g 37g
00011100000000000000000000000000000000	ជាបានស្ដេចស្ដេចជានិស្ថាជាថា ស្ថា ១០១៩សុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខាធីសុខា	3555353777777777	12 6 12 7 13 7
2738000883727277777777777777777777777777	3373222222777	777777777777777777777777777777777777777	2232
2	50 95 50 95	7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 7 8 8 8 7 8 7 8 8 8 7 8 7 8 8 8 7 8 7 8 8 8 7 8 7 8 8 8 7 8 7 8 8 8 7 8 7 8 8 8 7 8 7 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 7 8 7 8 8 8 8 8 7 8 7 8 8 8 8 8 7 8 7 8 8 8 8 8 7 8 7 8 8 8 8 8 7 8 7 8 8 8 8 8 7 8 7 8 8 8 8 8 7 8 7 8 8 8 8 8 7 8 7 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 8 7 8 8 8 8 8 7 8 8 8 8 8 8 7 8	8 2 8 8 2 2 3 9 2 3 9 9

Fage (6 of 19

	*		:	Stages verd
	Routine Eating		RO Unil deum dus Ro Commandos	Commande
3452 42 3459 18 3459 18 3459 18 3460 18 3461 16 3461 16 3461 16 3462 16 3463 10 3463 10 3463 10	3399 11 3400 11 3401 52 3401 52 3440 52 3440 22 3442 22 3442 22 3442 22 3442 22 3442 22 3443 22 3446 22 3466 24 3466 2	73 9 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	31893 31893	Terne (hra)
3 T T T T T T T T T T T T T T T T T T T	10999 5 5 AM 10999 15 AM 10999 15 AM 10999 15 AM 10999 17 AM 10999 17 AM 10999 19 AM 10999	100 C 100 C	CORRECT OF A PROPERTY OF A PRO	97999 10 43 AM
2 2 2 3 5 2 2 2 2 3 3 3 3 2 2 3 3 3 3 3		\$\$\$\$#\$	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	i i
1989 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	35 24 36 80 36 20 36 20 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 37 18 38 20 30 30 30 30 30 30 30 30 30 30 30 30 30	2502525252538312855555555555555555555555555	2 日本 1 日本 1 日本 1 日本 1 日本 1 日本 1 日本 1 日本	interellage 33 56
70 26 70 45 70 45 70 87 70 87 70 87 70 25 70 26 70 26 89 84 89 84 89 84 89 84 89 84	52 Pl 52 Pl 52 Pl 52 Pl 52 Pl 53 Pl 54 Pl 55 Pl 56 Pl	2	888666666678368686866666666666666666666	28 68
1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	7 of Prod
				Rejection
1312222288533355	1007	9912332235999999999999999999999999999999	00000000000000000000000000000000000000	0 98
12222337657	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	\$ \$ \$ \$ 4 5 4 5 7 7 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	(VICI-VpCp/Ve)/Ce
2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	######################################	28282222222222222222222222222222222222	1	Salt Rejection
7 88 7 88 7 88 7 88 7 88 7 88 7 88 7 8	55 55 55 55 55 55 55 55 55 55 55 55 55	- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Salt Pessage
457 457 457 457 457 458 458 458 458 458	564 669 669 695 695 598 598 599 530 530 530 530 530		5 6 6 6 6 6 7 7 7 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	ž ą
232277777788888888	22222222222222	おきましているない ないだい サイド かんじょ はいしょう はいしょう はいしょう はいしょう はいしょう はいしょう はいしょう はいしょう はいしょう はいしょう はいしょう しゅうしゅう しゅう	87887855578887887878888888888	8
1 219 1 223 1 223 1 223 1 225 1 226 1 226 1 226 1 226 1 227 2 20 2 20 2 20 2 20 2 20 2 20 2 20	115	1100		1178
3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	7 (2) 4 3 4 3 4 3 4 5 4 5 4 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6		J (L m-2hr-1atm-1 3 21
7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	9 99 9 10 00 10 00 10 00 10 00 10 00 10 00 10 1	6611156676868686868686666666666666666666	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	(2 30
9 7 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	200 6 2 7 2 2 2 3 5 5 5 7 8 9 2 5 200 200 200 200 200 200 200 200 200 200	7826228732235667326674676	シングン できまれる 2 8 8 2 8 8 2 8 8 2 3 4 2 4 2 4 4 4 4 4 4 4 4 4 4 4 4 4 4	325
\$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$ \$	115		5 & 7 & 7 & 7 & 7 & 7 & 7 & 7 & 7 & 7 &	13.0
## ### ### ## ## ## ## ## ## ## ## ## #	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	277288877788887778888	888828888888888888377772888888	Z Singe 2
				4
77 0 44 77 0 75 78 0 7	75 64 76 68 77 78 68 77 78 78 78 78 78 78 78 78 78 78 78 78 7	72 00 00 00 00 00 00 00 00 00 00 00 00 00	72 28 72 28	٦,

Page 17 of 19

	9477 66 9477 6
0 (1) 20 (2) 20	1749 6 12 1749 7 12 1749 1 10 1749 1
	0000001111111000000 00000011111111000000
NNAS 4 18 5 2 8 5 2 8 5 2 8 5 2 8 4 5 2 8 4 5 2 8 4 5 2 8 5 2 8 5 2 8 8 8 2 8 5 2 8	2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.
28 8 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	% # # 5 5 5 6 6 8 7 7 7 7 7 8 8 7 5 7 6 8 8 8 8 7 7 7 7 7 7 8 5 7 8 7 8 7 8 7 8
	\$ 7 5 8 8 5 2 2 2 8 8 8 8 8 8 8 8 8 8 8 8 8
	00000000000000000000000000000000000000
	201100000000000000000000000000000000000
2600288748887488874888888989999988888888874488654	5888861111125441888
230447476247777777777777777777777777777777	32323232323333333333333333333333333333
12 年 2 日 2 日 2 日 2 日 2 日 2 日 2 日 2 日 2 日	
\$ # # # # # # # # # # # # # # # # # # #	12 S S S S S S S S S S S S S S S S S S S
	スカスリカ 町 万 円 内 内 石 石 石 石 石 石 石 石 石 石 石 石 石 石 石 石 石
	2
	2
 1. 1. 1. 1. 1. 1. 1. 1	500000000000000000000000000000000000000
	222222222222222222222222222222222222222
\$	7 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2

Page 18 of 19

	•	Catalogy States	>																StagesEvent
	AVERAGE	AVERAGE	AVERAGE	TESTING	THE OF MACUAL	_	_		_	_		_	_					1	Comments
				371541	3711 11	3710 11	3708.11	3706.11	70	3701.40	3600 20	3694.29	3697 28	1 2	3844 19	3843 19	36.2 T	W41 19	Elapsed Time (hra)
				10/21/99 10 13 AM	INV 55-5 66/12/01	10/21/98 2 55 AM	10/21/MB 2 55 AM	1021/98 12-55 AM	1070W 11-55 PM	100000 100000	107099 8 05 94	107070 5.05 PM	1070 PM + 05 PM	10/20/90 2 05 PM	10/10/00 10 50 AM	MY 85 6 66/81/01	10/16/20 8 55 AM	10718799 7 SQ AM	STIMM
				12.39		_		_	8.1		230	24	2	3	8	3	: :	ŝ	Ē
				30 67	29 76	22.52	29 17	29.54	25	2 2	28 83	28 48	28 47	2	0.08	18 93	2		Interstage
				98 37	85 97	8 9	67 87	2	2 S	2	83.13	25	25 1	:	42 43	80 60	8	518	0
				0.55	£ 5	0 0	0.62	0.65	2	7 8		8	8	367	0.33	943	2	å	Tet Prod
22 2 2 2 5 2 2 3 3 2 5 	97 23	95 48 95 48 97 18	98 02	980	99	9 6	98	0.98	2 2		9	2	2	•	0.80	ŝ	8	98	Rejection
				1 54	20	29	1 29	1 22	ន៍វ	2 3	100	8	128	8	95	995	95	9	
				1 65	22	122	121	Ē	i :		127	1.17	2	:	000	ē	2	2	(AICI-ABCP/AFIX)
94 57 93 53 94 18	93 98	95 55 55 56 55 56 56 55 56	94 83	35	3	25	3.00	2	2 1	2 8	94.47	¥	¥ ;			98 26	23	2	VICT-VpCp/Vc)/Cd Salt Rejection Salt Passage
5 6 37 5 73 5 73	601	934 1074 1075	\$ 07	444	9	6	ŝ	518	8 8	2 2	2	5	5.50	:		374	377	1	Sall Parties
					626	Š 2	ē	51	ŝ	5	: 5	576	£ }	ê		920	21	910	ğ
					= 2	5 %	8	2	2 2	2	T	r	5, 8			ř	ē	170	
				1004	1.028		1037	2	2 2		9	-	2		1 037	985	05	1052	ផ្
					327	115	322	3	9 1	3 2	4	3 38	338	:		710	2	313	Jil a-Shr-Isla-1)
175571 22875	363	10 65 7 13 19 14	1443		12 %	1210	12 34	12.78	270	224	3	12.98	12 K	;	_	9 9	<u>.</u>	+	E MPF (Chira
3 4 4 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	38	2 81 1 88 3 47 2 38	3 61		3.32	322	326	336	7 J	3 2		342				213	2 5	1	- z
				13.6	-		ī	143			ú	140	<u>.</u>	:	= 5	15	= :	-	Stage 1
				-	5.		50	•	5 :	- 2	2	5	5 6	:	•	• 2	: :		\$.
						_							_						balance from Col
27888 88:28	71 51	63 67 70 37 54 98 47 88	24 50	81 53	3 5	8 8	80 39	28	3:	8 8 2	=	8	8 8		79 83	3 8	2 :	76 83	Recovery

n											~													_		_													_					·		_	_		Stage/Event
FH 6/11/99	Thu 6/10/99	SENCIS DOM	Mon 6/7/99	SEASO UNS	Sercia INC	Fri E/4/99	Thu 6/2/99	Wad 6/2/99	Tue 6/1/59	Hon 5/31/99	Sun 5/20/99	2000 FES	66.72cm	66/92/5 Pe.M	Tue \$/25/99	Mon 5/24/98	Sun S/21/99	Sat 5/22/99	FH 5/21/99	17m 5/20/99	00 S/18/99	Mon 5/17/99	Sun 5/18/90	ST STILL	CACTOR DEL	Wed 5/12/99	Tue 5/11/99	Mon S/10/98	66/6/5 unS	St. 507.099	Thu 5/8/99	Med 5/5/99	Tue 5/4/99	Mon S/1/98	Sun 5/2/99	50 E/1/2009	Thu 4/29/99	Wed 4/28/99	Tue 4/27/99	Sun 4/25/99	Sat 4/24/99	Fri 4/23/99	Thu 4/22/90	A COLUMN	Mon 4/19/94	Sun 4/18/98	Sad 4/17/88	Fri 4/16/79	Date
7	S .	504.00	456.88	432.00	8	384 88		336 00	312.00	288.00	264.00	2 6	20281	- No.	14.00	120 00	96.08	7 8	8 00	8	T						_													•	_			1				Ţ	Bun Time (hrs)
1	_			_			_	_		713	_				_	_		_			1	_	_		_			ð	_	_			_	_	_		_		7.52		_			1	7.40		_	ž	
						_			_	1.651.00		_								_								1,630 00											1,483.00		_				1,850 00			1,000.00	Conductivity (uti/cm)
			6,17													6.16					T							os Ca														775	-						TOC (mg/L)
011		_				017	0 18	01		0.29			9	0.26					012	9				_			0.73	0.2						_					0			0.2%	0 6	3	0.31		_	2	Turbidity (PTU)
5		_				- 1	7	3		ŝ			-	30			_	_	1.60	ě																						. g	200	3 3					SØ4
67	_	_				0 55	069	8		0 42			ē		-				22	<u>.</u>	1						1 58	į,											2			1.55	<u>.</u>		3	_		3	Total Chlorine (mg/L)
0.12				_		0.08	8	0.07		ĝ			0.07	00/					010	012							0 10	0.16										_	075			013	ō :	0.00	0.07	_		0.15	Free Chiorine (mg/L)
į			1.031 00													966 00												929.00																	966.00			99700	TDS (mg/L)
			2.28							Ī					_										_												,							Ī					Total Collions (CFU/100 mL)
					_																																												Fecal Coliform (CFW160 mL)
24000			2000			2200						20000	1						96000																				68000			8000			•				Pseudomonas (1000° CFU/100mL)
			6.000.00				1,500.00		3,900 00				_		_	_											_					_		_				_	_							_			HPC (CFWmL)
		_							_	7 32													_					760						_				_	7.73						780			7.85	pH
										3,420 00																		6.250.00											3,380 00					}	4,120 00			6,060.00	Conductivity (uslem)
0.40	_					023	0	0.31		0.26			6		;				1.6	067	1				_		35	32									_		0.89			0.75	0.70		Ē			29	Turbidity (NTU)
						_			_																		_									_								1					sor E
			2.212.00							2.016 00						2,796 00		_										4,776.00											11.00						5.752.00			5,668.00	TØS (mg/L)
1	_	_		_	_	_	_	_		9						_ <u>~</u>	_	_		_	1							603							_		_	_	6 35		_	_	_	1	613			5 79	pH
										86.00											1							80 00		_									8				- 5		9.19	_		2.10	Conductivity (uS/cm)
			0.50	;												0 50												0.50														0.50	5	Š					TOC (mg/L)
0.04		_		_		90	6	0.04		0	_		9	2 0				_	0.09	o g	Ţ						005	0.04			_				_			_	8		_	0.06		-+	0.09			0.10	Turbidity (NTU)
\$		_			•••	0.20	020	0.40		0.40	_		9	3 8	,	_			å	20	1														_		_	_	_	_	_	5	0.50	3	_		_	4	SDI
_	_	_	8			_				8	_	_				70.00		_			1				_	_	_	8	_									_						+	8	_		24.00	TDS (mg/L)
3	_	_		_		_	98	_		0.46			- 5	3	<u>.</u>				23		1		_	_	_		_	_		_		_						_			.—			1		_			Total Chiorine (mg/L)
011					_	000	8	0.05		006			- 0,0	3	-		_		909	8	1				_					_					_		_				_	_		1					Free Chilorine (mg/L)
	!	_		_		_	_	_	_				_			700					1								_		_								_						.00	_		_	Total Celiform (CFU/100 mL)
		_		_																	1		_								_													1					Fecal Colliform (CPU/160 mL)
1,700,00			\$ 3			36.00	:	_		_		00.00	300		_				30 00							_						_							3			22:10			<u>.</u>	_		_	Pseudomonae (CFI // 190mL)
			8				10.00		1,200 00		_			200 (50	3	170 00	_		_							56.93		142.00		_					_			_	_			_	1	3	17.00		_		MPC (CFWmL)
		_	99	3		_	_	_		_		_	_	_	_	9191	_		_		I							92 73		_	_			_	_		_		_		_	93 55		2			_		% TOC Removal
		_	9.93	2		_		_					_			97.75					I			_				* 23	_	_	_												_						% TDS Removal R
4.15		_	55 35	_								i	5			_		_	6.51					_	_							_							713			5 58		-	3	_	_		No TDS Removal RE. MOVAL Log Reduction Log
63 64						2	1 1	71 43		51 72		_		3 4	3	_	_		25 00	22				_			78 26	80 98		_			_		_			_	86 36	_	_	72 73	75 08			_			% TurbidRy Removal

		_		_		_			_				_		_		_				_						_						_		_	_	_			_	_		_	_	_				_	Stage/Event
Fri 8/5/99 Sat 8/7/99	Thu 8/5/99	Med E/4/99	Tue U2/99	2010	San 1/3/199	FH 7/30/99	P6.KEZ/2 PW 3	Wed 7/ZU99	Tum 7/27/99	SEARCH UDDE		500 777.000	F # 7/21/99	1 %u 7722/99	Wed 7/21/99	Twe 7/20/99	Mon 7/19/99	Sun 7/18/99	San 7/17/78	Fri 7/16/99	Thu 7/15/99	Wed 7/14/20	Tue 7/13/99	Mon 7/12/99	Sun 7/11/09	Set 7/10/98	1 TO 17 TO 19 TO 1	Wad 7/7/99	Tue 7/6/99	Mon 7/5/70	Sun 7/499	Frt 7/2/99	1hu 7/1/98	B&nit/s Pe.M.	Tue 0/29/99	Sun 6/27/96	Sat 6/26/99	Fri 6/25/99	Thu 6/24/99	Wed 8/21/99	Tue 6/27/04	Sun 6/20/16	Sat 6/19/99	Fri 9/19/99	Thu 6/17/98	Medical States	-	Sun 6/13/98	Sal 6/12/99	Date
1896 00	1872 00	1848 00	824 00	3 8	1776.00	1728 00	1/04/00	1680 00	1656 00	102.00	1 000	504.00	560.00	1536.00	51200	88.00	2464 OG	1440 00	1416.00				1320 00	1296.00	1272.00	200	200 00	1178 00	1152.00	120	1104 00	1056.00	1032 00	1008.00	984 00	936.00	91200	888.00	964 00	840.00	792.00	768.00	744 00	720.00	98.00	672.00	8	900.00		Fluin Time (hrm)
			9,7								_					_	8		_		_	_		739		_		_		709		_	_		à	_				_	à			_		_	-			pH
	_		8	3													1,809 00	_			_			1.635.00					1	\$.509 00	3					554 00						5/3.00			Conductivity (utl/cm)
			0	•													711												,	Š											8 71									TOC (mg/L)
0.13	013	2	0 0	•	_	012	0.08	013	0.13	:			0.15	0		0	015			0.14	0.14	0 1	0.11	0 13		6	2 2	0 12	2	•		0 16	0.1	0.15	0 2	:		0.16	0	0 1		:		021	2 1	8 3		:		Turbidity (MTU)
å	å	å	<u> </u>			5	1.30	- 60					96	8	3 3	170	1 60			1.50	170				_		_		8	2 20		_		_						_	ē						200	3		SDI
0.34	003	15	0.59	5		0 77	1.29	1.56	0 77	ì			8	1.0	. 86	107	1 58			1.58	1.30	1.57	121	22		ä	; 5	9	167	2		1.38	65	1 86	147			1 36	5	2	2 4	i		1 73	3	174	: :	ì		Total Chiorine (mg/L)
8	003	90	90 .	:		9	918	040				_	013	3	3	0.26	1 29			0 20	017	075	0.08	0.08		:			0.16	013		9	210	18	0.29	3		007	=	8	0 1	:		0 16	2	0 0		?		Free Chlorine (mg/L)
			909 00	3													791 00							909 00						8					3	3					920 00	3								TDS (mg/L)
													_									_			_			_											8						-	8				Total Californi (CFL/100 mL)
				_		_					_				_	_	_		_	_		_	_			_		_						_			_		8						_				_	Facili Colliorm (CFU/100 ml.)
13000		_	74000			580000			280000				49000			ŝ				70000			17000		_		i	_	3600			17000			Энсоро			59000	_		1	_		57000		13000	ita			Passidomones (1800° CFU/100mL)
									_			_				_			_		_				_					_			_	_	_						120.00			_	-	400.00	_			HPC (CFU/mL)
			9	i					_								6.92							7 51						7 13						7					è	:						-		pH
			5.00	5										_			4.290.00					_		5.540.00				_		40000					0.00,000	3.56	_				2,700,00					_	*,020.00			Conductivity (uS/cm)
9.46	<u>.</u>	ຊິ	0.36	2		0.28	0.26	0.27	3 9	;			0 33	2	2 0	3	0.35			029	0.35	1	030	0.40			2 4	0 22	0.17	0.20		0.18	0.16	0.14	0 0	3		0.25	0.36	0 1	0 20	-		027	0.23	0.28	3 2	<u>:</u>		Turpidity (NTU)
ŝ	1.20	? 10	160	30		.90	K.10	2.20	3																																									SOI
			3.000	7066	_										_		2,758 00		_					3,320.00						1 444 00					8	3					548.00	3								TDS (mg/L)
_				<u>.</u>						_	_			_	_		5.5				_	_		5. 2.6	_	_				3	_	_	_	_	ā	ŝ			_		2	:		_		_		3	_	рН
			5	5				_				_					06.00	_	_	_		_		115 00				_		65.00					- 5	3					8	: 					Š	.		Conductivity (ut/en)
			è	5													0.50													950				_							Ş	;								70C (mg/L)
010	9	0 05	0 6	3		003	9	9	9				0.04	9 6	000	0	0.07			0.05	95	0.05	9	8		9	9	ŝ	0.03			0.05	5	003	0 0	3		9	9 8	_	9 9	_		8	9	00 0	2	3		Turbidity (NTU)
				_	_			_		_	_									_		_		_				_	0.20	-				_	_		_		_		8 6					_				Son
			_	3	_			_						_			90	_		_		_		8						8				_		3	_				8			_				_		TDS (mg/L)
0 27	0.02	0.15	8	8		9	9	ÿ		?	_		5			1 1	69	i		.68	47	ē	ä	25		- 2	; ;	0.92	ē.	<u>.</u>		5	1.67	.69	<u>.</u>	ē 		36	6	217	2 0	:		1.59	Ē :	9 2	ž =	<u>.</u>		Total Chiorine (mg/L)
0,	002	005	0 13	2		9		3 4	200		_		020	3 0	2 6	2 20	2	:		0.21	012	0.18	0.10	0.10			9 6	008	0 :	0.09		0.16	74	0.19	0 10	007		0.07	0.13	909	5 S	<u>.</u>	_	0.17	013	2	0 0	2	_	Free Chiorine (mg/L)
		_									,											_				_			L	_		_		_	-	3		_	2.08						_	8				Total Collform (CFU/100 mL)
	_	_		_	_		_	_			_						_												L					_							8	3					_		_	Fecal Cofform (CFU/100 mL)
9			3 OC						33.05	33.03				, 00	78	700		_		33 00			900			1	8		33 98			10 00			100 00			27 00			90		_	45 00			36			Pseudomones (CFU/100mL)
	_	00 OO		5000	_					_	_					_	_		_			10 00		200 00	_			80 00	8 %					600		700 00					8	3				350 00				HPC (CFU/mL)
				9	_				_		_			-			16.26	-				_				_				92 67		_	-								8, 95	e E			_					% TOC Removal
		_		2				_			_						9						_	2, 76	_	_	_			94 17				_		9						R S			_					% TDS Removal
5 29	_		6 97		_	1	-	_	9		_	_	_			9		_		6.33		_	6.33				6.27		504			6.23		_	6.58			6.33		_	5	_		610			5			Lag Reduction
23 0	15 3	500	50 00		_		; ;	3 2	5 9	-			3	3 5	54 29	77.0		3		64 29	64 29	64 29	63 64	53 65			8 9	2 8	78.57	88		8	7 6	80 0G	75 00			68 75	56 67	35 08	8 9	2	_	71 43	72.22	77 27	53 85	3		% Turbidity Removal

Page 2 of 4

Two scales Two scales Two scales Two scales Fel Active Sea Scales Two sc	Design Account of Control of Cont
	Dodo Dodo
	5
1,791.00	1.7 Comments (44)
§ §	g toc (mer)
00000 00 00 00 00 00 00 00 00 00 00 00	8 8 8 8 1 1 8 8 1 8 18 Tuesday (NTU)
2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	11 0 0 0 0 0 1 1 1 1 1 1 1 1 1 1 1 1 1
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	S S S S S S S S S S S S S S S S S S S
997.00	20 8 8 TOP (mapl.)
ğ	Total Collines. (CFU100 set.)
8	Postil Collions (CFU/100 mL)
	\$ 22 25 5 Pasudomonas (1906' C Pluridom

• • ;

TDS (mg/L)	2,936.00			313.00											.752.00		1012.00							
pH	ž			8 23				5 25							5 40		5		Ì					
Combicativity (utili	128.08			71.00			_	8							127.00		93.08		3					
TOC (mg/L)				9.50											0.50						9			
Turbidity (NTU)	2 2 3	9 9	9,0	0,0	0.00	8	0,02	6	0.02	0.07	0.05			8 8 9	p 0	8	200	000		0.02	0	000	0.02	
801																								
TDS (mg/L)	‡ 8			30.00				31.8							8		38.00		3					
Total Chiorina (mo		2 2	0.25	2 2	0.24	0.02		2	2	2 2	2 2			1.29	0.85	0.02	0.98	1.10		0.16	2	. š	ā	
Free Chilorina (mg	2 2 2	8 8	Š	2 00	000	0.02	0.12	8	0.03	000	0 0 0 0			9 1 3	0.06	0.02	0 10	0.12	3	8	8	2 2	0.09	
Total Collions (CFU1100 mL)										-														
Fepal Coliforn (CPU/100 mi.)																						_		
Perindomones (CPU/100mL)	130.00		87.00	3	82.00		8					<i>,</i>	V- <u>-</u>	380.00					_				-	
HPC (CFUALL)	11,000.00	1,000.00		20 00											.				3		340.00			
% TOC Removal				3											19						83	_		
% TDS Removal	ž.			2			.,	2 2						_	% %		8				_			
Log Reduction	2	;		Ē	9		5.80						, u ,	5										
% Turbidity Remo	2 2 2	3 3 3	8	5 8	98.67	‡	88.67	55.00	2 2	53.33	37 50			14 55 55 29 56	71,43 55,56	8	86 67 75 00	72.73		77.78		8 6		

L	0			n •			L	>						_	Blogs/Event			
WAX		MEAN	MAX		WEAH	MAX	£	MEAN	MAX	Į	MEAN	Fri 10/8/99 3	Thu 10/7/89 3	Med Indiana	Tue 10/5/50	Mars (0/4/98 3	Coto	-
Ĺ	_		_			L	_	_	L			1408.00	3384.00	3360.00	3336.00	3312.00	Rus Time (hrs)	_
7.39	â	ž	7.40	7.08	7.30 1.	7.13 1,	7.13 1.	7.73 %	7.52 1,	8	1	L					p++	
893.00	1,211.00	668.1	573.00	544.00	,560.00	,651.00	1,651.00	1,651.00	,630.00	483.00	554.50						Conductivity (uS/cm)	
7.30	6 .01	6.62	5.82	6.71	4.77	:1	6.17	6.1	7.99	ŝ	7.54						TOC (mg/L)	
0.24	0.08	2.11	0.22	0.11	0.18	0.29	0.12	0.10	0.44	0.16	0.25						Turbidity (NTU)	
28	8	5	2.50	.36	2	1.80	7.10	<u>.</u>	2.30	ž	2.07		68				SDI	
1,71	0.02	0.70	ž	1.10	1.71	1.41	0,42 2	0.92	2.14	ĭ	1.62						Tatal Chiorine (mg/L)	
.23 28	0.02	0.13	0.18	0.06	0.12	0.12	0.0 X	0,0	0,15	o. 16	0.12						Free Chlorine (mg/L)	FEED
1,006.00	781.00	898.67	961.00	920.00	943.33	1,031.00	968.00	998.50	929.00	929.00	929.00						TDS (mg/L)	
6.00	6.00	6 .00	8.00	4.00	<u>\$</u>	2.00	2.00	2.00									Total Coliform (CPU/100 mL)	
1.00	3.00	3.00	2.00	2.00	2.00											_	Fecal Coliform (CFU/100 mL)	
580000	98	97636	380000	3600	87950	96000	2200	39300	68000	8000	38000						Pseudomonae (1980° CFU/100mL)	
1,700.00	1,000.00	1,444.35	4 400 00	170.00	B64.87	6,000.00	1,500.00	3.274.18	L							1.000 00	MPC (CFU/mL)	
7.61	3.10	8	7.63	7.13	7.4	7.32	7.32	7.32	7.73	7.60	7.67						pH	
6,940.00	4,290.00	5,364.67	4,620.00	2,700.00	3,717.50	3,420.00	3,420.00	3,420.00	6,250.00	3,380.00	4,815.00						Conductivity (uS/cm)	2
1.58	0.14	0.36	1.62	0.14	0.32	1.40	23	0.54	1.35	0.70	0.97	L					Turbidity (NTV)	CONCENTRAT
3.00	0.30	1.57															SOR	á
5,186.00	2,751.00	3,503,22	2,114.00	1,444.00	1,702.00	2,796.00	2.016.00	2,341.33	4,778.00	11.00	2,393.50						TDS (mg/L)	
6.26	5.25	5.26	6.21	6.00	6.07	5.00	8	8	6.35	6.01	6.18						pH	_
150.00	71.00	109.56	72.DG	46,00	62.50	86 .00	8 .00	86.00	80.00	9.04	2						Conductivity (u\$/cm)	
0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50	0.50						TOC (mg/L)	
Ξ	0.02	8	0.07	8	93	0.15	9	90.0	0.0	0.04	8		_				Turbidity (NTU)	
		:	0.50			0.40			0.50		0.47	_					SDI	
62.00	29.00	40.11	56.00	34.00	2	70.00	1.00	51.00	35.00	35.00	35.00			_			TDS (mg/L)	
1.69	0.02	0.72	2.57		1.71	1.37	6	90.90									Total Chiorine (mg/L)	PERMEATE
0.54	0.02	=	0.19	96	21	0.09	9	0.06				_		_			Free Chlorine (mg/L)	
1.00	8	1.00	1.00	2.00	2.88	7.00	7.00	7.00				L					Total Coliform (CFU/100 mL)	
			2.00	2.00	2.00							L		_			Fecal Coliform (CFU/100 mL)	
380.00	7.00	66.57	1,700.00	9.00	276.75	100.00	30.00	50.25	22.00	5.00	13.50						Pseudomones (CFU/100mL)	
11,000.00	10.00	276.43	700.00	5 .00	65.18	1,200.00	10.00	110.29	142.00	32.00	76.67					350 00	HPC (CFU/ML)	
93.15	91.66	97.40	\$2.67	92.55	92.61	91.91	1.90	91,90	93,74	92.73	83.34						% TOC Removal	
96.99	93.72	95.56	96.30	94.17	95,32	95.93	92.75	94.34	96.23	96.23	96.23			_			% TDS Removal	REMC
7.14	4.47	5.97	ŝ	4.15	5.79	6.51	ŝ	5.67	7.13	2	6.35		_	_			Log Reduction	REMOVALS
	_	57.29	80.00	\$3.85	69 84	75.00	25.00	54.86	8.38	72,73	78.47						% Turbidity Removal	

Appendix D. Laboratory Reports



CH2M HILL

Applied Sciences Group

2300 NW Walnut Blvd

Corvallis, OR

97330-3538

P.O. Box 428

Corvallis, OR

97339-0428

Tel 541.752.4271

Fax 541.752.0276

September 22, 1999

McAllen WWTP #2, City of

149462.A1.ZG

RE:

Analytical Data for McAllen WWTP #2, City of

Applied Sciences Group Reference No. 9964

Dear Angie Fernandez/PHX:

On August 18, 1999, CH2M HILL Applied Sciences Group received four samples with a request for analysis of selected parameters.

The analytical results and associated quality control data are enclosed. Any unusual difficulties encountered during the analysis of your samples are discussed in the case narrative. Subcontracted analyses reports are attached.

Under CH2M HILL policy, your samples will be stored for 30 days after reporting. If you have not given us prior instructions for disposal, we will contact you if any samples require disposal as hazardous waste.

CH2M HILL Applied Sciences Group appreciates your business and looks forward to serving your analytical needs again. If you should have any questions concerning the data, or if you need additional information, please call Ms. Kathy McKinley at (541) 758-0235, extension 3120.

Sincerely,

Kelly Ensor

Senior Administrative Assistant

Enclosures

CLIENT SAMPLE CROSS-REFERENCE

CH2M HILL Applied Sciences Group Reference No. 9964

Sample ID	Client Sample ID	Date Collected	Time Collected
996401	ZGP	8/17/99	7:30
996402	ROP	8/17/99	7:30
996403	ROC	8/17/99	7:30
996404	WWTP#2Effluent	8/17/99	7:30

CASE NARRATIVE VOLATILES

Lab Reference No.: 9964

Client/Project: McAllen WWTP #2, City of

I. Holding Times:

All acceptance criteria were met.

- II. Analysis:
 - A. <u>Calibration</u>:
 All acceptance criteria were met.
 - B. <u>Blanks</u>: All acceptance criteria were met.
 - C. <u>Duplicate Sample(s)</u>: Not Applicable.
 - D. <u>Spike Sample(s)</u>: Not Applicable.
 - E. <u>Surrogate Recoveries</u>: All acceptance criteria were met.
 - F. <u>Lab Control Sample(s)</u>: All acceptance criteria were met.
 - G. Other:
- III. <u>Documentation Exceptions</u>:
 None

IV. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or designee, as verified by the following signature.

Prepared by:

Reviewed by:

CASE NARRATIVE GENERAL CHEMISTRY

Lab Reference No.: 9964

Client/Project: McAllen WWTP #2, City of

I. <u>Holding Time</u>:

All acceptance criteria were met.

II. Analysis:

A. <u>Calibration</u>:

Bromide recovery (132%) in final calibration verification exceeded acceptance criteria. All other acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>Matrix Spike Sample(s)</u>:

Bromide matrix spike recovery (200%) exceeded acceptance criteria. All other acceptance criteria were met.

D. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

E. <u>Lab Control Sample(s)</u>:

All acceptance criteria were met.

F. Other:

Not applicable.

IV. <u>Documentation Exceptions</u>:

None.

V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by:

Reviewed by:

CASE NARRATIVE METALS

Lab Reference No.: 9964

Client/Project: McAllen WWTP #2, City of

I. <u>Holding Time</u>:

All acceptance criteria were met.

II. <u>Digestion Exceptions</u>:

None.

- III. Analysis:
 - A. <u>Calibration</u>:

All acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>ICP Interference Check Sample</u>:

All acceptance criteria were met.

D. Spike Sample(s):

All acceptance criteria were met.

E. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

F. Laboratory Control Sample(s):

All acceptance criteria were met.

G. <u>ICP Serial Dilution</u>:

Not Required.

H. Other:

None

IV. <u>Documentation Exceptions</u>:

None

V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by: _	July	Don	
Reviewed by:		WUSL	

Client Information

Client Sample ID: ROC

Project Name: McAllen WWTP #2, City of Project Manager: Angle Fernandez/PHX

Basis: As Received

Sampled By: R. Trevino Sampling Date: 08/17/1999 Sampling Time: 7:30 Type: Grab Matrix: Water Lab Information

Lab Sample ID: 996403

Date Received: 08/18/1999

Report Revision No.: 0

Analyzed By: MG/DK/MS

Reviewed By:---

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
N-Nitrate	0.20	35.4		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.72		mg/L	EPA 351.4	08/25/1999
Total Dissolved Solids	5	3,230		mg/L	EPA 160.1	08/23/1999
TOC	5.0	33.7		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.25	9.89		mg/L	EPA 365.2/4	08/19/1999

Client Information

Client Sample ID: WWTP#2Effluent

Lab Sample ID: 996404

·

Date Received: 08/18/1999

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Report Revision No.: 0

Lab Information

Sampled By: R. Trevino Sampling Date: 08/17/1999

Analyzed By: MG/DK/MS

Sampling Time: 7:30

Reviewed By:

Type: Grab Matrix: Water

Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
N-Nitrate	0.04	2.96		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	08/25/1999
Total Dissolved Solids	5	799		mg/L	EPA 160.1	08/24/1999
TOC	0.50	8.39		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.25	2.98		mg/L	EPA 365.2/4	08/19/1999

Client Information

Lab Information

Client Sample ID: ZGP

Lab Sample ID: 996401

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Date Received: 08/18/1999 Report Revision No.: 0

Sampled By: R. Trevino Sampling Date: 08/17/1999 Analyzed By: DK/MG/MS/JJB

Sampling Time: 7:30 Type: Grab Matrix: Water Reviewed By: - 3---

Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
Alkalinity (as CaCO3)	2.0	121		mg/L	EPA 310.2	08/23/1999
Bromide	0.020	0.132		mg/L	EPA 300.0-B	08/19/1999
Chloride	1.0	160		mg/L	EPA 300.0-A	08/23/1999
Color (APHA) Apparent		22		color units	EPA 110.2	08/18/1999
Fluoride	0.10	1.07		mg/L	EPA 300.0-A	08/23/1999
N-Nitrate	0.10	9.55		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	08/25/1999
Silica-React.	0.40	15.1		mg/L	SM4500-Si D	09/01/1999
Sulfate	1.0	150		mg/L	EPA 300.0-A	08/23/1999
Total Dissolved Solids	5	774		mg/L	EPA 160.1	08/23/1999
TOC	0.50	7.48		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.25	2.48		mg/L	EPA 365.2/4	08/19/1999
UV-254	0.009	0.129		asb/cm	SM5910	08/19/1999

Client Information Lab Information

Client Sample ID: ZGP Lab Sample ID: 996401

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Basis: As Received

Sampled By: R. Trevino
Sampling Date: 08/17/99
Sampling Time: 07:30
Type: Grab
Matrix: Water

Date Received: 8/18/99
Report Revision No.: 0
Reported By: JG
Reviewed By:

Analyte	MRL	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
Analyto		HOUR	<u> </u>			7(1,11)204
Aluminum, Al	45.6	111		μg/L	SW6010B	08/27/99
Arsenic, As	3.9	3.9	U	μg/L	SW6010B	08/27/99
Barium, Ba	0.81	56.2		μg/L	SW6010B	08/27/99
Cadmium, Cd	0.38	2.7		μg/L	SW6010B	08/27/99
Calcium, Ca	21.3	72100		μg/L	SW6010B	08/27/99
Chromium, Cr	7.2	7.2	U	μg/L	SW6010B	08/27/99
Iron, Fe	2.8	31.9		µg/L	SW6010B	08/27/99
Lead, Pb	2.3	28.4		μg/L	SW6010B	08/27/99
Magnesium, Mg	41.0	20400		μg/L	SW6010B	08/27/99
Manganese, Mn	1.0	14.5		μg/L	SW6010B	08/27/99
Mercury, Hg	0.25	0.25	U	μg/L	SW7470A	08/23/99
Potassium, K	1810	17800		μg/L	SW6010B	08/27/99
Selenium, Se	6.8	6.8	U	μg/L	SW6010B	08/27/99
Silver, Ag	8.0	8.0	U	μg/L	SW6010B	08/27/99
Sodium, Na	5930	157000		μg/L	SW6010B	08/27/99
Strontium, Sr	28.6	1870		μg/L	SW6010B	08/27/99
Zinc, Zn	2.3	46.3		μg/L	SW6010B	08/27/99

Client Information

Lab Information

Client Sample ID: ZGP

Lab Sample ID: 996401

Project Name: McAllen WWTP #2, City of

Analysis Method: SW 8260B

Project Manager: Angie Fernandez/PHX

Units: µg/L

Sampled By: R. Trevino Date Collected: 8/17/99

Date Received: 8/18/99 Date Analyzed: 8/27/99

Time Collected: 7:30

Dilution Factor: 1 Report Revision No.: 0

Type: Grab Matrix: Water

Reported By: MCB Reviewed By: 342

Basis: As Received

Analyte	CAS#	Reporting Limit	Sample Result	Qualifier
D				
Purgeable Volatiles				
Vinyl Chloride	75-01-4	1.0	1.0	U
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	U
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	U
1,1,1-Trichloroethane	71-55-6	1.0	1.0	U
Carbon Tetrachloride	56-23-5	1.0	1.0	U
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	1.0	U
Dibromofluoromethane	1868-53-7		94%	SS
1,2-Dichloroethane-d4	17068-07-0		89%	SS
Toluene-d8	2037-26-5		103%	SS
p-Bromofluorobenzene	460-00-4		103%	SS

E=Estimated value above instrument calibration range

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

SS=Surrogate standard

Client Information

Lab Information

Client Sample ID: ZGP

Lab Sample ID: 996401

Project Name: McAllen WWTP #2, City of

Analysis Method: SM 5710.D

Project Manager: Angie Fernandez/PHX

Date Received: 8/18/99

Sampled By: R. Trevino Date Collected: 8/17/99 Time Collected: 7:30

Report Revision No.: 0 Analyzed By: BDW

Type: Grab

Reviewed By: 2494

Matrix: Water Basis: As Received

SDS-HAA/THM Formation Potential Test Conditions

	Target			Contact	Chlorine	
Set-up Date/Time	Contact Time (h:mm)	Initial pH	Contact pH	Temperature (°C)	Dosage (mg/L)	
8/23/99 9:34	72:00	7.7	7.8	23	10.10	-

Chlorine Demand Test Results

Take-off Date/Time	Actual Contact Time (h:mm)	Measured pH	Measured Temperature (°C)	Chlorine Residual (mg/L)
8/26/99 13:10	75:36	7.8	23	0.68

Client Information

Client Sample ID: ROP

Project Name: McAllen WWTP #2, City of Project Manager: Angle Fernandez/PHX

Basis: As Received

Sampled By: R. Trevino Sampling Date: 08/17/1999 Sampling Time: 7:30 Type: Grab Matrix: Water Lab Information

Lab Sample ID: 996402

Date Received: 08/18/1999 Report Revision No.: 0

Analyzed By: DK/MG/MS/JJB
Reviewed By: ----------------------/ 24

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
Alkalinity (as CaCO3)	2.0	14		mg/L	EPA 310.2	08/23/1999
Bromide	0.020	0.020	U	mg/L	EPA 300.0-B	08/19/1999
Chloride	0.10	9.73		mg/L	EPA 300.0-A	08/23/1999
Color (APHA) Apparent		5	U	color units	EPA 110.2	08/18/1999
Fluoride	0.10	0.32		mg/L	EPA 300.0-A	08/23/1999
N-Nitrate	0.01	1.11		mg/L	EPA 353.2	08/19/1999
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	08/25/1999
Silica-React.	0.40	0.65		mg/L	SM4500-Si D	09/01/1999
Sulfate	0.10	4.00		mg/L	EPA 300.0-A	08/23/1999
Total Dissolved Solids	5	33		mg/L	EPA 160.1	08/23/1999
TOC	0.50	0.63		mg/L	EPA 415.1/2	08/19/1999
Total Phosphate-P	0.05	0.10		mg/L	EPA 365.2/4	08/19/1999

Client Information

Client Sample ID: ROP

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Sampled By: R. Trevino Sampling Date: 08/17/99 Sampling Time: 07:30 Type: Grab

Matrix: Water Basis: As Received **Lab Information**

Lab Sample ID: 996402

Date Received: 8/18/99 Report Revision No.: 0

Reported By: JG

Reviewed By:

Analyte	MRL	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
	· · · · · · · · · · · · · · · · · · ·	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,				
Aluminum, Al	45.6	45.6	U	μg/L	SW6010B	08/27/99
Arsenic, As	3.9	3.9	U	μg/L	SW6010B	08/27/99
Barium, Ba	0.81	0.81	U	μg/L	SW6010B	08/27/99
Cadmium, Cd	0.38	0.38	U	μg/L	SW6010B	08/27/99
Calcium, Ca	21.3	714		μg/L	SW6010B	08/27/99
Chromium, Cr	7.2	7.2	U	μg/L	SW6010B	08/27/99
Iron, Fe	2.8	9.9		μg/L	SW6010B	08/27/99
Lead, Pb	2.3	2.3	U	μg/L	SW6010B	08/27/99
Magnesium, Mg	41.0	197		μg/L	SW6010B	08/27/99
Manganese, Mn	1.0	1.0	U	μg/L	SW6010B	08/27/99
Mercury, Hg	0.25	0.25	U	μg/L	SW7470A	08/23/99
Potassium, K	181	1360		μg/L	SW6010B	08/27/99
Selenium, Se	6.8	6.8	U	μg/L	SW6010B	08/27/99
Silver, Ag	8.0	8.0	U	μg/L	SW6010B	08/27/99
Sodium, Na	593	13000		μg/L	SW6010B	08/27/99
Strontium, Sr	28.6	28.6	U	μg/L	SW6010B	08/27/99
Zinc, Zn	2.3	7.2		μg/L	SW6010B	08/27/99

Client Information Lab Information

Client Sample ID: ROP Lab Sample ID: 996402

Project Name: McAllen WWTP #2, City of Analysis Method: SW 8260B

Project Manager: Angie Fernandez/PHX
Sampled By: R. Trevino
Date Received: 8/18/99
Date Collected: 8/17/99
Date Analyzed: 8/27/99
Time Collected: 7:30
Dilution Factor: 1
Type: Grab
Report Revision No.: 0

Matrix: Water Reported By: MCB Basis: As Received Reviewed By: >AH

Analyte	CAS#	Reporting Limit	Sample Result	Qualifier
Purgeable Volatiles				
Vinyl Chloride	75-01-4	1.0	1.0	U
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	Ŭ
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	Ü
1,1,1-Trichloroethane	71-55-6	1.0	1.0	Ū
Carbon Tetrachloride	56-23-5	1.0	1.0	Ü
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	1.0	U
Dibromofluoromethane	1868-53-7		96%	SS
1,2-Dichloroethane-d4	17068-07-0		96%	SS
Toluene-d8	2037-26-5		104%	SS
p-Bromofluorobenzene	460-00-4		103%	SS

E=Estimated value above instrument calibration range

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

SS=Surrogate standard

Client Information

Client Sample ID: ROP

Project Name: McAllen WWTP #2, City of

Project Manager: Angie Fernandez/PHX

Sampled By: R. Trevino Date Collected: 8/17/99 Time Collected: 7:30

> Type: Grab Matrix: Water Basis: As Received

Lab Information

Lab Sample ID: 996402

Analysis Method: SM 5710.D

Date Received: 8/18/99 Report Revision No.: 0

Analyzed By: BDW

Reviewed By: 242

SDS-HAA/THM Formation Potential Test Conditions

	Target			Contact	Chlorine
Set-up Date/Time	Contact Time (h:mm)	Initial pH	Contact pH	Temperature (°C)	Dosage (mg/L)
8/23/99 9:42	72:00	6.0	7.8	23	1.30

Chlorine Demand Test Results

Take-off Date/Time	Actual Contact Time (h:mm)	Measured pH	Measured Temperature (°C)	Chlorine Residual (mg/L)
8/26/99 13:14	75:32	7.8	23	0.24

			Formation Po	tential Trihalom	ethanes (THM	s) Disinfection B	y-Products, (ug/L)
		FP	FP	FP	FP	FP	
Client ID	Lab ID	CHC13	BDCM	DBCM	CHBr3	TTHM	
McALLEN-ZGP-3D	300301	150	38.8	9.5	<1	198	CHCl3 = Chloroform
McALLEN-ROP-3D	300302	3.7	1.7	I	<i< td=""><td>5.4</td><td>BDCM = Bromodichloromethane</td></i<>	5.4	BDCM = Bromodichloromethane
						[·	DBCM = Dibromochloromethane
							CHBr3 = Bromoform
						11	
							EPA TTHM Stage 1 MCL = 80 ug/L
					·	†I	EPA TTHM Stage 2 MCL = 40 ug/L
		·					

			Formation Po	tential Haloac	etic Acids (HAA:	s) Disinfection 1	By-Products (ug	/L)			
		FP	FP	FP	FP	FP	FP	FP	FP		
Client ID	Lab 1D	MCAA *	MBAA *	DCAA *	TCAA *	BCAA	DBAA *	HAA5	HAA6		
McALLEN-ZGP-3D	300301	8.6	1.4	49.9	57.3	12.8	1.6	119	132		
McALLEN-ROP-3D	300302	<2	</td <td>1.1</td> <td><1</td> <td><!--</td--><td><l< td=""><td>1.1</td><td>1.1</td><td>1</td><td></td></l<></td></td>	1.1	<1	</td <td><l< td=""><td>1.1</td><td>1.1</td><td>1</td><td></td></l<></td>	<l< td=""><td>1.1</td><td>1.1</td><td>1</td><td></td></l<>	1.1	1.1	1	
					·		ļ			_ _	ļ
									· ·		
				ļ							
					1			· · · · · · · · · · · · · · · · · · ·			
							I				
		MCAA = Monoc	hloroacetic acia	'	BCAA = Bromo	chloroacetic aci	d	EPA HAA5 Stage 1 N	ACL = 60 ug/L		
		MBAA = Monob	romoacetic acid		DBAA = Dibron	noacetic acid		EPA HAA5 Stage 2 N	MCL = 30 ug/L	T	L
		DCAA = Dichlo	roacetic acid		* These compou	nds make up the	HAA5				
		TCAA = Trichlo	roacetic acid		= Estimated val	ие	1				

ì

Client Information

Client Sample ID: McAllen-ZGP-3d

Lab Sample ID: 300301

Project Name: McAllen WWTP #2, City of

Date Received: 8/26/99 Report Revision No.: 0

Lab Information

Project Manager: Angie Fernandez/PHX Sampled By: B. Warloe Date Collected: 8/26/99

Analyzed By: DAH
Reviewed By: mbos

Time Collected: Not Indicated

Type: Grab Matrix: Water Basis: As Received

Analyte	CAS#	MCL*	Reporting Limit	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
Haloacetic Acids								
Chloroacetic acid	79-11-8		2.0	8.6		μg/L	SM 6251.B	9/3/99
Bromoacetic acid	79-08-3		1.0	1.4		μg/L	SM 6251.B	9/3/99
Dichloroacetic acid	79-43-6		5.0	51.4		μg/L	SM 6251.B	9/16/99
Trichloroacetic acid	76-03-9		5.0	56.0		μg/L	SM 6251.B	9/16/99
Bromochloroacetic acid	5589-96-3		1.0	12.8		μg/L		9/3/99
Dibromoacetic acid	631-64-1		1.0	1.6		μg/L		9/399
HAA5		60	5.0	119		μg/L	SM 6251.B	9/16/99
2,3-Dibromopropanoic ac	ei 600-05-5			116%	SS			
Trihalomethanes								
Chloroform	67-66-3		5.0	150		μg/L	EPA 502.2	9/1/99
Bromodichloromethane	75-27-4		1.0	38.8		μg/L	EPA 502.2	8/31/99
Dibromochloromethane	124-48-1		1.0	9.5		μg/L		8/31/99
Bromoform	75-25-2		1.0	1.0	U	μg/L	EPA 502.2	8/31/99
ТТНМ		80	1.0	198		μg/L	EPA 502.2	9/1/99
1,2-Dichloroethane-d4	17068-07-0			102%	SS			

U=Not detected at specified reporting limit *=MCL according to Stage 1 of D/DBP rule SS=Surrogate standard

Client Information

Lab Information

Client Sample ID: McAllen-ROP-3d

Lab Sample ID: 300302

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Date Received: 8/26/99 Report Revision No.: 0 Analyzed By: DAH

Sampled By: B. Warloe
Date Collected: 8/26/99

Analyzed By: DAH Reviewed By: mbos

Time Collected: Not Indicated

Type: Grab Matrix: Water Basis: As Received

Analyte	CAS#	MCL*	Reporting Limit	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
Haloacetic Acids								
Chloroacetic acid	79-11-8		2.0	2.0	U	μg/L	SM 6251.B	9/3/99
Bromoacetic acid	79-08-3		1.0	1.0	U	μg/L		9/3/99
Dichloroacetic acid	79-43-6		1.0	1.1			SM 6251.B	9/3/99
Trichloroacetic acid	76-03-9		1.0	1.0	U	μg/L		9/3/99
Bromochloroacetic acid	5589-96-3		1.0	1.0	U	μg/L		9/3/99
Dibromoacetic acid	631-64-1		1.0	1.0	Ü	μg/L		9/3/99
HAA5		60	1.0	1.1			SM 6251.B	9/3/99
2,3-Dibromopropanoic ac	i 600-05-5			115%	SS			
Trihalomethanes								
Chioroform	67-66-3		1.0	3.7		μg/L	EPA 502.2	8/31/99
Bromodichloromethane	75-27-4		1.0	1.7		μg/L		8/31/99
Dibromochloromethane	124-48-1		1.0	1.0	U	μg/L		8/31/99
Bromoform	75-25-2		1.0	1.0	Ŭ	μg/L		8/31/99
TTHM	,0202	80	1.0	5.4	Ü	μg/L		8/31/99
1,2-Dichloroethane-d4	17068-07-0			99%	SS			

U=Not detected at specified reporting limit *=MCL according to Stage 1 of D/DBP rule SS=Surrogate standard

CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Walnut Boulevard Corvalils, OR 97330-3638 (541) 752-4271 FAX (541) 752-0278

															· · · · · ·												C #		
Project #							P	urch	186	Orc	ler i	•			1			Requ	lested	Analyti	cal Me	thod#			THIS A	REA FO	R LAB	USE O	NLY
															_ ,	[}	""					Lab#	1	Pi	ge	Of
Project Name		Λ). ,		/	cl	. 1					Ö				1 4	p		25	2.0		1991	04	-		
McAlles Company Name	1_	<u> [Ce</u>	u	<u>L</u>	<u> </u>	1/0	27)	ud	4				- Å				200	23		200	2 0		Lab PM		Ċ	ustody	Review
Company Name	_	v	20	<i>n 1</i>	i						•					3	3 4	10 0	3 6	3 3		20	2 6				1		
City O Project Manage	+		110	1411	er	v_									- ``	25	£ 2	4 8	50	1		5 9	ي چ		Log In		- 	ue Var	fication
Project Manage	or (Con	tect	& Pi	ione			еро							F		HAAS, THMS	SDS HAAS	TKW , NO3 - NO2	TKU, NO3-NOZ, T-PLosphorous	50	S a	TKU, NO3-NOZ, T-Phosphorous	5	rog m		"	MO ARI	IICation
Kally McK	104	eu					1	M	4	Me	K	nl	eu		C	Z V	505	S S	ع م		0	29	25	a					
Requested Compl	rtion	Dat	e:	Site	ID						T)isposel:	Ň	3	\$05 \$ 05	Spo	メデ	3 7	-	34	X	17	рH		C	ustody	Seale Y N
1 1 1 1 1			ļ			- 1	#	7			Ī	Diag	2000	Return	1	ļ	/					/- ·					lc	9	(YW
ASAP				W	ω	11		<u> </u>				¥:	<u> </u>	<u> </u>	N E				Pro	eservat	Ive		,		QC Level 1	2 2	3 Oth		
	Ty	pe	Ma		-										A				-			7	<u> </u>	۱ ۵	QC Level		- Oth	er .	
Sampling	0	Ä	Ă		1			ENT)		LAB		La	9	9	SO	Õ	ال	SO4	000	ع	Cooler Temp	erature	1	1—	
Date Time	P	B	Ė	A I R			(9 (CHA	RAC	TEF	is)			QC		H	70	ICE	H2.504	4554	H	H25	H2504	H	Altern	ate Desc	rintia	<u>.</u>	Lab ID
		-+	-	+-	1	Τ.	Т.		T-	$\overline{}$	T	$\overline{}$	1		+-	 	 ' -	 	 _		11				Altern	ale Desc	- Puoi	<u>'</u>	
8/17/19/07:30		4	4	1	12		P		\perp		-	\perp			11		ļ		<u> </u>	ļ	ļ	ļ					_		<u> </u>
8/17/99 "		\checkmark	V		R				1,	1	1/	77	11	,		<u> </u>	<u></u>	1	<u> </u>		ļ	ļ							2
8/17/99 11			4	-	2	9	P	15.44	7.	3/	$\int_{\mathcal{I}}$	g_{i}^{\dagger}		ļ	11	ļ						ļ	ļ ·						
8/17/19 11		ス	7		R	0				1	1	1			1				-										3
8/17/29 11			オ	1-	R	٥			1	1	T	\top	1		1,														ラ
			1		R	7	1.	1	+		\dagger	╁	1		1:		}	1	 			-	i						323
8/17/99 11	-			+-					+	+	+	╂	+-		╁╌	 	 		 			 							12
8/17/99 4	Н	4		-	2	G	F	1.	+			╀	١.	<u> </u>	+	ļ	ļ	↓	ļ		ļ		ļ						<u> </u>
8/17/25 11		コ	1	_ _				#		84						ļ		ļ	ļ		ļ		~		- 				4
1/17/99 11		レ		_	W	W	1) =	2 8	H	lu	Je s	$\sqrt{+}$											_					14
		-					T			7		-																	
		7					T	1				1	1		1														
Relinquished By	٠,,				ı	1	ــــــــــــــــــــــــــــــــــــــ				٠		ate/T		Receiv		<u> </u>	-	Emp	ty Bottle	\$		L	Date/Ti	8/17/99				
Reinquished By	U	ar	100	ℓ_{-}										1:25				_ `		<u> </u>					8/17/99	0	7:2	<u>5 </u>	 .
Sampled By and T	itie	_ •			Ø	Please A M	elgn A∕\	and pr	int naz > (/	ne)		27	ate/T	lme 1 7:30	Relinq	ulshed E	у			-	ign and pric	nt name) (CV) N		Date/II	me	7 :39			
Received By					(1	Please	algn	end pr	int ner	ne)		þ	ate/T	lme	Reling	ulshed E	ly ·			(Please E	ign and prir	nt name)		Date/Ti	717/99	<u> </u>			
Ropie VI	la	na	<u>u</u>	<u> </u>				<u> 1] (</u>			<u> 1</u>	_		7:39		<u>eir 1</u>	/Ma	red		Rosic	<u>- Vil</u>	MRZ	n)	<u> </u>	117/99				
Received By					(1	Please	e elgn	and pr	int ne	ne)		0	ate/T	imė	Shippe UP8	od Via Fed-l	ix (Other		8	hipping	*							
Special instructio	na:		744									ļ					····	-											
1																													

CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Walnut Boulevard Corvalits, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

Purchase Order # Project # Requested Analytical Method # THIS AREA FOR LAB USE ONLY Lab : **Project Name** 0 McAllen Reuse Pilot Study 0 Lab PM **Custody Review** 9 2 N ∞ Log In LIMS Verification 3Cs Kayly Mckinley
Requested Completion Date: Kashy Mckinley \bigcirc d pН Custody Seals Y ASAP WWTP#2 Preservative QC Level 1 2 3 Other H2504 Type H2504 H2504 W S A A O I T I R E L R CORAB PB Sampling S **CLIENT SAMPLE ID** 子に LAB Cooler Temperature 土 (9 CHARACTERS) Time Date Aitemate Description Lab ID 191 2 8 17/19 7:30 ROP 2 x117/94 7:30 ROP 8/11/97:32 2_ wwtp#2 Effluent 2 nh9 7:37 R 0 Z 4 2 8/17/19 7:30 **Empty Bottles** Relinquished By Date/Time Received By Date/Time Booie Villaned 7:25 8/17h9 7:25 Sampled By and Title Date/Time Refinguished By (Please sign and print name) Date/Time (Please sign and print name) 8/17/97:30 X IL 7:39 RammTlevino Runn Tierino Date/Time Date/Time Reijnquished By (Please sign and print name) Received By Logie Posie VillARREAL osie VIII nRRENI 8/17/99 7:39 llanı L copie Shipping # Date/Time Shipped Via Received By (Please sign and print name) Fed-Ex Other Special instructions:

CH2MHILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Walnut Boulevard Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

																									COC		JUI DUC
Project (ŧ						Į	P	urch	480	Orde	r#			1					Analyt		thod #		THIS	AREA FOR	LAB USE O	NLI
Project I	Name Ollean			, 50	P	 :	· / ·		- Inc	 {\(\lambda \)	_				TOTAL	Mg, M,	75	(also,	46,	Al Ba, Ca, Fe, Mg, Mn, K, Na, Sr, As, Ca, Cr,	471	Braide, Chloride, Fluoride, Sulfede,		Lab#	64	Page	OI 3
Compan	y Name	<i>-</i> -	-0.0			, <u>/</u> <u> </u>			,	7					- î	ن ع	19	2,4	ने द	القري	क्	15 H	4	COD PM		Custody	LIBAIRM
C; ¢	- 4 0	t.	m	A	110	h)										F. A.	3	F .		12 X	5	ि दुर्ग र				_	
Project A	lanage	ror	Con	tact	& Ph	one	#	R	epor	t Co	py to	:		******	- ₽	g %	18	37	4	ું છે. દ્ર	S	7000	!	Log In		LIMS Veri	fication
Kath	y M	4	Sin	lei	-			k	W	41	nck	(i)	ley	Disposal:	CON	A1, Ba, Ca, Fe, N	, на	alin	10 . T	8a, 8a	, H5, Se, H3, Zn	Alkalinity, TOS, Samide, Chlor Fluoride, Sulf		рН			
Requeste	i Compi	etio	n Det	- 1								- 1				₹ ¥	9	造品		Z Z	46	A 2017 %	2	l bu		Custody	Seals Y N
AS	AP			-	W	W	N	H	2			P	leposa []	Return	A			1	P	reserva	tive	1 -				Ice	(v)}
			/ре	 Mat		Γ			 -					Ι	Ë		ሐ	 	T	-}		1	1	QC Level	1 2 3	Other	
Samp	ling			W S A O T E R							PLE TERS			LAB	8	Hr33.	0		4		€? <u>*</u>	3		Cooler Tem	perature	4	
Date	Time			Ē L			•					,				1		F	+ 1	群 =	丰			Alten	nate Descri	iption	Lab ID
\$ 17/79	הג:7	Τ	V	7		R	0	P	7						1	,											2
8/17/99	1.20	1	J		1	R	3	P		1		\dashv	_		1,	\		— ,		<u> </u>		1-1					7
811 (111	1.30	+-	J		1-	5	7	P		 		-		 		1	1		1	rost,							
sl17/19	1:30	╁╴	\Box	-	+	2 2	9	r	+			\dashv	-	1 -	1	1			 -`	1000			}				1
8/17/99	7:30	╀	1	1	+-	1	4	P	-	-	\vdash	-		 -		ļ	 		 		 	<u> </u>	 -				
		<u> </u>	Ш		1-	_	 -	_	-	-	\vdash	\dashv	_	ļ	- -	ļ	ļ	 			ļ	 					
		L		_	1_				\perp			_ _	_	ļ			ļ		ļ		ļ		<u> </u>				<u> </u>
		_			1_		ļ									<u> </u>			<u> </u>	<u> </u>							
		1		_	1	-			1			7	\top	<u> </u>	1	-	1	1	1	1	 						
		-	╁╌╂	+	+-		t-	-	+	-	-	+		 	+-	 	 	 	 	1		 	<u> </u>				·
		┼	$\left \cdot \right $	+	+-			├	╁╌	-	-+	+	+-	 -		 	 -	+			 						
Relinguis	had By	_				<u> </u>	1	L.				+	Date/	lme.	Becel	red By	ــــــــــــــــــــــــــــــــــــــ		Em	pty Bottk	<u> </u>		Detect				<u> </u>
100		V.	ill	an	10d	-						1	linh	9		L	٤			4	•		Date/T	717/99			
Sampled	By and T	Title				_ (F			and pri	k name)			17:30	XK		1			Rar	July W	Transa	Date/T	me paka	07:3	19	
Received	Ву	111	an	1	_	(F	10054	elgn	and pri	RR		, [,	Date/1	Time 7 b7:39	Relino	julshed !	By .	lane		(Please	algn and pr	HRREAL	Date/Ti	8/17/99			
Received	By	المك	A TA	ure						t name		╙	Date/		Shipp	od Via	vui	wyw	<u>"\</u>		Shipping	<u> 17にを長り</u> 東	<u> </u>	011111			
Ĺ															UPS	Fed-	Ex	Other -				·	. 				
Special in	atructio	ns:																								· ·	



Ms. Anne McKee-Robbins CH2M HILL/CVO 2300 N.W. Walnut Blvd. Corvallis, OR 97330

> Columbia Analytical Services Report City of McAllen D9901502/D1227

> > September 13, 1999

Submitted by:

Beyon force

Bryan Jones

Project Manager/Client Services

TABLE OF CONTENTS

CAS Lab Reference No.: D1227 Level 1

	Page
	No.
Organic Data Qualifiers	i
Organic Sample ID Qualifiers	
Sample Identification Cross-Reference	iii
GC ORGANOCHLORINE PESTICIDES	1
Case narrative	
Sample results	
Chain of Custody Documentation	17

Organic Data Qualifiers

- A-- This qualifier indicates that a TIC is a suspected aldol-condensation product
- **B--** This flag is used when the analyte is found in the associated blank as well as the sample. This notation indicates possible blank contamination and suggests that the data user evaluate these compounds and their amounts carefully.
- C-- The "C" flag indicates the presence of this compound has been confirmed by the GC/MS analysis.
- **D--** This qualifier is used for all the compounds identified in an analysis at a secondary dilution factor. "D" qualifiers are used only for the samples reported at more than one dilution factor.
- E-- This flag indicates that the value reported exceeds the linear calibration range for that compound. Therefore, the sample should be reanalyzed at the appropriate dilution. The "E" qualified amount is an estimated concentration, and the results of the dilution will be reported on a separate Form I.
- I-- The qualifier indicates that the reporting limit to the "I" qualifier has been raised. It is used when the chromatographic interference prohibits detection of a compound at a level below the concentration expressed on the Form I.
- J- Indicates an estimated value. It is used when the data indicates the presence of a target compound below the reporting limit or the presence of a Tentatively Identified Compound (TIC).
- N-- This qualifier indicates presumptive evidence of a compound. This flag is only used for Tentatively Identified Compounds (TIC), where the identification is based on a mass spectral library research. It is applied to all TIC results. For generic characterization of a TIC, such as chlorinated hydrocarbon, the "N" qualifier is not used.
- P-- This qualifier is used for Pesticide/Aroclor target analytes when there is a greater than 25% difference for detected concentrations between the two columns. The lower of the two values is reported on Form I and flagged with a "P".
- U-- Indicates the compound was analyzed for but not detected. The number adjacent to the "U" qualifier indicates the reporting limit for that compound. The reporting limit can vary from sample to sample depending on dilution factors or percent moisture adjustments when indicated.

Organic Sample ID Qualifiers

The qualifiers that may be appended to the Lab Sample ID and/or the Client Sample ID for organic analysis are defined below:

- **DL--** Diluted reanalysis. Indicates that the results were determined in an analysis of a secondary dilution of a sample or extract. A digit to indicate multiple dilutions of the sample or extract may follow the "DL" suffix. The results of more than one diluted reanalysis may be reported.
- **MS--** Matrix spike (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- MSD-- Matrix spike duplicate (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- R-- Reanalysis. The extract was reanalyzed without re-extraction. The "R" is not used if the sample was also re-extracted. May be followed by a digit to indicate multiple reanalysis of the sample at the same dilution.
- **RE--** Re-extraction analysis. The sample was re-extracted and reanalyzed. May be followed by a digit to indicate multiple re-extracted analysis of the same sample at the same dilution.

Sample ID Cross-reference Table

CAS Lab Sample	Client ID Sample ID	Collect Date Sample Matr	ix Additiona	l Description	
FS = Field	d Sample				
D1227001 D1227002	FS ZGPERMEATE FS ROPERMEATE	08/17/99 Water 08/17/99 Water			

The above lab sample ID's and cross reference information apply to samples as received by the laboratory. Modifiers to the lab sample ID may be added for internal tracking purposes. Any modified sample ID will be reflected in the appropriate case narrative only.

GC ORGANOCHLORINE PESTICIDES

CASE NARRATIVE GC ORGANOCHLORINE PESTICIDES

CAS	Lab	Reference	No./SDG.:	D1227

Project: City of McAllen

I. RECEIPT

No exceptions were encountered unless a Sample Receipt Exception Report is attached to the Chain-of-Custody included with this data package.

II. HOLDING TIMES

- A. Sample Preparation: All holding times were met.
- B. Sample Analysis: All holding times were met.

III. METHOD

Preparation: SW-846 3520C

Cleanup: NA

Analysis: SW-846 8081A

IV. PREPARATION

Sample volume may vary based on the amount of sample received per container.

V. ANALYSIS

- A. Calibration. In the ending CCV, toxaphene, exceeded 15%D however the average of all analytes was within therefore no corrective action was taken.
 - 1. Retention Time Windows: All analytes were within criteria.
 - Degradation: All acceptance criteria were met.
- B. Blanks: All acceptance criteria were met.
- C. Surrogates: All acceptance criteria were met.
- D. Internal Standards: All acceptance criteria were met.
- E. Spikes: All acceptance criteria were met.
- F. Samples: Sample analysis proceeded normally.

I certify that this data package is in compliance with the terms and conditions agreed to by the client and Columbia Analytical Services, both technically and for completeness, except for the conditions noted above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or designated person, as verified by the following signature.

SIGNED: Jerry Watega 9/10/99 Reviewer: Hope Walker 9-10-99

Scientist, GC Organics

PWB10820

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227

SDG No.: D1227

Lab Sample ID:

PWB10820

Matrix:

WATER

Extraction Type: Continuous

Level: LOW Lab File ID:

B0904010

Sample Wt/Vol: 1.000 L

Date Received:

Extract Vol:

Date Extracted: 08/20/99

10 ML

Date Analyzed: 09/04/99

Column: DB5

Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8	gamma-BHC (L Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.020 0.040 0.50	משט

LOW

CLIENT ID.

PWB10820LCS

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227

SDG No.: D1227

Lab Sample ID:

PWB10820LCS

Matrix: WATER

Level:

Lab File ID:

B0904008

Sample Wt/Vol: 1.000 L

Date Received:

Date Extracted: 08/20/99

Extract Vol:

Date Analyzed: 09/04/99

Column: DB5

Extraction Type: Continuous

Dilution Factor: 1.0

CAS NO. COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
58-89-9gamma-BHC (72-20-8Endrin 72-43-5Methoxychlo 8001-35-2Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.56 0.52 0.46 0.50	Ū

CLIENT ID.

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

PWB10820LCS

Case No.: D1227 SDG No.: D1227

Lab Sample ID: PWB10820LCS

Matrix: WATER Level: LOW

Lab File ID:

B0904009

Sample Wt/Vol: 1.000 L

Date Received:

Extract Vol:

10 ML

Date Extracted: 08/20/99

Column: DB5

Date Analyzed: 09/04/99

Extraction Type: Continuous

Dilution Factor: 1.0

CAS NO. COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
58-89-9gamma-BHC (I 72-20-8Endrin 72-43-5Methoxychlor 8001-35-2Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.090 0.075 5.1	U

CLIENT ID.

ZGPERMEATE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227 Lab Sample ID: D1227001

Matrix: WATER Level: LOW Lab File ID: B0904011

Sample Wt/Vol: 1.000 L Date Received: 08/18/99

Extract Vol: 10 ML Date Extracted: 08/20/99

Column: DB5 Date Analyzed: 09/04/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8 72-43-5	gamma-BHC (L Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.024 0.020 0.040 0.50	U U

CLIENT ID.

ROPERMEATE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

. . . .

Case No.: D1227 SDG No.: D1227 Lab Sample ID: D1227002

Matrix: WATER Level: LOW Lab File ID: B0904012

Sample Wt/Vol: 1.000 L Date Received: 08/18/99

Extract Vol: 10 ML Date Extracted: 08/20/99

Column: DB5 Date Analyzed: 09/04/99

Extraction Type: Continuous Dilution Factor: 1.0

CAS NO. COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
58-89-9gamma-BHC 72-20-8Endrin_ 72-43-5Methoxychl 8001-35-2Toxaphene_		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.020 0.040 0.50	ת מ מ

WATER SEMIVOLATILE SURROGATE RECOVERY

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227

	l 		- 63			
	1	l <u> </u>	S1	S2	S2	TOT
	LAB ID	CLIENT ID.	#	#	,	OUT
	=========	=======================================	======	=====	=====	===
01	PWB10820LCS	PWB10820LCS	107	86		ol
02	PWB10820LCS	PWB10820LCS	105	72		Ö
03	PWB10820	PWB10820	102	76		
						0
04	D1227001	ZGPERMEATE	105	74		0
05	D1227002	ROPERMEATE	68	47		0
06				l :		
07						
08						
09						
10		·····				
11	 -					
12						
12						
13						
14						
15						
16						
17						
18						
19						
20	· —————					
21						——]
21	 					
22						<u> </u>
23						
24						
25		l			-	
26						
27						— I
28						
29						
30			l	l		

QC LIMITS (45-125) = Tetrachloro-m-xylene S1 = Decachlorobiphenyl (34-133)

Column to be used to flag recovery values
* Values outside of contract required QC limits

D Surrogates diluted out

3E WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227

SDG No.: D1227

Column: DB5

LCS - Sample No.: PWB10820

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
gamma-BHC (Lindane)	0.5000	0.0000	0.5583	112	73-125
Endrin	0.5000	0.0000	0.5193	104	43-134
Methoxychlor	0.5000	0.0000	0.4603	92	73-142

Column to be used to flag recovery and RPD values with an asterisk

* Values ou	tside	of	OC	li	mi	ts
-------------	-------	----	----	----	----	----

RPD: 0 out of 0 outside limits Spike Recovery: 0 out of 3 outside limits

COMMENTS:	 	 	 	 _,	

WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227

SDG No.: D1227

Column: DB5

LCS -

Sample No.: PWB10820

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
Toxaphene	5.000	0.0000	5.095	102	41-126

- # Column to be used to flag recovery and RPD values with an asterisk
- * Values outside of QC limits

RPD: 0 out of 0 outside limits Spike Recovery: 0 out of 1 outside limits

COMMENTS:	

SW846

SEMIVOLATILE METHOD BLANK SUMMARY

Client ID.

PWB10820

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227

SDG No.: D1227

Lab File ID:

B0904010

Lab Sample ID:

PWB10820

Date Extracted:

08/20/99

Extraction Type:

CONT

Date Analyzed: 09/04/99

Time Analyzed:

2010

Matrix:

WATER

Level: (low/med)

LOW

Instrument ID:

GCB

THIS METHOD BLANK APPLIES TO THE FOLLOWING SAMPLES, MS and MSD:

	CLIENT ID.	LAB SAMPLE ID	LAB FILE ID	DATE ANALYZED
01 02 03 04 05 06 07 08 09 10 11 12 13 14 15 16 17 18 19 19 19 19 19 19 19 19 19 19 19 19 19		i	B0904008 B0904009 B0904011 B0904012	09/04/99 09/04/99 09/04/99 09/04/99
21 22 23				

7B PESTICIDE CONTINUING CALIBRATION CHECK

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Instrument ID: GCB Case No.: D1227 SDG No.: D1227

GC Column: DB5 ICAL Date/Time (1st pt): 08/23/99 0959

ICAL Date/Time (Last pt): 08/23/99 1314

CONTRACT	AVERAGE		CT 1771		MAX
COMPOUND	RF	RF	CURVE	%D	%d
	=======		=======	=====	====
alpha-BHC	2.751	2.834	AVG		15.0
beta-BHC	0.871	0.873	AVG		15.0
delta-BHC	2.640	2.722	AVG		15.0
gamma-BHC (Lindane)	2.495	2.682	AVG		15.0
Heptachlor	2.542	2.637	AVG		15.0
Aldrin	2.351	2.464	AVG		15.0
Heptachlor epoxide	2.134	2.243	AVG		15.0
Endosulfan I	1.886	1.816	AVG		15.0
Dieldrin	2.243	2.299	AVG	2.5	15.0
4,4'-DDE	1.919	1.835	AVG	-4.4	15.0
Endrin	1.972	1.946	AVG	-1.3	15.0
Endosulfan II	1.832	1.774	AVG	-3.2	15.0
4,4'-DDD	1.503	1.447	AVG	-3.8	15.0
Endosulfan sulfate	1.801	1.593	AVG	-11.5	15.0
4,4'-DDT	1.717	1.709	AVG	-0.4	15.0
Methoxychlor	0.903	0.865	AVG	-4.2	15.0
Endrin ketone	1.951	1.832	AVG	-6.1	15.0
Endrin aldehyde	1.334	1.278	AVG	-4.2	15.0
alpha-Chlordane	2.115	2.176	AVG		15.0
gamma-Chlordane	2.117	2.087	AVG		15.0
	=======	=======	======	=====	====
Tetrachloro-m-xylene	1.075	1.146	AVG	6.6	20.0
Decachlorobiphenyl	1.920	1.713	AVG	-10.8	20.0
		i		,	
	· —————				· ——— ·

PESTICIDE CONTINUING CALIBRATION CHECK

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Instrument ID: GCB

Case No.: D1227

SDG No.: D1227

Lab File ID: B0904005

CCV Date/Time:

09/04/99

1605

GC Column: DB5

ICAL Date/Time (1st pt): 08/22/99

1725

ICAL Date/Time (Last pt): 08/22/99

2040

COMPOUND	AVERAGE RF	RF	CURVE	%D	MAX %d	
=======================================	=======	=======	=======	=====	====	1
Toxaphene	0.044	0.038	AVG	-12.0	15.0	İ
(2)	0.047	0.039	AVG	-17.6	15.0	<-
(3)	0.050	0.048	AVG	-4.3	15.0	1
						1

7B PESTICIDE CONTINUING CALIBRATION CHECK

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Instrument ID: GCB

Case No.: D1227

SDG No.: D1227

Lab File ID: B0904020

CCV Date/Time:

09/05/99

0417

GC Column: DB5

ICAL Date/Time (1st pt): 08/23/99

0959

ICAL Date/Time (Last pt): 08/23/99

1314

	AVERAGE				MAX	!
COMPOUND	RF	RF	CURVE	%D	%d	
alpha-BHC	2.751	2 102	7770	=====	====	
beta-BHC	0.871	3.182 0.968	AVG		15.0	<-
		1	AVG		15.0	İ
delta-BHC	2.640	2.951	AVG		15.0	
gamma-BHC (Lindane)	2.495	2.825	AVG		15.0	İ
Heptachlor	2.542	2.917	AVG		15.0	
Aldrin	2.351	2.658	AVG		15.0	
Heptachlor epoxide	2.134	2.365	AVG		15.0	
Endosulfan I	1.886	1.963	AVG		15.0	
Dieldrin	2.243	2.438	AVG		15.0	
4,4'-DDE	1.919	1.922	AVG		15.0	1
Endrin	1.972	2.030	AVG		15.0	ĺ
Endosulfan II	1.832	1.892	AVG		15.0	ĺ
4,4'-DDD	1.503	1.543	AVG	2.6	15.0	
Endosulfan sulfate	1.801	1.684	AVG	-6.5	15.0	ĺ
4,4'-DDT	1.717	1.732	AVG	0.9	15.0	
Methoxychlor	0.903	0.864	AVG	-4.3	15.0	í
Endrin ketone	1.951	1.960	AVG	0.5	15.0	i.
Endrin aldehyde	1.334	1.342	AVG	0.6	15.0	
alpha-Chlordane	2.115	2.222	AVG	5.1	15.0	i
gamma-Chlordane	2.117	2.223	AVG	5.0	15.0	; V
	=======	=======	======	======	====	
Tetrachloro-m-xylene	1.075	1.249	AVG	16.2	20.0	
Decachlorobiphenyl	1.920	1.792	AVG	-6.6	20.0	
						ŀ

PESTICIDE CONTINUING CALIBRATION CHECK

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Instrument ID: GCB

Case No.: D1227

SDG No.: D1227

Lab File ID: B0904021

CCV Date/Time:

09/05/99

0506

GC Column: DB5

1725

ICAL Date/Time (1st pt): 08/22/99

ICAL Date/Time (Last pt): 08/22/99

2040

COMPOUND	AVERAGE RF	RF	CURVE	%D	MAX %d	
=======================================	=======	=======	=======	=====	====	1
Toxaphene	0.044	0.039	AVG	-10.4	15.0	
(2)	0.047	0.036	AVG	-24.2	15.0	<-
(3)	0.050	0.043	AVG	-12.5	15.0	
						İ

8D PESTICIDE ANALYTICAL SEQUENCE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1227 SDG No.: D1227

Instrument ID: GCB

	CLIENT SAMPLE NO.	LAB SAMPLE ID	DATE ANALYZED	TIME ANALYZED
	SAMPLE NO.	SWIFTE ID	ANALIZED	ANADIZED
01	PSTD#3 PEST	PSTD#3 PEST	09/04/99	1517
02	PSTD#3 TOX	PSTD#3 TOX	09/04/99	1605
03 04	PWB10820LCS PWB10820LCS	PWB10820LCS PWB10820LCS	09/04/99 09/04/99	1832 1921
05	PWB10820LCS PWB10820	PWB10820LCS	09/04/99	2010
06	ZGPERMEATE	D1227001	09/04/99	2058
07	ROPERMEATE	D1227002	09/04/99	2147
80	PSTD#3 PEST	PSTD#3 PEST	09/05/99	0417
09 10	PSTD#3 TOX	PSTD#3 TOX	09/05/99	0506
11				
12		·		
13				
14 15				<u> </u>
16				
17				
18				
19				
20 21				
22				
23				
24				
25 26				
27			·	
28				
29				
30				
31 32				
33				
34				
35				

CHAIN OF CUSTODY DOCUMENTATION

CH2MHILL Analytical Services
CHAIN OF CUSTODY RECORD
AND AGREEMENT TO PERFORM SERVICES

(LMG 2567 Fairlane Drive Montgomery, AL 36116-1622 (334) 271-1444 FAX (334) 271-3428

[] LRD 5090 Caterpillar Road Redding, CA 96003-1412 (916) 244-5227 FAX (916) 244-4109

LKW Canviro Analytical Laboratories, Inc. 50 Bathurst, Unit 12, Waterloo, Onlario, Canada N2V 2C5 (519) 747-2575 FAX (519) 747-3806

CV0 2300 NW Walnut Boulevard Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

						COC	: <u># 4801827</u>
Project #	Purchase Order #		9	Requested A	nalytical Method #	THIS AREA FOR	LAB USE ONLY
			2	phene		Lab#	Page of
Project Name	-1 1	Ö	0 6	d		D1227	
Mullen Relice Pilot	Study	Å	dane,	Toxa		Lab PM	Custody Review
Company Name) .	10 of				screened
City of McAlles Project Manager or Contact & Phone # Kathy McKinley	J		4/0	रश			BY 8/18/99
Project Manager or Contact & Phone #	Report Copy to:	0 F	()			100 184 199	LIMS Verification
KAYNY MCKINLEY	Kathy Marking	9 c	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	770		My Eliz	
541 / 758 - 0235 # 3/44 Requested Completion Date: Site ID		O N	Endring Methory	1		pH	Custody Seals Y
requested completion Date: Site ib	of M. Mless	Jisposai.	12 E	Methoxy			
ASAP NWTI		Return I N	ļ		servative		lce Y M
Type Matrix		E R S				QC Level 1 2 3	Other
Sampling C G W S A O I R A T I R Date Time R R	CLIENT SAMPLE ID (9 CHARACTERS)	LAB QC				Cooler Temperature	2 ċ
						Alternate Descri	ption Lab ID
8/17/107:30 / 26	7 Permeate	2 2	/				
8/17/29 07:30 W RD	Permeate	2					2
*/////	 			V			
		l	ļ				
		l l	ļ				
		<u> </u>					
		T T					
	-	 					
		 	ļ				
		_					
		 -	l				
Relinquished By . , Empt	y Bottles Date/Ti	lme Receiv	ed By	Empty	Bottles	Date/Time	
logie Villanece		0/12/44 X P			/	8/17/99 07:2	25
Sampled By and Title (Pleas	e sign and print name) Date/Ti	ime Reling	uished By			Date/Time	^
X F - " Kano	N Trevino 07:30	8/17/94 XR	سام س		(Please sign and print name)	8/17/99 07:3 Date/Time ,	9
Received By Villancel Rosi	e sign and print name) Date/TI P VIII/4/2/25 B/ 07:39	17/21 LOD	uished By.	laned Ro	Sic Villar P. FA	8 / 7 / 9 9	
Received By (Pleat	e sign and print name) Date/Ti	ime Shippe	d Vla		Shipping #		
Received By (Please Suttern	8/18/99	2 loco UPS	(Fed-Ex)	Other	- 81290072	5209	
Social Instructions:	, ,						
18				· · · · · · · · · · · · · · · · · · ·			



5090 Caterpillar Road

Redding Ca., 96003

Phone: 530-244-5227

Fax: 530-244-4109

0019

SAMPLE RECEIPT EXCEPTION REPORT

Samp	ole Batch Number: 101227	Client/Project: CITY & McALLEN
-		Comments:
	No custody seal as required by project.	9) COC STATES CLIENT ID IS ZGPERMEATE CONTAINER LABELS SAY ZENOGEM PERMEATE
	Analysis, description, date/time of collection not provided.	
	Samples broken or leaking on receipt.	
	Temperature of samples inappropriate for analysis requested.	
	Container inappropriate for analysis requested.	
	6. Inadequate sample volume.	
	Preservation inappropriate for analysis requested.	
	8. Samples received out of holding time for analysis requested.	
χ	Descrepencies between COC form and container labels.	
	10. Other	
RAC	TION(S) AFFECTED (specify which fi	raction was affected by the exceptions detailed above by writing
4.5	npreserved: Metals:	GC Volatiles: GC/MS Volatiles:
	yanide: Extractables: ctive Actions Taken:	Extractables: Other (specify):
	not required 800 8/19/199	
50,0	Notified:Client Client Services	By: Bluller Date: 8/18/99

Sound Analytical Services, Inc.

ANALYTICAL & ENVIRONMENTAL CHEMISTS

4813 Pacific Hwy East • Tacoma, WA 98424 (253) 922-2310 • FAX (253) 922-5047

e-mail: saincl@uswest.net



TRANSMITTAL MEMORANDUM

DATE: September 13, 1999

TO: Kathy McKinley CH2M Hill 2300 NW Walnut Blvd. Corvallis, OR 97330-3538

PROJECT: McAllen Reuse Pilot Study

REPORT NUMBER: 83466

Enclosed are the test results for two samples received at Sound Analytical Services on August 18, 1999.

The report consists of this transmittal memo, analytical results, quality control reports, a copy of the chain-of-custody, a list of data qualifiers and analytical narrative when applicable, and a copy of any requested raw data.

Should there be any questions regarding this report, please contact me at (253) 922-2310.

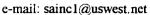
Sincerely,

Katie Downie Project Manager

Sound Analytical Services, Inc.

ANALYTICAL & ENVIRONMENTAL CHEMISTS

4813 Pacific Hwy East • Tacoma, WA 98424 (253) 922-2310 • FAX (253) 922-5047





ANALYTICAL NARRATIVE

Client:

CH2M Hill

Date: September 13, 1999

Project:

McAllen Reuse Pilot Study

Lab No.: 83466

Delivered By: Federal Express

<u>Condition of samples upon receipt</u>: Samples were received in good condition. Chain of custody was in order.

Sample Identification:

Lab. No.	Client ID	Date Sampled	<u>Matrix</u>
83466-1	Zenogem Permeate	08-17-99	Liquid
83466-2	RO Permeate	08-17-99	Liquid

SAMPLE PREPARATION AND ANALYSIS

ORGANOCHLORINE HERBICIDES

Samples 83466-1 and 83466-2 were analyzed for organochlorine herbicides in accordance with EPA SW-846 Method 8151A GC/MS Modified. Samples 83466-1 and 83466-2 were extracted in accordance with EPA SW-846 Method 3510C on 8-24-99 and analyzed on 08-24-99. The samples were extracted and analyzed within the required holding time.

EPA SW-846 Method 8151A has been modified to include the use of a mass spectrometer (MS) for quantitation of the herbicides. The introduction to Method 8151A allows the use of the MS as a qualitative confirmation of detected compounds.

The relative percent difference (RPD) between the percent recoveries of Silvex in the blank spike and blank spike duplicate exceeded the quality control; acceptance limits. No corrective action was taken because there was no remaining sample volume for reextraction. The RPD has been flagged "N".

All other quality control parameters were within the acceptance limits.

No difficulties were encountered during the organochlorine herbicide analyses.

Client Name

CH2M Hill

Client ID:

ZENOGEM PERMEATE

Lab ID:

83466-01

Date Received:

8/18/99

Date Prepared: Date Analyzed:

8/24/99

% Solids

8/24/99

Dilution Factor

10

			Kecove	ery Limits	
Surrogate	% Recovery	Flags	Low	High	
2,4-Dichlorophenylacetic acid	100		48	124	

	Result			
Analyte	(ug/L)	PQL	MDL	Flags
 2,4-D	ND	0.095	0.083	
Silvex (2,4,5-TP)	ND	0.095	0.077	

Client Name

CH2M Hill

Client ID:

RO PERMEATE

Lab ID:

83466-02 8/18/99

Date Received:

Date Prepared: Date Analyzed: 8/24/99

% Solids

8/24/99

Dilution Factor

10

			Recov	ery Limits	
Surrogate	% Recovery	Flags	Low	High	
2,4-Dichlorophenylacetic acid	102		48	124	

		Result			
	Analyte	(ug/L)	PQL	MDL	Flags
_	2,4-D	ND	0.1	0.09	
	Silvex (2,4,5-TP)	ND	0.1	0.083	

Lab ID:

Method Blank - HB876

Date Received:

Date Prepared: Date Analyzed: 8/24/99 8/24/99

% Solids

_

Dilution Factor

10

			Recov	ery Limits
Surrogate	% Recovery	Flags	Low	High
2,4-Dichlorophenylacetic acid	97.6		48	124

	Result			
Analyte	(ug/L)	PQL	MDL	Flags
2,4-D	ND	0.1	0.087	_
Silvex (2,4,5-TP)	ND	0.1	0.081	

Blank Spike/Blank Spike Duplicate Report

 Lab ID:
 HB876

 Date Prepared:
 8/24/99

 Date Analyzed:
 8/24/99

 QC Batch ID:
 HB876

	Blank	Spike	BS		BSD			
	Resuit	Amount	Result	BS	Result	BSD		
Compound Name	(ug/L)	(ug/L)	(ug/L)	% Rec.	(ug/L)	% Rec.	RPD	Flag
Dalapon	0	5	2.91	58.2	3.07	61.4	5.4	_
Dicamba	0	5	3.65	73	4.42	88.4	19	
2,4-D	0	5	5.24	105	4.81	96.2	-8 .7	
Pentachlorophenol	0	5	5.3	106	5.77	115	8.1	
Silvex (2,4,5-TP)	0	5	4.36	87.2	3.2	64	-31	N
Dinoseb	0	5	4.44	88.8	4.11	82.2	-7.7	
MCPA	0	5	5.43	109	4.63	92.6	-16	

Chlorinated Herbicides by USEPA Method 8151A GC/MS Modified

Aquired 6/12/1999 Valid until12/12/99

8151 SURROGATE ACCEPTANCE CRITERIA

	Water	Water	Soil	Soil
	low	high	Low	High
Surrogate	%Rec	%Rec	%Rec	%Rec
2,4,6 - Tribromophenol	48	124	65	131
2,4-Dichlorophenylacetic Acid	48	142	60	142

8151 SPIKE ADVISORY LIMITS FOR %RECOVERY AND RPD

	Water	Water	Water	Soil	Soil	Soil
	low	high	RPD	Low	High	RPD
Compound Name	%Rec	%Rec	%Rec	%Rec	%Rec	%Rec
Dalapon	23	114	27	22	87	22
Dicamba	31	148	45	25	150	24
2,4-D	29	149	24	21	152	28
Pentachiorophenol	56	146	28	31	156	25
Silvex (2,4,5-TP)	42	129	19	54	149	22
Dinoseb	50	155	40	54	148	27
2,4-DB	29	125	25	31	123	32
MCPA	65	127	26	46	154	41

8151 SPIKE ADVISORY LIMITS FOR TCLP % RECOVERY AND RPD

	Leachate	Leachate	Leachate
	Low	high	RPD
Compound Name	%Rec	%Rec	
2,4-D	36	137	36
Silvex (2,4,5-TP)	42	149	36

ANALYTICAL & ENVIRONMENTAL CHEMISTS

4813 PACIFIC HIGHWAY EAST, TACOMA, WASHINGTON 98424 - TELEPHONE: (253) 922-2310 - FAX: (253) 922-5047

DATA QUALIFIERS AND ABBREVIATIONS

- B1: This analyte was detected in the associated method blank. The analyte concentration was determined not to be significantly higher than the associated method blank (less than ten times the concentration reported in the blank).
- B2: This analyte was detected in the associated method blank. The analyte concentration in the sample was determined to be significantly higher than the method blank (greater than ten times the concentration reported in the blank).
- C1: Second column confirmation was performed. The relative percent difference value (RPD) between the results on the two columns was evaluated and determined to be < 40%.
- C2: Second column confirmation was performed. The RPD between the results on the two columns was evaluated and determined to be > 40%. The higher result was reported unless anomalies were noted.
- M: GC/MS confirmation was performed. The result derived from the original analysis was reported.
- D: The reported result for this analyte was calculated based on a secondary dilution factor.
- E: The concentration of this analyte exceeded the instrument calibration range and should be considered an estimated quantity.
- J: The analyte was analyzed for and positively identified, but the associated numerical value is an estimated quantity.
- MCL: Maximum Contaminant Level
- MDL: Method Detection Limit
 - See analytical narrative.
- ND: Not Detected
- PQL: Practical Quantitation Limit
- X1: Contaminant does not appear to be "typical" product. Elution pattern suggests it may be
- X2: Contaminant does not appear to be "typical" product.
- X3: Identification and quantitation of the analyte or surrogate was complicated by matrix interference.
- X4: RPD for duplicates was outside advisory QC limits. The sample was re-analyzed with similar results. The sample matrix may be nonhomogeneous.
- X4a: RPD for duplicates outside advisory QC limits due to analyte concentration near the method practical quantitation limit/detection limit.
- X5: Matrix spike recovery was not determined due to the required dilution.
- X6: Recovery and/or RPD values for matrix spike(/matrix spike duplicate) outside advisory QC limits. Sample was reanalyzed with similar results.
- X7: Recovery and/or RPD values for matrix spike(/matrix spike duplicate) outside advisory QC limits. Matrix interference may be indicated based on acceptable blank spike recovery and/or RPD.
- X7a: Recovery and/or RPD values for this spiked analyte outside advisory QC limits due to high concentration of the analyte in the original sample.
- X8: Surrogate recovery was not determined due to the required dilution.
- 19: Surrogate recovery outside advisory QC limits due to matrix interference.



Sound Analytical Services, Inc. ANALYTICAL & ENVIRONMENTAL CHEMISTS

4813 Pacific Hwy East • Tacoma, WA 98424 (253) 922-2310 • FAX (253) 922-5047

e-mail: saincl@uswest.net

SAS Lab No. 83466

TURNAROUND REQUEST (business days)
Standard (10 days)

RUSH: 24 hrs ___ 48 hrs ___ 5 day ___

	CHAIN OF	CUST	DDY/RI						TO	<u>RY /</u>	ANA	LYS	SIS		t	<u>}</u>	
Client: City of	McAllen				Analyse	es Req	ueste	d									
Project Name:					P. X												
McAllen Reuse	Pilot Stu	du			2,4,5.TP	Silvex					ļ						
Phone No.: 541/758-0235 ant. 3144					3.0	يئر						İ					
Phone No.: 541/7	58-0235	mt. 31	44	ers	2						}						
Fax No.: 541 /766	- 2852	<u> </u>		Containers		2											
Email: Kmckin!	le D ch 21	n . C DA	<u> </u>	Co	9	4- D 5-TP											
Use Sample ID		Time	Matrix	# of	-h¹2	2,4,5					} 				;		
LAURA		├ ──			114	* 2	 					 					
2 Zenogem Per	meate 8/17/99	07:33	Liguid	1_	V		 				<u> </u>	 -					
2 RO Perme	ite 8/17/49	07:30	Lignid	1		<i>'</i>	├					ļ			<u>.</u> .		
						,	ļ					<u> </u>					·- <u>-</u>
							<u> </u>										
Ę.	1		<u> </u>			,											
						Ŧ									e.		,
3	g .	1											-				
														_			
					1												
		 															
												 		 			. ,
		 			<u> </u>					_		\top					
		<u> </u>					_	 		t	†	†	 	-			
		<u> </u>				<u> </u>						_					
			l				1					<u></u>	L				
Sign	ature	Printed N	lame	F	irm	Time	e/Date	3 8	necia	l Ins	tructi	ons					

	Signature	Printed Name	Firm	Time/Date	Special Instructions	
Relinquished By:	R - 1 .	Ramin	City of Mc Allen	09:40 8/17/19		
Received By	Rece Villand	Rosie Villarrsal	MCAlleN	8/17/19 08:40		
Relinquished By:	Rosie Villand	Rosie VillARREAL	Millen	1/17/19		
	MHodonan	MHodoman	SAS	9:00 8/18/0	9	
Relinquished		0'			,	
ceived By						

COC No.	



ENERGY LABORATORIES, INC.

SHIPPING: 2393 SALT CREEK HIGHWAY • CASPER, WY 82601

MAILING: P.O. BOX 3258 • CASPER, WY 82602

E-mail: energy@trib.com • FAX: (307) 234-1639 • PHONE: (307) 235-0515 • TOLL FREE: (888) 235-0515

CASE NARRATIVE

DATE:

September 21, 1999

TO:

Kathy McKinley

FROM:

Sheryl Garling

RE:

CH2MHill Water Samples

SAMPLE NUMBERS: 32370 001 through 002

Samples Zenogem Permeate and RO Permeate were received on August 18, 1999. Samples were shipped using Energy Laboratories, Inc. contract service with UPS. The overnight option was used for shipping the samples to the laboratory. Samples were in good condition and properly preserved.

No analytical problems were indicated for this sample delivery group.

The methods used are methods published by US EPA for drinking water analyses. The methods used are as follows:

Radium 226 - EPA Method 903.0 (alpha emitting),

Radium 228 - EPA Method 904.0, and

Gross Alpha -EPA Method 900.1 (gross alpha minus uranium and

radon).

The standard detection limits for these methods are 0.2 pCi/L, 1.0 pCi/L, and 1.0 pCi/L, respectively. The initial e-mail response incorrectly identified methods and detection limits.

If additional information is required, please advise.



ENERGY LABORATORIES, INC.

SHIPPING: 2393 SALT CREEK HIGHWAY • CASPER, WY 82601

MAILING: P.O. BOX 3258 • CASPER, WY 82602

E-mail: energy@trib.com • FAX: (307) 234-1639 • PHONE: (307) 235-0515 • TOLL FREE: (888) 235-0515

LABORATORY ANALYSIS REPORT - CH₂M HILL

Project:
Sample ID:
Laboratory ID:
Sample Matrix:
Sample Date/Time:
Date Received:
Report Date:

McAllen Reuse	Pilot Study	
Zenogem Permeate	RO Permeate	
32370-001	32370-002	
Wat	ег	
08-17-99 (@ 07:30	
08-18	-99	
September	12, 1999	

			Reporting				
Radiometric		Method	Limit	Units	Results		
	²²⁶ Ra						
Radium-226	Ka	903.0	0.2	pCi/L	< 0.2	< 0.2	
Radium Precision ±					-	<u> </u>	
Radium-228	²²⁸ Ra	904.0	1.0	pCi/L	<1.0	<1.0	
Radium Precision ±					-	-	
Gross Alpha	Gross α	900.1	1.0	pCi/L	< 1.0	< 1.0	
G. Alpha Precision ±					-		



RADIOCHEMICAL QUALITY ASSURANCE REPORT - CH2M HILL

Laboratory ID Range:
Sample Matrix:
Sample Date / Time:
Date Received:
Report Date:

32370-001-002 Water 08-17-99 @ 07:30 08-18-99 September 12, 1999

	<u>Method</u>	Relative Percent <u>Difference¹</u>	Spike Recovery (Percent) ²	LCS Recovery (Percent)	Method Blank (pCi/L) ³	Date Analyzed	Analyst
Laboratory #:		56010-001	90156-001		GA-18633		
Gross Alpha:	900.1	0.0	92	98	<1.0	08-24-99	RS
Laboratory #:		32627-001	32428-003		RA-186		
Radium-226:	903.0	0.8	98	104	< 0.2	09-07-99	RS
Laboratory #:		32443-001	32443-002		228-212		
.dium-228:	904.0	0.0	117	119	< 1.0	09-10-99	LMH

(3) Uranium is reported in mg/L.

eport Approved By:

Reviewed By: Lalle

lmh r:\Reports\Clients.99\CH2M_Hill\Water\rc32370-001.xls

Log In No. 32370

Log In. No.

⁽¹⁾ These values are an assessment of analytical precision. The acceptance range is 0-20% for sample results above 10 times the reporting limit. This range is not applicable to samples with results below 10 times the reporting limit.

⁽²⁾ These values are an assessment of analytical accuracy. They are a percent recovery of the spike addition. ELI performs a matrix spike on 10 percent of all samples for each analytical method.

ENERGY LABORATORIES, INC CHAIN OF CUSTODY RECORD

toll free 1 235-0515

BillingsCasperGillette • Rapid City

Mail Only: UPS/FedEx Deliveries: 2393 Salt Creek Highway •

PO Box 3258 • Casper, WY

82602-3258 Casper, WY • 82601 voice 307-235-0515 fax 307-234-1639

For Sa	mple Tra	ıckin	g Pur	poses, Please Provide Contact Name and Telephone	#'s as Indicate	d (S	EE BAC	CK OF	FORM .	FOR EX	(AMPL)	ES AND INSTRUCTIONS)
Project	Name /	Loc	catior	n / Purchase Order # / Bid #								Special Requests
MLAlle	n Reus	e Pi	lit	McAllen, / NU. P.U.#	000		Type o	of Analy	ses Rec	luested		Stud TAT
					ers U (رفو						
Name	/ Phone	:# /	Fay	(#	ain V	22	28					
Kathy CH2M	McKinl 1 Hill	24	/5	x# -41-758-0235#3144/541-766-2852	Cont W S Vegerati	adium	101					
Date	Time	composite	sample	Send Invoice to: Kathy McKinby CHZM Hill Applied Sciences Group (call Dabine phone number) Send Report to: Same as abone	Number of containers Sample Type: A (W) S V U O Air Water Solis/solids <u>Veg</u> etation <u>U</u> rine <u>O</u> the	n 226, Radium 228,	26, Radium					
		сош	grab	Send Report to: Same as above Sample I.D.	Sar Sar Air <u>W</u> ater	Radium Gross A	Radium 2 Gross F					Comments, Special Instructions, etc.
8 17/99	07:30		/	ZenoGem Permeate	1	Х						
8/17/24	07:30		/	RO Permeate	1	<u> </u>	X					
				ARS-AT								
	1							!				
								-				
		\Box										

1	1. Sampler: (signature)	Date	Time	Received by: (signature)	2. Relinquished by: (signature)	Date	Time	Received by: (signature)
	R-2.	8/17/99	07.30	Rosie Villaneal	Recie Villaned	8/17/99		
1	3. Relinquished by: (signature)	Date	Time	Received by: (signature)	4. Relinquished by: (signature)	Date	Time	Received at Laboratory by:
						8-18-99	10:15	Kris Port
L	<u> </u>			<u> </u>				

Scope of Work/Instructions

CH2M HILL Point of Contact for Final report/Invoicing

CH2M HILL Kathy McKinley 2300 NW Walnut Blvd. Corvallis, OR 97330

Phone: 541/758-0235 ext. 3144

FAX: 541/766-2852

Analytical Methods/Prices:

Radium 226 by EPA 903.0 for \$40 per sample Radium 228 by EPA 904.0 for \$50 per sample Gross Alpha by EPA 903.0 for \$35 per sample

Sample Delivery: \$25

Return Cooler/Samples: \$6.40

The laboratory shall clearly and completely document and justify the preparation and analysis procedures when modifications to the methods have been made/requested.

Holding Times: Samples must be analyzed within EPA holding for each analytical method specified. CH2M HILL will deliver samples to the laboratory in a timely manner to facilitate the meeting of holding times.

Quality Assurance/Quality Control Requirements: QA/QC procedures will follow the protocols set forth in the EPA methods.

Data Package: A final data package must be submitted to CH2M HILL. The package will include: a lab narrative and data summary.

The laboratory narrative will include:

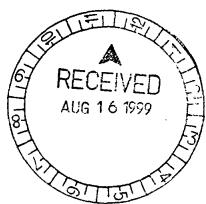
A description of any deviation from the prescribed methodologies or protocols as discussed in this SOW.

Summarization of quality control information exceeding the laboratory's acceptance criteria, a discussion of possible reasons for these discrepancies, and a description of corrective action taken.

All blank values exceeding three times the average method blank will be addressed.

A synopsis of all holding times achieved.

A discussion of any other analytical problems that may have been encountered.



Turnaround Time: Standard (3 weeks)



CH2M HILL

Applied Sciences Group

2300 NW Walnut Bivd

Corvallis, OR

97330-3538

P.O. Box 428

Corvallis, OR

97339-0428

Tel 541.752.4271

Fax 541.752.0276

October 26, 1999

McAllen WWTP #2, City of

149462.A1.ZG

RE:

Analytical Data for McAllen WWTP #2, City of Applied Sciences Group Reference No. 3089

Angie Fernandez/PHX:

On September 15, 1999, CH2M HII request for analysis of selected para

The analytical results and associate difficulties encountered during the narrative.

Under CH2M HILL policy, your shave not given us prior instruction disposal as hazardous waste.

CH2M HILL Applied Sciences (serving your analytical needs agif you need additional information extension 3120.

Sincerely,

Kelly Ensor

Senior Administrative Assistant

Enclosures

Group received four samples with a tached.

ısual

: case

ting. If you nples require

rward to ning the data, or 758-0235,

5
Ò
9,
ا
0

E	VERC	oY ES	•	Billings Casper Gillette Rapid City	UP:		Only:	RATORIES, INC PO Box 3258 • 2393 Salt Cree	Casper, V	VY •		602-325	8	01		toll free voice fax	1 235-0515 307-235-0515 307-234-1639
For Sa	mple Tra	cking	g Pur	rposes, Ple	ease Pr	ovide Cor	ıtact Nan	ie and Telephone #	r's as Indicate	d (S	SEE BA	CK OF	FORM F	OR EXA	MPLE	ES AND IN	STRUCTIONS)
				n / Purc					e							Spec	al Requests
MUAILE	n Keus	ι ρ,	lot	/ McAlle	m, /	NO. P.O	.#		Ogh		Type	of Analy	yses Requ	ested		Stud	TAT
	fuely / Phone	# /	Fax	/ Tx .					ners ' U Urin	25	1~2		<u> </u>				
Kathy CH2 M	McKinl	ley	/ 5	41-758				-766-2852	contai (W) S V egeration	ndium 2	Lm 228,						
Date	Time	composite	sample	Send Inv	oice to Hill I	Kathy Applied &	McKin Sciences phore n	by Group umber)	Number of containers Sample Type: A (W) S V U O ir Water Solls/solids Vegetation Urine Other	m 226, Radium 228 Alpha	1~3						
		шоэ	grab	Send Rep	port to:		as a	umber) bre	I Sa <u>A</u> ir <u>W</u> ater	Radium Gross A	Radium 2 Gross F						ents, Special actions, etc.
8/17/99	07:30		/	Zeno	Gen	n Per	meat	e		X							
8/17/94	07:30		/	1		mean			1		X						
						AT											
				7271							1						
				 						 	 -		1				
				 						-	 	 					
				 						ļ	} -	ļ					
L				ļ							<u> </u>	 					
					<u>-</u> -			·									
1 Came	oler: (signa	tura))ate	Time	Do	eeived by: (signature)	2 Police	unishad	by: (sigr	iatura)	Date	Tin	ne	Decaivad	by: (signature)
i. samp	nei: (signa	(are)					1			1			1		ne	Received	oy. (signature)
K-	1_	<u>=:</u>		18/1	7/99	07.30	Kopie	Villaneal	Ricce	.V.M	aned	· 	8/17/9	9			
3. Relin	quished by	: (sig	nature	e) I	Date	Time	Rec	eived by: (signature)	4. Reli	nquished	by: (sig	nature)	Date	Tin	ne	Received at	Laboratory by:

	Name / Thunde	Loc rbasi :#/	ation in Fax		Casper, W k Highway	'Y • • C	826 asper, V EE BAC	02-3258 VY •	826 ORM F	OR EXA	MPLES	voice 307-235-0515 fax 307-234-1639 SAND INSTRUCTIONS) Special Requests Please fax results
Date Time Send Invoice to: Jeff Jones PO Box Nowhere Hope, WY 80000 Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D.			Number of containers Sample Type: A W S V U O Air <u>W</u> aer Solis/solids <u>Vege</u> tation <u>U</u> rine <u>O</u> the	Asbestos - TEM	IOC's - RADs	NO ₂ , NO ₃ , F	VOCs - 502.2	50Cs - 504,505,50	50Cs - 515, 531.1	as soon as possible Thank you. Comments, Special Instructions, etc.		
1995		_	_	Jampa 1.5.				ļ				
5/28	11:35	-	x	Entry to Distribution	4	х	-	-	×	-		Phase II SDWA Primary
5/28	11:45		x	Distribution Tap	9		х	х		X	х	4

1.Sampler: (signature) Jeff Jones	Date 5-28-95	Time 1 2:05 p	Received by: (signature) Harry Truckers	2.Relinquished by: (signature) Harry Truckers	Date 5-28-95	Time 13:15 p	Received by: (signature) Sheryl A. Garling
3. Relinquished by: (signature) N/A	Date	Time	Received by: (signature)	4. Relinquished by: (signature)	Date	Time	Received at Laboratory by:
	N/A	N/A	N/A	Sheryl A. Garling	5-28-95	14:00y	Roger A. Garling

Instructions:

- (1)
- A completed Chain-of-Custody must be submitted with all samples Special Requests area can include (but not limited to) the following: (2)
 - Turnaround status, Rush status, Due Date, etc.
 - Special mailing instructions:
 - send copy of Report and/or Invoice to a second party
 - send copy of Report to a Government Agencies (EPA, etc.)
- Public Water System (PWS) Number
- Do you want samples returned to you or disposed of?

Scope of Work/Instructions

CH2M HILL Point of Contact for Final report/Invoicing

CH2M HILL Kathy McKinley 2300 NW Walnut Blvd. Corvallis, OR 97330

Phone: 541/758-0235 ext. 3144

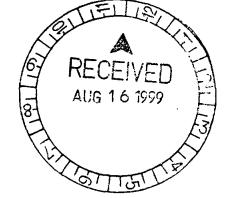
FAX: 541/766-2852

Analytical Methods/Prices:

Radium 226 by EPA 903.0 for \$40 per sample Radium 228 by EPA 904.0 for \$50 per sample Gross Alpha by EPA 903.0 for \$35 per sample

Sample Delivery: \$25

Return Cooler/Samples: \$6.40



The laboratory shall clearly and completely document and justify the preparation and analysis procedures when modifications to the methods have been made/requested.

Holding Times: Samples must be analyzed within EPA holding for each analytical method specified. CH2M HILL will deliver samples to the laboratory in a timely manner to facilitate the meeting of holding times.

Quality Assurance/Quality Control Requirements: QA/QC procedures will follow the protocols set forth in the EPA methods.

Data Package: A final data package must be submitted to CH2M HILL. The package will include: a lab narrative and data summary.

The laboratory narrative will include:

A description of any deviation from the prescribed methodologies or protocols as discussed in this SOW.

Summarization of quality control information exceeding the laboratory's acceptance criteria, a discussion of possible reasons for these discrepancies, and a description of corrective action taken.

All blank values exceeding three times the average method blank will be addressed.

A synopsis of all holding times achieved.

A discussion of any other analytical problems that may have been encountered.

Turnaround Time: Standard (3 weeks)



October 26, 1999

McAllen WWTP #2, City of

149462.A1.ZG

RE:

Analytical Data for McAllen WWTP #2, City of Applied Sciences Group Reference No. 3089

Angie Fernandez/PHX:

On September 15, 1999, CH2M HII request for analysis of selected para

The analytical results and associate difficulties encountered during the narrative.

Under CH2M HILL policy, your have not given us prior instruction disposal as hazardous waste.

CH2M HILL Applied Sciences (serving your analytical needs ag: if you need additional information extension 3120.

Sincerely,

Kelly Ensor

Senior Administrative Assistant

Enclosures

as Group received four samples with a *tached.

> ısual : case

CH2M HILL

Fax 541.752.0276

Applied Sciences Group 2300 NW Walnut Blvd Corvallis, OR 97330-3538 P.O. Box 428 Corvattis, OR 97339-0428 Tel 541.752.4271

ting. If you nples require

rward to ning the data, or 758-0235,

CLIENT SAMPLE CROSS-REFERENCE

CH2M HILL Applied Sciences Group Reference No. 3089

• • • • • • • • • • • • • • • • • • • •		Date	Time
Sample ID	Client Sample ID	Collected	Collected
308901	ZGP	09/14/1999	08:50
308902	ROP	09/14/1999	08:50
308903	WWTP#2Effluent	09/14/1999	08:50
308904	ROC	09/14/1999	08:50

CASE NARRATIVE VOLATILES

Lab Reference No.: 3089

Client/Project: McAllen WWTP #2, City of

I. Holding Times:

All acceptance criteria were met.

- II. Analysis:
 - A. <u>Calibration</u>:
 All acceptance criteria were met.
 - B. <u>Blanks</u>: All acceptance criteria were met.
 - C. <u>Duplicate Sample(s)</u>:
 All acceptance criteria were met.
 - D. <u>Spike Sample(s)</u>:
 All acceptance criteria were met.
 - E. <u>Surrogate Recoveries</u>:
 All acceptance criteria were met.
 - F. <u>Lab Control Sample(s)</u>: All acceptance criteria were met.
 - G. Other:
- III. <u>Documentation Exceptions</u>:

None

IV. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or designee, as verified by the following signature.

Jank A Handy

Prepared by:

Reviewed by:

CASE NARRATIVE GENERAL CHEMISTRY

Lab Reference No.: 3089

Client/Project: McAllen WWTP #2, City of

I. <u>Holding Time</u>:

All acceptance criteria were met.

II. <u>Digestion Exceptions</u>:

None

III. Analysis:

A. <u>Calibration</u>:

All acceptance criteria were met.

B. Blanks:

All acceptance criteria were met.

C. <u>Matrix Spike Sample(s)</u>:

All acceptance criteria were met.

D. <u>Duplicate Sample(s)</u>:

All acceptance criteria were met.

E. <u>Lab Control Sample(s)</u>:

All acceptance criteria were met.

F. Other:

Not applicable.

IV. Documentation Exceptions:

None.

V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by:

Reviewed by:

CASE NARRATIVE METALS

Lab Reference No.: 3089



I. <u>Holding Time</u>:

All acceptance criteria were met.

II. <u>Digestion Exceptions</u>:

None.

- III. Analysis:
 - A. <u>Calibration</u>:
 All acceptance criteria were met.
 - B. <u>Blanks:</u> All acceptance criteria were met.
 - C. <u>ICP Interference Check Sample</u>: All acceptance criteria were met.
 - D. <u>Spike Sample(s)</u>: All acceptance criteria were met.
 - E. <u>Duplicate Sample(s)</u>:
 All acceptance criteria were met.
 - F. <u>Laboratory Control Sample(s)</u>: All acceptance criteria were met.
 - G. <u>ICP Serial Dilution</u>: Not Required.
 - H. Other:
- IV. <u>Documentation Exceptions</u>: None
- V. I certify that this data package is in compliance with the terms and conditions agreed to by the client and CH2M HILL, both technically and for completeness, except for the conditions detailed above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or his designee, as verified by the following signature.

Prepared by:	Aud 1 De Com	
Reviewed by:	'cally	



CH2M HILL

Applied Sciences Group

2300 NW Walnut Blvd

Corvallis, OR

97330-3538

P.O. Box 428

Corvallis, OR

97339-0428

Tel 541.752.4271

Fox 541.752.0276

October 4, 1999

McAllen WWTP #2, City of

149462.A1.ZG

RE:

Analytical Data for McAllen WWTP #2, City of

Applied Sciences Group Reference No. 3089 & 3113

Angie Fernandez/PHX:

On September 15, 1999, CH2M HILL Applied Sciences Group received four samples with a request for analysis of selected parameters. From two of these samples, CH2M HILL Applied Sciences Group generated two samples with a request for analysis of selected parameters.

The analytical results and associated quality control data are enclosed. Any unusual difficulties encountered during the analysis of your samples are discussed in the case narrative.

Under CH2M HILL policy, your samples will be stored for 30 days after reporting. If you have not given us prior instructions for disposal, we will contact you if any samples require disposal as hazardous waste.

CH2M HILL Applied Sciences Group appreciates your business and looks forward to serving your analytical needs again. If you should have any questions concerning the data, or if you need additional information, please call Ms. Kathy McKinley at (541) 758-0235, extension 3120.

Sincerely,

Kelly Ensor

Senior Administrative Assistant

Enclosures

CLIENT SAMPLE CROSS-REFERENCE

CH2M HILL Applied Sciences Group Reference No. 3089 & 3113

		Date	Time	
Sample ID	Client Sample ID	Collected	Collected	
308901	ZGP	9/14/99	8:50	
308902	ROP	9/14/99	8:50	
308903	WWTP#2Effluent	9/14/99	8:50	
308904	ROC	9/14/99	8:50	
311301	ZGP-3D	9/20/99		
311302	ROP-3D	9/20/99		

- - - -

CASE NARRATIVE DBPs/ORGANICS

Lab Reference No.: 3089 & 3113

Client	Project	: McAllen WWTP #2, City of
I.		g Times: eptance criteria were met.
II.	Analys	<u>is</u> :
	A.	Calibration: All acceptance criteria were met.
	B.	Blanks: All acceptance criteria were met.
	C.	Duplicate Sample(s): All acceptance criteria were met.
	D.	Spike Sample(s): All acceptance criteria were met.
	E.	Surrogate Recoveries: All acceptance criteria were met.
	F.	Lab Control Sample(s): All acceptance criteria were met.
	G.	Other: None
III.	Docum None	nentation Exceptions:
cli ab	ent and ove. Re	at this data package is in compliance with the terms and conditions agreed to by the CH2M HILL, both technically and for completeness, except for the conditions detailed lease of the data contained in this hardcopy data package has been authorized by the Manager or designee, as verified by the following signature.
Prenar	ed hv	

Reviewed by:

	Formation Potential Test Conditions													
		FP	Free	Free	Total	FP	Measured	FP	FP	FP	FP			
Client ID	Lab ID	Dose	Residual	Demand	Residual	Temp.	pН	Start	Take-Off	Time H:M	Time (Hour)			
ZGP	308901	10.00	0.21	9.79		23	7.9	9/17/99 12:05	9/20/99 13:17	73:12	73.20			
ROP	308902	1.60	0.71	0.89		23	7.7	9/17/99 12:12	9/20/99 13:21	73:09	73.15			

			Formation Pot	ential Trihalon	nethanes (TH!	Ms) Disinfection	By-Products,	, (ug/L)		
Client ID	Lab ID	FP CHCl3	FP BDCM	FP DBCM	FP CHBr3	FP TTHM			:	
ZGP-3D	311301	105	77.6	51.5	9.5	244				
ROP-3D	311302	2.9	2.9	2.5	</td <td>8.3</td> <td>ļ</td> <td></td> <td> </td> <td></td>	8.3	ļ		 	
<u></u>		CHCl3 = Chlor	oform			EPA TTHM Su	ige I MCL =	80 ug/L	 	
		BDCM = Brom	odichlorometha	ne		EPA TTHM Sta	ige 2 MCL =	40 ug/L		
		DBCM = Dibro	mochlorometha	ne						
		CHBr3 = Brom	ofor m							

			Formation Pol	tential Haloac	etic Acids (HAA:	s) Disinfection	By-Products (ıg/L)			
		FP	FP	FP	FP	FP	FP	FP	FP		
Client ID	Lab ID	MCAA *	MBAA *	DCAA *	TCAA *	BCAA	DBAA *	HAA5	HAA6		
CGP-3D	311301	7.5	3.2	39.8	31.3	22.8	8.8	90.6	113		
ROP-3D	311302	<2	<l< td=""><td>1.1</td><td><1</td><td><1</td><td><1</td><td>1.1</td><td>1.1</td><td></td><td></td></l<>	1.1	<1	<1	<1	1.1	1.1		
		MCAA = Mono	chloroacetic acid	1	BCAA = Bromo	chloroacetic ac	 cid	EPA HAA5 Stage 1	MCL = 60 ug/L		
		MBAA = Mono	bromoacetic acid	1	DBAA = Dibroi	moacetic acid		EPA HAA5 Stage 2		1	
		DCAA = Dichle	oroacetic acid		* These compou	ınds make up th	e HAA5			1	
		TCAA = Trichl	oroacetic acid								7

212 Set FOC

Client Information

ormation Lab Information

Client Sample ID: ROC

Lab Sample ID: 308904

Project Name: McAllen WWTP #2, City of

Date Received: 09/15/1999

Project Manager: Angie Fernandez/PHX

Report Revision No.: 0

Sampled By: R. Villareal Sampling Date: 09/14/1999

Analyzed By: MG/MAS/DHK

Sampling Time: 8:50

Reviewed By: -----

Type: Grab Matrix: Water Basis: As Received

		Sample			Analysis	Date
Analyte	MRL.	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
N-Nitrate/Nitrite	0.20	24.4		mg/L	EPA 353.2	09/20/99
N-Total Kjeldahl	2.0	3.6		mg/L	EPA 351.4	09/21/99
Total Dissolved Solids	10	4,330		mg/L	EPA 160.1	09/20/99
TOC	5.0	22.6		mg/L	EPA 415.1/2	09/21/99
Total Phosphate-P	1.0	10.5		mg/L	EPA 365.2/4	09/21/99

Client Information

Client Sample ID: WWTP#2Effluent

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Sampled By: R. Villareal Sampling Date: 09/14/1999 Sampling Time: 8:50

Type: Grab Matrix: Water Basis: As Received Lab Information

Lab Sample ID: 308903

Date Received: 09/15/1999

Report Revision No.: 0

Analyzed By: MG/MAS/DHK

Reviewed By: ------

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
General Chemistry						
N-Nitrate/Nitrite	0.04	3.94		mg/L	EPA 353.2	09/20/99
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	09/21/99
Total Dissolved Solids	10	1,060		mg/L	EPA 160.1	09/20/99
TOC	0.50	6.10		mg/L	EPA 415.1/2	09/20/99
Total Phosphate-P	0.10	1.78		mg/L	EPA 365.2/4	09/21/99

End Six IPR

Client Information

Client Sample ID: ZGP

Project Name: McAllen WWTP #2, City of

Project Manager: Angie Fernandez/PHX
Sampled By: R. Villareal

Sampling Date: 09/14/1999
Sampling Time: 8:50
Type: Grab

Matrix: Water
Basis: As Received

Lab Information

Lab Sample ID: 308901

Date Received: 09/15/1999

Report Revision No.: 0

Analyzed By: MG/MAS/JJB/DHK

Reviewed By: m 53 - 54

Analyte	MRL	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
General Chemistry						
Alkalinity (as CaCO3)	2.0	153		mg/L	EPA 310.2	09/24/99
Bromide	0.020	0.322		mg/L	EPA 300.0-B	09/20/99
Chloride	2.0	281		mg/L	EPA 300.0-A	09/22/99
Color (APHA) Apparent		17		color units	EPA 110.2	09/15/99
Fluoride	0.10	1.14		mg/L	EPA 300.0-A	09/22/99
N-Ammonia	0.10	0.10	U	mg/L	EPA 350.3	09/23/99
N-Nitrate/Nitrite	0.04	7.90		mg/L	EPA 353.2	09/20/99
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	09/21/99
Silica-React.	0.4	16.1		mg/L	SM4500-Si D	09/23/99
Sulfate	2.0	247		mg/L	EPA 300.0-A	09/22/99
Total Dissolved Solids	10	1,950		mg/L	EPA 160.1	09/20/99
TOC	0.50	5.90		mg/L	EPA 415.1/2	09/20/99
Total Phosphate-P	0.10	2.89		mg/L	EPA 365.2/4	09/21/99
UV-254	0.009	0.126		asb/cm	SM5910	09/15/99

Client Information Lab Information

Client Sample ID: ZGP Lab Sample ID: 308901

Project Name: McAllen WWTP #2, City of Project Manager: Angie Fernandez/PHX

Basis: As Received

Sampled By: R. Villareal
Sampling Date: 09/14/99
Sampling Time: 08:50
Type: Grab
Matrix: Water

Report Revision No.: 0
Reported By: JG
Reviewed By:

Date Received: 09/15/1999

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
Aluminum, Al	100	100	U	μg/L	SW6010B	10/14/99
Arsenic, As	10.0	10.0	U	μg/L	SW6010B	10/14/99
Barium, Ba	25.0	61.6		μg/L	SW6010B	10/14/99
Cadmium, Cd	5.0	5.0	U	μg/L	SW6010B	10/14/99
Calcium, Ca	500	86900		μg/L	SW6010B	10/14/99
Chromium, Cr	10.0	10.0	U	μg/L	SW6010B	10/14/99
Iron, Fe	100	: 100	U	μg/L	SW6010B	10/14/99
Lead, Pb	3.0	3.0	U	μg/L	SW6010B	10/14/99
Magnesium, Mg	500	25600		μg/L	SW6010B	10/14/99
Manganese, Mn	10.0	17.0		μg/L	SW6010B	10/14/99
Mercury, Hg	0.3	0.3	U	μg/L	SW7470A	09/28/99
Potassium, K	2000	29900		μg/L	SW6010B	10/14/99
Selenium, Se	7.0	7.0	U	μg/L	SW6010B	10/14/99
Silver, Ag	10.0	10.0	U	μg/L	SW6010B	10/14/99
Sodium, Na	1000	253000		μg/L	SW6010B	10/14/99
Strontium, Sr	100	2000		μg/L	SW6010B	10/14/99
Zinc, Zn	20.0	54.4		μg/L	SW6010B	10/14/99

Client Information

Client Sample ID: ZGP

Project Name: McAllen WWTP #2, City of Project Manager: Angle Fernandez/PHX

Sampled By: R. Villareal Date Collected: 9/14/99 Time Collected: 8:50 Type: Grab

> Matrix: Water Basis: As Received

Lab Information

Lab Sample ID: 308901

Analysis Method: SW 8260B

Units: µg/L eceived: 9/15/9

Date Received: 9/15/99 Date Analyzed: 9/27/99

Dilution Factor: 1
Report Revision No.: 0
Reported By: MCB
Reviewed By:

Analista	CAC#	Reporting	Sample	
Analyte	CAS#	Limit	Result	Qualifier
Purgeable Volatiles				
Vinyl Chloride	75-01-4	1.0	1.0	U
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	บ
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	U
1,1,1-Trichloroethane	71-55-6	1.0	1.0	U
Carbon Tetrachloride	56-23-5	1.0	1.0	U
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	1.0	U
Dibromofluoromethane	1868-53-7		103%	SS
1,2-Dichloroethane-d4	17068-07-0		94%	SS
Toluene-d8	2037-26-5		115%	SS
p-Bromofluorobenzene	460-00-4		95%	SS

E=Estimated value above instrument calibration range

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

SS=Surrogate standard

Client Information

Lab Information

Client Sample ID: ROP

Lab Sample ID: 308902

Project Name: McAllen WWTP #2, City of

Date Received: 09/15/1999

Project Manager: Angie Fernandez/PHX

Report Revision No.: 0

Sampled By: R. Villareal Sampling Date: 09/14/1999 Analyzed By: MG/MAS/JJB/DHK

Sampling Time: 8:50

Reviewed By:

Type: Grab

Matrix: Water Basis: As Received

Analyte	MRL	Sample Result	Qualifier	Units	Analysis Method	Date Analyzed
General Chemistry						
Alkalinity (as CaCO3)	2.0	16		mg/L	EPA 310.2	09/24/99
Bromide	0.020	0.020	U	mg/L	EPA 300.0-B	09/20/99
Chloride	0.10	15.2		mg/L	EPA 300.0-A	09/22/99
Color (APHA) Apparent		5		color units	EPA 110.2	09/15/99
Fluoride	0.10	0.45		mg/L	EPA 300.0-A	09/22/99
N-Ammonia	0.10	0.10	U	mg/L	EPA 350.3	09/23/99
N-Nitrate/Nitrite	0.01	1.08		mg/L	EPA 353.2	09/20/99
N-Total Kjeldahl	2.0	2.0	U	mg/L	EPA 351.4	09/21/99
Silica-React.	0.4	0.9		mg/L	SM4500-Si D	09/23/99
Sulfate	0.10	5.31		mg/L	EPA 300.0-A	09/22/99
Total Dissolved Solids	10	72		mg/L	EPA 160.1	09/20/99
TOC	0.50	0.52		mg/L	EPA 415.1/2	09/20/99
Total Phosphate-P	0.10	0.10	U	mg/L	EPA 365.2/4	09/21/99

Client Information Lab Information

Client Sample ID: ROP Lab Sample ID: 308902

Project Name: McAllen WWTP #2, City of Date Received: 09/15/1999

Project Manager: Angie Fernandez/PHX
Sampled By: R. Villareal
Sampling Date: 09/14/99
Sampling Time: 08:50
Type: Grab

Report Revision No.: 0
Reported By: JG
Reviewed By: JG
Reviewed By: JG
Reviewed By: JG

Matrix: Water Basis: As Received

		Sample			Analysis	Date
Analyte	MRL	Result	Qualifier	Units	Method	Analyzed
					011100100	
Aluminum, Al	100	100	U	μg/L	SW6010B	10/14/99
Arsenic, As	10.0	10.0	U	μg/L	SW6010B	10/14/99
Barium, Ba	25.0	25.0	U	μg/L	SW6010B	10/14/99
Cadmium, Cd	5.0	5.0	U	μg/L	SW6010B	10/14/99
Calcium, Ca	500	833		μg/L	SW6010B	10/14/99
Chromium, Cr	10.0	10.0	U	μg/L	SW6010B	10/14/99
Iron, Fe	100	100	U	μg/L	SW6010B	10/14/99
Lead, Pb	3.0	3.0	U	μg/L	SW6010B	10/14/99
Magnesium, Mg	500	500	U	μg/L	SW6010B	10/14/99
Manganese, Mn	10.0	10.0	U	μg/L	SW6010B	10/14/99
Mercury, Hg	0.3	0.3	U	μg/L	SW7470A	09/28/99
Potassium, K	2000	2000	U	μg/L	SW6010B	10/14/99
Selenium, Se	7.0	7.0	U	μg/L	SW6010B	10/14/99
Silver, Ag	10.0	10.0	U	μg/L	SW6010B	10/14/99
Sodium, Na	1000	16200		μg/L	SW6010B	10/14/99
Strontium, Sr	100	100	U	μg/L	SW6010B	10/14/99
Zinc, Zn	20.0	20.0	U	μg/L	SW6010B	10/14/99

Client Information

Client Sample ID: ROP Lab Sample ID: 308902

Project Name: McAllen WWTP #2, City of Analysis Method: SW 8260B

Project Manager: Angie Fernandez/PHX

Sampled By: R. Villareal

Date Received: 9/15/99

Date Collected: 9/14/99

Time Collected: 8:50

Dilution Factor: 1

Type: Grab Report Revision No.: 0

Matrix: Water Reported By: MCB

Basis: As Received Reviewed By:

Reported By: MCB

Lab Information

		Reporting	Sample	
Analyte	CAS#	Limit	Result	Qualifier
Purgeable Volatiles				
Vinyl Chloride	75-01-4	1.0	1.0	U
trans-1,2-Dichloroethene	156-60-5	1.0	1.0	U
cis-1,2-Dichloroethene	156-59-4	1.0	1.0	U
1,1,1-Trichloroethane	71-55-6	1.0	1.0	U
Carbon Tetrachloride	56-23-5	1.0	1.0	U ·
Trichloroethene	79-01-6	1.0	1.0	U
1,4-Dichlorobenzene	106-46-7	1.0	0.6	J
Dibromofluoromethane	1868-53-7		110%	SS
1,2-Dichloroethane-d4	17068-07-0		102%	SS
Toluene-d8	2037-26-5		115%	SS
p-Bromofluorobenzene	460-00-4		104%	SS

E=Estimated value above instrument calibration range

J=Estimated value below reporting limit

U=Not detected at specified reporting limit

SS=Surrogate standard

CH2N...ILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CV0 2300 NW Walnut Boulevard Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

Project #	Purchase Order #		T		Demi	and A		al Metho			OR LAB USE O	
Froject#				T	пеци	ested v	maiyuk	al meulc	/ 			
Project Name		⊢ :								2000	Page	of
Project Name Mchilen Re USE Company Name	P. 1. 4 Stady	O T A						29		3089	Ĺ	12
Company Name	77187 21009	— î		ام				26		Leb PM	Custody F	Review
C. I as C. M. C. Ilan	·			9				00				
City of meallen Project Manager or Contact & Phone #	Report Copy to:	ہِ ا		8260				١ .		Log in	LIMS Verif	Ication
	1	[TOC	Vocs -	u	U	U	N.				
Kathy McKinley Requested Completion Date: Site ID	Kathy Mc Kinley	CON		$ \mathcal{C} $	TOC	TOC	Toc	700		· · · · · · · · · · · · · · · · · · ·		
1	• • • • • • • • • • • • • • • • • • •			9	 -			>		рН	Custody 8	edis Y)N
ASAP W.W.	T.P. #2 Dispose Retur	1					servati				Ice	4 V)N
	1916 11 62 1	— Ē		<u>-</u>		P T G	sor vau	V		QC Level 1 2	3 Other	
Type Matrix	i	R	 		7	×	4			40 1040.		
Sampling C G W S A O I M A T L P B E L R	CLIENT SAMPLE ID LA		HzSO4		4252H	H2504	H2504			Cooler Temperature	\sim \sim	
Date Time PBEL	(9 CHARACTERS) QC	Ì	77	12	72	~	2	7		Alternate Des	orintian	Lab ID
			1							Alternate Des	Cription	Lab ID
9/14/19/08:50 // ZG	P	2										
7/14/94 08:50 RO	P	3										Z
9/14/19/08:50 // Z G 9/14/19/08:50 // R O 4/14/19/08:50 // R O	PV	2					İ					7
4/14/94 08:50 / WW		2				/				<u> </u>		2
-' `-U-\' == 		2										7
		- -	 							· · · · · · · · · · · · · · · · · · ·		7
9/14/9908:50 2 5	P	2	 									l
								ļ		i i		
								 				
		+-				 -						
	Date/Time	Recel	and Day			Emph	Bottles			Date/Time		
Relinquished By Lillance	1/14/19 OB:3		laun	M.	•	Empty	43	•		9/14/19 08:3	0	
Sampled By and Title (Pleas	e sign and print name) Date/Time	Reling	ulshed By	1 1	.		(Please sto	jn and print na	me) (Date/Time		
	vier Hinojosa 7/14/69 08:50		ana		~y~	<u>- 5</u>	avier	n and print na	jaser	Date/Time 9/14/95 08:55	<u> </u>	
	e sign and print name) QUILARLON 11/4/4 OS:5	Reilnig	ulshed By	illo	riod		(Please sig	n and print na: ا ا زار ع	ma) ARRKAL	Date/Time 9/14/99		
Received By / (Piess	e sign and print name) Data/Time 1 / 99 / 34	Shippe	od Via		-			ipping #	I THE PART			
CVICIN	4715/49 1.34-	UPS	Fed-Ex	C OI	her							
Special instructions:	,											

CH2N. ILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CVO 2300 NW Walnut Boulevard Corvallis, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

					***				COC		文学
Project #	Purchase Order #			Requ	ested Analyti	cal Metho	d #		THIS AREA FOR	LAB USE ONLY	
Project Name McAllen Reuse Pilot Company Name City Of McAlle Project Manager or Contact & Phone # Kayly McKinley Requested Completion Date: Site ID	Report Copy to: Kathy McKinky Sample D			SDS HAHS SDS THM'S TKN, NO3-NO2/N, T-Phospherous	505 HAAS, 505 THM'S TKN, NO2-NO3/N, T-Phosphoraus, NH3-N	1.05 THU, MOS-MOS/N.	T-Phasphoraus MH3-N TKN, NO2-NO3/N, T-Phosphorous	207	Lab PM Log In pH	Custody Rev	tion
ASAP IJWTI	P#2 Dispose	Return I N E			Preservat					Ice	(Ŷ)N
Type Matrix	•	R		5	حد اره		7 _	(ه	QC Level 1 2 3	Other	
	CLIENT SAMPLE ID	LAB QC	ICE	TCE TO	I Ce Hz 504	LCe	H2504	Tile	Cooler Temperature	2	
Date Time PBELL	(9 CHARACTERS)	uc	17	H BAN	7 2		H2 H2	 	Alternate Descrip	tion I	Lab ID
9/14/99 08:50 / 29	Ρ	1	V								1
9/14/99 08:50 VV R O	P	ı		V							2
	P				V						
9/14/99 08:50 V ZG											1
9/14/19 08:50 UN RO	P				1						4
9/14/19 08:50 V RD						/					4
					***************************************						1
9/14/99 08:50 VV Z G	TP # 2 8 filluent										2
0/11/179 0(1.0)	P#-2 Effluent							/		····	3
9/14/99 09:01 VV WINT	1 - Z E F F WENT							<u> </u>			2
Relinguished By	Date/Tir		ed By		Empty Bottle	•		Date/Ti			
Ropie VillaMool	9/14/29	08:30 X h	in the	Lugar	9			9/	14/99 08:30	0	
	sign and print name) Data/Tir Data/Tir N. e. (1) 11 81056 11/4/99		Ished By	Denoin	_ Javi	gn and print nan	0,044	Date/Til	me 14/99 08:55	-	
Received By // / (Please	sign and print name) Date/Tit	me Relinqu	Ished By		(Pisase si	gn and print nan	ne)	Date/Ti	114/99		
	sign and print name) (7) 1 Parts/Til	Me, Shipper		illand	7(CoS) 8	hipping #	1254		17/99		
	eign and print name) Q Date Ti	me 3 Shipper	Fed-Ex	Other					· · · · · · · · · · · · · · · · · · ·		
Special Instructions:	•	·									ļ

CH2N-FILL Applied Sciences Lab CHAIN OF CUSTODY RECORD AND AGREEMENT TO PERFORM SERVICES

CVO 2300 NW Walnut Boulevard Corvalils, OR 97330-3638 (541) 752-4271 FAX (541) 752-0276

COC#

Project #	Purchase Order #	Π	Requested Analytical Method #				THIS AREA FOR LAB USE ONLY			
		_					 	Lab#		* Y
Project Name] [ا کی کے	1 3 x	ب ج	2 2 7		3089		\preceq
McAllen Kellse Pil	ot Study	O T A	8 P N	डिन्स मेर	2,	3 2 3		Lab PM	Custody Rev	lew
Company Name			E 0 8	N 214 715	Q 2	105, 5,11.2			1	
McAllen ReUse Pil Company Name City of McAl Project Manager or Contact & Phone #	lew	Ö	17 4 2	15 20 0 B	A 3	FONS		Log In	LIMS Verificat	lon
		F	300	कि गुरु होते	3 3	五部三百		rog in	LIMO VOITICA	LIOII
Ka My McKinley Requested Completion Date: Site ID	Kathy McKinley	C	Al, Ba, Ca, Fe, Mg, Ma, K, Na, Sr, As, Cd, Cr, Pb, Hg, Se, Ag, Zn	Alkalinity 1705, Color, Bromide, Chloride, Fluoride, Sulfate, Reactive Silica Al, Bay Ca, Fe, Ms, Mn,	K, Na, Sc, As, Cd, Cr Pb, 14g, Se, Ag, Zn	Alkalinity, TDS, Color, Bramide, Chloride, Flubride, Sultate, Recative, Silica				
Requested Completion Date: Site ID	/ Sample Disposal:	N T	2 2 6	16 18 E	گر ای	当る3.3		рН	Custody Sea	e x h
Requested Completion Date: Site ID A 5 A P NUT 1 Type Matrix	#2 Diapose Return	A I	4 2 4	Preser	vative	a. — L.			ice (N N
		E R						QC Level 1 2 3	Other	
Sampling C G W S A I M A T I R B E L R	CLIENT SAMPLE ID LAB	S	H 1003	ું હ	4003	9		Cooler Temperature	2	
M A T I A P B E L	(9 CHARACTERS) QC		3		3) <u> </u>		·		
	_,	<u> </u>		H				Alternate Descript	tion (Lab ID
9/14/99 08:50 UV R C 9/14/99 08:50 UV R O 9/14/99 08:50 UV Z G 9/14/99 08:50 UV Z G	9 9 1 1 1 1 1 1		V					•		Z
9/4/99 08:50 4 20	ρ									Z
9/14/09 68:50 / 26	dP)			\checkmark					
9/14/94 08:50 44 29	ρ					V				1
7/7/9/9/30										
	 									
								1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		
					-			I		
Relinguished Ry	Date/Time R	lecely	ad By	. Empty Bo	l j		Date/Ti			
Relinquished By LOOL VILLAND Sampled By and Title X Went June 1 (Please Received By LOUNTERNAME RESIDENCE CONTROLLED TO THE PROPERTY OF	9/14/4 D8: 3 0 X	X A	aver He	10 h	7			9/14/99 08:30		
Sampled By and Title (Please	ell Hing's Su 9/14/9/08:50 X	phillet	ished By	(Ple	use sign and print	i name)	Date/Tir	1/14/99 08:55		
Received By . // (Please	e sign and print name) Pate/Time R	lelingi	Ashed By	nojose Jan	JICHK HIN	O D S CC	Date/Ti	ר <u>ק איי אין דין דין דין דין דין דין דין דין דין ד</u>		
X Received By Date/Time Performe Relinguished By (Please sign and print name) Pate/Time Relinguished By (Please sign and print name) Resirving Res										
Received By (Please sign and print name)										
Special instructions:	71:101390	<u> </u>		· · · · · · · · · · · · · · · · · · ·	<u> </u>					
	•									



Ms. Anne McKee-Robbins CH2M HILL/CVO 2300 N.W. Walnut Blvd. Corvallis, OR 97330

> Columbia Analytical Services Report City of McAllen D9901720/D1454

> > October 20, 1999

Submitted by:

Karen Sellers

Project Manager/Client Services

TABLE OF CONTENTS

CAS Lab Reference No.: D1454 Level 1

	Page
	No.
Cover Page	i
Table of Contents	ii
Organic Data Qualifiers	iii
Organic Sample ID Qualifiers	
Sample Identification Cross-Reference	v
GC ORGANOCHLORINE PESTICIDES	
Case narrative	
Sample results	3
Chain of Custody Documentation	9
(This report contains a total of 16 pages.)	

Organic Data Qualifiers

- A -- This qualifier indicates that a TIC is a suspected aldol-condensation product
- B -- This flag is used when the analyte is found in the associated blank as well as the sample. This notation indicates possible blank contamination and suggests that the data user evaluate these compounds and their amounts carefully.
- C -- The "C" flag indicates the presence of this compound has been confirmed by the GC/MS analysis.
- This qualifier is used for all the compounds identified in an analysis at a secondary dilution factor. "D" qualifiers are used only for the samples reported at more than one dilution factor.
- E -- This flag indicates that the value reported exceeds the linear calibration range for that compound. Therefore, the sample should be reanalyzed at the appropriate dilution. The "E" qualified amount is an estimated concentration, and the results of the dilution will be reported on a separate Form I.
- I -- The qualifier indicates that the reporting limit to the "I" qualifier has been raised. It is used when the chromatographic interference prohibits detection of a compound at a level below the concentration expressed on the Form I.
- J -- Indicates an estimated value. It is used when the data indicates the presence of a target compound below the reporting limit or the presence of a Tentatively Identified Compound (TIC).
- N -- This qualifier indicates presumptive evidence of a compound. This flag is only used for Tentatively Identified Compounds (TIC), where the identification is based on a mass spectral library research. It is applied to all TIC results. For generic characterization of a TIC, such as chlorinated hydrocarbon, the "N" qualifier is not used.
- P This qualifier is used for Pesticide/Aroclor target analytes when there is a greater than 25% difference for detected concentrations between the two columns. The lower of the two values is reported on Form I and flagged with a "P".
- Indicates the compound was analyzed for but not detected. The number adjacent to
 the "U" qualifier indicates the reporting limit for that compound. The reporting limit
 can vary from sample to sample depending on dilution factors or percent moisture
 adjustments when indicated.

Organic Sample ID Qualifiers

The qualifiers that may be appended to the Lab Sample ID and/or the Client Sample ID for organic analysis are defined below:

- DL -- Diluted reanalysis. Indicates that the results were determined in an analysis of a secondary dilution of a sample or extract. A digit to indicate multiple dilutions of the sample or extract may follow the "DL" suffix. The results of more than one diluted reanalysis may be reported.
- **MS** -- Matrix spike (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- **MSD** -- Matrix spike duplicate (may be followed by a digit to indicate multiple matrix spikes within a sample set).
- R -- Reanalysis. The extract was reanalyzed without re-extraction. The "R" is not used if the sample was also re-extracted. May be followed by a digit to indicate multiple reanalysis of the sample at the same dilution.
- **RE** -- Re-extraction analysis. The sample was re-extracted and reanalyzed. May be followed by a digit to indicate multiple re-extracted analysis of the same sample at the same dilution.

Sample ID Cross-reference Table

CAS Lab Sample	Client ID Sample ID	Collect Date Sample Matrix	Additional Descripti	on () () () () () () () () () (
FS = Field	d Sample FS ZGPERMEATE	09/23/99 Water	TOP DUP A TE	
D1454001	FS ROPERMEATE	09/23/99 Water 09/23/99 Water	ZGPERMEATE ROPERMEATE	

The above lab sample ID's and cross reference information apply to samples as received by the laboratory. Modifiers to the lab sample ID may be added for internal tracking purposes. Any modified sample ID will be reflected in the appropriate case narrative only.

GC ORGANOCHLORINE PESTICIDES

CASE NARRATIVE GC ORGANOCHLORINE PESTICIDES

Project: <u>City of McAllen</u>

I. RECEIPT

No exceptions were encountered unless a Sample Receipt Exception Report is attached to the Chain-of-Custody included with this data package.

II. HOLDING TIMES

- A. Sample Preparation: All holding times were met.
- B. Sample Analysis: All holding times were met.

III. METHOD

Preparation: SW-846 3520C

Cleanup: NA

Analysis: SW-846 8081A

IV. PREPARATION

Sample volume may vary based on the amount of sample received per container.

V. ANALYSIS

- A. Calibration. All acceptance criteria were met.
 - Retention Time Windows: All analytes were within criteria.
 - 2. Degradation: All acceptance criteria were met.
- B. Blanks: All acceptance criteria were met.
- C. Surrogates: All acceptance criteria were met.
- D. Internal Standards: All acceptance criteria were met.
- E. Spikes: All acceptance criteria were met.
- F. Samples: Sample analysis proceeded normally.

I certify that this data package is in compliance with the terms and conditions agreed to by the client and Columbia Analytical Services, both technically and for completeness, except for the conditions noted above. Release of the data contained in this hardcopy data package has been authorized by the Laboratory Manager or designated person, as verified by the following signature.

SIGNED:	J. Water 10/10/99	Reviewer: /# WCC
	Jerry Watega Scientist, GC Organics	

CLIENT ID.

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

ZGPERMEATE

Case No.: D1454 SDG No.: D1454

Lab Sample ID:

D1454001

Matrix: WATER Level:

LOW

Lab File ID:

B1001024

Sample Wt/Vol: 1.050 L

Date Received: 09/24/99

Extract Vol:

10 ML

Date Extracted: 09/27/99

Column: DB5

Date Analyzed: 10/02/99

Extraction Type: Continuous

Dilution Factor: 1.0

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8	gamma-BHC (L: Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.011 0.0093 0.040 0.50	J J

CLIENT ID.

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

ROPERMEATE

Case No.: D1454 SDG No.: D1454

Lab Sample ID:

D1454002

Matrix: WATER

Level: LOW Lab File ID:

B1001025

Sample Wt/Vol: 1.050 L

Date Received:

09/24/99

Extract Vol:

10 ML

Date Extracted: 09/27/99

Column: DB5

Date Analyzed:

10/02/99

Extraction Type: Continuous

Dilution Factor: 1.0

CAS NO. COM	POUND Units: ug/L	MDL	RL	RESULT	Q
58-89-9gam 72-20-8End 72-43-5Met 8001-35-2Toxa	noxychlor	0.0032 0.0021 0.017 0.23	0.020 0.040	0.020 0.020 0.040 0.50	น บ บ

CLIENT ID.

PWB10927

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Lab Sample ID: PWB10927

Case No.: D1454 SDG No.: D1454 LOW Lab File ID: Matrix: WATER Level: B1001023

Sample Wt/Vol: 1.000 L Date Received:

Extract Vol: 10 ML Date Extracted: 09/27/99

Column: DB5 Date Analyzed: 10/02/99

Dilution Factor: 1.0 Extraction Type: Continuous

CAS NO.	COMPOUND	Units: ug/L	MDL	RL	RESULT	Q
72-20-8 72-43-5	gamma-BHC (1 Endrin Methoxychlor Toxaphene		0.0032 0.0021 0.017 0.23	0.020 0.020 0.040 0.50	0.020 0.020 0.040 0.50	บ บ บ

2C WATER SEMIVOLATILE SURROGATE RECOVERY

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1454 SDG No.: D1454

LAB ID		ı 	,	 			
01 PWB10927LCS PWB10927LCS 93 74 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0				j S1	S2	i S2	TOT
01 PWB10927LCS PWB10927LCS 93 74 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		TAR TO	CLIENT ID	! #	ĺ ±	i	OFF
01 PWB10927LCS PWB10927LCS 93 74 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		Í		1	1	1	1 1
02 PWB10927LCS PWB10927 96 89 0 04 D1454001 ZGPERMEATE 112 73 0 05 D1454002 ROPERMEATE 106 62 0 07 O8 O9						=====	1 1
03 PWB10927 PWB10927 96 89 0 04 D1454001 ZGPERMEATE 112 73 0 05 D1454002 ROPERMEATE 106 62 0 07 08 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0						i	0
03 PWB10927 PWB10927 96 89 0 04 D1454001 ZGPERMEATE 112 73 0 05 D1454002 ROPERMEATE 106 62 0 07 08 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	02	PWB10927LCS	PWB10927LCS	1 92	80		0
04 D1454001 ZGPERMEATE 112 73 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	03	PWR10927				I	
05 D1454002 ROPERMEATE 106 62 0 06 07						l ————	
06 07 08 09 <td< td=""><td></td><td></td><td></td><td></td><td></td><td>}</td><td></td></td<>						}	
07 08 09 10 11 12 13 14 15 16 17 18 19 20 20 21 22 23 24 25 26 27 28 29	05	D1454002	ROPERMEATE	106	[62		0
07 08 09 10 11 12 13 14 15 16 17 18 19 20 20 21 22 23 24 25 26 27 28 29	06		!		}		
08	07						
09	0,0					————][
10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29	00			·][
11][
12	10][
12	11][
13	12			·			<u> </u>
14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29	12		 ;				
15 16 17 18 19 20 21 22 23 24 25 26 27 28 29							[
16	14						
16	15						
17 18 19 20 21 22 23 24 25 26 27 28 29	16						
18	17						[
19	1						l
20 21 22 23 24 25 26 27 28 29	18						
21 22 23 24 25 26 27 28 29	19						1
21 22 23 24 25 26 27 28 29	20						
22 23 24 25 26 27 28 29	21		' 				[
23 24 25 26 27 28 29	21						lI
24	22						
24 25 26 27 28 29	23						
25 26 27 28 29	24						
26 27 28 29	25		 (
27 28 29	22						
28 29	46		<u></u>				[I
29		,					
29	28						
							
30[l
	301			 	l		ll

QC LIMITS (45-125) = Tetrachloro-m-xylene
= Decachlorobiphenyl (34-133)

page 1 of 1

FORM II

SW846

[#] Column to be used to flag recovery values
* Values outside of contract required QC limits
D Surrogates diluted out

WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1454

SDG No.: D1454 Column: DB5

LCS -

Sample No.: PWB10927

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
gamma-BHC (Lindane) Endrin Methoxychlor	0.5000	0.0000	0.5002	100	73-125
	0.5000	0.0000	0.4876	98	43-134
	0.5000	0.0000	0.4194	84	73-142

- # Column to be used to flag recovery and RPD values with an asterisk
- * Values outside of QC limits

RPD: 0 out of 0 outside limits Spike Recovery: 0 out of 3 outside limits

COMMENTS:	

SW846

3E WATER PESTICIDE LAB CONTROL SAMPLE

Lab Name: COLUMBIA ANALYTICAL SERVICES - REDDING

Case No.: D1454

SDG No.: D1454

Column: DB5

LCS -

Sample No.: PWB10927

COMPOUND	SPIKE	SAMPLE	LCS	LCS	QC.
	ADDED	CONCENTRATION	CONCENTRATION	%	LIMITS
	(ug/L)	(ug/L)	(ug/L)	REC #	REC.
Toxaphene	5.000	0.0000	4.895	98	41-126

- # Column to be used to flag recovery and RPD values with an asterisk
- * Values outside of QC limits

RPD: 0 out of 0 outside limits Spike Recovery: 0 out of 1 outside limits

COMMENTS:		

SW846

CHAIN OF CUSTODY DOCUMENTATION



CHAIN OF CUCTODY

5090 Caterpillar Road • Redding, CA 96003 • Phone: (530) 244-5227 • FAX: (530) 244-4109

coc # N? 90802

Project #							P	urcha	se O	rder	*									Requ	ested A	Analy	ytical N	lethod	#			THIS AREA FO	R LAB	USE O	NLY	
							┸										w ?										Lab	#		Page	of	
Project Na	ame	0		Λ	. 1	, ,	- ,	1							Ţ] :	3	704]			}				}	1	1454_	1	l	1 ('
MLA	lkn.	Kell	Lse	<u>. P</u>	10	<u> 45</u>	Au	dy							P	7.	對	ر و ر				Ì			}		Lab	ig. ventie	1	Custody	Review	
Company	Name	- -			n 11			•							12	\Š :	1			1	1	- 1					70	g verget	illa	3		
(1)	ty (2+		1/2/	/ [/	<i>3/W</i>	, T =		0						#	Lindane	116414	Methorus				İ					Log	16	7/7	LIMS V	erification	1
Company Company Project Mi Kathy Begggste	anageror Mulii	Cont	tact &	Phone 541 -	7.5	8-		eport	Lopy	/ 10: /}/	Kî.	nle	4		P	- 1	٠.	.,	L		,											
Requeste	d Comple	tion [9 3ate:	023	>	<u> </u>	Sit	e ID	/			Sa	mple	Disposal:	8	1	3			ļ		1					рН			Custody	Seals (N (S
·						C	17	4 9	f		Ì				N	Endrin, 1	000	3 3		-		1		1						ice	((3 z
AS	AP					W	W 7	م ا 4 الم 1 م -	en #2				pose	Return	N		<u> </u>			servativ	/e (to b	oe fill	led out	by cus	tomer)		ОС	Level 2 3	Oth	her		
Samp	oling	Tyl C		Matrix V S							LE II	D		LAB	R S	304		7				Ì		<u> </u>			Coc	oler Temperature	5.0	مو		
Date	Time	COMP	A T B E	V S 0 - L	R						ERS)			QC		H,		#25			_							Alternate Descri	ption		Lab II	D
9/23/99		ŀ	V	1	-	2 4	P	21	m	le	a	+	e		4	~															-1	
9/2 3 /99 9/2 3 /99			1	1		0	1 ^				.a		1		4			$\overline{\mathcal{L}}$													-2	,
	<u> </u>		T			T	Ţ										ļ								,							
		\Box	1	11	1	1				T		Γ					1		<u> </u>		1	\neg			1			······································				
 	 	H	\dashv	++		╅	†-	 	╁╌	╁	╁╌	+-	\vdash				十			1	+	_			 	†	T					
 	<u> </u>	-	+	┼┥	+	+-	╁	+-	╁	╁	+-	┼~	 - 		+		+		 	+	+-	-			 	┼─	+-					
		\vdash		╁╼┧	+		┿	╂—	┼-	╁	┼	┼-	⊢		┼	├	+		 	┼	┪	-+		 	ļ	 -	┼					
		\sqcup	_	$\bot \bot$	_	_ _	1	↓ _	 	╀	1_				<u> </u>	<u> </u>	4-		<u> </u>	 			<u></u>		 	<u> </u>	igspace					
]			-		-						ļ	ł			l		L	_			_	_			l					ļ		
					\top		T	Τ		Π		Π							ĺ								Τ					
l		\vdash	+	11	1	1	十	1	1	⇈	1	Ι-	\Box			 	Ť		l	T	1					 	\vdash		-			
Sampled F	ly and Tit	L_L			i_	1.	Pleas	e sio	n and	print	t nam	e)	لہل	Date/Tim	l	Ref	inqui	shed E	L	1			(Plea:	se sian a	ind print	name)	<u> </u>	Date/Time .				
Inus	in Pi	u R	0.	Tea	h,	È	nri	qu		K	/cz	<u> </u>	9	13/99	3:30					1/1	_ع		_En	rigue	e Per	CZ		9/20/0	g a) <u>8</u>	:40	
Sampled B	By C	il	<i>b</i>	1.0		الر	Pleas	e sig	n and	print	CZ t nam	e)		Date/Tim	e •	Reli	ingui:	eried E	Vil	lan	ام		(Pleas	se sign a	ind print	name)		Date/Time 9/2/4				
Received	<i>J.C.L. V</i> Bv	<u> </u>	an	.//	1	(Pleas	e sig	N and	prin	nam	<i>E P</i> ,	'+	Date/Tim	<u> 5. Ч</u> ю	Ship	oped	Via	7 40	uru	W.C.		Shipp	ing #	II MARC	14		1/297	7			
mer	1 m	L	elle	ار امیرورا	<u>/_</u>	M	2	10/	406	<u> /</u>	2	حكت		-24-99	02:	PO OB	3(Féd	Ex)	Other_				8	1290	700	<u>25</u>	117				
Received Special In	structions	r~ν	L	1	م و	, ,	n.l	lla	Ł	d	. 8	n	(1/23	1	99												INVOR		RMATIC	N	
<u>.</u>		' ' ፞፞፞፞፞፞፞፞፞፞	, , , , ,	, 00		_ `			-					•	′	•	•											P.O. #				}
2																												Bill To				
•																																
																												<u> </u>				



An Employee-Owned Company

5090 Caterpillar Road

Redding Ca., 96003

Phone: 530-244-5227

Fax: 530-244-4109

SAMPLE RECEIPT EXCEPTION REPORT

			<u> </u>				
Sampl	e Batch Number: D 1454	Client/Project:	CIty	of 1	McAller	2	
, , , , , ,							3 15 SA
\$.45 L		Comments:		er grande. Grant Levil	Al College Broker Suderest in State of	ing any aris	
	No custody seal as required by project.	2) No tim	e san	pled	RECORI From	ded on	P.E
$\overline{\mathcal{A}}$	2. Analysis, description, date/time of collection not provided.	labels.					
	Samples broken or leaking on receipt.						•
	Temperature of samples inappropriate for analysis requested.						
	Container inappropriate for analysis requested.						
	6. Inadequate sample volume.						
	7. Preservation inappropriate for analysis requested.						
	8. Samples received out of holding time for analysis requested.		ordina.				
	Descrepencies between COC form and container labels.					**	
	10. Other						
7.7							

Corrective Actions Taken:

Nove Regured

8ND 9/28/99

Sound Analytical Services, Inc.

ANALYTICAL & ENVIRONMENTAL CHEMISTS

4813 Pacific Hwy East • Tacoma, WA 98424 (253) 922-2310 • FAX (253) 922-5047 e-mail; sainc1@uswest,net



TRANSMITTAL MEMORANDUM

DATE: September 23, 1999

TO: Kathy McKinley City of McAllen 4100 Idela McAllen, TX 78503

PROJECT: McAllen Re-Use Pilot Study

REPORT NUMBER: 84099

Enclosed are the test results for two samples received at Sound Analytical Services on September 15, 1999.

The report consists of this transmittal memo, analytical results, quality control reports, a copy of the chainof-custody, a list of data qualifiers and analytical narrative when applicable, and a copy of any requested raw data.

Should there be any questions regarding this report, please contact me at (253) 922-2310.

Sincerely,

Daria Powell
Project Manager

Client Name

City of McAllen

Client ID:

ZENOGEM PERMEATE

Lab ID:

84099-01

Date Received:

9/15/99

Date Prepared: Date Analyzed: 9/21/99

% Solids

9/22/99

Dilution Factor

10

Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

			Recov	ery Limits
Surrogate	% Recovery	Flags	Low	High
2,4-Dichlorophenylacetic acid	86.4		48	124

Result

(ug/L)

PQL

MDL

Flags

Analyte 2,4-D Silvex (2,4,5-TP)

ND ND 0.096 0.096 0.084 0.077

Client Name
Client ID:
Lab ID:
Date Received:
Date Prepared:

Date Received:
Date Prepared:
Date Analyzed:
% Solids
Dilution Factor

City of McAllen RO PERMEATE 84099-02 9/15/99 9/21/99 9/22/99

10

Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

Recovery Limits
Surrogate % Recovery Flags Low High
2,4-Dichlorophenylacetic acid 73.6 48 124

 Result

 Analyte
 (ug/L)
 PQL
 MDL
 Flags

 2,4-D
 ND
 0.1
 0.087

 Silvex (2,4,5-TP)
 ND
 0.1
 0.081

Lab ID:

Method Blank - HB885

Date Received:

9/21/99

Date Prepared: Date Analyzed:

9/22/99

% Solids

1122195

Dilution Factor

10

Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

			Recov	ery Limits
Surrogate	% Recovery	Flags	Low	High
2,4-Dichlorophenylacetic acid	67.8		48	124

	Result			
Analyte	(ug/L)	PQL	MDL	Flags
2,4-D	ND	0.1	0.08 7	
Silvex (2.4.5-TP)	ND	0.1	0.081	

Blank Spike/Blank Spike Duplicate Report

Lab ID: Date Prepared: Date Analyzed: HB885 9/21/99 9/22/99 HB885

QC Batch ID:

Chlorinated Herbicides by USEPA Method 8151GC/MS Modified

	Blank	Spike	BS		BSD			
	Result	Amount	Result	88	Result	BSD		
Compound Name	(ug/L)	(ug/L)	(ug/L)	% Rec.	(ug/L)	% Rec.	RPD	Flag
2,4-D	0	5	4.73	94.6	4.48	89.6	-5.4	
Silvex (2,4,5-TP)	0	5	5.44	109	5.17	103	-5.7	

ANALYTICAL & ENVIRONMENTAL CHEMISTS
4813 PACIFIC HIGHWAY EAST, TACOMA, WASHINGTON 98424 - TELEPHONE: (253) 922-2310 - FAX; (253) 922-5047

DATA QUALIFIERS AND ABBREVIATIONS

- B1: This analyte was detected in the associated method blank. The analyte concentration was determined not to be significantly higher than the associated method blank (less than ten times the concentration reported in the blank).
- B2: This analyte was detected in the associated method blank. The analyte concentration in the sample was determined to be significantly higher than the method blank (greater than ten times the concentration reported in the blank).
- C1: Second column confirmation was performed. The relative percent difference value (RPD) between the results on the two columns was evaluated and determined to be ≤ 40%.
- C2: Second column confirmation was performed. The RPD between the results on the two columns was evaluated and determined to be > 40%. The higher result was reported unless anomalies were noted.
- M: GC/MS confirmation was performed. The result derived from the original analysis was reported.
- D: The reported result for this analyte was calculated based on a secondary dilution factor.
- E: The concentration of this analyte exceeded the instrument calibration range and should be considered an estimated quantity.
- J: The analyte was analyzed for and positively identified, but the associated numerical value is an estimated quantity.
- MCL: Maximum Contaminant Level
 - MDL: Method Detection Limit
 - N: See analytical narrative.
 - ND: Not Detected
 - POL: Practical Quantitation Limit
 - X1: Contaminant does not appear to be "typical" product. Elution pattern suggests it may be
- X2: Contaminant does not appear to be "typical" product.
- X3: Identification and quantitation of the analyte or surrogate was complicated by matrix interference.
- X4: RPD for duplicates was outside advisory QC limits. The sample was re-analyzed with similar results. The sample matrix may be nonhomogeneous.
- X4a: RPD for duplicates outside advisory QC limits due to analyte concentration near the method practical quantitation limit/detection limit.
- X5: Matrix spike recovery was not determined due to the required dilution.
- X6: Recovery and/or RPD values for matrix spike(/matrix spike duplicate) outside advisory QC limits. Sample was reanalyzed with similar results.
- X7: Recovery and/or RPD values for matrix spike(/matrix spike duplicate) outside advisory QC limits. Matrix interference may be indicated based on acceptable blank spike recovery and/or RPD.
- X7a: Recovery and/or RPD values for this spiked analyte outside advisory QC limits due to high concentration of the analyte in the original sample.
- X8: Surrogate recovery was not determined due to the required dilution.
- X9: Surrogate recovery outside advisory QC limits due to matrix interference.

SAS-QAM REV 11 3/99

Sound Analytical Services, Inc.

ANALYTICAL & ENVIRONMENTAL CHEMISTS
4813 Pacific Hwy East • Tacoma, WA 98424
(253) 922-2310 • FAX (253) 922-5047
c mail. sainet@nswest net

90	2
----	---

TURNAROUND REQUEST	business days)
Standard (10 days)	
RUSH: 24 hrs. 48 hrs	5 day

	c	HAII	N OF	CUST	ODY/R	EQI	UEST	FOR L	.AB	OR/	ATO	RY A	ANA	LYS	sis				
Client:	City OF	MA	Hear	<u>-</u> -		<u> </u>	Analys	es Requ	este	d									
Project	Name:	<u> </u>					Γ			[_	Γ	1		1	Г	Γ	Γ
MUAI	len Re-Use	P.1	ot 5	Hudy			ex cx	a F X											
Phone	len Re-Use t Kathy Mckinley No 541-758-	- 1701 DZ39	<u> lical 5</u> # 3	<u>rience j</u> S144	<u> </u>	of Containers	1-27	2,4,5-TP 5,14ex									į		
Fax No	Fax No.: 541-766-2852						2.	2 Q											
Email:	Kmckinlea) (h	7.m	CAO	`	5	<u></u>	6							ĺ			İ	
Use	Sample ID		Date	Time	Matrix	# Of	2,4-D; 2,45-TP	2,4-0,						İ					
	Zenogen Perm	ente	4114/69	08:20	Lignich	1	V												
7	RO Permeate		9/14/14	03:50	Liquid	1													
And the second s																 			
					1														
					 	 				·					-				
A A A A A A A A A A A A A A A A A A A							ļ	 		_						-		 	
Control of the contro															 				
				<u> </u>	İ .								!			 			
																 			
			-		ļ			ļ							_	-			
an Mari and nagarage																			
Antonio de la companio del companio de la companio del companio de la companio del companio de la companio del companio de la companio del					ļ														
					<u> </u>														
The control of the co																			
							1												
Comments of the comments of th									-						<u> </u>	-			
entre de la companya	,	-						 										-	

	Signature	Printed Name	Firm	Time/Date	Special Instructions
Relinquished By:	Jan Him	Janet Hinojosa	City of Not llen	08:55	
Received By	logie Villand	Posse VillALESA!	NiAlbn	08:55	
Relinquished By:	Rosie Villams	Posit VillARKS 174	acaller	9114149	
Received By	Cliana	Giana	SAS	9)15/99	DAm
Relinquished	0	- 0			""
Received By					

COC No	Page	_ of



ENERGY LABORATORIES, INC.

SHIPPING: 2393 SALT CREEK HIGHWAY . CASPER, WY 82601

MAILING: P.O. BOX 3258 • CASPER, WY 82602

E-mail: energy@trib.com • FAX: (307) 234-1639 • PHONE: (307) 235-0515 • TOLL FREE: (888) 235-0515

CASE NARRATIVE

DATE:

October 5, 1999

TO:

Kathy McKinley

FROM:

Sheryl Garling

RE:

CH2MHill Water Samples

SAMPLE NUMBERS: 32965 001 through 002

Samples Zenogem Permeate and RO Permeate were received on September 15, 1999. Samples were shipped using Energy Laboratories, Inc. contract service with UPS. The overnight option was used for shipping the samples to the laboratory. Samples were in good condition and properly preserved.

No analytical problems were indicated for this sample delivery group.

The methods used are methods published by US EPA for drinking water analyses. The methods used are as follows:

Radium 226 - EPA Method 903.0 (alpha emitting),

Radium 228 - EPA Method 904.0, and

Gross Alpha –EPA Method 900.1 (gross alpha minus uranium and

radon).

The standard detection limits for these methods are 0.2 pCi/L, 1.0 pCi/L, and 1.0 pCi/L, respectively. The initial e-mail response incorrectly identified methods and detection limits.

If additional information is required, please advise.



ENERGY LABORATORIES, INC.

SHIPPING: 2393 SALT CREEK HIGHWAY • CASPER, WY 82601

MAILING: P.O. BOX 3258 • CASPER, WY 82602 E-mail: energy@trib.com • FAX: (307) 234-1639 PHONE: (307) 235-0515 • TOLL FREE: (888) 235-0515

LABORATORY ANALYSIS REPORT - CH2M HILL

Project:
Sample ID:
Laboratory ID:
Sample Matrix:
Sample Date/Time:
Date Received:
Report Date:

McAllen Reuse	e Pilot Study
Zenogem Permeate	RO Permeate
32965-001	32965-002
Wat	er
09-14-99	9/0850
09-15	-99
October	4, 1999
09-15	-99

-		\	Reporting	TT 11		
Radiometric		Method	Limit	Units	Res	sults
Radium-226	²²⁶ Ra	903.0	0.2	pCi/L	< 0.2	< 0.2
Radium Precision ±					-	-
Radium-228	²²⁸ Ra	904.0	1.0	pCi/L	<1.0	<1.0
Radium Precision ±					-	-
ross Alpha	Gross a	900.1	1.0	pCi/L	<1.0	<1.0
G. Alpha Precision ±		,m.u.				-



RADIOCHEMICAL QUALITY ASSURANCE REPORT - CH2M HILL

Laboratory ID Range: Sample Matrix: Sample Date / Time: Date Received: Report Date:

32965-001-002 Water 09-14-99/0850 09-15-99 October 4, 1999

	Method	Relative Percent <u>Difference</u> 1	Spike Recovery (Percent) ²	LCS Recovery (Percent)	Method Blank (pCi/L)	Date Analyzed	Analyst
Laboratory #:		32996-002	32880-022		GA-40		
Gross Alpha:	900.1	0.0	104	106	< 1.0	10-01-99	RS
Laboratory #:		32880-001	32880-022		RA-206		
Radium-226:	903.0	0.0	100	101	< 0.2	09-29-99	RS
boratory #:		32880-010	32880-020		228-235		
adium-228:	904.0	0.0	79	7 7	< 1.0	10-04-99	LMH

(1) These values are an assessment of analytical precision. The acceptance range is 0-20% for sample results above 10 times the reporting limit. This range is not applicable to samples with results below 10 times the reporting limit.

(2) These values are an assessment of analytical accuracy. They are a percent recovery of the spike addition. ELI performs a matrix spike on 10 percent of all samples for each analytical method.

Report Approved By DI Raila

Reviewed By:

Log In No. 99-32965

lmh r:\Reports\Clients.99\CH2M_Hill\Water\rc32965-001.xls



ENERGY LABORATORIES, INC

Mail Only: PO Box 3258 •

Casper, WY

CHAIN OF CUSTODY RECORD 82602-3258

82601

toll free 1 \\ \frac{1}{235-0515} voice

307-235-0515

BillingsCasperGilletteRapid City UPS/FedEx Deliveries:

2393 Salt Creek Highway

Casper, WY •

fax 307-234-1639

For Sa	mple Tra	cking	g Pur	poses, Please Provide Contact Name and Telephone	"s as Indicate	d (S.	EE BAC	CK OF I	FORM I	FOR EX	AMPL	ES AND INSTRUCTIONS)
Project McAlle Polst S	Name / n lettse fudy	/ Me	cation Alkn	· /	ners ' U O Urine Other		Type of Analyses Requested				Special Requests	
Name Kafly N	ame / Phone # / Fax # Wathy McKinky / 541-758-0235 / 54-766-28252 Azm Hi /				Number of containers Sample Type: A W S V U O Air Water Soils/solids Legetation Urine Qthen	10s. A1pha	coss Alpha,					
Date	Time	composite	grab sample	Send Invoice to: Kathy McKinley CH2M HILL Corvallis OK. SAMES above	Vumber o) mple Type: A r <u>S</u> oils/solids	m 226, Gros Alpho m 228	226, 4005					
		сош	grab	Send Report to: Sample I.D.	l Sa <u>A</u> ir <u>W</u> ate	Radiun	Radium					Comments, Special Instructions, etc.
9/14/59	08:50			Zonogem Permeate RO Permeate		V						
9/14/99	08:50		/	RO Permeate	1		/					
				UPS-Al								
				•								
									-			
								:				

	1. Sampler: (signature)	Date	Time	Received by: (signature)	2. Relinquished by: (signature)	Date	Time	Received by: (signature)	
	claving Stingosa	9/14/99	01:50	Rosie Villanal	Regie Villaned	9/14/99	08:35		
	3. Relinquished by: (signature)	Date	Time	Received by: (signature)	4. Relinquished by: (signature)	Date 9/15/90	Time	Received at Laboratory by: (signifure)	1
ł						. //			_

For Sample Tracking Purposes, Please Provide Contact Name and Telephone # Project Name / Location / Purchase Order # Thunderbasin Town of Hope No PO # Name / Phone # / Fax # Jeff Jones @ (307) 555-1515, (307) 555-5555 fax				r of containers e: A W S V U hids <u>Vegetation U</u> rine	Σ				505, 508	31.1	Please fax results as soon as possible Thank you.
ime	composite	grab sample	Send Invoice to: Jeff Jones PO Box Nowhere Hope, WY 80000 Send Report to: Bob Brown	Number of containers Sample Type: A W S V U O Air <u>W</u> ater <u>S</u> olis/solid <u>Vegetation Unite O</u> the	sbestos - TEM	j's - RADs	, NO ₃ , F	Ss - 502.2	- 504,	- 515,5	
			PO Box Somewhere USA, WY 81111 Sample I.D.		¥	001	Ž)0 <i>x</i>	90	906	Comments, Special Instructions, etc.
			<u>, </u>		-						
1:35		х	Entry to Distribution	4	Х			Х		<u> </u>	Phase II SDWA Primary
1:45		X	Distribution Tap	9		Х	Х		х	Х	*
1:2	35	35	woo qara	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample 1.D. X Entry to Distribution	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample 1.D. Somewhere USA, WY 81111 Sample 1.D. Sample 1.D.	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D. Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D.	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D. Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D.	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D. X Entry to Distribution 4 X	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D. Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample I.D.	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample 1.D. Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample 1.D.	Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample 1.D. Send Report to: Bob Brown PO Box Somewhere USA, WY 81111 Sample 1.D. X Entry to Distribution 4 X X X

1.Sampler: (signature) Jeff Jones	Date 5-28-95	Time 12:05p	Received by: (signature) Harry Truckers	2.Relinquished by: (signature) Harry Truekers	Date 5-28-95	Time 13:15p	Received by: (signature) Sheryl A. Garling
3. Relinquished by: (signature)	Date N/A	Time N/A	Received by: (signature)	4. Relinquished by: (signature) Sheryl A. Garling	Date 5-28-95	Time 14:00y	Received at Laboratory by: Roger A. Garling

Instructions:

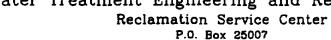
- (1) A completed Chain-of-Custody must be submitted with all samples
- Special Requests area can include (but not limited to) the following:

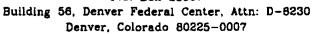
 Turnaround status, Rush status, Due Date, etc. (2)

 - Special mailing instructions:

 - send copy of Report and/or Invoice to a second party
 send copy of Report to a Government Agencies (EPA, etc.)
- Public Water System (PWS) Number
- Do you want samples returned to you or disposed of?

United States Department of the Interior Bureau of Reclamation Water Treatment Engineering and Research Group







FAXOGRAM

Date:
To: Jim Lozier / Angre Fornandez
Company: CH2MH1)
Fax Number:
From: Michell USBR
Fax Number: (303) 445-6329 Telephone Number: (303) 445-2245
Number of pages (including cover sheet)
Message: Copy of the Cleaning Solution
analysis. They are sending out
ter the Soy, I'll let you know.
Mahill

DATA TRANSMITTAL FAX COVER

Environmental Research Chemistry Laboratory, D-8240
US Bureau of Reclamation - Technical Service Center
PO Box 25007, Denver CO 80225-0007
Margaret Lake, Laboratory Manager, 303-445-2181
Douglas Craft, QC Officer, 303-445-2182
FAX 303-445-6326

-millim

DATE: 6/10/99
FROM: Barb Frost PHONE: X2190
TO: Michelle Chapman MAIL CODE:
OFFICE: FAX NUMBER:
PROJECT: McAllen DO LAB NUMBERS: \$5313-1
SAMPLES COLLECTED ON: 61199 NUMBER OF SAMPLES:
ANALYSES PERFORMED BY: BF I VM
This is an electronic transmission of analytical results. The final data and memorandum with appropriate formal review and requested QC reports will follow. The data in the attached report has been reviewed by the laboratory QC Officer (or designate) and meets TSC Chemistry Laboratory precision and accuracy requirements unless qualified in the section below. Please review your data and let us know if there are problems that require corrective action.
QUALIFIERS: The following issues may affect the usability of your data: \(\frac{1}{2} \) \\ \(\frac{1}{2} \) \\ \(\frac{1}{2} \) \(\fr
was acceptable
MESSAGE: Contract Soy and yind
APPROVAL Barb Frost Barb 5705 6/10/99 Client Representative For OC Officer Date
PAGE 1 OF REVIEWED-QUALIFIED SEE COMMENTS
LAB QC OFFICER DATE

SAMPLE LOG-IN SUMMARY

USBR ENVIRONMENTAL RESEARCH CHEMISTRY LABORATORY Denver, Colorado

	ntrol No: McAllen-99 gin Date: 6/3/99	Project Name: M Description: Cl	cAllen W-R leaning Solution			Reps: Bai Name: M.	rb Frost Chapman-Wilber
Chem Lab#	Client SampleID		Analysis	Sample Type	Sampled Date	Due Date	COC#
K5313-1	McAllen		ck	eaning sol	n. 6/1/99	6/10/99	
	unfiltered/unacidified, SO4/Ca	a/Fe/AVBa/Si	200.7_ICP 300.0_ANIO 355.1.365.2	NS lo	P Metals n chromatography al phosphomus h		rtnanalvzer

SAMPLE SUBMITTAL REQUEST FORM SHEET 1 OF							
Environmental Research Chemistry Laboratory, U.S. Bureau of Reclamation - Technical Service Building 56, Room 2340, Denver Federal Cente Margaret Lake, Laboratory Manager, 303-445-2	e Center er, PO Box 25007, Denv 2181						
Today's Date: $\frac{\sqrt{2/99}}{\sqrt{2/99}}$	f Report Data By: 4	10/99					
Samples Submitted By: Michelle Chaman W.	Report Data By: 4	e4					
Mailing Address: D-8>30	FAX/LAN:						
Project Name: McAllen W.R	Job Number/WOII	D5945					
Sample Collection Location: Mallen							
Sampling Date(s): $\frac{6/1/99}{}$ Type of Samp	les: Clouming So Ni	ımber of Samples:	2_				
Samples Filtered? No Samples Preserved?	(describe) Cust						
Official Data Report To: Michello C U	U. lbert						
Copies To:		Report Requested?					
Special Instructions:	encum, Sulfat	le Silica.P.	hospha				
7	Requested	Method or	7				
SAMPLE IDENTIFIERS	Analyses	Det Lim					
1. Calcum							
2. Iran							
3.							
4.							
5.							
6.							
7.							
8.							
9.							
10.							
11.							
12.							

Report o	of Chemical Analyses	·		McAilen W-R Collected: 6/1/99								
-	ment of the Interior - Bureau of Re 07, Building 56, Room 2300, Den 80225-0007		-	,			*****					
Laboratory		SIO2	TP-P									
Number	Sample (D	mg/L	mg/L		 							•
K5313-1	McAllen	2.53	11.9		 							
	Detection limit:	0.02	0.005									
,·	Date Analyzed:	6/9/99	6/7/99		1	T		T	Γ	7		<u> </u>
	Analyst:	bf	vm					<u> </u>			<u> </u>	
· ·	EPA Method:	200.7	365.1						T			

Chem Lab#: K5313-1

Station ID: McAllen

MoreID:

Sampled Date: 6/1/99

Received Date: 6/2/99

Login Date: 6/3/99

Chain-Of-Custody:

Sample Type: cleaning soln.

Note: unfiltered/unacidified,

SO4/Ca/Fe/Al/Ba/Si

A	nalyte	Method_Ref	Result	Units Qualifier	MDL	Date Extract	Date Analyzed ^D	Oilution
	Al	200.7 EPA	5530	hg/L	30		6/10/99	1
	Ba	200.7 EPA	449	µg/L	4		6/10/99	1
	Ça	200.7 EPA	26	mg/L	0.03		6/10/99	1

U: Not Detected at Listed MDL.

J: Estimated.

MDL: Method Detection Limit.

Chem Lab#: K5313-1

Station ID: McAllen

MoreID:

Chain-Of-Custody:

Sample Type: cleaning soln.

Sampled Date: 6/1/99

Received Date: 6/2/99

Login Date: 6/3/99

Note: unfiltered/unacidified,

SO4/Ca/Fe/Al/Ba/Si

Analyte	Method_Ref	Result	Units (Qualifier MDL	Date Extract	Date Analyzed D	ilution
Fe	200.7 EPA	722	µg/L	4		6/10/99	1

U: Not Detected at Listed MDL.

J: Estimated.

MDL: Method Detection Limit.

Appendix F. ZenoGem Permeate Ion Analysis

Table F-1ZenoGem Permeate Scale Potential

Parameter	Units		6/11/99	6/14/99	6/16/99	6/21/99	6/23/99	Average
	e marine en la la la la la la la la la la la la la	ini with						in a man in u
Alkalinity	mg/L as CaCO ₃	150	-	190		158		166
Total Phosphorus	mg/L as P			2.72		2.26		2.49
Sulfate	mg/L	250	214	214				226
Adde:								
Aluminum ^a	mg/L	0.1	0.1	0.1	0.1	0.1	0.1	0.1
Barium	mg/L	0.06	0.06	0.06	0.05	0.05	0.06	0.06
Calcium Hardness	mg/L	360		348		360		356
Iron ^a	mg/L_	0.1	0.1	0.1	0.1	0.1	0.1	0.1

^aNot dectected at specified reporting limits for each sampling event.

SPIRAL WOUND MEMBRANE ELEMENT AUTOPSY

PURPOSE AND LOCATION OF AUTOPSY

Purpose of Autopsy: McAllen, TX Wastewater Reclamation Project: Determination of scaling in end element.

Date and Place: October 29, 1999, USBR WTER Pilot Plant Lab, Denver, CO.

Date of This Report: 12/30/99

Names of Observers:

Frank Leitz Bill Boegli Michelle Chapman Wilbert Kim Linton Qian Zhang

ELEMENT IDENTIFICATION	
Manufacturer:	Hydranautics
Element Location:	Housing #6, 2nd element
Serial Number:	x03529
Element Dimensions:	2.5 in. x 40 in.
Number of Leaves:	2
Size of Leaves:	92.1 cm x 71.1cm Total Area 84.5 cm x 63.5cm Active Area per side (2.1 m² per element or 22.1 ft²)

OPERATING HISTORY

The RO system was operated for six months on site at the McAllen, TX South Waste Water Treatment Plant. Screened de-gritted sewage was first treated in a Zenogem bioreactor/microfiltration system, then chlorine and ammonia was added and the Zenogem effluent was forwarded to the RO system. The RO element array was a 2x2x1x1 and had 3 elements per vessel for a total of 18 elements in the system. RO recovery rates were set from 50% to 80% of 15.2 L/min feed flow.

Sulfuric acid and antiscalent were added to prevent scaling. However, due to changes in the chemical character of the Zenogem effluent, or excessive gas formation in the acid tank which caused the acid feed pump to loose it's prime, the pH was not controlled well at all times. This resulted in a loss of permeate flow from the last vessel.

Also, traditional constituents used in an RO projection do not include phosphorous compounds. The researchers involved in this project began to suspect that phosphorous salts were the cause of excessive scale problems due to the nature of waste water treatment. Attempts at adjusting the pH to control phosphorous salts included running a projection with non-RO software to determine the potential for phosphate scaling. A range of pH settings and two control points for pH were tested in an attempt to control the scaling problems. The pH ranges tested were from 5.5 to 7 on the feed, and 5.5 to 6 on the concentrate. The lower pH control ranges were in response to this non-RO projected information.

Scaling also caused operators to clean the system approximately 4 times with a low pH solution at a pH of about 3. A high pH solution was not used to clean the membranes as there was no indication of biofouling and the system's performance was recovered using the acid cleanings.

DESCRIPTION OF EVENTS LEADING TO AUTOPSY

This element was subjected to one needle hole to help evaluate the integrity test methods.

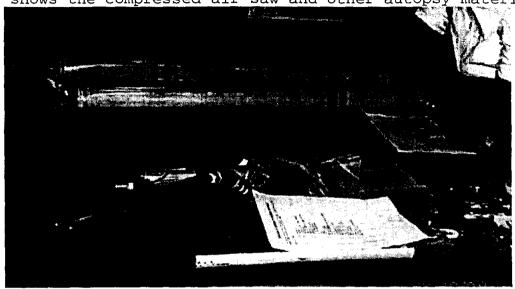
Subject element was the second to last element of the last vessel (vessel #6). Permeate recovery flow from the last vessel varied from 1.4 L/min to 0.01 L/min. The last fouling was a result of turning off the acid feed pump for approximately 8 hours.

This autopsy was primarily done to determine how deep the hole in the membrane leaves had penetrated, and to determine the general nature of the scaling composition.

NARRATIVE DESCRIPTION OF AUTOPSY PROCEDURE

Fiberglass wrapping was cut open and peeled or pried off.

Picture shows the compressed air saw and other autopsy materials.



Anti-telescoping devices were removed and tape wrap was unwound.

Unwound membrane and separated spacer material from first leaf.

Measured leaf dimensions and active area.

A squeegee was used to wipe both sides of one leaf. DI water was used to liquefy the fouling substance

Applied congo red dye to the first leaf.

Samples were cut from the feed and reject ends of the second leaf for SEM analysis. Feed side is Sample 2 and the reject side is Sample 3.

OBSERVATIONS

There was a crack, ~2 cm long, ~10 cm from the feed end.

Sample #1 is the piece of fiberglass with the crack.

The brine seal was in good condition; it was saved as Sample #2

There was extra glue, possibly rubber cement, under the tape at the ends of the element-- probably to keep the end caps tight. Sample #3 is a bit of the glue peeled away from the end.

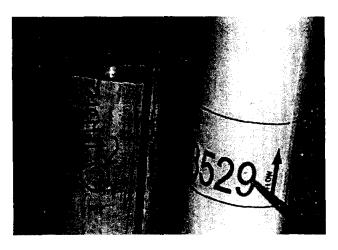
There was no evidence of the crack extending into the membrane material.

Picture was taken of the feed end of the rolled element.





Hole location was marked on the outer fiberglass cover from where a needle had been poked into the membrane. Picture taken of hole location in element. The hole location is shown in the fiberglass wrap and in the number 9 of the tape wrap.



At least 2 leaves had holes which were identified using a

magnifying glass (10x). The hole on the on the outer leaf was a cresent shape which is the same shape that would be formed by the tip of the hypodermic needle used to inflict the damage. The second hole protruded out, which would also be consistent with the direction the needle would penetrate.

The glue line appeared to have attracted more fouling material than the active area of the leaf. This may be due to the excessive use of glue.

Dye test on the second leaf with congo red dye took evenly over the membrane surface. This could be damage from low pH. There was no evidence of the hole extending beyond the tape wrap.

Test and Test Objective: No additional tests were done on this element.

DISCUSSION AND CONCLUSIONS

This element had at least two holes from the needle puncture which penetrated the active area of the membrane. The visible damage was configured in such a way that it can be attributed to the needle. One of the holes was cresent shaped and poked inward. The hole on the opposite leaf protruded outward.

SPIRAL WOUND MEMBRANE ELEMENT AUTOPSY

PURPOSE AND LOCATION OF AUTOPSY

Purpose of Autopsy: McAllen, TX Wastewater Reclamation Project: Determination of scaling in end element.

Date and Place: October 29, 1999, USBR WTER Pilot Plant Lab, Denver, CO.

Date of This Report: 11/21/1999

Names of Observers:

Frank Leitz Michelle Chapman Wilbert Kim Linton

ELEMENT IDENTIFICATION	
Manufacturer:	Hydranautics
Element Type:	LFC1X 2540
Element Location:	Housing #3, 2nd element
Serial Number:	x03531
Element Dimensions:	2.5 in. x 40 in.
Number of Leaves:	2
Size of Leaves:	91.8cm x 72.4cm Total Area 83.8cm x 62.8cm Active Area of one side (2.1 m² per element or 22.6 ft²)

OPERATING HISTORY

The RO system was operated for six months on site at the McAllen,TX South Waste Water Treatment Plant. Screened de-gritted sewage was first treated in a Zenogem bioreactor/microfiltration system, then chlorine and ammonia was added and the Zenogem effluent was forwarded to the RO system. The RO element array was a 2x2x1x1 and had 3 elements per vessel for a total of 18 elements in the system. RO recovery rates were set from 50% to 80% of 15.2 L/min feed flow.

Sulfuric acid and antiscalent were added to prevent scaling. However, due to changes in the chemical character of the Zenogem effluent, or excessive gas formation in the acid tank which caused the acid feed pump to loose it's prime, the pH was not controlled well at all times. This resulted in a loss of permeate flow from the last vessel.

Also, traditional constituents used in an RO projection do not include phosphorous compounds. The researchers involved in this project began to suspect that phosphorous salts were the cause of excessive scale problems due to the nature of waste water treatment. Attempts at adjusting the pH to control phosphorous salts included running a projection with non-RO software to determine the potential for phosphate scaling. A range of pH settings and two control points for pH were tested in an attempt to control the scaling problems. The pH ranges tested were from 5.5 to 7 on the feed, and 5.5 to 6 on the concentrate. The lower pH control ranges were in response to this non-RO projected information.

Scaling also caused operators to clean the system approximately 4 times with a low pH solution at a pH of about 3. A high pH solution was not used to clean the membranes as there was no indication of biofouling and the system's performance was recovered using the acid cleanings.

DESCRIPTION OF EVENTS LEADING TO AUTOPSY

Subject element was the second element in housing #3, one of two vessels that received flow first. Permeate recovery flow from this vessel varied from 2.8 L/min to 2.3 L/min. This element was subject to two holes punctured with a hypodermic needle. The fouling on the membrane was a result of turning off the acid feed pump for approximately 8 hours.

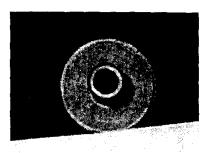
This autopsy was primarily done to determine the size and extent of damage resulting from the hypodermic needle. In addition, the general nature of the membrane and scaling composition is of interest.

NARRATIVE DESCRIPTION OF AUTOPSY PROCEDURE

Fiberglass wrapping was cut open and peeled or pried off. Sample #1 is the fiberglass with the 2 holes marked.

Anti-telescoping devices were removed.

Photographed the feed end of the element.



X03531

Tape wrap was unwound.

Measured the total area and active area of one side of one leaf.

Applied congo red dye to the first leaf. Photograph of the dye stained membrane.



Sample #2 is a cutting from the leaf with the 2 holes in the glue line.

OBSERVATIONS

There were no cracks in this element fiberglass casing.

Two needle holes were visible in the fiberglass and tape wrap at a distance of 17.75 cm (~7 in) from the reject end.

The membrane was wound backwards - which probably makes no difference in performance, but does make autopsy confusing.

There were little black flecks on the membrane surface.

Glue lines were all solid.

Dye test showed no pin hole damage. There were only 2 holes in the glue line, neither of which extended through the hard, thick glue.

Test and Test Objective: Chemical analysis of fouling material on leaf 1

Organization Performing Test: USBR Chemistry Lab

Date: Submitted November 1, 1999

Observations from Test:

The analysis methods used for TDS, TSS, SO4, and Cl do not used acid to digest the samples. The method used for SO4 and Cl was EPA method 300.0A, ion chromatography. The other metals, except for phosphorous were digested with nitric acid and analyzed using the ICP (inductively coupled plasma) EPA method 30.15. Phosphorous is also digested, but under EPA method 365.1.

The results from both housing #3 and #6 are shown for comparison.

Analytes	Housing #3	Equivalent	Equivalent	Housing #6	Anions =>	Cations =>
	concentration	Anions =>	Cations =>	concentration	Ox. State *	Ox. State *
	(mg/L)	Ox. State *	Ox. State *	(mg/L)	Conc. / At.	Conc. / At.
İ		Conc. / At.	Conc. / At.		Wt.	Wt.
		Wt.	Wt.			
Total P	36.69	-3.6		135.2	-13.1	
Al	2.52		0.3	9.1		1.0
Ba	7.02		0.1	20.8		0.3
Fe	1.1		0.1	3.8		0.2
Ca	76.5		3.8	298.0		14.9
K	2.7		0.1	4.8		0.1
Mg	4.07		0.3	13.4		1.1
Na	21.3		0.9	38.0		1.7
Si	2.46		0.4	7.4		1.1
SO4	15.7	-0.3		20.6	-0.4	
CI	21.6	-0.6		33.7	-1.0	
Totals		-4.5	5.9		-14.5	20.3

DISCUSSION AND CONCLUSIONS

The holes did not penetrate through the heavy glue line into the permeable membrane surface.

The solids precipitated onto the membrane surface originally come from a saturated solution. When the autopsy is done, de-ionized water is used to rinse the scrapings from the surface of the membrane. Since the samples are scraped from the membrane using DI water, the concentration expressed as a value in milligrams per liter is not meaningful as a concentration unless it is expressed in equivalents.

When the concentrations are interpreted as equivalents, it can then be shown in both housing #3 and housing #6 that there are roughly the same number of equivalents of calcium and phosphorous in each housing. This indicates that the predominant form of what was left on the membrane was most likely calcium phosphate (hydroxy apetite). Housing #6 had a larger amount than housing #3 resulting in the flow almost ceasing in housing #6.

When dye was applied to the element from the 6th housing, it did not adhere. That membrane element was the second membrane from the end of the system. The membrane in the 3rd housing at the front end of the system absorbed the dye indicating damage to the membrane surface. One possible reason why is that the acid solution was stronger at the front end of the system, especially if there was a problem with the chemical feed system and the pH dropped towards 2. Another possible explanation is the phosphate scale acted as a buffer to protect the membrane surface from the sulfuric acid in the end of the system. Phosphoric acid is a weaker acid than sulfuric. Using the 1st ionization constants, phosphoric acid would be a pH of about 3, and sulfuric is less than 2. Using the second ionization constant, phosphoric acid would be a pH of about 8, and sulfuric would still be about 2. As the water became more saturated with calcium phosphorous, the sulfuric acid became buffered significantly.

SPIRAL WOUND MEMBRANE ELEMENT AUTOPSY

PURPOSE AND LOCATION OF AUTOPSY

Purpose of Autopsy: McAllen, TX Wastewater Reclamation Project: Determination of scaling in end element.

Date and Place: October 29, 1999, USBR WTER Pilot Plant Lab, Denver, CO.

Date of This Report: 12/30/1999

Names of Observers:

Frank Leitz Michelle Chapman Wilbert Kim Linton

ELEMENT IDENTIFICATION					
Manufacturer:	Hydranautics				
Element Type:	LFC1X 2540				
Element Location:	Housing #6, final element				
Serial Number:	x03536				
Element Dimensions:	2.5 in. x 40 in.				
Number of Leaves:	2				
Size of Leaves:	92.1cm x 72.7cm Total Area 82.6cm x 62.2cm Active Area per side (2 m ² per element or 22.1 ft ²)				
OPERATING HISTORY					

The RO system was operated for six months on site at the McAllen,TX South Waste Water Treatment Plant. Screened de-gritted sewage was first treated in a Zenogem bioreactor/microfiltration system, then chlorine and ammonia was added and the Zenogem effluent was forwarded to the RO system. The RO element array was a 2x2x1x1 and had 3 elements per vessel for a total of 18 elements in the system. RO recovery rates were set from 50% to 80% of 15.2 L/min feed flow.

Sulfuric acid and antiscalent were added to prevent scaling. However, due to changes in the chemical character of the Zenogem effluent, or excessive gas formation in the acid tank which caused the acid feed pump to loose it's prime, the pH was not controlled well at all times. This resulted in a loss of permeate flow from the last vessel.

Also, traditional constituents used in an RO projection do not include phosphorous compounds. The researchers involved in this project began to suspect that phosphorous salts were the cause of excessive scale problems due to the nature of waste water treatment. Attempts at adjusting the pH to control phosphorous salts included running a projection with non-RO software to determine the potential for phosphate scaling. A range of pH settings and two control points for pH were tested in an attempt to control the scaling problems. The pH ranges tested were from 5.5 to 7 on the feed, and 5.5 to 6 on the concentrate. The lower pH control ranges were in response to this non-RO projected information.

Scaling also caused operators to clean the system approximately 4 times with a low pH solution at a pH of about 3. A high pH solution was not used to clean the membranes as there was no indication of biofouling and the system's performance was recovered using the acid cleanings.

DESCRIPTION OF EVENTS LEADING TO AUTOPSY

Subject element was the last element of the last vessel (vessel #6). Permeate recovery flow from the last vessel varied from 1.4 L/min to 0.01 L/min. This fouling was a result of turning off the acid feed pump for approximately 8 hours.

This autopsy was primarily done to determine if phosphate salts were of primary concern, or not. In addition, the general nature of the scaling composition is of interest.

NARRATIVE DESCRIPTION OF AUTOPSY PROCEDURE

The membrane was inspected during the autopsy at every step. First, the fiberglass wrapping was cut open using an air-powered cast saw set to cut at a shallow depth. The wrapping was then peeled or pried off. Anti-telescoping devices were removed from both ends of the membrane. Finally, the tape wrap was removed.

A squeegee was used to wipe both sides of the first leaf. DI water was used to liquefy the fouling substance. The material was collected in a sample jar labeled as Sample 1.

Researchers then applied a strong red red dye, congo red, to the second leaf.

Samples were cut from the feed and reject ends of the second leaf for SEM analysis with DI water added to the baggie to keep the membrane supple. Feed side is Sample 2 and the reject side is Sample #3.

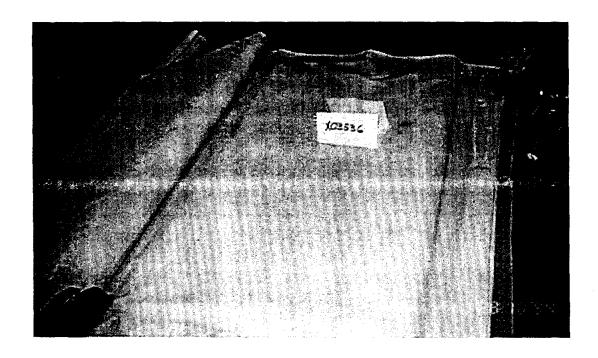
The material was collected from the first leaf was funneled into a sample jar labeled as Sample #4.



OBSERVATIONS

The scrapings from the first element were a brownish pink color. The pink may be dye. No visible scaling was apparent.

Dye test on the second leaf with congo red was negative indicating no structural damage or biofouling on the membrane surface. Dye will highlight biofouling as the dye adheres to a surface ripe with organisms.



Test and Test Objective: Chemical analysis of fouling material on leaf 1
Organization Performing Test: USBR Chemistry Lab

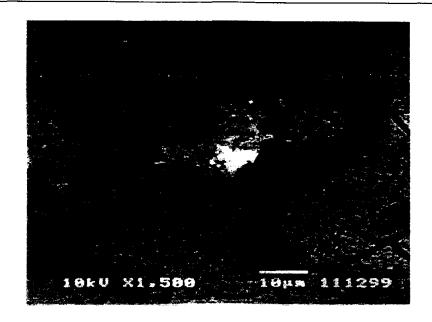
Date: Submitted November 1, 1999

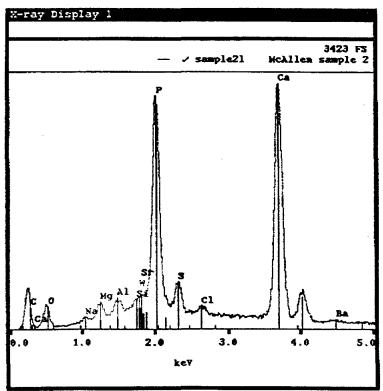
Test Results

Analytes	Housing #3	Equivalent	Equivalent	Housing #6	Anions =>	Cations =>
	concentration	Anions =>	Cations =>	concentration	Ox. State *	Ox. State *
	(mg/L)	Ox. State *	Ox. State *	(mg/L)	Conc. / At.	Conc. / At.
		Conc. / At.	Conc. / At.		Wt.	Wt.
l		Wt.	Wt.			
Total P	36.69	-3.6		135.2	-13.1	
Αl	2.52		0.3	9.1		1.0
Ba	7.02		0.1	20.8		0.3
Fe	1.1		0.1	3.8		0.2
Ca	76.5		3.8	298.0		14.9
K	2.7		0.1	4.8		0.1
Mg	4.07		0.3	13.4		1.1
Na	21.3		0.9	38.0		1.7
Si	2.46		0.4	7.4		1.1
SO4	15.7	-0.3		20.6	-0.4	
CI	21.6	-0.6		33.7	-1.0	
Totals		-4.5	5.9		-14.5	20.3

Observations from Test:

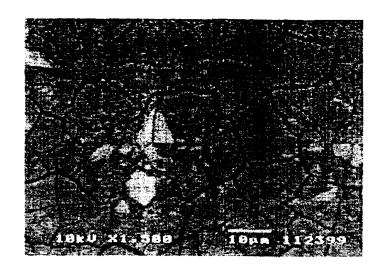
The analysis methods used for TDS, TSS, SO4, and Cl do not used acid to digest the samples. The method used for SO4 and Cl was EPA method 300.0A, ion chromatography. The other metals, except for phosphorous were digested with nitric acid and analyzed using the ICP (inductively coupled plasma) EPA method 30.15. Phosphorous is also digested, but under EPA method 365.1.

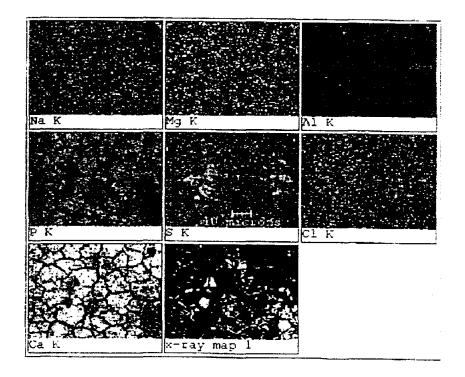




Test and Test Objective: SEM/Elemental Analysis of membrane samples from the second leaf to determine the nature of the scalant for element number X03536.

Organization Performing Test: USBR Date: Submitted November 1, 1999





SEM Distribution map of sampled elements for membrane # X03536

DISCUSSION AND CONCLUSIONS

SEM Test:

The X-ray display peaks should be interpreted as a qualitative analysis, not a quantative one. This analysis captures the energy spikes from the entire picture, not just the particle in the middle. The sample was hit with 10 kV of energy and magnified 3,500 times. Certainly, phosphorous and calcium are prevalent peaks. Barium and sulfur also show strong peaks on other samples not shown as part of this report because they are redundant to the information captured in the body of this report.

Although no visible scaling was apparent to the naked eye, this analysis clearly shows a fine silt-like layer covers the surface of the membrane. It appears from the distribution map that there is an even covering of these elements across the face of the membrane. The particle in the middle does not seem to be of a different character as compared to the rest of the scale layer.

Chemical Analysis of Scraping:

The solids precipitated onto the membrane surface originally come from a saturated solution. When the autopsy is done, de-ionized water is used to rinse the scrapings from the surface of the membrane. Since the samples are scraped from the membrane using DI water, the concentration expressed as a value in milligrams per liter is not meaningful as a concentration unless it is expressed in equivalents.

Using equivalents, it can then be shown in both housing #3 and housing #6 that there are roughly the same number of equivalents of calcium and phosphorous in each housing. This indicates that the predominant form of what was left on the membrane was most likely calcium phosphate (hydroxy apetite). Housing #6 had a larger amount than housing #3 resulting in the flow almost ceasing in housing #6.

The enclosed materials are considered proprietary property of ZENON Environmental Inc. No assignments either implied or expressed, of intellectual property rights, data, know how, trade secrets or licenses of use thereof are given. All information is provided exclusively to the addressee for the purposes of evaluation and is not to be reproduced or divulged to other parties, nor used for manufacture or other means or authorize any of the above, without the express written consent of ZENON Environmental Inc. The acceptance of this document will be construed as an acceptance of the foregoing conditions.

ZeeWeed® Tertiary Treatment System

BUDGET PROPOSAL for a ZeeWeed® Membrane Filtration Tertiary Filtration Treatment System for the City of McAllen, Texas Proposal Number #374-98 Rev. 2.0

Submitted to:

CH2M Hill 1620 W. Fountain Head Pkwy. #550 Tempe, AZ 85282

Attention:

Jim Lozier / Fair Miller

Submitted by:

ZENON Environmental Systems – Municipal Division 845 Harrington Court Burlington, Ontario L7N 3P3

December 7, 1999

Copyright[©] ZENON Environmental Systems 1999

Table of Contents

1.0	COMMERCIAL INFORMATION	3
1.1	PRICING SUMMARY	3
1.2	STANDARD TERMS AND CONDITIONS	5
1.3	STANDARD TERMS AND CONDITIONS ZENON STANDARD TERMS AND CONDITIONS	6
2.0	SYNOPSIS OF THE ZEEWEED® TERTIARY TREATMENT PROCESS	8
3.0	FEATURES & BENEFITS OF THE ZEEWEED® SYSTEM	9
4.0	ZEEWEED® TERTIARY TREATMENT PLANT	12
5.0	MAJOR EQUIPMENT	14
6.0	ATTACHMENTS	16

1.0 COMMERCIAL INFORMATION

1.1 Pricing Summary

The budget pricing to supply equipment and services as described in this proposal is as follows:

ZeeWeed® Membrane Tertiary Treatment System including membranes, permeate pumps, membrane air scour blowers, instruments and control system & equipment F.O.B. McAllen, Texas.

Four (4) Train ZeeWeed® Membrane Tertiary Treatment System to treat a maximum daily hydraulic capacity of 8.5 MGD.

Process equipment will be supplied loose, i.e. not on skids, for installation by others.

Fixed Capacity Flow

8.5 MGD

Budgetary System Price

US \$5,075,000.00

Validity

Pricing is for budgetary purposes only and does not constitute a final offer of sale.

Taxes and Duties

No taxes or duties or brokerage are included in the above pricing. Any taxes, duties, tariffs of any type are for the account of the Purchaser.

Field Service

The equipment pricing above includes Field Service from ZENON Technicians for assistance with the equipment installation, commissioning, operator training and process start-up assistance.

Any additional days of Field Service required will be at ZENON's Standard per diem rate of US\$650 per day plus living and travelling expenses.

Terms of Payment

The budgetary pricing quoted in this proposal is based on the following payment terms

- 15% with Purchase Order
- 25% on submission of General Arrangement Drawings

- 50% on shipment of equipment or notification that equipment is ready to ship (partial shipments permitted)
- 10% within 30 days of equipment start up or within 60 days of equipment shipment whichever is sooner.

Performance & Maintenance Bonds

The cost of providing performance or maintenance bonds is not included. If required these will be at additional cost.

Equipment Shipment and Delivery

A typical drawing submission and equipment shipment schedule is indicated below. Drawing submission milestones and equipment shipment periods are quoted from the date of acceptance of a formal signed Purchase Order:

Submission of GA Drawings:

8 to 10 weeks from acceptance of P.O

Drawing Approval:

3 weeks from submission of drawings

Equipment Shipment:

24 to 26 weeks from acceptance of P.O.

Plant Operation Manuals:

2 weeks after shipment of equipment to site When preferred by Customer but no later than

Operator Training:

when preferred by Customer but no later tha

2 weeks prior to the scheduled plant start-up

The above estimated delivery schedule is presented based on current workload backlogs and production capacity. If a formal purchase order is not received within the period of validity of this proposal, the delivery schedule is subject to review and adjustment.

The estimated delivery period quoted is presented based on review <u>and approval</u> of equipment shop drawings within a two (2) week period. Any delay in approval of shop drawings may affect the proposed shipment schedule.

Quality Basis

For the purposes of establishing a quality basis for equipment supply, reference is made herein to particular equipment manufactured by certain suppliers. The term "or equal" where used herein shall be deemed to mean "ZENON Approved Equivalent". ZENON reserves the right to substitute equipment that ZENON considers to be of equal quality and suitability for the intended application from alternative suppliers to those named herein. With regard to determining the suitability or otherwise of any particular manufacturer's equipment for inclusion as part of the ZeeWeed® system, ZENON's decision shall be final.

1.2 Standard Terms and Conditions

ZENON's Standard Terms and Conditions apply.

1.3 ZENON STANDARD TERMS AND CONDITIONS

Seller desires to provide its Customers with prompt and efficient service. However, to negotiate individually the Terms and Conditions of each Sales contract would substantially impair Seller's ability to provide such service. Accordingly, Products and Services furnished by Seller are sold only on the Terms and Conditions stated herein. Notwithstanding any terms or conditions on Customer's order, Seller's performance of any contract is expressly made conditional on Customer's agreement to Seller's Terms and Conditions of Sale unless otherwise specially agreed to in writing by Seller. In the absence of such agreement, commencement of performance and/or shipment shall be for Customer's convenience only and shall not be deemed or construed to be acceptance of Customer's Terms and Conditions, or any of them. If a contract is not earlier formed by mutual agreement in writing, acceptance of any Product or Service shall be deemed acceptance of the Terms and Conditions stated herein. All contracts for the Sale of Products shall be construed under and governed by the law of the location of Seller's plant at Burlington, Ontario, Canada.

QUOTATION AND PRICES

All quotations are subject to the Terms and Conditions stated herein as well as any additional Terms and Conditions that may appear on the face hereof. In the case of a conflict between the Terms and Conditions stated herein and those appearing on the face hereof, the latter shall control. Seller's prices and quotations are subject to the following:

- a) All published prices are subject to change without notice.
- b) UNLESS OTHERWISE SPECIFIED IN WRITING, ALL QUOTATIONS EXPIRE THIRTY (30) DAYS AFTER DATE THEREOF, MAY BE TERMINATED EARLIER BY NOTICE AND CONSTITUTE ONLY SOLICITATIONS FOR OFFER TO PURCHASE; further, budgetary quotations and estimates are for preliminary information only and shall neither constitute offers, nor impose any obligation or liability upon Seller.
- c) Unless otherwise stated in writing by Seller, all prices quoted shall be exclusive of transportation, insurance, taxes (including, without limitation, any sales, use, or similar tax, and any tax levied on or assessed to Seller after Product shipment by reason of Seller's retention of a security interest as provided herein), license fees, customs fees, duties and other charges related thereto and Customer shall report and pay any and all such shipping charges, premiums, taxes, fees, duties and other charges related thereto, and shall hold Seller harmless therefrom, provided that, if Seller, in its sole discretion, chooses to make any such payment, Customer shall reimburse Seller in full upon demand.
- Stenographic, typographical and clerical errors are subject to correction.
- e) Prices quoted are for Products only and do not include technical data, proprietary right of any kind, patent rights, qualification, environmental or other than Seller's standard tests and other than Seller's normal domestic commercial packaging unless expressly agreed to in writing by Seller.
- f) Published weights and dimensions are approximate only. Certified dimension drawings can be obtained upon request. Manuals, drawings or other documentation required hereupon must be referenced specifically.

This is merely a quotation, and the technology disclosed herein may be covered by one or more ZENON Environmental Inc. (ZENON) patents or patent applications. Any disclosure in this offer does not hereby grant, and nothing contained in the offer shall obligate ZENON to grant, an option to obtain a license to any technology or any other rights under any patent now or hereafter owned or controlled by ZENON.

TERMS OF PAYMENT

Inless credit is granted or otherwise specified in writing, payment is due upon shipment. All payments on approved credit accounts

shall be due in full thirty (30) days from date of invoice. Past due balances shall be subject to a service charge of 1-1/2% per month (18% per annum), but not more than the amounts allowed by law. Partial shipments will be billed as made and payments therefor are subject to the above terms. Payment shall not be withheld for delay in delivery of required documentation unless a separate price is stated therefor, and then only to the extent of the price stated for such undelivered documentation. Seller may cancel or delay delivery of Products in the event Customer fails to make prompt payment therefor, or in the event of an arrearage in Customer's account with Seller. Seller hereby retains a security interest in the Products finished until Customer has made payment in full in accordance with the terms hereof. Customer shall cooperate fully with Seller to execute such documents and to accomplish such filings and/or recordings thereof as Seller may deem necessary for the protection of Seller's interest in the Products furnished.

TRANSPORTATION AND RISK OF LOSS

Transportation will normally follow Customer's shipping instructions, but Seller reserves the right to ship Products freight collect and to select the means of transportation and routing when Customer's instructions are deemed unsuitable. Unless otherwise advised, Seller may insure to full value of the Products or declare full value thereof to the transportation company at the time of shipment and all freight and insurance costs shall be for Customer's account. Risk of loss and/or damage shall pass to Customer at the FOB point, which shall be the point of manufacture or such other place as Seller shall specify in writing, notwithstanding installation by or under supervision of Seller. Confiscation or destruction of, or damage to, Products shall not release, reduce or in any way affect the liability of Customer therefor. All Products must be inspected upon receipt and claims should be filed with the transportation company when there is evidence of shipping damage, either concealed or external. Notwithstanding any defect or nonconformity, or any other matter, risk or loss and/or damage shall remain with the Customer until the Products are returned at Customer's expense to such place as Seller may designate in writing. Customer, at its expense, shall fully insure Products against all loss and/or damage until Seller has been paid in full therefor, or the Products have been returned, for whatever reason, to Seller.

PERFORMANCE

Seller will make all reasonable effort to observe its dates indicated for performance. However, Seller shall not be liable in any way because of any delay in performance hereupon due to unforeseen circumstances or to causes beyond its control, including, without limitation, strike, lockout, riot, war. fire, act of God, accident, failure or breakdown of components necessary to order completion, subcontractor, supplier or customer caused delays, inability to obtain or substantial rises in the price of labour, materials or manufacturing facilities, curtailment of, or failure to obtain sufficient, electrical or other energy supplies, or compliance with any law, regulation or order, whether valid or invalid of any cognizant governmental body or any instrument thereof whether now existing or hereafter created. Performance shall be deemed suspended during, and extended for, such time as any such circumstances or causes delay its execution. Whenever such circumstances or causes are remedied, Seller will make, and Customer shall accept, performances hereupon. In addition, Seller's inventories and current production must be allocated so as to comply with applicable Government regulations. In the absence of such regulations, Seller reserves the right, in its sole discretion, to allocate inventories and current production and substitute suitable materials when, in its opinion, such allocation or substitution is necessary due to such circumstances or causes. No penalty clause of any kind shall be effective. As used herein, "performance" shall include, without limitations, fabrication, shipment, delivery, assembly, installation, testing, and warranty repair or replacement as applicable.

ACCEPTANCE

The furnishing by Seller of a Product to the Customer shall constitute acceptance of that Product by Customer, unless notice of defect or nonconformity is received by Seller within thirty (30) days of receipt of the Product at Customer's designated receiving address; provided that, for Product for which Seller agrees in writing to perform acceptance testing after installation, the completion of Seller's applicable acceptance tests, or execution of Seller's acceptance form

by Customer, shall constitute acceptance of the Product by Customer. Notwithstanding the foregoing, any use of a Product by Customer, its agents, employees, contractors or licensees for any purpose, after receipt thereof, shall constitute acceptance of that Product by Customer. Seller may repair or, at its option, replace defective or non-conforming parts after receipt of notice of defect or nonconformity.

ASSIGNMENTS AND TERMINATIONS

Any assignment by Customer of any contract hereupon without the express written consent of Seller is void. No order may be terminated by Customer except by mutual agreement in writing. Terminations by mutual agreement are subject to the following

- Customer will pay, at applicable contract prices, for all Products which are completely manufactured and allocable to Customer at the time of Seller's receipt of notice of termination.
- Customer will pay all costs, direct and indirect, which have been incurred by Seller with regard to Products which have not been completely manufactured at the time of Seller's receipt of notice of termination.
- Customer will pay a termination charge on all other determined costs and other charges. To reduce termination charges, Seller will divert completed parts, material or work-in-process from terminated contracts to other Customer's whenever, in Seller's sole discretion, it is practicable to do so.

PATENTS AND OTHER INDUSTRIAL PROPERTY RIGHTS

Seller will hold Customer harmless, as set forth herein, in respect to any claim that the design or manufacture of any Product in Seller's commercial line of Products, or manufactured to specifications set by Seller and furnished herein, constitutes an infringement of any patent or other industrial property rights of the United States or Canada. Seller will pay all damages and costs, either awarded in a ait or paid, in Seller's sole discretion, by way of settlement, which re based on such claim of infringement, provided that Seller is notified promptly in writing of such claim of infringement but there is no liability whatsoever herein with respect to any claims settled by Customer without Seller's prior written consent. In the event that Seller is required to hold Customer harmless hereupon, Seller will, in its sole discretion and at its own expense, either procure for Customer the right to continue using said Product, replace it with a customer the fight to continue using said Product, replace it with a non-infringing product, or remove it and refund an equitable portion of the selling price and transportation costs thereof. THIS SHALL CONSTITUTE SELLER'S ENTIRE LIABILITY FOR ANY CLAIM BASED UPON OR RELATED TO ANY ALLEGED INFRINGEMENT OF ANY PATENT OR OTHER INDUSTRIAL RIGHTS. Customer shall hold Seller harmless against any expense, loss, costs or damages resulting from claimed against any expense, loss, costs or damages resulting from claimed infringement of patents, trademarks, or other industrial property rights arising out of compliance by Seller with Customer's designs, specifications, or instructions. SELLER DISCLAIMS LIABILITY FOR U.S. OR CANADIAN PATENT OR COPYRIGHT INFRINGEMENT ARISING FROM USE OR MANUFACTURE BY ANYONE OF INVENTIONS IN CONNECTION WITH PRODUCTS OR SERVICES SOLD, USED, OR INTENDED FOR SALE OR USE, IN PERFORMING CONTRACTS WITH THE UNITED STATES OR CANADA. OR CANADA.

WARRANTY

Unless otherwise agreed to in writing, Seller warrants its Products to be free from defects in material or workmanship for a period of 12 months from the shipment of Product by Seller, provided that such Product are used, cleaned and maintained in accordance with the Seller's instructions. This warranty does not apply to normally replaceable parts or components such as

- filter cartridges, pump seals, membranes etc., (see below for membrane warranties)
- Customer undertakes to give immediate notice to Seller if goods or performance appear defective and to provide Seller with reasonable opportunity to make inspections and tests. If Seller is not at fault, Customer shall pay Seller the costs and expenses of the inspections and tests.
- Seller's obligations under this warranty is limited to the repair or replacement at its factory, or any device or part thereof which shall prove to have been thus defective. If Customer asks Seller to replace defective parts at Customer's premises, Customer agrees to pay for any traveling time and expenses, plus the Seller's labour to complete the replacement/repair.
- Goods shall not be returned to Seller without Seller's permission. Seller will provide Customer with a "Return Material Authorization" number to use for returned goods. All returns are F.O.B. Burlington, Ontario, Canada.
- Warranty on the membranes applies only if the membrane element(s) has been operated and cleaned according to Seller's instructions. When either permeate or concentrate flow drops by 10% from the original rates at the same operating conditions, cleaning must be initiated or the warranty will be null and void. Elements must be clean and be kept moist. They should be shipped to Seller in water-tight bags and must be protected from freezing. WARNING if element conditions of use given in Seller's instructions are not followed, the warranty will be null and void.

IMPLIED WARRANTIES, INCLUDING, BUT NOT LIMITED TO, WARRANTIES OF FITNESS FOR PARTICULAR PURPOSE, USE, OR APPLICATION, AND ALL OTHER OBLIGATIONS OR LIABILITIES ON THE PART OF THE SELLER, UNLESS SUCH OTHER WARRANTIES, OBLIGATIONS OR LIABILITIES ARE EXPRESSLY AGREED TO IN WRITING BY SELLER, ARE NULL AND VOID.

DAMAGES AND LIABILITY

DAMAGES AND LIABILITY
SELLER'S LIABILITY FOR DAMAGES SHALL NOT
EXCEED THE PAYMENT, IF ANY, RECEIVED BY SELLER
FOR THE UNIT OF PRODUCT OR SERVICE FURNISHED OR
TO BE FURNISHED, AS THE CASE MAY BE, WHICH IS THE
SUBJECT OF CLAIM OR DISPUTE. IN NO EVENT WILL
SELLER BE LIABLE FOR INCIDENTAL, CONSEQUENTIAL
OR SPECIAL DAMAGES, OF ANY KIND, HOWEVER
CAUSED, ARISING OUT OF, OR IN ANY WAY CONNECTED
WITH, THE PRODUCTS FURNISHED BY SELLER TO
CUSTOMER.

DISPUTES

All disputes under any contract concerning Products not otherwise resolved between Seller and Customer shall be resolved in a court of competent jurisdiction for the location of Seller's plant at Burlington, Ontario, Canada, and no other place. Provided that, in Seller's sole discretion, such action may be heard in some other place designated by Seller, if necessary to acquire jurisdiction over third persons, so that the dispute can be resolved in one action. Customer hereby consents to the dispute can be resolved in one action. Customer hereby consents to the jurisdiction of such court or courts and agrees to appear in any such action upon written notice thereof. No action, regardless of form arising out of, or in any way connected with, the Products or Services furnished by Seller, may be brought by Customer more than one (1) year after the cause of action has occurred. If any part, provision or clause of the Terms and Conditions of Sale, or the application thereof to any person or circumstances, is held invalid, void or unenforceable, such holding shall not affect and shall leave valid all other parts, provisions, clauses or applications of the Terms and Conditions remaining, and to this end the Terms and Conditions shall be treated as severable. severable

2.0 SYNOPSIS OF THE ZEEWEED® TERTIARY TREATMENT PROCESS

ZeeWeed[®] ultrafiltration system is a proprietary ZENON process technology that produces high quality treated water by drawing raw water through immersed ZeeWeed[®] membrane modules. ZeeWeed[®] "Outside-In", hollow-fibre membranes are manufactured ultrafiltration (UF) pore size. The ZeeWeed[®] UF Membranes have an absolute pore size of 0.1 microns and thus ensure removal of particulate matter greater than 0.1 microns in size such as most particulate matter, including bacteria, solids, Giardia cysts and Cryptosporidium oocysts, cannot enter the treated effluent stream. The ZeeWeed[®] Membrane ensures removal of a large percentage of impurities. The ZeeWeed membranes produce a high quality effluent, optimal for post-treatment by reverse osmosis.

The membranes operate under a slight vacuum created within the hollow membrane fibres by a permeate pump. Treated water is drawn through the membranes, enters the hollow fibres and is pumped out to the treated water storage tank (or distribution system). Air flow is introduced at the bottom of the membrane modules to create turbulence which scrubs and cleans the outside of the membrane fibres allowing them to operate at a high flux. The aeration also oxidizes iron and organic compounds, resulting in a treated water quality that is better than that provided by ultrafiltration alone.

ZeeWeed® membranes are immersed and therefore can tolerate high levels of solids. This is a main advantage when used as a tertiary treatment plant, since the ZeeWeed plant continues to operate well even when the upstream clarifier is upset and rejects solids to the UF. The capacity to handle solids also means that there is no need to pre-treat the clarified effluent, avoiding therefore the costs of sand filters or cartridge filters often required by other membrane technologies.

ZeeWeed® membranes have the additional benefit of being chlorine resistant up to concentrations of 1,000 mg/L. Therefore, influent water can be pre-chlorinated or the membranes can be easily cleaned, even when heavy fouling occurred.

The ZeeWeed® Membrane Technology process consistently produces high quality water, as the membranes are not subjected to stress, pressurization or rapid pressure fluctuations. Membrane cleaning by backpulsing is achieved by reversing the permeate flow and backwashing the fibre's lumen with permeate at low pressure (due to the high permeability of the ZeeWeed® membrane, the backpressure during backpulsing is low). The small variations in operating pressure occur smoothly over relatively long periods so that at no time is the membrane stressed. This, in turn, results in a membrane filtered permeate with the lowest sustainable particle count on the market.

3.0 FEATURES & BENEFITS OF THE ZEEWEED® SYSTEM

High Treated Effluent Quality

ZENON's ZeeWeed[®] Membrane Tertiary Treatment System is a cost effective method for membrane filtration removal of solids and is particularly recommended for treatment of the following contaminants in water:

Feed Water Element	Treated Water Quality
Suspended Solids	≥ 6 log removal
Average Turbidity	≤ 0.1 NTU
Particle Counts	Average $\leq 5/\text{mL}$, size range > 2 microns

Note: The information provided in this section of the proposal is general only and is intended only to indicate what is capable of being achieved with ZeeWeed® Membrane Water Treatment Technology based on consideration of specific raw water qualities and the type of treatment processes utilized.

Since the presence of air is continuous or semi-continuous in the process tank, materials which will readily oxidize, such as iron in its ferrous state, will be micro-precipitated and separated by the membrane, therefore producing a better quality water than if treated by ultrafiltration alone.

Advantages of an "Outside-In" Immersed Membrane

a) Single Step Treatment

The ZeeWeed® membrane is an outside-in membrane where the flow of water is from the outside of the membrane to the inside of the hollow fibre. This means that the inside of the membrane only comes in contact with clean, filtered water. The solids to be removed remain outside of the membrane where they do not cause fouling and plugging.

b) Low Energy Requirement.

Being immersed allows ZENON's ZeeWeed[®] Membranes to operate under a slight vacuum instead of under a high positive pressure, as do other membranes on the market. The ZeeWeed[®] Membrane operates under a differential pressure of 5"Hg to 18"Hg (5-20 ft H₂O) vacuum. This operational energy is very low and to ZENON's knowledge is the lowest in the membrane market.

c) Ability to Operate in a High Solids Environment

The ZeeWeed® membranes are immersed within the process tank, where suspended solids can exist without interfering with membrane operation. The operating flux rates of ZeeWeed® membrane modules are, for all practical purposes, independent of the solids content and turbidity of the raw water supply. This reflects in its capacity to operate well in a solids environment seen when the clarifiers get upset.

d) Stable and Low Particle Counts in the Effluent

The low energy backpulse of an immersed membrane does not produce significant expansion of the membrane pores. Expansion of the membrane pores, which results from high energy air backpulsing of the membranes as utilized in some types of membrane systems, can result in high particle counts immediately following backpulsing. This expansion of the membrane pores may potentially permit the passage of particles of larger sizes through the membranes until the membrane fibre fully relaxed from the expansion induced by the backpulsing process. Such systems cannot reliably use particle counters to verify the membrane integrity.

With the ZeeWeed[®] Membrane system expansion of the membrane pores is insignificant and the ZeeWeed[®] process consistently produces high quality treated water, which remains stable at all phases of plant operation.

Resistance to Oxidizing Chemicals

The ZeeWeed® membrane is resistant to chlorine and other typical water treatment plant oxidants (such as chlorine dioxide and potassium permanganate) in concentrations as high as 1,000 mg/L. This means that it is possible to pre-chlorinate the water without having to add a de-chlorination step such as Granular Activated Carbon (GAC) or bisulfite injection, which not only requires periodic chemical filling and maintenance, but also adds an unnecessary compound into the water. Where prechlorination is desired, chemical resistance also provides protection against dechlorination equipment failure, which could lead to severe damage of a chlorine sensitive membrane. Finally, chlorine resistance also allows for easy disinfection of the membrane and the plant should this be required.

Exceptional Membrane Durability

The ZeeWeed® membrane has been designed to be exceptionally durable and resistant to breakage. To achieve a high level of membrane durability ZENON utilizes a patented internal support on which the membrane is caste. This provides resistance to the membrane and protects it against tearing and breakage without reducing its flux capacity.

Simplicity of Operation

The ZeeWeed® process is an easy and inexpensive system to operate both in terms of maintenance costs and personnel requirements. Since treatment is a single stage process, there is no need for coagulants (except for colour and organics removal), clarifiers or sand filters as with some other membrane systems. Instead the plant operators are only required to ensure they maintain proper membrane permeating conditions by maintaining the permeate pumps and blowers in operation.

Ruggedness of Operation / Operational Flexibility

The ZeeWeed® Treatment Process consistently produces high quality treated effleunt irrespective of seasonal, operational and weather related variations in the source raw water quality, since the membranes can operate equally well in low or high solids concentrations and at varying temperatures:

without clogging

- without the need for pressurized air backpulsing cycles which consistently stress the membranes and lead to premature failure
- without any detrimental effects on the membrane flux since the ZeeWeed[®] membrane was developed for environments of high solids concentrations
- without breaking since the hollow fibre membrane is a composite developed to be both highly durable structurally as well as chemically resistant to outside elements

4.0 ZEEWEED® TERTIARY TREATMENT PLANT

Design Philosophy and Equipment Selection

ZENON proposes to offer a four (4) Process Stream Membrane Treatment Plant with each process train designed to produce a continuous treated water output of 1/4 of the required capacity of the plant. In the event of any type of operational problem or failure with one train the plant will function at 75% of the nominal average day flow design capacity, by adjusting the vacuum applied to the operating membrane modules. Future plant expansion, if and when required, can be achieved by adding additional treatment units.

The equipment proposed is designed for simplicity of operation. All plant operations are automatically controlled via a PLC. There are no normal operations that require manual operation of valves, pump speeds, etc. The system design philosophy is to reduce as far as possible the potential for system problems caused by operator error.

The treatment system proposed by ZENON does not include a chlorine dosing system to add residual chlorine to the treated effluent.

CONCRETE, EQUIPMENT LOOSE

The ZeeWeed® Membrane Tertiary Treatment System is designed with major process equipment supplied loose for installation on concrete pads. The ZeeWeed® membranes are supplied for installation in concrete tanks (by others) within Zenon supplied membrane support beams. The membrane air scour blowers are supplied loose for installation within an acoustically insulated blower room to minimize the noise transmission to the rest of the plant. Reject water will flow by gravity to the disposal point. The plant control panel will be supplied loose so that it can be either wall mounted adjacent to the plant or located in a separate control room depending on the Owner's preference.

5.0 MAJOR EQUIPMENT

The list below summarizes the major equipment and the quantities of items included for the ZenoGem® plant design.

SCOPE OF SUPPLY SYNOPSIS for the ZeeWeed® Plant			
Item	Size	Units	Quantity
Raw Water Feed			
Raw Influent Feed Pumps			Not Incl.
Inlet & Discharge Isolating Valves			Not Incl.
Discharge Check Valves			Not Incl.
Piping Manifold			Not Incl.
Wet Well Level Switches			Not Incl.
VFD's			Not Incl.
Raw Water Screening			
Raw Influent Screen			Not Incl.
Raw Influent Grinder			Not Incl.
Raw Influent Flowmeter			Not Incl.
Raw Influent Flow Control Flowmeter			Not Incl.
Raw Influent Flow Control Valve			Not Incl.
Membranes/Membrane Cassettes			
Individual Membrane Modules			640
Membrane Cassettes			80
Process Tanks & Frames		_	
Membrane Support Frames			Incl.
Process Tanks			Not Included
Permeate Collection Headers			4
Air Scour Headers			4
Permeate Pumps			
Permeate Pumps	2,497	USgpm	5
VFD's/Control Valves	50	HP	4
Piping Manifold			Not Incl.
Valves			Incl.
Air Extraction System			
Air Removal Separation Columns			4
Vacuum Pumps	24	scfm	3
Backpulse System			
Backpulse Water Storage Tank	6,480	USg	2
Hypochlorite Storage Tank	106	USg	1
Hypochlorite Feed Pumps	6.9	USgphr	2
Item	Size	Units	Quantity

Air Blowers			
Membrane Air Scour Blowers incl. Silencers	5,129	Scfm	3
Inlet & Discharge Isolation Valves			6
Discharge Check Valves			3
Inlet Control Valves			Incl.
Chemical Addition System (if required)			
Chemical Storage Tank			Not Incl.
Chemical Feed Pumps			Not Incl.
CIP System	•		
CIP Chemical Storage Tank			Incl.
CIP Chemical Feed Pump			Incl.
Instruments			
Permeate Flowmeters			4
Permeate Header Pressure Transducers			4
Process Tank Level Transmitters			4
Process Tank Level Switches			16
pH Transmitters			Not Incl.
Turbidimeters			1
Particle Counters			4
Membrane Blower Flow Switches			3
Permeate Pump Pressure Gauges			4
Membrane Air Scour Blower Pressure Gauges			3
Control Panel			
PLC-based Control Panel			1
Back-Up PLC			Not Incl.
Electrical			
MCC Panel			Not Included
Miscellaneous			
Air Compressor			2
Air Drier			1
Monorail for Cassette Removal			Not Incl.
Field Service Allowed			Days
Installation Supervision			5
Mechanical Checkout			5
Operator Training			2
Process Start-Up	***************************************		3
Commissioning			5
TOTAL MAN-DAYS			20
TOTAL No. TRIPS			3
Freight			
Delivery to Site			Incl.

6.0 ATTACHMENTS

Plant Power Consumption and Estimated Yearly Operating Cost

Table 9.1.1 Connected Power and Estimated Power Consumption at Average Day Flow

City of McAllen Eff Filtration Rev 2

Average Day Flow Maximum Day Flow 8,500,026 USgpd 8,500,026 USgpd 32,173 m3/day 32,173 m3/day

ITEM #		EQUIPMENT DESCRIPTION		# Operating Pumps Blowers etc.	Design Capacity	Discharge Head	Duty Point Efficiency	Equipment Operating BHP	Motor HP	Total Equipment BHP	Total Connected HP	Motor Efficiency %	Equipment kW	Hours / Day Continuous Operation	Energy Cost per year
1	-	Raw Water/Wastewater Screen	n/a	-				-		-	·	<u> </u>	-	24.00	
2	4.00		By Zenon	4.00	1,664.32 USgpm	35.00 ft	81.00	18.44	30.00	73.76	120.00	91.40	60.18	22.40	36,901
3		Backpulse Pumps	n/a	-	- USgpm	30.00 ft	-	-	-	•		<u> </u>	· .	6.40	
4	-	Recirculation Pumps	n/a	-	- USgpm	10.00 ft	55.00	-	-	-	-		_	24.00	-
5		Sludge Wasting Pumps	n/a		- USgpm	30.00 ft	50.00	-	-	•			-	2.00	-
6		Reject Water Pumps	n/a	•	 USgpm 	25.00 ft	55.00	-				-		24.00	
7_	3.00	Membrane Air Scour Blowers	By Zenon	2.00	3,840.00 scfm	4.25 psi	n/a	110.49	200.00	220.97	600.00	94.60	174.19	24.00	114,440
8	-	Process Air Blowers	n/a	. *	- scfm	6.00 psi	n/a	-	<u> </u>	-				24.00	
9	-	Miscellaneous Air Blowers	n/a	-	- safm	6.00 psi	n/a					-	-	24.00	
10	-	Anoxic Zone Mixers	n/a	- ·			n/a	-	l -	-		-		24.00	·
11	3.00	Air Separation System Vacuum Pumps	By Zenon	2.00	22.25 ac/m	18.00 ins Hg	n⁄a	2.25	3 00	4.50	9.00	87.50	3.84	24 00	2,520
12	2.00	Backpulse Sodium Hypochlorite - Metering	By Zenon	1,00	0.099 USgpm	50.00 ft	n/a	0.10	0.10	0.10	0.21	100.00	0 08	3.20	7
13	-	CIP Wash Pump	n/a	•	- USgpm	30.00 ft	55.00	-		-	-		-	0.02	-
14		CIP Chemical Metering	n/a		USgpm			•		-	-		-		-
15	-	Chemical Feed #1 System #1 - Metering	n/a	-	1.365 USgpm	50.00 ft	n/a	-	0.50	-	-	100.00	-	24.00	•
16	-	Chemical Feed #1 System #2 - Metering	n/a	-	0.101 USgpm	50.00 ft	n/a	-	0.03	-	•	100.00		24.00	+ .
17	•	Chemical Feed #1 System #3 - Metering	n/a	-	0.057 USgpm	50.00 ft	n/a	-	0.03	-	•	100.00	-	24.00	*
18		Chemical Feed #1 System #4 - Metering	n/a	-	0.101 USgpm	50.00 ft	n/a	-	0.03	-	-	100.00	-	24.00	-
18	2.00	Air Compressors	By Zenon	1.00	52.00 sc/m	100.00 psi	n/a	18.75	25.00	18.75	50.00	91.30	15.31	6.00	2,515
19	2.00	Air Driers	By Zenon	1.00	75.00 scfm		n/a	-	-	_		80.00	-	6.00	-
20	1.00	Controls & Instrumentation	By Zenon								1.34		1.00	24.00	657
21	1.00	Miscellaneous	By Zenon								1.34		1.00	24.00	657
		Total Connected Power				<u> </u>]		<u> </u>	1	781.89	HP	<u> </u>	<u></u>	
		Total Operating Power								318.09			255.59	ŁW .	
		Total Operating Cost	·····							0,0.00	<u></u>		200.00	US\$	157,696
		Total Operating Oost												- 009	101,030

Notes

Energy Costs based on

0.0750

US\$ per kW.hr

Power Consumption of other plant equipment required (raw water feed pumps, high lift pumps etc.) Is not included by ZENON

Where operating efficiencies are not known, the equipment operating power is assumed to be 75% of the motor nameplate power rating

The operating hours for the permeate pump are corrected for the downtime during backpulse cycles (and Membrane Pressure Decay Test Cycles if applicable)

Permeate Pump Backpulses every 15 mins for 30 seconds 2,496 USgpm @ 30.00 ft TDH = 24.89 BHP

Motor Efficiencies indicated are typical only. Efficiencies used are usually within 2% of actual when motor is operating within 50-100% of its full load rating

Operation of Air Compressor is assumed to be only 25% of time

Operation of the Sodium Hypochlorite Pumps is intermittent - operation for 25% of time is used for energy calculation

Blower Energy Consumption Estimated as:

6.770 BHP per 1,000 scfm per psig.

The motor sizes in the above table are preliminary only and estimated based on the information available at the time of preparing this proposal. It must be understood that at the time of proposal preparation, final headlosses or pressure drops in piping systems have not been calculated accurately Motor sizes are subject to confirmation (and if necessary adjustment) during final design. Use of the above information for sizing or selection of any ancillary equipment is entirely at the USER's own risk. Whilst the motor sizes indicated above are ZENON's best estimate based on design criteria assumed during preparation of the proposal, ZENON accepts no responsibility for the absolute accuracy of the information contained herein.

Table 9.2.2 Estimated Total Annual Operating Cost
City of McAilen Eff Filtration Rev 2
Average Day Flow 8,500,026 US
Maximum Day Flow 8,500,026 US 8,500,026 USgpd 8,500,026 USgpd

32,173 m3/day 32,173 m3/day

em			Cost per year		
Electrical Equipment - Zenon		Calculated at Average Day Flow	157,696	US\$	
Electrical Equipment - Others				USS	
Backpulse Chemicals	Sodium Hypochlorite	Calculated at Average Day Flow	8,232	USS	
CIP Chemical #1	MC-1		3,211	USS	
CIP Chemical #2	Sodium Hypochlorite - 250 mg/L		4,435	US\$	
CIP Neutralization Chemical #1			175	US\$	
CIP Neutralization Chemical #2			117	US\$	
Suggested Membrane Accrual			190,905	US\$	
Estimated Total Annual Opera	atina Cost		364,772	USS	

2511172100	Total Allinda operating ocs.			
Notes	Backpulse Chemical Consumption		Sodium Hypod	hiorite
	Sodium Hypochlorite Consumption		71.91	Litres per day
	Sodium Hypochlorite Consumption		26.248	Litres per vear
	Sodium Hypochlorite Cost	US\$		per Litre
	Codian rypodinana Cast			po. 2o
	CIP Cleaning Chemical #1		MC-1	
	Design Dosage		2,000.00	mg/L
	Solution Concentration		50.00	%
	Specific Gravity		1.240	
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tan	ks)	1,918.24	Litres
	Total Annual Chemical Consumption		1,918.24	Litres
	Chemical Cost	US\$	1.67	per Litre
	Chemical Cost	US\$	2.70	per kg
	CIP Cleaning Chemical #2		Sodium Hypod	hiorite - 250 mg/L
	Design Dosage		250.00	mg/L
	Solution Concentration		10.80	%
	Specific Gravity		1,168	
	Wash Frequency		12.00	times / year
	Chemical Consumption per Wash (all tan	ks)	1,178.52	Litres
	Total Annual Chemical Consumption		14,142.26	Litres
	Chemical Cost	US\$	0.31	per Litre
	CIP Neutralization Chemical #1		Sodium Hydro	wirta
	Design Dosage		625.00	
	Solution Concentration		50 00%	myrL
	Specific Gravity		1.520	
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tan	Los	489.02	
	Total Annual Chemical Consumption	IKS)	489.02	
	Chemical Cost	US\$		
	Chemical Cost	USS	0.47	per kg
	Chemical Cost	034	0.47	per ky
	CIP Neutralization Chemical #2		Sodium Blaulf	ite
	Design Dosage		146.00	mg/L
	Solution Concentration		38.00%	•
	Specific Gravity		1,290	
	Wash Frequency		12.00	times / year
	Chemical Consumption per Wash (all tan	ks)	177.11	
	Total Annual Chemical Consumption	,	2,125.32	
	Chemical Cost	US\$		per Litre
	Chemical Cost	US\$	0.55	per kg
			·	. •

12/07/1999 : 4:01 PM ZENON - CONFIDENTIAL

The enclosed materials are considered proprietary property of ZENON Environmental Inc. No assignments either implied or expressed, of intellectual property rights, data, know how, trade secrets or licenses of use thereof are given. All information is provided exclusively to the addressee for the purposes of evaluation and is not to be reproduced or divulged to other parties, nor used for manufacture or other means or authorize any of the above, without the express written consent of ZENON Environmental Inc. The acceptance of this document will be construed as an acceptance of the foregoing conditions.

ZenoGem[®]/ZeeWeed[®]
BUDGET PROPOSAL
for the City of McAllen, Texas
Wastewater Treatment Plant

BUDGET PROPOSAL # 374-98 Rev 1

Submitted to:

CH2M Hill 1620 W. Fountain Head Pkwy. #550 Tempe, AZ 85282

Attention:

Jim Lozier & Fair Miller

Submitted by:

ZENON Environmental Systems – Municipal Division 845 Harrington Court Burlington, Ontario L7N 3P3

December 7, 1999

Copyright® ZENON Environmental Systems

1999

CONFIDENTIAL

Table of Contents

COMMERCIAL INFORMATION	4
PRICING SUMMARY	4
STANDARD TERMS AND CONDITIONS	7
ZENOGEM® PROCESS DESCRIPTION	10
ZENOGEM® ADVANTAGES	12
Effluent Quality	12
Compact Plant	12
Lower Sludge Yield	13
Process Reliability	13
Advantages of an "Outside-In" Membrane	13
Exceptional Membrane Durability	13
ZENOGEM® PLANT	14
MAJOR EQUIPMENT	17
ATTACHMENTS	20
Plant Power Consumption and Estimated Yearly Operating Cost	20
	STANDARD TERMS AND CONDITIONS ZENOGEM® PROCESS DESCRIPTION ZENOGEM® ADVANTAGES Effluent Quality Compact Plant Expandability. Simple Operation. Lower Sludge Yield. Process Reliability Advantages of an "Outside-In" Membrane Exceptional Membrane Durability ZENOGEM® PLANT. MAJOR EQUIPMENT.

1.0 COMMERCIAL INFORMATION

1.1 PRICING SUMMARY

The budget pricing to supply equipment and services as described in this proposal is as follows:

One (1) ZenoGem® Membrane Bioreactor Waste Treatment System including membranes, aeration system, pumps, blowers, instruments, control system and equipment, FOB McAllen Texas.

Process equipment will be supplied loose, i.e. not on skids, for installation by others.

Fixed Capacity Flow

8.5 MGD

Budgetary System Price

US\$ 8,620,000.00

Validity

Pricing is for budgetary purposes only and does not constitute a final offer of sale.

Taxes and Duties

No taxes or duties or brokerage are included in the above pricing. Any taxes, duties, tariffs of any type are for the account of the Purchaser.

Field Service

The equipment pricing above includes Field Service from ZENON Technicians for assistance with the equipment installation, commissioning, operator training and process start-up assistance.

Any additional days of Field Service required will be at ZENON's Standard per diem rate of US\$650 per day plus living and traveling expenses.

Terms of Payment

The budgetary pricing quoted in this proposal is based on the following payment terms

- 15% with Purchase Order
- 30% on submission of General Arrangement Drawings
- 50% on shipment of equipment or notification that equipment is ready to ship (partial shipments permitted)
- 5% within 30 days of equipment start up or within 60 days of equipment shipment whichever is sooner.

Performance & Maintenance Bonds

The cost of providing performance or maintenance bonds is not included. If required these will be at additional cost.

Equipment Shipment and Delivery

A typical drawing submission and equipment shipment schedule is indicated below. Drawing submission milestones and equipment shipment periods are quoted from the date of acceptance of a formal signed Purchase Order:

Submission of GA Drawings:

8 to 10 weeks from acceptance of P.O

Drawing Approval:

3 weeks from submission of drawings

Equipment Shipment:

24 to 26 weeks from acceptance of P.O.

Plant Operation Manuals:

2 weeks after shipment of equipment to site

Operator Training:

When preferred by Customer but no later than

2 weeks prior to the scheduled plant start-up

The above delivery schedule is presented based on current workload backlogs and production capacity. If a formal purchase order is not received within the period of validity of this proposal, the delivery schedule is subject to review and adjustment.

The delivery period quoted is presented based on review <u>and approval</u> of equipment shop drawings within a two (2) week period. Any delay in approval of shop drawings may affect the proposed shipment schedule.

Quality Basis

For the purposes of establishing a quality basis for equipment supply, reference is made herein to particular equipment manufactured by certain suppliers. The term "or equal" where used herein shall be deemed to mean "ZENON Approved Equivalent". ZENON reserves the right to substitute equipment that ZENON considers to be of equal quality and suitability for the intended application from alternative suppliers to those named herein. With regard to determining the suitability or otherwise of any particular manufacturer's equipment for inclusion as part of the ZeeWeed® system, ZENON's decision shall be final.

Definitions

For the purposes of defining milestone dates for payments, commencement of equipment warranties and turnover of responsibility for the operation of equipment from ZENON to the OWNER, the following definitions apply:

Commissioning

Commissioning of the plant is defined as the date when wastewater first flows through the plant.

Substantial Completion Substantial Completion is defined as the date when the equipment supplied first meets the required treatment quality and quantities as defined in accordance with Performance Warranties. In cases where the equipment supplied is designed for a future plant design capacity it is the responsibility of the Owner to provide wastewater in sufficient quantities for the performance tests within the time frame outlined in section 7.0 (Performance Warranties).

On the date Substantial Completion is achieved:

- 1. Equipment and Process Warranties start.
- 2. Responsibility for the plant operation transfers from ZENON to the OWNER.
- 3. Holdbacks become due and payable.

OWNER

For the purposes of this document the term "OWNER" shall be also deemed to include the OWNER's appointed agents or assigns who will be responsible for the operation of the equipment / plant / treatment facility.

Equipment Drawings, Plans & Specifications

Unless otherwise specified, ZENON will furnish as part of this order the following types of drawings:

- 1. Process Flow Diagram
- 2. Process and Instrumentation Diagrams
- 3. General Arrangement Drawings showing equipment dimensions and weights required for the equipment foundations (foundations by others), and the utility requirements for the process equipment being furnished by ZENON with the System being supplied.
- 4. Standard sub-vendors dimensional outline drawings for the items of major process equipment (e.g. pumps, blowers, air compressors) which are necessary for the purchaser to complete its engineering and installation.
- 5. Standard sub-vendors equipment cut sheets for the major process equipment and other equipment items (major instruments and system components)
- Electrical Drawings including Single Line Diagrams, Control Panel Layouts and 6. Interconnecting Wiring Diagrams.
- 7. Assembly Drawings including General Equipment Layouts, deemed necessary by ZENON to be required for the Purchaser's field forces to erect the equipment.

Flow Definitions

For the purposes of defining membrane plant capacity after flow equalization, the following definitions shall apply:

Average daily flow. The average flowrate occurring over a 24-hour period based on total annual flowrate data.

<u>Maximum daily flow</u>. The maximum flowrate that occurs over a 24-hour period based on annual operating data.

<u>Maximum daily four hour flow</u>. The maximum sustained flowrate that occurs over a 4-hour period based on annual operating data.

<u>Peak hourly flow</u>. The peak sustained hourly flowrate occurring during a 24-hour period based on annual operating data.

<u>Minimum daily flow</u>. The minimum flowrate that occurs over a 24-hour period based on annual operating data.

<u>Minimum hourly flow.</u> The minimum sustained hourly flowrate occurring over a 24-hour period based on annual operating data.

<u>Sustained flow.</u> The flowrate value sustained or exceeded for a specified number of consecutive days based on annual operating data.

<u>Maximum monthly average flow</u>. This is the flow that is obtained by taking the month with the highest total flow and dividing by the number of days in that month. It provides information on the highest average flow that can be sustained for a one month period.

1.2 STANDARD TERMS AND CONDITIONS

ZENON's Standard Terms and Conditions apply.

ZENON STANDARD TERMS AND CONDITIONS

Seller desires to provide its Customers with prompt and efficient service. However, to negotiate individually the Terms and Conditions of each Sales contract would substantially impair Seller's ability to provide such service. Accordingly, Products and Services furnished by Seller are sold only on the Terms and Conditions stated herein. Notwithstanding any terms or conditions on Customer's order, Seller's performance of any contract is expressly made conditional on Customer's agreement to Seller's Terms and Conditions of Sale unless otherwise specially agreed to Terms and Conditions of Sale unless otherwise specially agreed to in writing by Seller. In the absence of such agreement, commencement of performance and/or shipment shall be for Customer's convenience only and shall not be deemed or construed to be acceptance of Customer's Terms and Conditions, or any of them. If a contract is not earlier formed by mutual agreement in writing, acceptance of any Product or Service shall be deemed acceptance of the Terms and Conditions stated herein. All contracts for the Sale of Products shall be construed under and governed by the law of the location of Seller's plant at Burlington, Ontario,

OUOTATION AND PRICES

All quotations are subject to the Terms and Conditions stated herein as well as any additional Terms and Conditions that may appear on the face hereof. In the case of a conflict between the Terms and Conditions stated herein and those appearing on the face hereof, the latter shall control. Seller's prices and quotations are subject to the following:

- a) All published prices are subject to change without notice.
- b) UNLESS OTHERWISE SPECIFIED IN WRITING, ALL QUOTATIONS EXPIRE THIRTY (30) DAYS AFTER DATE THEREOF, MAY BE TERMINATED EARLIER BY NOTICE AND CONSTITUTE ONLY SOLICITATIONS FOR OFFER TO PURCHASE; further. budgetary quotations and estimates are for preliminary information only and shall neither constitute offers, nor impose any obligation or liability upon Seller.
- Unless otherwise stated in writing by Seller, all prices quoted Unless otherwise stated in writing by Seller, all prices quoted shall be exclusive of transportation, insurance, taxes (including, without limitation, any sales, use, or similar tax, and any tax levied on or assessed to Seller after Product shipment by reason of Seller's retention of a security interest as provided herein), license fees, customs fees, duties and other charges related thereto and Customer shall report and pay any and all such shipping charges, premiums, taxes, fees, duties and other charges related thereto, and shall hold Seller harmless therefrom, provided that, if Seller, in its sole discretion, chooses to make any such payment, Customer shall reimburse Seller in full upon demand.
- d) Stenographic, typographical and clerical errors are subject to correction.
- Prices quoted are for Products only and do not include technical data, proprietary right of any kind, patent rights, qualification, environmental or other than Seller's standard tests and other than Seller's normal domestic commercial packaging unless expressly agreed to in writing by Seller.
- Published weights and dimensions are approximate only. Certified dimension drawings can be obtained upon request. Manuals, drawings or other documentation required hereupon must be referenced specifically.

This is merely a quotation, and the technology disclosed herein may be covered by one or more ZENON Environmental Inc. (ZENON) patents or patent applications. Any disclosure in this offer does not hereby grant, and nothing contained in the offer shall obligate ZENON to grant, an option to obtain a license to any technology or any other rights under any patent now or hereafter owned or controlled by ZENON.

TERMS OF PAYMENT

Unless credit is granted or otherwise specified in writing, payment is due upon shipment. All payments on approved credit accounts shall be due in full thirty (30) days from date of invoice. Past due balances shall be subject to a service charge of 1-1/2% per month (18% per annum), but not more than the amounts allowed by law. Partial shipments will be billed as made and payments therefor are subject to the above terms. Payment shall not be withheld for delay in delivery of required documentation unless a separate price is stated therefor, and then only to the extent of the price stated for such undelivered documentation. Seller may cancel or delay delivery of Products in the event Customer fails to make prompt payment therefor, or in the event of an arrearage in Customer's account with Seller. Seller hereby retains a security interest in the Products finished until Customer has made payment in full in accordance with the terms hereof. Customer shall cooperate fully with Seller to execute such documents and to accomplish such filings and/or recordings thereof as Seller may deem necessary for the protection of Seller's interest in the Products furnished.

TRANSPORTATION AND RISK OF LOSS

Transportation will normally follow Customer's shipping instructions, but Seller reserves the right to ship Products freight collect and to select the means of transportation and routing when Customer's instructions are deemed unsuitable. Unless otherwise advised, Seller may insure to full value of the Products or declare full value thereof to the transportation company at the time of shipment and all freight and insurance costs shall be for Customer's account. Risk of loss and/or damage shall pass to Customer at the FOB point, which shall be the point of manufacture or such other place as Seller shall specify in writing, notwithstanding installation by or under supervision of Seller. Confiscation or destruction of, or damage to, Products shall not release, reduce or in any way affect the liability of Customer therefor. All Products must be inspected upon receipt and claims should be filed with the transportation company when there is evidence of shipping damage, either concealed or external. Notwithstanding any defect or nonconformity, or any other matter, risk or loss and/or damage shall remain with the Customer until the Products are returned at Customer's expense to such place as Seller may designate in writing. Customer, at its expense, shall fully insure Products against all loss and/or damage until Seller has been paid in full therefor, or the Products have been returned, for whatever reason, to Seller. account. Risk of loss and/or damage shall pass to Customer at the whatever reason, to Seller.

PERFORMANCE

Seller will make all reasonable effort to observe its dates indicated for performance. However, Seller shall not be liable in any way because of any delay in performance hereupon due to unforeseen circumstances or to causes beyond its control, including, without limitation, strike, lockout, riot, war, fire, act of God, accident, failure or breakdown of components necessary to order completion, subcontractor, supplier or customer caused delays, inability to obtain or substantial rises in the price of labour materials or manufacturing or substantial rises in the price of labour, materials or manufacturing facilities, curtailment of, or failure to obtain sufficient, electrical or other energy supplies, or compliance with any law, regulation or order, whether valid or invalid of any cognizant governmental body or any instrument thereof whether now existing or hereafter created. Performance shall be deemed suspended during, and extended for, such time as any such circumstances or causes delay its execution. Whenever such circumstances or causes are remedied. Seller will make, and Customer shall accept, performances hereupon. In addition, Seller's inventories and current production must be allocated so as to comply with applicable Government regulations. In the absence of such regulations, Seller reserves the right, in its sole discretion, to allocate inventories and current production and substitute suitable materials when, in its opinion, such allocation or substitution is necessary due to such circumstances or causes. No penalty clause of any kind shall be effective. As used herein, "performance" shall include, without limitations, fabrication, shipment, delivery, assembly, installation, testing, and warranty repair or replacement as applicable.

ACCEPTANCE

The furnishing by Seller of a Product to the Customer shall constitute acceptance of that Product by Customer, unless notice of defect or nonconformity is received by Seller within thirty (30) days of receipt of the Product at Customer's designated receiving address; provided that, for Product for which Seller agrees in writing to

erform acceptance testing after installation, the completion of seller's applicable acceptance tests, or execution of Seller's acceptance form by Customer, shall constitute acceptance of the Product by Customer, snail constitute acceptance of the Product by Customer. Notwithstanding the foregoing, any use of a Product by Customer, its agents, employees, contractors or licensees for any purpose, after receipt thereof, shall constitute acceptance of that Product by Customer. Seller may repair or, at its option, replace defective or non-conforming parts after receipt of notice of defect or nonconformity.

ASSIGNMENTS AND TERMINATIONS

Any assignment by Customer of any contract hereupon without the express written consent of Seller is void. No order may be terminated by Customer except by mutual agreement in writing. Terminations by mutual agreement are subject to the following conditions:

- Customer will pay, at applicable contract prices, for all Products which are completely manufactured and allocable to Customer at the time of Seller's receipt of notice of
- Customer will pay all costs, direct and indirect, which have been incurred by Seller with regard to Products which have not been completely manufactured at the time of Seller's receipt of notice of termination.
- Customer will pay a termination charge on all other determined costs and other charges. To reduce termination charges, Seller will divert completed parts, material or work-in-process from terminated contracts to other Customer's whenever, in Seller's sole discretion, it is practicable to do so.

PATENTS AND OTHER INDUSTRIAL PROPERTY RIGHTS

Seller will hold Customer harmless, as set forth herein, in respect to any claim that the design or manufacture of any Product in Seller's commercial line of Products, or manufactured to specifications set y Seller and furnished herein, constitutes an infringement of any atent or other industrial property rights of the United States or Canada. Seller will pay all damages and costs, either awarded in a suit or paid, in Seller's sole discretion, by way of settlement, which are based on such claim of infringement, provided that Seller is notified promptly in writing of such claim of infringement but there is no liability whatsoever berein with respect to any claims settled is no liability whatsoever herein with respect to any claims settled by Customer without Seller's prior written consent. In the event that Seller is required to hold Customer harmless hereupon, Seller will, in its sole discretion and at its own expense, either procure for Customer the right to continue using said Product, replace it with a non-infringing product, or remove it and refund an equitable portion of the selling price and transportation costs thereof. THIS SHALL CONSTITUTE SELLER'S ENTIRE LIABILITY FOR ANY CLAIM BASED UPON OR RELATED TO ANY ALLEGED INFRINGEMENT OF ANY PATENT OR OTHER ENDITSTRIAL PICHTS. Customer shall hold Seller harmless INDUSTRIAL RIGHTS. Customer shall hold Seller harmless against any expense, loss, costs or damages resulting from claimed against any expense, loss, costs or damages resulting from claimed infringement of patents, trademarks, or other industrial property rights arising out of compliance by Seller with Customer's designs, specifications, or instructions. SELLER DISCLAIMS LIABILITY FOR U.S. OR CANADIAN PATENT OR COPYRIGHT INFRINGEMENT ARISING FROM USE OR MANUFACTURE BY ANYONE OF INVENTIONS IN CONNECTION WITH PRODUCTS OR SERVICES SOLD, USED, OR INTENDED FOR SALE OR USE, IN PERFORMING CONTRACTS WITH THE UNITED STATES OR CANADA OR CANADA.

WARRANTY

Unless otherwise agreed to in writing, Seller warrants its Products to be free from defects in material or workmanship for a period of 12 months from the shipment of Product by Seller, provided that such Product are used, cleaned and maintained in accordance with the Seller's instructions. This warranty does

- not apply to normally replaceable parts or components such as filter cartridges, pump seals, membranes etc.. (see below for membrane warranties).
- 2. Customer undertakes to give immediate notice to Seller if goods or performance appear defective and to provide Seller with reasonable opportunity to make inspections and tests. If Seller is not at fault, Customer shall pay Seller the costs and expenses of the inspections and tests.
- Seller's obligations under this warranty is limited to the repair or replacement at its factory, or any device or part thereof which shall prove to have been thus defective. If Customer asks Seller to replace defective parts at Customer's premises, Customer agrees to pay for any traveling time and expenses, plus the Seller's labour to complete the replacement/repair.
- 4. Goods shall not be returned to Seller without Seller's permission. Seller will provide Customer with a "Return Material Authorization" number to use for returned goods. All returns are F.O.B. Burlington, Ontario. Canada.
- Warranty on the membranes applies only if the membrane element(s) has been operated and cleaned according to Seller's instructions. When either permeate or concentrate flow drops by 10% from the original rates at the same operating conditions, cleaning must be initiated or the warranty will be null and void. Elements must be clean and be kept moist. They should be shipped to Seller in water-tight bags and must be protected from freezing. WARNING – if element conditions of use given in Seller's instructions are not followed, the warranty will be null

IMPLIED WARRANTIES, INCLUDING, BUT NOT LIMITED TO, WARRANTIES OF FITNESS FOR PARTICULAR PURPOSE, USE, OR APPLICATION, AND ALL OTHER OBLIGATIONS OR LIABILITIES ON THE PART OF THE SELLER, UNLESS SUCH OTHER WARRANTIES, OBLIGATIONS OR LIABILITIES ARE EXPRESSLY AGREED TO IN WRITING BY SELLER, ARE NULL AND VOID.

DAMAGES AND LIABILITY

SELLER'S LIABILITY
SELLER'S LIABILITY FOR DAMAGES SHALL NOT
EXCEED THE PAYMENT, IF ANY, RECEIVED BY SELLER
FOR THE UNIT OF PRODUCT OR SERVICE FURNISHED
OR TO BE FURNISHED, AS THE CASE MAY BE, WHICH IS
THE SUBJECT OF CLAIM OR DISPUTE. IN NO EVENT
WILL SELLER BE LIABLE FOR INCIDENTAL,
CONSEQUENTIAL OR SPECIAL DAMAGES, OF ANY
KIND, HOWEVER CAUSED, ARISING OUT OF, OR IN ANY
WAY CONNECTED WITH, THE PRODUCTS FURNISHED
BY SELLER TO CUSTOMER.

DISPUTES

All disputes under any contract concerning Products not otherwise resolved between Seller and Customer shall be resolved in a court of competent jurisdiction for the location of Seller's plant at Burlington, Ontario, Canada, and no other place. Provided that, in Seller's sole discretion, such action may be heard in some other place designated by Seller, if necessary to acquire jurisdiction over third persons, so that the dispute can be resolved in one action. Customer hereby consents to the jurisdiction of such court or courts and agrees to appear in any such action upon written notice thereof. No action, regardless of form arising out of, or in any way connected with, the Products or Services furnished by Seller, may be brought by Customer more than one (1) year after the cause of action has Conditions of Sale, or the application thereof to any person or circumstances, is held invalid, void or unenforceable, such holding shall not affect and shall leave valid all other parts, provisions, clauses or applications of the Terms and Conditions remaining, and to this end the Terms and Conditions shall be treated as severable.

2.0 ZENOGEM® PROCESS DESCRIPTION

The ZenoGem® Process is a proprietary ZENON technology that consists of a suspended growth biological reactor integrated with a microfiltration membrane system, based on the ZeeWeed® hollow fibre membrane. Essentially, the microfiltration system replaces the solids separation function of secondary clarifiers and sand filters in a conventional activated sludge system.

The ZeeWeed[®] microfiltration membranes are typically submerged in the aeration tank, in direct contact with the mixed liquor. Through the use of a suction duty pump, a vacuum is applied to a header connecting the membranes. The vacuum draws the treated water through the hollow fibre microfiltration membranes and into the pump. Treated water is then discharged by the pump. The energy associated with permeate pumping is relatively small. An airflow is introduced to the bottom of the membrane module producing turbulence which scours the external surface of the hollow fibres transferring rejected solids away from the membrane surface. This airflow also provides a large portion of the process biological oxygen requirements; the remainder is provided by a diffused aeration system. Waste sludge is pumped directly from the aeration tank.

The ZenoGem® technology effectively overcomes the problems associated with poor settling of sludge in conventional activated sludge processes. The ZenoGem® technology permits bioreactor operation with considerably higher mixed liquor solids concentrations than conventional activated sludge systems which are limited by sludge settling. The ZenoGem® process is typically operated at a mixed liquor suspended solids (MLSS) concentration in the range of 8,000 to 12,000 mg/L. The elevated biomass concentrations allow for highly effective removal of both soluble and particulate biodegradable material in the waste stream. The ZenoGem® process combines the unit operations of aeration, secondary clarification and filtration into a single process, simplifying operation and greatly reducing space requirements.

Since the ZenoGem® process can be operated at elevated MLSS concentrations, extended solids retention times (SRTs) are readily attainable. Accurate SRT control is very simple since no solids are lost in the effluent. Many municipal ZenoGem® plants are operated with SRTs exceeding 25 days. These extended SRTs ensure complete nitrification even under extreme cold weather operating conditions. At extended SRTs, sludge yields can be considerably less than conventional aerobic processes, due to endogenous decay.

The ZenoGem[®] process is readily adapted for denitrification if total nitrogen removal is required. The elevated levels of biomass become readily anoxic in the absence of aeration, ensuring high denitrification rates. An upstream anoxic zone and mixer readily accommodates denitrification; this can be incorporated in the ZenoGem[®] tank design.

The ZenoGem® process is ideally suited for phosphorus removal, where required. Through the addition of metal salts such as alum or ferric chloride to the raw wastewater or mixed liquor, soluble phosphorus in the waste stream can be precipitated. The ZeeWeed® membranes have a pore size that provides an absolute barrier to the discharge of precipitated phosphorus. The phosphorus is retained in the mixed liquor and removed with the waste activated sludge. The ZenoGem® process can reliably achieve

significantly lower effluent phosphorus concentrations than conventional municipal treatment processes.

3.0 ZENOGEM® ADVANTAGES

Effluent Quality

Depending on the specific application and design requirements, a ZenoGem[®] plant can achieve either high quality nitrified effluent or with the addition of an anoxic zone, high quality denitrified effluent. Phosphorus removal is readily achieved through the addition of metal salts to the feed wastewater or mixed liquor. Typically, ZenoGem[®] systems are capable of achieving the following effluent qualities.

 $\begin{array}{lll} BOD & <2 \ mg/L^{Note \ 1} \\ TSS & <2 \ mg/L^{Note \ 1} \\ TN & <10 \ mg/L^{Note \ 1} \ (cool \ climate) \\ & <3 \ mg/L^{Note \ 1} \ (hot \ climate) \\ TP & <0.1 \ mg/L \\ Turbidity & <1 \ NTU \\ Total \ Coliforms & <100 \ cfu/100 \ mL \\ Faecal \ Coliforms & <20 \ cfu/ \ 100 \ mL \\ \end{array}$

Note 1: The information provided in this section of the proposal is general only and is intended only to indicate what is the ZeeWeed®/ZenoGem® Membrane Wastewater Treatment Technology is capable of achieving. For the specific design treated wastewater quality, based on the consideration of specific raw wastewater characteristics and the required discharge criteria for the treated effluent, refer to Section 4.0.

Compact Plant

The ZenoGem® process can operate at mixed liquor suspended solids (MLSS) concentrations in the range of 8,000 to 12,000 mg/L, which is substantially greater than conventional activated sludge processes. This allows for conventional organic loading rates to be achieved with much lower hydraulic residence times. In addition, the ZenoGem® process requires a single tank in which aeration and solids separation are both achieved. If required, sludge digestion can also be accomplished in this tank. This single stage process results in an overall plant footprint substantially smaller than conventional tertiary wastewater treatment plants.

Expandability

Since the ZenoGem[®] equipment is modular in nature, plant expansion can be phased. Civil works can be designed for ultimate flow while membranes are added in phases as plant operating capacity dictates.

Simple Operation

Since the ZenoGem® process uses membranes to perform solid/liquid separation, there is no requirement for sludge to settle and thus no need for a secondary clarifier or polishing filters. Sludge is wasted directly from the aeration tank at a solids concentration in the range of 1.5 to 2.0 percent solids. The result is a single system which is simple to operate.

Lower Sludge Yield

The ZenoGem® plant can be operated at extended solids retention times (SRTs) allowing for lower net solids yields than conventional municipal treatment processes.

Process Reliability

Since the ZenoGem® plant is typically operated at low organic loading rates and the membrane provides an absolute barrier to particulate discharge, ZenoGem® effluent quality is not susceptible to hydraulic or organic surges which can negatively affect effluent quality in conventional activated sludge and fixed film plants. At periods of low flow (and organic load), the sludge within the reactor basin simply digests itself, without affecting the effluent quality.

Advantages of an "Outside-In" Membrane

a) Resistance To Fouling

The ZeeWeed® membrane is an outside-in membrane where the flow of water is from the outside of the membrane to the inside of the hollow fibre, meaning that the inside only sees clean, microfiltered water. The bacteria and inert solids to be removed from the wastewater remain outside the membrane and never enter the membrane to cause fouling.

b) Low Energy

Being immersed allows for the operation of the ZeeWeed® membrane under a slight vacuum (suction) instead of under positive pressure like other membranes on the market. The ZeeWeed® membrane operates under a vacuum of between -2 to -8 psi. The pump energy requirements to achieve this vacuum are relatively small.

Exceptional Membrane Durability

The ZeeWeed® membrane has been designed for exceptional durability and resistance to breakage. To achieve this high level of membrane durability ZENON utilizes a patented internal support to which the membrane is bonded. This support strengthens the membrane and protects it against tearing and breakage without reducing its flux capacity.

4.0 ZENOGEM® PLANT

Firm Capcity Flow

The proposed ZenoGem[®] plant is designed to continuously treat an average daily flow of 8.5 MGD. The ZenoGem[®] plant is a six (6) train system and the capacity of each parallel train is .1.417 MGD.

The ZenoGem® plant is capable of producing an effluent meeting or exceeding the following criteria:

8.5 MGD

Design Parameters

•				
<u>Parameter</u>	<u>Influent</u>		Effluent	
BOD	200	mg/L	≤2	mg/L
TSS	150	mg/L	≤2	mg/L
TKN	46	mg/L	≤3	mg/L
TN	46	mg/L	≤17	mg/L
TP	9	mg/L	≤1	mg/L
Wastewater Temperature	≥20	°C	≥20	°C

Equipment Selection

The main process equipment for the ZenoGem® plant, including permeate pumping equipment, membrane air scour blowers and supplemental aeration blowers, CIP membrane cleaning system, air extraction system, controls and other miscellaneous items, is designed for installation within equipment buildings (equipment buildings not included in ZENON's scope of supply).

The sizing of the main process equipment selected is as follows. Section 5.0 gives further details of the equipment items included by ZENON for this project.

Bioreactor (Process) Tank(s)

The bioreactors will consist of concrete tanks (concrete tanks not in ZENON's scope of supply). Six (6) individual process streams are required, each with the minimum dimensions of 160 ft long x 20 ft wide x 17 ft high (15 ft SWD). Each process tank will have an anoxic/aerobic and an aerated membrane zone separated by a baffle (baffle not included in ZENON's scope of supply).

Membrane cassettes will be supported by structural steel beams that will span between the concrete walls of the process tanks and will use the concrete walls as supports.

Process Tanks

Total Bioreactor Volume	2.154	MUS gallons
Design HRT	6	hours
Number of Membrane Trains	6	
Number of Bioreactor Tanks	6	
Volume of Each Bioreactor	359,000	US gallons

Length of Each Bioreactor	160	ft
Width of Each Bioreactor	20	ft
Side Water Depth of Bioreactor	15	ft

Note: Process tanks may be of concrete construction or fabricated steel tanks, whichever suits the client's preferences and are not included in ZENON's scope of supply.

Tank dimensions are preliminary only and may change slightly once final detail design commences.

ZW-500 Micro-Filtration Membrane Modules

Membrane	Design 1	Flux	11.55	gfd at Fixed Capacity Daily flow
Rate				
Minimum	Design Lie	quid	20	°C
Temperatur	e			
# Membran	e Modules		1104	
# Membran	e Cassettes		138	(8 modules per Cassette)

ZENON is committed to continuous development and invests continuously in research to develop better and higher flux membranes. For this reason ZENON reserves the right to change the number of membranes in its design, if by way of membrane technology improvements the permeability or operating flux rates of the membranes have been improved. This does not change the warranty since ZENON guarantees the design flow capacity and the operational performance of the membrane system.

Aeration System

The design air flow required for the fine bubble aeration system used with the ZenoGem® plant is approximately 5,550 scfm at the plant design capacity.

Aeration Blowers

Three (3) aeration blowers are included - two duty blower and one common stand-by unit. Each blower has a design capacity of 2,775 scfm. The aeration blowers are equipped with variable frequency drives (VFDs) to allow air delivery and dissolved oxygen levels in the wastewater to be controlled according to the system air requirements.

Membrane Air Blowers

Four (4) blowers are included for the membrane air scouring - four duty blower and one common standby unit The total required capacity of membrane air scouring is approximately 21,983 scfm. Each blower has a design capacity of 7,328 scfm.

Permeate Pumps

Seven (7) permeate pumps are included - six duty pumps and two shelf spares. Each pump is designed for a maximum permeate flow of 1,110 USgpm. The pumps will also provide backpulse flow at 2,880 USgpm The speed of the permeate pumps is controlled via VFD units according to the liquid level in the bioreactor tanks.

Sludge Recirculation Pumps

Seven (7) sludge recirculation pumps are included - six duty pumps and one shelf spare. Each pump is designed for a flow of 3,395 USgpm. The recirculation pumps are provided with VFD units to allow flow variation to allow optimization of the system process performance.

Sludge Wasting Pumps

Seven (7) sludge wasting pumps are included – eight duty pumps and one shelf spare. Each pump is designed for a flow of 207 USgpm.

Miscellaneous

No influent screening facilities are included. There must be existing screening and/or primary clarifiers upstream of what will become the ZenoGem[®] aeration (bioreactor) tanks. The screening equipment must be capable of screening particles down to 3.0 mm to prevent hair and other stringy materials from tangling with the membranes.

Equipment Installation cost is not included.

5.0 MAJOR EQUIPMENT

The list below summarizes the major equipment and the quantities of items included for the ZenoGem® plant design.

SCOPE OF SUPPLY SYNOPSIS		· · · · · · · · · · · · · · · · · · ·			
for the ZenoGem® Plant					
tor the Benodem Trans					
Item	Size	Units	Quantity		
Raw Wastewater Feed					
Raw Influent Feed Pumps			Not Incl.		
Inlet & Discharge Isolating Valves			Not Incl.		
Discharge Check Valves			Not Incl.		
Piping Manifold			Not Incl.		
Wet Well Level Switches			Not Incl.		
VFD's			Not Incl.		
Raw Water Screening					
Raw Influent Screen			Not Incl.		
Raw Influent Grinder			Not Incl.		
Raw Influent Flowmeter			Not Incl.		
Raw Influent Flow Control Flowmeter			Not Incl.		
Raw Influent Flow Control Valve			Not Incl.		
Membranes/Membrane Cassettes					
Individual Membrane Modules			1,104		
Membrane Cassettes			138		
Process Tanks & Frames					
Membrane Support Beam(s)			Included		
Process Tanks			Not Incl.		
Permeate Collection Headers			6		
Air Scour Headers			6		
Permeate Pumps					
Permeate Pumps	1,110	USgpm	7		
VFD's	50	HP	6		
Piping Manifold			Not Incl.		
Valves			Incl.		
Air Extraction System					
Air Removal Separation Columns			6		
Vacuum Pumps	22	scfm	3		
Backpulse System					
Backpulse Water Storage Tank	5,160	gallons	2		
Hypochlorite Storage Tank	106	gallons	1		
Hypochlorite Feed Pumps	6.08	USgphr	3		

Item	Size	Units	Quantity
DIP Tank Cleaning System			
DIP Tank			Not Incl.
Chemical Wash Pump			Incl.
Monorail & Pulley/Hoist for membrane removal			Not Incl.
Sludge Recirculation			
Sludge Recirculation Pumps	3,935	USgpm	7
Inlet & Discharge Isolation Valves			N/A
Discharge Check Valves			N/A
Piping			Not Incl.
VFD's	2.5	HP	6
Sludge Wasting			
Sludge Wasting Pumps	206.6	USgpm	7
Inlet & Discharge Isolation Valves		1	6
Discharge Check Valves		<u> </u>	6
Piping			Not Incl.
VFD's			N/A
Air Blowers			
Membrane Air Scour Blowers incl. Silencers	7,328	scfm	4
Inlet & Discharge Isolation Valves			4
Discharge Check Valves			4
Inlet Control Valves			4
Aeration System Blowers incl. Silencers	2,775	scfm	3
Inlet & Discharge Isolation Valves			3
Discharge Check Valves			3
VFD's	200	hp	3
Biological Aeration System			
Fine Bubble Diffuser System			Incl.
Phosphorus Removal System (if required)		1	
Chemical Storage Tank	9,600	USg	1
Chemical Feed Pumps	112	USgphr	2
Instruments			
Permeate Flowmeters			6
Permeate Header Pressure Transducers			6
Process Tank Level Transmitters			6
Process Tank Level Switches			48
Dissolved Oxygen Sensors			6
pH Transmitters			N/A
Turbidimeters			6.
Turbidimeter Calibration Kits			1

Membrane Blower Flow Switches		4
Aeration Blower Flow Switches		3

Item	Size	Units	Quantity
Permeate Pump Pressure Gauges			6
Membrane Air Scour Blower Pressure Gauges			4
Aeration Blower Pressure Gauges			3
Recirculation Pump Pressure Gauges			N/A
Sludge Wasting Pump Pressure Gauges			6
Control Panel			
PLC-based Control Panel			1
Back-Up PLC			Not Incl.
Electrical			
MCC Panel			Not Incl.
Miscellaneous			
Air Compressor			2
Air Drier			1
Field Service Allowed			Days
Installation Supervision			10
Mechanical Checkout			6
Operator Training			8
Process Start-Up			3
Commissioning			3
TOTAL MAN-DAYS			30
TOTAL No. TRIPS			3
Freight			
Delivery to Site			Incl.

6.0 ATTACHMENTS

Plant Power Consumption and Estimated Yearly Operating Cost

Table 9.1.1 Connected Power and Estimated Power Consumption at Average Day Flow

City of McAllen (ZenoGem) Rev 1

Average Day Flow 8,500,132 USgpd 32,173 m3/day Maximum Day Flow 8,500,132 USgpd 32,173 m3/day

ITEM #		EQUIPMENT DESCRIPTION		# Operating Pumps Blowers etc.	Design Capacity	Discharge Head	Duty Point Efficiency	Equipment Operating BHP	Motor HP	Total Equipment BHP	Total Connected HP	Motor Efficiency %	Equipment kW	Hours / Day Continuous Operation	Energy Cost per year
1	-	Raw Water/Wastewater Screen	n/a	-				-	-	-	-	-	-	24.00	-
2	6.00	Permeate Pumps	By Zenon	6.00	1,109.56 USgpm	35.00 ft	81.00	12.29	20.00	73.76	120.00	90.20	60.98	22.40	37,392
3		Backpulse Pumps	n/a	-	2,880.00 USgpm	30.00 ft	74.00	29.94	40.00	-		-		6 40	-
4		Recirculation Pumps	By Zenon	6.00	3,935.25 USgpm	10.00 ft	55.00	18.35	25.00	110.08	150.00	91.30	89.91	24.00	59,068
5	6.00	Sludge Wasting Pumps	By Zenon	6.00	206.60 USgpm	30.00 ft	50.00	3.18	5.00	19.07	30.00	87.50	16.25	2.00	890
6	-	Reject Water Pumps	n/a		- USgpm	25.00 ft	55.00	-	-	-	-		-	24.00	-
7	4.00	Membrane Air Scour Blowers	By Zenon	3.00	5,520.00 scfm	4.25 psi	n/a	153.32	250.00	459.97	1,000.00	95 00	361.05	24.00	237,213
8	3.00	Process Air Blowers	By Zenon	2.00	2,775.00 scfm	6.00 psi	n/a	114.89	150.00	229.77	450.00	94.20	181.89	24.00	119,501
9	-	Miscellaneous Air Blowers	r/a	-	- scim	6.00 psl	n/a	-	-	-	-	-	•	24 00	•
10	6.00	Anoxic Zone Mixers	By Zenon	6.00			n/a	-		-		80.00		24.00	•
11	3.00	Air Separation System Vacuum Pumps	By Zenon	2.00	22.25 acfm	18.00 ins Hg	n/a	2.25	3.00	4.50	9.00	87.50	3.84	24.00	2,520
12	3.00	Backpulse Sodium Hypochlorite - Metering	By Zenon	1.50	0.066 USgpm	50.00 ft	n/a	0.03	0.03	0.04	0.09	100.00	0.03	3.20	3
13		CIP Wash Pump	n/a	-	- USgpm	30.00 ft	55.00		-	-	-		-	0.03	•
14		CIP Chemical Metering	n/a		USgpm			•		-	-		-		
15	2.00	Chemical Feed #1 System #1 - Metering	By Zenon	1.00	1.140 USgpm	50.00 ft	n/a	0.50	0.50	0.50	1.00	100.00	0.37	24.00	245
16	-	Chemical Feed #1 System #2 - Metering	n/a	-	0.101 USgpm	50.00 ft	n/a	-	0.03		*	100.00	-	24.00	
17		Chemical Feed #1 System #3 - Metering	n/a	-	0.057 USgpm	50.00 ft	n/a	-	0.03		-	100.00		24.00	-
18	-	Chemical Feed #1 System #4 - Metering	n/a	-	0.065 USgpm	50.00 ft	n/a	-	0.02			100.00		24.00	,
18	2.00	Air Compressors	By Zenon	1.00	52.00 scfm	100.00 psi	n/a	18.75	25.00	18.75	50.00	91.30	15.31	6.00	2,515
19	1.00	Air Driers	By Zenon	1.00	75.00 scfm		n/a	-	-			80.00	-	6.00	•
20	1.00	Controls & Instrumentation	By Zenon								1.34		1.00	24.00	657
21	1.00	Miscellaneous	By Zenon								1.34		1.00	24.00	657
		_													
	Total Connected Power 1,812.77 HP														
	•	Total Operating Power		*****	······································			····		916.44			731.64	kW	
	•	Total Operating Cost		*****			···							USS	460,661

Notes

Energy Costs based on

0.0750

US\$ per kW hr

Power Consumption of other plant equipment required (raw water feed pumps, high lift pumps etc.) is not included by ZENON

Where operating efficiencies are not known, the equipment operating power is assumed to be 75% of the motor nameplate power rating

The operating hours for the permeate pump are corrected for the downtime during backpulse cycles (and Membrane Pressure Decay Test Cycles if applicable)

Permeate Pump Backpulses every 15 mins for 30 seconds 1,664 USgpm @ 30.00 ft TDH = 16.59 BHP

Motor Efficiencies indicated are typical only. Efficiencies used are usually within 2% of actual when motor is operating within 50-100% of its full load rating

Operation of Air Compressor is assumed to be only 25% of time

Operation of the Sodium Hypochlorite Pumps is intermittent - operation for 25% of time is used for energy calculation

Blower Energy Consumption Estimated as:

6.536 BHP per 1,000 scfm per psig.

The motor sizes in the above table are preliminary only and estimated based on the information available at the time of preparing this proposal. It must be understood that at the time of proposal preparation, final headlosses or pressure drops in piping systems have not been calculated accurately Motor sizes are subject to confirmation (and if necessary adjustment) during final design. Use of the above information for sizing or selection of any ancillary equipment is entirely at the USER's own risk. Whilst the motor sizes indicated above are ZENON's best estimate based on design criteria assumed during preparation of the proposal, ZENON accepts no responsibility for the absolute accuracy of the information contained herein.

Table 9.2.2 Estimated Total Annual Operating Cost
City of McAllen (ZenoGem) Rev 1
Average Day Flow 8,500,132 USgpd
Maximum Day Flow 8,500,132 USgpd

32,173 m3/day 32,173 m3/day

em			Cost per year	
Electrical Equipment - Zenon		Calculated at Average Day Flow	460,661	US\$
Electrical Equipment - Others			•	US\$
Backpulse Chemicals	Sodium Hypochlorite	Calculated at Average Day Flow	8,232	US\$
CIP Chemical #1	MC-1		220	USS
CIP Chemical #2	Sodium Hypochlorite - 250 mg/L		304	US\$
Chemical #1	Aluminum Sulphate (Liquid @ 48.5%)	Calculated at Average Day Flow	201,764	US\$
Suggested Membrane Accrual			329,311	US\$
Estimated Total Annual Opera	ating Cost		1.000.492	USS

Notes	Backpuise Chemical Consumption		Sodium Hypoc	hlorite
	Sodium Hypochlorite Consumption		71.91	Litres per day
	Sodium Hypochlorite Consumption		26,248	Litres per year
	Sodium Hypochlorite Cost	US\$	0.31	per Litre
	CIP Cleaning Chaminal #1		MC-1	
	CIP Cleaning Chemical #1			
	Design Dosage		_,	mg/L %
	Solution Concentration		50.00	70
	Specific Gravity		1.240	N
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tal	nks)	131.54	Litres
	Total Annual Chemical Consumption		131.54	Litres
	Chemical Cost	US\$	1.67	per Litre
	Chemical Cost	US\$	2.70	per kg
	CIP Cleaning Chemical #2		Sodium Hypoc	hlorite - 250 mg/L
	Design Dosage		250.00	mg/L
	Solution Concentration		10.80	%
	Specific Gravity		1,168	,3
	Wash Frequency		12.00	times / year
		nke\	80.81	Litres
	Chemical Consumption per Wash (all tar	nics)	969.76	
	Total Annual Chemical Consumption	HOP		
	Chemical Cost	US\$	0.31	per Litre
	CIP Neutralization Chemical #1		Sodium Hydro	xide
	Design Dosage			mg/L
	Solution Concentration		50.00%	
	Specific Gravity		1.520	
	Wash Frequency		1.00	times / year
	Chemical Consumption per Wash (all tai	nks)	-	Litres
	Total Annual Chemical Consumption	,	-	Litres
	Chemical Cost	US\$	0.36	per Litre
	Chemical Cost	US\$	0.47	per kg
	CIP Neutralization Chemical #2		Sodium Bisulf	
	Design Dosage		·	mg/L
	Solution Concentration		38.00%	
	Specific Gravity		1.290	
	Wash Frequency		12.00	times / year
	Chemical Consumption per Wash (all ta	nks)	-	Litres
	Total Annual Chemical Consumption			Litres
	Chemical Cost	US\$	0.06	per Litre
	Chemical Cost	US\$	0.55	per kg
	Chemical Feed System #1		Aluminum Sul	phate (Liquid @ 48.5%)
	Design Dosage		90.00	
	Solution Concentration		48.50	%
	Specific Gravity		1.335	70
			4,472.10	Litres per day
	Chemical Consumption Chemical Consumption		1,632,315	
	Chemical Consumption	US\$	0.12	
				•
	Chemical Cost	US\$	0.19	per kg

12/07/1999 : 3:59 PM

PROPOSAL





845 Harrington Court, Burlington, Ontario, L7N 3P3 Tel. No.: (905) 639-6320 Fax No.: (905) 639-1812

DATE:

November 29, 1999

PREPARED FOR:

CH2M Hill

ATTENTION:

Mr. Jim Lozier

FROM:

Roland Lamoca

Re:

McAllen South WWTP

ITEMS COVERED:

Packaged water treatment plant incorporating Reverse Osmosis treatment.

The plant is to be designed for three trains, each with an effluent flowrate of 2.3 MGD of final product from the Reverse Osmosis system. The projected recovery rates from each unit operations have been established in the specifications provided CH2M Hill and are estimated at 80% - 85%.

The preliminary design criteria are:

One Reverse Osmosis Train

Effluent Flow (MGD)

2.3 MGD

System Recovery (%)

80 - 85 %

SCOPE OF SUPPLY:

Three Reverse Osmosis System Trains - Each:

- eighty-eight (88) 6 element long membrane pressure vessels, 400 psi rating, arranged in a 50:28:10 array configuration for optimal cross-flow conditions.
- five hundred twenty eight (528) Hydranautics spiral wrap high rejection type membrane modules. Six membrane elements will be installed in each membrane pressure vessel. A total membrane area of 192,720 ft2 is supplied,
- one (1) duplexed 5 micron prefiltration cartridge system, isolatable for cartridge replacement,
- one (1) horizontal, split case centrifugal-type feed supply pump, 1880 USgpm @530 ftH, 1780 rpm TEFC, Goulds or equal,

PROPOSAL



990153-M

845 Harrington Court, Burlington, Ontario, L7N 3P3
Tel. No.: (905) 639-6320 Fax No.: (905) 639-1812

- one (1) sodium metabisulfite chemical injection system with chlorine analyzer, Prominent or equal,
- one (1) antiscalant injection system, Prominent or equal,
- one (1) acid injection system with pH probe and controller, Prominent or equal,
- one (1) lot process instrumentation for the RO system, includes feed conductivity, permeate conductivity, permeate flow transmitter, concentrate flow transmitter, concentrate pressure transmitter, membrane feed pressure transmitter, permeate pressure transmitter, feed supply residual chlorine analyzer, and feed supply pH.
- one (1) lot process valves for the RO system, Bray or equal,
- one (1) lot process low pressure piping Sched. 10 304 SS,
- one (1) lot process high pressure piping Sched. 10 316 SS,
- one (1) NEMA 4 PLC based control panel (Allen Bradley PLC complete with PanelView Operator Interface),

One Reverse Osmosis System Clean In Place Tank:

• one (1) skid mounted membrane cleaning tank with prefiltration cartridge system, and cleaning pump (316SS Goulds, or equal) and controls,

PRICE ESTIMATE:

US\$ 2,300,000.00

TERMS:

- All pricing in Dollars, FOB ZENON Burlington, Ontario.
- Duty, if applicable, is not included. Any Taxes, if applicable, are extra.
- Shipment shall be 20 24 weeks from receipt of order.
- Payment Terms: 15% with order, 25% on submission of drawings, 50% on equipment shipment, 10% on start-up or thirty days whichever is less, all terms are Net 30.
- ZENON's Terms and Conditions as attached shall apply.
- This is a budgetary estimate only at this time, and does not constitute a binding offer of supply by ZENON.





JAN 18 2000



CH2M HILL/PHUENIX Water for the World

Project Number: 990212-M

FAX:

480 966 9450

ATTN.:

Ms. Fair Miller

CH2M Hill

PHONE:

480 966-8577 x 249

cc:

TO:

Jim Lozier - CH2M Hill Dave Bingham - ZENON cc FAX:

DATE:

18 January, 2000

OF PAGES

(Including Cover): 5

FROM:

Roland Lamoca

Manager, Technical Support Division

Industrial Wastewater Division

SUBJECT: McAllen Reverse Osmosis Operating Cost Estimates - Revision

Hello Fair and Jim;

The operating costs have been revisied based on our discussions today.

The higher pressure we had included previously accounted for a 5 year operation with a 10% flux decline/year. This is typical of ZENON's experience, but may not reflect recent experiences you have noted. As agreed upon, the following have been based on your experiences.

Please feel free to contact ZENON if you have any questions.

Regards,

Roland Lamoca

If you do not receive all pages, please call Lisa Ashton as soon as possible.

ZENON Environmental Systems Inc.

845 Harrington Court, Burlington, Ontario, L7N 3P3 Telephone: (905) 639-6320 Fax: (905) 639-1812 email: rlamoca@zenonenv.comhttp://www.zenonenv.com

This message is intended only for the use of the individual or entity to which it is addressed, and may contain information that is privileged, confidential and exempt from disclosure under applicable law. Any other distribution, copying or disclosure is strictly prohibited. If you have received this message in error. please notify us immediately by telephone, and return the original transmission to us by mail, without making a copy.



Operating Cost Summary

<u>Item</u>	<u>Assumptions</u>	Annual Cost, US\$
Power Consumption	(based on \$0.07 /kW-hr)	\$357,495 /year
Steam Consumption	(based on \$5.00 /1000 lb)	
Membrane Replacement (every 5 years)	(based on current prices, subject to change)	\$190,179 /year
Cartridge Filter Replacement (once per year)	(based on current prices, subject to change)	\$24,637 /year
Annual Process Chemical Cost		\$130,698 /year
Annual Cleaning Chemical Cost		\$15,144 /year

TOTAL ANNUAL OPERATING COSTS

\$718,152 /year

Water Volume Produced Annually:

(based on 4800 USgpm)

2,522.9 Million gallons per year

Operating Cost per Thousand Gallons

\$0.28 /1000 gallons



Operating Cost - Power

Power Consumption

<u>Unit</u>	# of units	Power/unit	<u>Total power</u>	
Pre-treatment Chemical Mixers, 0.25 Hp	total of 6	0.2 kW	1.1 kW	
1st Pass - R.O. Process Pump, 260 Hp	total of 3	194.0 kW	581.9 kW	
Reverse Osmosis CIP Pump, 125 Hp	total of 1	93.3 kW	Intermittent use	

RO process pump pressure is 165 psi @ 1883 USgpm each

Total Power	Requirement	583 kW	
Operating period	Days / year	365 days	
	Hours / day	24 hours	
Utility	rate (\$/kW-hr)	\$0.07 /kW-hr	
Annual Power Cons	umption Cost	\$357,495 /year	



Operating Cost - Process Chemicals

Process Chemical Requirements

	<u>Annual</u>		
<u>Chemical</u>	<u>Consumption</u>	Unit Cost, US\$	Annual Cost, US\$
Sulphuric acid	10374 USgallons	\$0.04 /ib	\$5,745 /year
Sodium bisulphite	12288 USgallons	\$0.25 /lb	\$2,594 /year
Antiscalant	9892 USgallons	\$3.27 /litre	\$122,359 /year

Annual Process Chemical Cost

\$130,698 /year

Operating Cost - Cleaning Chemicals

Cleaning Chemicals / Preservative Requirements

<u>Chemical</u>	<u>Annual</u> Consumption	<u>Unit Cost,US\$</u>	Annual Cost, US\$
Organic Acid: MC-1	3788 kilograms	\$2.29 /kg	\$8,658 /year
Alkali Surfactant: MC-4	568 kilograms	\$3.06 /kg	\$1,738 /year
Sanitizer: MP-1	947 litre	\$5.01 /litre	\$4,748 /year

Annual Cleaning Chemical Cost

\$15,144 /year

ltem		ZenoGem'		ZeeWeed*
Fine Screening	\$	20,000	\$	20,000
ZenoGem* / ZeeWeed* System*	\$		\$	5,075,000
Bioreactor/Equalization / ZeeWeed Tanks	S	1,307,808		162,468
Sid-and Colore	 *	1,007,000		102,400
Installation	\$	2,155,000	\$	1,268,750
Installed Costs Subtotal	\$	12,102,808	\$	6,526,218
ZenoGem / ZeeWeed Equipment Building	\$	288,000	\$	84,000
Installed Costs and Building Cost Subtotal	\$	12,390,808	\$	6,610,218
Unit Process Noncomponent Costs				
Yard Piping Allowance (10%)	\\$	1,239,081	\$	661,022
Site Electrical Allowance (8%)	\$	991,265	\$	528,817
Site I&C Allowance (5%)	\$	619,540		330,511
Site Civil Allowance (5%)	\$	619,540	\$	330,511
Unit Process Subtotal	\$	15,860,234	\$	8,461,079
Contingency (10%)	\$	1,586,023	\$	846,108
Contractor Overhead & Mark-up (10%)	\$	1,586,023	\$	846,108
Total Construction Cost	\$	19,032,281	\$	10,153,295
Engineering & Administration (15%)	\$	2,854,842		1,522,994
Total Capital Cost	\$	21,887,123	\$_	11,676,289
Total Capital Unit Cost (\$/1,000 gallon)	\$	9.28	\$	4.95
Amortized Capital Cost (20yr @ 6.5%)	<u> </u>	1,986,396	<u> \$ </u>	1,059,698
Operation & Maintenance Costs				
Major Chemical Costs				
Backpulse Chemicals: Sodium Hypochlorite		8,232	\$	8,232
CIP Chemical #1: MC-1	1 \$	220	\$	3,211
CIP Chemical #1: MC-1 CIP Chemical #2: Sodium Hypochlorite (250 mg/L)	\$	304	\$	4,435
CIP Neutralization Chemical #1: Sodium Hydroxide		304	\$	175
CIP Neutralization Chemical #2: Sodium Bisulfite	\$		\$	117
On Modulatedion of Chical #2. Oodian Sibanic			<u> </u>	
Major Power Costs				
Screening	\$		\$	
Aeration Basins	\$		\$	419,000
Permeate Pumps	- \$	37,392	\$	36,901
Recirculation Pumps	\$	59,068	\$	74,500
Sludge Wasting Pumps	\$	890	\$	
Membrane Air Scour Blowers	\$	237,213	<u> \$ </u>	114,440
Process Air Blowers	\$	119,501	\$	<u> </u>
Anoxic Zone Mixers	\$		\$	
Air Separation System Vacuum Pumps	\$	2,520	\$	2,520
Backpulse Sodium Hypochlorite - Metering	\$		\$	
Chemical Feed #1 - Metering	\$		\$	
Air Compressors	\$	2,515	\$	2,515
Air Driers	\$		\$	
Controls & Instrumentation Miscellaneous	\$	657 657	\$	657 657
MISSORIBITEOUS		- 057	Ψ	
Membrane Replacement Costs	\$	329,311	\$_	190,905
Labor	\$	280,800	\$	218,400
Table Association & Market State Control		4.070.500	•	1 076 070
Total Annual Operation & Maintenance Cost	\$	1,079,528	\$	1,076,672
Total Annual O&M Unit Cost (\$/1,000 gallon)	\$	0.46	\$	0.46
Total Annual Cost	\$		\$	2,136,370
Total Annual Unit Cost (\$/1,000 gallon)	\$\$	1.30	\$	0.91

DEMONSTATION TESTING OF ZENOGEM AND REVERSE OSMOSIS FOR INDIRECT POTABLE REUSE

FINAL TECHNICAL REPORT ADDENDUM

City of McAllen, TX

by

James C. Lozier, P.E. and Angela M. Fernandez, E.I.T CH2M HILL

Cooperative Assistance Agreement No. 98-FC-81-0073

Desalination Research and Development Program Report No. 51 February 2000

U.S. DEPARTMENT OF THE INTERIOR
Bureau of Reclamation
Technical Service Center
Water Treatment Engineering and Research Group

Draft and Final Report Comments

D-8230 ACM-1.10

Mr. James C. Lozier, P.E. Project Manager, CH2M Hill 1620 Fountainhead Parkway Suite 550 Tempe AZ 85282

Re: Agreement Number 98FC810073, Desalination Research and Development Program Report No. 51, Draft Report Review Comments

Dear Mr. Lozier:

Thank you for presenting the data and results from the project titled "Demonstration Testing of Zenogem and Reverse Osmosis For Indirect Potable Reuse" on December 14, 1999. Ms. Angie Fernandez also deserves to be recognized for her valuable assistance in both the presentation and in overseeing the piloting activities.

Attached, for your consideration are select comments, both editorial and technical, which I believe will strengthen the final report's technology transfer capability.

If you have any questions on these comments, please do not hesitate to call at 303 445-2254.

Sincerely,

Robert A. Jurenka, P.E.

Attachment

cc: D-7810 (Mulligan)

cc: Mr. Wm. Bart Hines, City of McAllen TX,

bc: D-8230 (Price, Jurenka)

Review Comments, "Demonstration Testing of Zenogem and Reverse Osmosis For Indirect Potable Reuse"

City of McAllen TX,

Cooperative Agreement No. 98-FC-81-0073

The following are suggested editorial comments:

- 1. Complete the acknowledgment page
- 2. Complete all missing appendices
- 3. Page 1-7: Shouldn't the last paragraph be indented?
- 4. Page 1-8 second line: delete "should".
- 5. Page 3-3, section 3.2.1: To the second paragraph:

 Third line, delete "...can (or may)" and replacewith

 "may":

4th line: add of after "value" and delete the parentheses;

5th line: move ">3 months" ahead of "infrequently" and replace"during" with "at";
7th line: replace "insitu" to "in situ"

- 6. Section 3.2.2, last line: delete the parentheses.
- 7. Page 3-7: section 3.3.2:
- a. second paragraph: The lat 2 sentences seem redundent considering the previous section. Can they be rephrased?
 - b. third paragraph antiscalent is mispelled.
- c. 5^{th} paragrpah: replace in the 3^{rd} line, "can (or may)" with "may".

The following are recommended technical comments:

1. Page 1-1:

- a. To the first paragraph, add: This Program sponsors research in an effort to lower the cost of treatment technologies.
- b. The second paragraph describes UV treatment (also listed on page 1-5), however, there is nothing in the conclusions regarding it. Obviously the decision was made to use chloramines both in the pilot and in the projections of costs at full scale. Add sentences in the report describing why this disinfectant technique was replaced.

- c. Second paragraph, last sentence: define "intended purpose".
- d. Restructure the 4^{th} paragraph by either using a colon and numbering the items, or make each point a separate sentence.
- 2. Page 1-3, re: El Paso Texas paragraph: Add to the end of the next to the last sentence..."because the increased pumping is lowering the aquifer level to the higher salinity water source."
- 3. Page 1-4: In section 1-2 the second sentence: It is recommended that "...from the Rio Grande River, water rights that it shares with multiple parties, including..." be replaced with, "...from water rights in the Rio Grande River that it shares with multiple parties including ..."

4. Page 1-6: Section 1.5.1,

- a. second bullet: List the WWTP effluent limits (as shown on page 4-1, section 4.1.1) and reference the table, by table number and page number, of the final values.
- b. The term maintenance clean or acid maintenance clean is used here and on pages 1-7, 1-9, 3-3, etc. Define this term prior to its use or add as a reference the page number where it is defined.

5. Page 1-7:

a. First point: At the start of this point, replace "Flow Peaking" with "Flow peaking tests were run over a 24 hour period of time to simulate the types of peak loading conditions that typically occur in a conventional wastewater treatment plant. However, this (significantly)...

Also, at the end of this point add, "As a result, additional means must be provided such as ?? to ensure that slower changes in loading occur to give the membrane bioreactor system time to react to the change in loading."

- b. Second Bullet: Clarify what "intermittent aeration" is. Delete the words, "treatment conditions resulting in".
 - c. Third bullet: Add a reference to the table of results.
- d. Add a fourth bullet with the following: Per Table 5-16, Zenogem permeate was of lesser quality and the RO permeate was of greatert quality than the City's existing raw water source.
 - e. To the end of the fourth bullet add the following

sentence: However, the RO system always removed any remaining coliform regardless of the MF or UF pretreatment. Also, add the table number and page on which it can be found for the results supporting this conclusion.

- f. Add one last point about how cost effective and how much smaller the footprint area is as compared to a conventional treatment system.
- g. Section 1.5.2 RO System, Bullet 1, $4^{\rm th}$ line: Add "in the predominant form of monochloramine..." after "Continuos disinfection..." Also, add the table numbers and pages on which to be found for the results supporting this conclusion.

6. pages 1-7 and 1-8,

- a. RO System, bullet 2: If 80% is "higher" as stated, state what the normal or target recovery rate is. Also, clarify why the 80% recovery rate is described differently between bullet 2 and bullet 3. (I.E. higher vs design).
- b. RO System, bullet 3: Will blending the RO product water with Zenogem product water be acceptable in terms of final effluent quality? With MF not retaining all viruses, isn't there a concern over exposure to small viruses? Also, specify what type of limits are being described on page 1-8, line 2.
- c. Section 1.6.1.4 Replace the first sentence with: "This research project tested one MBR product, Zenon Corporations ZenoGem MF system The ZenoGem UF system should be retested at the 10g/L MLSS level. Also, other..."
- d. Section 1.6.1.4: Add to the end of this paragraph: "The Bureau of Reclamation is currently funding Montgomery Watson and the City of San Diego to perform research testing of this type, comparing the performance of ZenoGem and Mitsubishi systems.
- e. Section 1.6.2.1: add the approximate concentration of an aluminum based coagulant to complete the words in parentheses.
- f. Section 1.6.2.2 After the last word, "feasible", add "if the scale control can be resolved as discussed herein."
- 7. Section 2: There are many other RO treatment objectives which the Bureau would like to see listed. As shown in Jim's presentation graphic, these include:
- a. RO Feed: RO feed must be < 2 ntu; SDI<3; and heterotrophic plate count <500 cfu/ml.
- b. McAllen discharge limits: TSS<0.5 mg/L; CBOD5 <10 and NH3n <3 mg/L.</pre>

- c. Reliability of Operation
- d. RO concentrate: Determine the impacts of the RO concentrate.
- 8. Page 3-1: Add consistency so that all figures are called figures and not exhibits.
- 9. Can a vacuum pump be added to Exhibit 3.2?
- 10. Page 3-3, section 3.2.1:
- a. State the complete downtime to the system for the backpulsing that occurs every 10 minutes? State the complete downtime for the maintenance cleans described as at least 75 minutes? Add the total downtime from the backpulsing and the maintenance cleans and clarify if a full scale plant must be slightly oversized to produce a given flowrate (ie plant reliability factor of 90-95%).
- b. Define permeation in the first paragrpah, second to the last line.
- c. To the second paragraph's 9th line: delete the first "membrane" in this line. Also, clarify ..." clean membrane initial level". Is the post-chemically cleaned TMP level reduced to a clean membrane level or restored to a new membrane level.
- 11. Page 3-4, 3rd line: Replace "The RO" with "The thin film composite RO". Section 3.2.3: Change the last sentence to read: This allows for a higher organic loading of wastewater in the treatment system.
- 12. Page 3-5: Specify the micron rating of the cartridge filter in the second line of the second paragraph. Also, in the second paragraph's $4^{\rm th}$ line, delete the first two "ands". Lastly, can the cleaning skid be shown in Exhibit 3.3?
- 13. Page 3-6: Change the TDS sum of ions values for 12/14 and 12/18 to 1465 and 1473. Also, to the second bullet, state the recommended antiscalent from the Hydranautics program.
- 14. Page 3-8: delete the parentheses in the first line. Also, clarify why in the last line, "Zenogem system" is in parentheses.
- 15. Page 3-9: Define stages A through D.
- 16. Page 4-1: Secton 4-1 item 4: Where in the report are the results of each of these tasks? Where are the air requirements summarized for the process for cleaning and for nutrient consumption?

- 17. Tables 4.1 and 4.2: Clarify under responsible party, what WWTP and WTP really means (ie who)?
- 18. Page 5-7: Add a figure, after Exhibit 5.2, of a complete project timeline that shows both the Zenogem and the RO stages. Then to all of the RO performance figures, modify the timeline hours to match this new complete timeline (ie RO start at 1200 hours instead of 0 hours). This will eliminate confusion arising from the fact that stages A-D differ depending on the equipment.
- 19. Section 5: Can a nitrification rate be determined and added? Also, on Page 5-8, from line 6 replace the second paragraph with:
- Table 5.5 presents the target and average operating conditions for th ZenoGem system during Stage C operation. At the beginning of this stage (after 1,783 hours of operation), the MLSS concentration was decreased to 10 g/L. From 4,130 to 4,158 hours (Event 3) and from 4,225 and 4,326 hours (Event 4) of operation, the permeate flow rate was increased by 46 percent (6.5 to 9.5 gpm) for a period of 6 hours (flow peaking) over a 24-hour period to simulate the types of hydraulic peak loading that typically occur in a conventional wastewater plant. This was done to determine if the MBR system could be operational in the same manner or if additional means would have to be provided to ensure slower changes in the loading to give the MBR time to react to the change in loading. After 4,876 hours of operation, the membrane module height was raised (Event 6) to minimize sludge accumulation in the module aerators during non-aeration periods. From 4,894 to 5,136 hours (Event 7) of operation, air was cycled to the membrane tank at an applied rate of 30 scfm for 10 seconds on and 10 seconds off to evaluate the effect of intermittent aeration on operations and membrane performance. From 5,136 to 5,187 hours
- 20. Page 5-14, Permeability Section: Replace the first paragraph with the following:
- Stages A C. Figure 5.3 illustrates changes in ZenoGem permeability as a function of operating time (TMP is also shown for reference). During Stage B, permeability (normalized to 20°C) steadily decreased as TMP increased, indicating membrane fouling at the higher MLSS concentration of 13 g/L. In contrast, at the lower MLSS concentration in Stage C, permeability increased and remained relatively constant as TMP very gradually increased. However during the flow peaking test periods (Events 3, 4 and 8), permeability sharply decreased as TMP increased. This showed that the MBR system must be provided with a means of ensuring slower changes in peak loading. The peak loading can not be raised as quickly over a 24 hour period as fast as a conventional wastewater treatment plant. These results also confirm that ZenoGem operation at 10 g/L MLSS concentration and constant flux provides

for very stable system operation.

- 21. Page 5-48, last paragraph: State why no useful data was obtained from the instruments. Section 5.3.3, RO Water Quality Impacts: Add to this section the table of RO manufacturer's membrane information and data, which Jim had shown in the presentation.
- 22. Page 5-50, section 5.4: Elaborate what is said in the very last paragraph. Define mass loading basis and be very specific here so non-technical readers can understand what is being concluded.
- 23. Page 5-51, section 5-5: change existing to exist in lkine 1. Also, delete the s on parameters in line 7. Lastly add conclusions for the data being displayed in Table 5-16 and for any blending being contemplated.

24. Cost Section 6:

- a. Add text describing the overall conclusions of that can be derived from this study. Would a MBR system be cost effective or not, and under what conditions?
 - b. What labor rate was used in the cost estimates?
- c. Clarify if the costs presented are based to a certain month/year.
 - d. Where is the square footage of the building?

P.02

Bob Jurenka' - Re: RE: McAllen Integrity Report Status

Pagn 1

From:

Bob Jurenka

To:

ibr8dm00:jlozier@[CH2M.com]

Date:

Fri, Feb 25, 2000 1:12 PM

Subject:

Re: RE: McAllen Integrity Report Status

Jim: Michelle is wrapping up the integrity report, having received internal review comments.

After receiving the final McAllen report, here are 4 final review comments which will need clarification. After you read these, lets discuss how best to finalize the report.

- 1.Table 6.1: It is not clear why the Zenogem process needs 1.3M of new tankage,

2. Table 6.1: The economic analysis says @ 6.5% was the rate used. My tables of A/P values show a 7 % value was used.

3. Table 6.1: The total unit cost of \$2.10 per 1,000 is questioned. Explain how this was derived and not 1.98/1000 gallons.

4. Page 6-9, 3rd sentence: Provide more details to better justify the costs associated for new tankage, and the difference between \$1.3M vs \$0.1M for zeeweed.

Thanks

PS: We are still looking at ways to assist with autopsy work for Sherman. Hope the knee is doing better.

Bob Jurenka, 303 445-2254

Fernandez, Angie/PHX

From:

Fboudkirk@cs.com

ົ າt:

December 20, 1999 12:32 PM

Afernand@ch2m.com

Subject:

McAllen

Angie,

Here are a few editorial comments on the December 7, draft report. Bear in mind that the EPRI folks who take the time to read it will be starting from ground zero and the don't know ZeeWeed from break tank.

Page 1-1, UV is mentioned here but nowhere else in the report. I suggest deleting these references to UV as the project did not address its use.

Page 1-3 first paragraph; for the sake of current info, the San Vincente Reservoir recharge project was killed because of politics. It might be resurrected but as of August, 1999 the politicians killed it claiming it was an Anglo plot to make Hispanics drink dirty water!

Page 3-2. Somewhere we need to have a glossary for abbreviations like CIP. I know what it means but a person not informed about membranes might not. Also the term break tank is not is not self explanatory. On this page we have labeled an aerobic tank in the diagram while in the text a "aeration tank" is mentioned as well as "a 200 gallon calibrated receiving tank." These descriptions should be consistent with the diagram.

ge 3-3. In the first and second paragraphs a "process tank" is mentioned. I eve the words "membrane tank" should be used for consistency's sake. Also in the second paragraph it might be helpful to mention that the maintenance cleaning flush liquid is drained to waste.

The last sentence of this paragraph might confuse a first time reader as it seems to imply that maintenance cleaning is not a part of "normal" operation. I would suggest the sentence read "Maintenance cleaning is done insitu and is necessary to sustain the membrane flux." (Is it insitu or in situ?)

Page 3-4, I think adding the words "For pilot testing" to the beginning of the last sentence of the first paragraph sentence would avoid confusion about how a full-scale system would operate. The terms CBOD5, MLSS, MLVSS, SRT, etc., show the need for a glossary.

Page 3-5, The pore size of the cartridge filter would be informative as would be a few words about why the filter is required.

Page 3-6, I believe the samples were taken in 1998 not 1999 as the charts says.

Page 4-4, Again, since my audience is made up mainly of power plant types who are given job assignments outside their technical field of expertise, I would prefer the last sentence of the first paragraph of section 4.33 to "could adversely affect marine ecology." If that is indeed what we mean.

Page 4-5, ASL should be define in a glossary.

rage 5-18, Here we introduce an other CBOD term which I think is the same as CBOD5. If not it needs to be define in a glossary.

Page 5-20, Ditto for BOD5.

Page 5-52, Some explanation why some chemical element levels in the ZenoGem Permeate are higher than in the raw water would be helpful. Could these be a seasonal variation?

ATTACHMENT 1

Texas Water Development Board Review Comments: City of McAllen Contract No. 99-483-276

Board Staff offers the following comments.

The study shows that effluent, and especially effluent with high hardness and high total dissolved solids, can be brought to drinking water standards for between \$1.24 and \$1.80 per thousand gallons. The study shows that using the Zenon technologies tested, that existing wastewater treatment plant capacities could be significantly increased (doubled or tripled) at costs similar to new plants (under \$1.5 per gallon/day of capacity). Savings may be realized by removing the possible impediments of new construction such as site location and additional distribution lines by utilizing the Zenon technology in existing wastewater treatment plants. The report also shows that Zenon technology can produce a higher quality treated effluent.

Specific recommended changes to the report include:

- 1. Table 5.16 should be modified so that applicable safe drinking water act criteria are included in the table for reference.
- 2. The summary tables of water quality parameters compared to target values shown in the overheads at the Denver meeting should be included in the summary of this report.
- 3. The cost for the micro filtration process, including costs in dollars per thousand gallons should be broken out separately from the RO costs in Chapter 6.
- 4. 4.4.2 Sampling and Analysis: 1st paragraph, 3rd sentence (The WWTP....) mentions one of the samples collected is nitrate/nitrate nitrogen. This is redundant. This should be changed to read nitrate/nitrite nitrogen.
- 5. The Texas Water Development Board should be acknowledged as helping to fund this study.